



# Cost-Effective Method for Producing Self-Supporting Pd Alloy Membrane for Use in the Efficient Production of Coal-derived Hydrogen

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# Overview



### Timeline

- Project start: Sep. 09, 2003
- Project end: Oct. 31, 2007
- Percent complete: ~95%

## Budget

- Total project funding (3 year)
  - DOE share: \$775,771
  - Contractor share: \$194,200
- Funding received in FY06
  - \$263,671
- Funding for FY07
  - \$0



### **Barriers**

- Barriers addressed
  - N. Defects (high yield, large area)
  - O. Selectivity (>99.9%)
  - Q. Flux (>100 scth/ft<sup>2</sup>)
  - S. Cost (<\$1500/ft<sup>2</sup>)

## Partners

- Colorado School of Mines (Way)
  - H<sub>2</sub> permeation measurements
  - Membrane characterization
- IdaTech (Pledger)
  - Large-scale testing
  - Module demonstration
  - Sealing

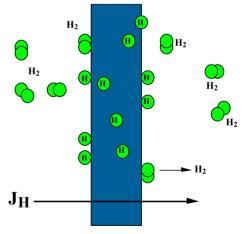




# Objectives



- Overall DOE Goal: Develop technologies that effectively and economically separate hydrogen from mixed gas streams that would be produced by coal gasification
- Develop a process methodology for the cost-effective manufacturing of thin, dense, self-supporting palladium (Pd) alloy membranes for hydrogen separation from the mixed gas streams of coal gasification processes,
- Reduce Pd membrane thickness by >50% over current stateof-art, and show potential to meet DOE 2010 technical targets.
- Demonstrate viability of using large-area vacuum processing to "engineer" a membrane microstructure that optimizes hydrogen permeability, separation efficiency, and lifetime,
- Demonstrate efficacy of large-batch and/or continuous roll-toroll manufacturing of membrane material with performance and yields within pre-defined tolerance limits
- Demonstrate separation efficiency of thin palladium membrane in commercial-type fuel processor using mixed gas streams.











# Approach



- Year 1 (Complete)
  - Task 1: Magnetron Sputter Deposition of Pd-Cu Alloys on Small Samples
  - Task 2: Development of Backing Removal Techniques
  - Task 3: Materials Characterization of Sputtered Pdalloy Membranes
  - Task 4: Pressure and Purification Testing
  - Task 5: Prototype Module Design
    - Year 3

- Year 2 (Complete)
  - Task 1: Fabrication of Larger Area Membranes
  - Task 2: Optimization of Membrane Composition/Microstructure
  - Task 3: Refinement and Downselection of Backing Removal Methods
  - Task 4: Production of Membranes at least 75 in<sup>2</sup> in Area
  - Task 5: Prototype Module Construction
- Task 1: Final Optimization/Selection of Membrane Alloy Composition (Complete)
- Task 2: Pressure and Purification Testing Pilot-Scale Membranes (Complete)
- Task 3: Prototype Module Final Assembly and Testing (75% Complete)
- Task 4: Develop Cost Estimates for Production of Pd Membranes (Complete)





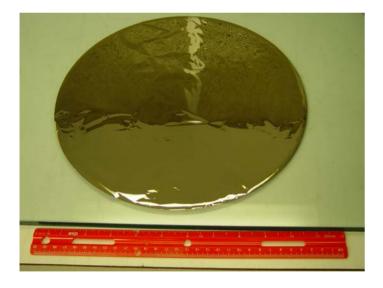


Deposition



	Plasma Clean	Compliant Layer	Deposition
Power (Watts)	18	500	500
Pressure (mTorr)	0.2	18.0	0.15
Deposition rate (A/s)	-	3.6	3.6
Duration (min)	15	2	245











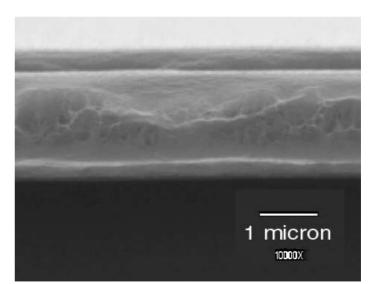


## Membranes



Sample Number	Date	Maker Pd %	EDAX Pd %	Max Flux @ 400C & 20psi [cm <sup>3</sup> /cm <sup>2.</sup> min]	CSM Thickness [microns]	Source	Maker Thickness	Permeance @ 400C [cm <sup>3</sup> (STP)/cm <sup>2</sup> s <sup>-</sup> cmHg <sup>0.5</sup> ]	Permeability @ 400C [cm <sup>3</sup> (STP) <sup>·</sup> cm/cm <sup>2</sup> ·s <sup>·</sup> cmHg <sup>0.5</sup> ]
051206#1	7/25/2002		57.00	17.9	8.80	SEM		5.98E-02	5.26E-05
051206#1	7/25/2002		57.00	30	8.80	SEM		1.00E-01	8.83E-05
072806#1	8/6/2002	62.00		N/A		SwRI	4.40	N/A	N/A
072806#1	8/27/2002	62.00		22.21	4.40	SwRI	4.40	5.14E-02	2.26E-05
073106#1	8/6/2002	62.00		N/A		SwRI	4.40	N/A	N/A
073106#1	8/7/2002	62.00		N/A		SwRI	4.40	N/A	N/A
073106#1	8/7/2002	62.00		N/A		SwRI	4.40	N/A	N/A
073106#1	9/10/2002	62.00		19.3	4.40	SwRI	4.40	6.46E-02	2.84E-05











# Measured H<sub>2</sub> Flux Has Surpassed Program Goals

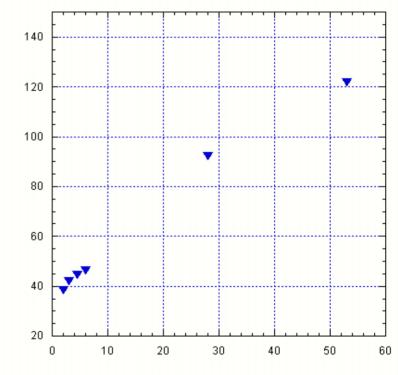
/olumetric Flux H<sub>2</sub> (cm<sup>3</sup> cm<sup>-2</sup> min<sup>-1</sup>)



- Best performance data @ 400 °C
  shown for a 2.5 µm Pd-Cu alloy foil,
  area = 2.6 cm2
  - Pure H2 permeability =

### 8 •10<sup>-5</sup> cm<sup>3</sup>•cm/cm<sup>2</sup>•s•cmHg<sup>0.5</sup>

- $H_2$  Flux = 124 cm<sup>3</sup>/cm<sup>2</sup>•min = 242 scfh/ft<sup>2</sup>
- Feed pressure = 20 psig
- Exceeds DOE Hydrogen Program and 2010 DOE Fossil Energy targets



#### Time (hours)

	SwRI	2007	2010	2015
	Membrane	Target	Target	Target
Flux scfh/ft <sup>2</sup> @ 100 psi DP H <sub>2</sub> partial pressure & 50 psid	564	100	200	300

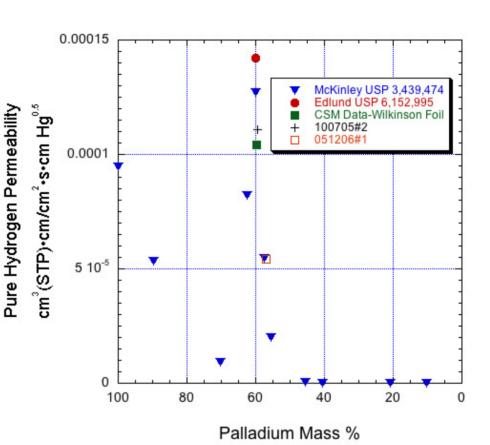






**Membrane Composition** 

- Permeability correlation
  with composition
  consistent with literature
- Wilkinson Foil as a standard
- Test Cycle
  - Forming gas, 8hrs 400°C
  - He, 24 hrs, 400°C (no flux)
  - H<sub>2</sub>, 250hrs, 400°C
  - Air Purge, 400°C
  - H<sub>2</sub>, 400°C





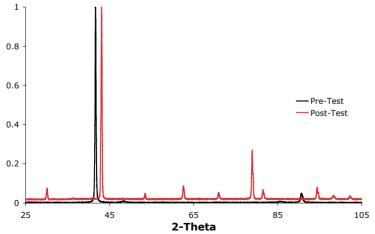




## Annealing

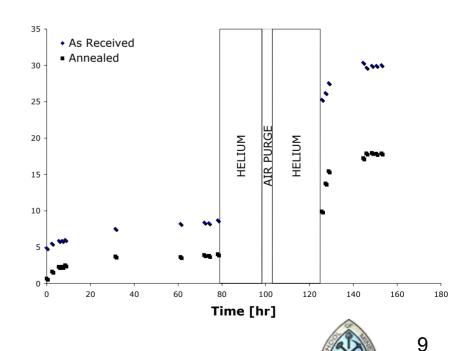






An IDACORP Company

- As prepared – 8.83x10<sup>-5</sup> cm<sup>3</sup>(STP)cm/cm<sup>2</sup>.s,cmHg<sup>0.5</sup>
- Annealed 450°C
  - $-5.26 \times 10^{-5} \text{ cm}^{3}(\text{STP})\text{cm/cm}^{2}.\text{s,cmHg}^{0.5}$
- Stress relieved following annealing
- Phase change from alpha to beta





# Module Development and **Testing at IdaTech**



- Measured  $H_2$  flux of 420 SCFH/ft<sup>2</sup> (400°C and 100 psig) on smaller samples provided by SwRI.
- Investigating gasketing arrangements to reliably seal thin membranes.
- Full-scale module test delayed
- More than a dozen full-size prototype membranes have been delivered to IdaTech







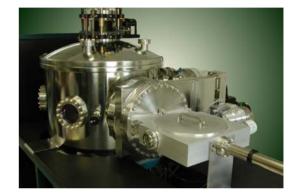


# **Cost Projections**

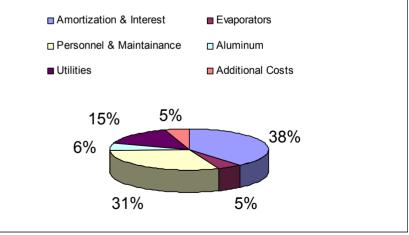


### Total Cost/ft<sup>2</sup> = (F + L + E) / (P\*S\*1.75 x10<sup>5</sup>) + R

- F is the equipment depreciation,
- L is the fully burdened labor costs
- E is the cost of utilities and maintenance,
- P is the throughput per minute,
- S is the # of 8 hour shifts per day
- R is the raw material cost



- \$35/ft<sup>2</sup> of Pd
  - Total final cost \$45.50/ft<sup>2</sup>









## **Future Work**



## High Permeability Ternary Palladium Alloy Membranes with improved Sulfur and Halide Tolerance - DE-PS26-06NT42800

**Objective:** To utilize a iterative modeling, rapid fabrication, and testing approach to develop and demonstrate an ultra-thin (<5 micron) durable ternary Pd-alloy membrane with excellent resistance to sulfur and halogen attack.

#### Scope of Work

- 1) Materials modelling and composition selection:
- 2) Fabrication of high-performance ternary alloy membranes:
- 3) Membrane testing and evaluation:

#### **Partners**

Colorado School of Mines (Way) TDA Research (Alptekin) Carnegie Mellon University (Sholl) IdaTech (Pledger)







# Future Work (Continued)



### Milestones

### Phase I (Year 1)

- Milestone 1.1: Use DFT methods to predict H2 flux through Pd96M4 for M = Ni, Rh, Pt, Nb, Ta, V, Mg and Y. Use same methods to predict H<sub>2</sub> flux Pd74Cu22M4 for at least 3 of the same M.
- *Milestone 1.2*: Screening of initial set ( $\leq 6$ ) of ternary alloys by pure gas (H<sub>2</sub> and N<sub>2</sub>) permeation experiments.

### Phase II (Year 2)

- *Milestone 2.1*: Fabricate a minimum of 20 membrane specimens with different copper concentrations based on CMU hydrogen transport predictions for the 2-3 most promising ternary element additions.
- *Milestone 2.6*: Complete 4-5 preliminary tests membrane samples at TDA and IdaTech with clean Syngas and single impurity additions of H<sub>2</sub>S and COS.

### Phase III (Year 3)

- *Milestone 3.1*: Produce a minimum of 5 sq. ft. of optimized membrane material for use at CSM and TDA and for independent third-party evaluation by IdaTech.
- *Milestone 3.2*: CSM will complete mixture permeation testing with H2/CO and  $H_2/H_2S$  binary mixtures with best three samples from the final optimization study.







# **Project Summary**



### Relevance

- Robust, high efficiency methods to extract pure hydrogen from coal gas and other sources is critical to the development of a hydrogen economy
- Approach
  - Use a novel, scalable vacuum deposition method to fabricate free standing Pd alloy hydrogen separation membranes and evaluate their performance

### Accomplishments

 Produced some of the thinnest (3 um), largest area (110 in2), highest performance separation membranes reported







# Summary (Cont'd)



	2005 DOE Target	2010 DOE Target	SwRI
Flux (scfh/ft²)	100	200	242
Cost (\$/ft²)	1500	1000	1500
Hydrogen Quality	99.9	99.95	99.95
DP Operating Capability	200	400	100

### Collaborations

 Commercial partner in IdaTech, long track record testing hydrogen membranes at CSM, new interactions with CMU

### Future R&D

 Test under more aggressive conditions, develop new ternary alloy formulations with increased durability, demonstrate low-cost pilot production



