

POWER GENERATION FROM AN INTEGRATED BIOMASS REFORMER AND SOLID OXIDE FUEL CELL

SBIR Phase III Xlerator Program

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INNOVATEK

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Project ID: FC096

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Overview

Timeline

Start: 10-01-2010

Finish: 09-30-2013

2nd Period funding delay until 4-1-2012

33% Complete

Barriers

Cost, Durability & Performance

Targets: H2 production from diverse domestic sources;
distributed power demo 2Q 2018

Year	Cost/kW	Efficiency	Lifetime	Technology
2015	\$1700	42.5%	40,000h	5 kW Dist Gen Sys
2020	\$1500	>45%	60,000h	5 kW Dist Gen Sys

Budget

Total: \$2.3M

Received FY11: \$900K

Planned FY 12: \$650K

Partners

Topsoe Fuel Cell

Washington State University &
PNNL for BioFuel

Energy Technology Services

Relevance: Public Benefits

Environmental Quality & Energy Security

The full benefits from fuel cells are possible only if the feedstock for hydrogen production is a renewable, domestically produced commodity that does not compete in the food chain.

Our technology will address these issues by:

- Helping shift the primary energy source for H₂ from fossil fuels to renewable non-food biomass.
- Using less fuel through high system efficiency by effective thermal integration and off-gas recycling.
- Providing an alternative method for distributed power generation near the source of the feedstock, enhancing grid stability.



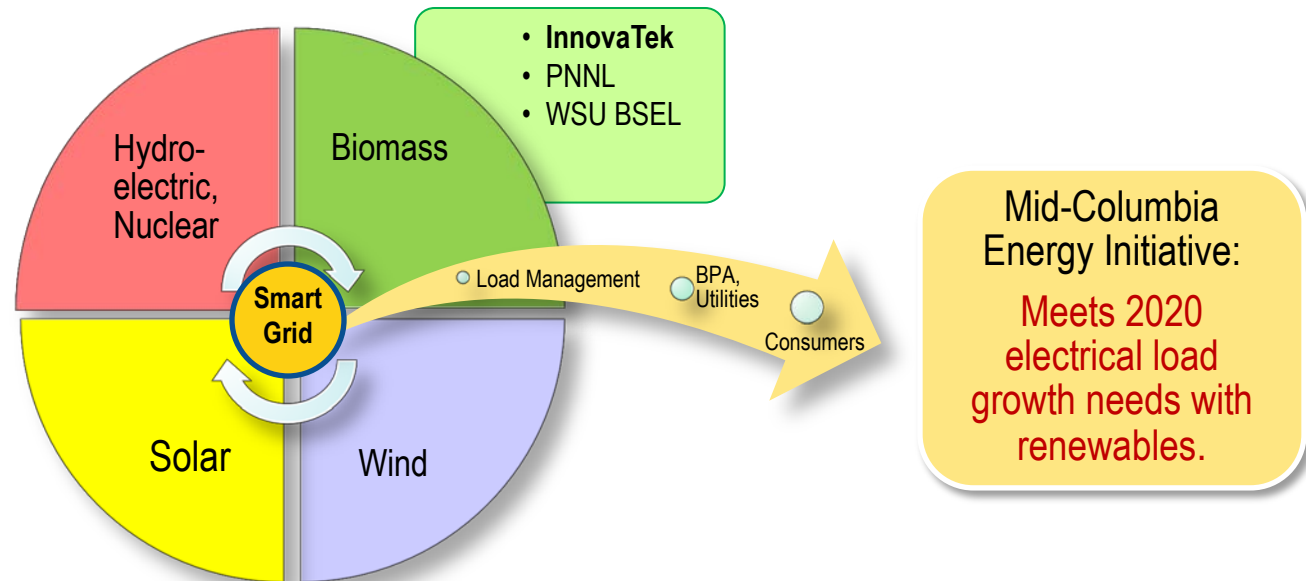
Relevance: Project Objectives

Year	Objective	DOE Barrier Addressed
2011 <i>Complete</i>	Establish design to meet technical and operational needs for distributed energy production from renewable fuels	SOFC power using renewable non-food biomass fuel; codes & standards
2011/2012 <i>50% complete</i>	Design, optimize, and integrate proprietary system components and balance-of-plant in a highly efficiency design.	Demonstration; system efficiency; design for low cost manufacturing
2012 2013 <i>Not started</i>	Demonstrate the technical and commercial potential of the technology for energy production, emissions reduction, and process economics	<ul style="list-style-type: none"> • 40,000 h lifetime • 99% availability • >40% efficiency • \$1700/kW equipment cost

Approach: Project Goal

Develop and demonstrate a fuel cell distributed energy system that operates with 2nd generation biofuel.

- System based on InnovaTek's steam reforming process and SOFC
- Non-food biofuels include pyrolysis oil and bio-kerosene processed locally
- To be demonstrated in Richland's renewable energy park and tied to grid



Approach: Milestones & Go/No Go

Date	Milestone or Go/No Go	Status
Dec 2010	M1: Criteria for design review to confirm compliance with user requirements/ codes & standards	Completed
Mar 2011	M2: 3 rd Party Review completed for System Design and Layout that meets Criteria	Complete for Gen1 continuing for Gen2
Sept 2011	M3: Solid model & CAD drawings complete; OEM components specified & acquired	Complete for Gen1 continuing for Gen2
Dec 2011	Go/No Go: Laboratory prototype system produces power from biofuel	Achieved for Gen1
July 2012	M4: Achieve 40% system operating efficiency	In progress
Aug 2012	M5: System performance proves superior energy efficiency & emissions reductions compared to conventional technology	In progress
Sept 2012	Go/No Go: Analysis of process economics supports commercial feasibility	Not started

Approach: Core Technology

InnovaGen® Fuel Processor



- Creates hydrogen from a range of liquid and gaseous fuels with high energy density
- Proprietary catalyst & hardware
- Water neutral steam reformer
- Compact and efficient

Topsoe Solid Oxide Fuel Cell



- 1.5 kW, 80V DC, 0-25 A
- 340mm x 200mm x 200mm
- 67% fuel utilization
- 750°C
- 20 kg



Uses Bio-kerosene made from wood sawdust and non-food camelina



Accomplishments: Established System Requirements & Specifications

Address DOE Barriers for Codes & Standards, Field Demonstration

- **Technical, operational, & safety requirements defined**

- **Energy Technology Services provided advice and 3rd Party Oversight, including regulatory codes & standards**

- NFPA 30 - CSA FC1 - CFR 47 FCC
- NFPA 853 - ASME PTC 50 - IEEE 1547
- NFPA 70 NEC - UL 1741

- **City of Richland Utilities established demo requirements**

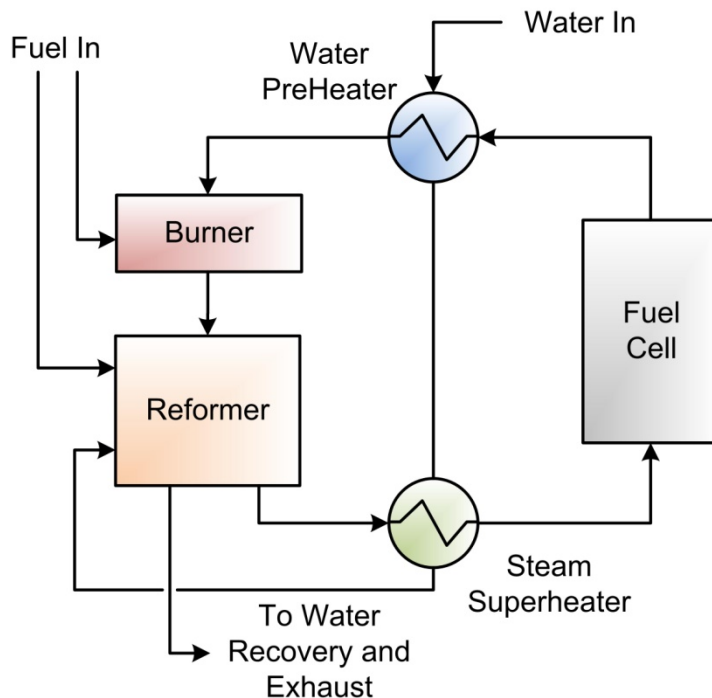
- Milestone 1** → • **Developed System Requirements Document based on CSA-America FC1 – *Stationary Fuel Cell Power Systems***

- *Kelvin Hecht, Consultant*

- **Developed Draft FMEA**

Progress: Completed Process & Component Modeling and Simulation

Use process simulation tools, CFD & FEA to develop optimal designs for chemical conversion and heat transfer.

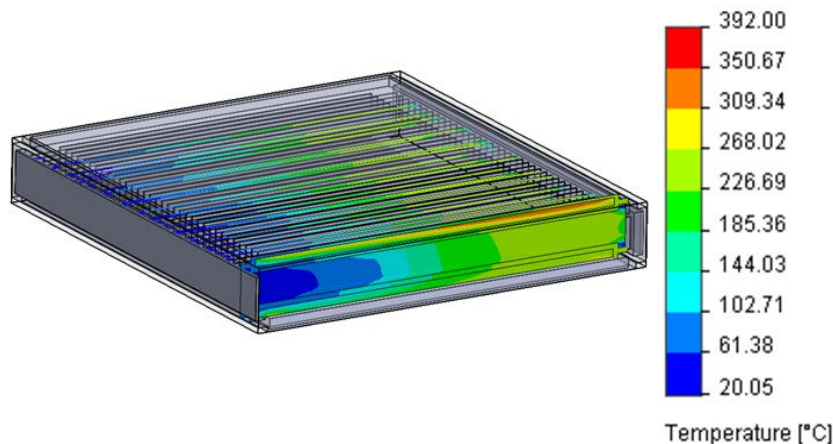


CFD simulations used to design core fuel processor components and identify critical design features to help balance:

- Heat Transfer
- Thermal Stresses
- Pressure Drop
- Desired flow patterns

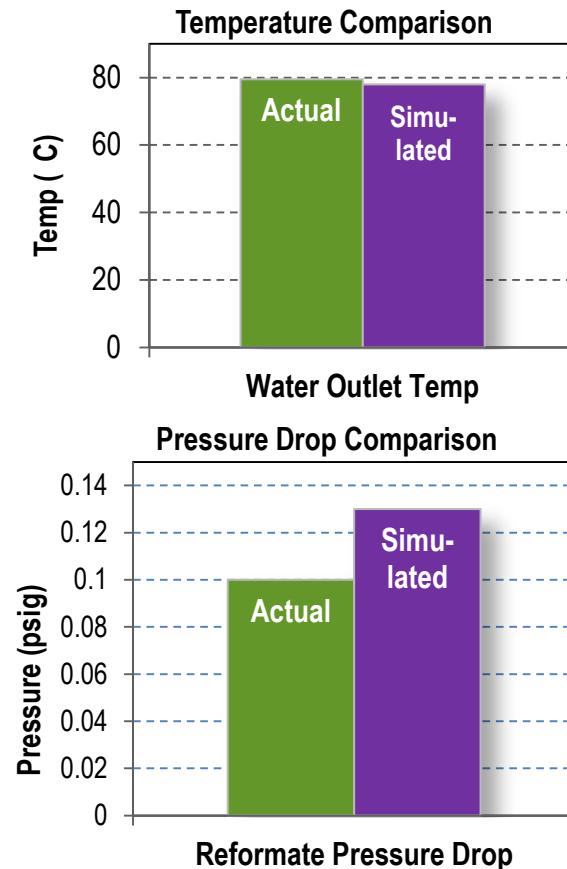
Progress: Component Modeling & Simulation used for design optimization

**Microchannel Heat Exchanger:
Pre-heats process water and cools
anode off-gas in cross flow design**



- **Simulation verified that pressure drop across channels meets design criteria;**
- **Design results in high heat transfer density, meeting performance criteria.**

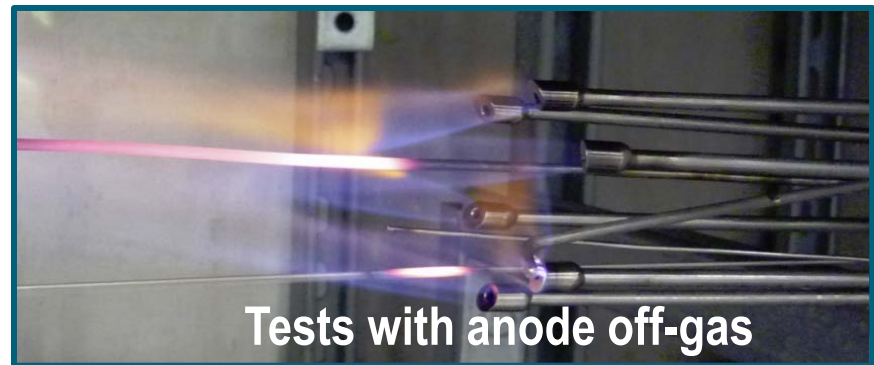
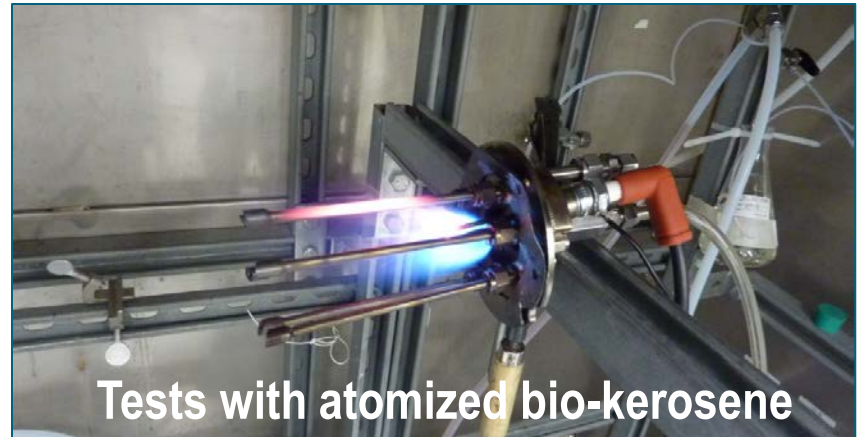
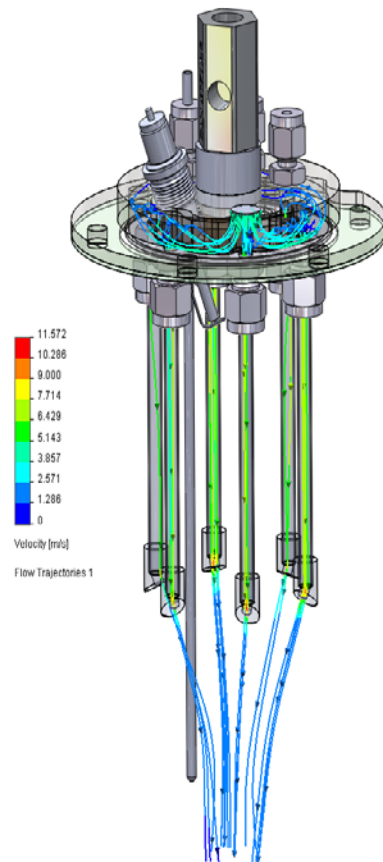
Component test results verified simulation



Progress: Used simulation to design multi-fuel burner; Confirmed during test

The fuel/off-gas burner is the primary source of thermal energy for the reforming reaction.

Correct distribution of H₂ essential for developing a desirable flame shape and optimizing heat transfer.



Accomplishments: Developed Highly Efficient Thermally Integrated System Design

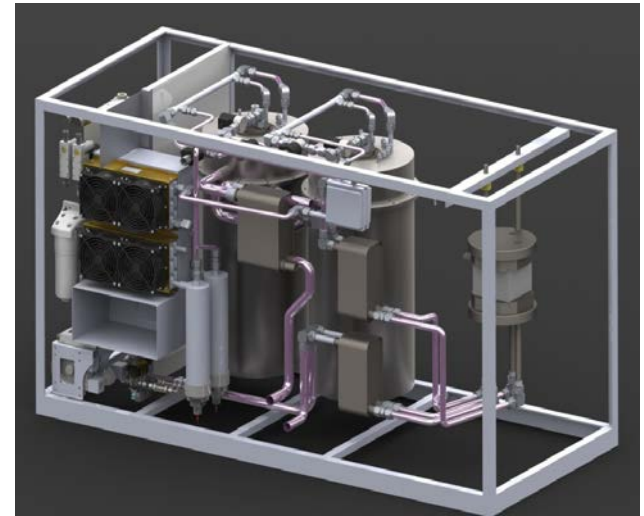
Process Flow Diagram

- Subdivided into 21 process streams

Mass and Energy Balance

- Completed for each of 21 process streams
- Determines input, output, efficiency

Optimized Layout, Piping & Instrumentation

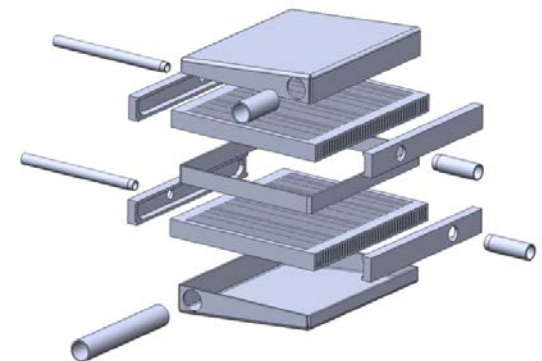
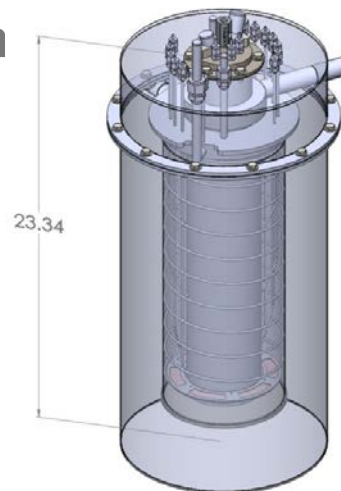


Solid Model of Integrated System

Milestone

3 Component Design and Analysis

- Process simulations
- Design trade-off analyses



Progress: Design Review & Materials Analysis

Design for manufacturing and assembly review

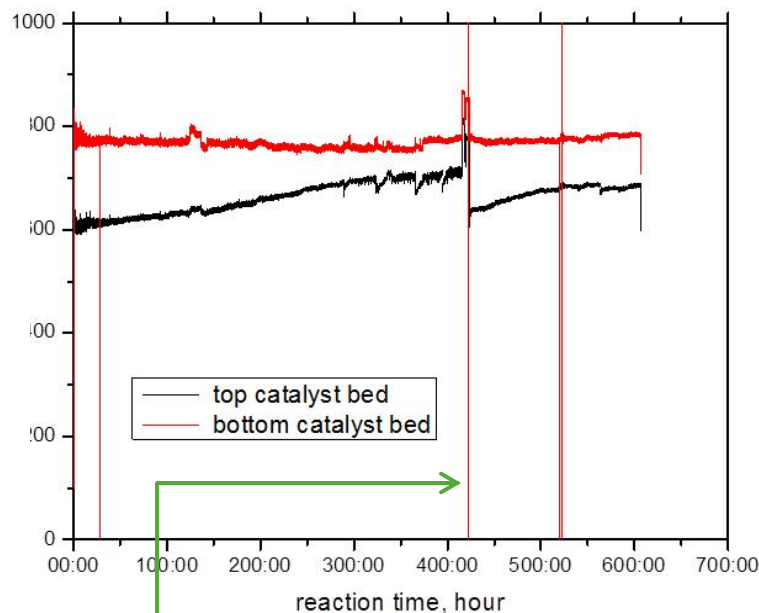
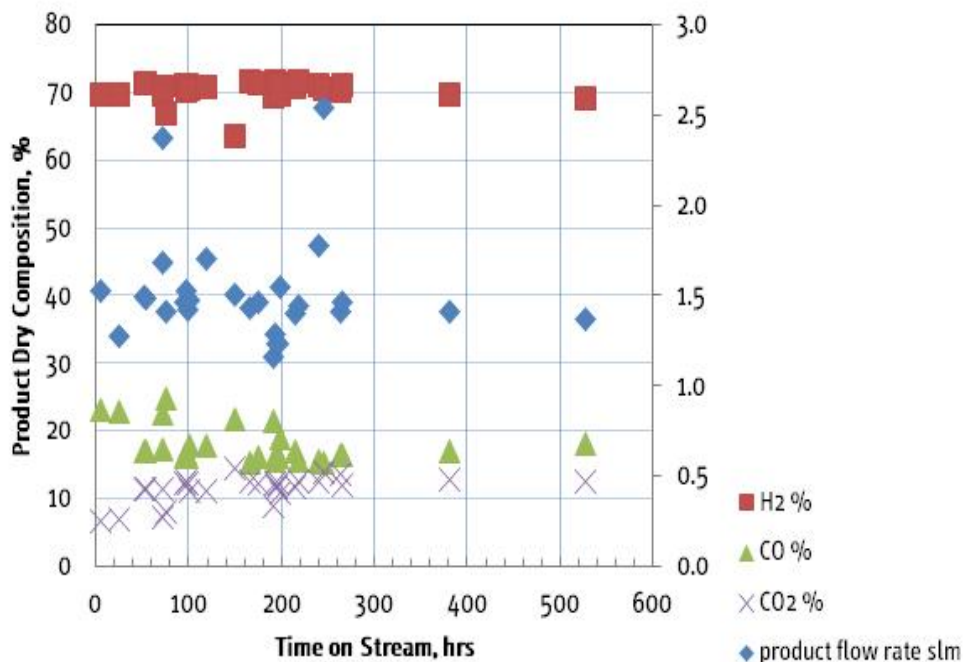
- Conducted by expert consultant ← **Milestone 2**
- Focus on materials and joining technology
- Assessed appropriateness for manufacturability
- Provided advice on reducing cost & increasing durability
 - Materials selection
 - Forming selection
 - Standardization
 - Consolidation of parts
 - Optimization of tolerances
 - Design for assembly
 - Vendor selection



Accomplishments: InnovaTek Proprietary Catalyst Reforms Bio-Kerosene during long-term test

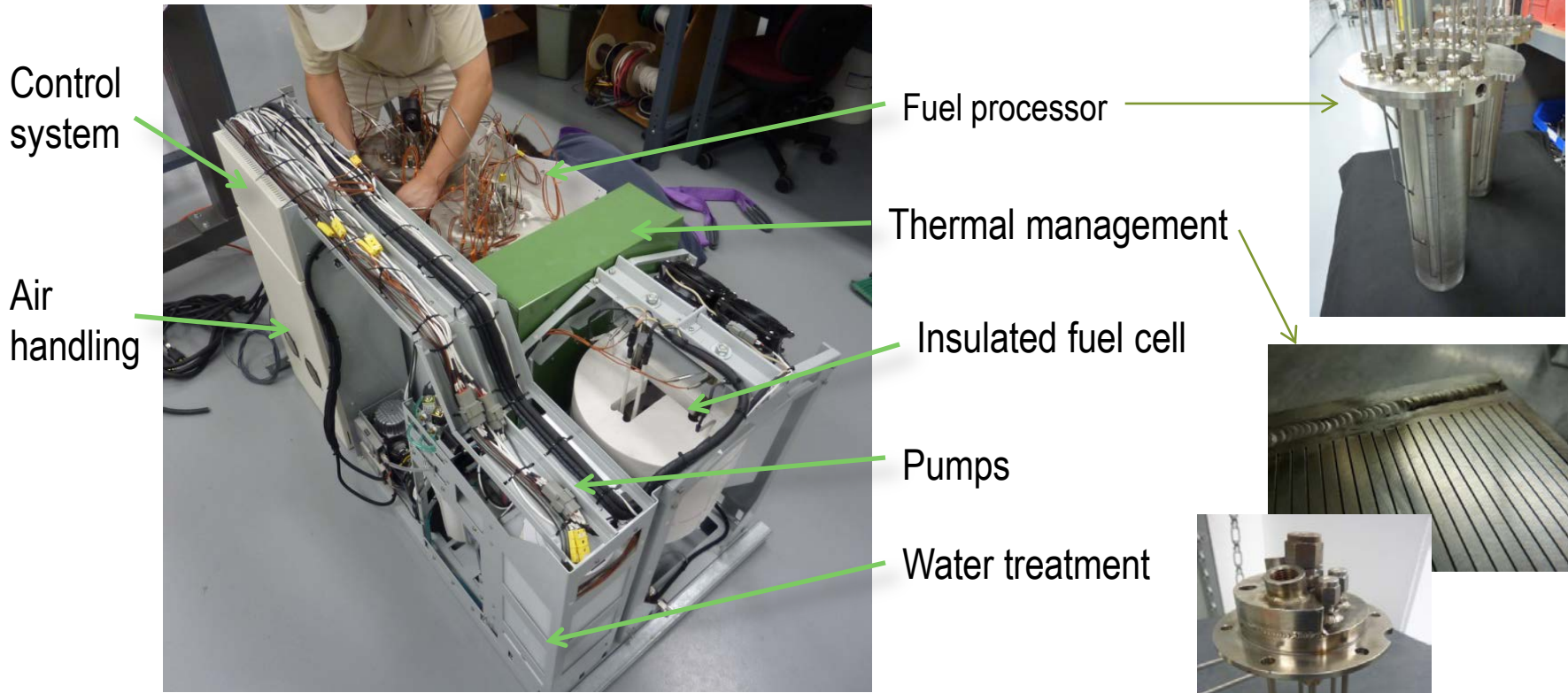
Stable over 600 hours with successful regeneration

Product flow rate and composition



Regeneration cycle at 420 hr after inadvertently running for several hrs without water

Progress: Proprietary Component Fabrication, Assembly and Integration

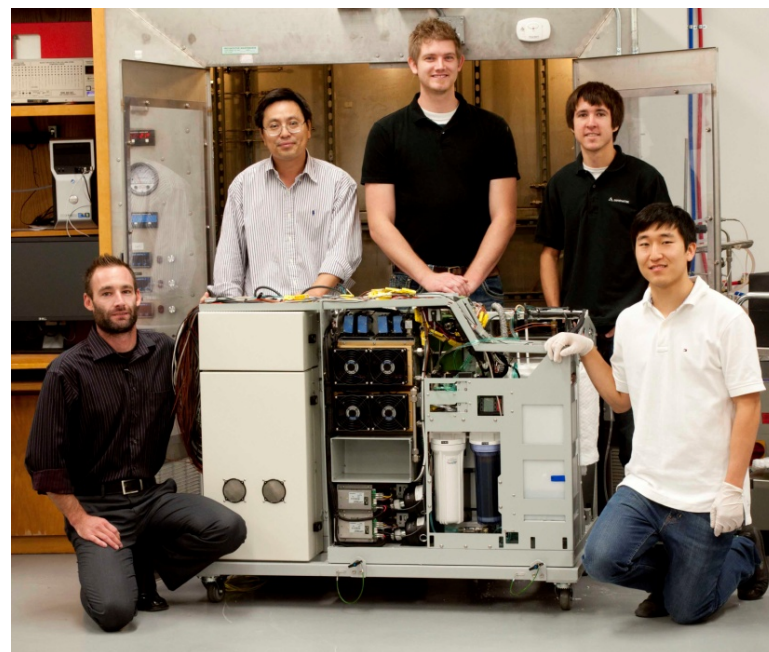


System is water neutral; no net consumption

Accomplishments: Fully Integrated InnovaGen® Power Unit Built & Tested

Proprietary Components

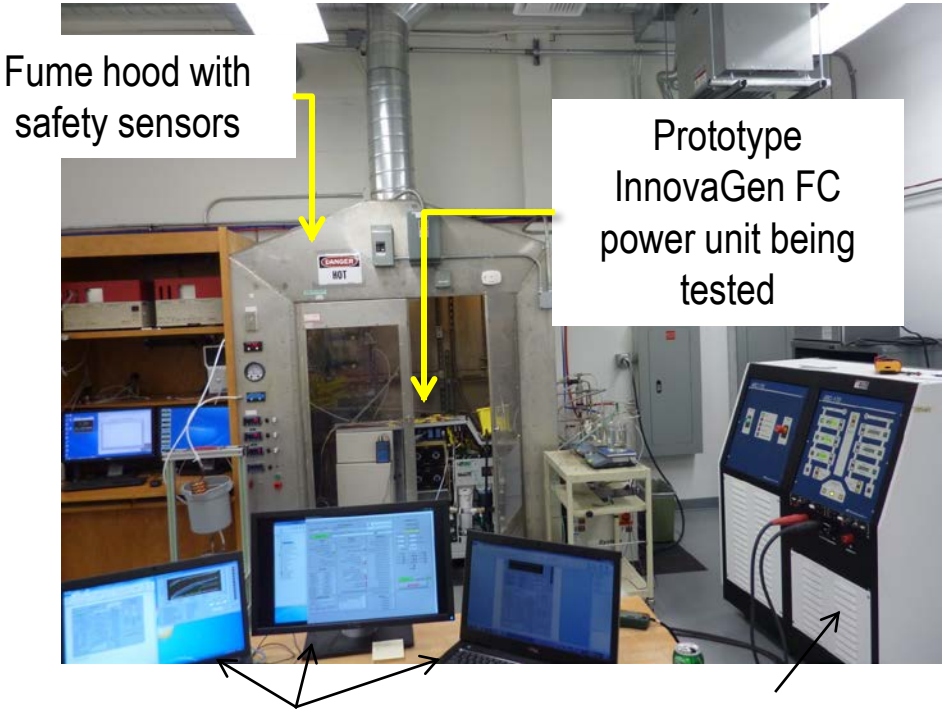
- **Hardware**
 - Chemical processing
 - Thermal management
 - Water management
 - Electrochemical
- **Software**
 - Control systems
 - Safety features
- **Catalysts**
 - Convert multiple fuels including biofuel



Accomplishments: Integrated System Produced Power from Bio-Fuel

➔ Go Year 2

1.2 kW power sent to grid

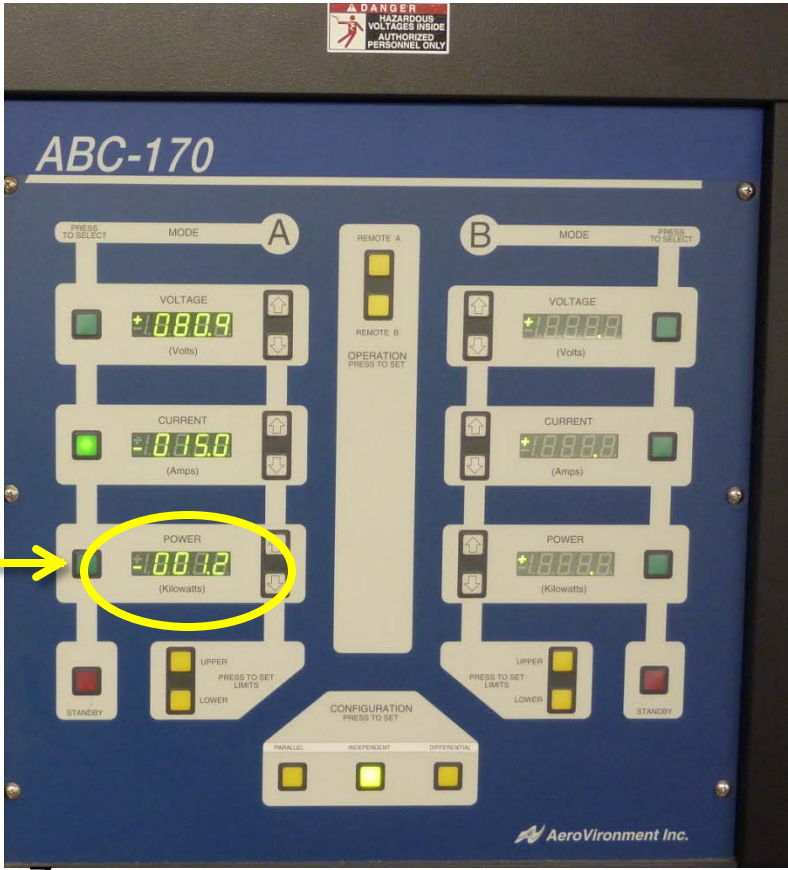


Fume hood with safety sensors

Prototype InnovaGen FC power unit being tested

Control system monitors

AeroVironment power processing system



Accomplishments: Analysis of Process Economics

Used EERE's HOMER Model in Phase II

- Examined several scenarios for delivering 5 kW electrical AC power for 20 years using InnovaGen FC power unit
- Compared bio-kerosene, upgraded bio-oil, non-upgraded pyrolysis oil, natural gas
- Used projected production and fuel pricing data from DOE sources

Significant Findings:

1. A fuel cell generator that operates on natural gas could produce electricity at prices at or below current grid prices when volume production brings capital costs down.
2. Up-graded bio-fuel is less costly to create electricity than raw pyrolysis oil because of its much higher heating value

Collaborations

Subcontractors

- **Energy Technology Services – former senior staff of UTC; developed first fuel cell system for NASA; acted as 3rd party design reviewers & advisors for codes & standards**
- **Topsoe Fuel Cell – provided SOFC stack**

Strategic Partners

- **PNNL & WSU-BSEL – provided bio-oil made from wood sawdust**
- **Boeing – provided bio-kerosene made from camelina**
- **City of Richland Electric Utility – providing site for field demo**
- **Mid-Columbia Energy Initiative**

Education

- **Supported 5 student interns from Kettering, WSU, U of WA in mechanical engineering, chemistry, electrical engineering, & business**

Proposed Future Work

Objective 3. Prove the technical and commercial potential of the technology

- **Increase system efficiency & durability; reduce cost**
 - Reduce FC parasitic power; improve FP thermal management
 - Enhance FC-FP integration; evaluate BOP alternatives
- **Assess Versa Power SOFC – Collaborator**
- **Optimize performance by testing & adjusting operating parameters**
- **Analyze process economics**

Go/No Go decision to proceed to Year 3

- **Design for manufacturing to reduce costs**
- **Build demo systems**
- **Verify durability with field demo at City Utility**

Summary

Relevance: Shift primary energy from fossil to renewable fuels

- Address codes & standards for fuel cells
- Increase system efficiency, lifetime and durability; decrease cost
- Distributed power production near source of feedstock to enhance grid stability

Approach: Develop reformer that generates hydrogen from non-food biofuels

- Develop highly efficient processing design of integrated SOFC and fuel processor
- Prove technology in long-term field demonstration with utility partner

Accomplishments: Developed system design criteria for codes and standards

- Used simulation and modeling to develop superior component /system designs
- Developed optimized catalyst for biofuel reforming
- Fabricated and integrated proprietary system hardware, software, and catalysts
- Demonstrated 1.2 kW power from bio-kerosene and sent to grid

Collaborations: Supported 5 students; Subcontractors for fuel cell & 3rd party oversight;

- Partnerships with PNNL, WSU, Boeing, City of Richland, Regional Energy Initiative

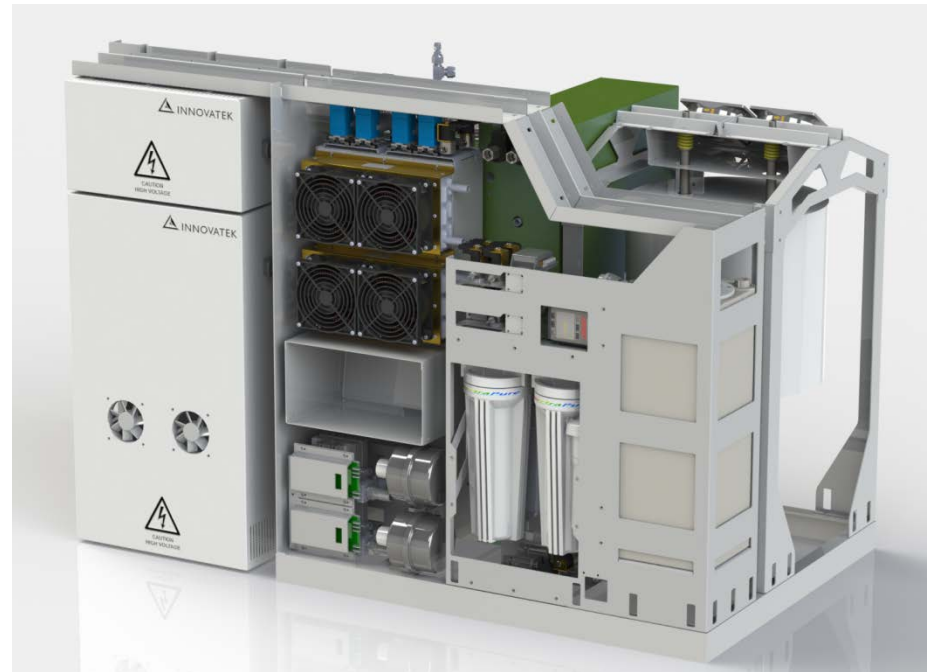
Future: Further technology improvements and system optimization

- Additional fuel cell collaborators; Analysis of process economics
- Field demonstration and long term operation

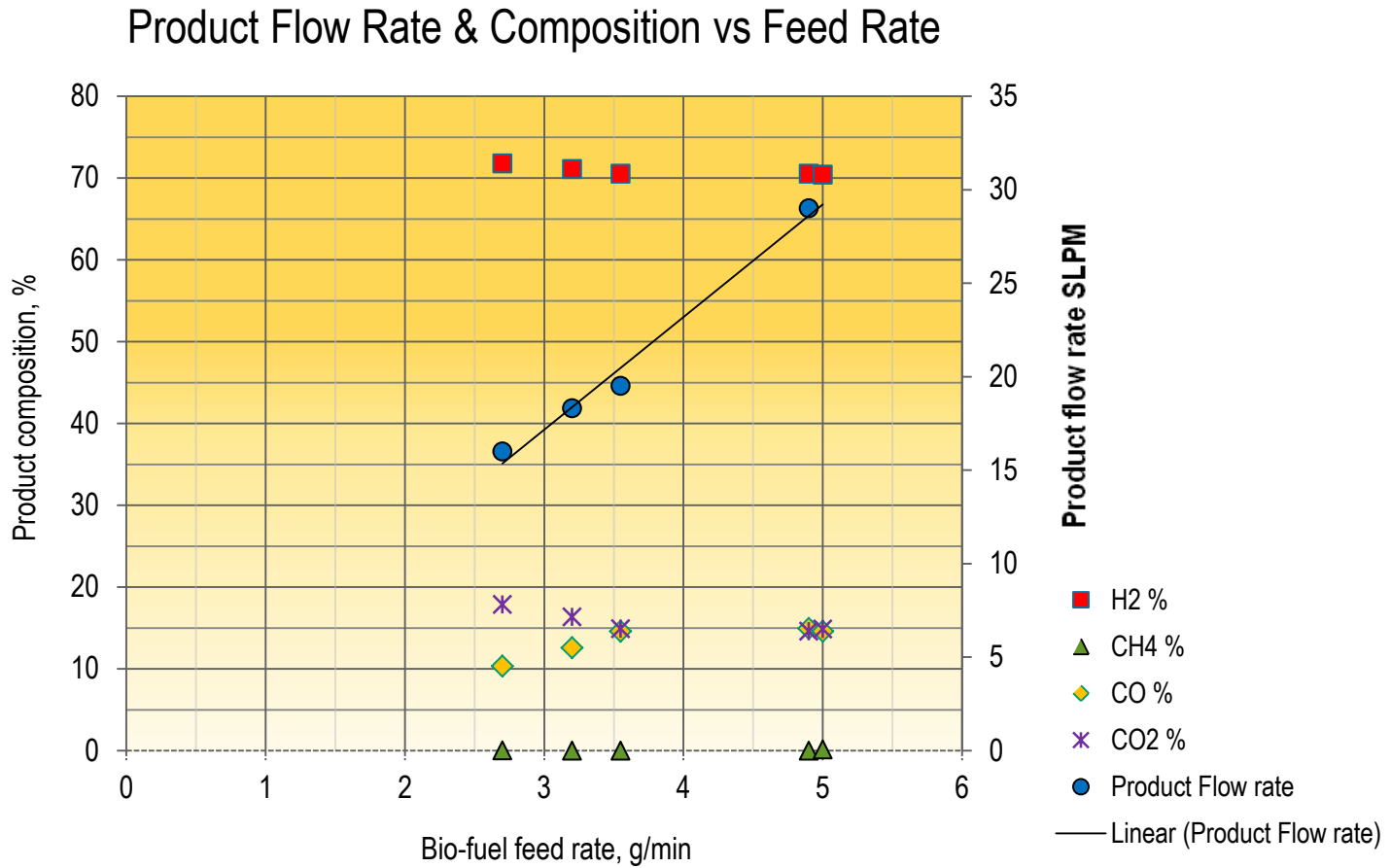
Technical Back-up

Technical: Developed & Integrated All Subsystems of Complete Power Unit

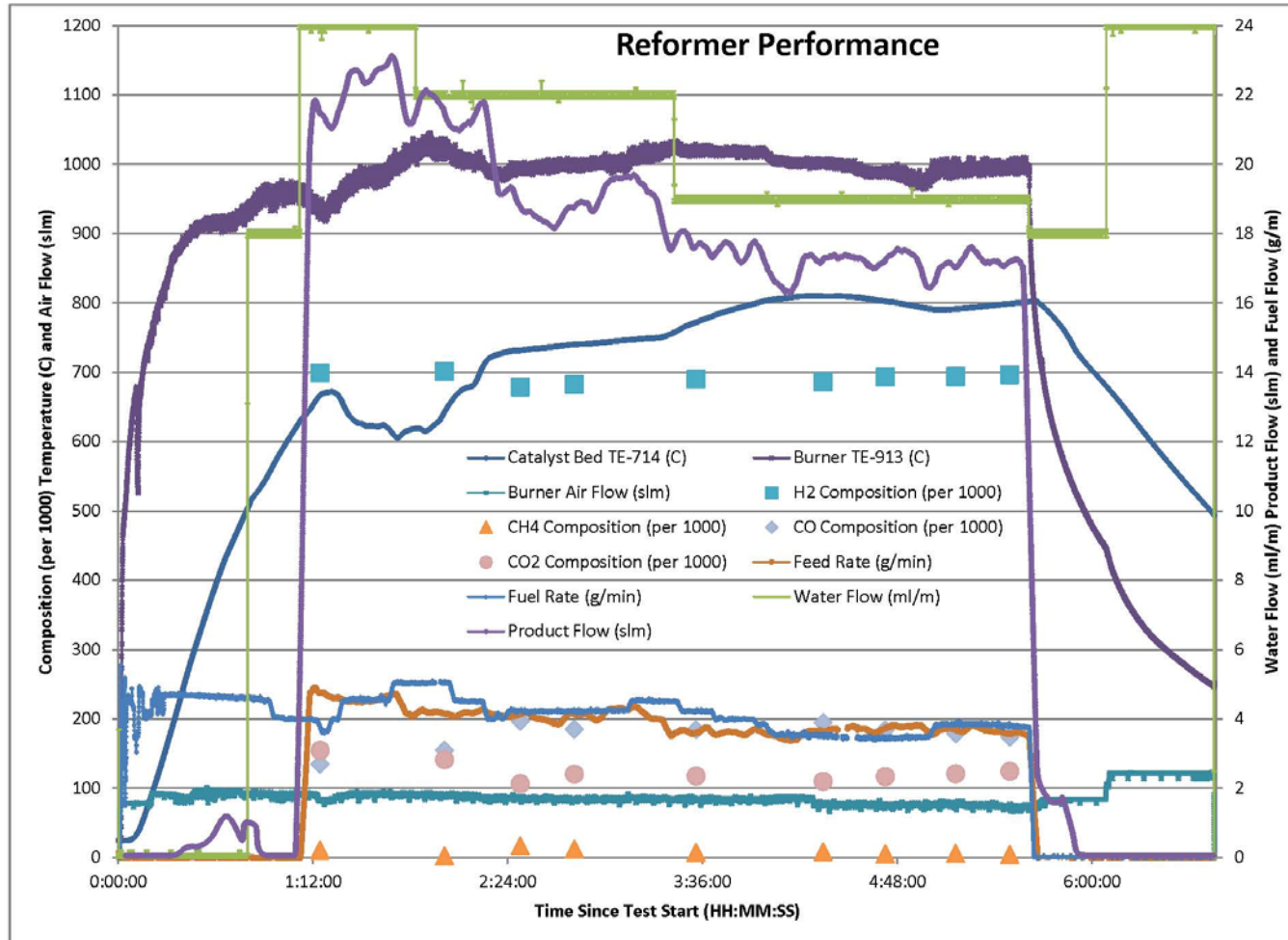
- Fuel processing
- Oxidant processing
- Thermal management
- Water treatment
- Power conditioning
- Automatic controls
- Ventilation
- Topsoe SOFC
- Onboard energy storage



Reformer Test Results with Bio-Kerosene



Data Summary – Reformer Tests



Accomplishment: Test of Integrated Reformer & 1 kW SOFC – Start-up

System Start-up

Data Management

Data Update Count: 15420 | Running Time: 0:0:0 | Current Controller State: MANUAL

LOGGING DATA ON | Data Log File Base Folder: c:\InnovaTek\Data\DoE1KW | Recording: [ON] | Test Name: PowerRun10_11_11

Command Center

SHOW ALARM DISPLAY | TOGGLE AUTO MODE | MANUAL CONTROL

Burner

AIR: Burner Air Flow MFM-301 (slm) 92.1, Flue Exhaust O2 Concentrate AT-901 (%) 6.9, Burner Air In PT-301 (psig) 0.83, Spark Plug BFI-911, Burner Air Power BLO-301, System Power.

FUEL: Bio SPK Fuel Power PMP-611, Fuel Valve CV-611/612.

Reactor

REFORMATE: Reformate Prior to Stack PT-701 (psig) 3.28, Reformate Divert 3-Way CV-711.

FEED: Bio SPK Feed PT-501 (psig) 9.2, Feed Water Conductivity CT-401 (us) 0.0, Bio SPK Feed PowerYC-501, Feed Valve CV-501.

WATER: Water Feed Pressure PT-412 (psig) 9.0, Water Flow Rate MFC-411 (mlm) 18.3, PT-411, Water Valve CV-401, Water Level Low LSL-401, Water Level Emergency Low LSSL-401.

Temperature

Burner Air TE-301 (C) 181.3, Feed Water After E-1 TE-411 (C) 57.7, Feed Water After E-2 TE-412 (C) 107.8, Catalyst Bed TE-714 (C) 685.2, Reformate After Cat Bed TE-726 (C) 405.4, Reformate After HXT-411 TE-727 (C) 176.5.

Water Setpoint (mlm) 18.2, Burner Air Setpoint (slm) 5.0, Feed Setpoint (mlm) 4.5, Cathode Air Setpoint (slm) 3.0, Fuel Setpoint (mlm) 7.2, Fuel Cell Heater Duty Cycle (%) 110.0, State Selection: COLD IRON.

Fuel Cell

TE-001 (C)	627.3	TE-701 (C)	537.3
TE-002 (C)	588.2	TE-801 (C)	107.8
TE-351 (C)	144.8	TE-802 (C)	53.1
TE-352 (C)	582.6	TE-803 (C)	79.2
TE-353 (C)	0.0	TE-804 (C)	28.6

PT-351 (psig) 0.52, PT-352 (psig) 0.46, PT-353 (psig) 0.06, FC Current (A) 0.0, PT-702 (psig) 3.02, FC Voltage (V) 58.9, PT-801 (psig) 3.22, FC Power (W) 0.0.

Controller Events

Origin: Not Available | Context: Not Available | Source: IFP controller was restarted ::

Priority: 50 | Entry Type: Event | Code: 1 | Time Stamp: 9:20:26.134 AM 10/11/2011

TEMPERATURE HISTORY

Graph showing Degrees Celcius vs Time (11:30:00 AM to 1:45:00 PM 10/11/2011). Multiple colored lines represent different temperature sensors, showing a rapid increase in temperature starting around 12:00 PM.

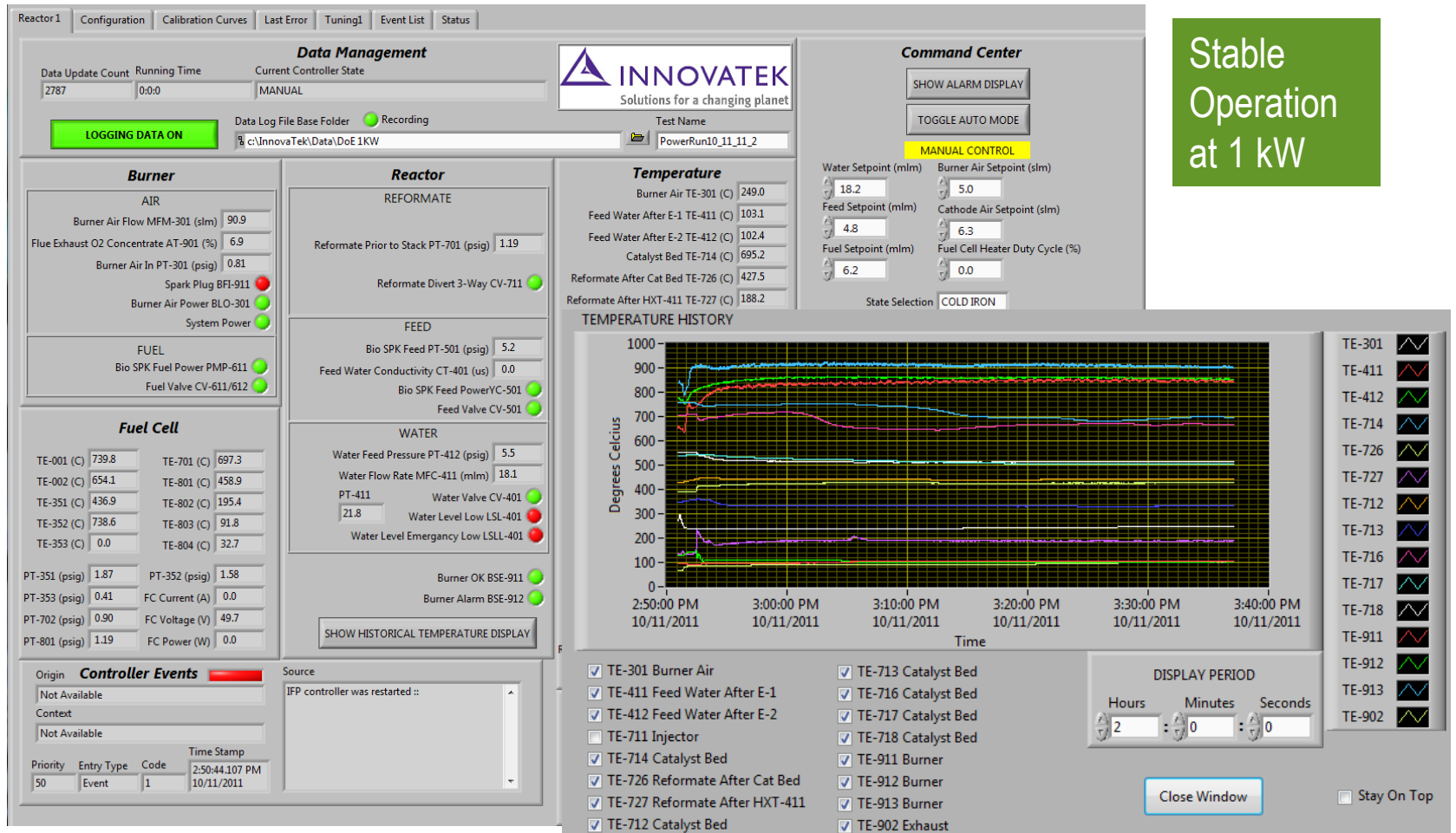
TE-301 [OK] **TE-411** [OK] **TE-412** [OK] **TE-714** [OK] **TE-726** [OK] **TE-727** [OK] **TE-712** [OK] **TE-713** [OK] **TE-716** [OK] **TE-717** [OK] **TE-718** [OK] **TE-911** [OK] **TE-912** [OK] **TE-913** [OK] **TE-902** [OK]

DISPLAY PERIOD

Hours: 2 | Minutes: 0 | Seconds: 0

Close Window | Stay On Top

Accomplishment: Test of Integrated System – Steady state



Stable
Operation
at 1 kW