

Low Temperature Electrolytic Hydrogen Production

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May 23, 2005

Project ID #PDP56



Overview

Timeline

- July 1, 2004
- December 31, 2005
- 60%

Budget

- Total project funding
 - DOE Share: \$244,693
 - Contractor share: \$0
- Funding received in FY04: \$244,693
- Funding for FY05: \$0

Barriers

- Barriers addressed
 - Energy Efficiency
 - System Cost
 - Robust Materials

Partners

- Savannah River National Laboratory: William Summers
- Argonne Natioinal Laboratory: Richard Doctor
- Idaho National Laboratory: Michael Simpson



Objectives

Assist DOE in developing highly efficient, cost affective thermochemical cycles for H₂ production. Our focus is on the electrochemical step used in a variety of thermochemical cycles (*e.g.*, hybrid sulfur, modified Ca-Br).



Approach

- Develop a gas phase proton exchange membrane (PEM) electrolyzer to convert HBr to Br₂ and SO₂ to H₂SO₄
- Quantify the relationships among design and operating parameters.

Our unique gas-phase process has significantly lower mass-transfer resistance that will provide:

- Higher current densities (i.e., lower electrolyzer cost)
- Better thermal management (i.e., higher efficiencies)
- Lower voltages (i.e., higher efficiencies)
- Lower reactant crossover (i.e., reduce poisoning providing longer life)
- Better control of product purity (i.e., higher efficiencies)
- Lower catalyst loadings (i.e., lower electrolyzer cost)



Key Measurements

- Voltage → Electrical Energy and Efficiency
- Current Density → Electrolyzer Size
 (i.e., capital costs)
- Outlet Concentration → Separation Cost and Efficiency
- Voltage Drift → Replacement Costs



Operating Parameters

- Current
- Temperature
- Pressure
- Anode feed flow rate
- Anode feed composition
- Acidity of cathode feed

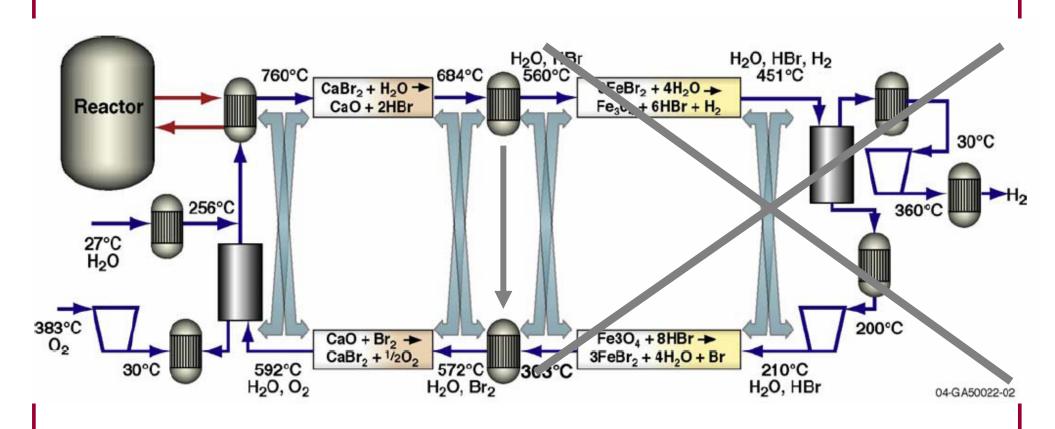


Design Parameters

- Catalyst type and loading
 - → Electrolyzer Costs
 - → Voltage
 - → Poisoning
- Membrane type and thickness
 - → Voltage
 - → Poisoning
 - → Water Management

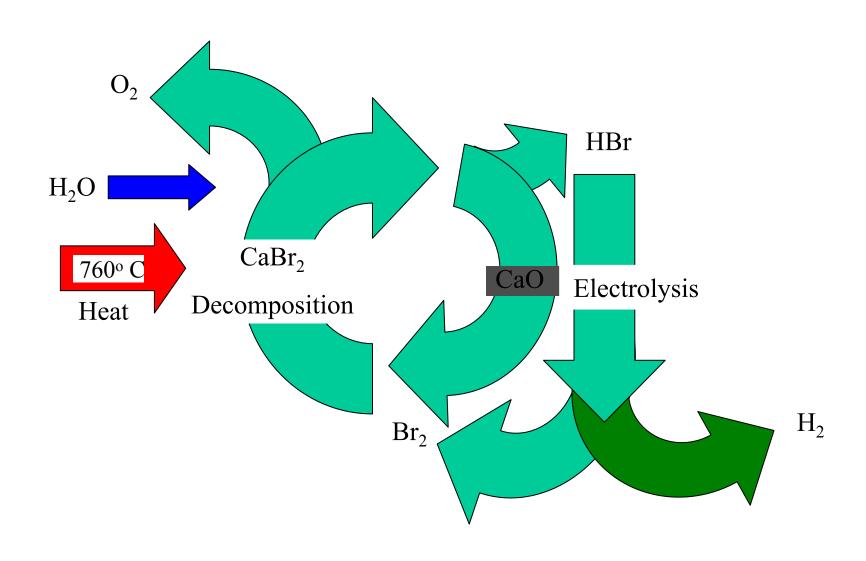


Ca-Br-Fe Cycle (UT-3)





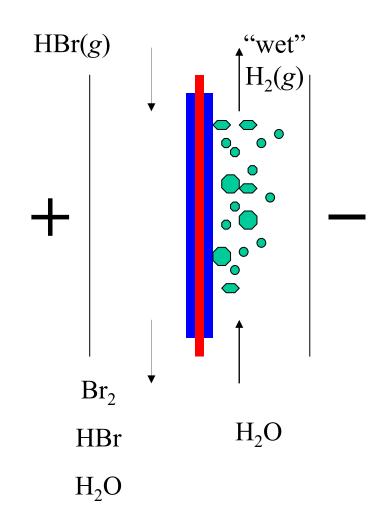
Modified Ca-Br Cycle





Anhydrous HBr Electrolysis Using a PEM Reactor

Anode:



$$2HBr(g) \rightarrow Br_2(g) + 2 H^+(aq) + 2 e^{-1}$$

Cathode:

$$2H^+(aq) + 2 e^- \rightarrow H_2(g)$$

Overall:

$$2HBr(g) \rightarrow H_2(g) + Br_2(g)$$

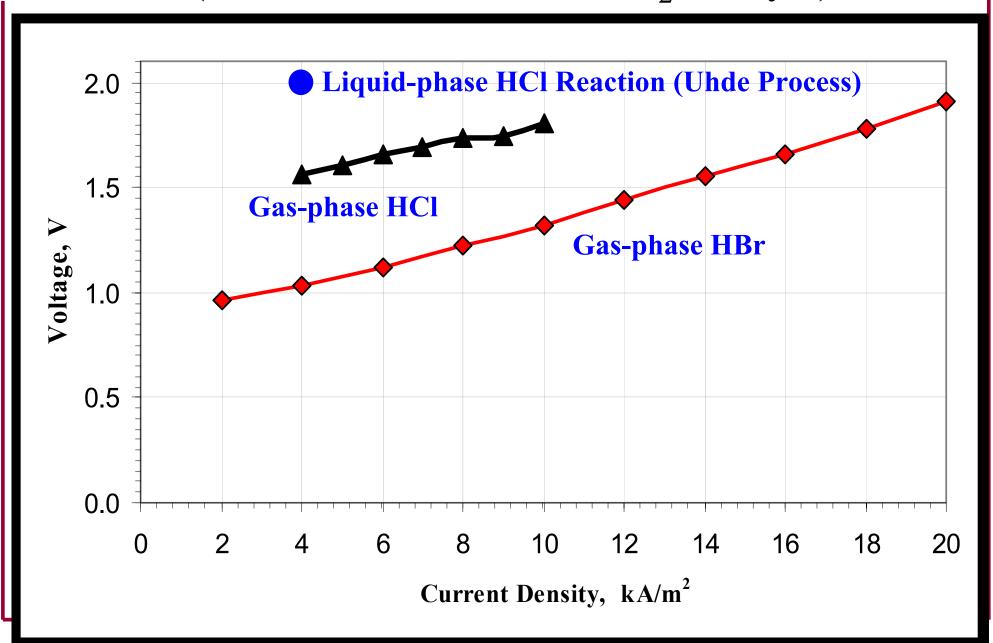
Anode Side Reaction:

$$2 \text{ H}_2\text{O} \rightarrow 4 \text{ H}^+ + \text{O}_2 + 4\text{e}^-$$



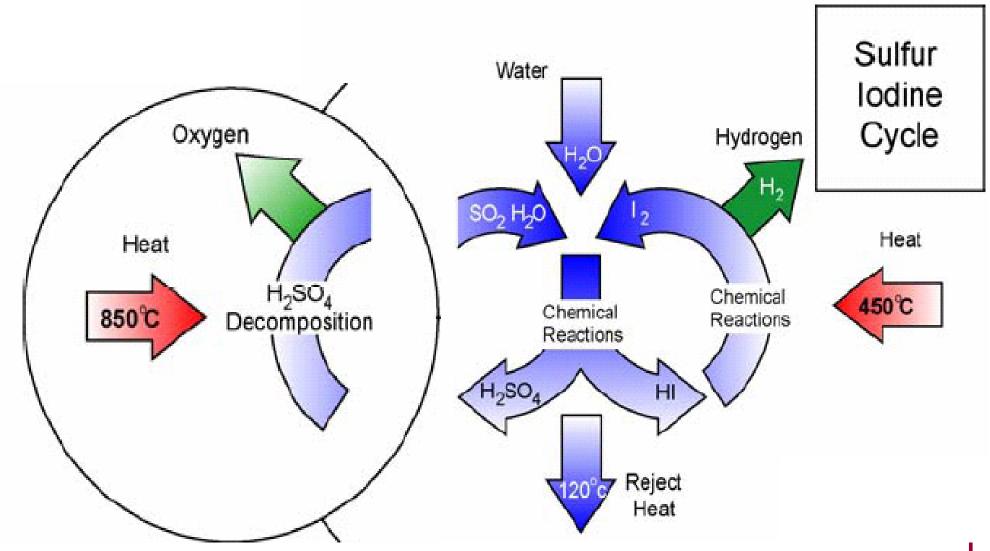
Electrochemical Conversion of Halides

(T= 80° C; P=1.0 atm; RuO₂ catalyst)



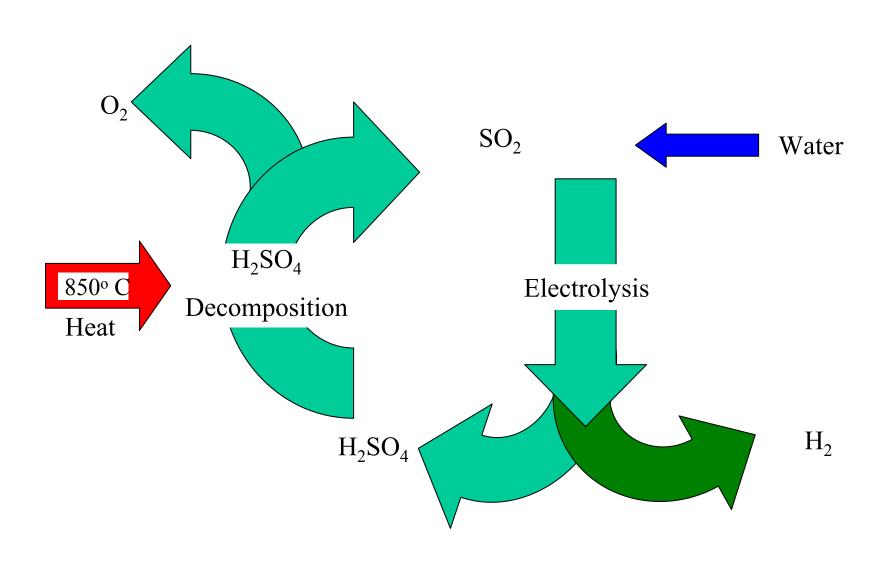


Sulfur Iodine (S-I) Process





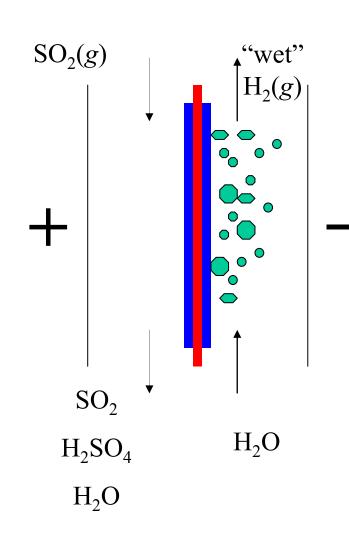
Hybrid Sulfur (HyS) Process





Anhydrous SO₂ Electro-Oxidation Using a PEM Reactor

Anode:



$$SO_2(g) + 2H_2O \rightarrow H_2SO_4 + 2 H^+(aq) + 2 e^-$$

Cathode:

$$2H^+(aq) + 2 e^- \rightarrow H_2(g)$$

Overall:

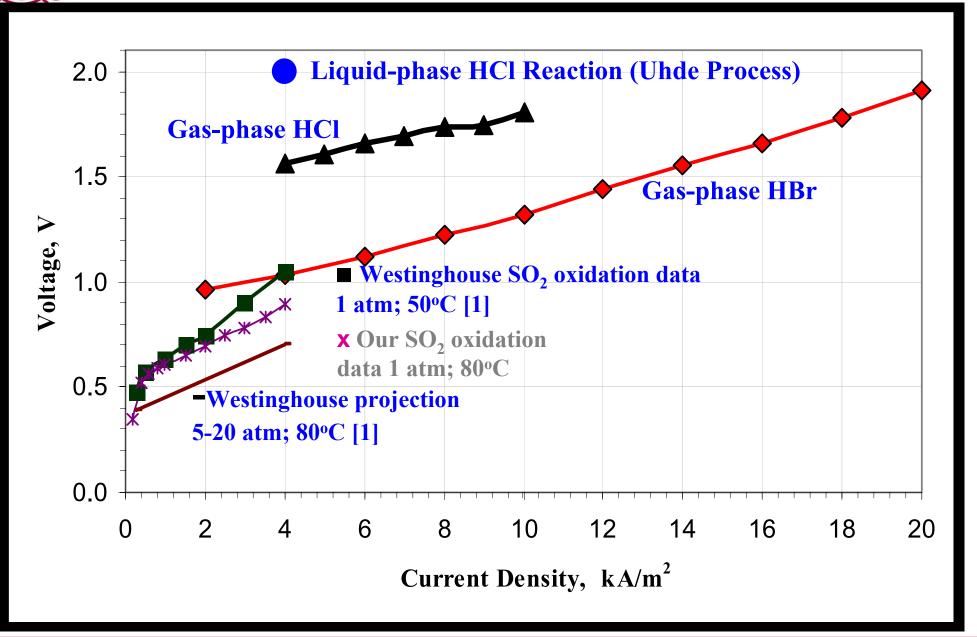
$$SO_2(g) + 2H_2O \rightarrow H_2(g) + H_2SO_4$$

Poisoning Reaction:

$$SO_2 \rightarrow S + O_2 + 2e^-$$

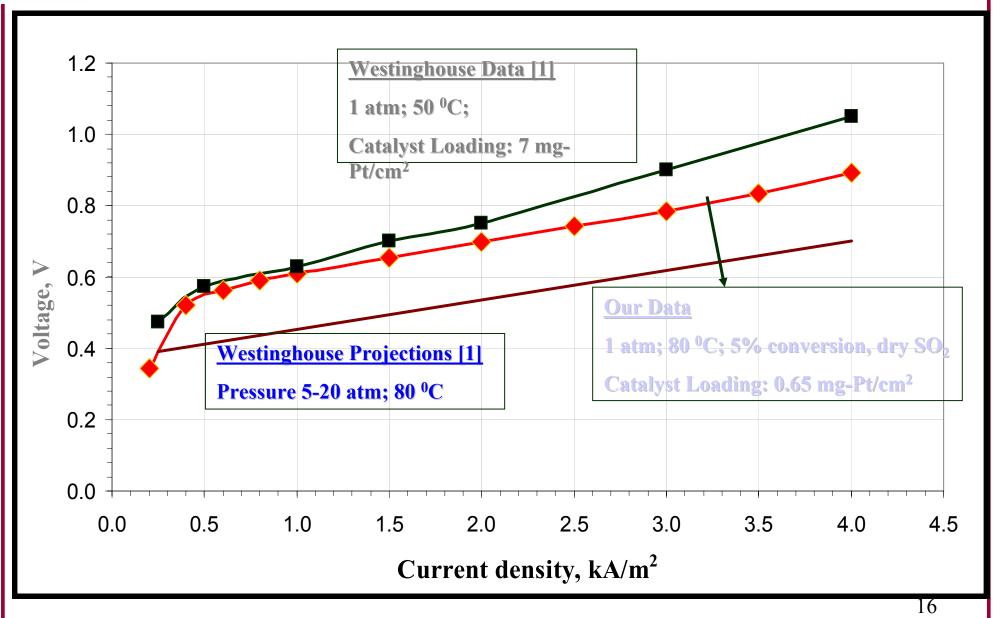


Low Temperature Electrolysis





Oxidation of SO₂ to H₂SO₄

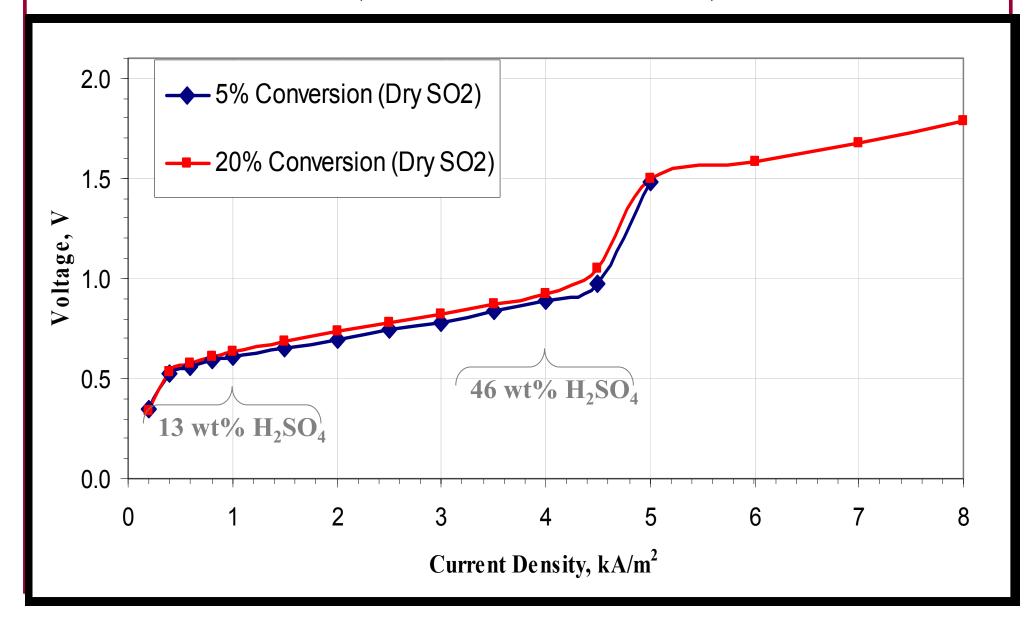


[1] P.W. Lu et. al., J. Appl. Electrochem., 347 (1981).



Oxidation of SO₂ to H₂SO₄

 $(T=80^{\circ}C; P=1.0 atm)$





Conclusions for Gas-Phase HBr Oxidation

• Electrochemical conversion of HBr to Br_2 and H_2 in a PEM reactor is very promising . (20 kA/m² @ < 2.0V)

Future Work

- Measure performance as a function of temperature and pressure
- Develop mathematical models that can predict cell performance. These models could be fed into process flowsheet models being developed by Argonne National Laboratory.



Conclusions for Gas-Phase SO₂ Oxidation

• Electrochemical conversion of SO₂ to H₂SO₄ and H₂ in a PEM reactor is encouraging (*e.g.*, 4 kA/m² @ 0.9V).

Future Work

- Measure performance as a function of temperature and pressure
- Develop mathematical models that can predict cell performance. Feed these models into process flowsheet models being developed by Savannah River National Laboratory.

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Technical Presentations (speaker underlined)

- <u>J. W. Weidner</u>, P. Sivasubramanian, R. Ramasamy, C.E. Holland and F. Freire, "Electrochemical Generation of Hydrogen via Thermochemical Cycles," The American Institute of Chemical Engineerings, Atlanta, GA, April, 2005.
- <u>J. W. Weidner</u>, P. Sivasubramanian, and F. Freire, "Electrochemical Conversion of Anhydrous HBr to Br2 for Hydrogen Production," The Electrochemical Society, Honolulu, HI, October, 2004. Please list any publications and presentations that have resulted from work on this project.



Hydrogen Safety

We produce hydrogen via our electrochemical reactor. However, the concentrations are low and the vented in a hood. The risk of a hydrogen explosion or very low.