

Fundamentals of a Solar-thermal Mn₂O₃/MnO Thermochemical Cycle to Split Water

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Overview

Timeline

- Start: 6-1-2005
- End: 5-31-2009
- 40% Complete

Budget

Total Project Funding

\$410,000 DOE (\$180,00 via UNLV)

\$102,500 Cost share

•Funds received in FY06

\$ 80,000

Barriers

- AU. High-Temperature
 Thermochemical Technology
- AV. High-Temperature Robust Materials
- AW. Concentrated Solar Energy Capital Cost
- AX. Coupling Concentrated Solar Energy and Thermochemical cycles

Partners

Swiss Federal Institute of Technology

University of Nevada – Las Vegas

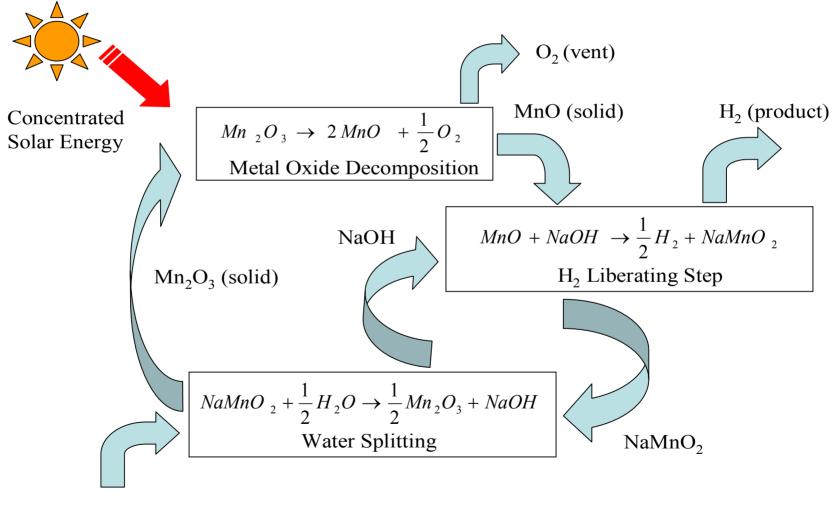




- Research and develop a cost effective Mn₂O₃/MnO solar-thermal thermochemical cycle through theoretical and experimental investigation
- Based on the above, develop a process flow diagram and carry out an economic analysis of the best process option



Literature Cycle



H₂O (vapor)



Approach

- Thermodynamic assessment of the cycle
- Experimental investigation
 - Investigate Mn_2O_3 dissociation and mechanism
 - Investigate H₂ generating step
 - Investigate ways in which to recover NaOH after H₂ generating step
 - Develop alternative methods in which to close the cycle
- Use H2A framework to economically evaluate the cycle

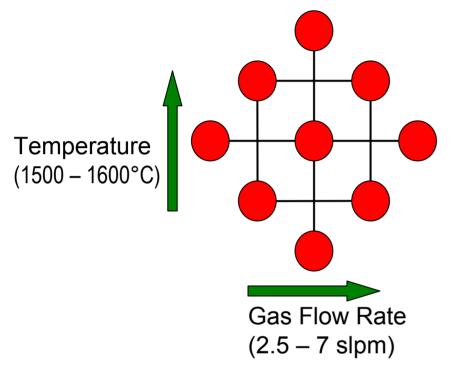


Technical Accomplishments / Progress / Results

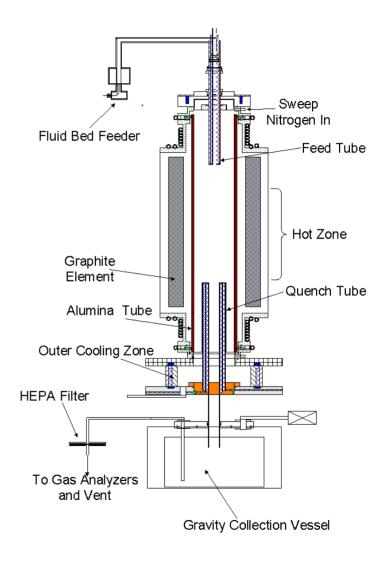
- Demonstrated high conversions of Mn₂O₃ dissociation in an Aerosol Flow Reactor (AFR)
- NaOH removal by vaporization was investigated
- Explored carrying residual NaMnO₂ through the cycle
- Testing in progress with mixed manganese oxides for more efficient NaOH recovery

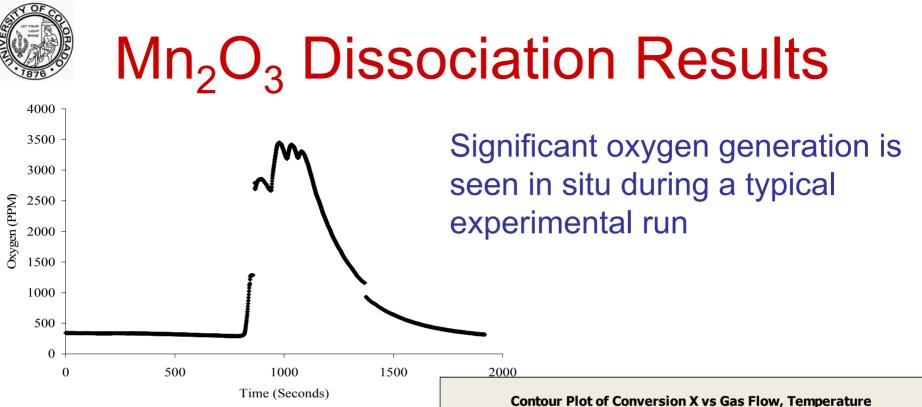


Mn₂O₃ Dissociation

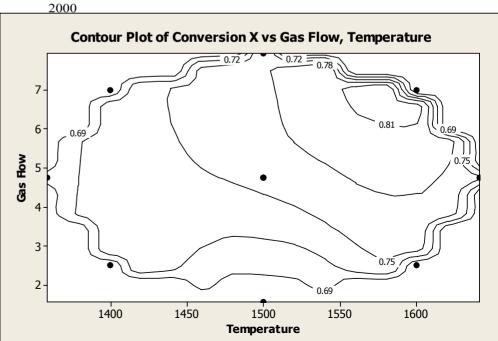


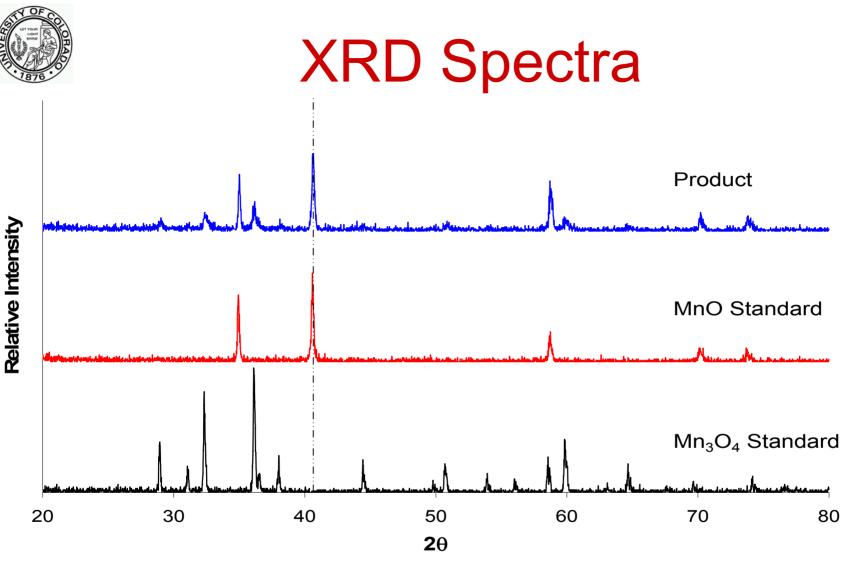
Experiments are being conducted with a two factor Central Composite Design (CCD)





Results show increasing temperature and gas flow rate resulted in the highest conversion. This indicates that recombination of oxygen may have a significant effect.





XRD spectra show a strong MnO spectrum and a weak Mn_3O_4 spectrum. A dotted line helps illustrate that all of the peaks can be seen from the MnO standard and only the major peaks from the Mn₃O₄ standard.



Dissociation Objective Progress

- Demonstrated high conversions in an AFR
 - Oxygen generation detected in situ
 - XRD confirmed MnO presence
 - $-O_2$ analysis showed conversions as high as 82%
- More experimental work to come
 - Investigation of recombination rates
 - Thermogravimetric mechanistic studies



Steps 2 - 3 in Manganese Cycle

- NaOH separation is the biggest challenge
 - 10% sodium residual
 - 100 torr H₂
- Solutions Currently investigating
 - Thermal separation of NaOH
 - Processing residual NaMnO₂
 - Mixed manganese oxides
- More Potential Solutions
 - Different M-OH sources (Potassium, ...)
 - Different separation approaches



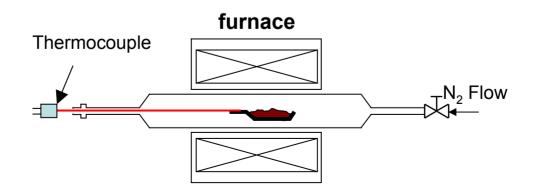
Thermal Separation of NaOH

Vaporize NaOH to separate it from Mn₂O₃

- 2_{III}⁵⁻² screening design
- FactorsSample MassNon-Isothermal/IsothermalGas Flow RateTemperatureHold Time

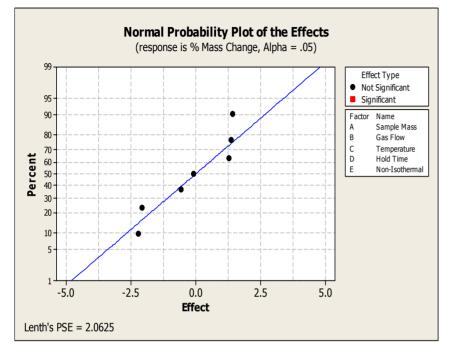
A horizontal tube furnace is utilized to conduct experiments

Pull sample into hot zone at desired temperature and time





NaOH Vaporization Results



Results indicate that a significant amount of NaOH was not vaporized. In addition, a statistical analysis shows that there are no significant effects. This indicates that within the ideal operating ranges selected for the factors that it is not possible to achieve a high vaporization rate of NaOH.

For the vaporization to proceed at an ideal rate a high temperature is required

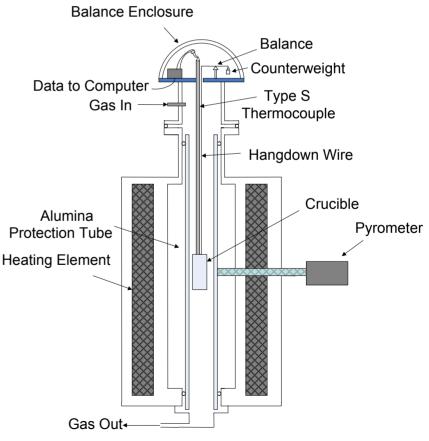
- Likely problems with a higher temperature
 - Reverse reaction to NaMnO₂
 - Partial reduction of Mn₂O₃ to Mn₃O₄

Conclusion: Vaporization of NaOH is not a viable method to separate Mn_2O_3 and NaOH

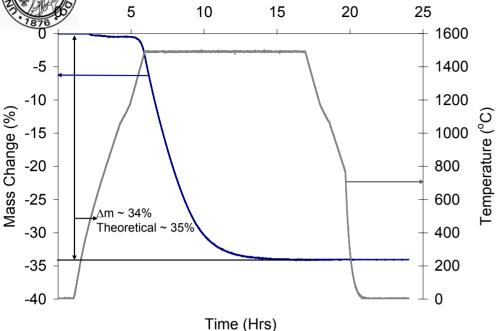
Processing Residual NaMnO₂

High temperature step with NaMnO₂ 2NaMnO₂(s) \rightarrow Na₂O(vapor) + 2MnO(s) + $\frac{1}{2}O_2$ Na₂O + H₂O \rightarrow 2NaOH Balance Enclosure

- Attempt proof of concept at Mn₂O₃ dissociation operating conditions
 - Use a Thermal Gravimetric Analyzer (TGA)



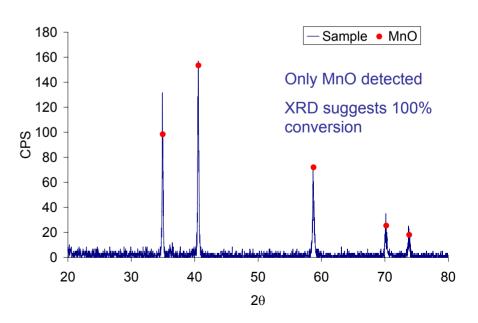
Proof of Concept Results



It has been demonstrated using a TGA that MnO is formed at 1500°C

- What form does the sodium take?
- Will the reaction kinetics become faster when diffusion resistances are negligible?

- Future work
 - Study sodium product gas with a mass spectrometer
 - Look at reactions kinetics in an AFR





Mixed Manganese Oxides

Use of mixed metal oxides may potentially improve $Mn_2O_3/NaOH$ separation

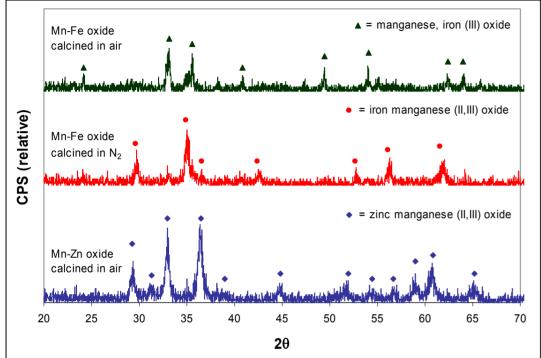
- Research divided into 3 phases
 - 1. Synthesize $Mn_xFe_{1-x}O$ and $Mn_xZn_{1-x}O$
 - 2. Verify hydrogen production with these mixed oxides

 $Mn_xFe_{1-x}O + NaOH \rightarrow ? NaMn_xFe_{1-x}O_2 + \frac{1}{2}H$

3. Investigate the mixed oxide – NaOH separation efficiency

- Compare with Mn_2O_3 - NaOH separation

Mixed Oxide Identification



Sol-gel precipitation reaction in basic solution from metal salts •Calcination of precipitate (air, N2)

Currently mixed manganese oxides are showing mixed oxidation states. It is necessary to produce these with only the +2 oxidation state

Next steps

- •Calcine with reducing atmosphere
- •Reduce existing mixed oxide into lower oxidation state
 - •This will verify hydrogen production



Future Work

- On sun testing of Mn₂O₃ dissociation
 - Reactor design and construction
 - Materials testing
 - Alumina
 - Silicon Carbide
- Continue future work plans detailed earlier in the presentation
 - $-Mn_2O_3$ decomposition
 - Processing residual NaMnO₂
 - Mixed manganese oxide investigation
- Update H2A analysis with new experimental results



Conclusions/Summary

Significant experimental progress has been made with the Mn₂O₃/MnO cycle

- High conversions for Mn₂O₃ have been demonstrated
- Potential solutions for NaOH recovery have been identified and investigations have begun
- Studies in alternative ways to close the cycle are ongoing
 - Mixed manganese oxides