



DOE Hydrogen Program

# Protic Salt Polymer Membranes:

## High-Temperature Water-Free Proton-Conducting Membranes

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**Organization: Arizona State University**

in collaboration with

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University of Akron

**Date: Tue, May 19, 2009**

**Time: 11:30 am**

**Project ID**

**fc\_06\_gervasio**

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# Overview

## Timeline

- January 15, 2006
- January 14, 2011
  - go/no go end of year 3
  - March 2009
- 60% completed

## Barriers

- Barriers addressed by this project from the HFCIT Program Multi-Year Program Plan
  - (A) Durability
  - (C) Electrode Performance

## Budget

- Total project funding \$1,500K
  - DOE: 80%, Contractor: 20%
- Funding received in FY06
  - \$300,000
- Funding for FY07
  - \$300,000
- Funding for FY08
  - \$300,000

## Partners

- Arizona State University (lead)
- University of Akron (sub-contractor)
- Boeing
  
- DOE Technology Development Manager: Donna Lee Ho
- DOE Project Officer: Greg Kleen
- ANL Technical Advisor: Thomas Benjamin

# Relevance

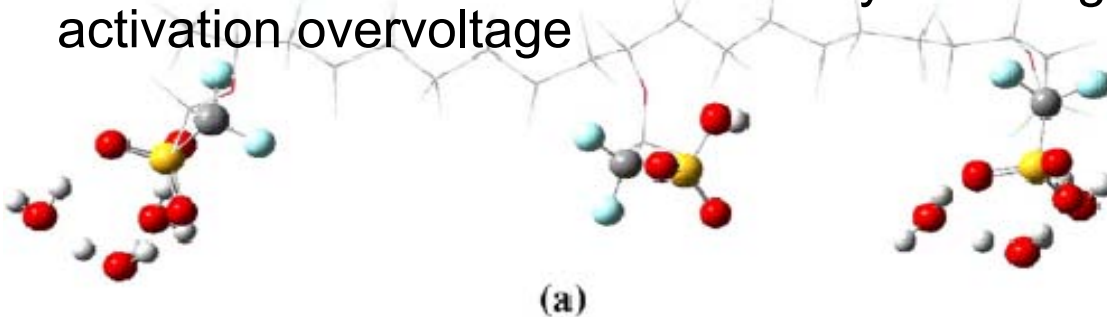
## OBJECTIVE:

To make a solid water-insoluble anhydrous proton-conducting electrolyte membrane that has good

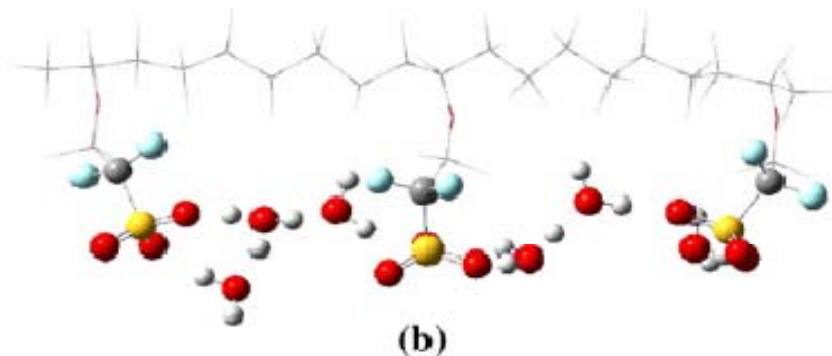
o *DURABILITY* by virtue of having

- proton conductivity that surpasses the 2009 target of  $> 0.1$  S/cm at  $120^{\circ}\text{C}$  and 50% RH
- effectively having no co-transport of molecular species with proton
- good mechanical strength and chemical stability

o *ELECTRODE PERFORMANCE* by assisting catalyst to promote reduced activation overvoltage



**a) Non-conducting  
Low water form**



**b) Conducting  
High water form**

The water solvated acid membrane only conducts proton under conditions (b) pendant acid and waters are in contact with adjacent units

# Relevance

## Benefits

High conductivity and Lower activation overvoltage lead to higher efficiency

No co-transport of water and higher temperature operation lead to elimination of bulky humidifier and radiator

# Approach

## SYNTHESIS OF “DRY” PROTON ELECTROLYTE MEMBRANES (PEMs)

- PEMs are being made based on “solvent free” liquid salts called *protic ionic liquid (pIL) concepts*.
- *pILs* can be *used to model membranes* (stability, conductivity).
- *Acid and base moieties* are *varied* to optimize electrolyte properties.
- *Polymers* are *varied* to optimize membrane solubility for water insoluble membranes with a high density (low EW) of covalently and electrostatically bound non-leachable ions.

## CHARACTERIZATION

- Proton conductivity characterized by electrochemical impedance spectroscopy (EIS) from -20 to 120°C
- Thermal oxidative stability of electrolytes measured by Thermal Gravimetry (TGA) from -20 to 120°C
- Electrochemical stability and electrode polarization surveyed by cyclic voltammetry on Pt
- Fuel cell performance/stability estimated by steady state I/V curves
- The mechanism of transport of protons, anions, and molecules investigated 3 NMR methods:
  1. pulse field gradient NMR to determine the diffusivity of ions,
  2. multipulse solid state NMR to measure the molecular motion and interactions of species in membranes,
  3. MRI while passing current to measure time-dependent distribution of species during proton conduction.

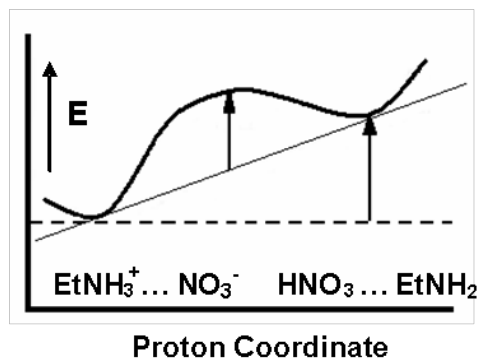
# Approach/Milestones

Month/Year	Milestone for Go/No-Go Decision
Jan-09	<p>Milestone: 2 kinds of high temperature proton-conducting protic salts membranes were made into MEAs and tested in fuel cells:</p> <ul style="list-style-type: none"><li>(i) membranes filled with leachable protic ionic liquids and</li><li>(ii) membranes with non-leachable salt moieties</li></ul> <p>Determine conductivity of membrane at 0 to 50% RH and the full range of temperature (-40 to 120°C) and compare to target of 0.1 S/cm . Determine conductivity in absence of water and other free solvents.</p>
Feb-09	<p>Milestone: Complete initial round of MEA fabrication and testing with selected new polymers (4 sent to Bekktech for evaluation and 2 more in progress) for external validation on the membrane conductivity at various temperatures and RH conditions.</p>
Feb-09	<ul style="list-style-type: none"><li>• A neat indium tin phosphate (ITP) membrane was made that has conductivity 0.16 S/cm from 25°C to greater than 120°C and 0% RH.</li><li>• Crossover eliminated by blending 70 wt% ITP with 30 wt% of a proton conducting organic polymer, PVPP, but at a cost of reduced conductivity.</li></ul>

# PROTIC IONIC LIQUID (pIL) CONCEPTS

□ pILs belong to a new class of solvent-free proton-conducting electrolyte that can function at very high temperatures

□ A protic ionic liquid (pIL) is made by transferring a proton from an acid to a base.



**Energy Diagram for the EAN (ethyl ammonium nitrate) pIL with:**

- proton transferred (Left)
- not transferred (Right),

	Occupied	Vacant	pK <sub>a</sub>	E (eV)
Acid Electrolytes	HSbF <sub>6</sub>	SbF <sub>6</sub> <sup>-</sup>		
	HTf	Tf <sup>-</sup>	-14	0.83
	HSO <sub>3</sub> F	SO <sub>3</sub> F <sup>-</sup>		
	HClO <sub>4</sub>	ClO <sub>4</sub> <sup>-</sup>	-10	
	H <sub>2</sub> SO <sub>4</sub>	HSO <sub>4</sub> <sup>-</sup>		
	HPO <sub>2</sub> F <sub>2</sub>	PO <sub>2</sub> F <sub>2</sub> <sup>-</sup>		
	HNO <sub>3</sub>	NO <sub>3</sub> <sup>-</sup>		
	CH <sub>3</sub> SO <sub>3</sub> H	CH <sub>3</sub> SO <sub>3</sub> <sup>-</sup>		
	CF <sub>3</sub> COOH	CF <sub>3</sub> COO <sup>-</sup>		
	H <sub>3</sub> O <sup>+</sup>	H <sub>2</sub> O	0	0
Neutral Electrolytes	HF	F <sup>-</sup>		
	HIm <sup>+</sup>	Im		
	EtNH <sub>3</sub> <sup>+</sup>	EtNH <sub>2</sub>		
Basic Electrolytes	H <sub>2</sub> O	OH <sup>-</sup>	14	-0.83
	NH <sub>3</sub>	NH <sub>2</sub> <sup>-</sup>		
	OH <sup>-</sup>	O <sub>2</sub> <sup>-</sup>	28	

EAN  
Δpk = 14

**Gurney proton energy level diagram.**  
For any pair of levels, the stable entities are upper right and lower left.

# Plan & Progress

60% complete

- ☐ **Task 1: pIL Design and Testing**
  - mixed acid and base moieties as electrolyte
  - models for high temp (120°C) membrane

30% complete

- ☐ **Task 4: Proton Conduction by NMR**
  - 4.1 Pulsed field gradient NMR
  - 4.2 Electrochemical NMR (eNMR)
  - 4.3 eNMR Hittorf

50% complete

- ☐ **Task 2: Proton Conducting Membranes**
  - 2.1.1 - Porous support with a pIL
  - 2.1.2 - pIL swollen in polymers
  - 2.2 - Immobilized pIL polymer

75% complete

- ☐ **Task 5: Iterate Synthesis**
  - to optimize stability, conductivity

50% complete

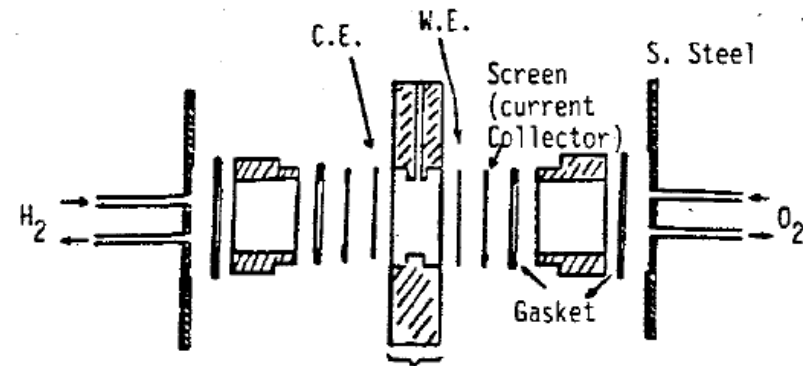
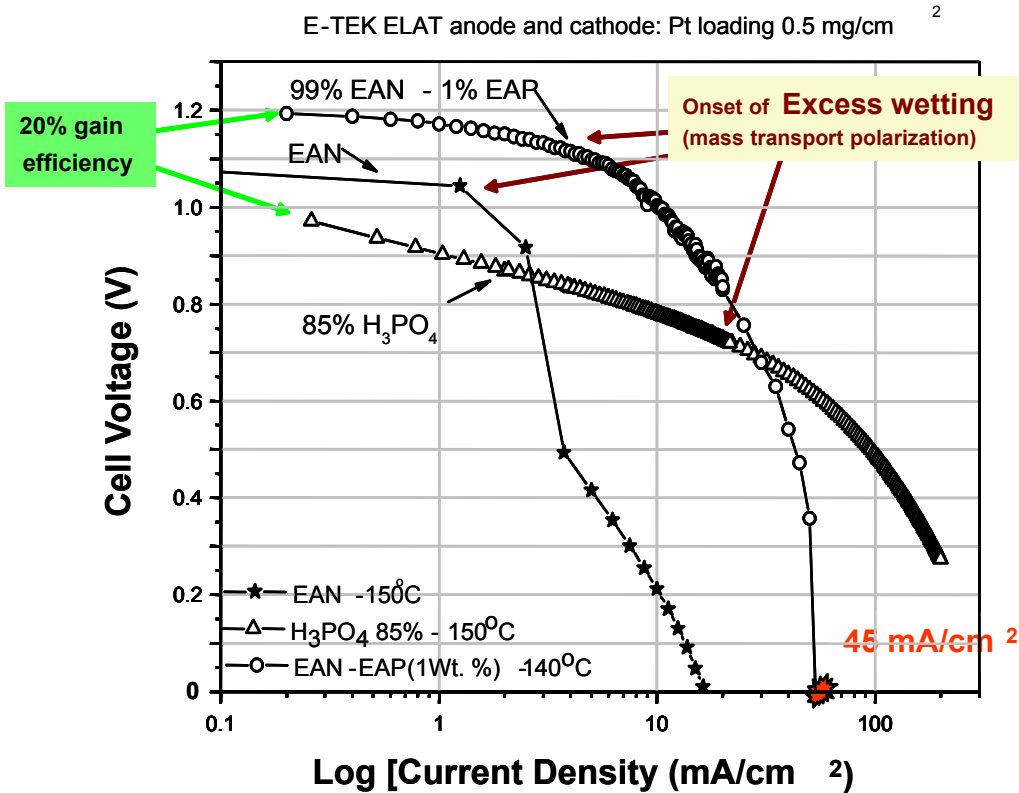
- ☐ **Task 3: Temp Dependence of Electrolyte**
  - 3.1 Conductivity, and durability of electrolytes
    - at T = 120°C, 100°C, 80°C, 20°C and -20°

60% complete

- ☐ **Task 6: Membrane Demonstration**
  - ASU sent 4 membranes to CFU
  - 2 more in preparation



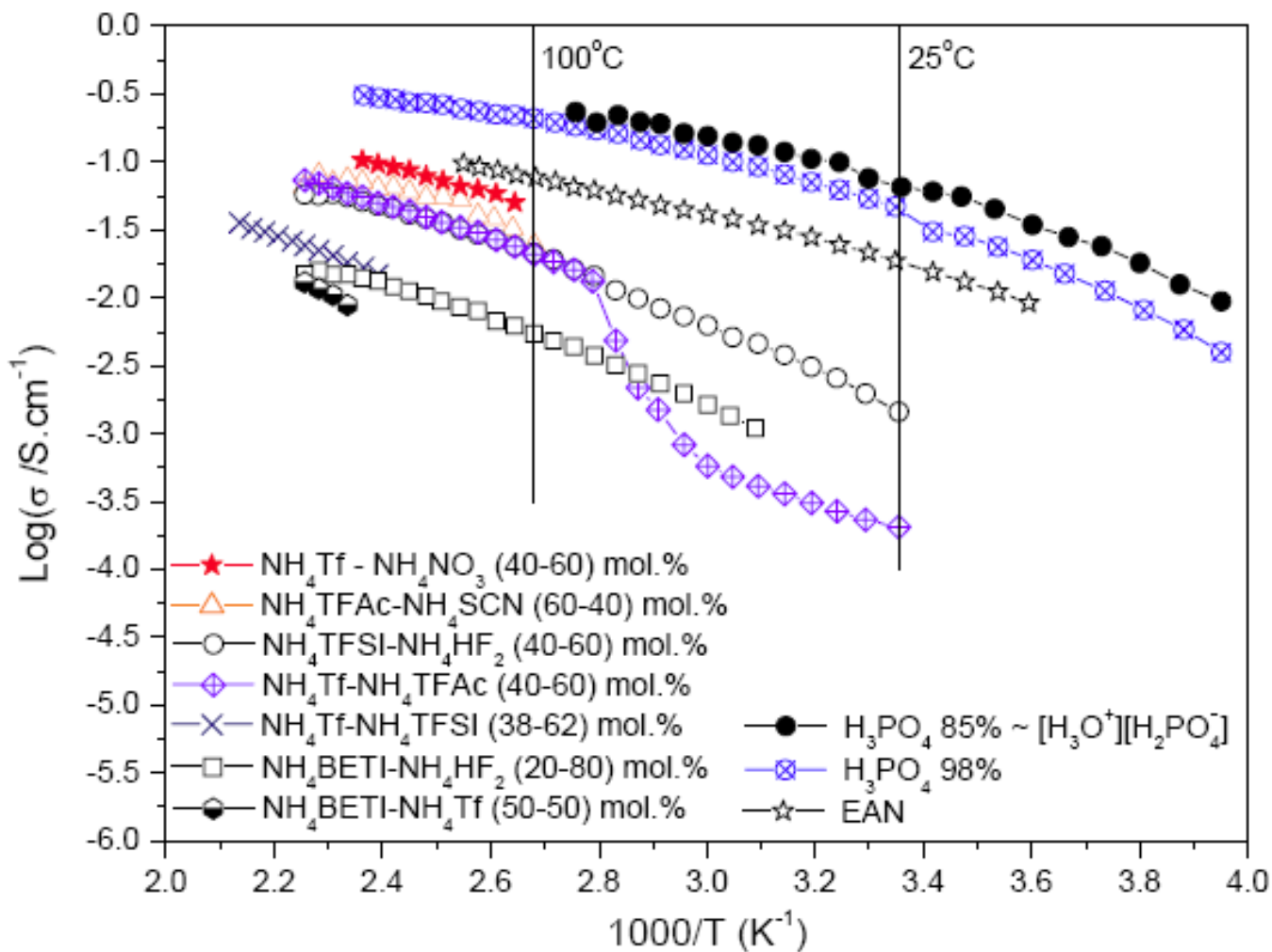
# Technical Accomplishments FY08: Fuel Cell with pL and gas fed Porous Electrode



Liquid Electrolyte Cell

- Fuel cells with protic salts still show better performance than with 85% H<sub>3</sub>PO<sub>4</sub>
- **New material goal, a more stable and non wetting electrolyte**

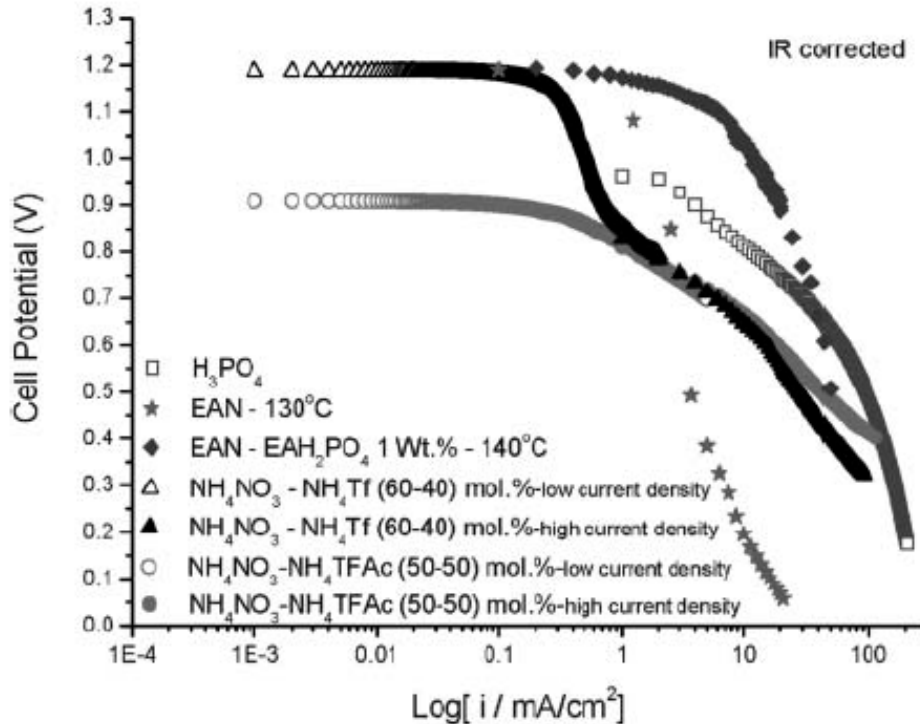
# Technical Accomplishments FY08: : Arrhenius plot of conductivity of ammonium salt mixtures



# Technical Accomplishments FY08: : Fuel Cells with New Stable PIL Electrolytes

binary ammonium salt mixtures:

- trifluoromethanesulfonate (triflate, Tf) + trifluoroacetate (TFAc),
- trifluoroacetate + nitrate,
- triflate + nitrate.



A Tafel plot, cell potential (V) versus log of current density, for a series of inorganic binary ammonium salts, an organic ammonium salt, and phosphoric acid. The plateau at low current density indicates barrier free electroreduction.

## Summary of recent results

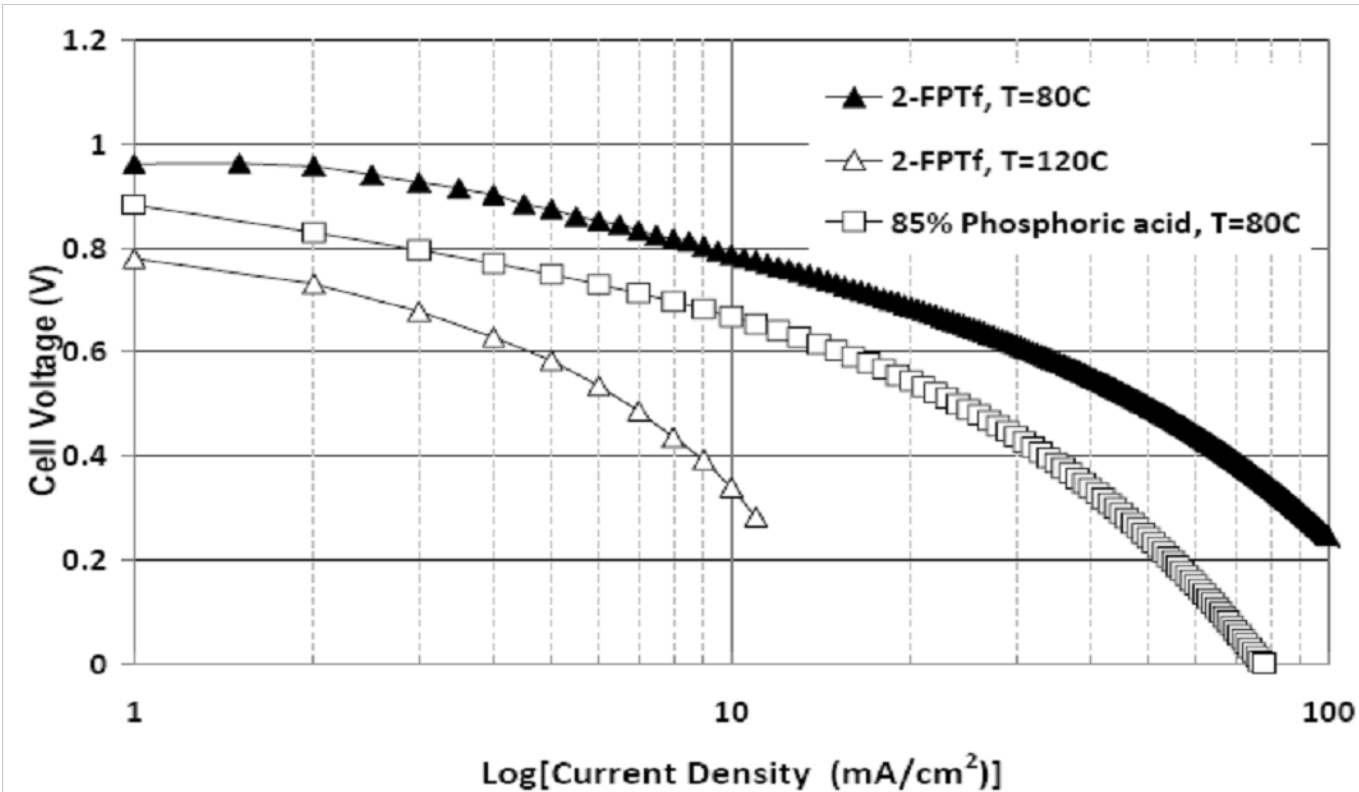
- \* New stable electrolyte found
- \* Tafel plots of the fuel cell data for ionic liquids indicate barrier free O<sub>2</sub> reduction at low currents probably due to the low water activity of the salts.
- \* The inorganic ammonium salts exhibit more polarization at intermediate loads, probably due to adsorption but remain stable through higher cell loads.
- \* Beyond the potential enhancement performance of an ionic protic liquid, a non-hydrous electrolyte allows for a greater array of catalysts and electrodes to be considered for use in a proton exchange fuel cell.

## What's next?

- Further tailor mixtures with non – adsorbing components for higher performance
- Continue fuel cell test of membranes loaded with salt mixtures
- Make polymeric forms of salt mixtures

Data from: Binary inorganic salt mixtures as high conductivity liquid electrolytes for > 100°C fuel cells, Jean-Philippe Belieres, Don Gervasio and C. Austen Angell, *Chem. Commun.*, 2006, 4799.

# Technical Results: More Efficient and Stable Fuel Cell with an Electrochemically and Physically stable pIL, 2-FPTf



**STEADY STATE I/V curves** for H<sub>2</sub> and O<sub>2</sub> fed to Pt-catalyzed porous electrodes in 2-FPTf electrolyte at 80C and 120C and 85% phosphoric acid electrolyte at 80C.  $\sigma(2-FPTf) = 4 \times 10^{-3} \text{ Scm}^{-1}$  A = 0.5 cm<sup>2</sup>,  $t^{\text{electrolyte}} = 0.3 \text{ cm}$ .

**Why is fuel cell better with this salt electrolyte ??**

# Technical Results: Cyclic voltammogram of Pt surface in:

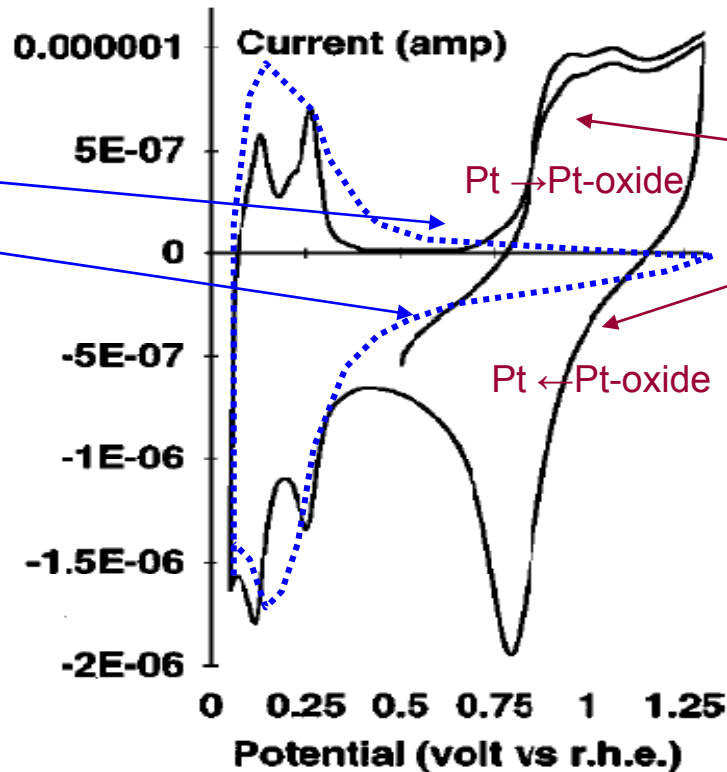
- **aqueous sulfuric acid electrolyte** (solid black line)
- **versus protic salt** (dotted blue line).

With protic salt electrolyte

There is

- no Pt-oxide formation
- nor reduction

to impede  $O_2$  reduction.



With aqueous electrolyte

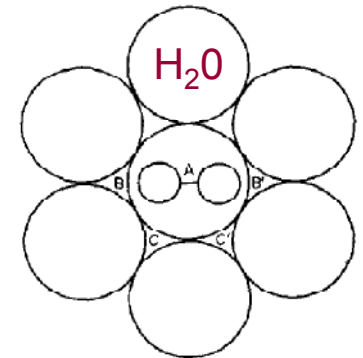
Pt-oxide formation



Pt-oxide reduction



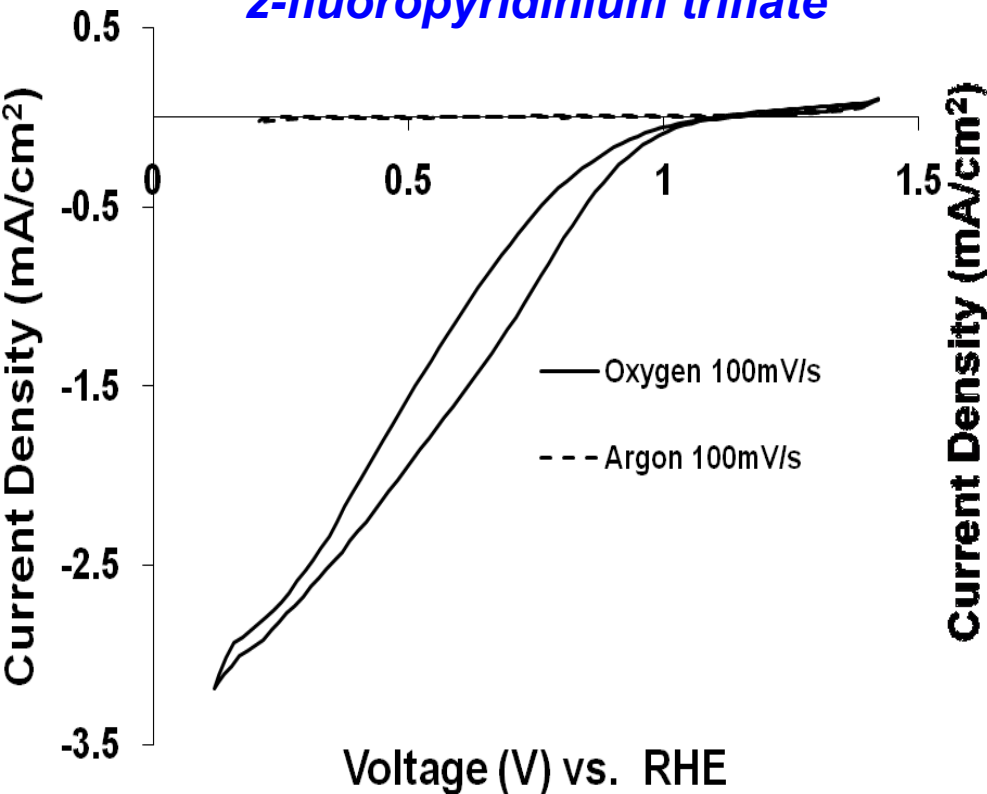
Pt-oxide impedes  $O_2$  reduction.



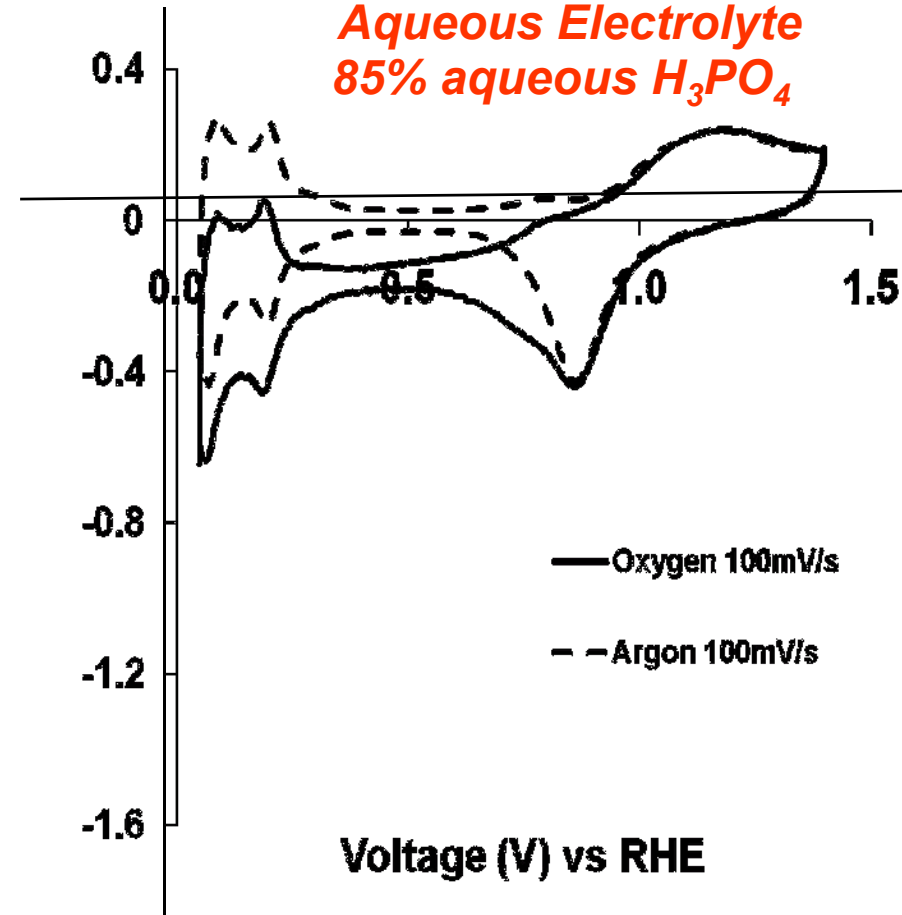
*Low water activity makes Pt a better cathode electrocatalyst*

# Technical Results: Voltammetry of Pt with Oxygen in:

**Salt Electrolyte**  
**2-fluoropyridinium triflate**



**Aqueous Electrolyte**  
**85% aqueous H<sub>3</sub>PO<sub>4</sub>**



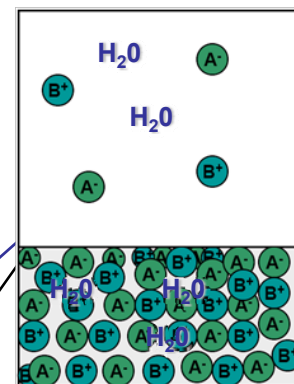
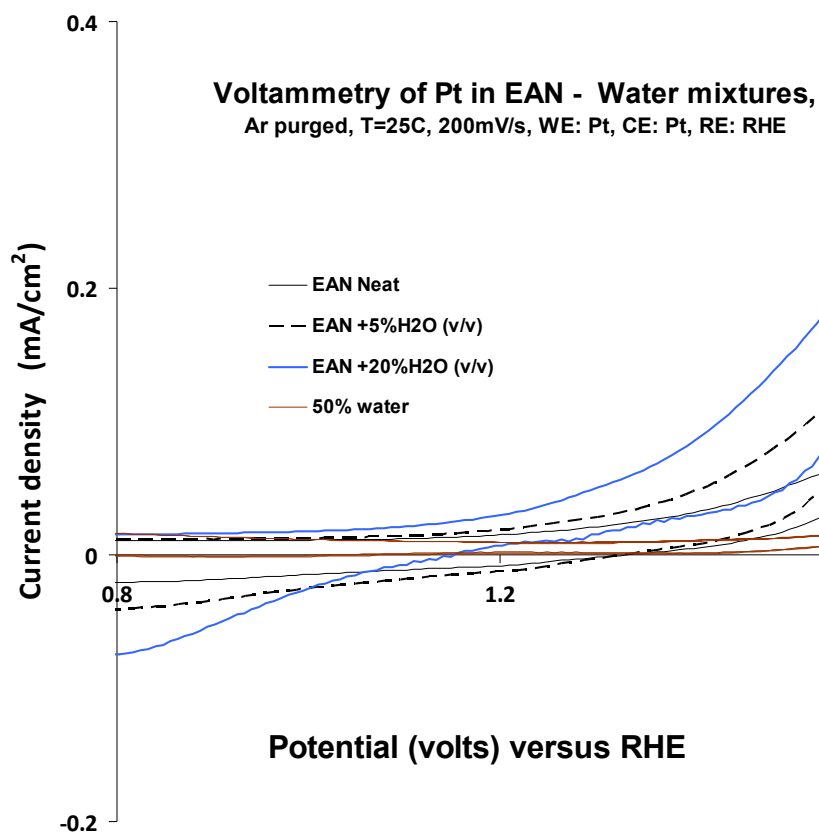
**Voltammetry of Pt in 2-fluoropyridinium triflate shows:**

- Stable after 100 cycles in presence of O<sub>2</sub>
- O<sub>2</sub> reduction starts near thermodynamic limit [1.18V at 80°C]
- Oxidation current at E>1.18V is not for electrolyte oxidation  
its for water oxidation to O<sub>2</sub>

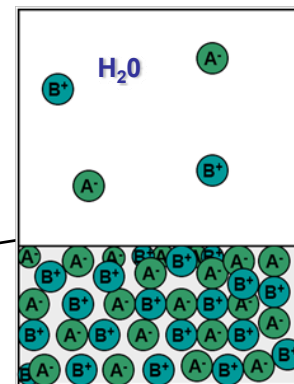
# Technical Results: Effects of Dispersed and Bulk Water

$H_2O$  = dispersed water

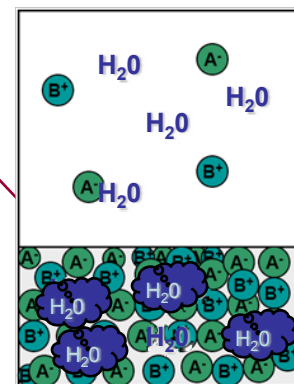
 = bulk water



5 to 20%  
Dispersed  
H<sub>2</sub>O in IL



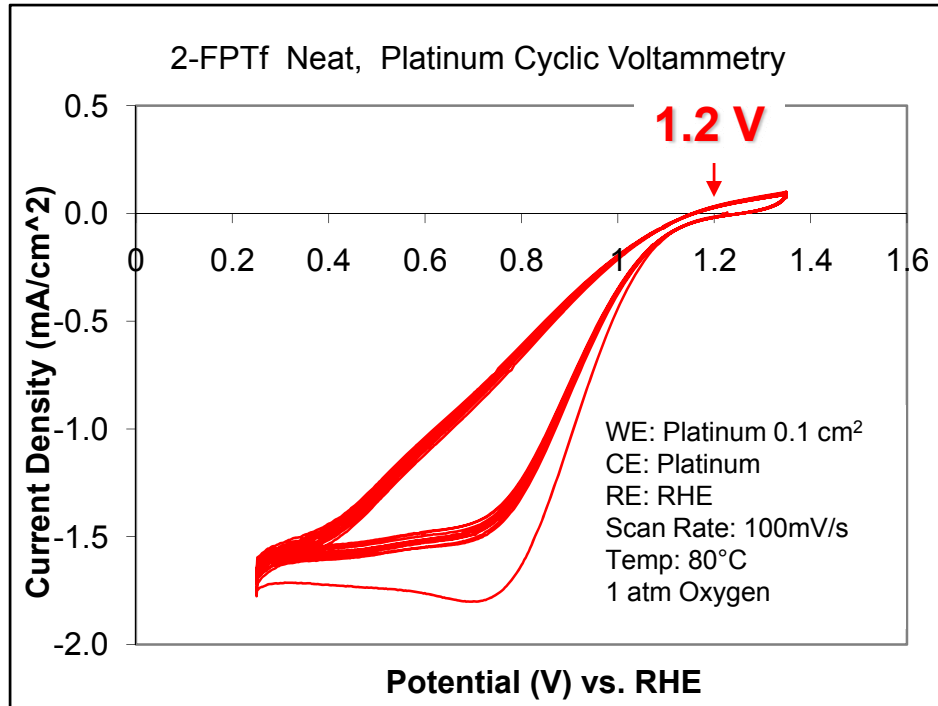
Trace H<sub>2</sub>O  
in Neat IL



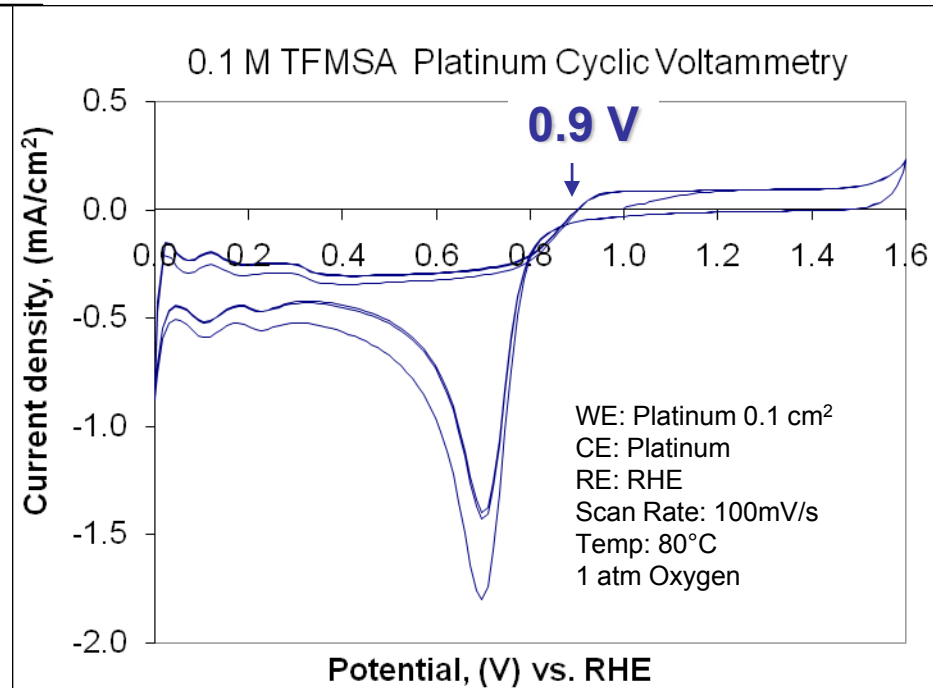
50% Dispersed  
and Bulk H<sub>2</sub>O  
in 50% IL

# Technical Results: Voltammetry of Pt in Fluorinated Ionic Liquid Electrolytes:

**without bulk water**



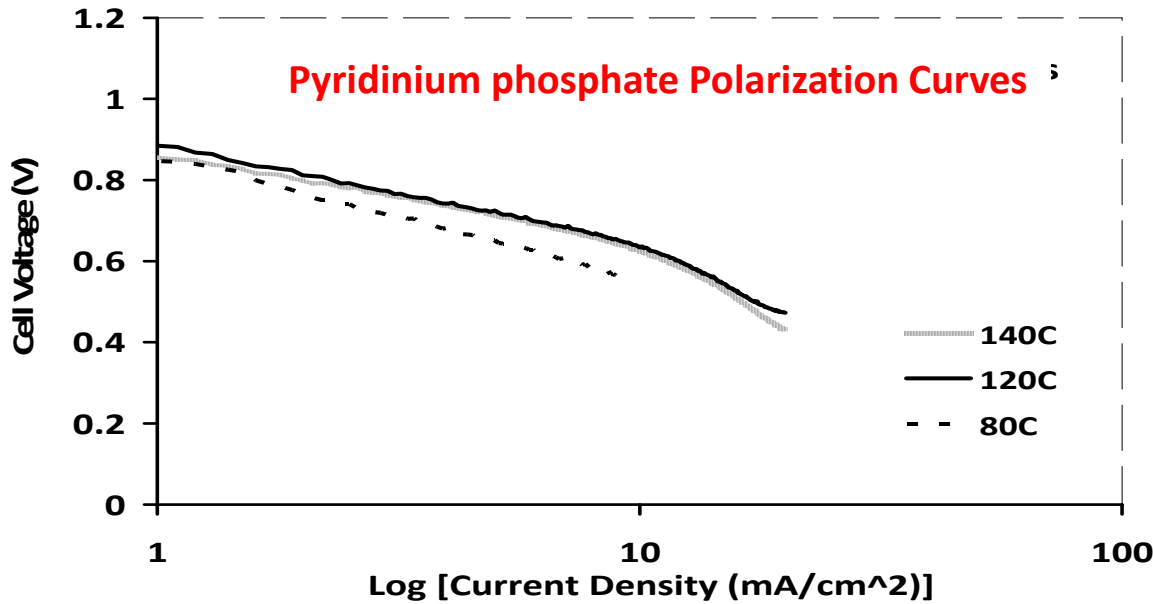
**with bulk water**



- Voltammetry of 2-Fluoropyridinium triflate shows that it is stable after 100 cycles.
- Oxygen reduction starts near the thermodynamic limit for ORR [1.18V at 80°C]



# Technical Results: hydrocarbon pIL vs fluorocarbon pIL

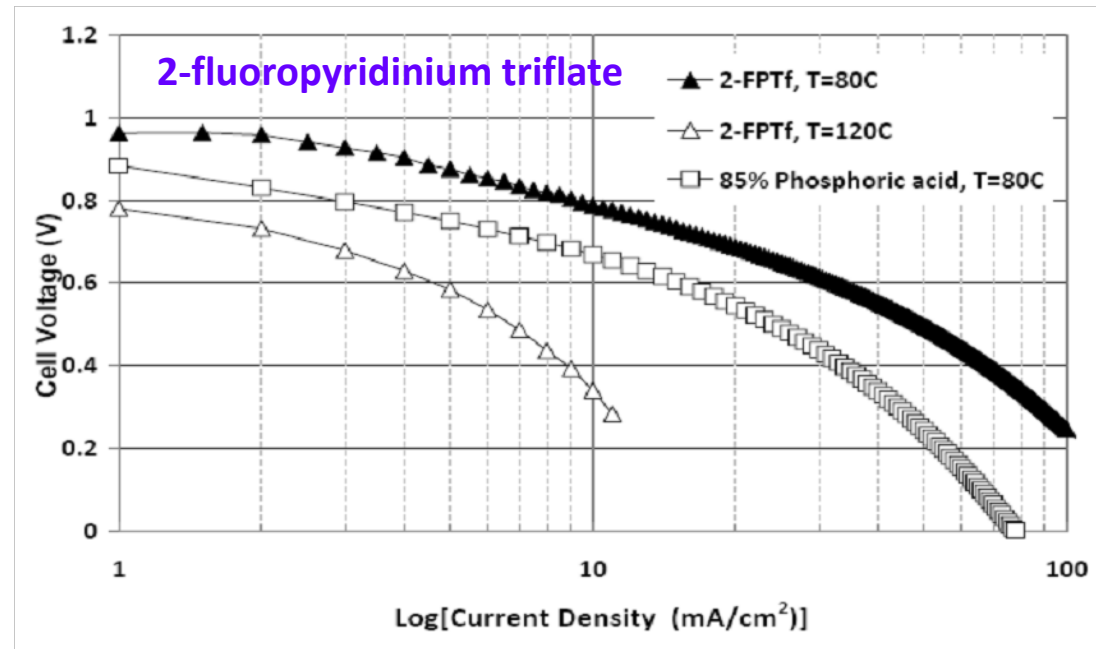


Hydrocarbon

- Stronger adsorbing
- Lower power

Fluorocarbon

- Weaker adsorbing
- Higher power



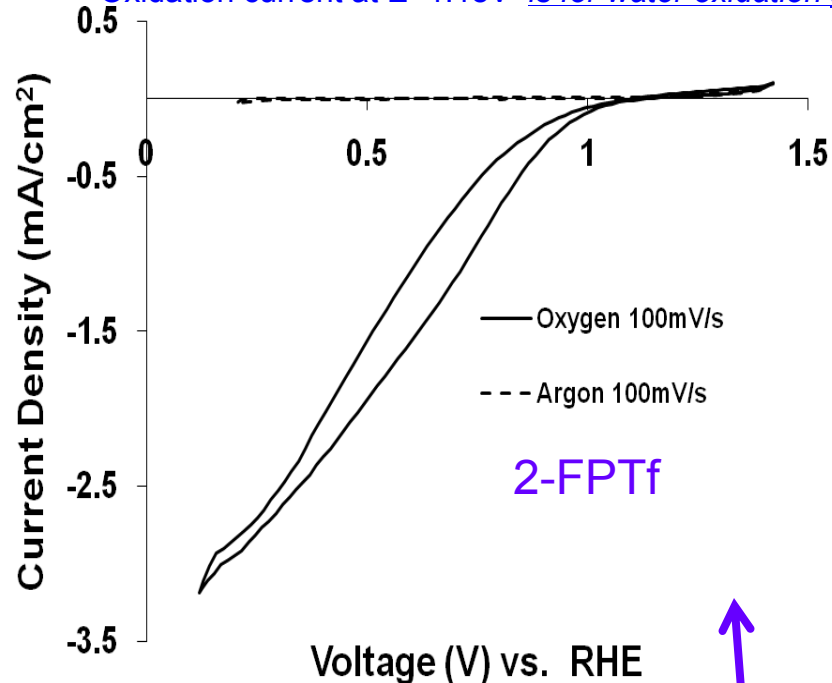
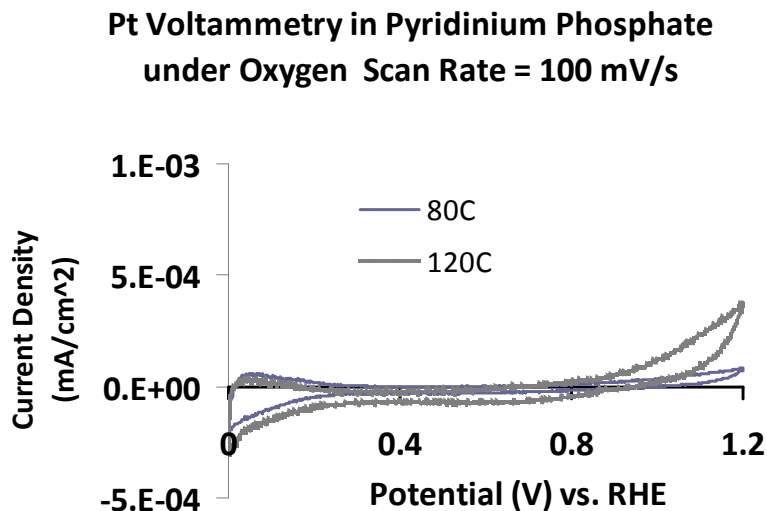
# Technical Results: Voltammetry of hydrocarbon and fluorocarbon Ionic Liquid Electrolytes

**Voltammetry of Pt in pyridinium phosphate shows:**

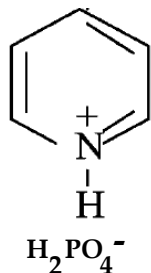
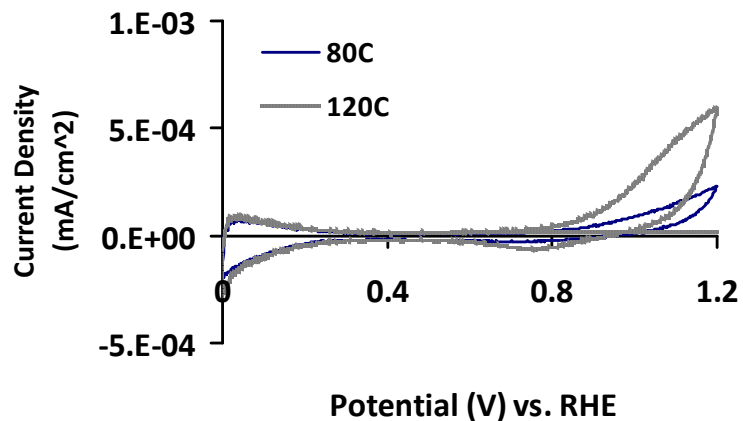
- Oxidatively unstable
- Lower O<sub>2</sub> reduction current

**Voltammetry of Pt in 2-fluoropyridium triflate shows:**

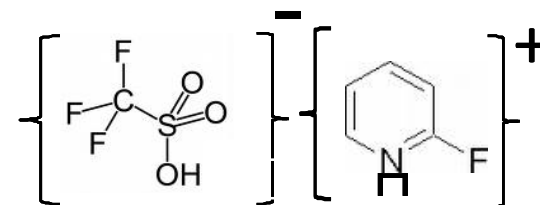
- Stable after 100 cycles in presence of O<sub>2</sub>
- O<sub>2</sub> reduction starts near thermodynamic limit [1.18V at 80°C]
- Oxidation current at E > 1.18V *is for water oxidation to O<sub>2</sub>*



**Pt Voltammetry in Pyridinium Phosphate under Nitrogen Scan Rate = 100 mV/s**



Pyridinium Phosphate



2-Fluoropyridinium triflate

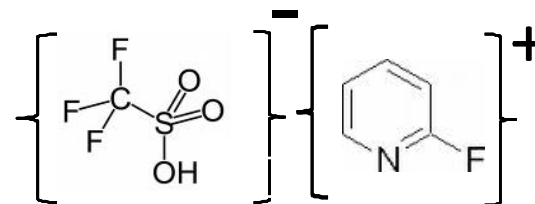
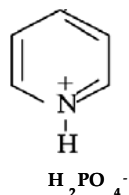
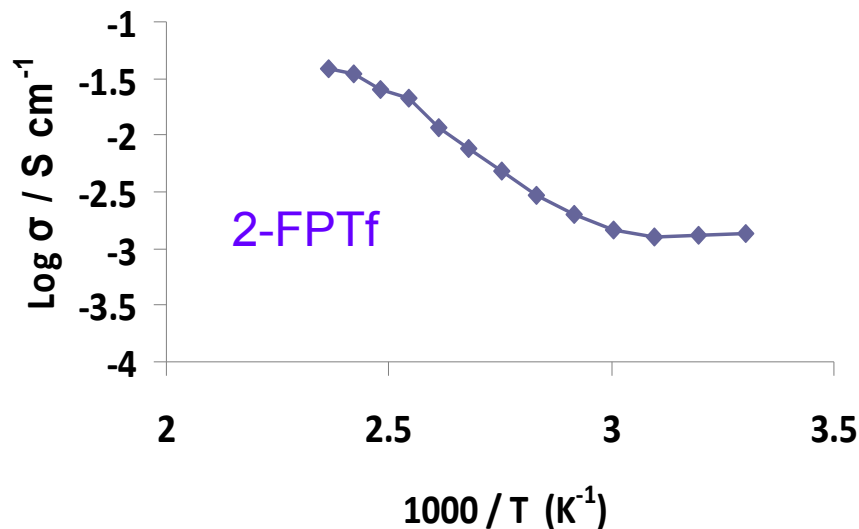
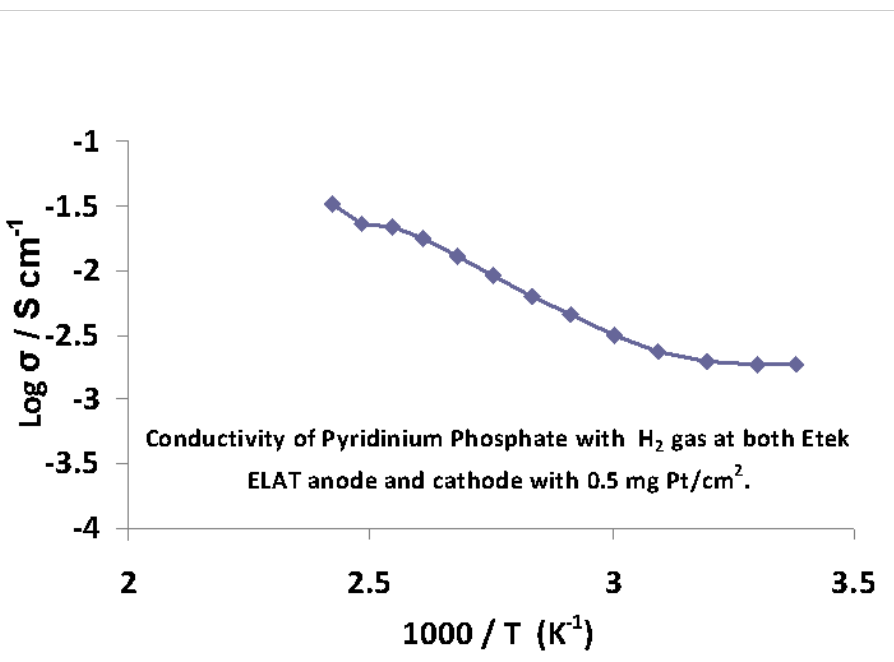
# Technical Results:

## Conductivity of Liquid hydrocarbon vs fluorcarbon pIL

as a function of temperature, dry H<sub>2</sub> gas fed to ETEK ELAT Pt anode and cathode

Liquid hydrocarbon pIL  
pyridinium phosphate (PP)

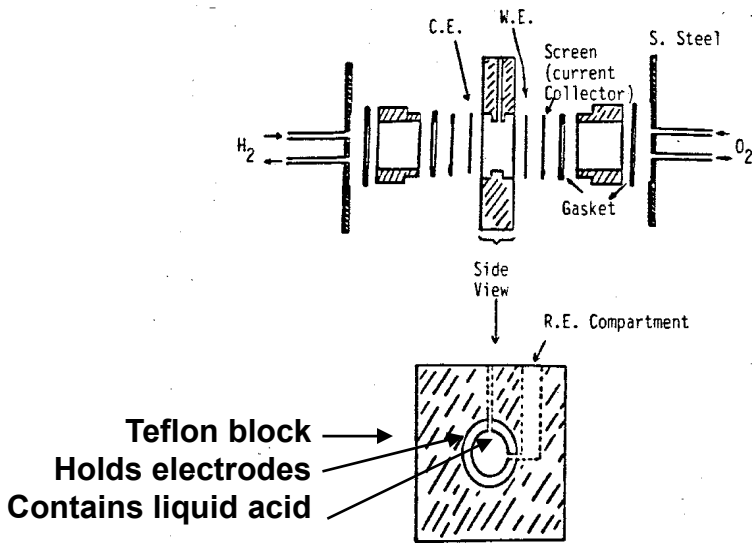
Liquid fluorocarbon  
Fluoropyridinium triflate 2-FPTf



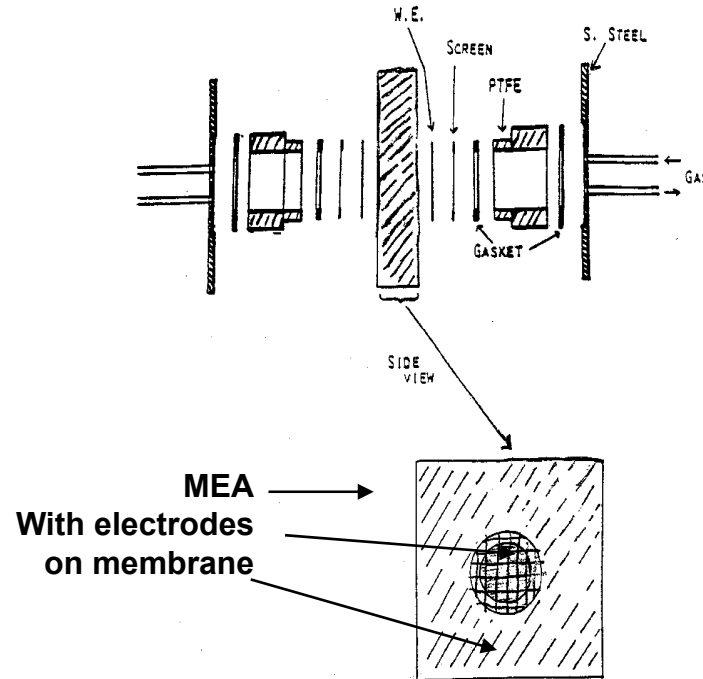
# Technical Accomplishments:

a stable & conductive membrane with immobilized ions in membrane

## Schematic Diagram of Liquid vs Solid PEM Fuel Cell



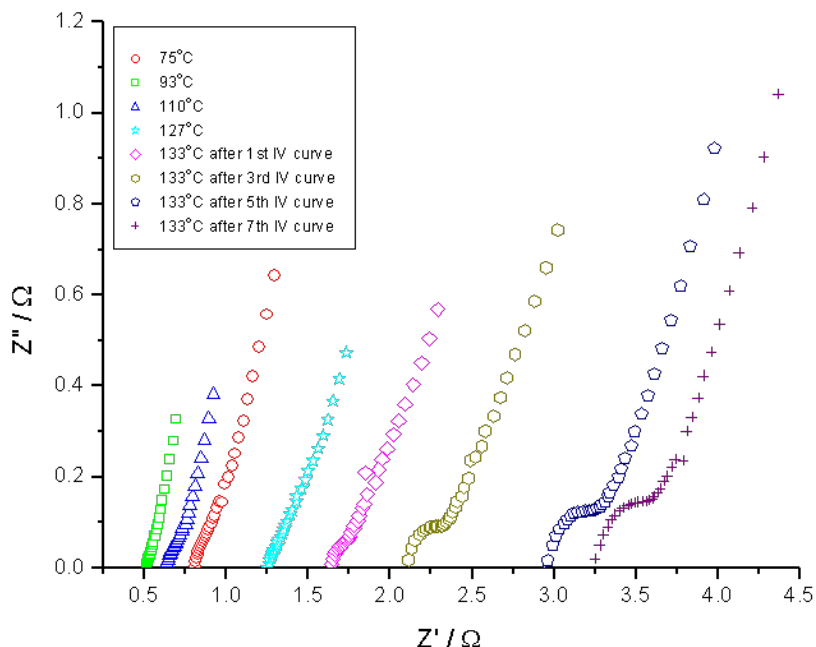
micro fuel cell with **liquid electrolyte**,  
like phosphoric acid.



micro fuel cell with **PEM electrolyte**,  
like Nafion®.

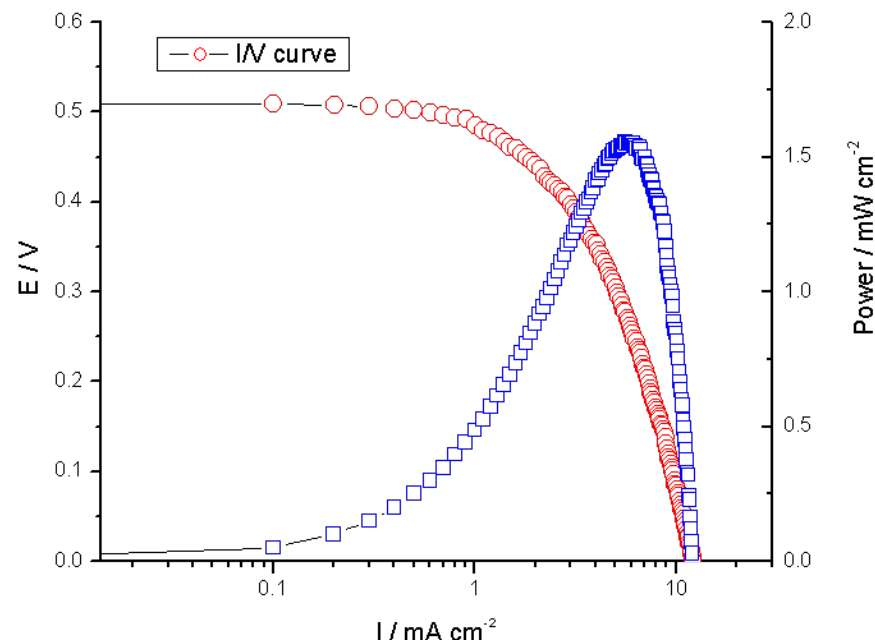
# FY08: Technical Accomplishments: non-leachable PEM 1

## EIS for H<sup>+</sup> conductivity



## Fuel Cell I/V Curve

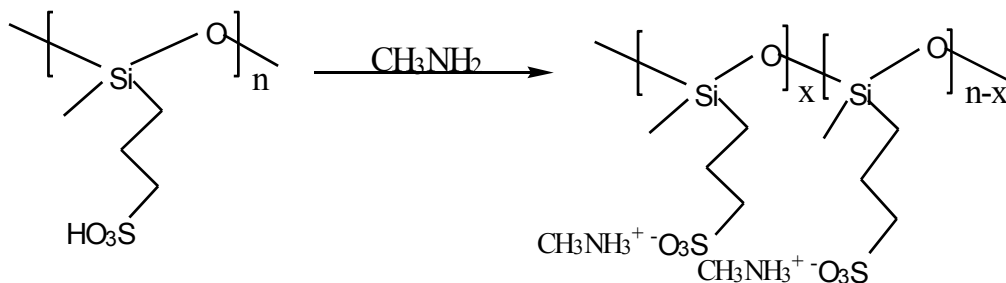
I/V curve and power for the fuel cell based on anodisc imbibed with polysiloxane with pendant sulfonic acid that neutralized by methylamine. Fuel cell runs at 127°C



Impedance and polarization curves for “dry” non leachable membranes consisting of an Anodisc (Whatman alumina membrane,  $t = 60$  micron, pore diameter = 100 micron) filled with solid polysiloxane with pendant sulfonic acid that fully neutralized with methylamine

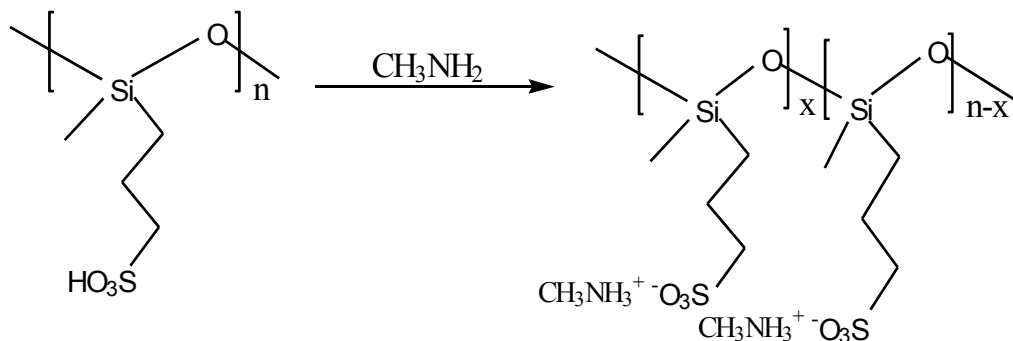
### Non-leachable

*Pendant sulfonic acid polymer fully neutralized with methylamine*

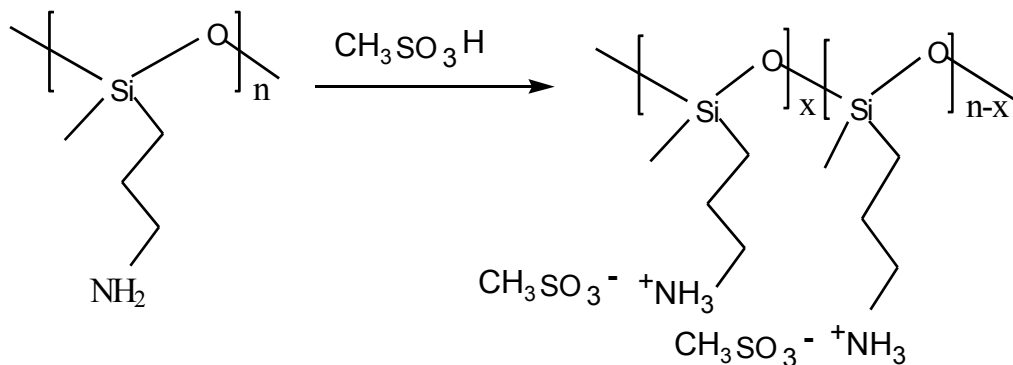


# Summary on non-leachable Siloxane-based PEMs

## Two non-leachable siloxane protic salt polymer membranes



### 1. Pendant sulfonic acid polymer fully neutralized with methyl amine



### 2. Pendant propyl amine polymer fully neutralized with methyl sulfonic acid

## Critique of non-leachable PEM

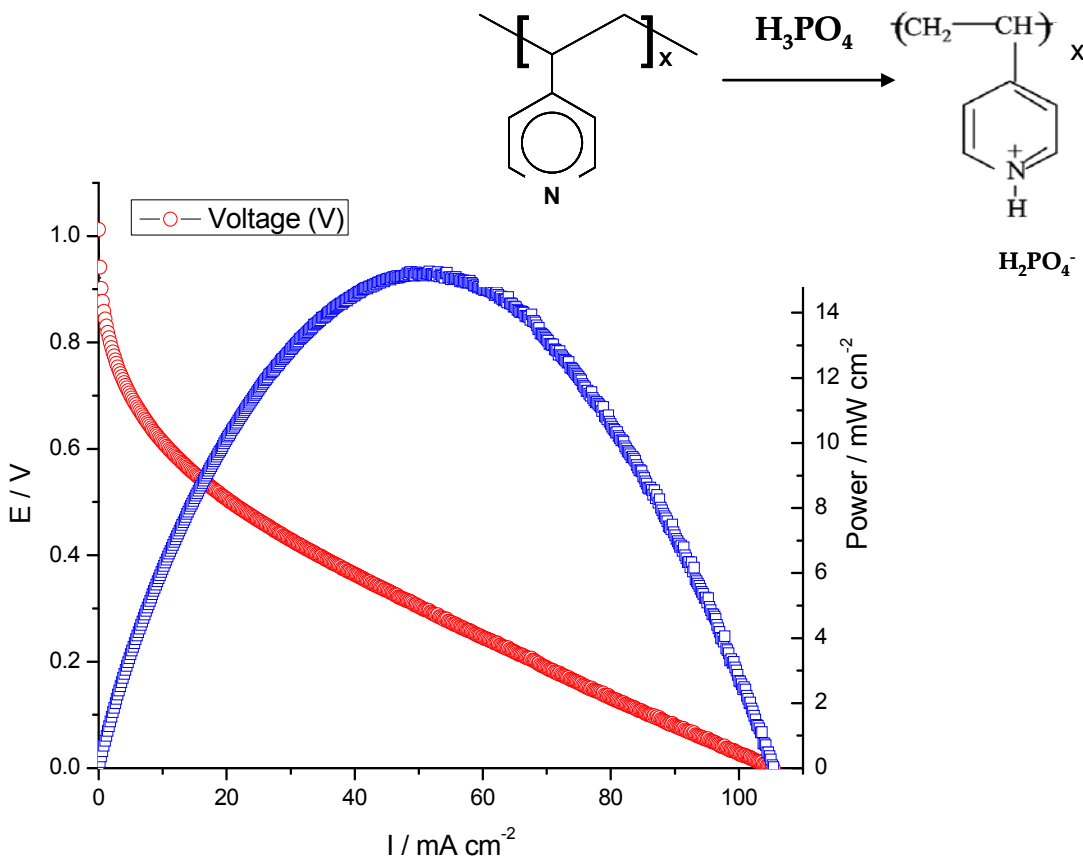
**Pro:** These data illustrate using a *protic-salt membrane* as a “dry” proton-conductor in a fuel cell membrane.

**Con:** siloxane membranes have limited physical stability (soft and water soluble) resulting in low performance (low open circuit voltage OCV, 0.45V, and low power, 2mW/cm<sup>2</sup>) in a fuel cell due to reactant crossover in this PEM.

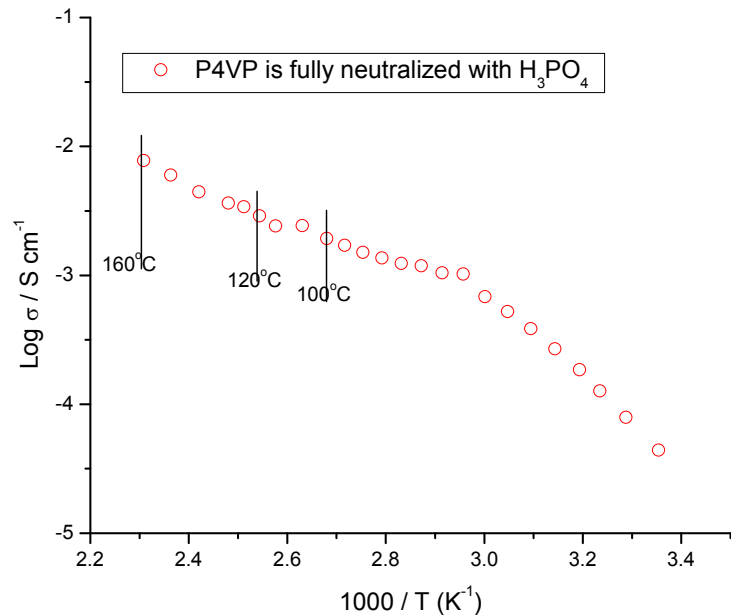
**What's next?**

# FY09: Technical Accomplishments: non-leachable PEM

## Poly Vinyl Pyridinium Phosphate (PVPP)



I/V curve for  $H_2/O_2$  fuel-cell with poly vinyl pyridine fully neutralized with phosphoric acid. Pt loading =  $0.5\ mg/cm^2$  E-Tek ELAT electrodes.  $\sigma = 0.005\ S/cm$ . Temp. =  $162^\circ C$ ;

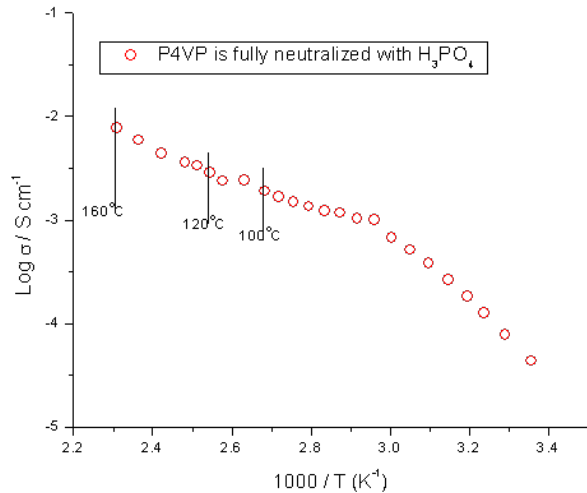


Conductivity of poly vinyl pyridine with 1  $H_3PO_4$  per 1 pyridine as a function of temperature.

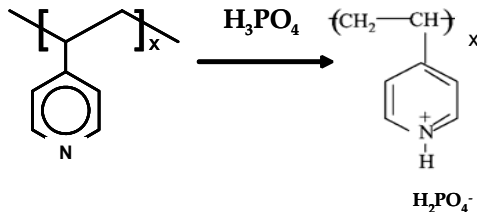
# FY09: Technical result: Liquid versus Solid Membrane of Pyridine Phosphate

Poly vinyl pyridine with 1 H<sub>3</sub>PO<sub>4</sub> per 1 pyridine

Solid Non-Leachable  
Membrane Electrolyte

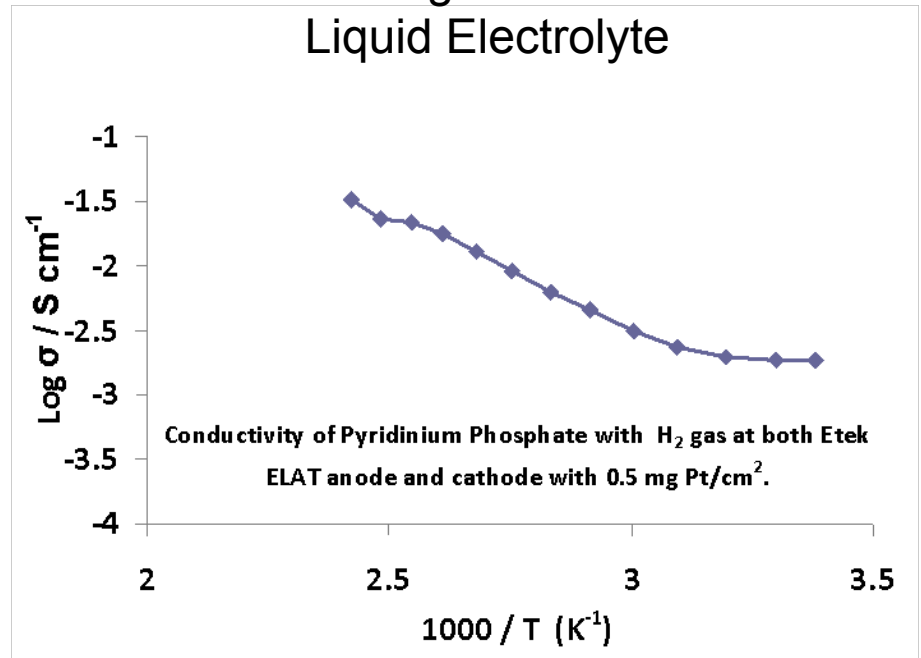


Conductivity of non-leachable solid poly vinyl pyridine with 1 H<sub>3</sub>PO<sub>4</sub> per 1 pyridine proton conducting PEM as a function of temperature.



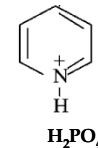
Liquid pyridinium phosphate

Analogous  
Liquid Electrolyte



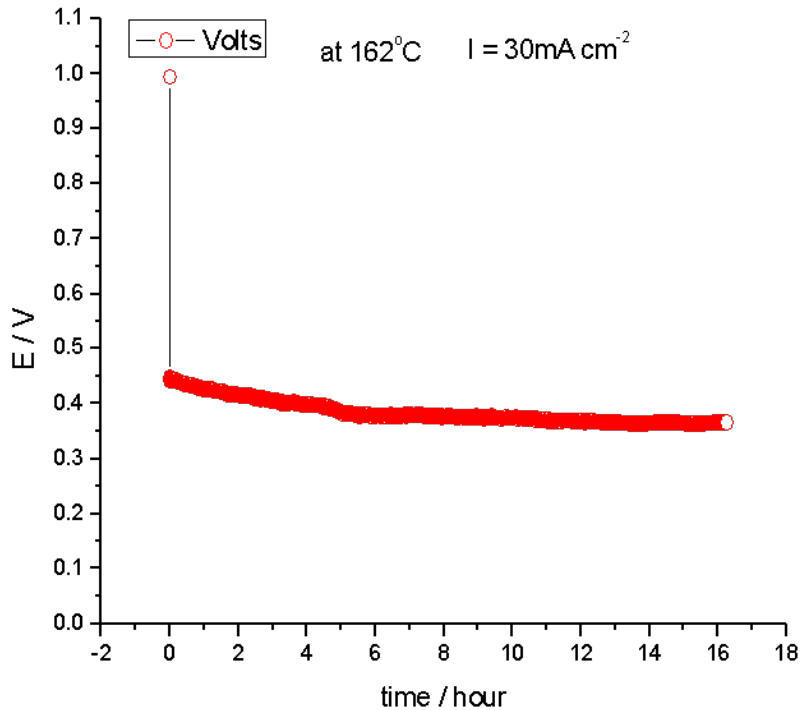
Conductivity of liquid pyridinium phosphate as a function of temperature, H<sub>2</sub> gas fed to both anode and cathode. Electrodes are E-tek ELAT with 0.5 mg Pt/cm<sup>2</sup>.

**SIMILAR !**





# Technical Result: Cell voltage in time at constant load for a H<sub>2</sub>/O<sub>2</sub> fuel-cell with a PVPP membrane



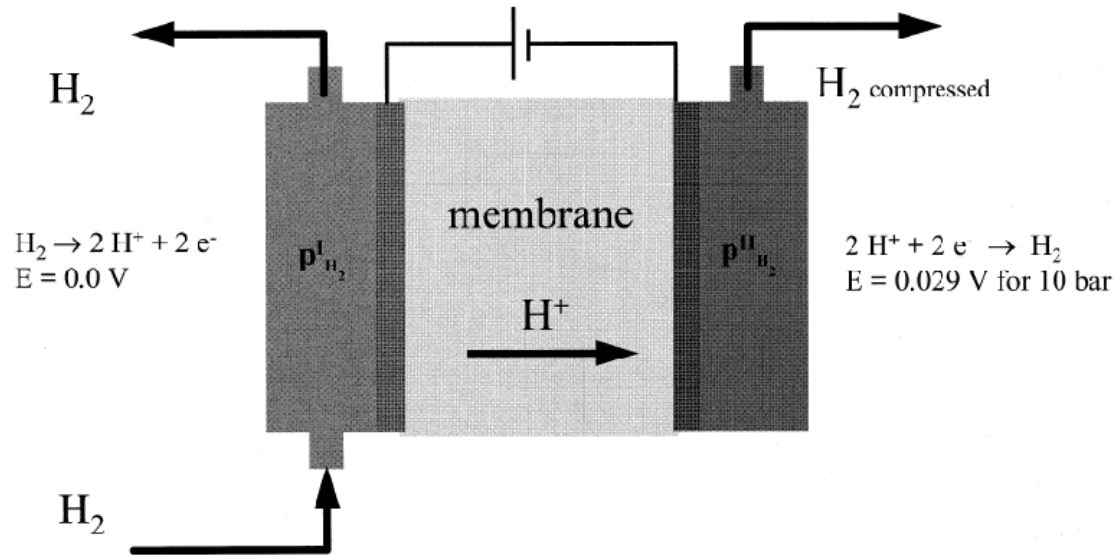
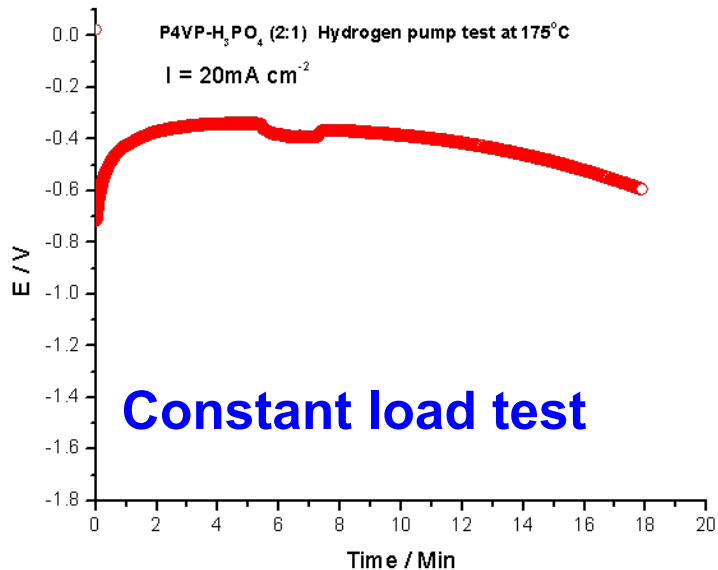
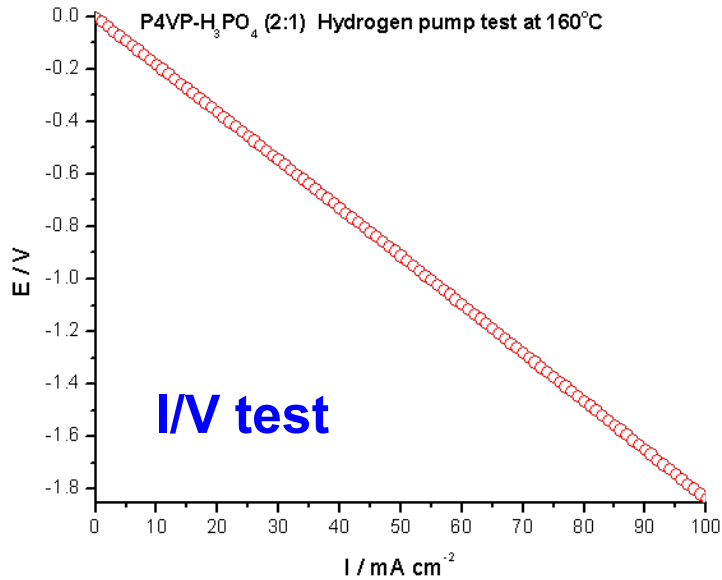
Cell voltage in time at constant load for a H<sub>2</sub>/O<sub>2</sub> fuel-cell with a membrane made of polyvinylpyridine in which each pyridine is reacted with phosphoric acid. Pt loading = 0.5 mg/cm<sup>2</sup> E-Tek ELAT electrodes. Load is 30 mA/cm<sup>2</sup>. Temperature = 162°C.

The cell was run overnight under constant load of 30 mA/cm<sup>2</sup>. After this overnight test, the polarization (I/V test) did not change.

***Overnight fuel cell stability while passing H<sup>+</sup> current***

***Strong evidence that the proton is hopping through this solid membrane*** that has no leachable ions or solvents.

# Technical Result: E-chem H-Pump with PVPP membrane



$$V = V_0 + \frac{RT}{2F} \ln \left[ \frac{p^{\text{II}}_{\text{H}_2}}{p^{\text{I}}_{\text{H}_2}} \right]:$$

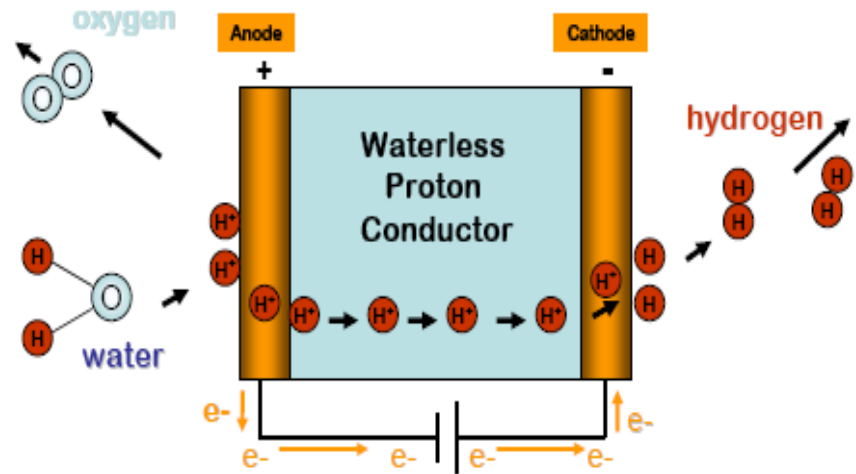
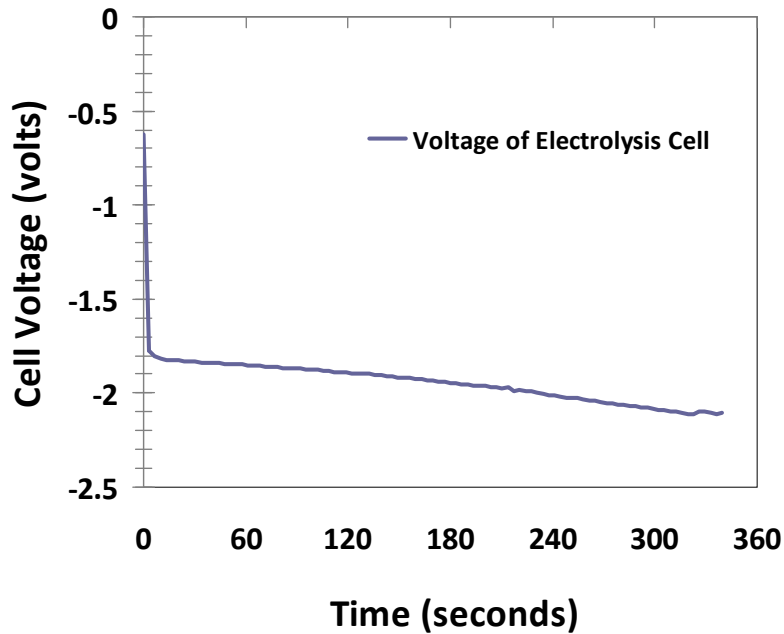
**Electrochemical H<sub>2</sub> pressurization**

Pt loading = 0.5 mg/cm<sup>2</sup> E-Tek ELAT electrodes.

**Proton is the only ion being conducted**

# Technical Result: Galvanostatic electrolysis of water on Pt in PVPP PEM cell

*PVPP membrane requires no water for H<sup>+</sup> conduction yet allows water electrolysis*



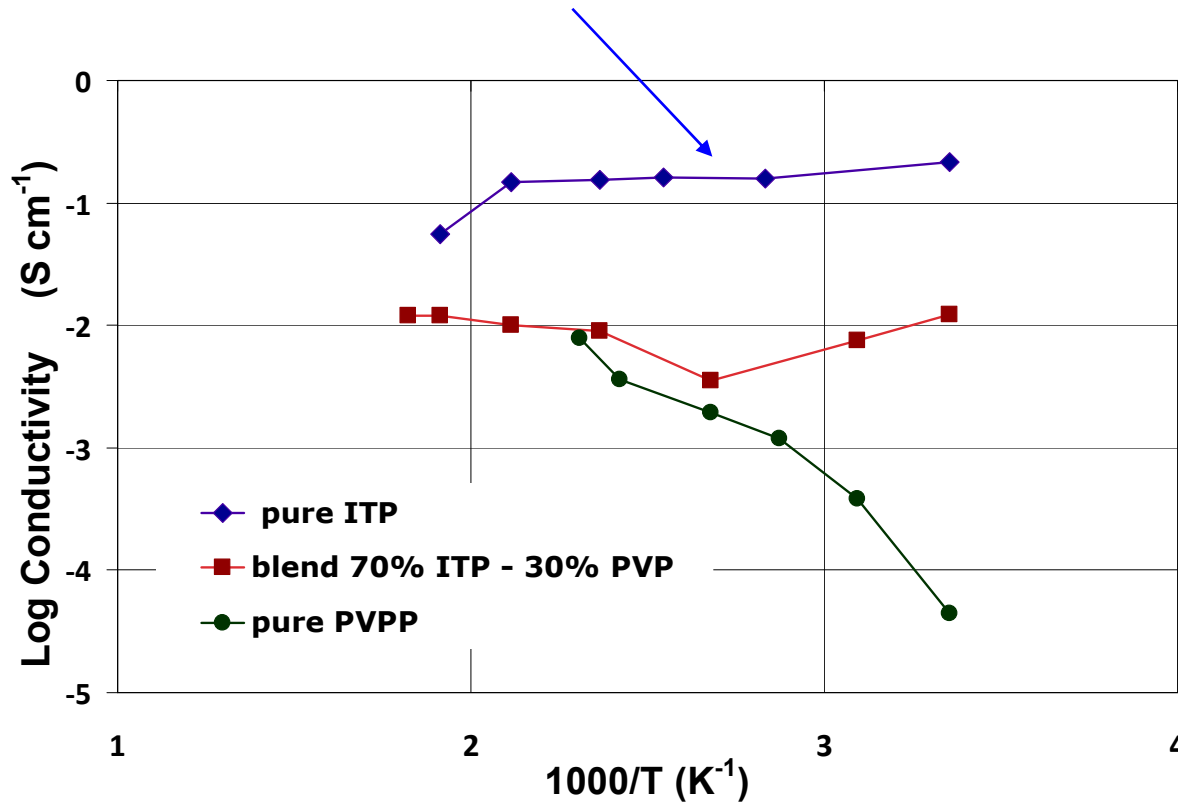
Cell voltage in time for the galvanostatic electrolysis of water on E-tek ELAT electrode with Pt loading of 0.5 mg/cm<sup>2</sup> used for anode and cathode with a solid electrolyte membrane (t=35 mil) of polyvinyl pyridinium phosphate (PV P<sup>+</sup>: H<sub>2</sub>PO<sub>4</sub><sup>-</sup>; 1:1). Constant cell load current = 11 mA/cm<sup>2</sup>, Cell Temperature = 150°C, Argon flow humidified at 80°C.

***Proton only conducted***

# Technical Result: Proton Conducting Membranes of Ceramic & Ceramic Organic Polymer Blend

Conductivity of neat ITP

**> 0.1 S/cm\*** from 25C to 200C



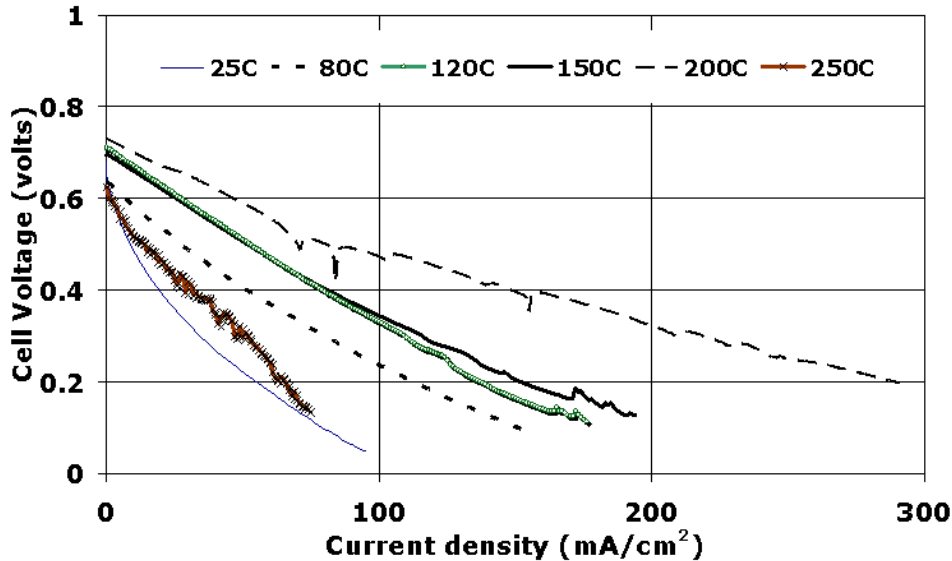
\*Sample sent to Bekktech in March 2009

# Technical Result:

## I/V curve for a fuel cell with neat ITP vs. a 70% ITP-30%PVPP membrane

### Neat ITP

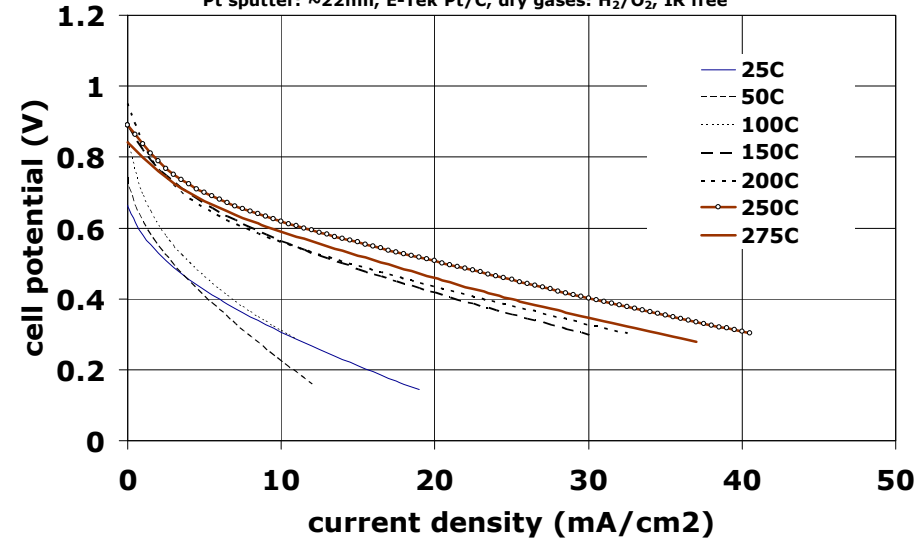
Fuel cell with pure ITP (10%In 90%Sn) electrolyte,  
t=1.0mm, area= 0.5cm<sup>2</sup>, no Pt sputter interface, electrodes: E-Tek Pt/C (0.6mg/cm<sup>2</sup>),  
fed dry H<sub>2</sub> and O<sub>2</sub>, temp: 25 to 250C.



### Blend 70% ITP 30% PVPP

Fuel cell with electrolyte of 70%ITP-30%PVPP,

t=1mm, active area: 0.5cm<sup>2</sup>,  
Pt sputter: ~22nm, E-Tek Pt/C, dry gases: H<sub>2</sub>/O<sub>2</sub>, IR free



t=1mm, active area: 0.5cm<sup>2</sup> and electrode of ~22nm sputtered Pt  
and  
E-Tek GDL fed dry H<sub>2</sub>/O<sub>2</sub>, Room Temperature to 250C

## Conclusions about Membranes with pure ITP and ITP-PVPP Blend

The best fuel cell results with ITP-PVPP blend were at  $T > 200\text{C}$ , which is unusual ... since TGA suggests that the PVPP organic compound should have decomposed.

The highest conductivity found for ITP-pVPP blend was  $\sim 0.014 \text{ S/cm @ } 275\text{C}$ .  
There was an unexpected drop in conductivity between  $25\text{C}$  and  $100\text{C}$ .

Pure ITP (10% In 90% Sn), has better conductivity than the blended pellet, which is expected since the conductivity of pure PVPP is lower than pure ITP.

Pure ITP showed higher power than blend

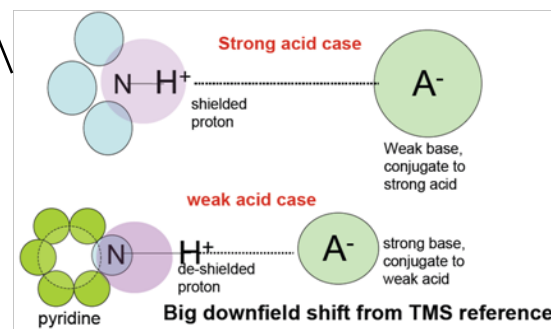
Still finding a suitable ITP-polymer blend is desirable to stop crossover in pure ceramic ITP

# Technical Accomplishment: classifying strong- and super-acids

## Table of \*N-H Proton chemical shifts for pLs:

Acid	H <sub>2</sub> O in pL (ppm)	$\delta$ (N-H) (ppm)
HFeI <sub>4</sub>		
HAICl <sub>4</sub>	Very low	4.618
HBF <sub>4</sub>		5.0
HTFSI	101	6.697
HBETI	183	6.65
HI		
HClO <sub>4</sub>	31	7.010
HTf	24	7.771
HSbF <sub>6</sub>	469	8.56 ??
H <sub>2</sub> CH <sub>2</sub> <sup>+</sup>		
HBr		
HCl		
HCH <sub>3</sub> SO <sub>3</sub>	910	9.5
HN(CN) <sub>2</sub>	1603**	9.5
HNO <sub>3</sub>	36	9.730
HCl <sub>2</sub> CHAc	1476**	10.245
HTfAc	230	11.268
Citric acid		
HAc	1306**	14.0

\*for base diethylmethylamine (DEMA),  
pKa (aqueous) = 10.55



From: J.-P. Belieres in the I&EC division,  
Paper #82, ACS, Philadelphia, PA 2008

**Chemical shift can be used for characterizing H<sup>+</sup> environment**

# Future Work

- ❑ **Continue to make and characterize pILs to model membranes**
  - i. Focus on non-leachable PEMs consisting of novel polymers and polymer blends with ceramics which allow all acid and base moieties to be immobilized by covalent and electrostatic binding.**
    - a. ITP**
    - b. Develop Polyphosphazenes as low EW, heat-melt formed and water insoluble membranes, Polyvinyl pyridines (PVPP), fluorinated (PVFP)**
    - c. Blends of a and b.**
  
- ❑ **Echem NMR and FTIR**
  - Continue pulse field gradient for H<sup>+</sup> mobility of new materials**
  - NMR Imaging under H<sup>+</sup> current (“NMR Hittorf”) experiment to investigate distribution of species during proton conduction**
  
- ❑ **Voltammetry of Pt and other metal electrodes in PILs to investigate:**
  - Pt-oxide formation**
  - Adsorption of pIL on Pt**
  - Check for O<sub>2</sub> reduction activity on Pt and non-Pt catalysts**
  - In situ Electrochemistry and FTIR to determine adsorption of hydrocarbon versus fluorocarbon pILs**



# Summary

- ❑ **Relevance: simpler more efficient fuel cell by using protic salt electrolyte membranes**
- ❑ **Approach: Protic salt membrane electrolytes conduct proton with no bulk water giving**
  - **simplified fuel cell with:**
    - no humidifier
    - smaller radiator
  - **little or no Pt-OH on Pt surface for:**
    - Lower overpotential for oxygen reduction, therefore higher cell efficiency
    - Possibly lower corrosion of Pt and lower Pt particle growth
- ❑ **Technical accomplishments: Status of Protic Ionic Liquids (pILs)**
  - **Designed pILs for high proton conductivity and fuel cell performance**
  - **Found stable pILs**
  - **Combined high activity and stability in some cases**
  - **Demonstrated proton conductivity and fuel cell performance in non-leachable protic salt polymer and ceramic membranes**
  - **Synthesized new poly-phosphazene polymer with pendant nitrogen heterocycles**
  - **ITP and polymer blends showed high proton conductivity from 25 to 200C**
- ❑ **Proposed Future Work:**
  - **Focus on pILs as guides to making non-leachable proton conducting salt membranes ITP, poly-phosphazenes, and blends**
  - **Continue NMR characterization of relative proton and counterion mobilities.**
  - **Chemical NMR imaging of membranes as a function of proton current.**

# Collaborations

## Project collaborators:

1. **Don Gervasio (PI) in collaboration with C.A. Angell, R. Marzke, J. Yarger (co-PI) at Arizona State University**
2. **W. Youngs (co-PI) University of Akron**
3. **Industry, Boeing Co.**