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DTE Energy



DTE Energy Hydrogen Technology Park 2006 DOE Program Review

**Rob Bacyinski
Bruce Whitney
May 18, 2006**



(I believe)

(I believe)

This presentation does not contain any
proprietary or confidential information

Project ID: TV 1



Overview

Timeline:

Start Date: Oct 2002
 Orig End Date: Oct 2005
 New End Date: Oct 2009
 % complete: ~75%

Budget:

Total (revised): \$4 M
 – DOE share: \$2 M
 – Cost share: \$2 M
 FY05 funding: \$0.6M
 FY06 funding: \$0.4M

Barriers:

C. Hydrogen Refueling Infrastructure
 E. Codes and Standards
 H. Hydrogen from Renewable Resources
 I. Hydrogen and Electricity Co-production

Partners/Collaborators:

- DaimlerChrysler
- BP
- Lawrence Technological University (LTU)
- Sandia National Laboratories
- The University of Michigan





Objectives

Project Objectives

Develop and test a hydrogen co-production facility having stationary fuel cell power and vehicle fueling capability that uses renewable & non-renewable resources (FY04)

Employ representative commercial units under real-world operating conditions (FY04)

Based on performance data, project experience, and market assessments evaluate the technical and economic viability of the power park system (FY05)



DOE Objectives

By 2008, validate an electrolyzer (powered by a wind turbine) with capital cost of \$600/kWe and efficiency of 68% (incl. compression to 5,000 psi)*

By 2008, develop a dist gen PEM fuel cell system that achieves 32% electrical efficiency and 20,000 hours durability at \$1500/kW

*when built in quantities of 1,000



Objectives

Project Objectives

Contribute to development of relevant safety standards & codes required for commercialization of hydrogen-based energy systems (FY04)

Identify system optimization and cost reduction opportunities including design footprint, co-production, and peak-shaving applications (FY05)

Increase public awareness and acceptance of hydrogen-based energy systems (FY04-F09)

DOE Objectives

Determine the relevant codes, safety standards, and engineering data required for Power Parks

Obtain real-world operating data to better understand performance, maintenance, operation, and economic viability of Power Parks





Approach: Project Overview

Design, install, and operate an integrated hydrogen co-production facility utilizing:

- Electrolytic hydrogen production (2.7 kg/hr, 43 kg/day)
- 50kW (DC) stationary fuel cell power (320 kWh/day)
- 5000 psig vehicle dispensing (15 kg/day)
- Renewable on-site solar energy (27 kW)
- Grid-connected biomass energy

Collect, analyze, and report system performance data & lessons learned for an integrated co-production facility operating under real-world conditions

Evaluate commercialization opportunities for an advanced Power Park facility



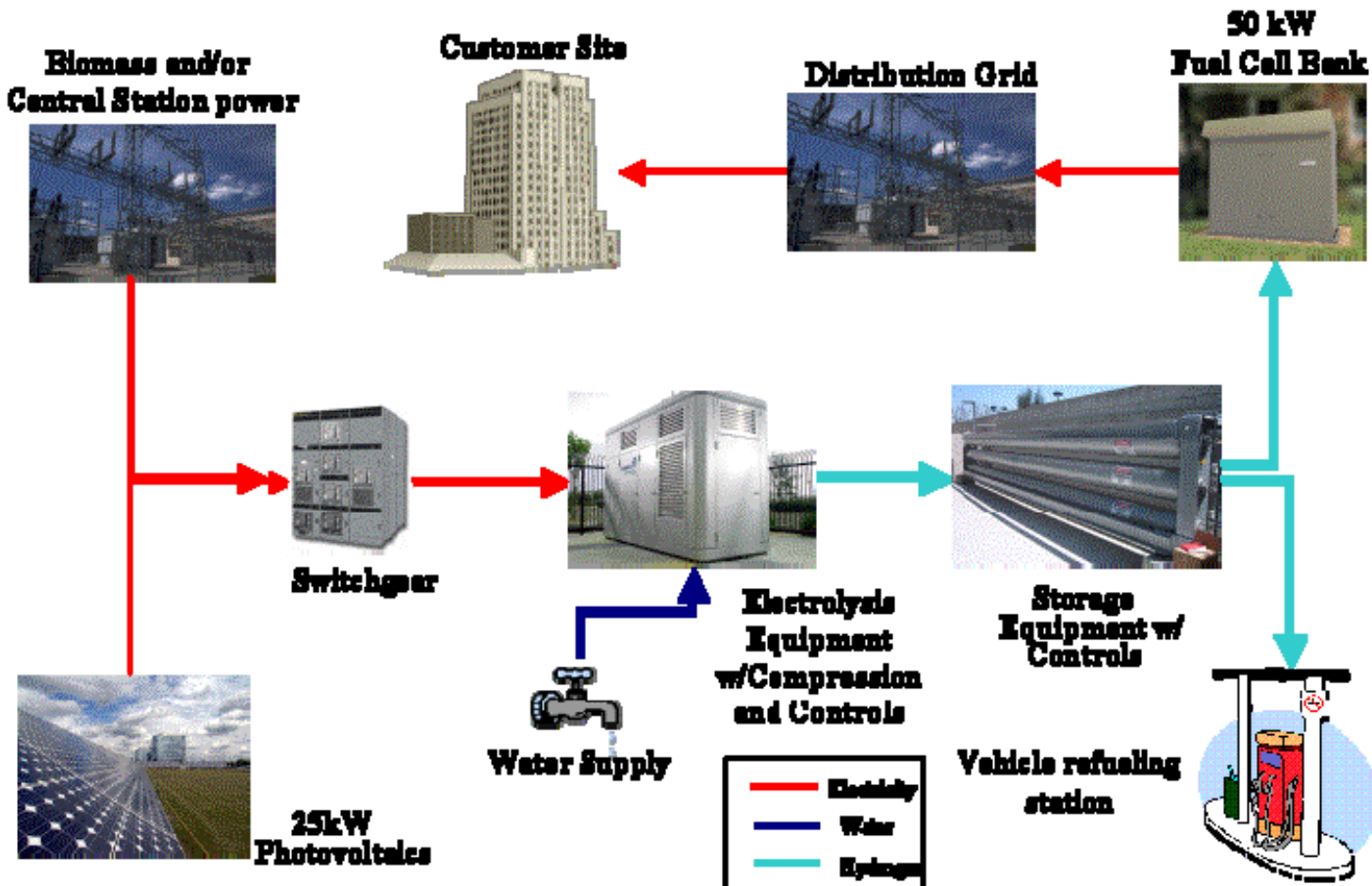


Approach: Process Flow Diagram

System Operations Center
(not shown):

- Provides remote monitoring & control, all data acquisition and web access

All AC systems connected to common 480 V Bus



Accomplishments:

Validated electrolyzer with capital cost of \$1500/kWe and efficiency of 59%



DTE HTP Demonstration Project Electrolyzer

- **Measured running efficiency* 59% (DOE 2008 goal 68%)**
- **\$1500/kWe (DOE 2008 goal \$600/kWe)**
- **Off Peak operation (16 hrs/day) - 43 kg/day production**
- **2.7 kg/hr production rate**

Projected System Performance (manufacturer quote, 2006 prices)

- **Manufacturer rated efficiency 62.25%**
- **\$700/kWe (DOE 2008 goal \$600/kWe)**
- **Off Peak operation (16 hrs/day) - 1440 kg/day production**
- **90 kg/hr production rate**

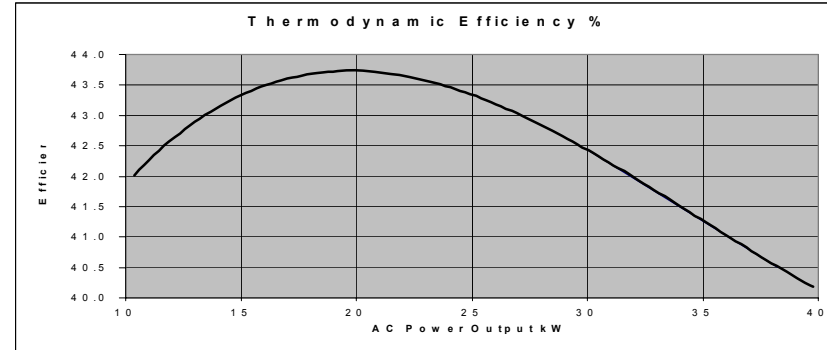
*SNL data analysis for steady operation



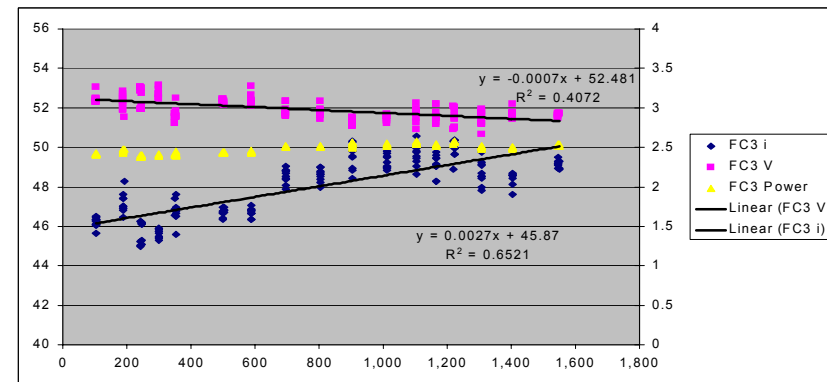


Accomplishments: Validated 40kW 'peak shaving' PEM fuel cell system

- Achieved 44% peak fuel cell efficiency
- Generated 41,034 kWh from installed bank
- Demonstrated 1500 Hour (6,000 kWh) stack durability at capital cost of \$3,000/kW (DC)
- Determined stack V-I Curves, transient response, and service performance for future improvement



Running efficiency (AC) measured @ 44%



Stack performance, 1500 hr design life

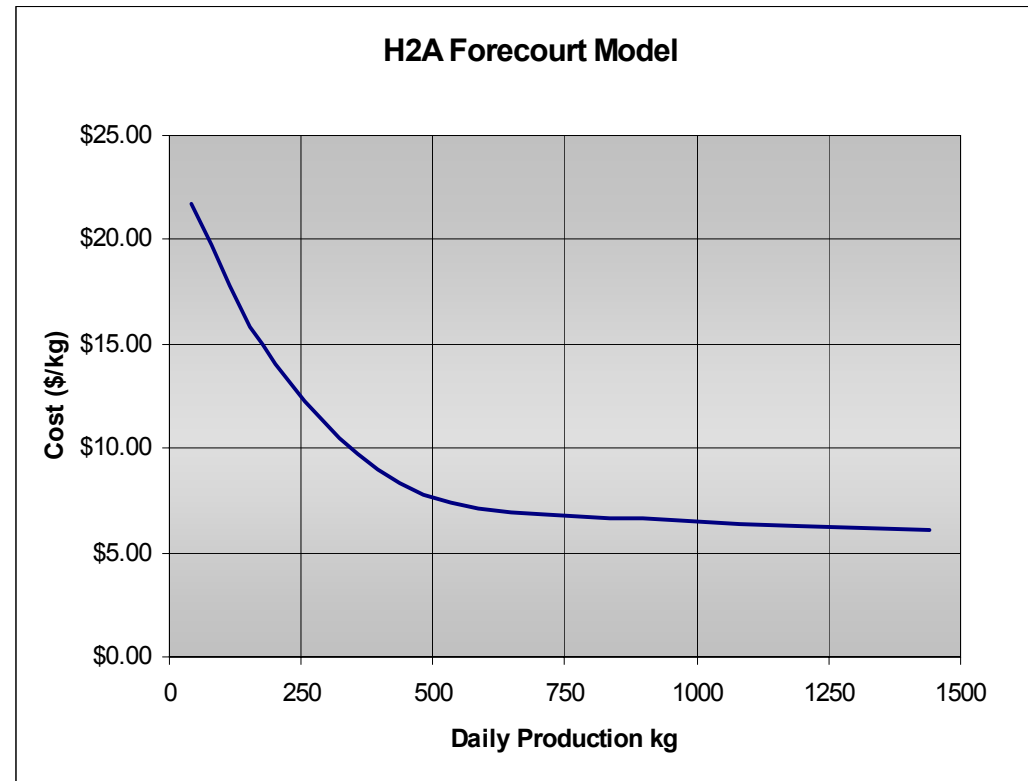




Accomplishments:

Obtained real-world data to better understand economic viability of Power Parks

- Calculated project and high volume hydrogen cost using H2A Forecourt model, 2006 prices and scaled BOP (shown at right)
- Determined 2005 DOE goal of \$4.75 /kg may be attainable
- Determined hydrogen production cost using DTE financials of IRR & Capital
- Verified UofM financial model with H2A (for matched costs and financial assumptions)





Accomplishments:

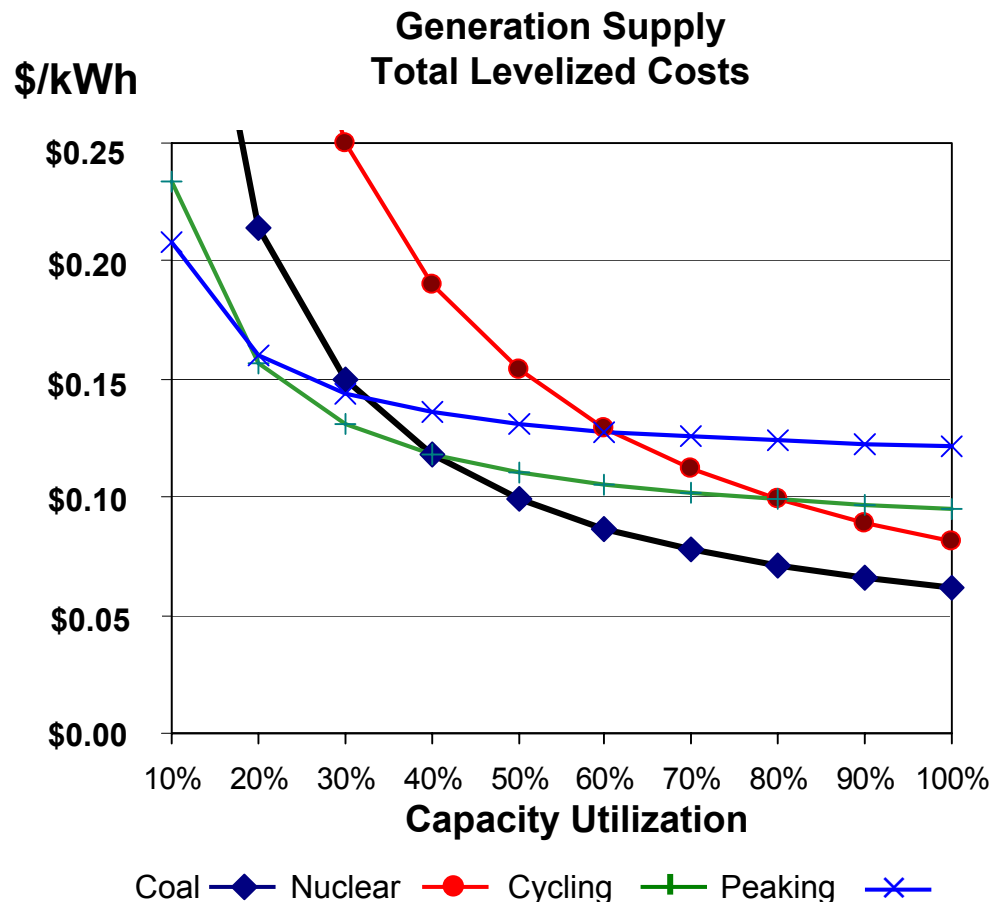
Obtained real-world data to better understand economic viability of Power Parks

D.G Units:

| | <u>Cap/kW</u> | <u>Fuel</u> | <u>Total</u> |
|---------|---------------|-------------|--------------|
| Nat Gas | \$870 | \$0.068 | \$0.199 |
| Diesel | \$600 | \$0.110 | \$0.200 |

Fuel Cells:

| | <u>Cap/kW</u> | <u>Fuel</u> | <u>Total</u> |
|-----------|---------------|-------------|--------------|
| FC HTP | \$5,000 | \$0.325 | \$1.075 |
| FC Future | \$893 | \$0.286 | \$0.420 |

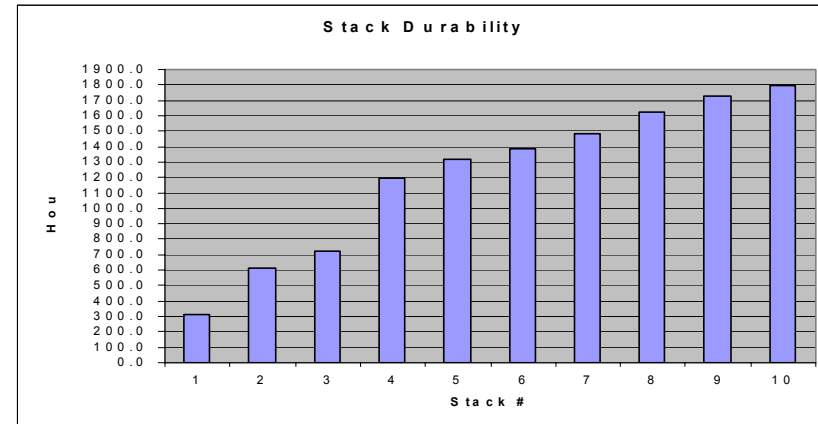


Accomplishments:

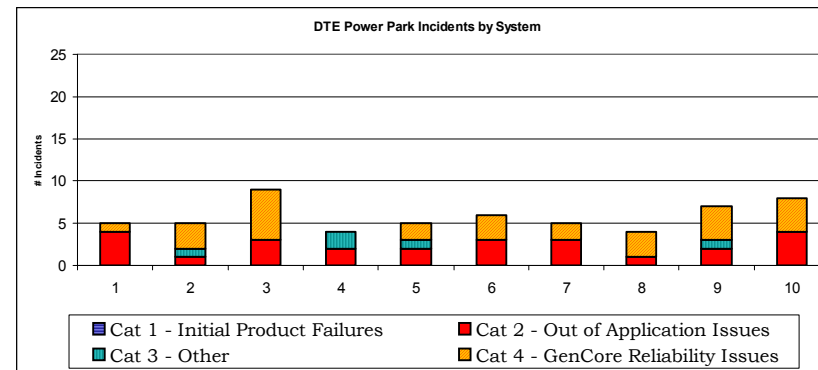
Obtained real-world data to better understand performance & maintenance of Power Parks



- Overcame design & operational issues with fuel cells for cold weather climate
- Addressed stack life issues:
 - Demonstrated 1500 hours (6,000 kWh) durability on recent stacks
- Resolved key maintenance issues:
 - Infant mortality/start up failures
 - Part defects
 - Service incidents/unit/month: down to 0.9 incidents/unit/month



Stack durability



Service incidents



Accomplishments:

Identified system optimization and cost reduction opportunities



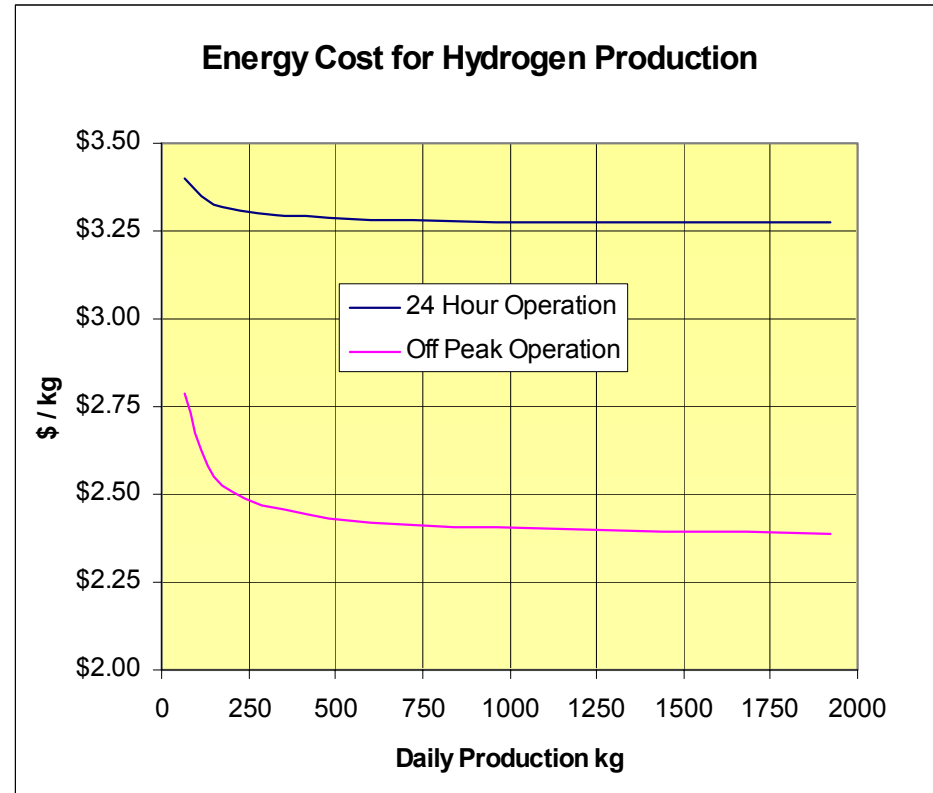
Off-Peak vs. 24 Hour Operation of Electrolyzer:

Based on actual electrical rate structure (D6) and production volumes, demonstrated benefit of Off-Peak operation

Graph: Energy cost/kg for same daily hydrogen production (same daily energy consumption)

Off-Peak and 24 hour operation shown

On-Peak 11AM-7PM, M-F



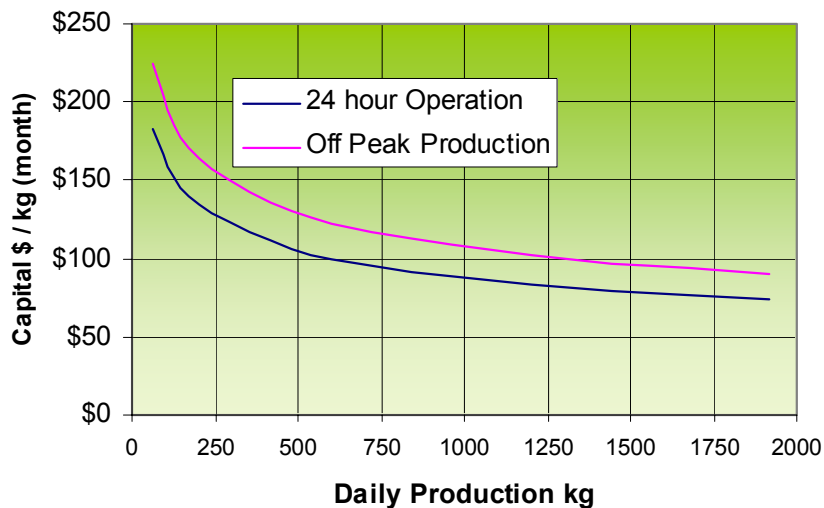
Off Peak vs. 24 Hour Operation





Accomplishments: Identified system optimization and cost reduction opportunities

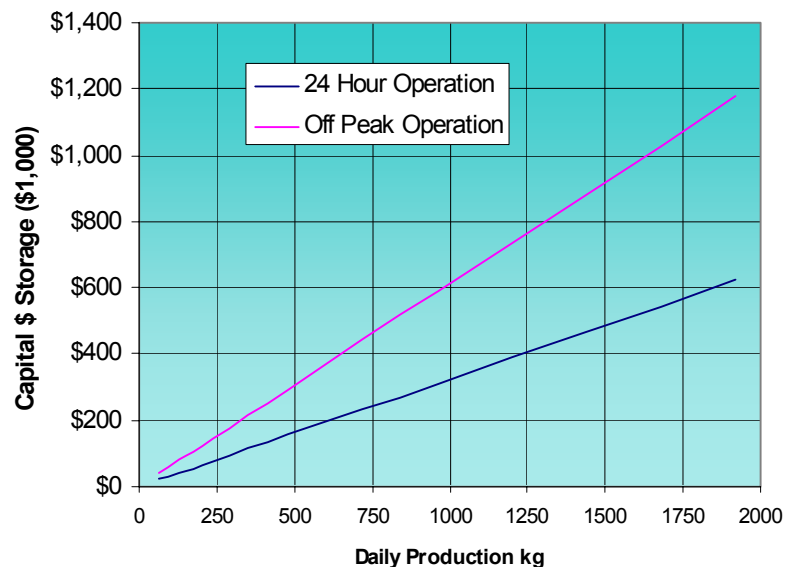
Capital Cost for Electrolyzer



Impact of daily operating plan on electrolyzer cost

Impact of daily operating plan on storage cost

Capital Cost of Storage



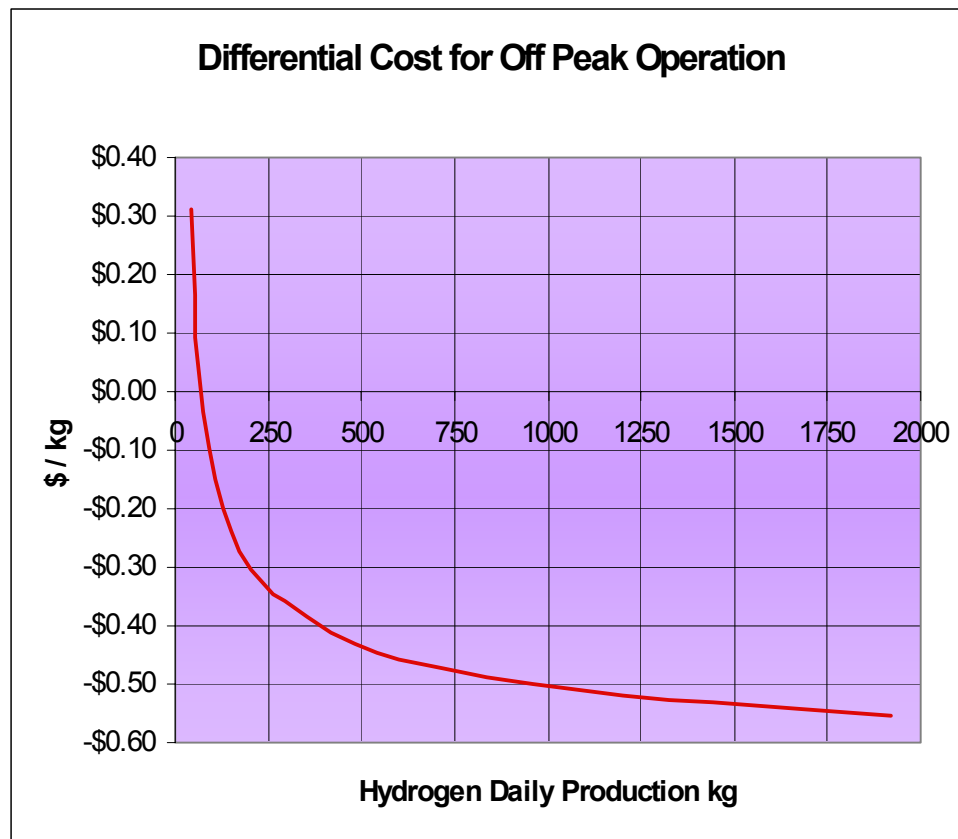


Accomplishments:

Identified system optimization and cost reduction opportunities

Operation plan and system design optimized for minimum production cost based on electric rate and dependent variables of electrolyzer and storage cost

'Off peak' design also offers increased surge capacity and maintenance advantages









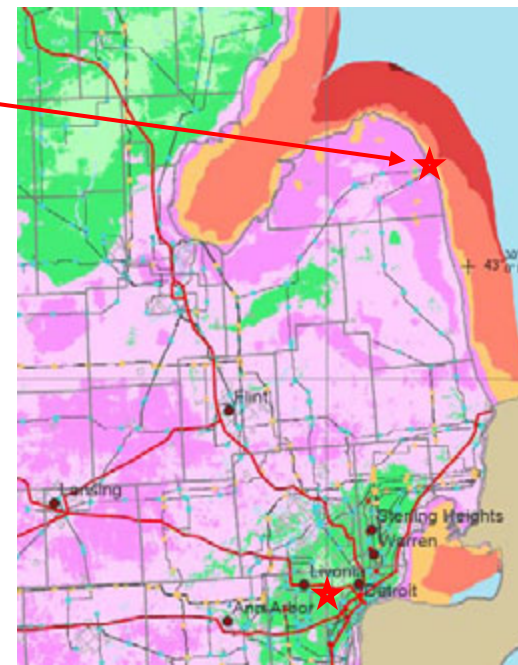


Accomplishments: Examined best case wind resource*

Harbor Beach Power Plant Site Best Wind Resource* Available

- 30% Annual Capacity Factor
- \$1,000/kW installed (assumed)
- \$0.06/kWh Energy Cost

| | mph | m/s |
|--|-------------|-----------|
|  | < 12.3 | < 5.5 |
|  | 12.3 - 13.4 | 5.5 - 6.0 |
|  | 13.4 - 14.5 | 6.0 - 6.5 |
|  | 14.5 - 15.7 | 6.5 - 7.0 |
|  | 15.7 - 16.8 | 7.0 - 7.5 |
|  | 16.8 - 17.9 | 7.5 - 8.0 |
|  | 17.9 - 19.0 | 8.0 - 8.5 |
|  | 19.0 - 20.1 | 8.5 - 9.0 |
|  | 20.1 - 21.3 | 9.0 - 9.5 |
|  | > 21.3 | > 9.5 |

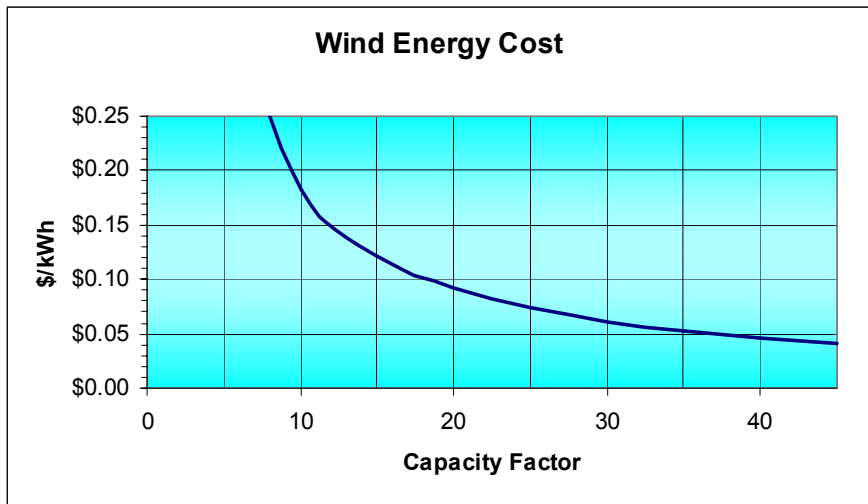


@ 100 Meters

Investigated 10/14/05 (LTU)

Using Weibll – NREL ArcGis

* in DTE Energy service territory





Accomplishments:

Calculated hydrogen production cost from renewables

Hydrogen Production Costs (calculation assumptions)

Harbor Beach Wind Turbine

30% CF, \$1000/kW

(11% CF in August)

Sized for daily production

H2A model assumptions

No storage cost penalty

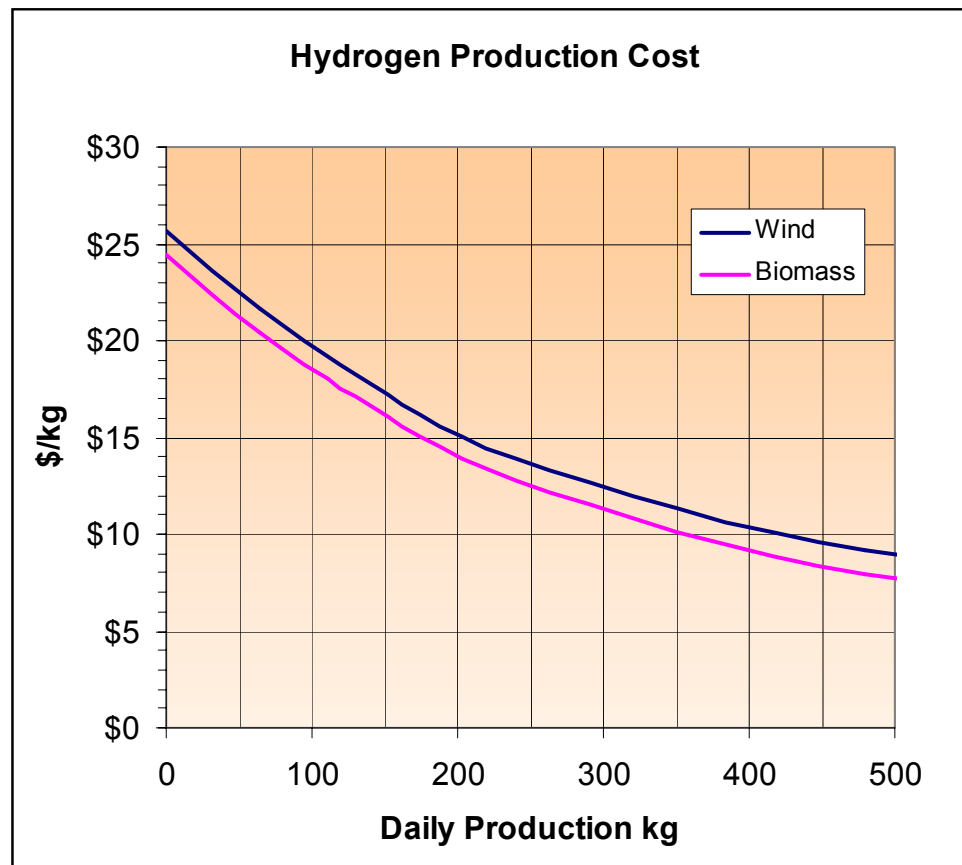
(Grid back-up)

Electrolyzer on site

Biomass at \$0.04/kWh

24/7 availability

Electrolyzer on site



Accomplishments:

Validated renewable (PV) generation to common bus for hydrogen production and 'parasitic' loads



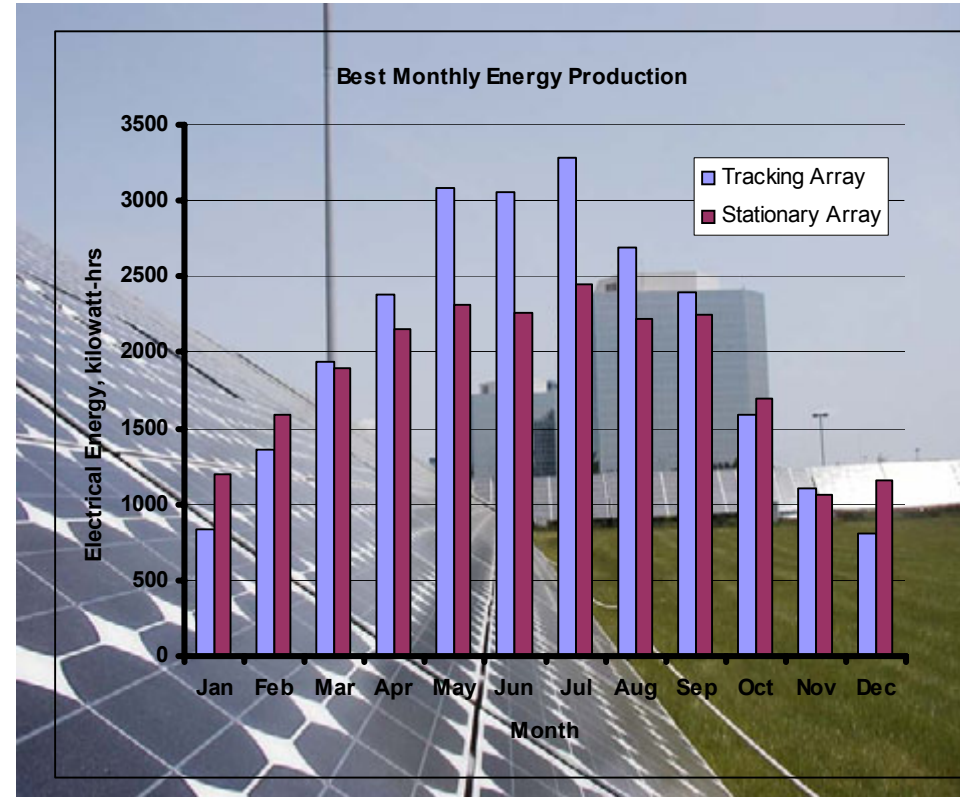
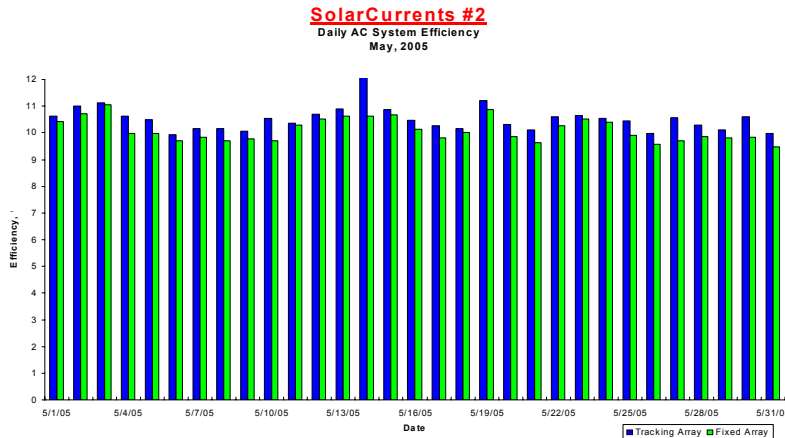
46,201 kWh of PV generation at 9-12% efficiency

Hydrogen Production:

22,176 kWh Off-Peak Energy producing 394 kg Hydrogen

Energy for Parasitic Loads:

24,025 kWh On-Peak



27 kW Solar Panels

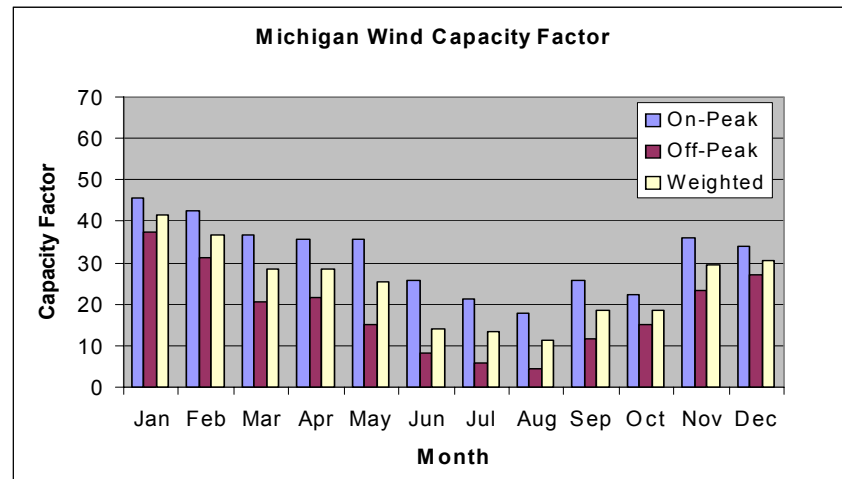
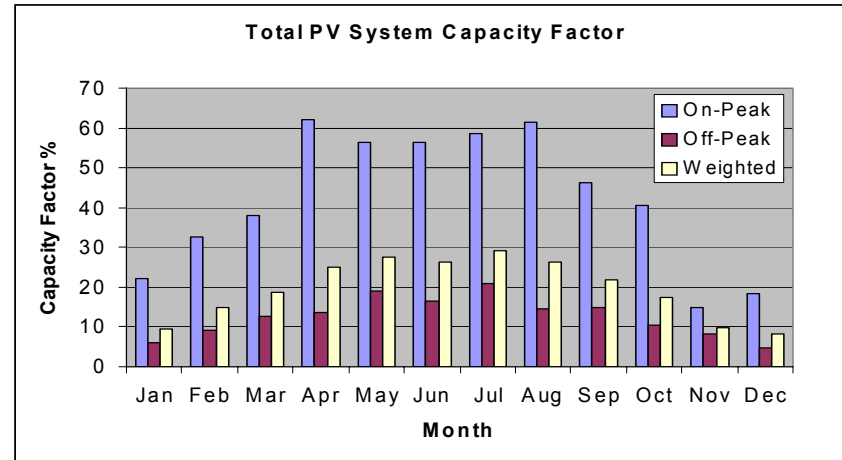
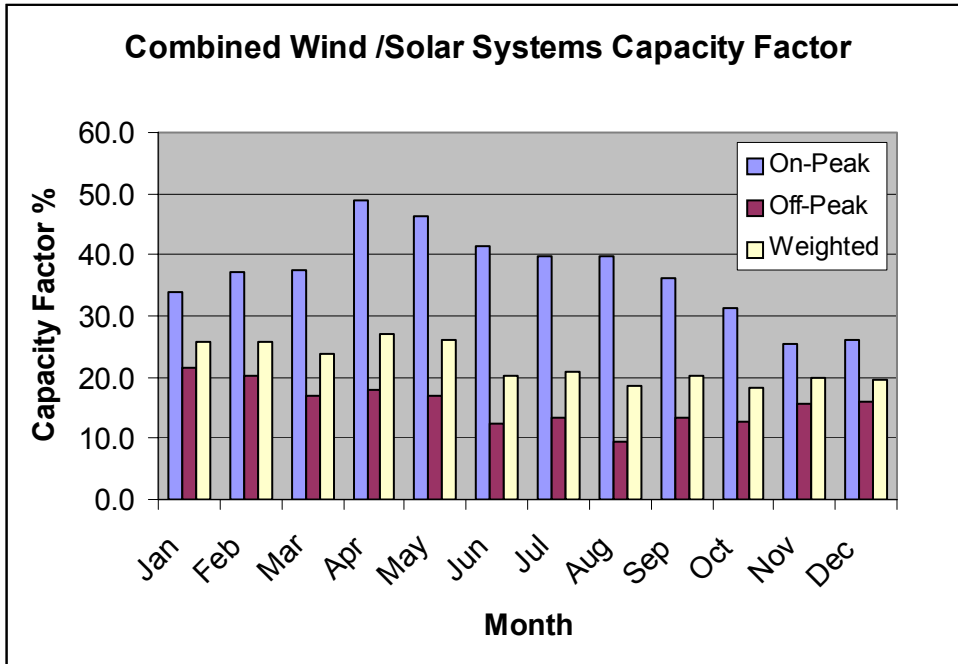


Accomplishments:

Investigated renewable PV and wind generation for complimentary capacity factor



Identified combined wind/solar systems for future technical and economic analysis



Accomplishments:

Closely coordinated work with partners / collaborators



Lawrence Technological University

Dr. Rob Fletcher, Department of Mechanical Engineering

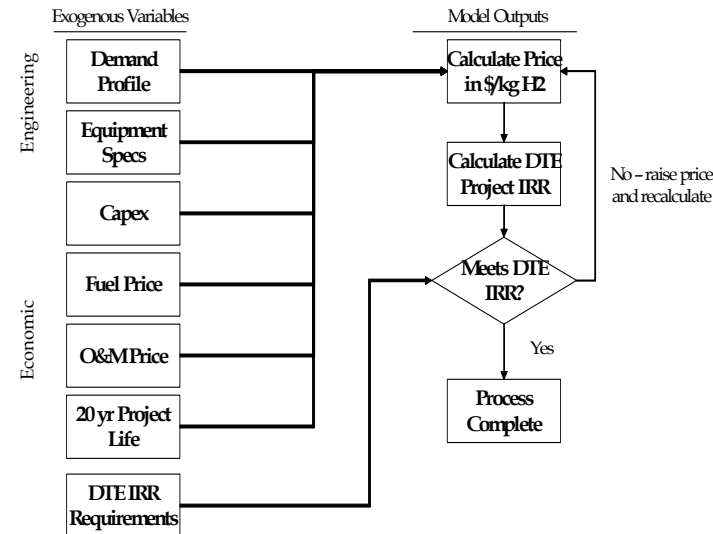
- Analyzed and recommended course of action for improving PEM fuel cell stack durability
- Developed wind resource site study
- Provided quarterly data collection, analysis, and reporting to DOE Hydrogen Fleet Demo project
- Performed student internship at Sandia National Labs to develop DTE Hydrogen Park model



University of Michigan

Student masters degree team project at School of Business and Natural Resources

- Title: DTE Hydrogen Park Economic Model and Market Assessment
- Economic viability assessment based on DTE Energy business requirements
- Project results validated by comparison to DOE H2A model



Accomplishments: Closely coordinated work with partners / collaborators



Daimler Chrysler and BP

Klaus Bonhoff, Giorgio Zoia

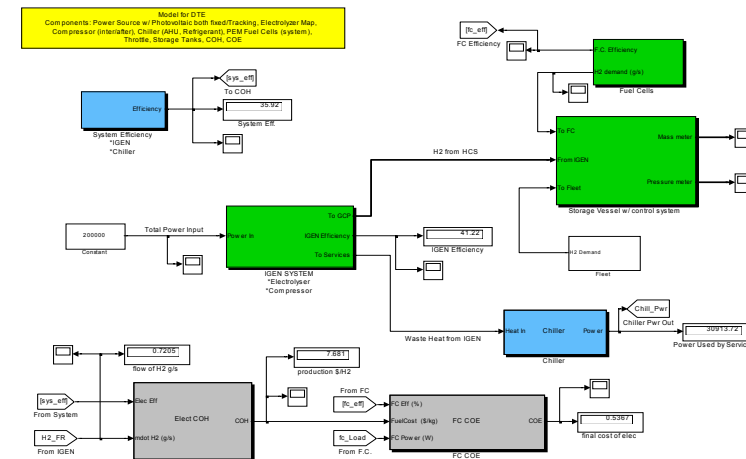
- Co-sponsored First Responder, hydrogen training event – first in State of Michigan
- Conducted hydrogen dispenser vehicle interface analysis FMEA



Sandia National Labs

Andy Lutz

- Developed component/system thermodynamic and economic models for DTE Hydrogen Park
- Sponsored student internship from LTU





Accomplishments:

Increased public awareness and acceptance of hydrogen-based energy systems

Conducted numerous public and media tours (>40 groups & >300 individuals)

- Educational institutions (LTU, Wayne State)
- Industry, Community & Government Groups
- State Fire Marshals
- Local and regional media, print and TV (4 interviews)

Sponsored open house event – over 350 from general public in attendance:



DAIMLERCHRYSLER





Accomplishments:

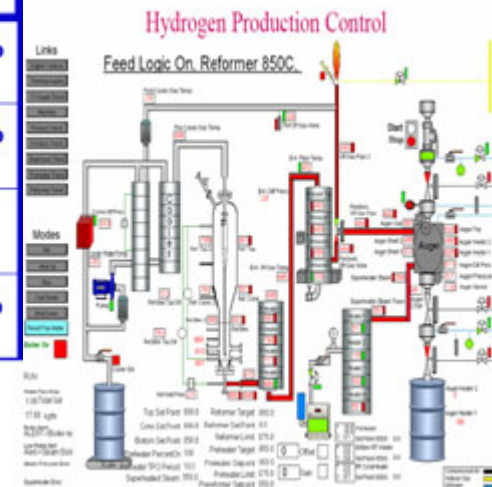
Conducted tour and initial assessment of pyrolysis demonstration project

- Toured EPRIDA peanut shell pyrolysis project (Athens, Georgia)
- Obtained preliminary syn gas composition data
- Determined analyses required to assess suitability of syn gas as a hydrogen source for use in a Power Park



| Pyrolyzer (Yields) | |
|--------------------|-----|
| Char | 32% |
| Water | 32% |
| Bio-Oils | 31% |
| Gases | 5% |

| Reformer (Gas product composition, on dry N ₂ -free basis) | |
|---|-----|
| Hydrogen | 49% |
| Carbon Dioxide | 36% |
| Carbon Monoxide | 9% |
| Methane | 8% |





Other Accomplishments

Participant in Michigan Department of Environmental Quality (MDEQ) Hydrogen Ad Hoc Storage Rules Committee

Participant in NextEnergy Hydrogen Infrastructure Working Group

Co-developed rapid mass loss detection system with vendor

Evaluated dispenser pad grounding issues re: SAE J2578 and SAEJ1645 and DIN EN 1081, plans made to resurface filling area

Participant in other projects: Advanced Communication and Control of Distributed Energy Resources at Detroit Edison: DE-FC02-04CH11234 and Development and Demonstration of Advanced Distribution Operations With Distributed Energy Resource Integration: DE-FC02-06CH11347





FY05 Comments & Responses

Major Questions / Comments from FY05

1. Solar power system appears to add little value to the project.
2. Geographic location not ideal for renewable resources.
3. Needs more emphasis on data sharing.
4. Include hydrogen and electricity production cost estimation.

Response

1. PV panels are a significant contributor to the project both in energy and for analysis of On/Off peak capacity factor and coordination with potential wind resources.
2. Site chosen for availability of scaling up grid source (at electrical substation), proximity to PV (at site), local customer hydrogen demand, public outreach (central to population center.)
3. Data sharing with all partners/collaborators, NREL Hydrogen Fleet Demonstration Project, and three university programs.
4. Complete reporting of cost calculations in this presentation.





Future Work (FY06-07)

- Integrate and install new electrolyzer (October 06)
- Resurface fueling area by hydrogen dispenser
- Analyze combined wind/solar resources
- Determine cost of 'cleaning' syn-gas product to 99.995% purity
- Determine market value of carbon product from pyrolysis as soil supplement
- Determine economics and practicality of pyrolysis based hydrogen
- Continue safe operation of site (FY06-FY09)
- Continue participation with project partners DCX and BP in DOE Hydrogen Fleet Demonstration Project
- Continue data collection, analysis and periodic reporting to DOE
- Continue education & outreach activities
- Publish final project reports (including recommendations)





DTE Energy Hydrogen Technology Park





Supplemental Slide

D6 Rate Parameters

- **Peak Hours: 11AM-7PM weekdays (no holidays)**
- **On-Peak demand: \$10.93/kW**
- **On-Peak energy: \$0.02364/kWh**
- **Off-Peak energy: \$0.02064/kWh**
- **Delivery charge: \$0.00703/kWh (all)**
- **Max demand: \$4.55/kW**
 - » (30 minute max demand or minimum of 50kW and not less than 65% of On Peak demand June-October)
- **Service Charge: \$275.00 / month**





Supplemental Slide

Fully Integrated Hydrogen Park into Fleet Demo Program

- Conducted 119 fueling activities
- Dispensed 134 kg hydrogen
- Provided infrastructure data to NREL through March '06 – (Holly Thomas - fuel purity)
- DCX customers: Inergy, City of Farmington Hills, Wayne State University
- Ford Vehicle (ICE) Fueling as requested

| Report Date | | 3/31/2006 | | | |
|---------------------------|----------------------------------|-------------------------------------|------------------|------------------------|---------------------|
| Energy Provider | | DTE Energy Hydrogen Technology Park | | | |
| Unique Station Identifier | | 25613 | | | Date ⁽³⁾ |
| | Constituent | Chemical Formula | Detection Limits | Analytical Method | 9/20/04 |
| 1 | Hydrogen Purity ⁽²⁾ | ----- | %, dry | ----- | 99.9952 |
| 2 | Ammonia ⁽¹⁾ | NH ₃ | < 6 ppm | SOP-112 | ----- |
| 3 | Carbon Dioxide ⁽¹⁾ | CO ₂ | < 1 ppm | SOP-103 | < 1.0 |
| 4 | Carbon Monoxide ⁽¹⁾ | CO | < 1 ppm | SOP-103 | < 1.0 |
| 5 | Total Sulfur | ----- | < 0.01 ppm | SOP-1100 / ASTM D-5504 | < 1.0 |
| 6 | Carbonyl Sulfide | COS | < 0.01 ppm | SOP-1100 / ASTM D-5504 | ----- |
| 7 | Hydrogen Sulfide ⁽¹⁾ | H ₂ S ⁽¹⁾ | < 0.01 ppm | SOP-1100 / ASTM D-5504 | < 1.0 |
| 8 | Carbon Disulfide | CS ₂ | < 0.01 ppm | SOP-1100 / ASTM D-5505 | ----- |
| 9 | Methyl Mercaptan | CH ₃ SH | < 0.01 ppm | SOP-1100 / ASTM D-5506 | ----- |
| 10 | Sulfur Dioxide ⁽¹⁾ | SO ₂ ⁽¹⁾ | < 0.01 ppm | SOP-1100 / ASTM D-5504 | ----- |
| 11 | Total Inert Gases ⁽¹⁾ | N ₂ + He + Ar | < 200 ppm | SOP-2000 / ASTM D-2650 | 5.0 |
| 12 | Nitrogen ⁽¹⁾ | N ₂ | < 200 ppm | SOP-2000 / ASTM D-2650 | 5.0 |
| 13 | Argon ⁽¹⁾ | Ar | < 200 ppm | SOP-2000 / ASTM D-2650 | ----- |
| 14 | Helium ⁽¹⁾ | He | < 200 ppm | SOP-2000 / ASTM D-2650 | < 6.0 |
| 15 | Oxygen ⁽¹⁾ | O ₂ ⁽¹⁾ | < 5 ppm | SOP-116 | 8.0 |
| 16 | Water ⁽¹⁾ | H ₂ O ⁽¹⁾ | < 5 ppm | SOP-109 / ASTM D-5454 | 33.0 |

