

Hydrogen Fuel Quality The Year In Review

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Project ID # SCS4

Overview

Timeline

- Project start date: 10/1/06
- Project end date: 9/30/11
- Percent complete: 30%

Barriers

- Barriers addressed
 - I. Conflicts between Domestic and International Standards
 - N. Insufficient Technical Data to Revise Standards

Budget

- Total project funding: \$1,100K
 - DOE share: 100%
 - Contractor share
- Funding received in FY07: \$250K
- Funding for FY08: \$850K

Partners/Collaborators

- University of Hawaii/HNEI
- University of Connecticut
- University of South Carolina
- Clemson University
- SRNL
- NIST
- NREL
- ANL

2

Milestones & Deliverables

Month/Year	Milestone or Deliverable	
Dec-07	Milestone: Evaluate sensitivity of H2S specific ion analysis methods. Completed	
Mar-08	Milestone: Evaluate cross interference effects of H2S specific ion analysis methods. Completed	
Jun-08	Deliverable: Report on analytical methods development. Completed Milestone: Determine tolerable impurity level specifications for hydrogen fuels. Completed sulfur Milestone: Evaluate sensitivity of NH3 specific ion analysis methods. In progress*	
Sep-08	Milestone: Evaluate cross interference effects of NH ₃ specific ion analysis methods. Milestone: Demonstrate proof of concept of CO analysis by electrochemical methods.	



Technical Approach

- Conduct gauge studies with testing labs and address experimental differences, thus increasing the confidence in the data.
- Create and standardize a Data Reporting Format
- Develop and test new analytical methods for detecting ppb levels of contaminants.
- Test the critical constituents (NH₃, CO, and H₂S) and provide data sets to FC modelers to establish predictive mechanistic models.



LANL's role in understanding the impact of fuel impurities



The two tasks are separate but complimentary in that they leverage one another. The Fuel Impurities solicitation winners participated in the LANL-led DOE Round Robin to ensure consistent testing procedures and data collection. The learnings from the Fuel Impurities Efforts help establish testing priorities in the Hydrogen Quality effort.



This effort consists of several collaborators: UConn, Clemson, SRNL, University of S. Carolina, NIST, and HNEI.

Technical Accomplishments DOE Round Robin Results

The VI-curves were:

- Taken after completing a break-in procedure (0.6V for 1 hr then cycled 20 minutes at 0.5 and 0.7V for 6 hrs, overnight at 30A (cc))
- Run in constant current mode using 1.2/2.0 stoichs (H₂/Air) until deviation ≤ 5 mV from the previous VI-curves at multiple points (Pressurized and Ambient)





The average of the last 3 VI-curves was submitted for a Round Robin Study.

Technical Accomplishments DOE Round Robin Results, Cont.

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Round Robin Test Cell No. 2 N112, 50cm² A/C: 0.2 mg Pt/cm² T_{cell}: 60°C; P: Ambient (sea-level); Fully humidified





The average of the last 3 VI-curves was submitted for a Round Robin Study.

Technical Accomplishments DOE Round Robin Results, Cont.

Round Robin Test Cell No. 2 N112, 50cm2 A/C: 0.2 mg Pt/cm2 Tcell: 80oC; P: 25 psig(sea-level); Fullyhumidified



- Before and after tests showed nearly identical results, thus making the round robin results valid for comparison.
- Largest difference observed in Mass Transport Region
- Further analysis/tests to probe those differences

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Technical Accomplishments DOE Round Robin Results, Cont.





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Technical Accomplishments DOE Round Robin Results, Comparisons



- Overall good agreement between sites, discussions are on-going to address differences.
- Other test sites have expressed interested in the cell and are scheduled to test.
- Final Report in progress



Data Reporting Format



The document's objective is to describe in detail all the information necessary to describe and/or reproduce the performed contaminant experiment



Data Reporting Format

excerpt from start-up procedure

FC Operating Conditions		
Diagnostic Identifier (e.g. MEA 012)	LANL_TR040908	
G as Type		
Anode Gas Composition & Quality		
(e.a. 100% H ₂ . 99.999%)	electrolysis grade	
Cathode Gas Composition & Quality		
(e.g. oiless compressor, in-house produced)	oiless compressor	
Stoichiometry Mode		
Flow Tracking (yes / no)	yes	
Flows		
Anode Stoich (e.g. 1.2 or N/A)	1.2	
Cathode Stoich (e.g. 2.0, or N/A)	2	
Anode Fixed Flow (e.g. 1200 sccm, or N/A)	n/a	
Cathode Fixed Flow (e.g. 3 NL/min, N/A)	n/a	
Minimum Flow		
minimum anode flow setpoint		
(e.g. 80 sccm, or flow at 0.2 A/cm ²)	80 sccm	
minimum cathode flow setpoint		
(e.g. 80 sccm, or flow at 0.2 A/cm ²)	343 sccm	

Temperatures	
Cell (°C)	80°C
Humidification	
Anode Humidifier w/o Contaminant (°C)	
	80°C
Anode Humidifier w Contaminant (°C)	by pass
Anode RH (%)	100%
Cathode Humidifier (°C)	80°C
Cathode RH (%)	100%
Pressures	
Anode Inlet (psia)	
Anode exit (psia)	30
Cathode Inlet psia)	
Cathode exit (psia)	
	30
Start-Up Procedure	
(e.g. Company A's Protocol,	
cycling from 0.2-0.7V until	
currents stabilize)	LANL protoco



Ammonia Studies

Effects of 1ppm



The graph on the left shows reproducibility after two different cells were exposed to 1 ppm NH_3 . Losses observed were ~70 mV.

The graph on the right shows the impact of NH_3 at 0.4 and 1 A/cm². Clearly, the losses become more pronounced at the higher current density. The data show that with more water, the NH_4^+ migrates to the cathode faster.



Carbon Monoxide Studies



- 100 ppb CO showed ~5 mV loss over 300 hrs
- 200 and 300 ppb CO showed ~30 mV
- Some CO adsorption detected by CV



H₂S Studies



- Sulfur chemisorption onto Pt-sites deactivating the catalyst for hydrogen dissociation
- Other in-house results indicate sulfur crosses over to the cathode
- Low levels of sulfur can disable a fuel cell
- An increase in local water decreases the sulfur impact



Analytical Methods for ppb H₂S Determination

- Chemical trap used to capture all H₂S
 - pH>12 to insure S⁼ species in solution (1M NaOH + ascorbic acid and EDTA); flow rates optimized for 100% capture of H₂S
- Ag/AgS electrode, sulfide ion probe
 - Mode 1: EMF converted to [S⁼] using calibration data for qualitative determinations
 - Mode 2: Electro-titration: Pb⁺² titration is used in combination with EMF endpoint determination to validate mass of H₂S captured
- Isothermal measurement to ensure • accurate calibration is maintained
- H₂S delivery to experiment must be ٠ optimized to prevent adsorptive losses





[S⁼] may be found using probe EMF and an accurate calibration against standards

using

$$\mathsf{E} = \mathsf{E}_{o} + \mathsf{SLog}_{10}\mathsf{X}$$

where

E = measured electrode potential E_{o} = reference potential set by ref. solution S = electrode slope (typically -27 to -30 mV) 16 X = activity of S⁼ in solution

Commercial Ion-Selective Probes

- Not suitable to directly measure [S⁼] even when concentrating with a trap
 - Problems with probe sensitivity at low sulfide ion concentrations
 - Addition of small quantities of H₂S in trap can be seen as a change in EMF but calculation of [S⁼] from these small EMF changes is overwhelmed by a summation of many errors
 - One may only obtain a calibration "window"
 - Repeated testing of commercial probes shows that only an average calibration curve may be obtained
 - Probe drift during extended immersions in trapping solution
 - Long immersions in solutions with a fixed [S⁼] show drift versus time
 - Accuracy of sulfide ion concentration in solutions used for standardization
 - Na₂S and Na₂S•9H₂O typically used to prepare standard solutions may contain large percentages of excess water and even sodium sulfate
 - Calibration standards prepared using calculation of initial [S⁼] based on weight is not acceptable
 - H₂S delivery to experiment must be optimized to prevent adsorptive losses





probe slope

Time (min)

600

800

1000

EMF of 10 $^{\text{-5}}$ M Na \sp{S} measured using standard

400

-0.68

-0.7

0

200

-0.71306 V

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Experimental Evidence



neat buffer solution.



Knowing the origin of these errors, new analytical H₂S techniques have been developed using selective ion probe techniques.





Precise measurement of time and flow rate and [S⁼] using ion probe titration methods permits calculation of concentration of trace H_2S in gases, crossover rates, surface area probe, etc.

Experimental verification of [S⁼] calculation using [Pb⁺²] titration

- Use of Pb(NO₃)₂ at a concentration 10x of anticipated [S⁼] may be titrated using the ion probe as an endpoint indicator.
- The first application was to accurately measure the true Na₂S concentration being used as stock standard for probe calibration.
- TGA analysis of Na₂S "anhydrous" from Alfa contained
 - 4 wt% H₂O

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- 19 wt% Na₂SO₄
- Possibility of inert substances?
- [S⁼] was measured by ISE probe titration using [Pb⁺²] of 3.089e⁻²M
 - Theoretical [S⁼] correcting mass of Na₂S for water and sulfate content :

2.02e⁻³M

Using titration curve data (right) :

2.00e⁻³ ± 4.24e⁻⁵ M

Error reflects error in volume measurement and TGA analysis of lead salt.



XRF is being used to corroborate titrations of μM or lower solutions



Titrated solutions may be analyzed for PbS precipitate.

The presence of Pb on trapped in filter paper confirms the presence of S.

Technical Accomplishments Summary

- Completed DOE Round Robin Testing
- Developed a Data Reporting Format
 - Accepted by ISO TC197 Working Group 12
 - Proposed for adoption as part of standard
- Developed analytical method for measuring and determining ppb levels of sulfur
- Tested critical constituents (NH₃, CO, and H₂S)



Future Work

- Complete final report on DOE Round Robin Testing
- Finalize the Data Reporting Format
 - Awaiting input from Japan, Europe, and Korea
- Optimize our analytical method and modify it for the other critical constituents
- Continue testing the critical constituents (NH₃, CO, and H₂S) and populating the test matrix
- Continue providing data sets and interacting with FC modelers

