

2005 DOE Hydrogen Program Review
Arlington, Virginia

Hydrogen Generation from Biomass-Derived Carbohydrates via the Aqueous-Phase Reforming (APR) Process

Randy D. Cortright, Ph.D.
Virent Energy Systems, Inc.

3571 Anderson Street
Madison, WI 53704
www.virent.com

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This Presentation does not contain any proprietary or confidential information



Project ID# PD7



Overview

Project Timeline

- Start Date - September 2005
- End Date - August 2008

Budget

- Total project funding \$2.62 M
 - DOE share \$1.94 M
 - Contractor share \$0.68 M
- Funding for FY05 None to Date

Barriers

- Barriers addressed
 - Cost Reduction of Distributed Hydrogen Generation from Renewable Liquids
 - By 2015, reduce cost to \$2.50/gge

Partners

- Virent Energy Systems
 - Project Lead – Catalyst/Reactor
- Archer Daniel Midland
 - Feedstock/Demonstration Unit Location
- UOP LLC
 - Systems Engineering
- University of Wisconsin
 - Fundamental Studies



First Year Objectives

- Identify candidate sugar streams (Glucose), document plant integration requirements and associated economic factors.
- Develop catalyst and reactor based on the Aqueous Phase Reforming (APR) process suitable for converting candidate sugar streams to hydrogen.
- Design a baseline hydrogen generation system utilizing the APR process.
- Calculate the thermal efficiency and economics of the baseline APR system.
- Assess the baseline APR system with respect to US Hydrogen program goals and make a go/no go decision to proceed with further development of a demonstration system.



Second and Third Year Objectives

- Develop the detail design of the demonstration APR hydrogen generator system (50 kg/day).
- Fabrication of the integrated hydrogen generator system.
- Install and operate the APR hydrogen generator system at a sugar facility owned by ADM.
- Assess APR hydrogen generator system performance with respect to US Hydrogen program goals.



Approach

Aqueous Phase Reforming (APR)

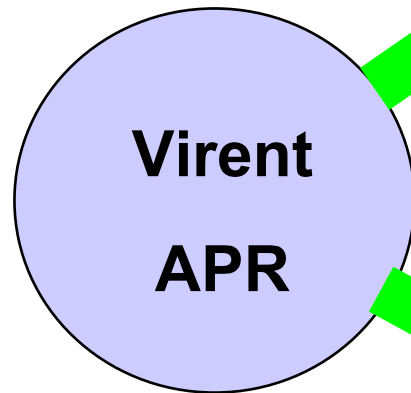
Ethylene Glycol
(AntiFreeze)

Glycerol from
Biodiesel

Sorbitol from
Glucose or
Sucrose sugar

Glucose from
Corn

Sugars and
Sugar
Alcohols from
hemi-cellulose



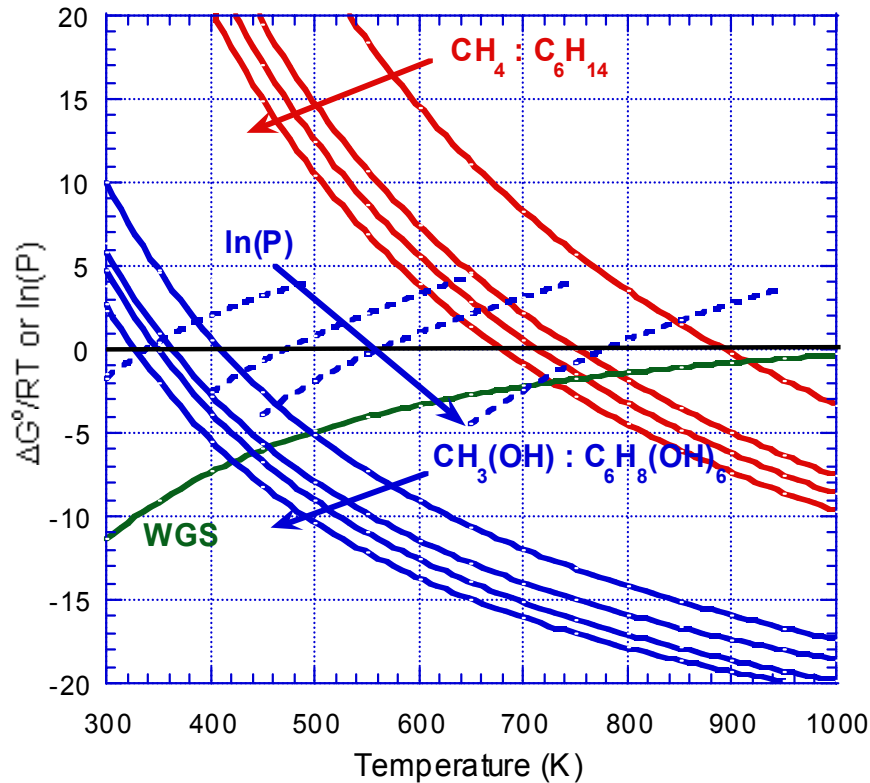
Alkanes

H₂/Alkane Mix

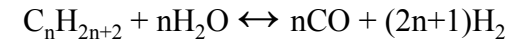
Pure H₂



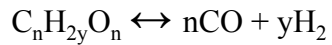
Reforming Thermodynamics



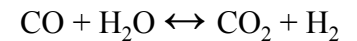
Reforming of Hydrocarbons



Reforming of Oxygenated Compounds



Water-Gas Shift

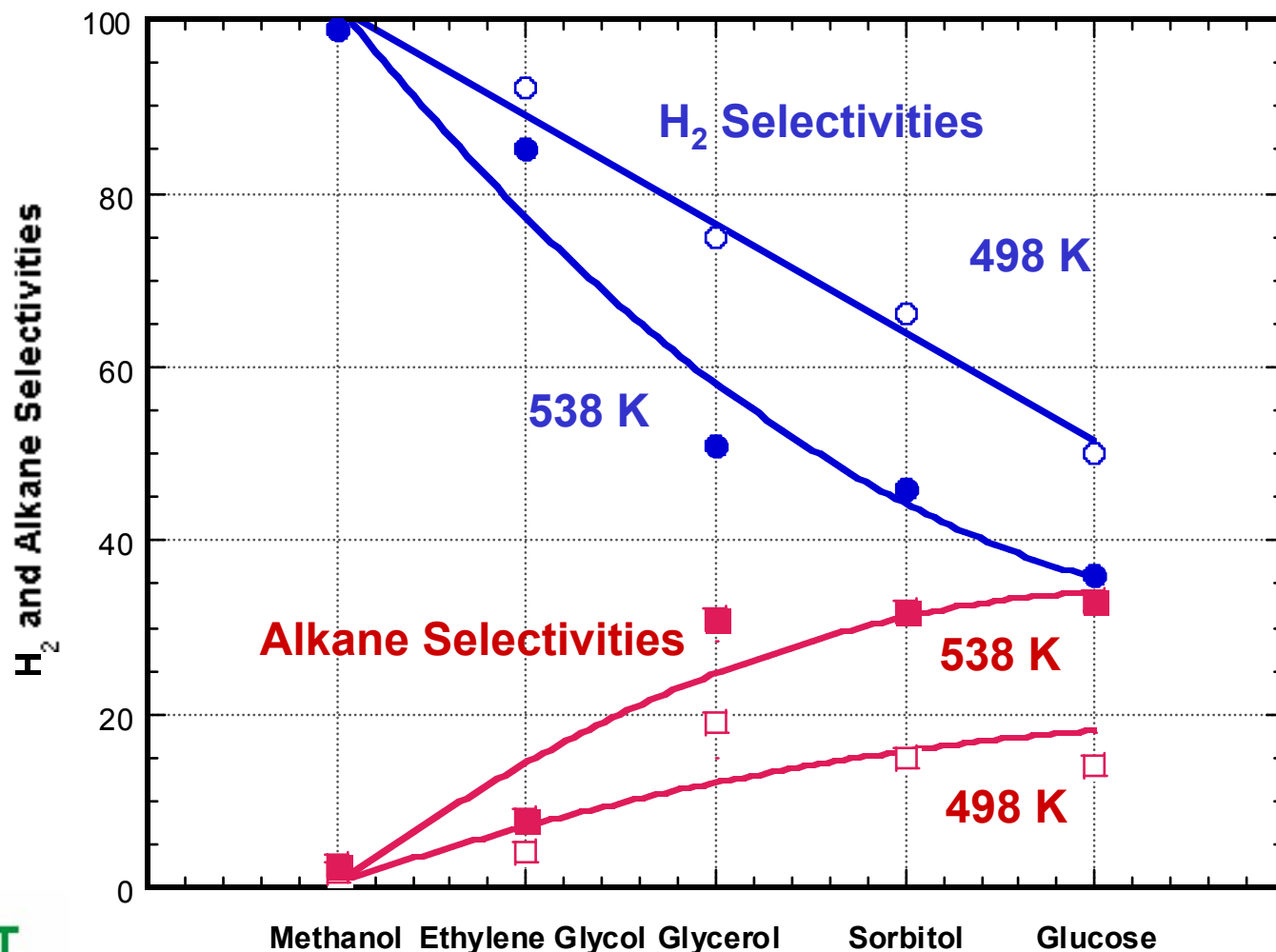


⇒ Equilibrium is favorable for reforming of oxygenated compounds at low temperatures.

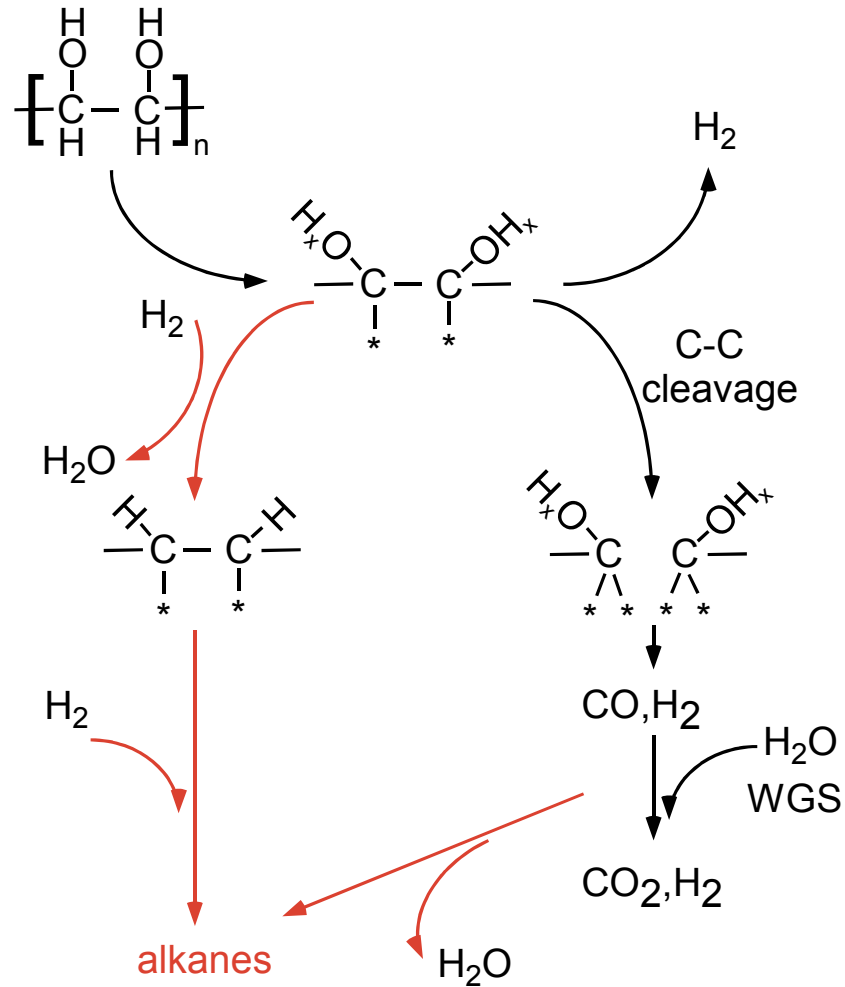


Aqueous-phase Reforming of 1 wt% Methanol, Ethylene Glycol, Glycerol, Sorbitol & Glucose

[Cortright, Davda, and Dumesic, *Nature*, Volume 418, page 964 (2002)]

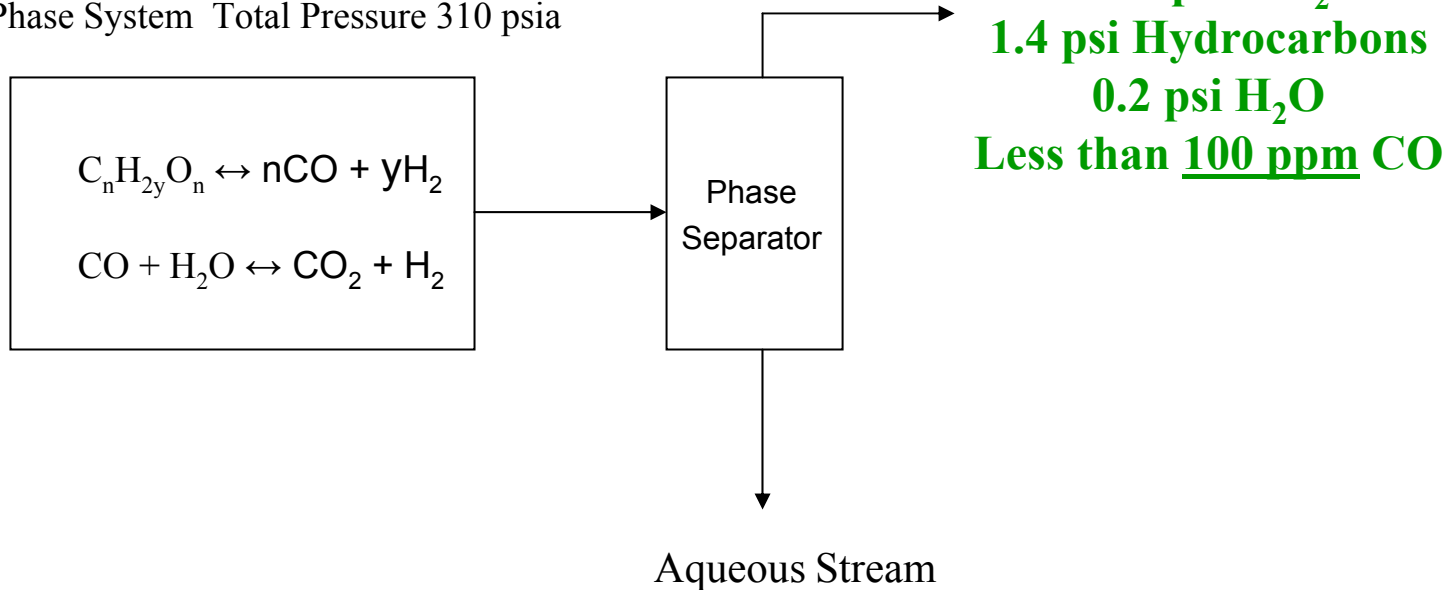


Reaction Pathways



APR Processing of Sorbitol

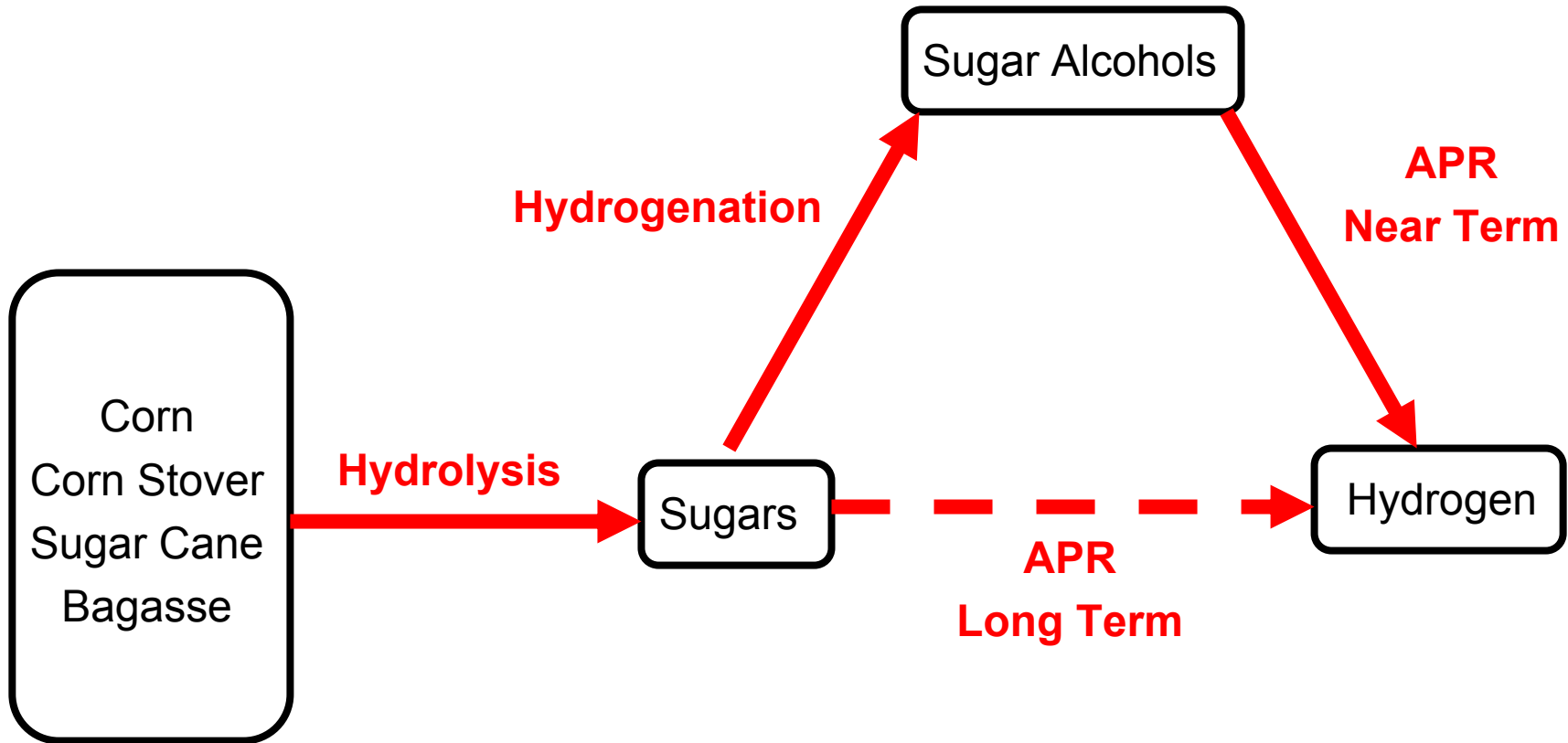
Low Temperature Reforming and Water-Gas Shift
215 °C over Platinum-Based Catalyst
Liquid-Phase System Total Pressure 310 psia



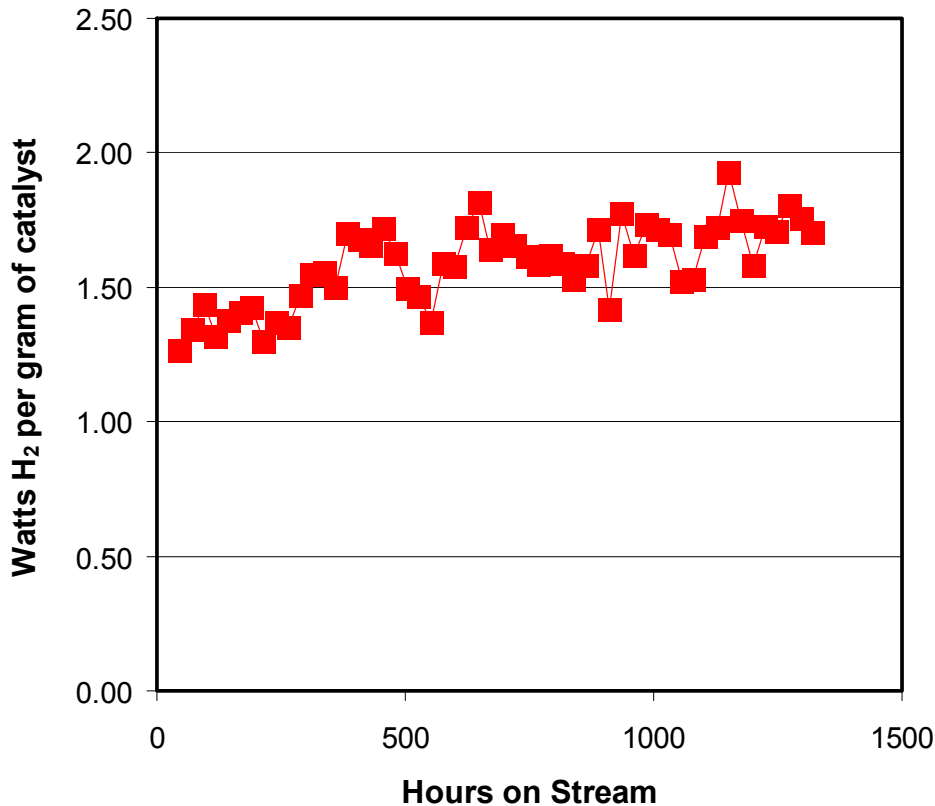
- Utilizes a Single Reactor
- Generation of High Pressure Hydrogen
- Low CO Concentrations



Hydrogen from Biomass-Derived Compounds



Catalyst Lifetime Study



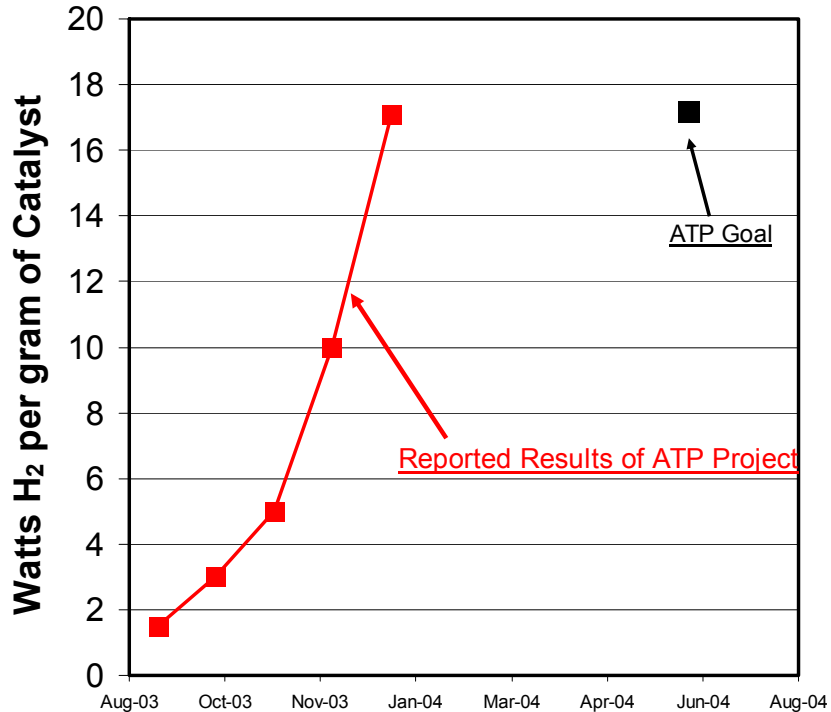
Results from NSF STTR
Phase I Project

Platinum-Based Catalyst
10% Glycerol Feed

Two Month Run from
September 2003 to November
2003



Catalyst Activity Studies



ATP Funded Project

Increased Activity due to Catalyst Composition, Reactor Design, and Reaction Conditions

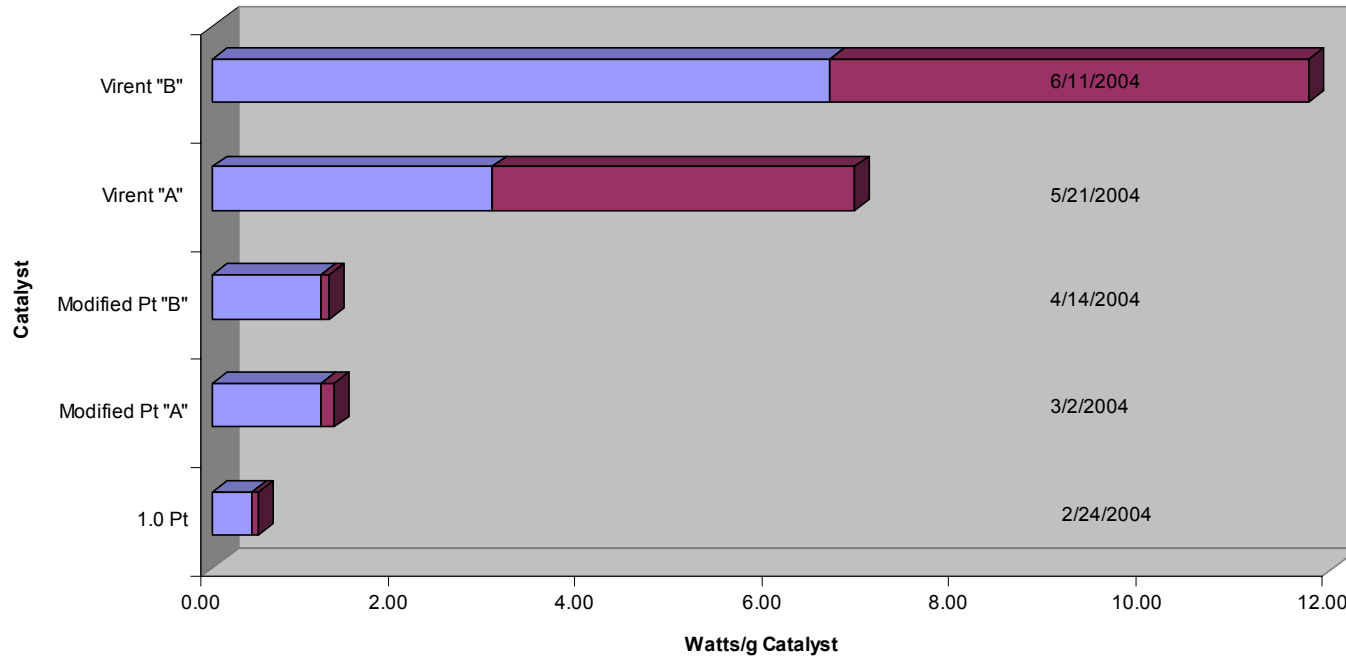
Ethylene Glycol Feed

70 vol% H₂ in reactor Effluent



Precious Metals Catalyst

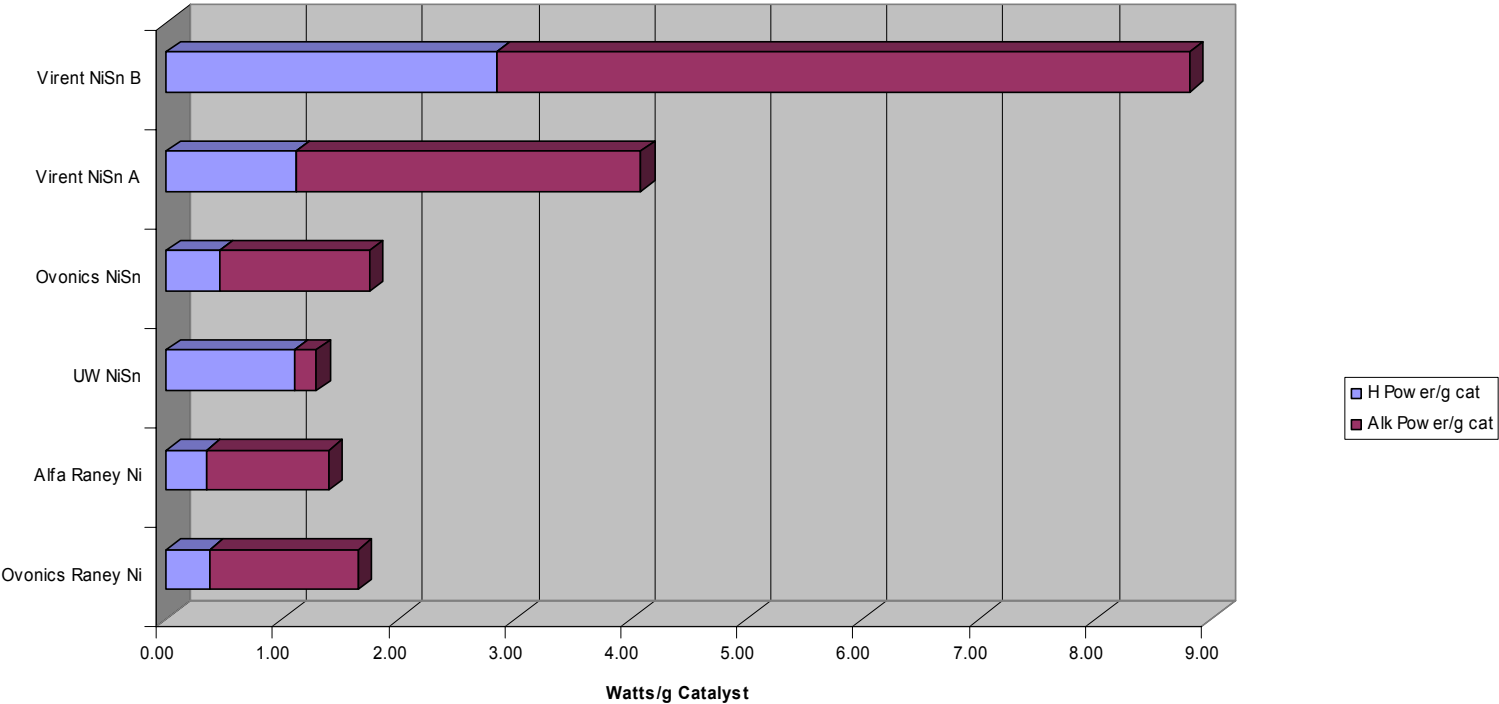
Catalyst Testing Progress February to June 2004
Standard Testing Conditions



	1.0 Pt	Modified Pt "A"	Modified Pt "B"	Virent "A"	Virent "B"
■ Alkane	0.07	0.13	0.09	3.87	5.12
■ Hydrogen	0.42	1.17	1.16	3.00	6.61



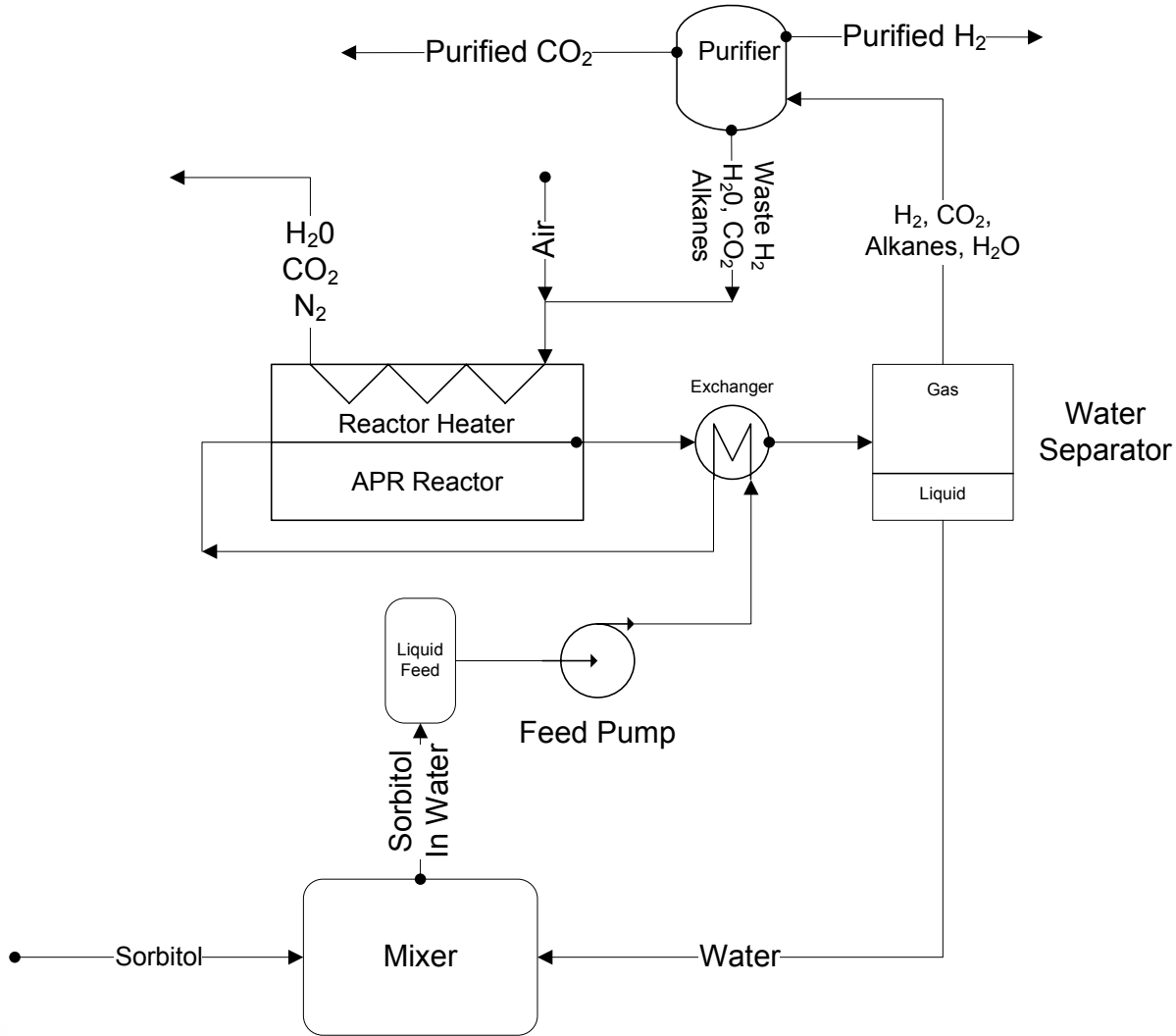
Investigation of Nickel-Based Catalyst



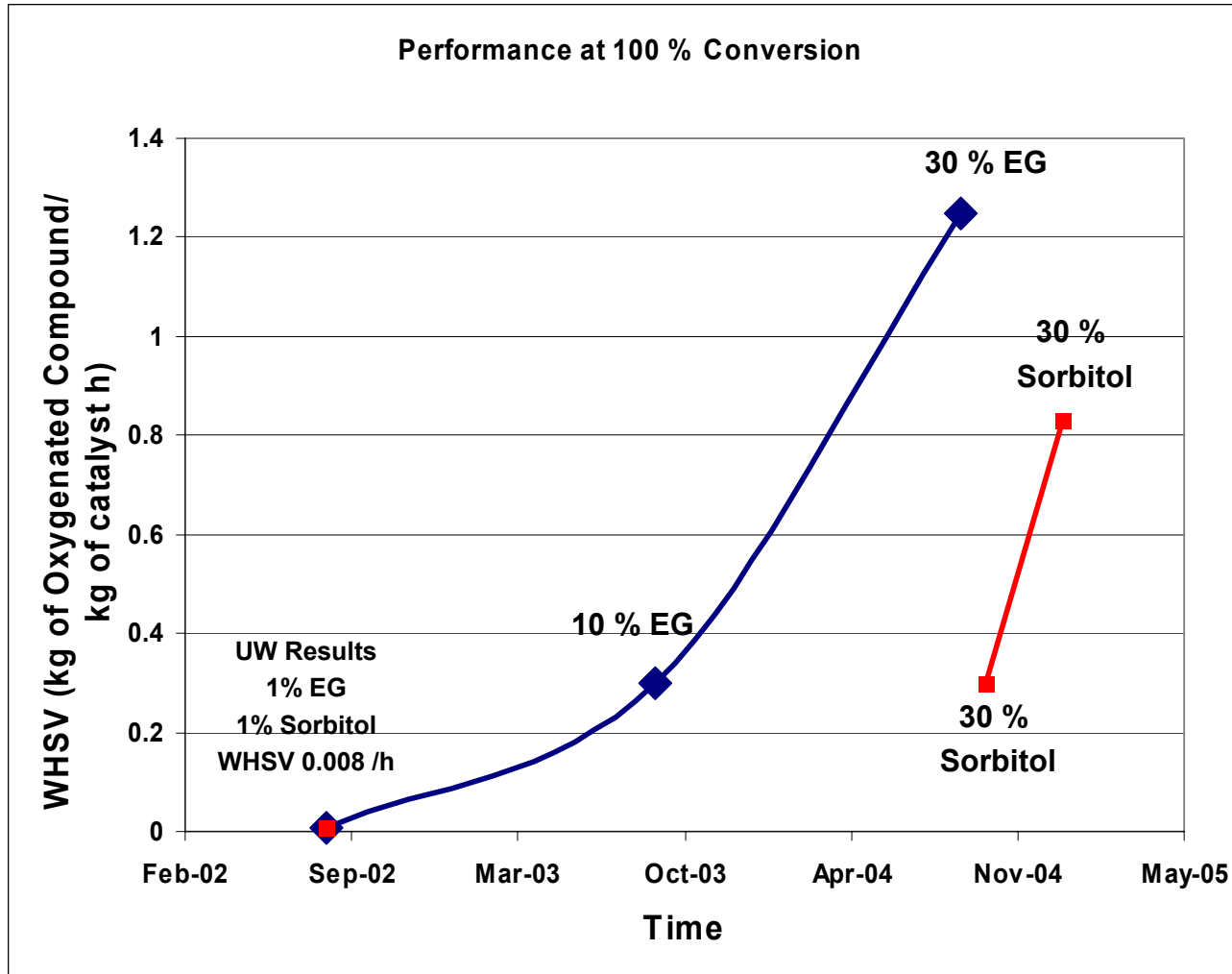
	Ovonics Raney Ni	Alfa Raney Ni	UW NiSn	Ovonics NiSn	Virent NiSn A	Virent NiSn B
Alk Power/g cat	1.28	1.06	0.19	1.29	2.97	5.97
H Power/g cat	0.37	0.34	1.10	0.46	1.12	2.84



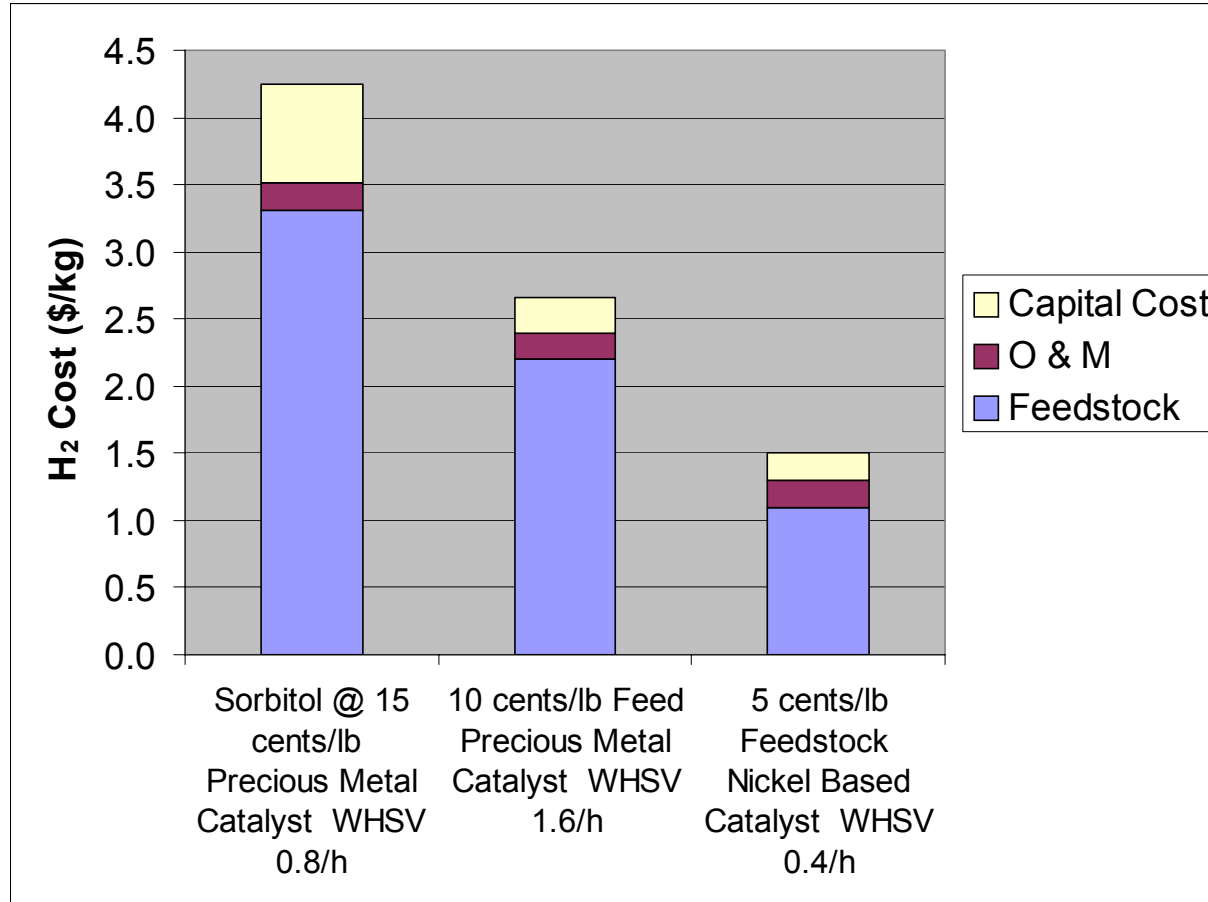
Hydrogen from Sorbitol



APR Catalytic Reactor Improvements



Projected Cost of Hydrogen Generation using the APR Process



Filling Station Application

500 kg H₂/day

5000 kg Sorbitol/day

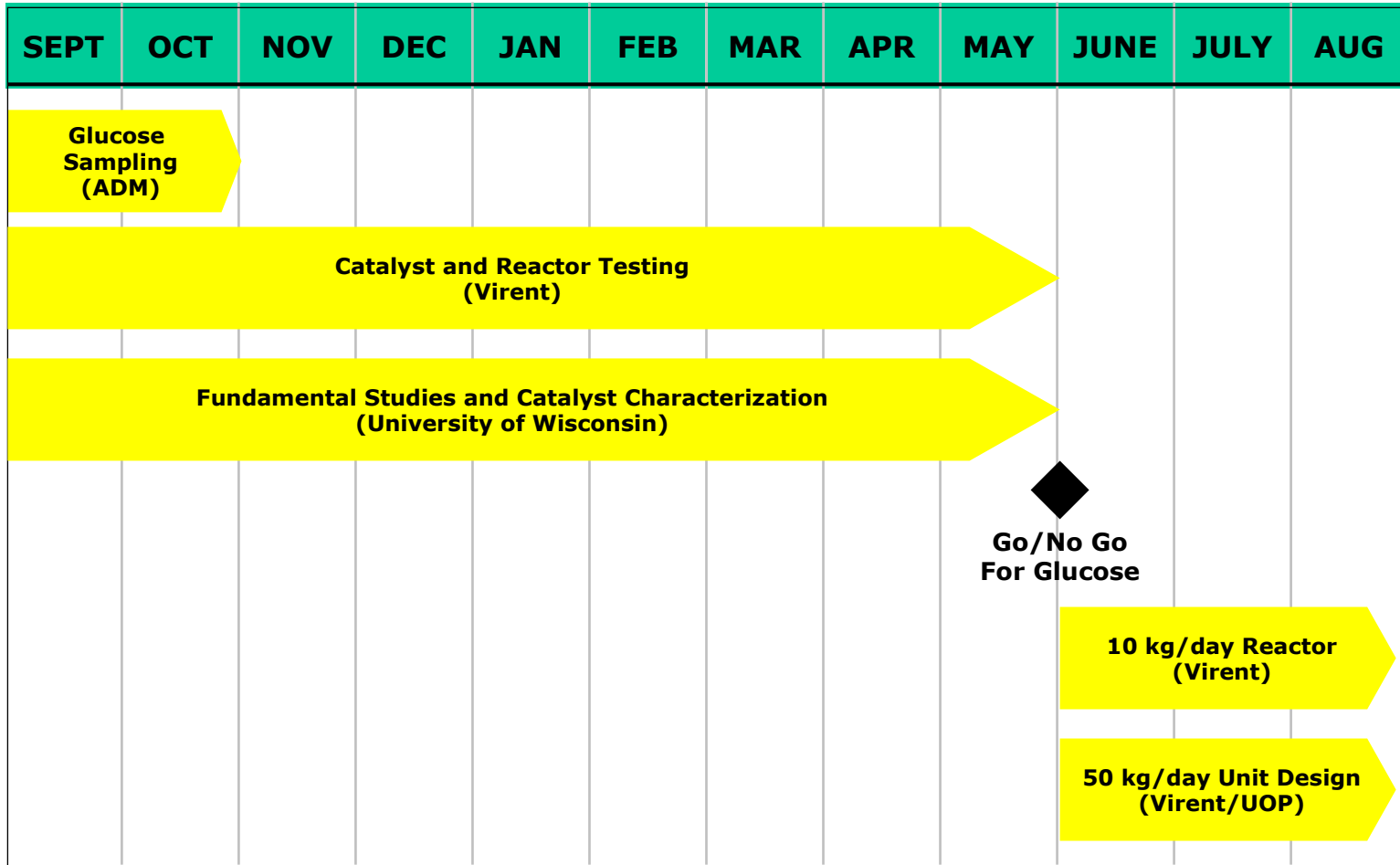
Catalyst Included in Capital Cost

10% ROI
15 Year Depreciation

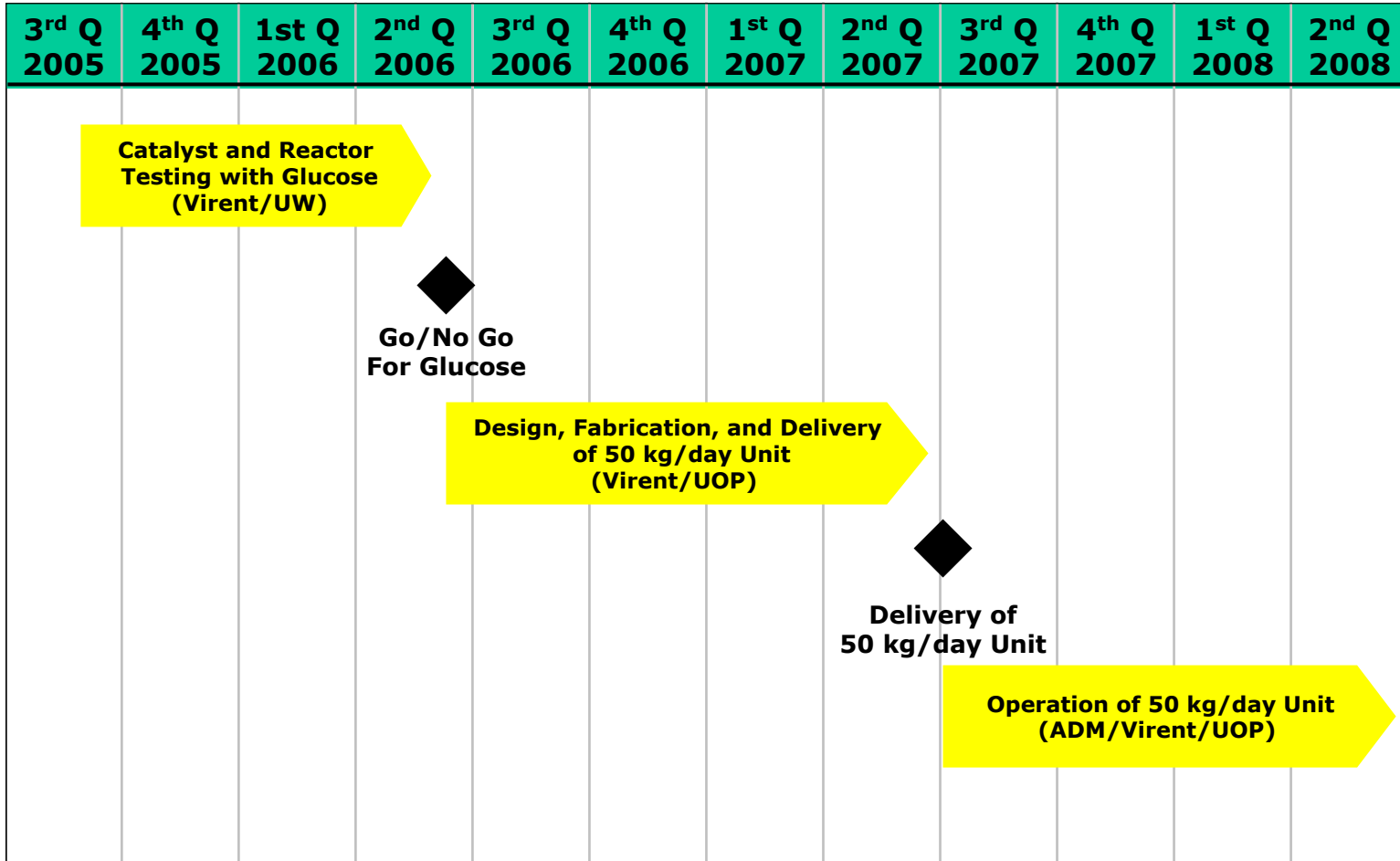
1 kg H₂ is approximately 1 gge



Future Work - First Year Timeline



Future Work - Overall Project Timeline



Facilities

- 6500 square feet facility in Madison, Wisconsin
- 14 Technical Personnel
- 9 test stands available
- Catalyst Preparation Equipment
- 3 GC, 1 TOC, 1 GCMS, and analytical backup from ADM
- Fully-equipped machine shop
 - Experienced machinist for prototype production



Virent Laboratory Hydrogen Safety System

- Hydrogen Exhaust System
 - Two inch SS tube running North to South in lab.
 - Blower is rated at 17000 L/min.
 - All Test Stand Vent into this system.
- Lab Hydrogen Monitor
- Master Permit Relay
 - Permits test stands to operate **unless** Hydrogen Exhaust System or Lab Hydrogen Monitor **are in alarm state.**



Supplemental Information

- Next Slides Contain Requested Supplemental Information



Publications and Presentations

- None to Date



Hydrogen Safety

The most significant hydrogen hazard associated with this project would be accumulation of a significant amount of hydrogen in the laboratory, for example near the ceiling. The impact to personnel, and/or destruction or loss of equipment or facilities could be devastating if that accumulation reached or exceeded the lower explosion limit (LEL) of 4% and subsequently did explode.



Hydrogen Safety

- Our approach to deal with this hazard is:
 - Limited Hydrogen Inventory
 - Hydrogen Exhaust System
 - Laboratory Ventilation
 - Hydrogen Monitor
 - Safety Interlocks

