

Development of an Advanced Chemical Hydrogen Storage and Generation System

- Participants in the Chemical Hydrogen Storage Center of Excellence -

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Project ID #: ST 7
Contract #: DE-FC36-05GO15056

Overview

Timeline

- Project start date: February 2005
- Project end date: February 2010
- Percent complete: 20%

Barriers

- Weight and Volume
- Efficiency
- Heat removal

Budget

Total project funding (5 Year)

- DOE share: \$2.4 million (80%)
- MCEL share: \$0.6 million (20%)

Funding received for FY05:

- \$200 K

Funding for FY06:

- \$400 K requested
- \$250 K obligated

Project Targets

	2005	2006	2007
System volumetric capacity (kWh/L)	1.0	1.1	1.2
System wt%	3.9	4.2	4.5

Partners

Center of Excellence – Chem. H₂ Storage
PNNL – System modeling and eng.
RandH, PSU, LANL – Regeneration

Objectives

Overall:

- To Improve capability to store and release H₂ from chemical hydride
- To Meet DOE 2007 target and beyond:
 - 1.2 kWh/L (36 g H₂/L) and 1.5 kWh/kg (45 g H₂/kg).
- To leverage MCEL engineering expertise and guide Center research

◆

Last Year:

- Data mining on the synthesis and regeneration of B-O → B-H.
- Rapid screening of options
- Initiate system analysis and reactor module development.

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This Year:

- Develop modeling tool for hydrogen generation reactor
- Validate modeling results with experimental data
- Conceptual design based on modeling
- Maintain progress to meet DOE go/no-go decision on SBH

Status at Start of Project

Hydrogen Generation System Metrics

Criteria	2007	2010	MCEL current	MCEL target for Phase I
Specific energy	4.5 wt% 1.5 kWh/kg	6 wt% 2.0 kWh/kg	3.9 wt%	4.5 wt%
Flow rate	0.02	0.02	0.02	✓
Density	36 g/L (1.2 kWh/L)	45 g/L (1.5 kWh/L)	33 g/L (1.0 kWh/L)	36 g/L (1.2 kWh/L)
Storage system cost	\$6 /kg H ₂ stored	\$4 /kg H ₂ stored	\$ 6.7 /kg H ₂ stored	\$ 6 /kg H ₂ stored

Accomplishments to Date

- Reactor modeling activity started and progressing well
 - Developed reactor packing sub-module
 - Completed Lattice Boltzmann microscopic modeling of reactant flow in the reactor
 - Established macroscopic reactor model that matches the experimentally observed parameters
- Generated experimental data to validate modeling results.
- Started to use the model to predict performance parameters
- Begin to build the experience and modeling tool that can be applied to other chemical hydrogen storage systems

Improve System Level Storage Capacity

Reduce Fuel Volume

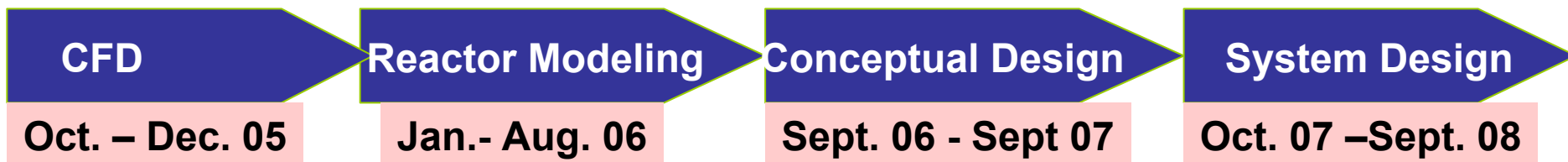
- Increase fuel concentration
- Improve catalyst's ability to process concentrated fuel
- Volume exchange tank design

Reduce Volume of Balance of Plant (BOP)

- Relationship between reactor liquid hold-up and size of ballast
- Manage heat exchange – size of exchanger
- Improve gas-liquid separation – size of separator

System Development Approach

Using NaBH₄ as Example



<ul style="list-style-type: none"> Develop modeling tools Lattice Boltzmann calculations Macroscopic modeling Star-CD data processing Validate model 	<p style="text-align: right;">PNNL Collaboration</p> <ul style="list-style-type: none"> Optimize Conversion Optimize reactor dimensions Increase throughput Fluid dynamics
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- Reactor features
- BOP designs
- Safety evaluation

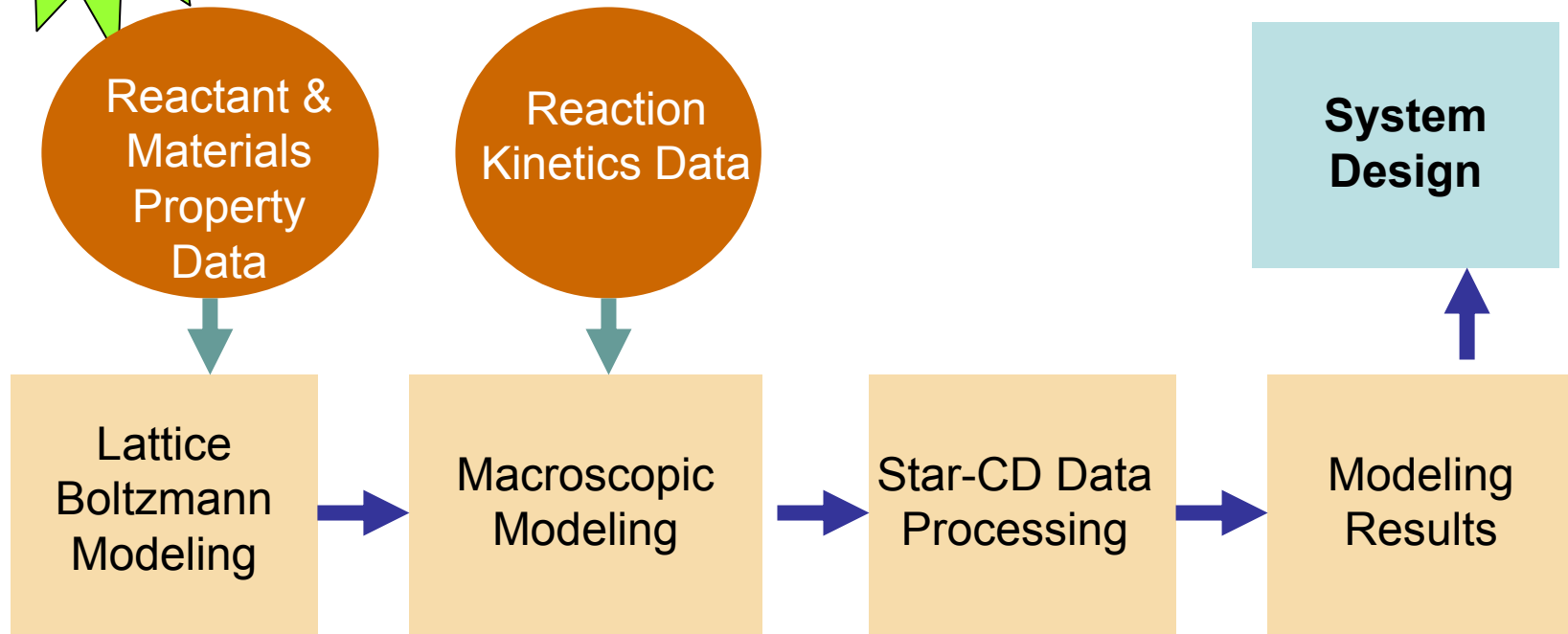
Go/no-go Decision

- Sub-system testing
- BOP testing
- System testing
- Prototype Demo:**
- > 45 g H₂/kg**
- > 36 g H₂/L**

System Development Approach

PNNL-MCEL
Collaboration

Modeling Approach Overview



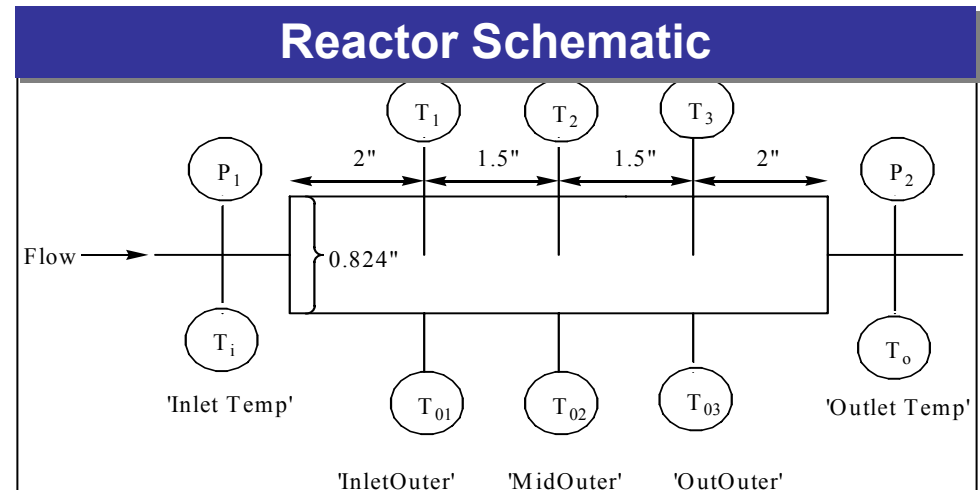
Develop "Tool Box" applicable to other chemical hydrogen storage systems

- Means to handle microscopic reaction basics
- Means to handle multi-phase reactions
- Means to incorporate thermodynamic and kinetic data
- Means to apply to other chemical hydride systems

Reactor for H₂ Generation

Preliminary Modeling

- 10 x 100 segmentation of reactor – simplifies overall heterogeneous microscopic properties into 1,000 individual homogeneous sections
- Solves the flow, energy and species transport equations for multiphase flow through a catalyst bed reactor
- Two-dimensional (axial and radial) finite-volume formulation
- Transient solution to reach a steady state

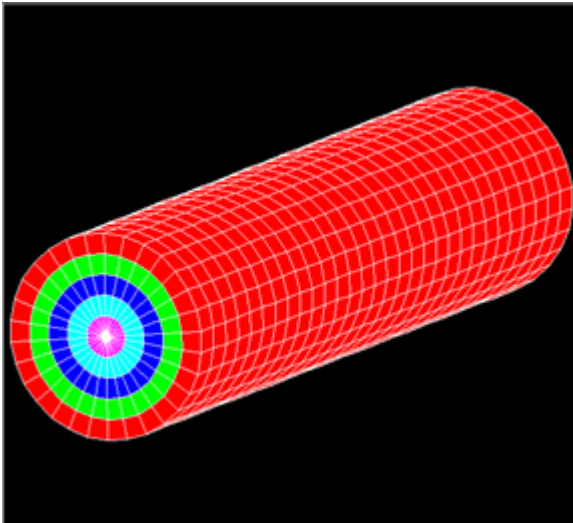


Technical Accomplishments

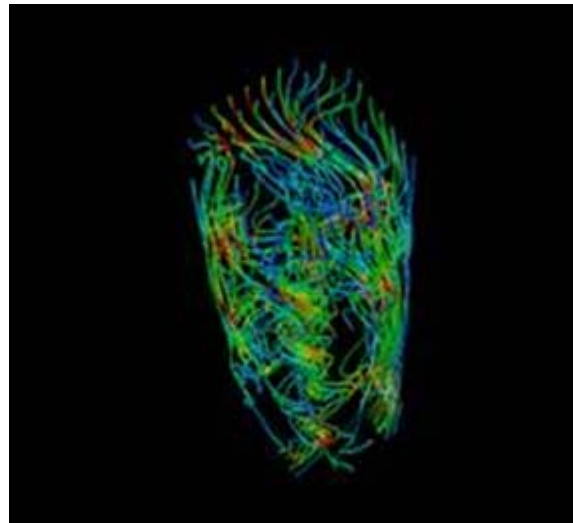
STAR-CD Data Process

- CFD reactor modeling program
- Commercially available from CD-adapco
- Customized subroutines for specific reactions (PNNL/MCEL)
 - Utilizes code from Fortran method
- Powerfully post-processing functions
- Complex to use for modeling heterogeneous catalytic surface reactions

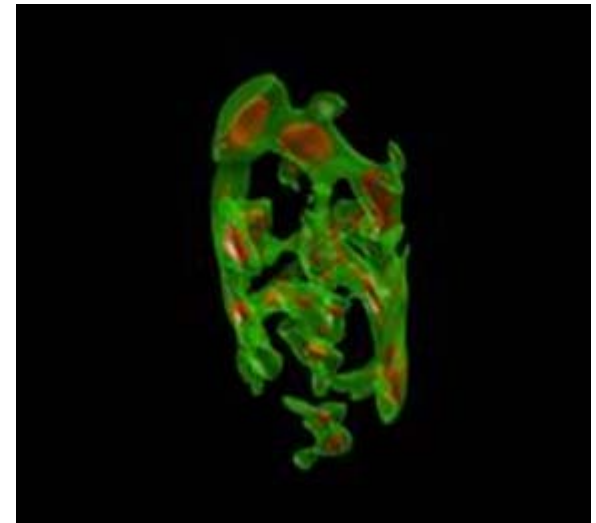
Reactor Geometry



Streamlines



High Velocity Regions

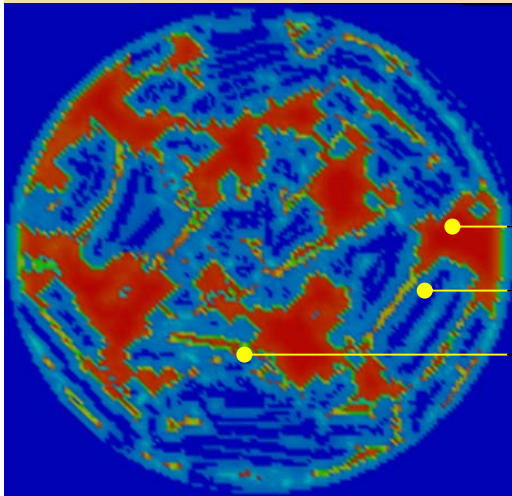


Technical Accomplishments

Lattice-Boltzmann Modeling (PNNL)

- **Microscopic discreet modeling**
 - Detailed nodes model separate solid, liquid, and gas regions/interfaces
 - Determine transport and reaction parameters for use in macroscopic model
- **Advantage** - includes effect of catalyst geometry, less empiricism
- **Process Design Implication**
 - Need efficient gas separation mechanism
 - Design of catalyst

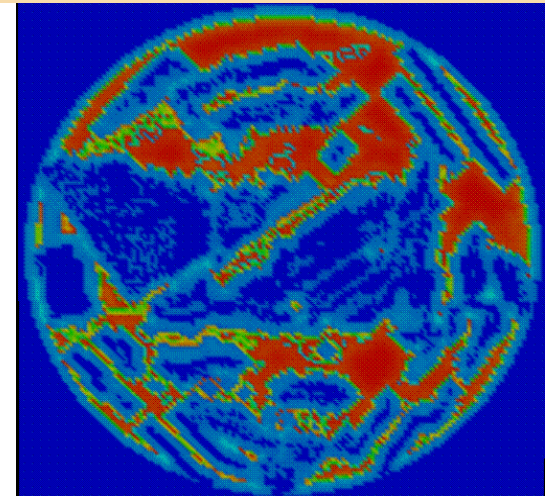
Example Data



Radial slices at different
lengths along the reactor

- (Red) Liquid phase
- (Dark Blue) Solid phase
- (Light Blue) Gas phase

“Gas Shielding”



Technical Accomplishments

Macroscopic Reactor Modeling

- **Validation parameters**

- SBH conversion
- Axial reactor temperature
- Overall reactor pressure drop
- Hydrogen flow rate

- **Simulation**

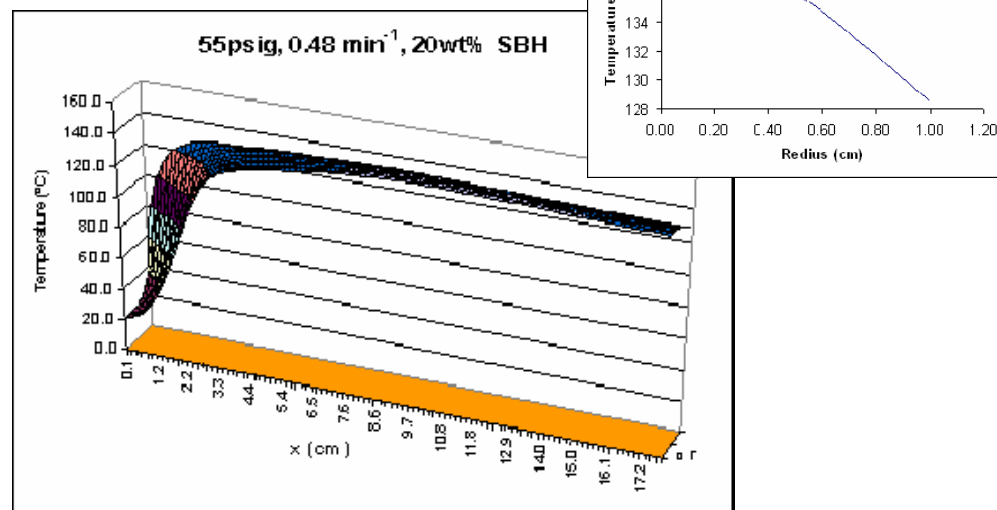
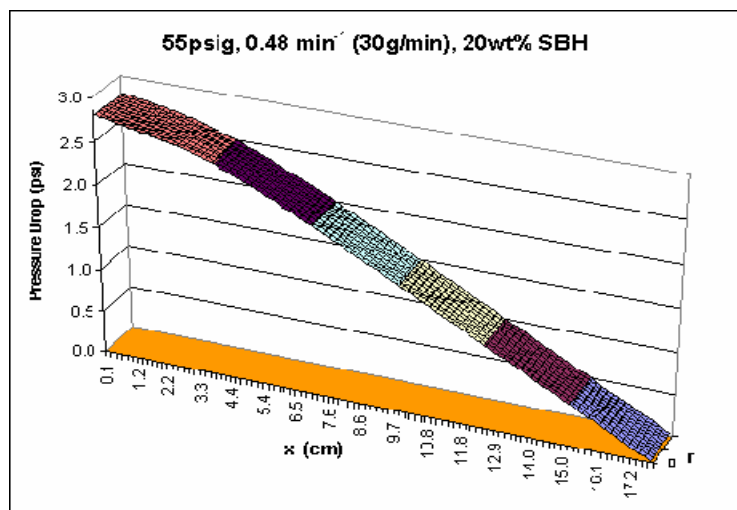
- NaBO₂ liquid flow
 - (NaBO₂ concentration)
- Water vapor flow
- Hydrogen distribution
- Void fraction

- **Optimization**

- Fuel space velocity
 - (flow rate)
- Reactor parameters
 - Total volume
 - D/L ratio
 - Geometry
 - Pressure
- Heat removal
- Fuel concentration
- Catalyst packing density

Validating the Model:

- Pressure Drop and Reactor Temperature

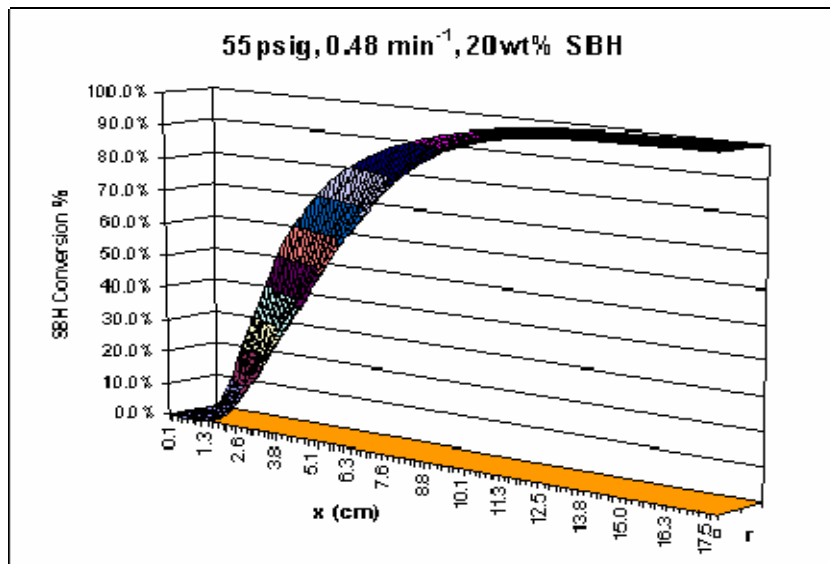


- Pressure drop is affected by catalyst porosity & packing density
- Temperature profile varies with:
 - system pressure; space velocity,
 - fuel concentration; water vaporization
- Simulated parameters match experimental measurements

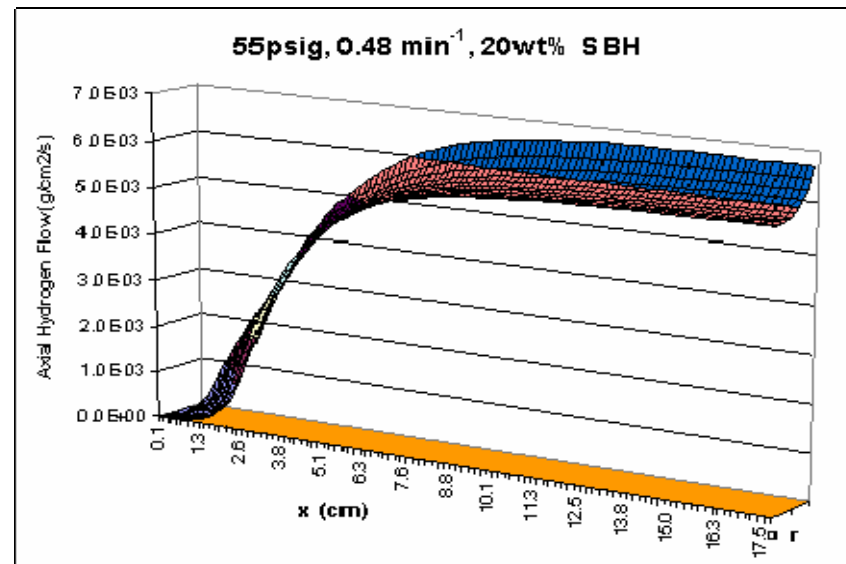
Validating the Model:

- SBH Conversion and H₂ Flow

SBH % Conversion



H₂ Flow Rate



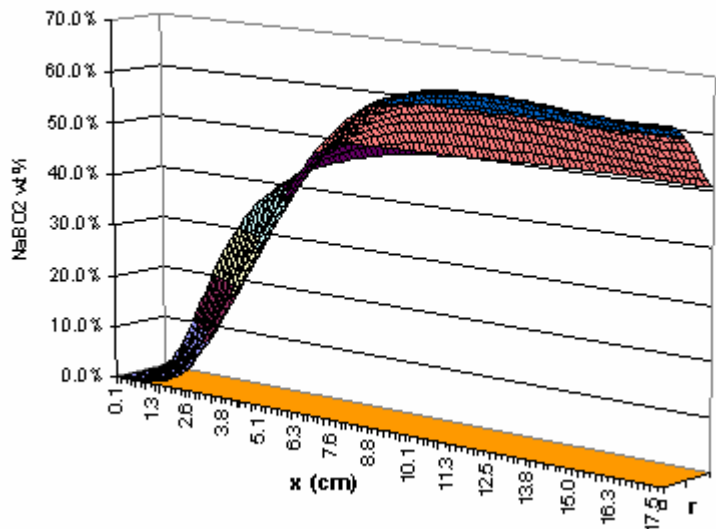
$$-rA = k_0 e^{-Ea/RT} [BH_4]$$

Accuracy of model generated conversion profile relies on the accuracy of kinetics equations describing the reactions

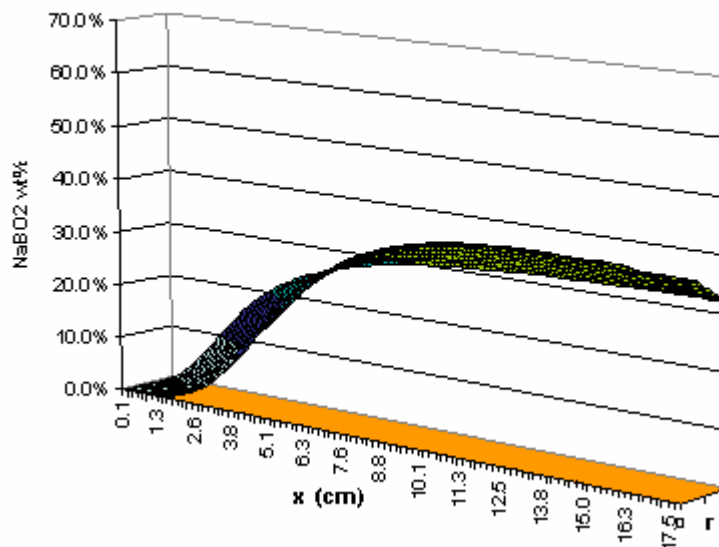
Simulated Results:

- “NaBO₂” Concentrations

55psig, 0.48 min⁻¹, 20wt% SBH



55psig, 0.48 min⁻¹, 15wt% SBH



- High NaBH₄ concentration can result in NaBO₂ concentrations that exceed the solubility limits
- Super-saturation has been observed experimentally
- Active management of reactor temperature (via reactor pressure) can mitigate the problem of borate precipitation

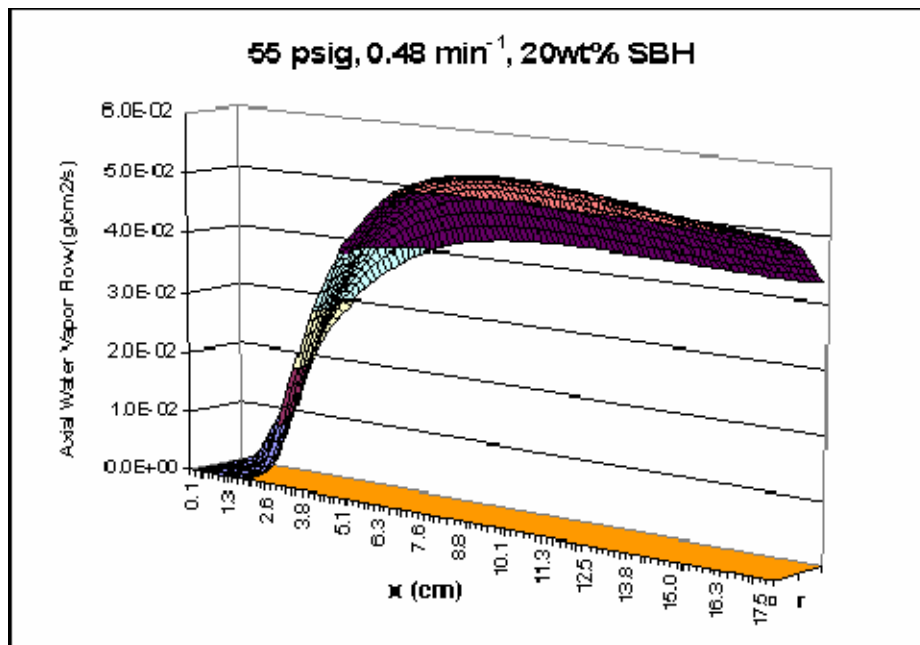
Solubility Table

Temp.	NaBO ₂ wt%
0°C	14.50
10°C	17.0
20°C	20.0
30°C	23.6
40°C	27.9
50°C	34.1
60°C	38.3
70°C	40.7
80°C	43.7
90°C	47.4
100°C	52.4

Simulated Parameters:

- Flow of Water Vapor

Profile of Vapor Phase Water Flow



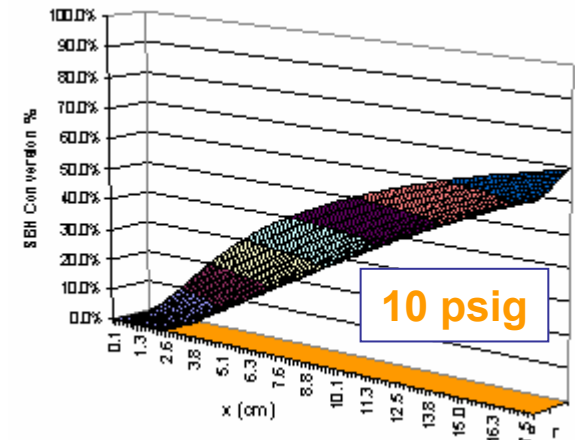
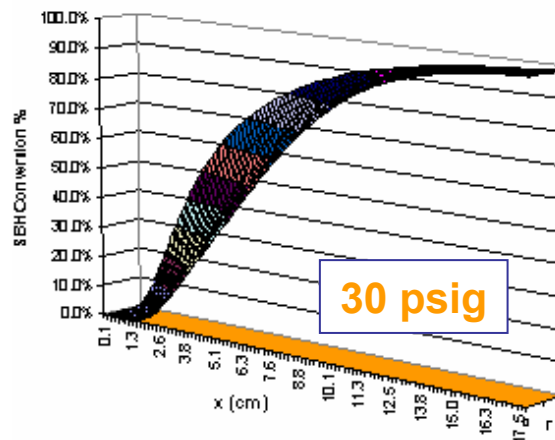
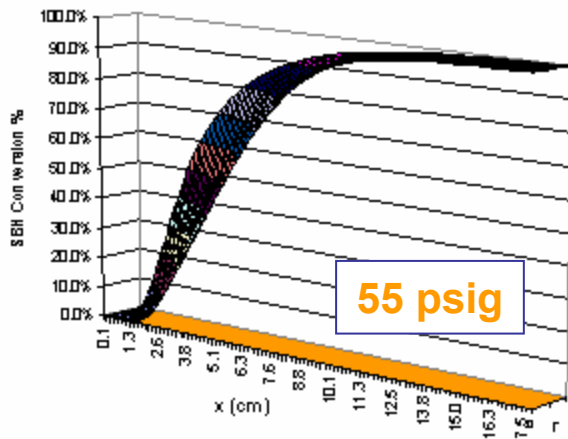
- High press. and low temp. → low H₂O vapor pressure
- Low gas volume → low void space → better contact between reactants and catalyst
- **Liquid water is favored to solubilize borate by-product.**

Optimization Using the Model

- Effect of System Pressure

NaBH₄ Conversion Profile At Various Reactor Pressures

0.48 min⁻¹ for 20 wt.% SBH



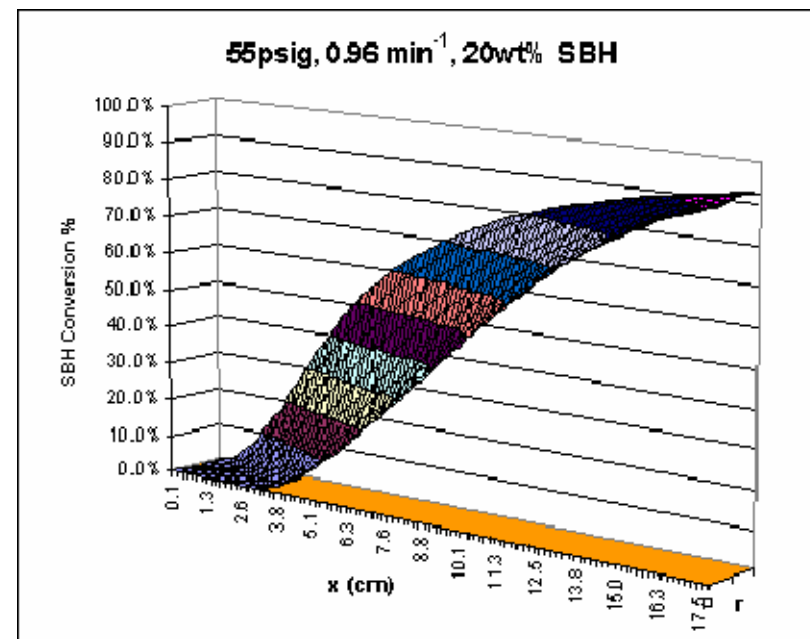
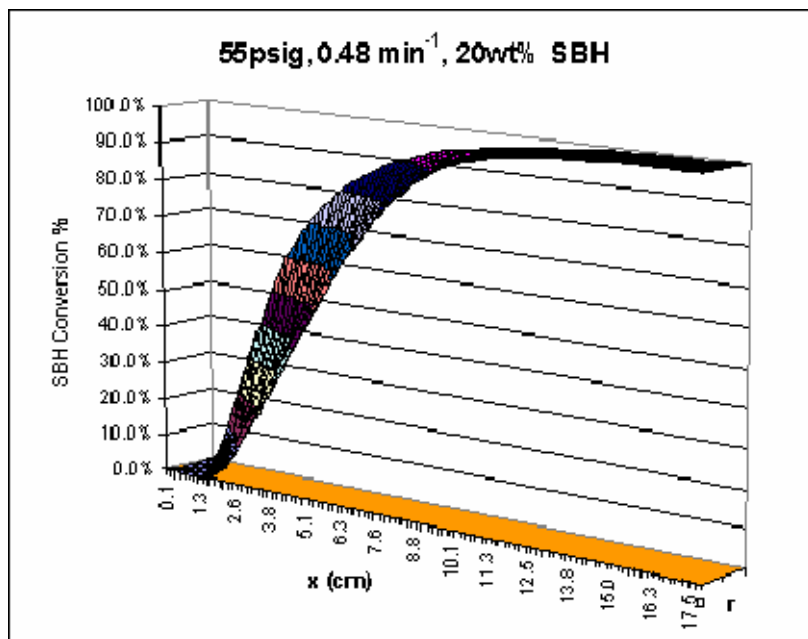
- Simulation provides additional insight within the reactor
- System pressure governs peak temperature in the reactor
- High system pressure is favored to increase SBH conversion

Will
Affect
BOP

Optimization Using the Model:

- Effect of Fuel Space Velocity

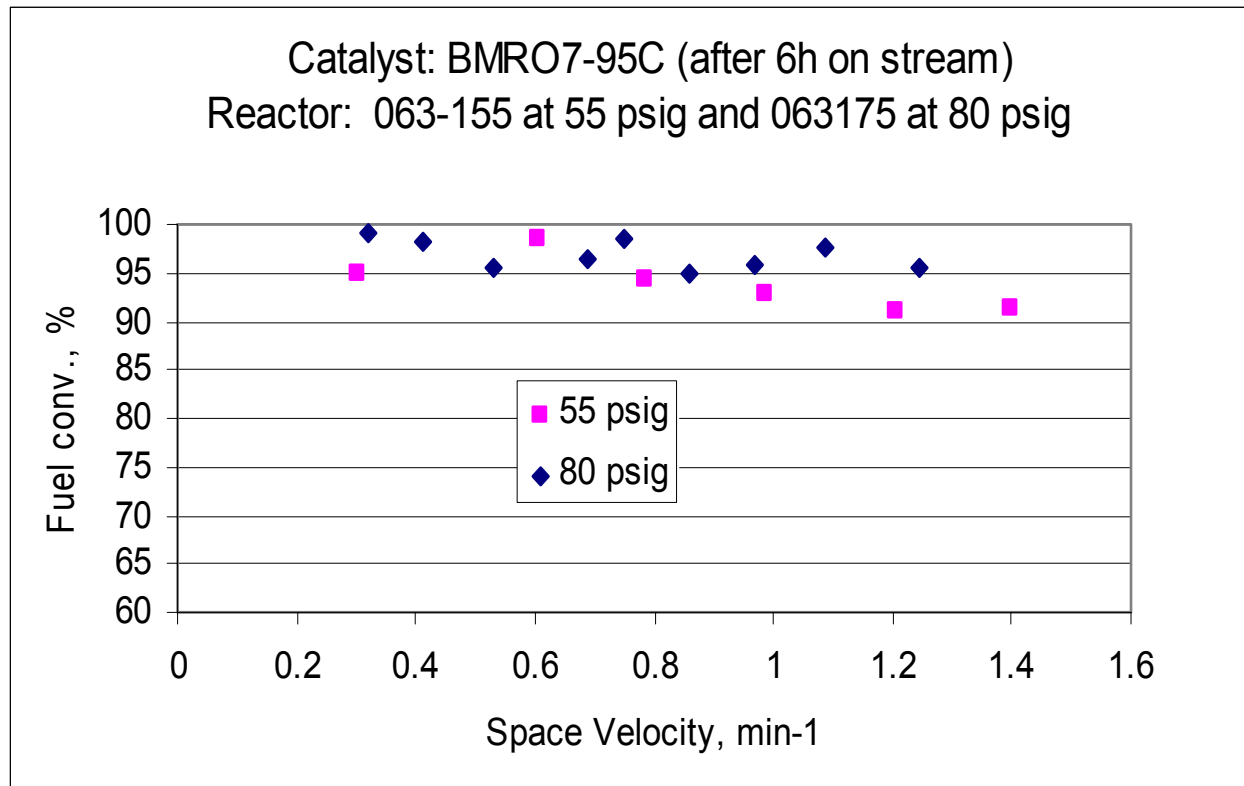
NaBH₄ Conversion as a Function of Space Velocity



- Increase in fuel space velocity reduces NaBH₄ conversion
- Space velocity also affects reactor temperature

Comparison to Experimental Data

Experimental data confirms that high reactor pressure will allow more rapid processing of fuel



Main Observations

1. **Modeling Method** has been validated as a tool to simulate and predict the experimental results.
2. **Reaction Kinetics** is critically important to establishing the validity of the model.
3. **Validation:** Steady state profiles of temperature, NaBH_4 concentration, pressure drop, and H_2 flow rate correspond to experimental data.
4. **Simulation:** Effects of fuel flow rate, fuel concentration, and system pressure were determined.
5. **Design Optimization:** reactor geometry, catalyst porosity, active control of pressure and temperature will have strong influence on the simulation results.
6. **Benefits:** Initial simulation results already generated additional insights to be used to optimize system design and operation.

Future Work

FY06

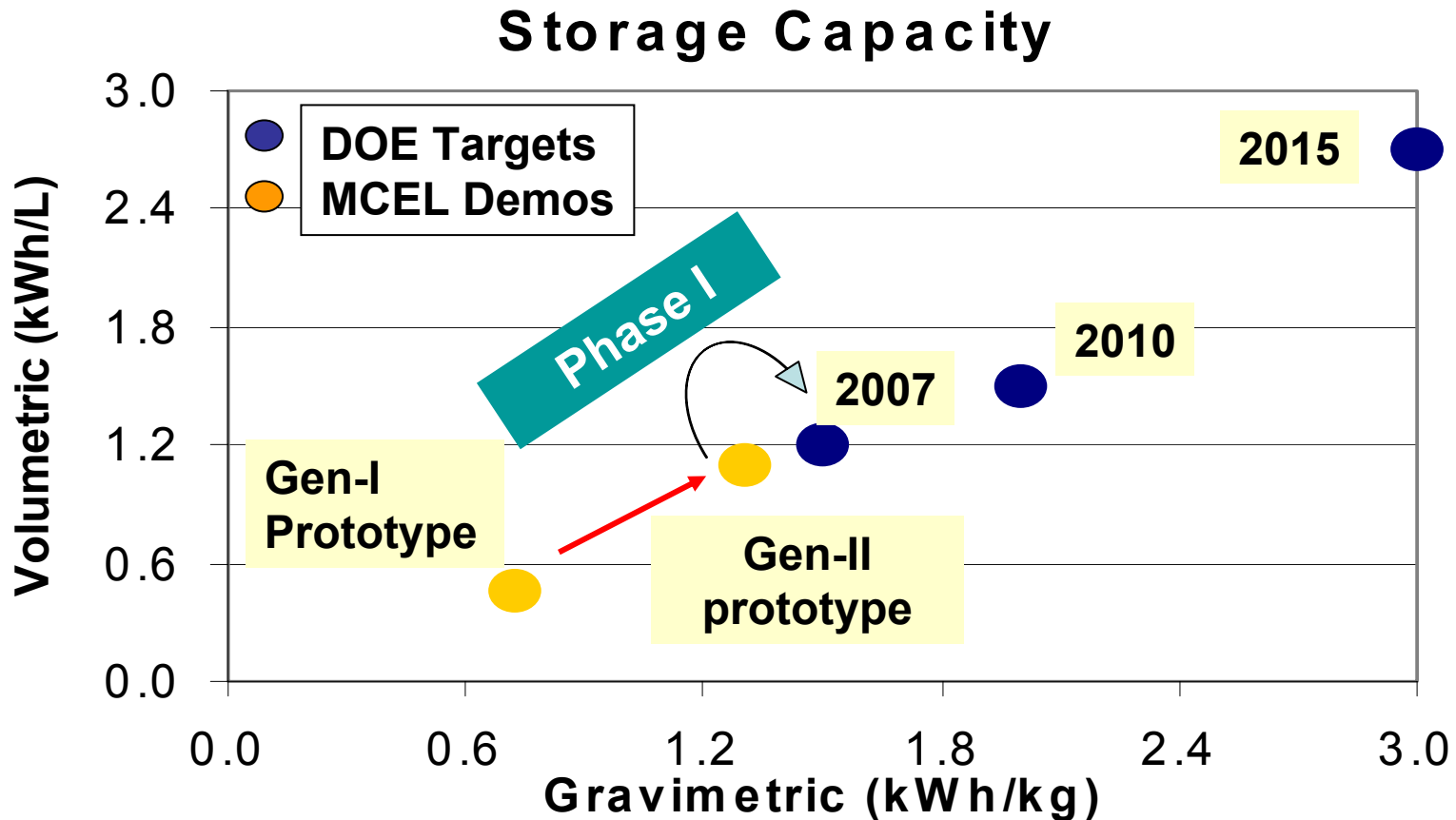
- **Complete reactor simulations**
 - Improve accuracy of reaction rate equation
 - Use Star-CD program to improve visualization of simulation results
 - Optimize operational parameters
- **Initiate reactor design**

FY07

- **Complete reactor design**
 - Optimize performance and parameters
- **Develop other sub-modules in BOP of system**
 - Use optimization results to guide H₂ generation system development
 - Evaluate possible system performance against FY07 DOE targets
- **Safety evaluation**
 - Individual sub-module components
 - Overall System

Storage Capacity Progress

Towards DOE Targets



Summary

Center Collaboration:

- Collaboration with PNNL has been very productive
- Insightful information has been generated from the modeling activities in a short period of time
- Microscopic and Macroscopic level modeling tools being developed for use with additional chemical hydrogen storage systems

System Development:

- Developed accurate tool/method that will be utilized to generate an optimized and improved on-board hydrogen generator
- Heat and water management can be accomplished by better understanding of operating conditions
- Borate precipitation can be managed by balancing fuel concentration and reactor pressure and temperature

Acknowledgements

- Center of Excellence for Chemical Hydrogen Storage
- Project Collaborators:
 - PNNL: modeling activities
 - Dave Rector, Scot Rassat
 - ROH, PSU, LANL, PNNL : SBH regeneration
- DOE program managers:
 - Grace Ordaz, Jim Alkire, Sunita Satyapal
- Center Coordinators
 - Chris Aardahl, Bill Tumas

Response to Previous Year Reviewers' Comments

- Comments received mostly pertain to Center as a whole, very few directly for this project.
 - MCEL's role:
 - develop modeling and engineering for on-board system;
 - Improve system level storage density
- Check the system gravimetric and volumetric capacity data from the previous DCX system demo (Natrium) and compare values by DCX and Millennium Cell.
 - Available information only limited to publicly disclosed data. DCX proprietary information not available.
- DOE request that the PI coordinate more closely on the overall efficiency analyses with TIAX and ANL.
 - Provided feedback to Argonne's paper on WTT calculations; learned the Excel tool for calculation WTT efficiency.
 - Became familiar with the H2A model for cost and efficiency.
- Communicate with Hydrogen Delivery Team, delivery has a capacity target of 13.2 wt% (though less stringent volumetric target of 27 g/l)
 - Presented to the Delivery Tech Team in October 2005 conference call.

Publications & Presentations



“Reactor Development for Hydrogen Generation from Sodium Borohydride”
Presentation by Ying Wu, MRS Spring Meeting, San Francisco, CA, April 18, 2006

Critical Assumptions & Issues

Accuracy of reaction kinetics

- Affects fluid dynamics and operational parameters
- Inaccuracy in kinetic expressions will alter design parameters of other system sub-modules

Application to other Chemical Hydride systems

- Adaptability to other chemical hydride (e.g. NH_3BH_3)
- Liquid vs. solid fuel

System design of a Chemical Hydride Prototype

- Detailed system design will occur after go/no-go evaluation
- Optimizing overall unit
- Assuring complete safety