

### Synthesis and Characterization of Alanes for Automotive Applications

Jason Graetz, J. Wegrzyn, J. Reilly, J. Johnson, WM Zhou

#### **BROOKHAVEN** NATIONAL LABORATORY

# Part of the DOE Metal Hydride Center of Excellence 05/17/2006

Project ID #: ST20

This presentation does not contain any proprietary, confidential, or otherwise restricted information

#### Overview

#### Timeline

- Project start date: FY05
- Project end date: FY10
- 40 % complete

#### Budget

- Expected total project funding: – \$3.00M (DOE)
- Funding received in FY06
  - \$400K (DOE)
- Funding for FY07:

NATIONAL LABOR

– \$925K (DOE)

#### Barriers

MYPP Section 3.3.4.2.1 On-Board

- **Storage Barriers**
- A. Weight & Volume
- B. Cost
- C. Efficiency
- D. Durability/Operability
- E. Charge/Discharge Rates
- **R.** Regeneration Processes

#### **Partners and Collaborators**

- Project D (aluminum hydride) Lead
  JPL, U. Hawaii, ORNL, SRNL, SNL
- Chemical Hydride Center
- IPHE and IEA collaborations

   IFE (Norway), Polish Academy of Sciences, Russian Academy of Sciences, Academy of Sciences of Ukraine



### Challenges and Objectives

**Goal**: Develop and demonstrate a hydrogen storage system that meets DOE targets using aluminum hydride as a hydrogen fuel source.

**Challenge**: AlH<sub>3</sub> thermodynamically unstable below 7 kbar (300K)

- In an AlH<sub>3</sub> system H<sub>2</sub> evolution controlled by T (rather than P) so the ability to tune decomposition kinetics will be critical Various routes exist to adjust kinetics (e.g. size & coatings)
- 2. The key issue is regeneration (hydrogenation of AI metal)
  - Multiple regeneration pathways are being investigated

#### **Objectives**:

- 1. Produce aluminum hydride with 9 wt. %  $H_2$  and 0.13 kg  $H_2/L$
- 2. Develop practical and economical process for the regeneration of  $AIH_3$  from the decomposed AI.
- 3. Assist in the design for an onboard fuel tank delivery system





### **BNL** Approach



#### Task 5: Management

- Coordinate MHCoE Alane subgroup
- Partnerships and reporting: supplying partners with samples (e.g. AIH<sub>3</sub>)
- Materials characterization at unique BNL facilities (e.g. NSLS and CFN)





# Why AIH<sub>3</sub>?

- $10^{1}$ - Large gravimetric & volumetric capacity  $\gamma$ -AIH<sub>2</sub> **10.1 wt%** (2010 S-Target = 6.0)  $10^{0}$ DOE target for 50 kW FC 149 g/L (2010 S-Target = 45) **Rate (g H<sub>2</sub>/s)** 10<sup>-1</sup> Low decomposition enthalpy  $\Delta H_{\alpha \Delta IH3} \approx 7 \text{ kJ/mol } H_2 (\approx 1/5 \Delta H_{\text{NaAIH4}})$ 10<sup>-2</sup> Dow stabilized  $\alpha$ -AIH<sub>a</sub> (Herley et al.) - Rapid H<sub>2</sub> evolution rates at low T Н 10<sup>-3</sup> Meets DOE target (50 kW FC) at 115°C with 45% FC efficiency  $10^{-4}$ (120kW at 100%) 40 60 120 160 80 100 140 Temperature (°C)
- Decomposition rates tuned through particle size and coatings
- High purity  $H_2$  AIH<sub>3</sub> decomposes to AI and  $H_2$  (no side reactions)
- Cyclability Offboard regeneration may reduce cycling problems

NATIONAL LABOR

- Regeneration will be challenging, but intrinsic energy costs are low



# **Progress on Regeneration**

- FY06: Background studies regeneration requires a basic understanding of physics/chemistry of AIH<sub>3</sub>
  - Crystallographic Structures of AIH<sub>3</sub>
  - Thermodynamics
  - *P*-*T* phase diagram for  $\alpha$ -AlH<sub>3</sub>
  - Literature Review (selected organometallic route for exp. study)
  - Preliminary experimental design and safety review
- Program Review Feedback- focus on regeneration
- FY07 Multiple approaches to regeneration
  - Recycling route studies (e.g. LiCl splitting)
  - Organometallic route Experimental progress to date:
    - Retrofit 200 bar Parr reactor and purchased 340 bar PPI reactor
    - Preliminary studies on  $AIH_3$ -TEDA in THF and dodecane
    - Reduced hydrogenation pressure using activated AI powder
  - Electrochemical route being investigated at SRNL
  - Supercritical fluid route being investigated at UH (proposal submitted)





### Synthesis of AIH<sub>3</sub>

- Regeneration rate and efficiency will likely be a function of crystallite size and surface condition
- Different AIH<sub>3</sub> morphologies easily prepared in conventional procedure

 $3LiAlH_4 + AlCl_3 + ether \rightarrow 3LiCl_{4} + 4AlH_3 \cdot 1.2[(C_2H_5)_2O] + ether$ **Desolvation Batch/Continuous Reactions Microcrystallization Reaction** 

 $\alpha$ -AlH<sub>3</sub> (Dow) 50-100 $\mu$ m

 $\alpha$ -AIH<sub>3</sub> (BNL) 100-200 nm

- Surface coatings (e.g. oxides) introduced through alcohol wash





# Which Structure of AIH<sub>3</sub> is Most Stable?

- Regeneration requires better understanding of phases and stability
- 2005 Ke et al. identified two structures of AlH<sub>3</sub> (orthorhombic *Cmcm* and cubic *Fd-3m*) more stable than  $\alpha$ -AlH<sub>3</sub> (hexagonal) using DFT
- 2006 IFE group solved the structure of  $\alpha$ '-AIH<sub>3</sub> (orthorhombic, *Cmcm*)
- 2006 Collaboration UH, BNL and IFE synthesized and solved structures of  $\beta$ -AIH<sub>3</sub> (cubic, *Fd-3m*) and  $\gamma$ -AIH<sub>3</sub> (tetragonal, *Pnnm*)
- All three phases less stable than  $\alpha$ -AlH<sub>3</sub> at temperatures  $\geq$  300K



(1) H.W. Brinks, A. Istad-Lem, B.C. Hauback, JPCB, **110** 25833 (2006); (2) H.W. Brinks, C. Brown, C.M. Jensen, J. Graetz, J.J. Reilly, B.C. Hauback, *JALCOM*, (2006); (3) H.W. Brinks, W. Langley, C.M. Jensen, J. Graetz, J.J. Reilly, B.C. Hauback, *JALCOM*, (2006); (3) H.W. Brinks, W. Langley, C.M. Jensen, J. Graetz, J.J. Reilly, B.C. Hauback, *JALCOM*, (2006); (3) H.W. Brinks, W. Langley, C.M. Jensen, J. Graetz, J.J. Reilly, B.C. Hauback, *JALCOM*, (2006); (3) H.W. Brinks, W. Langley, C.M. Jensen, J. Graetz, J.J. Reilly, B.C. Hauback, *JALCOM*, (2006); (3) H.W. Brinks, W. Langley, C.M. Jensen, J. Graetz, J.J. Reilly, B.C. Hauback, *JALCOM*, (2006); (3) H.W. Brinks, W. Langley, C.M. Jensen, J. Graetz, J.J. Reilly, B.C. Hauback, *JALCOM*, (2006); (3) H.W. Brinks, W. Langley, C.M. Jensen, J. Graetz, J.J. Reilly, B.C. Hauback, *JALCOM*, (2006); (3) H.W. Brinks, W. Langley, C.M. Jensen, J. Graetz, J.J. Reilly, B.C. Hauback, *JALCOM*, (2006); (3) H.W. Brinks, W. Langley, C.M. Jensen, J. Graetz, J.J. Reilly, B.C. Hauback, *JALCOM*, (2006); (3) H.W. Brinks, W. Langley, C.M. Jensen, J. Graetz, J.J. Reilly, B.C. Hauback, *JALCOM*, (2006); (4) H.W. Brinks, W. Langley, B.C. Hauback, *JALCOM*, (2006); (4) H.W. Brinks, W. Langley, B.C. Hauback, *JALCOM*, (2006); (4) H.W. Brinks, Hauback, *JALCOM*, (4) Hauback,





# Formation of $\alpha$ -AIH<sub>3</sub> From the H<sub>2</sub> and AI

– Does  $\alpha$ -AlH<sub>3</sub> transform to a more stable phase at high pressure? – What does the  $\alpha$ -AlH<sub>3</sub> phase diagram look like?



- Structural studies of  $\alpha$ -AIH<sub>3</sub> show no first-order phase transition at high pressure<sup>\*</sup>
- DFT results base on exp. lattice suggest structure is destabilized at pressure<sup>\*\*</sup>
- No hydrogenation below 573K low T region of phase diagram calculated from  $\Delta G$
- AIH<sub>3</sub> formation limited by thermodynamics <u>and</u> low temperature kinetics



\*\*Funded through BES

9



## Regeneration Energy Requirements and BNL Targets

In an effort to concentrate on the most promising pathways we have established two regeneration targets:

- (1) Energy required for regeneration will not exceed 30% of the fuel energy
- One mole of AlH<sub>3</sub> contains 360 kJ of fuel energy based on the lower heating value LHV<sub>H2</sub>=120 kJ/g = 240 kJ/mol H<sub>2</sub>. Therefore, 30% energy target equivalent to ∆E<sub>regen</sub>≤ 73 kJ/mol H<sub>2</sub>
- Direct hydrogenation of AI to form AIH<sub>3</sub> (298K) requires a minimum of 0.13 J for every 1.0 J of fuel energy (13% of fuel energy needed for regeneration)
- (2) Regeneration process will produce AlH<sub>3</sub> with at least 90% purity
- Offboard hydrogenation will utilize spent AI





### Recycling Route - LiCl splitting



<u>Synthesis</u>:  $AICI_3 + 3LiH \rightarrow AIH_3 + 3LiCI$ 

– Recycling byproducts (LiCl and Al) requires splitting 3LiCl per AlH<sub>3</sub>:

#### <u>Recycling</u>: AI + 3LiCl + $3/2H_2 \rightarrow AICl_3$ +3LiH

– With perfect efficiency (AICl<sub>3</sub> & LiH formation energy not wasted):

 $\Delta E_{\text{recycle}} \ge 167 \text{ kJ/mol H}_2$ 

– Recycling  $AIH_3$  by splitting LiCl (298K) requires a <u>minimum</u> of 0.7J for every 1J of fuel (**70% of fuel energy required for regeneration**)

– Recycling AIH<sub>3</sub> by splitting LiCI will not be investigated further





# Liquid Organometallic Route - Overview

- Form AlH<sub>3</sub> complexes from Al and H<sub>2</sub> in organic solvents (THF, Et<sub>2</sub>O)
- Reduce  $P_{eq}$  by forming a more stable intermediate phase
- Reaction between AI,  $H_2$  and triethylenediamine (TEDA =  $C_6H_{12}N_2$ )

AlH<sub>3</sub>  
Al + H<sub>2</sub> + 
$$N$$
  $N$   $N$  E.C. Ashby, JACS, (1964).

- FY07 Milestone: Improve hydrogenation kinetics & reduce required pressure
- Second step required to extract TEDA and recover pure AIH<sub>3</sub>:



– Another route under investigation is a reversible metal-organic hydride:





## Liquid Organometallic Route - Results

#### Organometallic hydrogenation of aluminum



 Hydrogenation of activated AI (AI\*) at 300K occurred at much lower pressures than expected (no reaction with non-activated AI up to 110 bar)

- Reaction is reversible: TEDA + AI\* +  $H_2 \leftrightarrow TEDA$ -AI $H_3$  (theor. 2.1 wt%  $H_2$ )



# Liquid Organometallic Route - XRD Analysis



- Powder XRD confirms 100% of AI consumed in reaction (yield near 100%) - No evidence of any phase other than TEDA-AIH<sub>3</sub> (no side reactions)





## Liquid Organometallic Route - FTIR Analysis





NATIONAL LABORATORY

#### Liquid Organometallic Route Energy Requirements

Energy required to form TEDA-AIH<sub>3</sub> is small, but how much energy is required to break AIH<sub>3</sub> from TEDA to recover pure AIH<sub>3</sub>?



#### Path Forward - Regeneration

#### **Preliminary Studies:**

- Crystal structures and phase stabilities (complete)
- Reproduce Ashby's reaction (complete)
- Reduce hydrogenation pressure and temperature (complete)
- Explore Activated AI powder (ongoing)

#### **Regeneration Routes To Be Investigated:**

Preparation of pure AIH<sub>3</sub> by isolating from alane-adduct



Examine amine/adduct substitutions
 that form less stable compounds
 Evaluate energy requirements

Reversible metal organic hydrides:

$$Al + H_2 + \bigvee_{N}^{N} \longleftrightarrow_{N}^{N}$$

Examine solvent and adduct
substitutions to determine if
capacity can be improved
Evaluate thermodynamics



#### Path Forward - Regeneration

#### **Collaborations:**

**MHCoE Theory Group** - Identify possible adduct substitutions; Search for lighter adducts that accommodate multiple AIH<sub>3</sub> units; amine-alane chemistry

**Chemical Hydride Center of Excellence** - Information exchange; Synergisms between amine-borane and amine-alane investigations **IPHE/IEA** - Fundamental high pressure studies; high pressure hydrogenation; decomposition kinetics, insitu synchrotron XRD

#### **Decisions and Milestones:**

- FY07 Milestone: Hydrogenate AI at low temp and pressure (P<70 bar)</li>
- FY08 Go/no-go: Regeneration using organometallic approach
- FY09: Overall objective to regenerate AlH<sub>3</sub> with energy penalty ≤73 kJ/H<sub>2</sub> and a yield of ≥90% and (2) Determine mass/energy balance over 100 cycles on 5g samples





#### **Project Summary**

Goal: Develop and demonstrate a hydrogen storage system that meets DOE targets using aluminum hydride as a hydrogen fuel source.

Significant accomplishment: Direct hydrogenation of activated Al powder at P<35 bar (ten-fold reduction in pressure) with a yield near 100%

Storage Parameter	Units	2010 System Target	FY07 materials*
Gravimetric Capacity	kWh/kg	2.0	3.17(3)
	wt. % H <sub>2</sub>	6.0	9.5(1)
Volumetric Capacity	kWh/L	1.5	4.75(4)×
	$\mathrm{Kg}~\mathrm{H_2/L}$	0.045	0.143(2)
Desorption Temperature	°C	85	<100
Rate**(114 °C)	g/s/kW	1.0**	0.14(1) / 1.0(1)
BNL Regeneration Target	kJ/ mol H <sub>2</sub>	73	

\* Data is based on material only, not system value; \*\* Based on 50kW FC with 45% efficiency for 100kg AlH<sub>3</sub>; <sup>x</sup> Does not account for packing density (a conservative estimate for packing density is 50%)



