

Water Transport in PEM Fuel Cells: Advanced Modeling, Material Selection, Testing, and Design Optimization

J. Vernon Cole

CFD Research Corporation

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Project ID: FC030

Overview

■ Timeline

- Start Date: 6/1/07
- End Date: 5/31/12
- Percent Complete: 95%

■ Budget:

- Total Project Funding:
 - DOE share \$ 4,958K
 - Cost share \$ 1,464K
- Funding Received in FY11: \$ 818K
- Planned Funding for FY12: \$ 0

■ Barriers:

- D. Water Transport within Stack
- E. System Thermal and Water Management
- G. Start-up and Shut-down Time and Energy / Transient Operation

■ Partners:

- Ballard Power Systems
- BCS Fuel Cells
- ESI Group, NA
- Techverse
- U. Victoria
- SGL Carbon

Program Objectives => Relevance

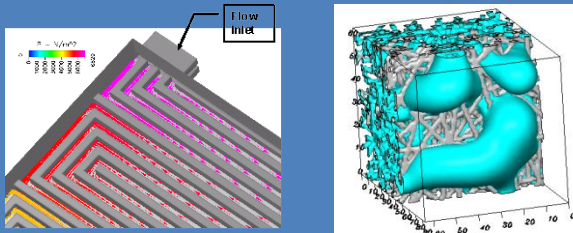
- **Overall:**
 - Improve understanding of the effect of various cell component properties and structure on the gas and water transport in a PEM fuel cell;
 - Demonstrate improvements in water management in cells and short stacks; and
 - Encapsulate the developed understanding in models and simulation tools for application to future systems.

- **FY 2011 and 2012:**
 - Complete cell scale model testing and validation against steady state and transient operational cell data
 - Complete fuel cell water transport model improvements and code package development to include two phase flow
 - Complete validation of water transport model based on data gathered during optimization studies, and make recommendations for water management improvement including operating strategies and GDL materials modification.
 - Data and tools for screening of concepts to improve water management while increasing power densities, mitigating liquid-water induced pressure drops and transients for system-level benefits

Approach

Improved Water Management Through Improved Component Designs and Operating Strategies

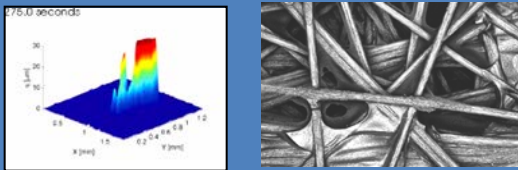
Advanced Model Development (CFD/Lattice Boltzmann Method)



- LBM models for microscale flow through porous media: in-plane and through-plane permeabilities, capillary pressure, and wetting characteristics
- CFD models for macroscopic two-phase flow in channels, GDLs and interfaces, coupled with electrochemical reaction and transport through membrane

Simulations of gas, water and thermal transport in a unit cell complement experiments to develop understanding, evaluate concepts

Experimental Characterization

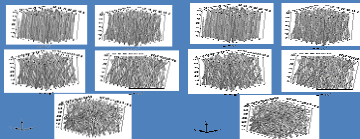


- Ex-situ characterization: key materials properties and sensitivity to treatments, water transport analysis in GDLs and micro-channels
- In-situ diagnostics: current and water distribution

Provides fundamental understanding, validation data for physics-based models from component to cell level

Improved Component and Fuel Cell Concepts

Thickness	Density		
	high	low	
200 μm/8 mil	GDL 24	GDL 25	2 D - paper
300 μm/12 mil	GDL 34	GDL 35	
400 μm/16 mil	GDL 10		3 D - nonwoven



- Cell flooding sensitivity to materials and operating strategies
- Implement and test performance improvement strategies

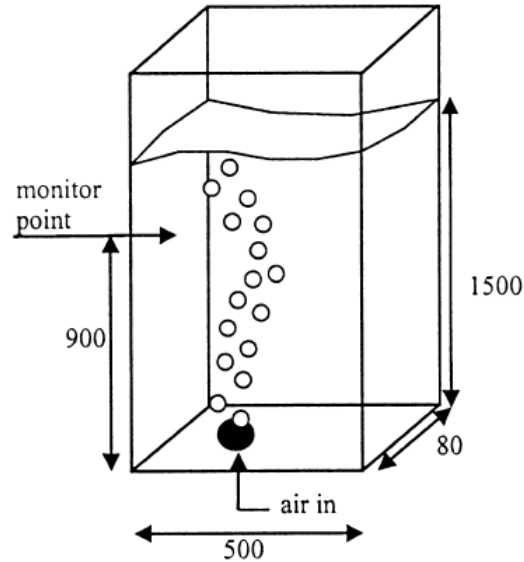
Improved component designs and operating strategies, tools for addressing water transport in future generation designs

FY 11-12 Plans and Milestones

Month/Year	Milestone	Comments	% Complete
Mar 12	Cell scale models tested and validated against steady and transient operational cell data	Steady state results show less mass transfer effect than expected; additional transients needed	90%
Mar 12	Complete fuel cell water transport model improvements and code package development	Source code transferred to ESI, user interfaces complete; test battery of sample models to be executed	90%
May 12	Complete validation of water transport model and make recommendations for water management improvement	Two-phase flow, porous media without capillary pressure complete and model formulation improved	80%

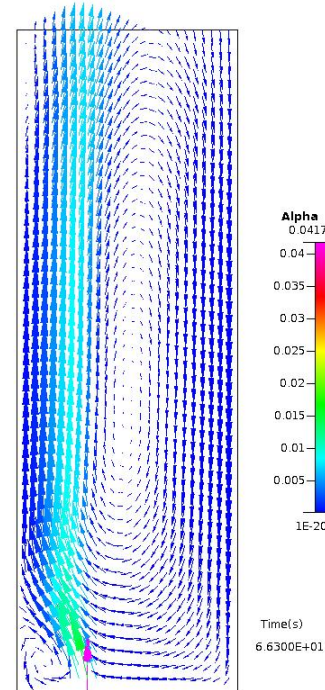
Recent Accomplishments: Model Evaluation: Two-Phase Flow Benchmarks

Bubble Column Experimental Setup



- Air injected at bottom, 1.6 l/min
- Water velocity sampled at the monitor point

CFDRC/ESI Results and Benchmark†



ESI Result

Mudde et al. benchmark results:

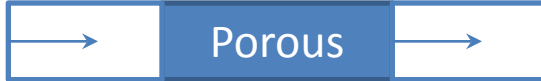
- Steady 0.144 m/s vertical velocity at the monitor point after 40 seconds
- Slightly more gas dispersion, due to symmetry condition instead of outlet at the top

- Good agreement for gas fraction distribution, time scale (45 seconds to steady state) and steady velocity at the monitor point (0.142 m/sec) in 2-dimensional test model

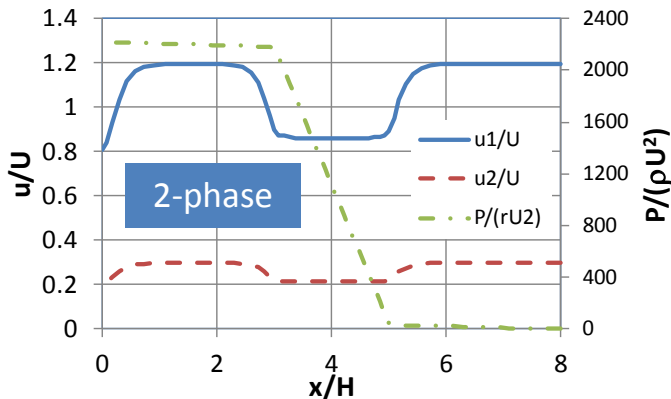
† R. F. Mudde, O. Simonin, 1999, "Two and three-dimensional simulations of a bubble plume using a two-fluid model.", Chemical Engineering Science 54 (5061)

Recent Accomplishments: Model Evaluation: Porous Media Flow Benchmarks

Porous Plug Test Case

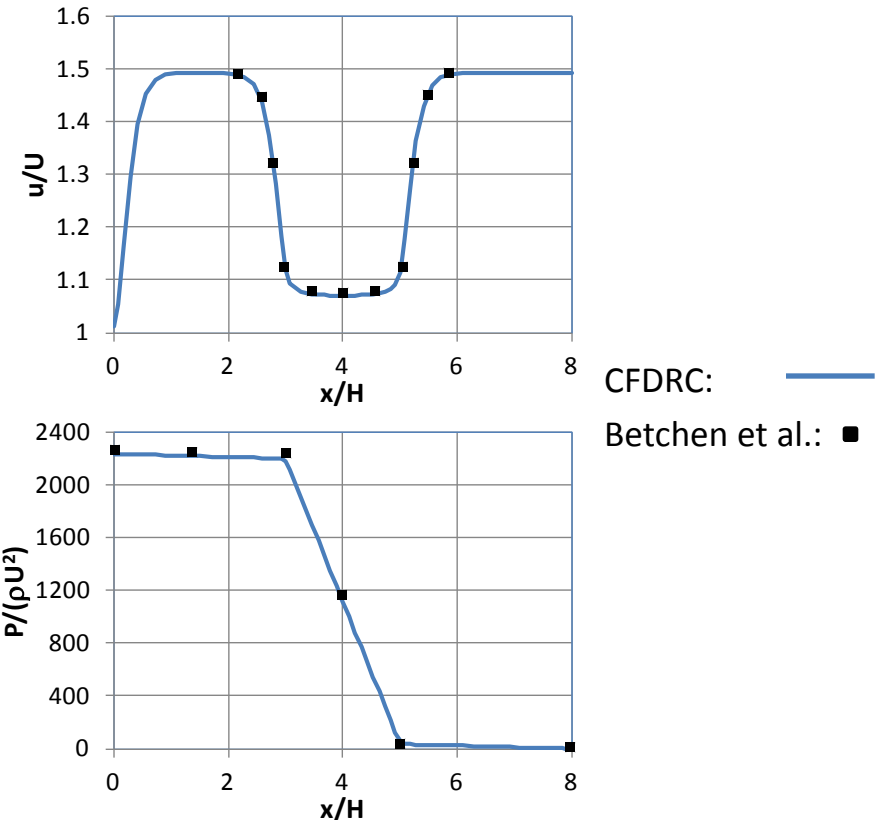


- Channel with porous plug, plug length = $3H$
- Darcy and Forcheimer drag terms included
- $Re=1$, $\varepsilon=0.7$, $Da=10^{-3}$



- Boundary treatment at open/porous interfaces improved to avoid pressure or velocity discontinuities; two-phase for identical fluids (ρ, μ) $\alpha=0.2$

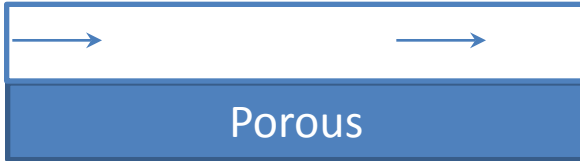
CFDRC/ESI Results and Benchmark†



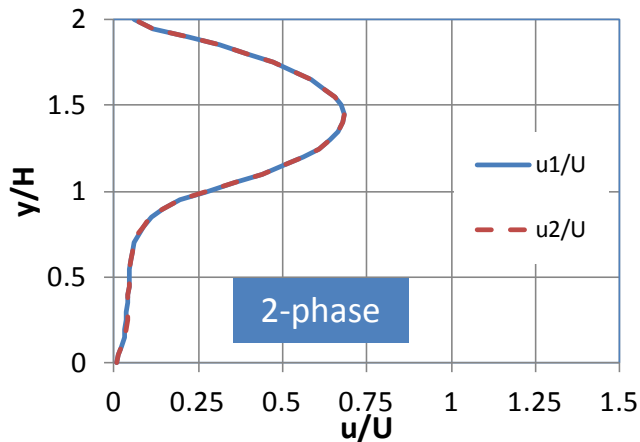
† Betchen, L., et al. "A Nonequilibrium Finite-Volume Model for Conjugate Fluid/Porous/Solid Domains," Numerical Heat Transfer: Part A: Applications 49, 543-565 (2006).

Recent Accomplishments: Model Evaluation: Porous Media Flow Benchmarks

Beavers-Joseph Problem

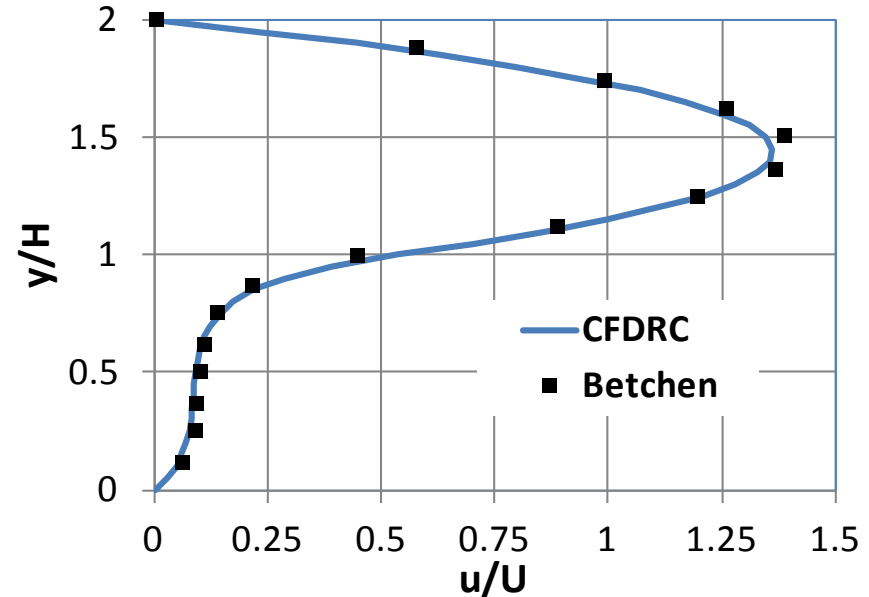


- Channel with porous region
- $Re=1$, $\varepsilon=0.7$, $Da=10^{-2}$



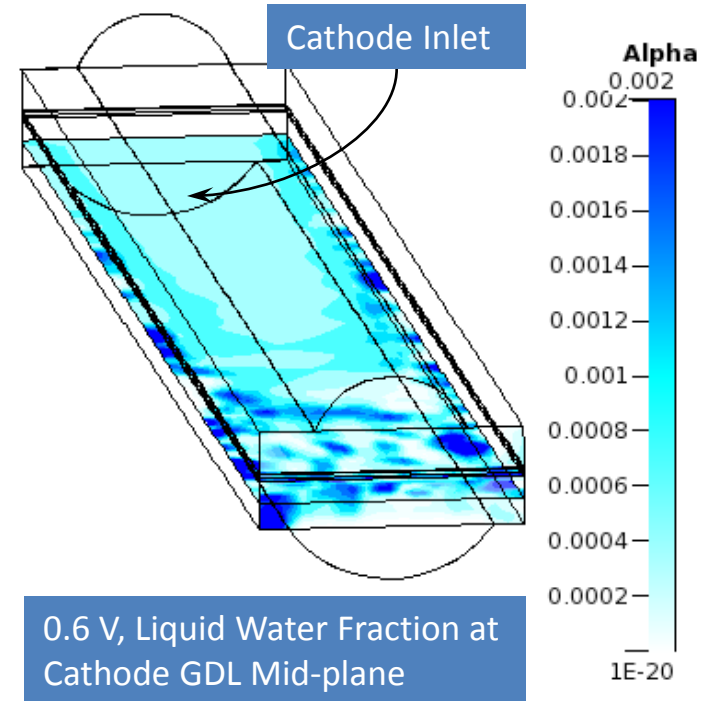
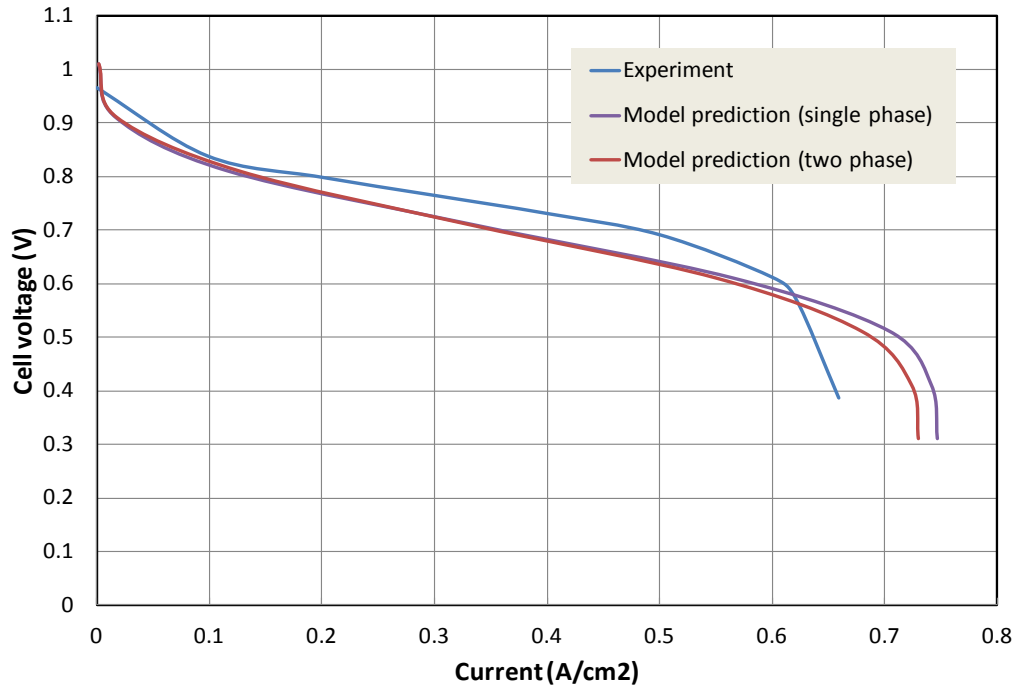
- Good agreement at open/porous interfaces; no pressure or velocity discontinuities; two-phase results for identical fluids (ρ, μ) $\alpha=0.5$

CFDRC/ESI Results and Benchmark†



† Betchen, L., et al. "A Nonequilibrium Finite-Volume Model for Conjugate Fluid/Porous/Solid Domains," Numerical Heat Transfer: Part A: Applications 49, 543-565 (2006).

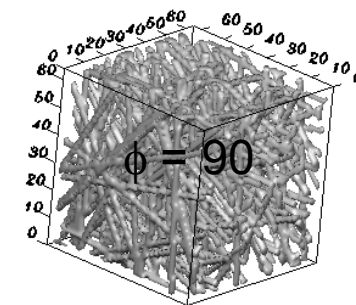
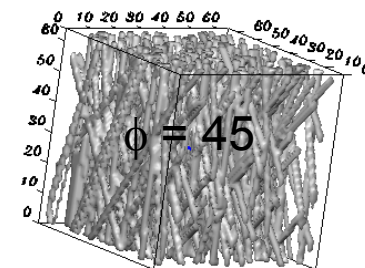
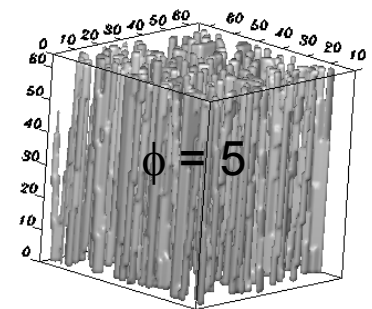
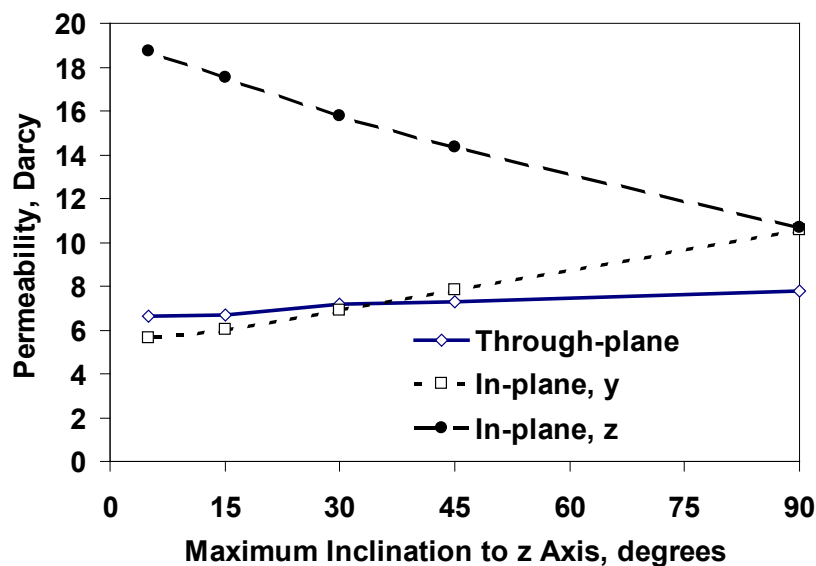
Recent Accomplishments: Model Evaluation: Operational Cell



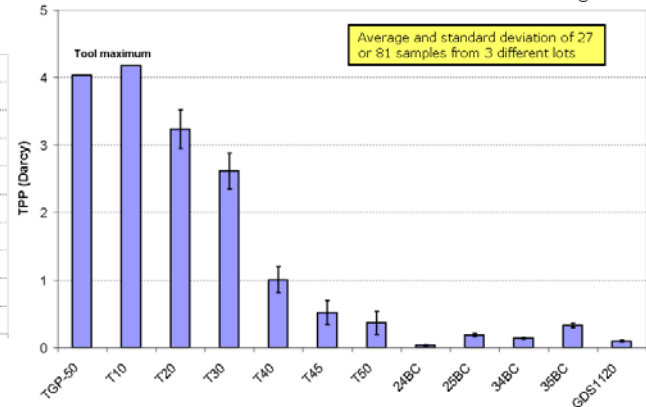
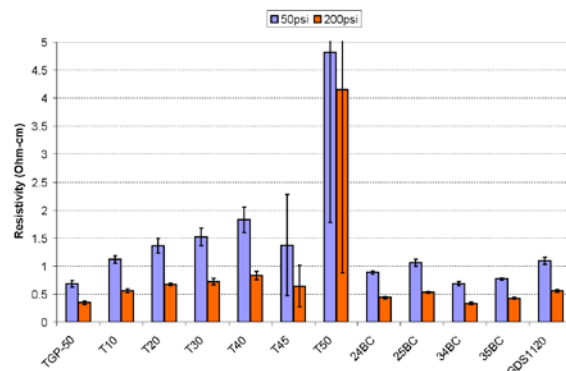
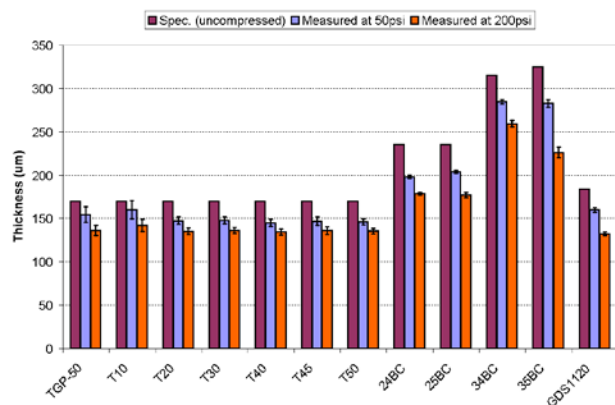
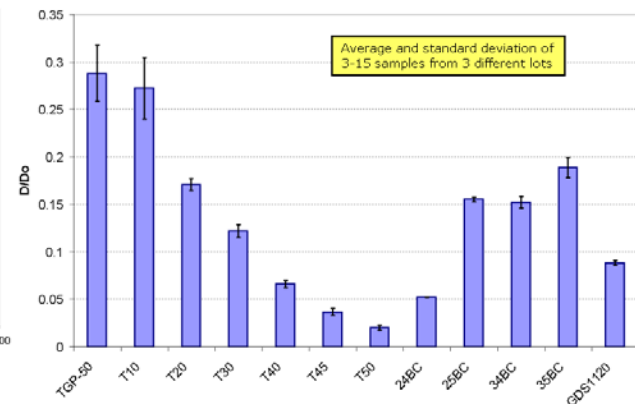
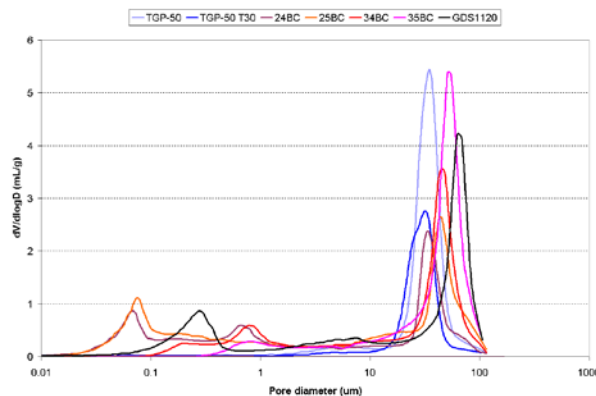
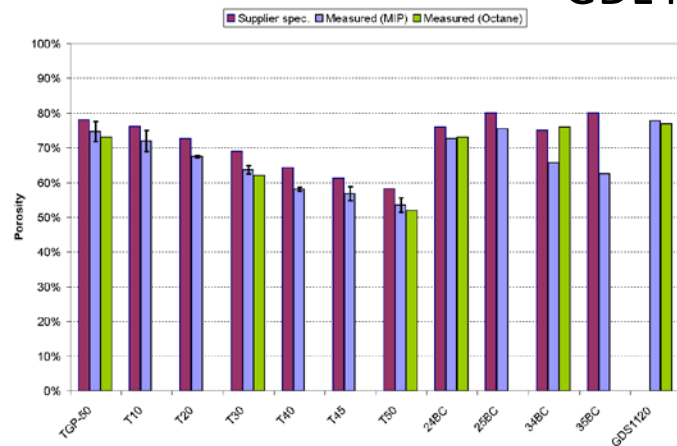
- Testing against characterization data gathered by Ballard in a test fixture operating at high stoichiometry:
 - 60 °C and 100% relative humidity operation
 - Based on measured effective diffusivity, transport limitations at 0.6 A/cm² should be due to only liquid water presence in GDLs and catalyst layers, $\alpha \approx 0.1$ needed with typical water effect on effective diffusivity

Overall Accomplishments: Materials Concept Screening (2008)

- Validated single-phase Lattice Boltzmann Model applied to screen GDL concept with oriented fibers:
 - Predicted possibility of controlling in-plane (transverse versus longitudinal) transport with fixed through-plane transport by modifying GDL microstructure
 - Experimental evaluation of similar work with experimental data supporting potential promise shown at 217th ECS meeting by Jonquille and Pauchet

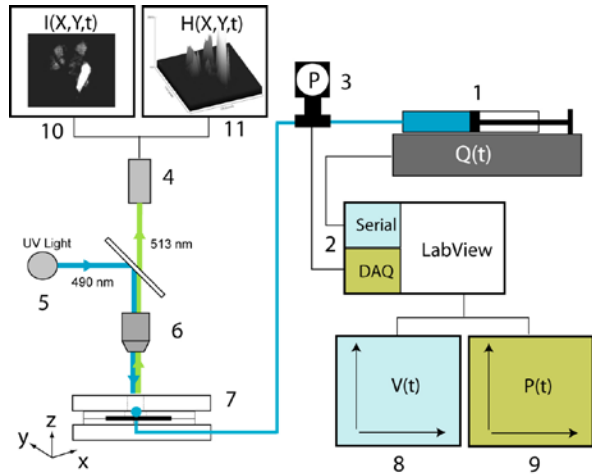


Overall Accomplishments: GDL Materials Characterization (2009)



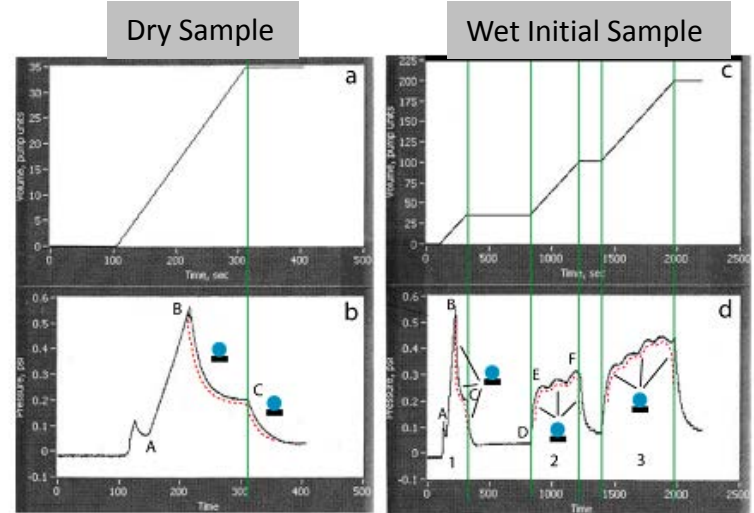
- Key property database established for SGL, BMP & Toray papers with a range of PTFE loadings (Ballard, Techverse):
 - Porosity and Pore Size Distribution (MIP, MSP)
 - In- and Through-Plane Gas Permeability, Effective Diffusivity
 - Electrical and Thermal Conductivity
 - Thickness & Electrical Resistance Variation with Compression

Overall Accomplishments: GDL Water Transport Characterization and Modeling (2009)

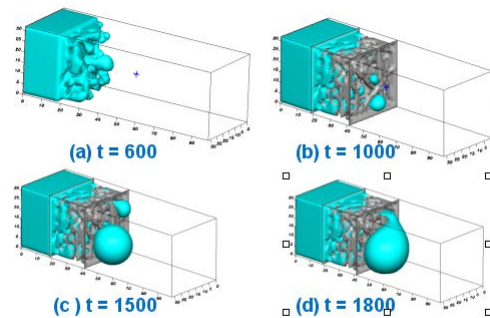


UVic *Simultaneously* monitored the development of the capillary flow, pressure, and volume injection rate of water percolating through the GDL porous layer

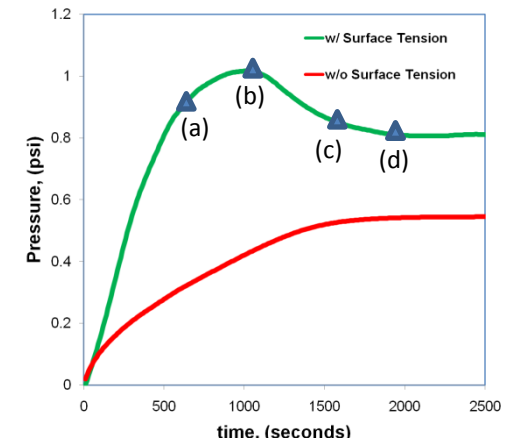
Experimental Observations



LBM Modeling of GDL Transport



Test GDL: porosity 0.75, thickness 100µm.

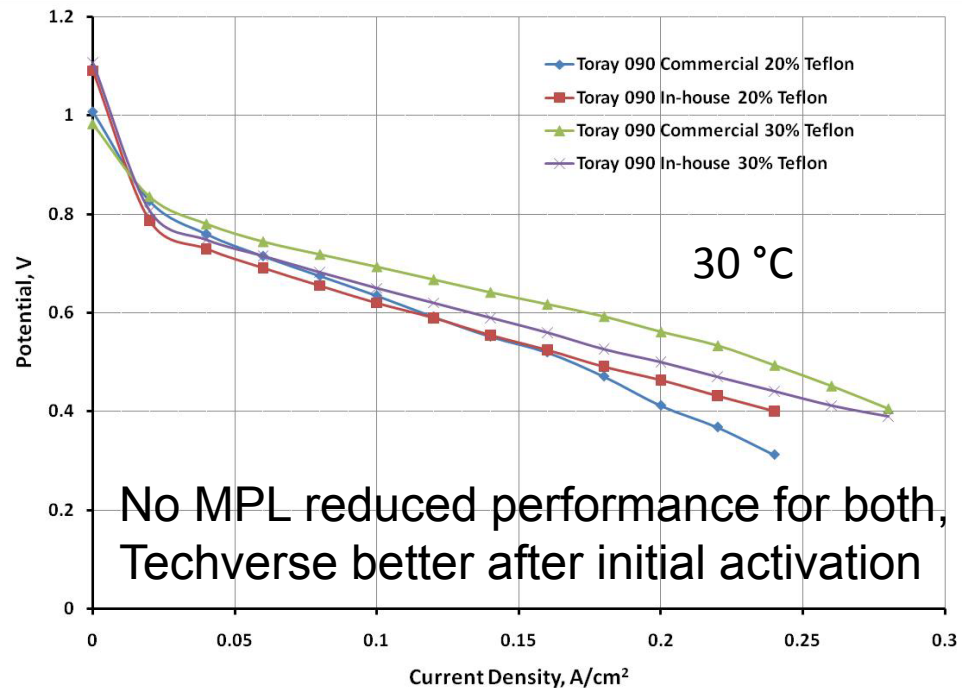


- Preferred channels for water transport, history dependent invasion observed
- 2-Phase Lattice Boltzmann Model predicted similar channeling
- Experiments and LBM guided CFD model formulation

Overall Accomplishments: Electrophoresis for Uniform GDL PTFE (2011)

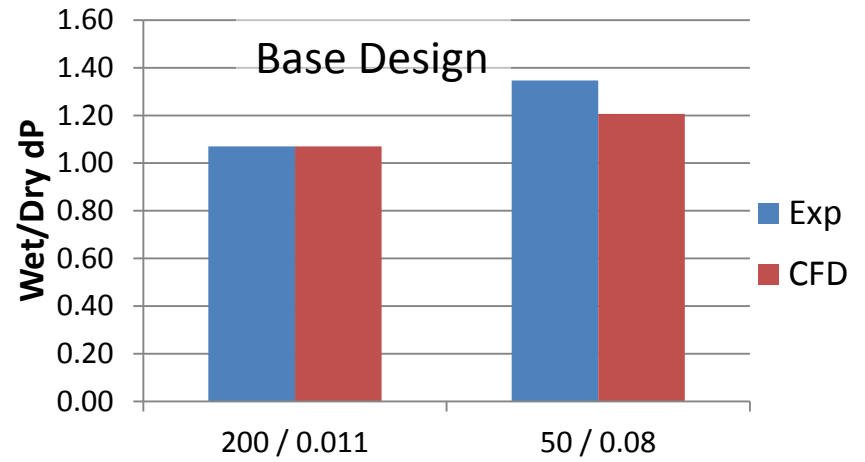
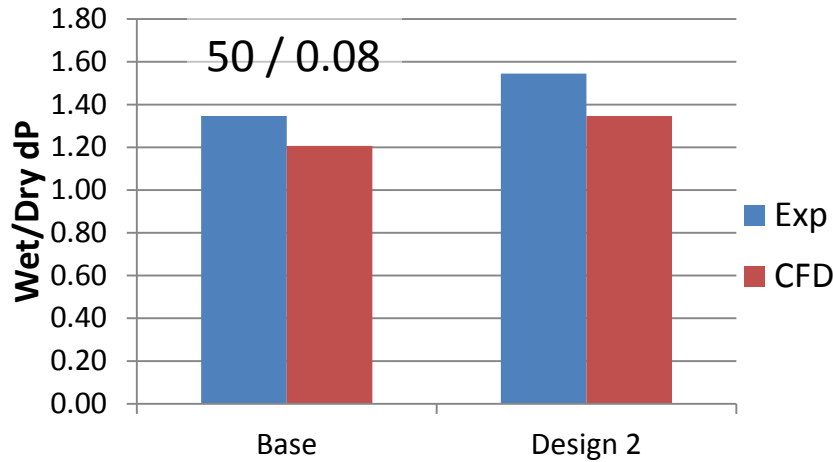
- More uniform PTFE coatings for 10x lower residual saturation (liquid water staying in the GDL), increased hydrophobicity at equivalent loadings.
- Testing at BCS Fuel Cells: Better performance than commercial media at moderate currents despite slight increase in activation losses and/or contact resistance

Sample	Residual Saturation	Breakthrough Pressure
n/a	%	Pa
35 EA - 30% Teflon	15.52	587
35 DA - 20% Teflon	25.54	1077
35 CA - 10% Teflon	7.6	1175
30% in-house AA sample	2.44	1959
7.5% in-house AA sample	2.32	1763
30% in-house A Toray	0.416	4800
15% in-house A Toray	0.6	3400
6% in-house A Toray	0.8	3100
30% in-house B Toray	0.769	3918
18% in-house B Toray	0.9	3300
4% in-house B Toray	1	3100
10% commercial Toray	3.3	780
20% commercial Toray	4	1000
30% commercial Toray	2.5	1100

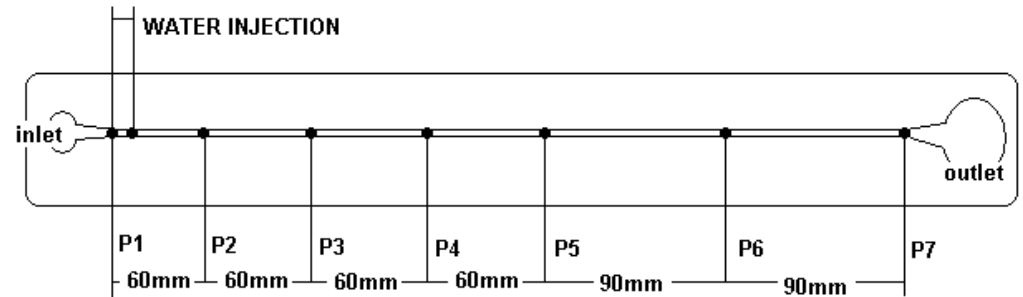
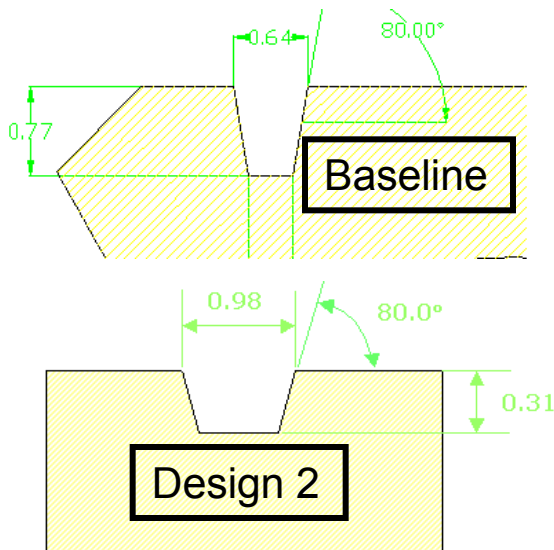


Teflon is a registered trademark of E.I. du Pont de Nemours and Company

Overall Accomplishments: Two-Phase Channel dP with GDLs (2011)



Design Effect



- Ballard Two-Phase dP measurements identified designs with low wet dP and pressure fluctuations
- Models predicted trends with design variation and operating conditions for GDL+channel

Overall Accomplishments: Software Package Summary

ESI is providing the developed and models into the commercial version of CFD-ACE+:

■ Solver capabilities:

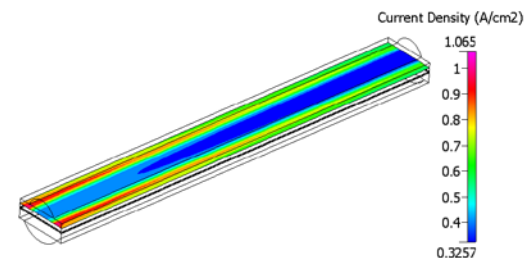
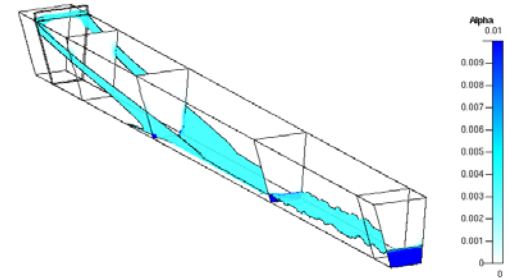
- Improved two-phase flow in fuel cell scale channels, two-phase flow in porous media: demonstrated to predict predict pressure drops in fuel cell GDL+channel assemblies as function of design and operating conditions => impact of channel design and GDL properties on balance of plant requirements, system efficiency
- Liquid water effect on effective diffusivity of reactants in GDL => impact of liquid water content and distribution on performance
- Mass transfer between fluid phases coupled with fuel cell chemistry via electrochemical reactions and evaporation/condensation

■ Model Definition

- GUI for problem setup to specify water transport model options and input parameters (relative permeability, capillary pressure models, liquid effect on tortuosity, etc.)

■ Post-Processing:

- Printed summaries (mass, energy, and chemical species balances) and graphical output (liquid volume fraction, mass transfer rates, liquid phase velocities; in addition to overpotentials, transfer current already provided for fuel cell models)



Interactions/Collaborations

■ Partners

- Ballard Power Systems: Measurement tools, material data, and operational test results to validate and support the development of models for water transport and management; continuing application of the developed models
- Techverse: Materials characterization and modification
- BCS Fuel Cells: Operational cell and stack diagnostics, materials sensitivity and serpentine channel design
- ESI Group, NA: Model implementation and software integration, model testing; commercial release of the developed models
- SGL Carbon: GDL and bipolar plate materials
- U. Victoria: GDL permeation, channel droplet injection and transport quantification

Summary

- Relevance:
 - Effective water management is necessary to improve automotive fuel cell performance, freeze/thaw cycle tolerance, and cold startup times
- Approach:
 - Integrated characterization and model development to advance understanding, application of the resulting knowledge to optimization
- Technical Accomplishments and Progress:
 - Developed and validated both single-phase and two-phase Lattice Boltzmann Models for flow in porous media, applied to screen microstructure design concepts and analyze fundamental characteristics of water transport in GDLs;
 - Characterized GDL materials over a broad range of PTFE treatment;
 - Developed a two-phase cell scale CFD model for analyzing cell components (channel design, GDL effective properties) and predicted cell performance; validated key sub-models for two-phase flows in channels and transport in porous media
 - Predicted design and operating condition sensitivity of observed wet pressure drop with experimental measurements of wet pressure drop for two-phase flows in channels and GDLs;
 - Developed a technique for reproducible, controllable hydrophobic treatment of GDL media