

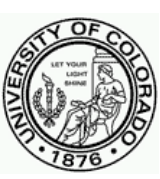
Fundamentals of a Solar-thermal $\text{Mn}_2\text{O}_3/\text{MnO}$ Thermochemical Cycle to Split Water

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**University of Colorado – Boulder
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Project ID No. PDP1

This presentation does not contain any proprietary or confidential information



Overview

Timeline

- 6-1-2005
- 5-31-2009
- 70%

Budget

•Total Project Funding

\$797,702

\$199,426 Contractor share

•Funds received in FY07

\$ 420,000

•Funds received in FY08

\$ 102, 298

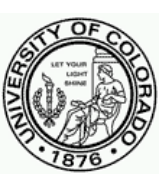
Barriers

- U. High-Temperature Thermochemical Technology
- V. High-Temperature Robust Materials
- W. Concentrated Solar Energy Capital Cost

Partners

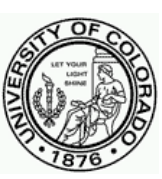
Swiss Federal Institute of Technology

University of Nevada – Las Vegas

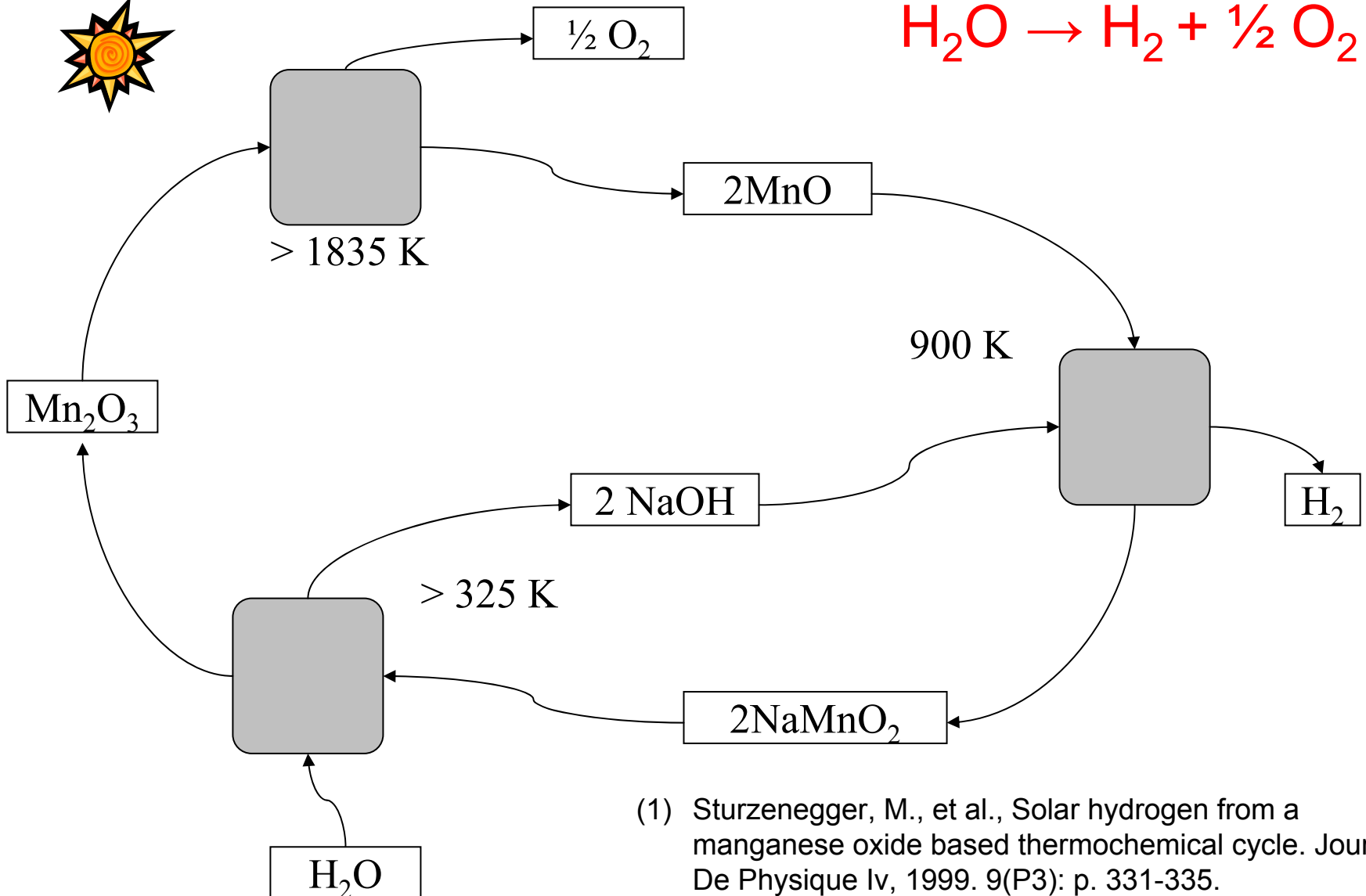


Objectives

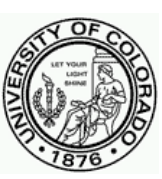
- Research and develop a cost effective $\text{Mn}_2\text{O}_3/\text{MnO}$ solar-thermal thermochemical cycle through theoretical and experimental investigation
- Based on the above, develop a process flow diagram and carry out an economic analysis of the best process option



Mn₂O₃/MnO Cycle



- (1) Sturzenegger, M., et al., Solar hydrogen from a manganese oxide based thermochemical cycle. Journal De Physique Iv, 1999. 9(P3): p. 331-335.



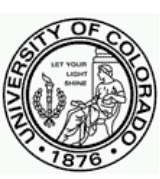
Approach

- Thermodynamic assessment of the cycle
- Experimental investigation
 - Investigate Mn_2O_3 dissociation and mechanism
 - Investigate H_2 generating step
 - Investigate ways in which to recover NaOH after H_2 generating step
 - Develop alternative methods in which to close the cycle
- Use H2A framework to economically evaluate the cycle



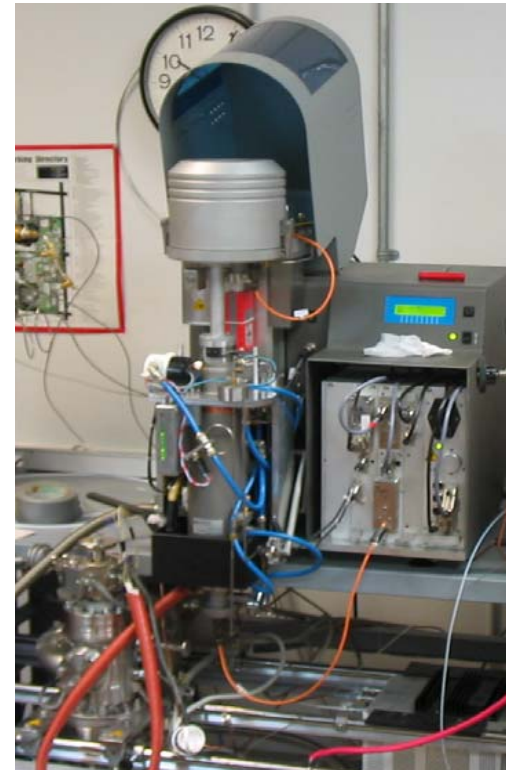
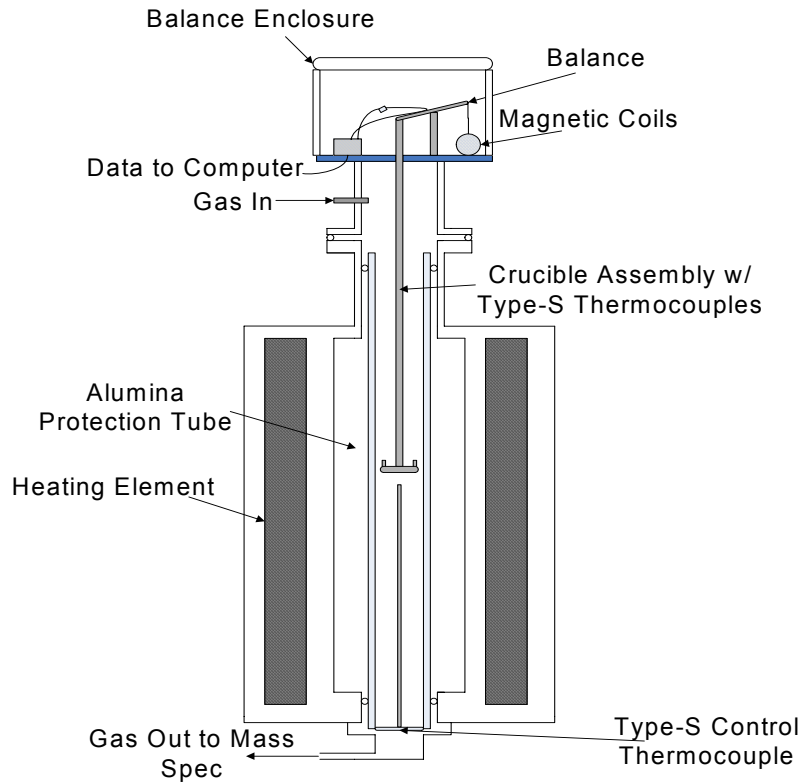
Technical Accomplishments / Progress / Results

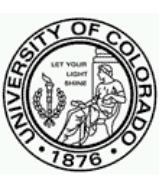
- Found a probable mechanism for manganese oxide dissociation
- Used mixed manganese oxides to study H₂ generation and NaOH recovery
- Investigated solid state synthesis of mixed oxide production
- Completed initial PFD



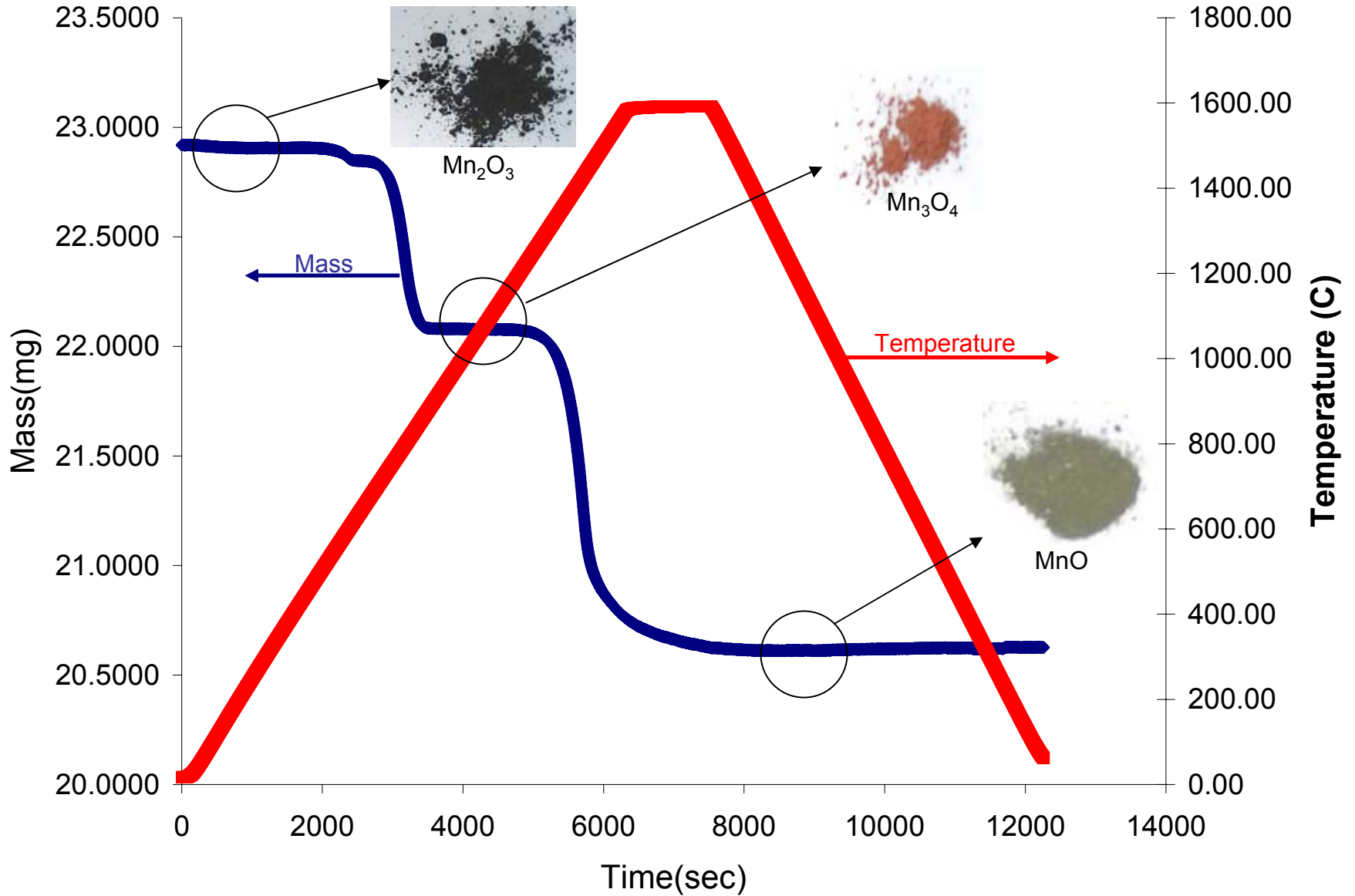
Reaction Kinetics From a TGA

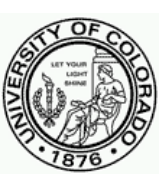
- Used TGA to understand mechanism and derive initial reaction kinetics
 - Reaction proceeds in two steps



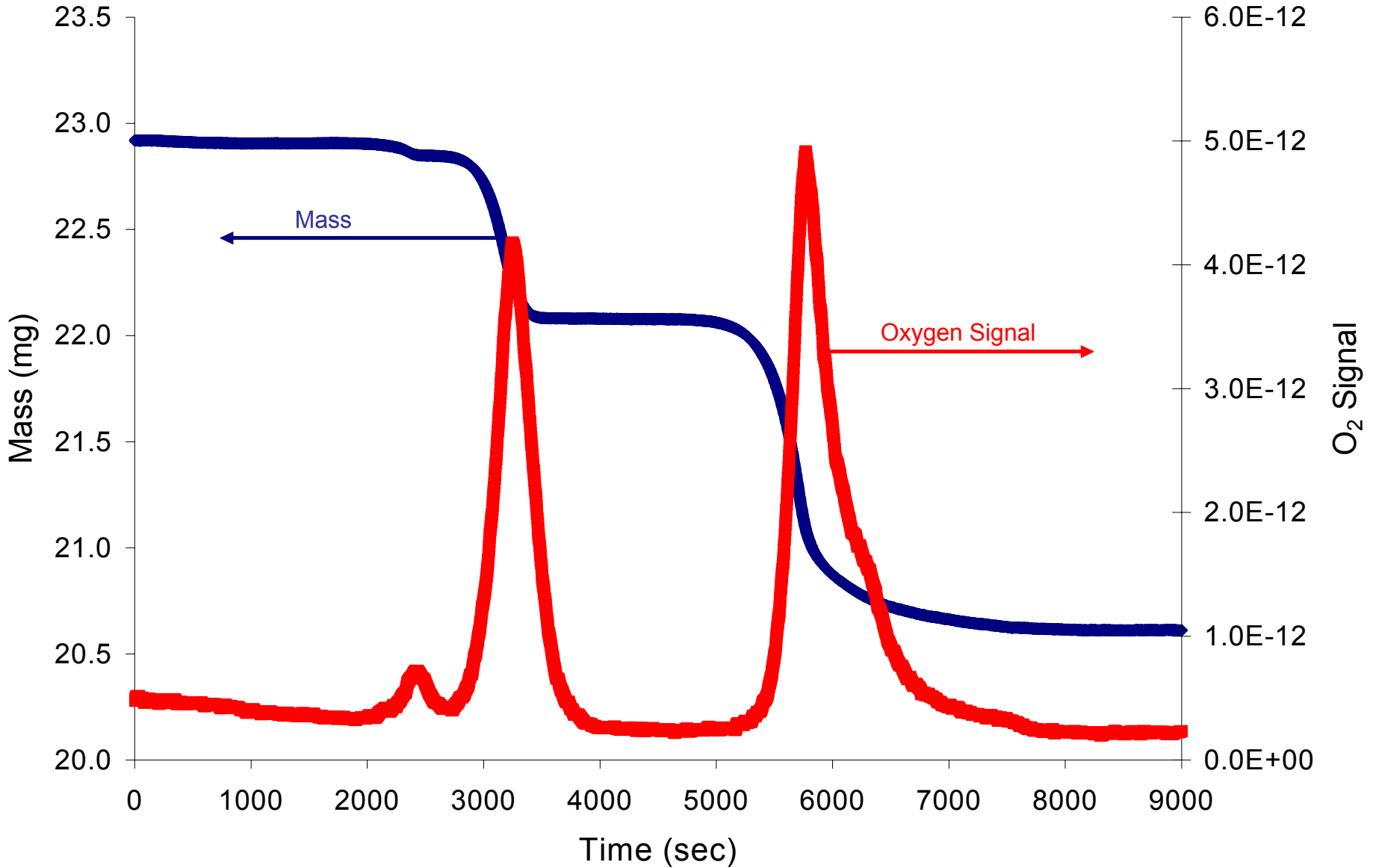


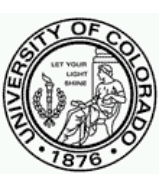
TGA Mass Trace





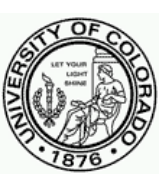
Mass Trace with Mass Spec Data





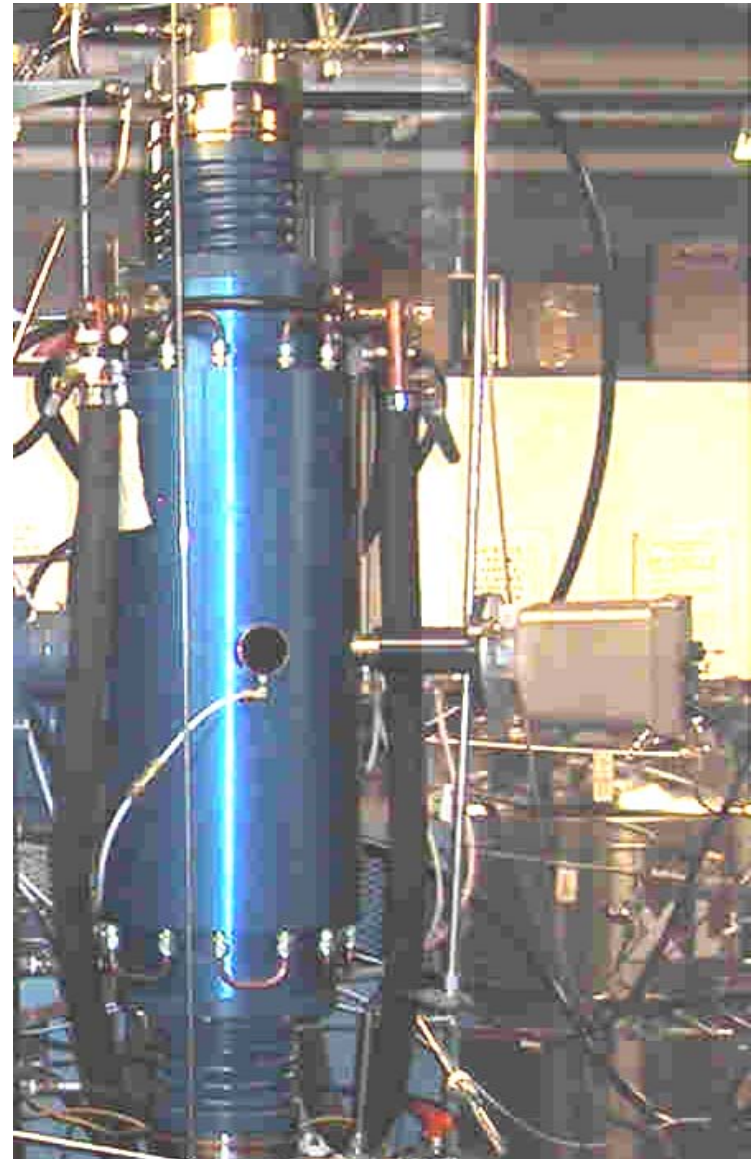
TGA Mechanism Progress

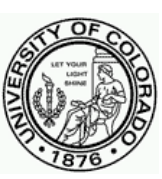
- An Avrami-Erofeev type mechanism is hypothesized to control both reactions
 - Parameters were calculated
- Hypothesized diffusion resistances control part of the $\text{Mn}_3\text{O}_4 \rightarrow 3\text{MnO} + \frac{1}{2}\text{O}_2$ transition



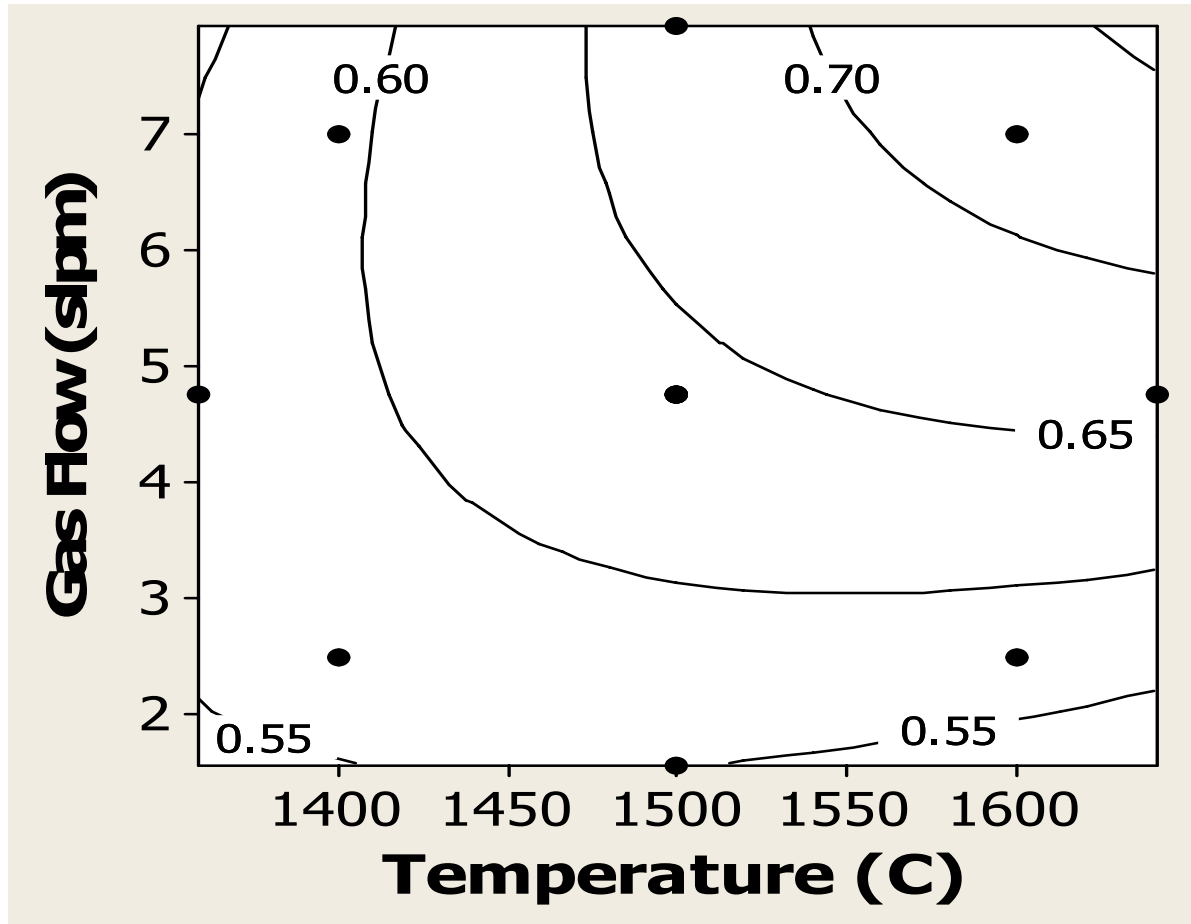
Mn_2O_3 Dissociation in an AFR

- Study manganese oxide dissociation in an Aerosol Flow Reactor
 - Diffusion resistances are limited
 - Reactor ideal for high volume processes
- Understand how oxygen can affect the reaction





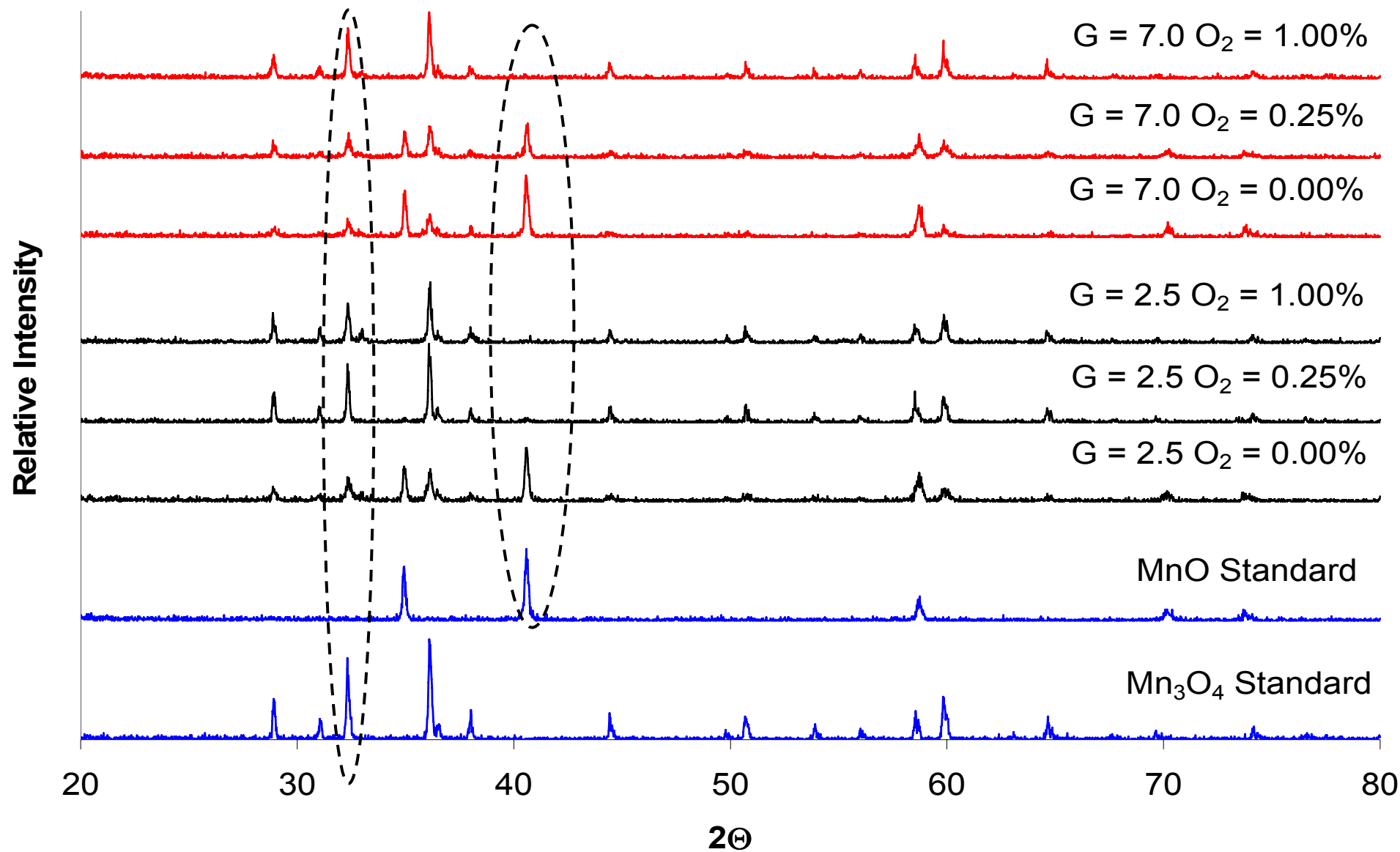
Reactor Conversions



Conversions ranged between 50 and 75%. Highest conversions achieved with high temperature and gas flow rate.



XRD Spectra 1400 °C





Reactant Regeneration Step

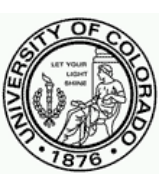


Issue: NaOH recovery

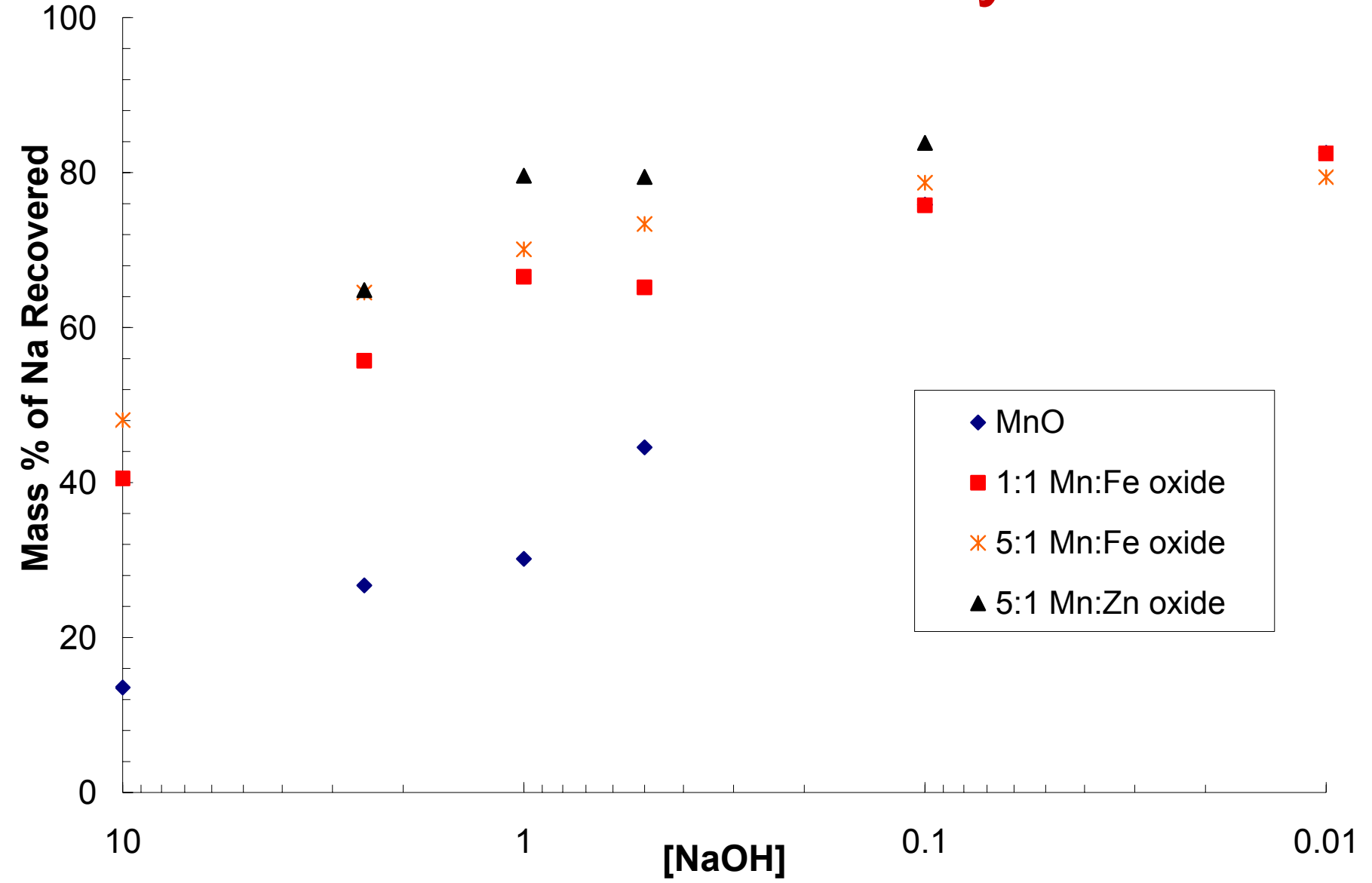
- 80 – 90% of NaOH can be removed with H₂O
- High energy requirement

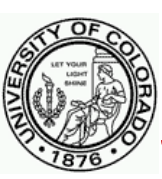
Solution: Mixed Manganese Oxides

- Rationale: Iron-analog NaFeO₂ can be hydrolyzed completely
- Test ratios Mn/Fe and Mn/Zn oxides



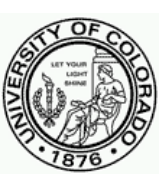
NaOH Recovery



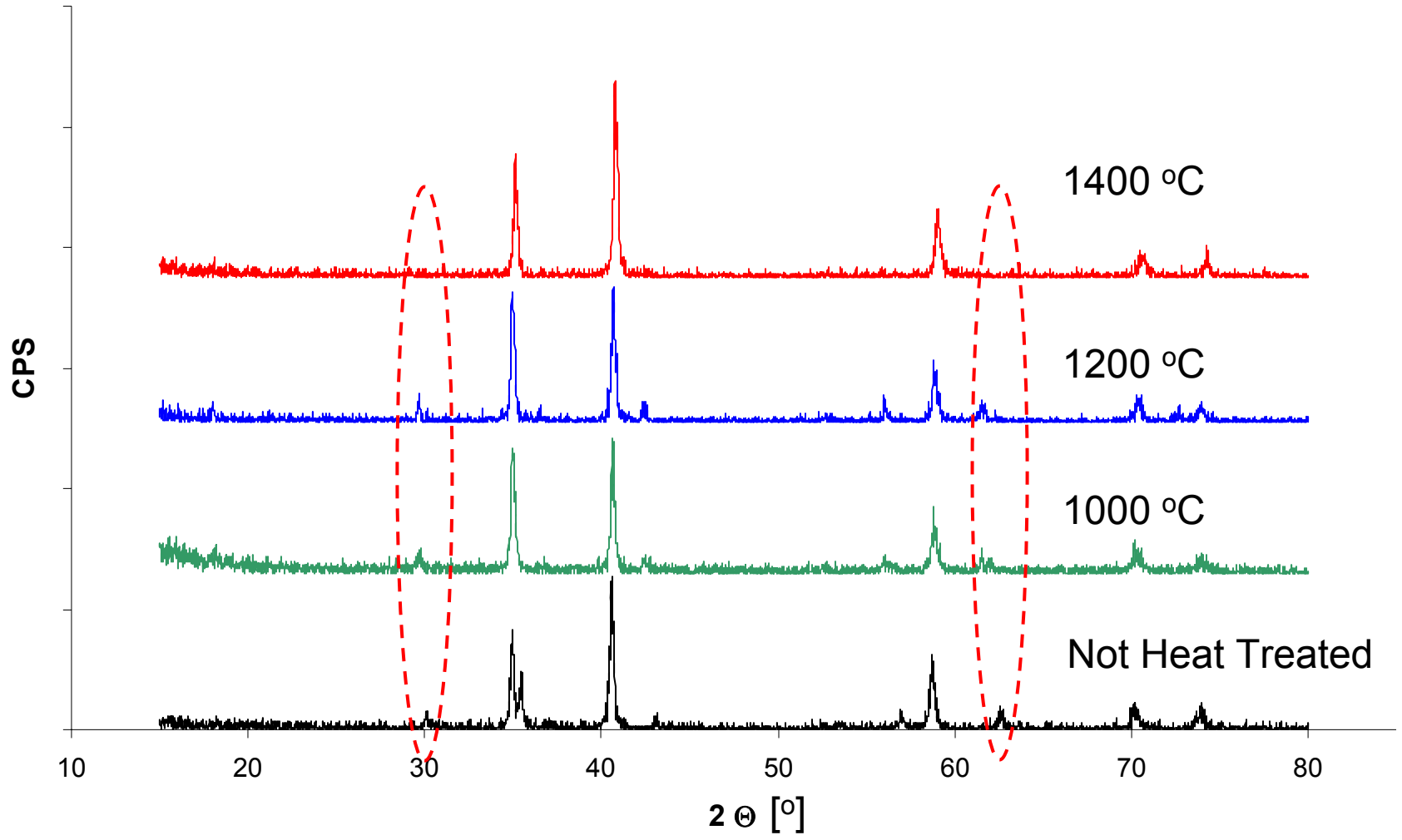


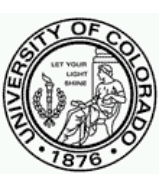
Synthesis of Mixed Metal Oxides

- **Solid state synthesis**
 - Provides control over composition
 - High temperature required
 - Large quantities easy to synthesize
 - Simple procedure
- **Method**
 1. Mill stoichiometric amounts of metal oxides
 2. Heat treat

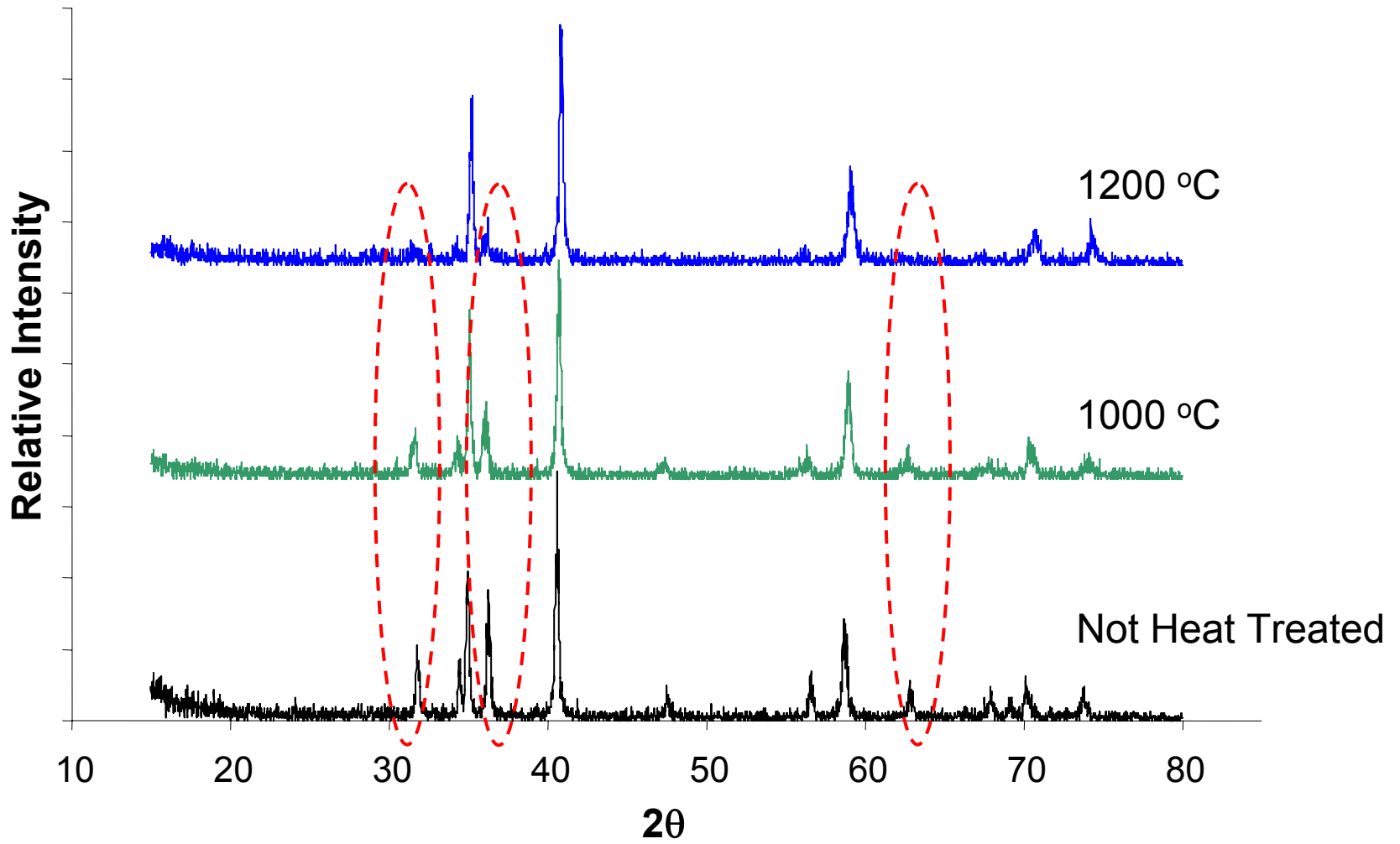


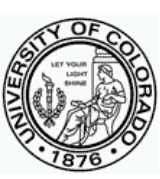
XRD Spectra of $\text{Mn}_{0.75}\text{Fe}_{0.25}\text{O}$



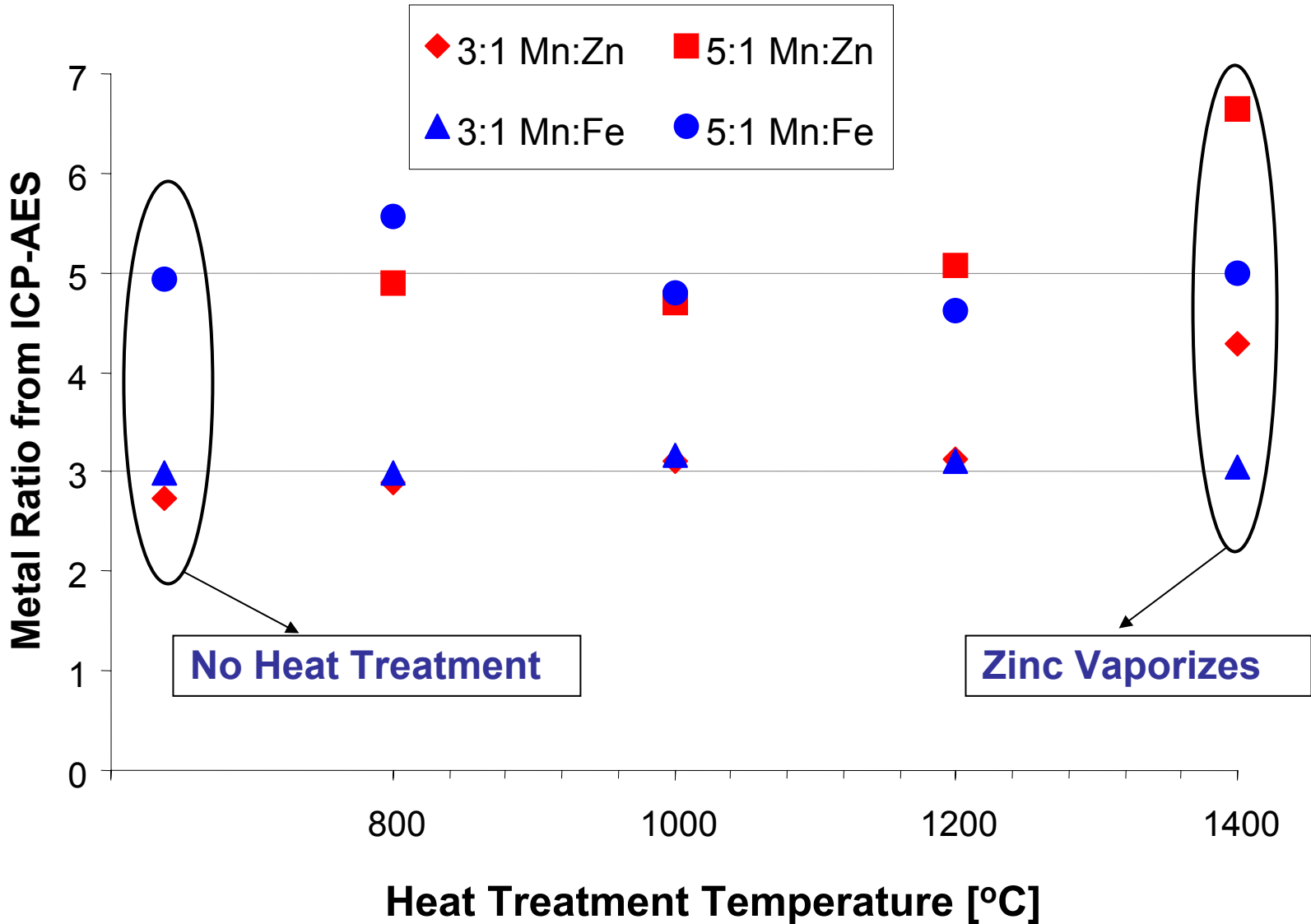


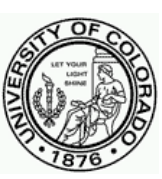
XRD Spectra of $\text{Mn}_{0.75}\text{Zn}_{0.25}\text{O}$



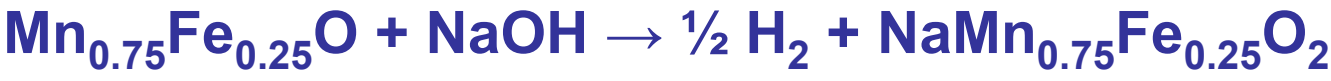
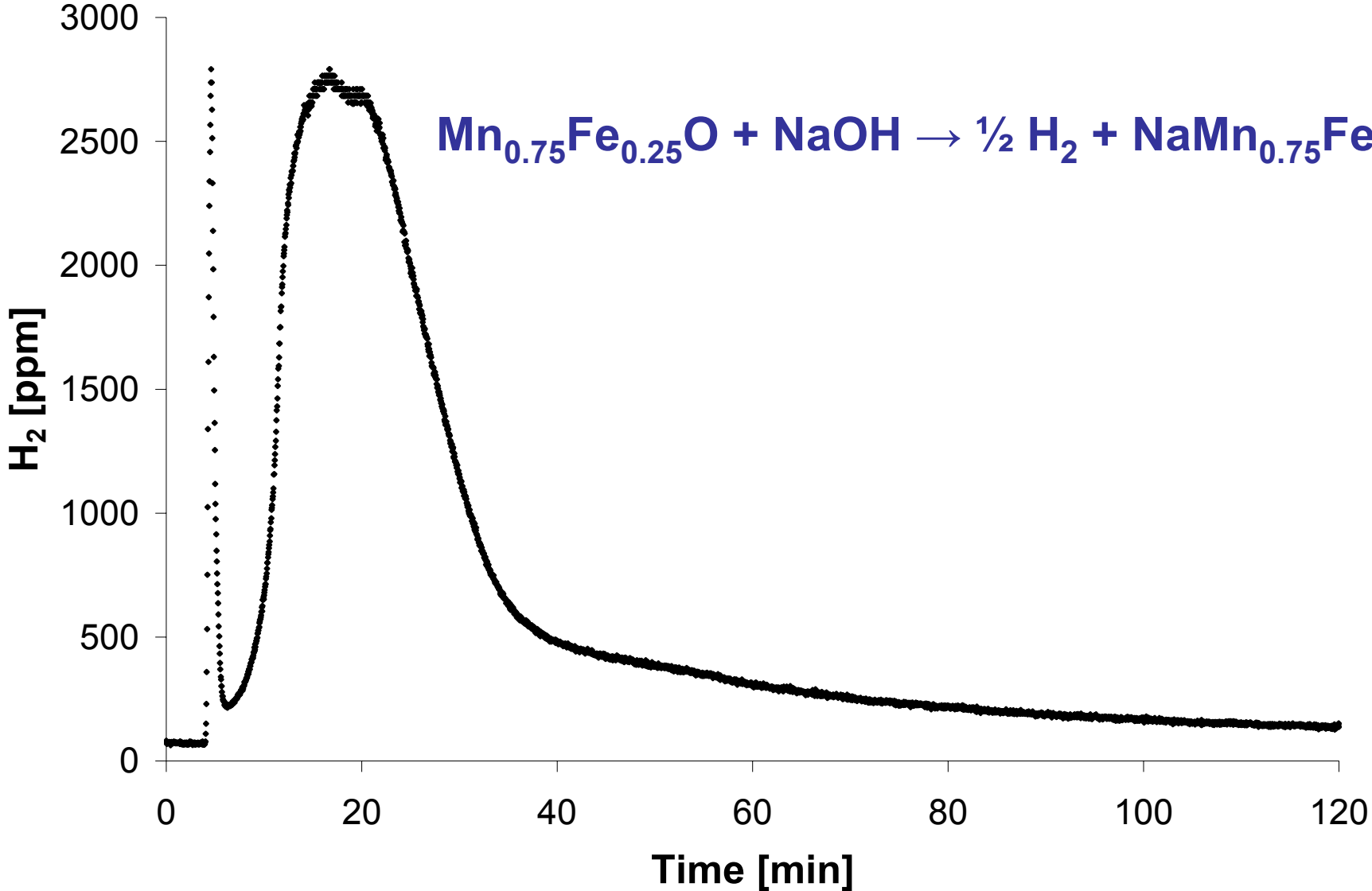


ICP of Mixed Mn Oxides



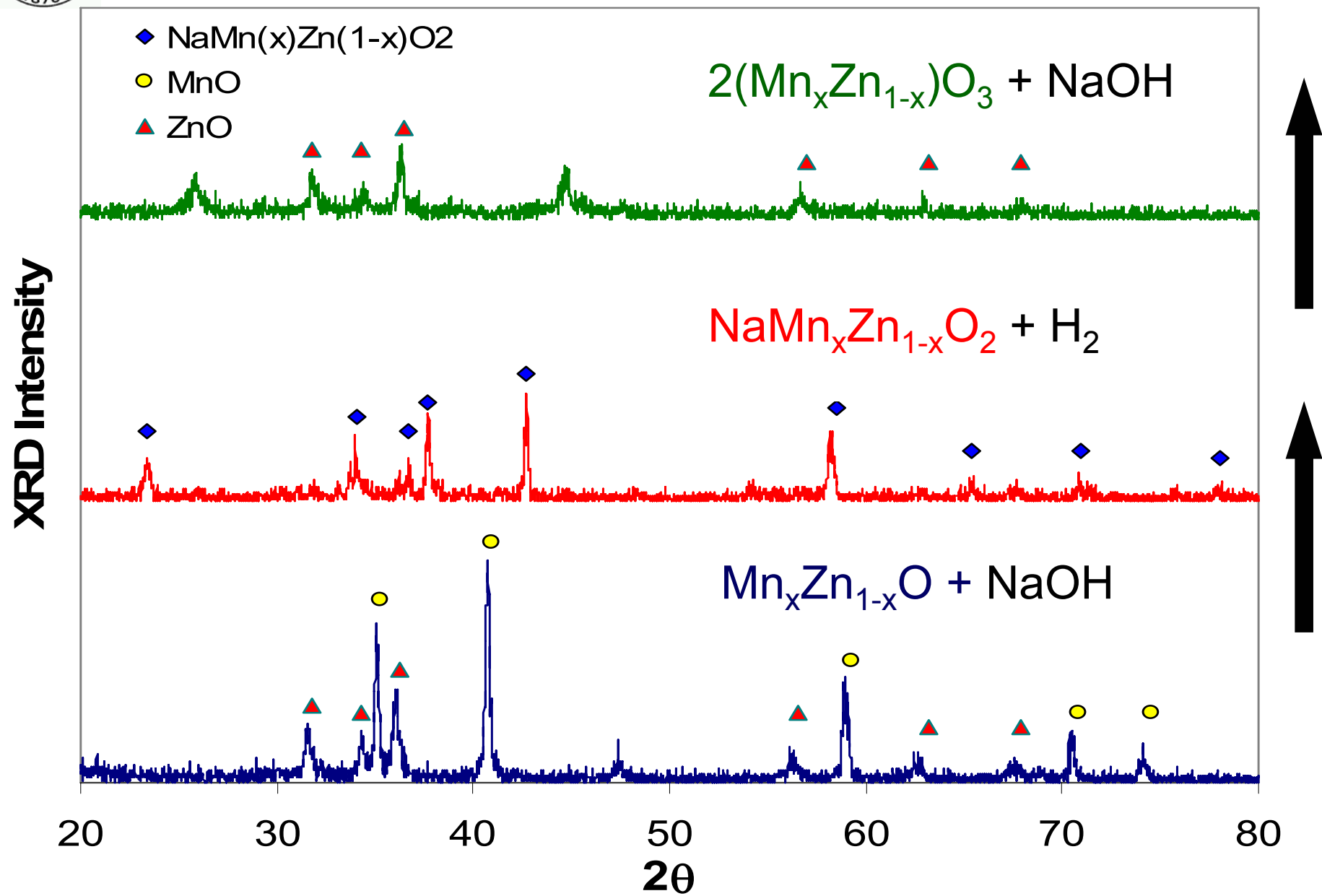


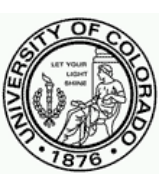
H₂ Generation From Mixed Oxide



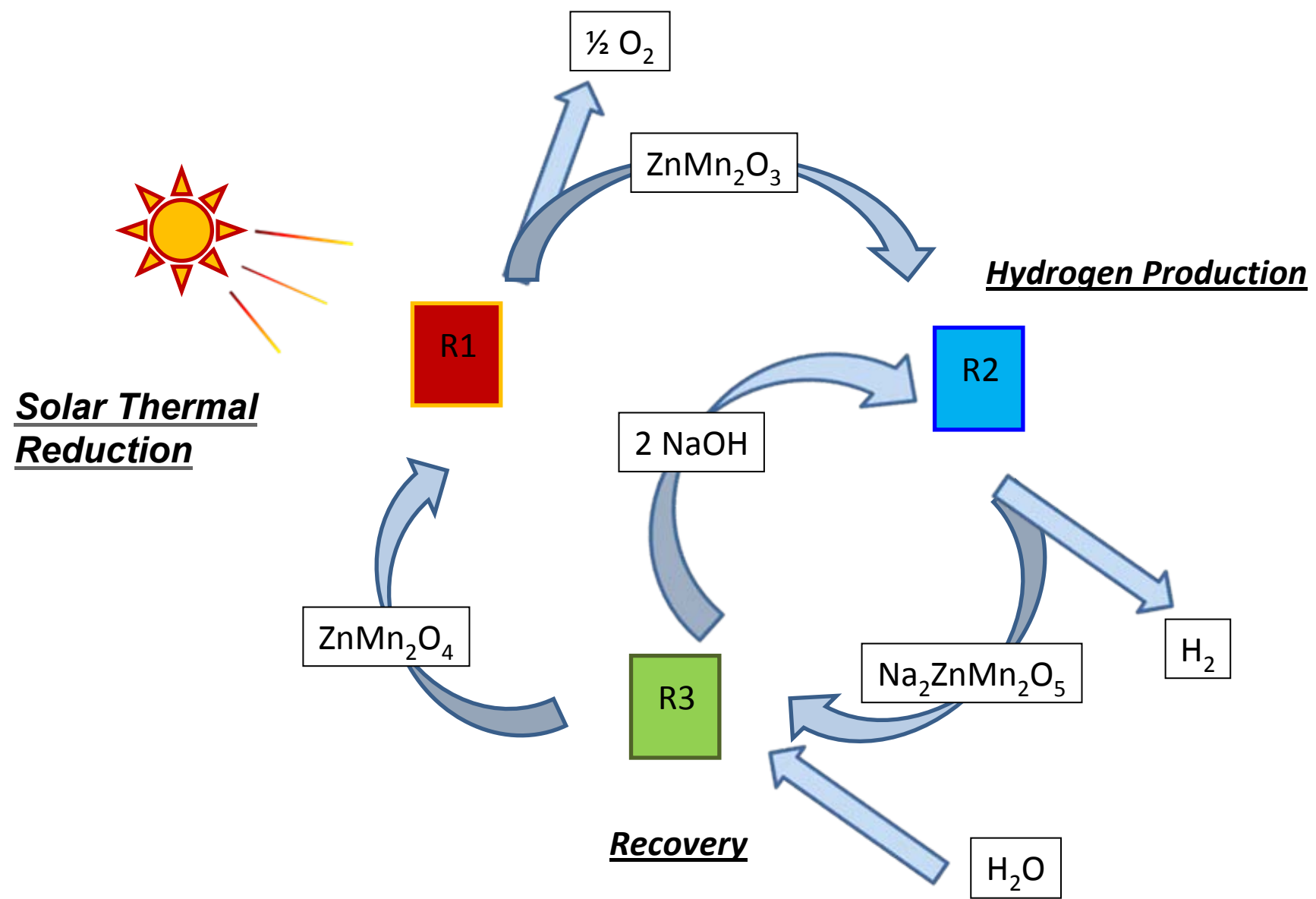


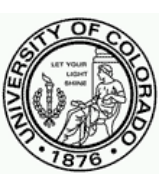
2nd and 3rd Steps Demonstrated



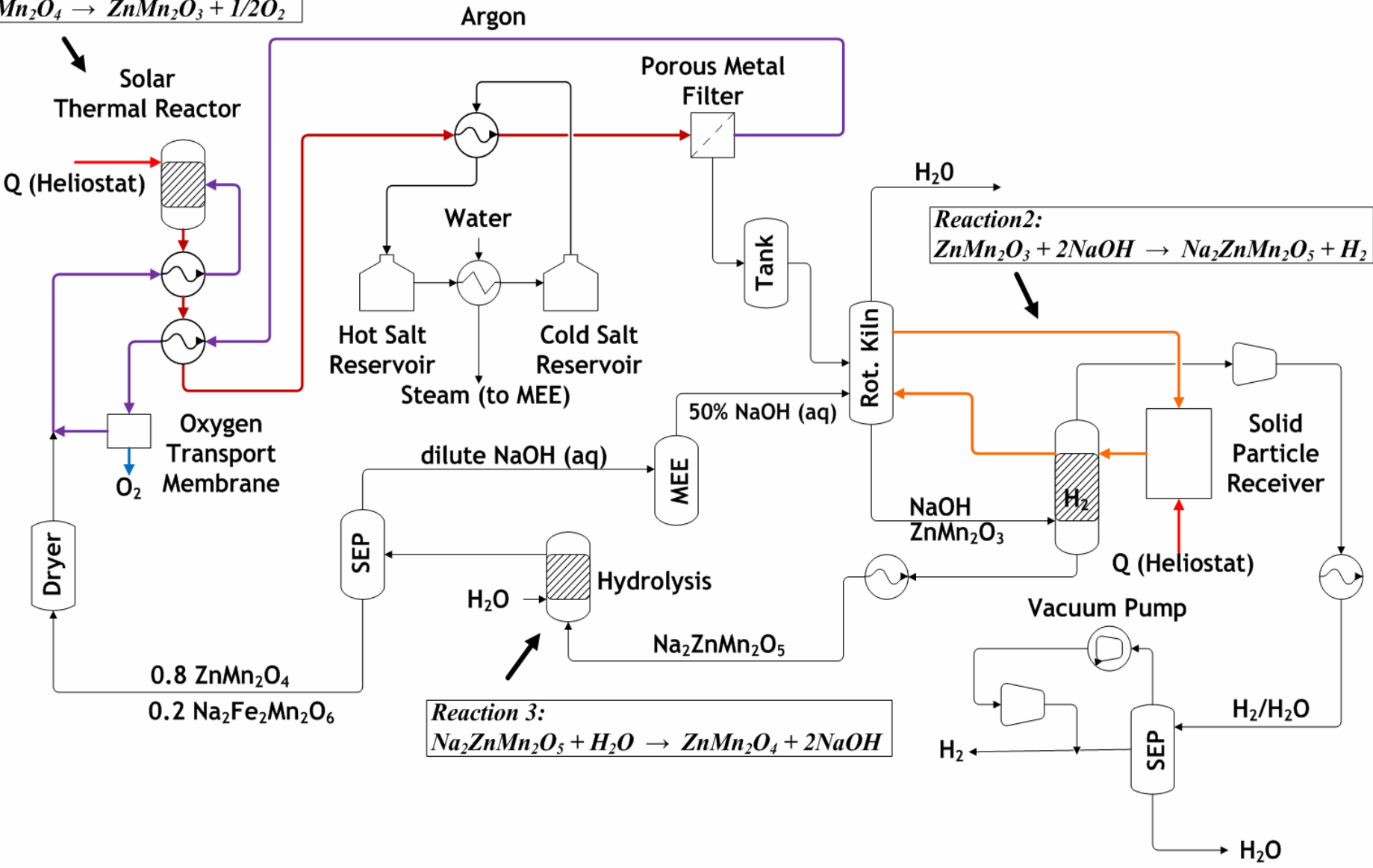


Mixed Metal Oxide Solar Thermal Cycle





ZnMn₂O₄/ZnMn₂O₃ – Process Flow Diagram





H2A Specifications

- Produce 100,000 kg H₂ per day at 300 psi
- 2012 startup at current inflation rate 2.4%
- 40 year economic analysis period
- Hydrogen cost goal of \$2-3 per kg



Economic Sensitivities

Carrier gas (Argon vs. Air)

- Best Case: Oxygen Transport Membrane

Heat recovery (Molten Salt)

- Heat feed stream
- Send steam to multiple effect evaporator
- Drive turbine to make electricity

NaOH recovery

- Improve chemistry to reduce water requirement

Compression

- Vacuum pump to draw off H₂



Future Work

- Testing of $\text{Mn}_{2-x}\text{Zn}_x\text{O}_3$ dissociation
 - Evaluate whether reaction mechanism is the same as Mn_2O_3
- Continue work on mixed manganese oxide synthesis
- Gain better understanding of H_2 generation with mixed manganese oxides
- Update process flow diagram with new results to reassess the $\text{Mn}_{2-x}\text{Zn}_x\text{O}_3 / \text{Mn}_{1-x}\text{Zn}_x\text{O}$ cycle



Conclusions/Summary

Significant progress has been made with the $\text{Mn}_2\text{O}_3/\text{MnO}$ cycle

- A reaction mechanism has been hypothesized for Mn_2O_3 dissociation
- Mixed manganese oxides have been shown to improve the product recovery steps
- Experimental investigation using a mixed manganese oxide is ongoing
 - Mn/Zn Oxide