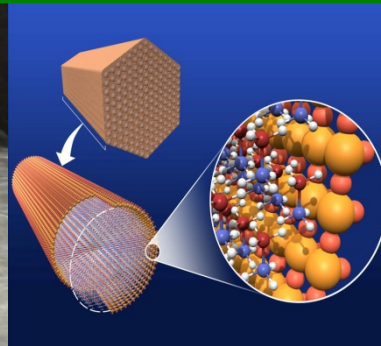




U.S. DEPARTMENT OF  
**ENERGY**



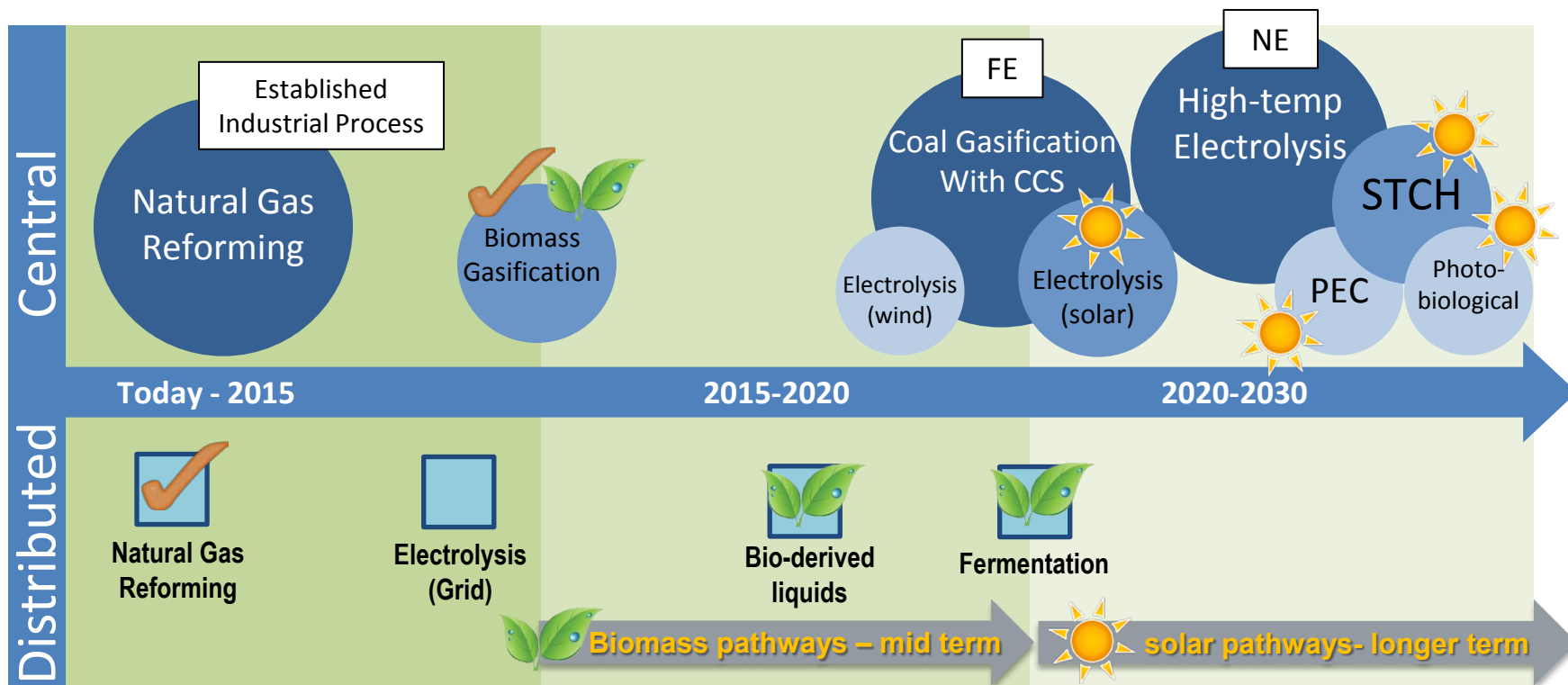
# Hydrogen Production -Session Introduction -

*Katie Randolph*

*2013 Annual Merit Review and Peer Evaluation Meeting  
May 16, 2013*

# Production Goal and Pathway Strategies

**Objective: Develop technologies to produce hydrogen from clean, domestic resources at a delivered and dispensed cost of \$2-\$4/kg H<sub>2</sub> by 2020**



**Estimated Plant Capacity (kg/day)**

Up to 1,500

50,000

100,000

≥500,000

P&D Subprogram R&D efforts successfully concluded

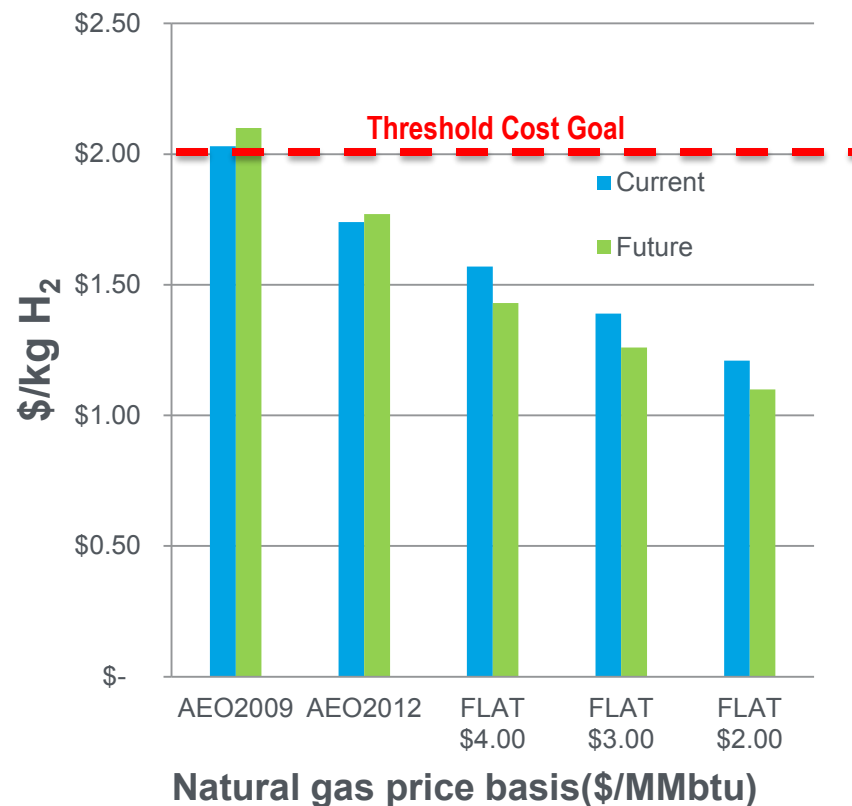
*FE, NE: R&D efforts in DOE Offices of Fossil and Nuclear Energy, respectively*

## Hydrogen Production from Natural Gas: Bridge to Longer-Term, Low-Carbon Technologies

Distributed H<sub>2</sub> Production from NG SMR (high volume/economies of scale)

- Cost of H<sub>2</sub> production not limiting factor
- Cost goals can be met by a wide range of NG prices\*
- Focus shifting to longer term, early development, renewable pathways

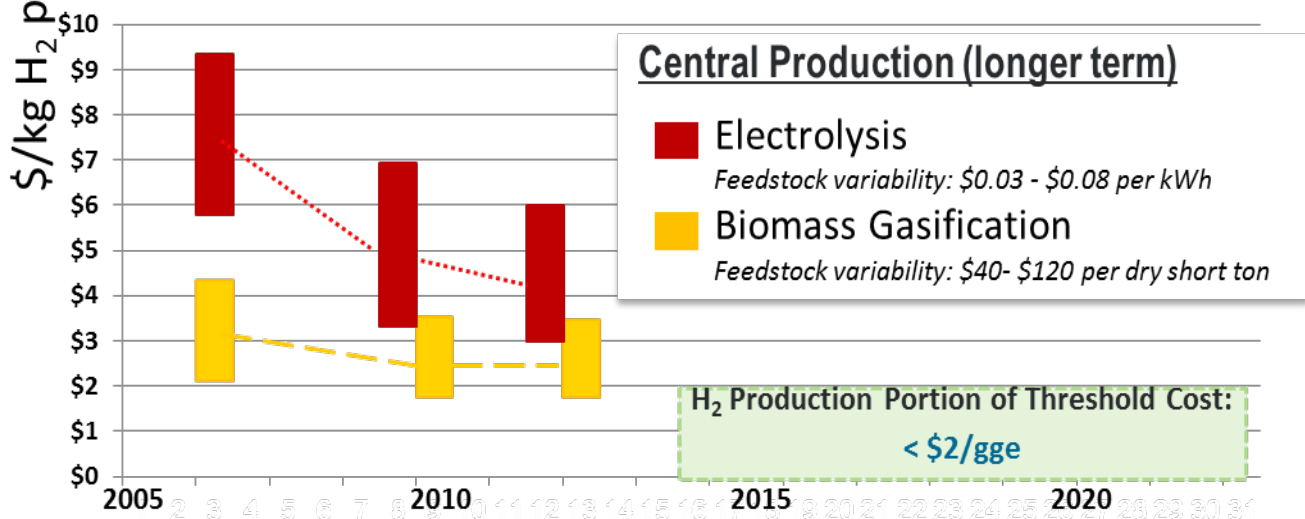
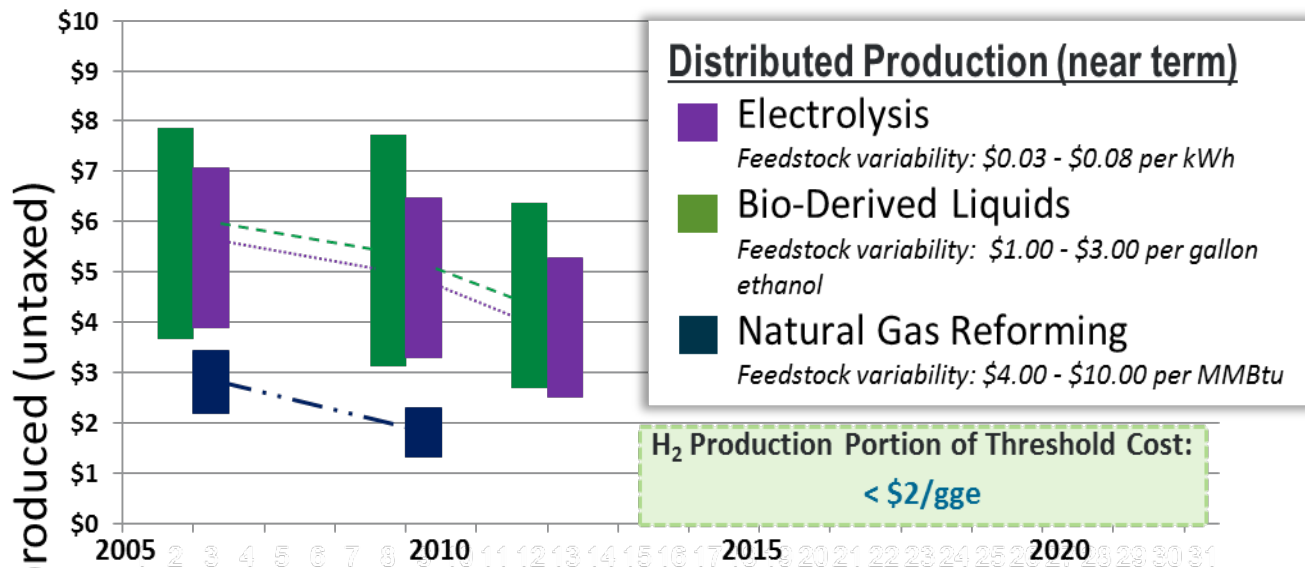
**\$/kg H<sub>2</sub> (produced & untaxed, today's technology) for Varying Natural Gas Spot Prices**



\*Production Cost Using Low-Cost Natural Gas, September, 2012, [http://hydrogen.energy.gov/pdfs/12024\\_h2\\_production\\_cost\\_natural\\_gas.pdf](http://hydrogen.energy.gov/pdfs/12024_h2_production_cost_natural_gas.pdf)

Based on H2A v3 Case Studies @ [http://www.hydrogen.energy.gov/h2a\\_production.html](http://www.hydrogen.energy.gov/h2a_production.html)  
 AEO2009 avg NG prices (HHV, \$/MMBtu): \$7.10 (Current, 2010-2030); \$8.44 (Future, 2020-2040)  
 AEO2012 avg NG prices (HHV, \$/MMBtu): \$5.28 (Current, 2010-2030); \$6.48 (Future, 2020-2040)

## Projected High-Volume Cost of Hydrogen for Near-Term Production Pathways



- Status of hydrogen cost (production only, does not include delivery or dispensing costs) is shown in vertical bars, reflecting values based on a range of assumptions (feedstock/capital costs).
- Cost ranges are shown in 2007 dollars, based on projections from H2A analyses, and reflect variability in major feedstock pricing and a bounded range for capital cost estimates.
- Projections of costs assume Nth-plant construction, distributed station capacities of 1,500 kg/day, and centralized station capacities of ≥50,000 kg/day.

# Current Targets and Status

	\$/kg (production costs only)	2011 Status	2015 Target	2020 Target	Ultimate Production Target
Distributed	Electrolysis from grid electricity	\$4.20	\$3.90	\$2.30	\$1-\$2
	Bio-derived Liquids (based on ethanol reforming case)	\$6.60	\$5.90	\$2.30	
Central	Electrolysis From renewable electricity	\$4.10	\$3.00	\$2.00	
	Biomass Gasification	\$2.20	\$2.10	\$2.00	
	Solar Thermochemical	NA	\$14.80	\$3.70	
	Photoelectrochemical	NA	\$17.30	\$5.70	
	Biological	NA	NA	\$9.20	

Apportionment of Threshold Cost: \$1-\$2/kg for production, \$1-\$2/kg for delivery.

**\*Based on the 2012 DOE-FCTP MYRD&D cost status and targets for Hydrogen Production** <http://www1.eere.energy.gov/hydrogenandfuelcells/mypp/pdfs/production.pdf>

## *Materials performance and capital costs identified as key challenges for ALL production pathways*

### Bio-Derived Liquids Reforming

- High capital costs
- High operation and maintenance costs
- Design for manufacturing
- Feedstock availability, quality, and cost

### Coal and Biomass Gasification

- High capital costs
- System efficiency
- Feedstock cost and purity
- Carbon capture and storage

### Water Electrolysis

- Low system efficiency and high capital costs
- Integration with renewable energy sources
- Design for manufacturing
- Electricity costs

➤ Meeting H<sub>2</sub> production cost threshold for all near- and longer-term pathways requires improvements in materials efficiency and durability, and reductions in overall capital costs

### Solar Thermochemical

- Cost-effective reactor and system
- Effective and durable reaction and construction materials

### Photo-electrochemical

- Efficient and durable photocatalyst materials
- Innovative integrated devices

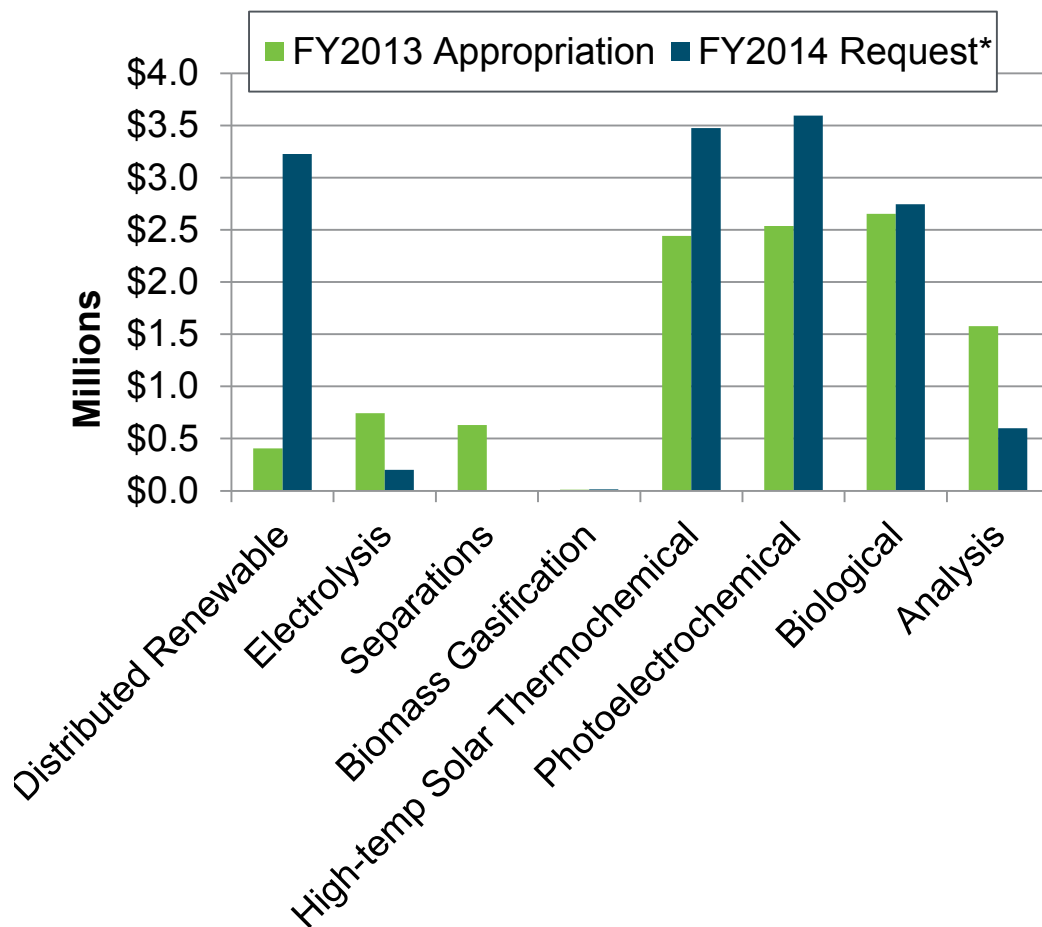
### Biological

- Sustainable H<sub>2</sub> production from microorganisms (O<sub>2</sub> tolerance)
- Optimal microorganism functionality (maximize yields and rates)

# Hydrogen Production Budget

**FY 2013 Appropriation = \$11.0M**

**FY 2014 Request = \$13.9M**



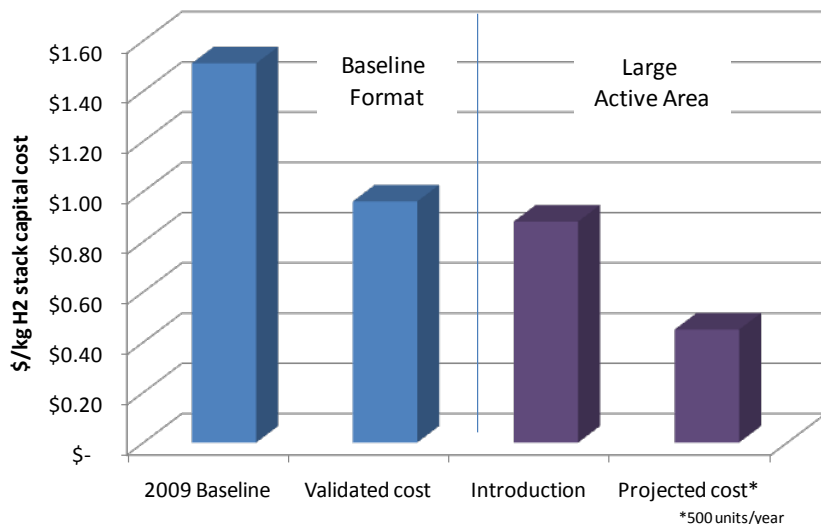
\* Subject to appropriations, project go/no go decisions and competitive selections. Exact amounts will be determined based on R&D progress in each area and the relative merit and applicability of projects competitively selected through planned funding opportunity announcements (FOAs).

## EMPHASIS

- New Hydrogen Analysis Award Made 2013
- Planning multiple FOAs over the next few FYs to replenish portfolio and address critical barriers.
  - Enhance leveraging of production R&D with DOE offices and other agencies.
  - Continue R&D on longer-term solar and bio-based renewable technologies
  - Continue to address key materials, device and reactor needs for production pathways
- Nearer term technologies being transitioned to Tech-Val portfolio and continue to be supported by SBIR Program

## Cost Reduction Progress and Successful System Validation

### Proton OnSite



- Electrolyzer stack capital cost reduction of >70% over the last 4 years
  - Contributions to cost reduction include:
    - A >50% reduction in catalyst pgm loading from >1 mg/cm<sup>2</sup> with no negative performance impact
- Advancements in bipolar plate coating, design, and manufacturing enabling an increase in the cell active area

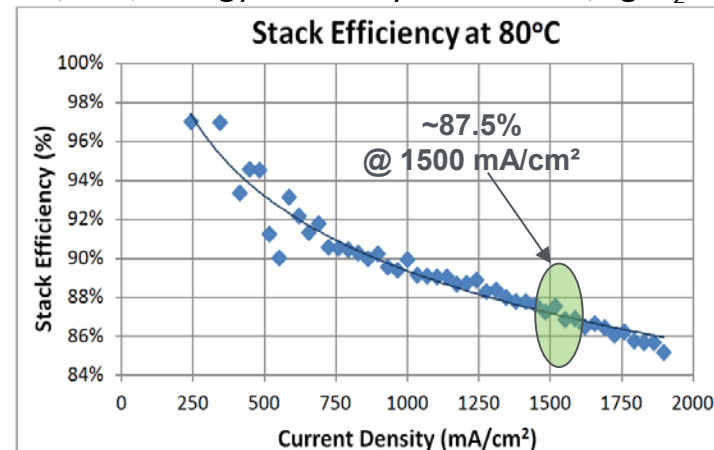


### NREL/Giner, Inc.



#### 12 kg H<sub>2</sub>/day Giner system validated at NREL in June 2012

- Nominal operating conditions: 390 psig, 1.5-1.9 A/cm<sup>2</sup>
- High stack voltage efficiency: 73.6% LHV (>87% HHV) @ 1.5 A/cm<sup>2</sup>; Energy efficiency=46.6 kWh/kg-H<sub>2</sub>



NREL Report: 200 Hour Testing - Giner Parker Electrolyzer Milestone 3.7.6 (CPS 52066)



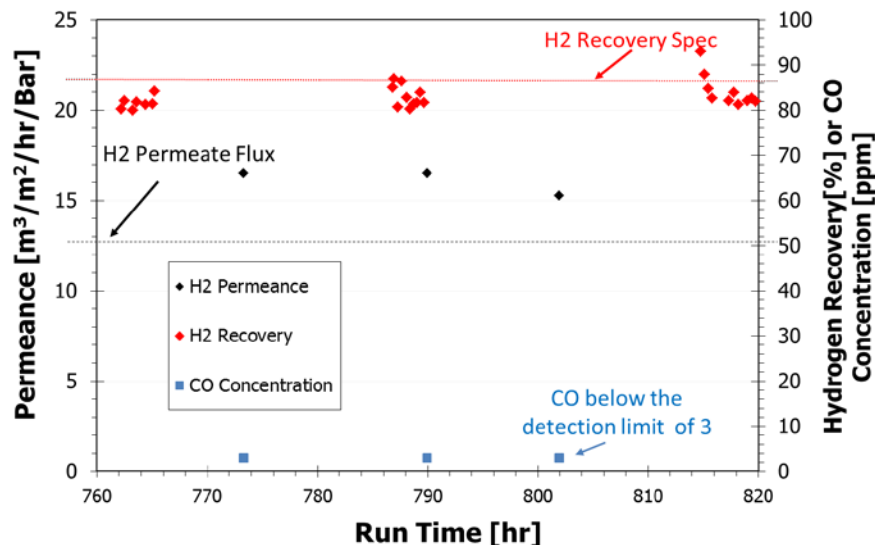
## Successful demonstrations of separations and purification

### Media and Process Technology, Inc.

- Completed 200 hour full-scale tubular Palladium (Pd) membrane field test
  - ✓ Demonstrated  $<10\text{ppm CO}$ ,  $>85\%$   $\text{H}_2$  recovery
- Working with industry to replace common Pd foil-based purifiers with their ceramic membranes for back-up power applications



Field Test of Pd Membranes (ID: Membrane #2)

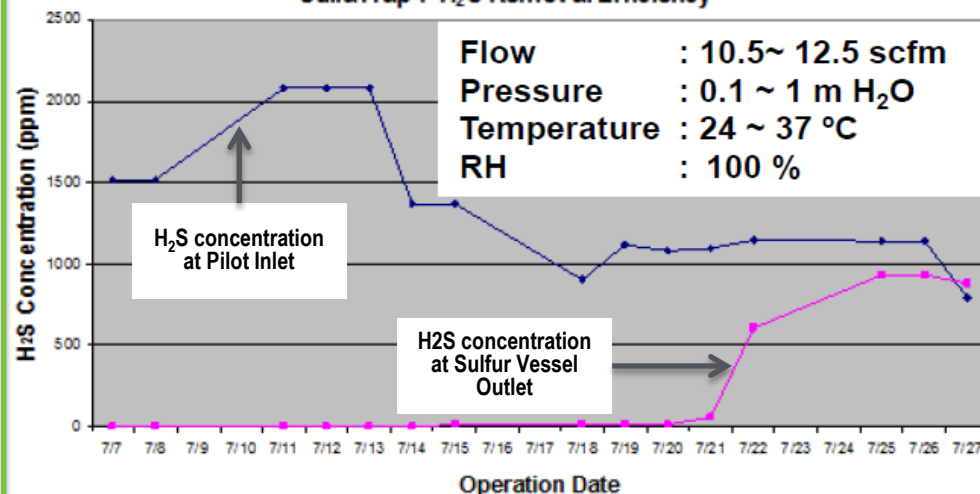


### TDA Research, Inc.



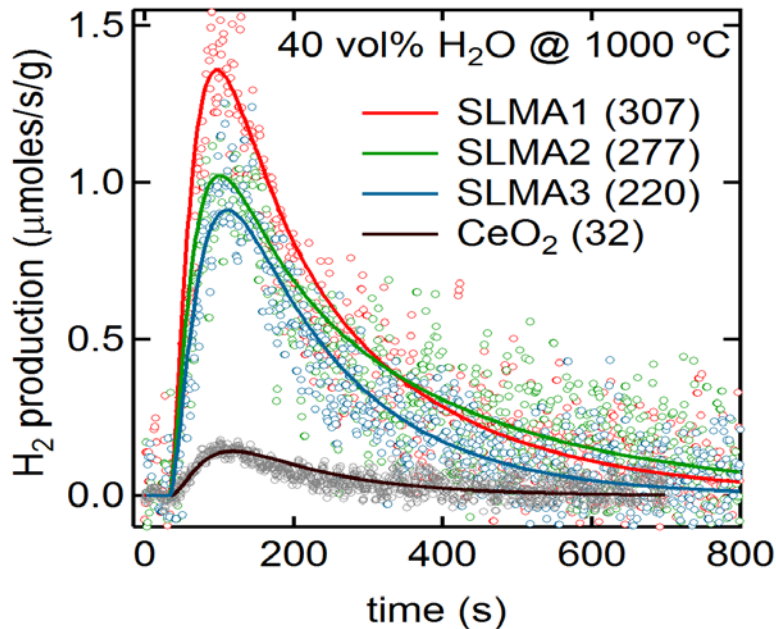
- Completed 21 day field test on the 12 CFM gas clean-up skid
  - ✓ Sorbent achieved 17.5 wt. % sulfur capacity
  - ✓ Potential for 2X higher capacity than commercially available sorbents
  - ✓ Sub ppm level of sulfur (undetectable)

SulfaTrap-7  $\text{H}_2\text{S}$  Removal Efficiency



*Perovskite compounds, nanostructured hercynite, show production yields ~9-10x that of CeO<sub>2</sub> at low reduction temperatures*

**Sandia National Laboratory**



- Perovskite kinetics benchmarked against CeO<sub>2</sub>
- At lower T<sub>R</sub> (1350 °C vs. 1500 °C) ~9x more H<sub>2</sub> w/ Perovskite as compared to CeO<sub>2</sub>
- Patent filed on a family of perovskite materials

**University of Colorado**

Temp Swing (TS) & Isothermal (IT) (Red/Ox); Temperature (°C)	CeO <sub>2</sub> (μmole/g)	Nanostructured Hercynite (μmole/ total g)*
1500/1200	159.1 ± 15.7	93.7 ± 19.2
1450/1450		167.4 (avg)
1350/1000	16.4 ± 3.6	31.4 ± 2.3
1350/1350		102 ± 18

\*The numbers shown for hercynite are per total g material. If per active g of material, they would be multiplied by 2.13.

- IT hercynite cycle produces ~ the same and 2X more H<sub>2</sub> on a total and active material basis respectively than TS CeO<sub>2</sub> at high reduction T.
- IT hercynite cycle produces about ~ 5X and 15X more H<sub>2</sub> on a total and active material basis respectively than TS CeO<sub>2</sub> at lower reduction T.
- IT hercynite cycle produces substantially more H<sub>2</sub> than TS “hercynite cycle”

## *Important progress in establishing standardized PEC protocols and in demonstrating manufacturability of large-scale devices*

### Developed critical standards & protocols for evaluating and reporting PEC materials

#### **EERE PEC Working Group**

- **Original JMR Review paper cited over 100 times to date;**
- **Expanded form being published as a “Springer Brief”**

#### REVIEW

*This section of Journal of Materials Research is reserved for papers that are reviews of literature in a given area.*

#### **Accelerating materials development for photoelectrochemical hydrogen production: Standards for methods, definitions, and reporting protocols**

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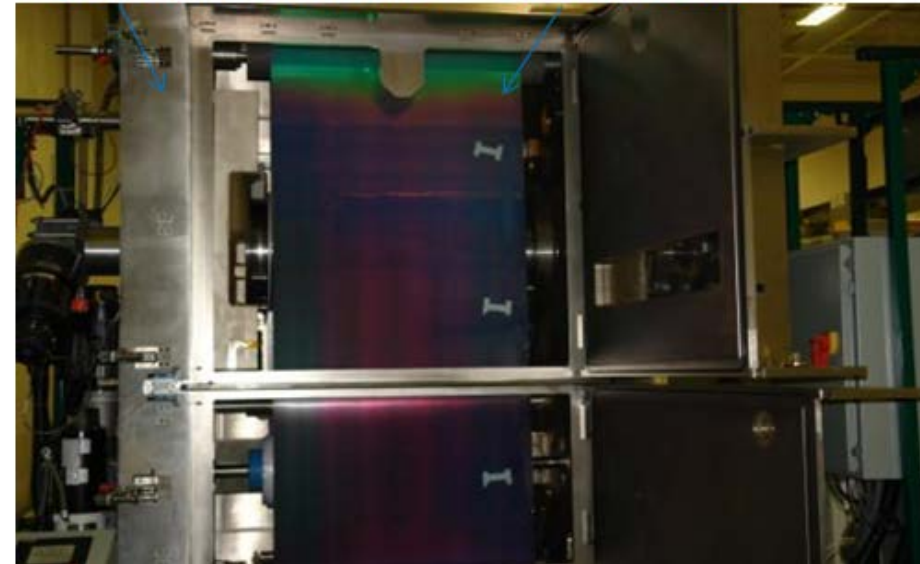
*Hydrogen Technologies and Systems Center, National Renewable Energy Laboratory, Golden, Colorado 80401*

### Demonstrated pathway to economical manufacturing of thin-film PEC devices

#### **MWOE**

*Pay-out chamber of 2MW line*

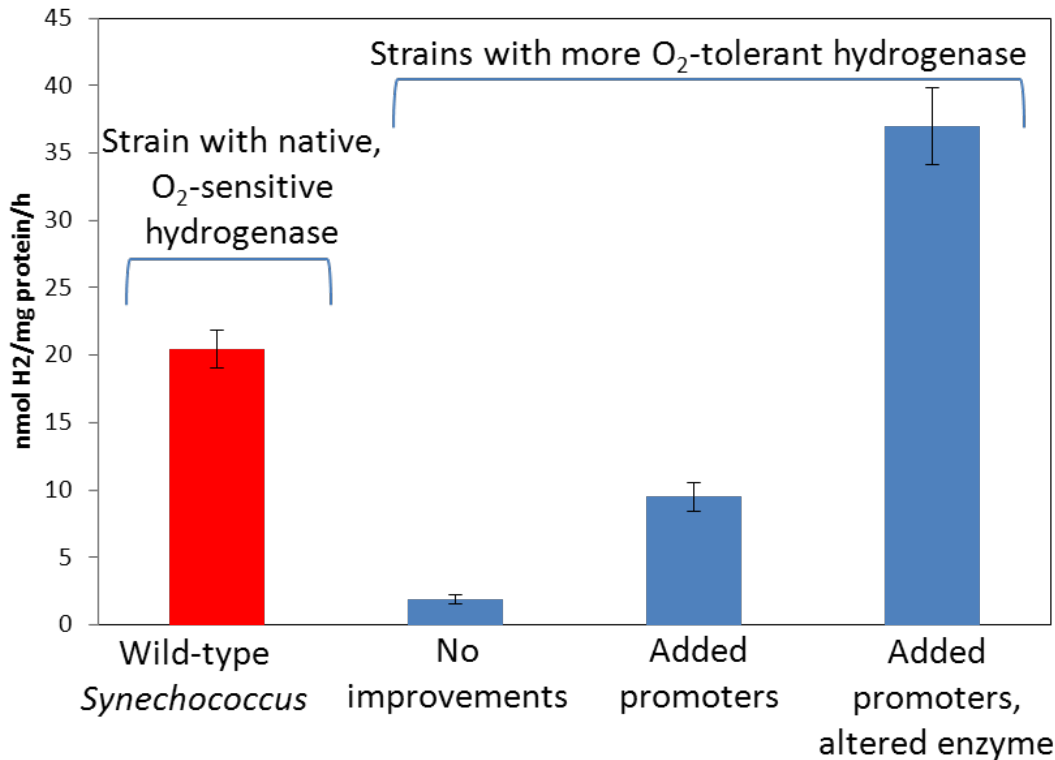
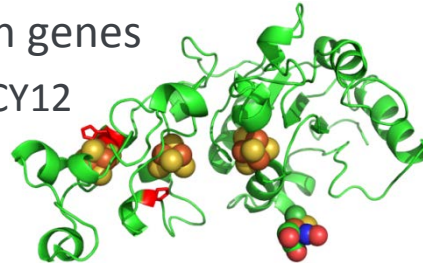
*3 ft. wide SS web*



- The 2MW roll-to-roll machine allows the fabrication of integrated thin-film PEC photoelectrodes based on amorphous silicon cells
- The prototype production machine produces large area PEC electrodes (3ft wide and hundreds of feet long) with good uniformity and minimal edge effects

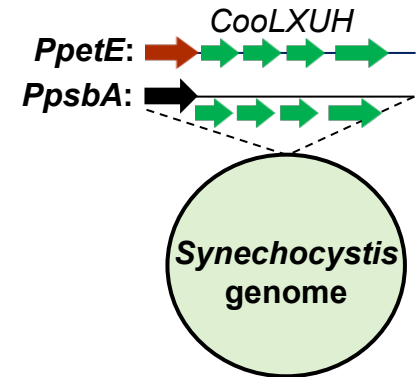
## Improved expression of recombinant hydrogenase proteins in cyanobacteria (JCVI)

- Added promoters to maturation genes
  - Increased activity by 4 fold in CY12
- Altered protein to improve electron transfer
  - Increased activity by 5 fold in CY12

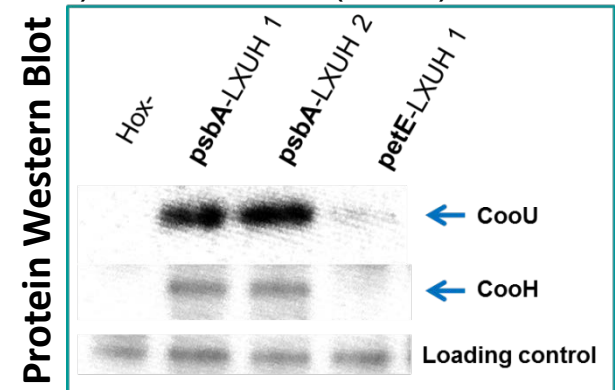


## Improved hydrogen evolution in recombinant cyanobacteria (NREL)

- Placed native *Synechocystis* promoter *psbA* in front of CBS hydrogenase genes inserted into *Synechocystis* genome

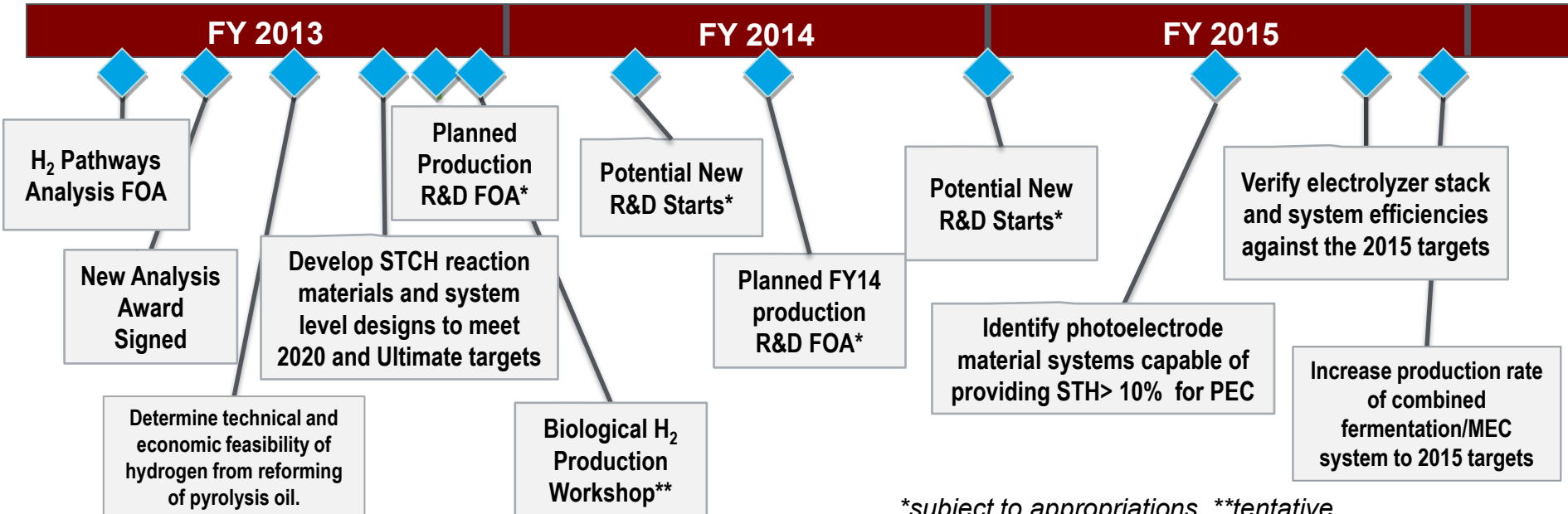


- Increased protein subunits 44-fold (*coolH*) and 16-fold (*coolL*)



## Key milestones and future plans

- Update of production cost targets and Multi-Year RD&D completed and published online
- Released H<sub>2</sub> Pathways Analysis FOA, Award made February FY13
- Potential FOA in Production R&D: Tentative\* - new starts FY14
- Updated Hydrogen Production US Drive Roadmap, to be published this summer
- Tentative Biological H<sub>2</sub> Production Workshop this summer



\*subject to appropriations \*\*tentative

- **Analysis & Testing**

- ORNL
- PNNL
- ANL
- NREL
- SA Inc.

- **Bio-Derived Liquids**

- PNNL
- NREL

- **Electrolysis**

- Giner Electrochemical
- Avalence
- Proton OnSite
- ORNL
- NREL

- **Membranes/Separations**

- TDA (SBIR Phase III)

- **Biological**

- NREL
- J Craig Venter Institute
- University of California, Berkeley

- **Solar High Temperature Thermochemical H<sub>2</sub> Production**

- SNL
- ANL
- SAIC
- Univ. of Colorado, Boulder
- NREL
- SRNL

- **Photoelectrochemical H<sub>2</sub> Production**

- LANL
- LLNL
- Midwest Optoelectronics
- MV Systems
- NREL
- LBNL

## *Hydrogen Production & Delivery Team*

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Angelo Cangialosi (Energetics, Inc.)  
Kim Cierpik (CNJV)

- This is a review, not a conference.
- Presentations will begin precisely at scheduled times.
- Talks will be 20 minutes and Q&A 10 minutes.
- Reviewers have priority for questions over the general audience.
- Reviewers should be seated in front of the room for convenient access by the microphone attendants during the Q&A.
- Please mute all cell phones and other portable devices.
- Photography and audio and video recording are not permitted.



- Deadline to submit your reviews is Friday, **May 24<sup>th</sup> at 5:00 pm EDT.**
- ORISE personnel are available on-site for assistance.
  - **Reviewer Lab Hours:**
    - Monday, 5:00 pm – 8:00 pm (Gateway ONLY)
    - Tuesday – Wednesday, 7:00 am – 8:00 pm (Gateway)
    - Thursday, 7:00 am – 6:00 pm (Gateway)
    - Tuesday – Thursday, 7:00 am – 6:00 pm (City)
  - **Reviewer Lab Locations:**
    - Crystal Gateway Hotel—*Rosilyn Room* (downstairs, on Lobby level)
    - Crystal City Hotel—*Roosevelt Boardroom* (next to Salon A)