



NaSi and NaSG Powder Hydrogen Fuel Cells

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SiGNa Chemistry

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Timeline

- Start date: 08/01/2008
- End date: 01/31/2010
- Percent complete: 28%

Barriers

- Hydrogen Storage Technology Capabilities
 - Specific Energy: 2kWhr/kg
 - Cost: \$4/kWhr
- Enabling Technology for Near-Term High-Volume Fuel Cell Commercialization for Portable Applications

Budget

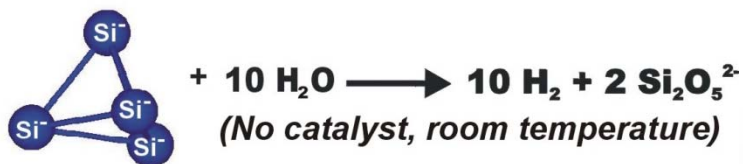
- Total funding in FY08: \$1,845,000
 - DOE share: \$1,476,000
 - Contractor share: \$369,000
 - Bulk of funds to be spent in FY09
- Additional funding for FY09
 - \$951,500
 - To be spent in FY09/FY10

Partners

- University of Texas Austin, Center for Electromechanics
 - Reactor Mechanism Research
 - Richard Thompson and Michael Lewis
- Trulite Inc.
 - 250W Fuel Cell Demonstration System
 - Ken Pearson

- Sodium Silicides rapidly liberate hydrogen from water (or water solutions) leaving a benign common industrial chemical (sodium silicate)

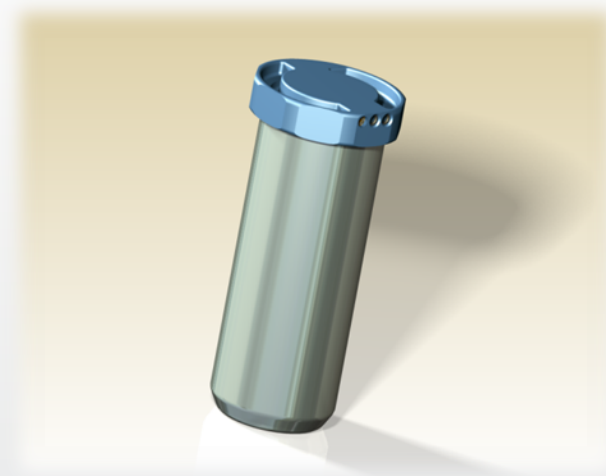
- Sodium-Silica-Gel: $2\text{Na-SG} + \text{H}_2\text{O} \rightarrow \text{H}_2 + \text{Na}_2\text{Si}_2\text{O}_5$
- Sodium Silicide: $2\text{NaSi(s)} + 5\text{H}_2\text{O(l)} \rightarrow 5\text{H}_2\text{(g)} + \text{Na}_2\text{Si}_2\text{O}_5\text{(aq)}$



- Significant System Benefits for Portable Power Applications (10 W to 3 kW)

- **Safety:** Does not ignite or oxidize in air at standard conditions even when fully exposed to air (i.e. opened storage canister).
- **Thermal Stability:** Material is stable over all practical temperature ranges (-55 to 300°C)
- **Storage:** The material has been demonstrated to have a shelf-life of over two years but is capable for being stored for significantly longer
- **Pressure:** The maximum developed pressure is determined by the system design not the material characteristics. The maximum pressure is expected to be under 50 psi (material capable of 1000's)
- **Ease of Use:** No catalyst required to produce hydrogen gas
- **By-products:** Generates a non-toxic aqueous waste, sodium silicate.

- Demonstrate enabling hydrogen storage technology suitable for early fuel cell market applications with high volume potential
- Demonstrate the benefits of sodium silicide technology in a push-to-start hydrogen generator system
- Develop a demonstration system capable of ~250 W for applications such as battery re-chargers, remote telecommunications, emergency responders, backup power, and personal mobility (i.e. scooter, bicycle, Segway)
- Demonstrate technology to approach DOE Hydrogen storage targets even for small systems (<1kW)



Market Example: 11 Day Mission for Special Forces




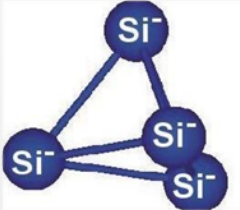
Technology	Per Unit	Unit Cost	Mission Qty	Mission Wt.	Mission Cost
BA 5590	<u>140 W-hrs</u> (1.0 kgs)	\$80	35 4,900 W-hrs	<u>35 kgs</u>	<u>\$2,800</u>
SiGNa NaSi	<u>700 W-hrs</u> (1.42 kgs) • Packaging: 0.2 kgs • Powder: 0.4 kgs • Water: 0.8 kgs	\$84 • Packaging: \$20 • NaSi: \$64 /kg	7 4,900 W-hrs	<u>11.4 kgs</u> • Cartridges: 9.9 kgs • Fuel Cell: 1.5 kgs	<u>\$688</u> • Cartridges: \$588 • Fuel Cell: \$3000 / 30 missions = \$100

Sodium Silicide provides significant value as compared to batteries with respect to weight, cost, and logistics.



Battery Disposal/Storage



Task 1.0 System Engineering	Task 2.0 Breadboard Testing and Reaction Control Mechanism	Task 3.0 Hardware Development	Task 4.0 Fuel Cell System Integration	Task 5.0 Advanced Materials Research and Manufacturing Methods
<p><u>Key Specifications</u></p> <ul style="list-style-type: none"> • Powder <ul style="list-style-type: none"> •Current: >3100 W-Hr/kg (LHV) •Advanced: >4100 W-Hr/kg (LHV) • Packaged Canister <ul style="list-style-type: none"> •Current: 1336 W-Hr/kg (LHV) •Advanced: 1676 W-Hr/kg (LHV) • Cartridge Capacity <ul style="list-style-type: none"> •>500 W-Hr (net Fuel Cell) •< 1 kg 	<p><u>Initial Results</u></p> <ul style="list-style-type: none"> • Reactor Volume <ul style="list-style-type: none"> • Demonstrated 100mL reactor • Fabricated 1 Liter reactor • Material Characteristics <ul style="list-style-type: none"> ▪ High Density ▪ Fast Reaction Times • Lessons Learned <ul style="list-style-type: none"> ▪ Hydrogen Filtration ▪ Water Distribution 	<p><u>Key Specifications</u></p> <ul style="list-style-type: none"> • Push-to-Start Hydrogen • System: <2kg • Suitable for lab H₂ generation or fuel cell company evaluation 	<p><u>Specs/Acquisition</u></p> <ul style="list-style-type: none"> • 250W with water recirculation • Initiated sub-contract 	<p><u>Status</u></p> <ul style="list-style-type: none"> • H₂ purity analysis (on-going) • Initiated manufacturing process dev. • Initiate work for additive for low temperature operation (FY2009) • Initiate Advanced Material Research (FY2009) 

Systems Analysis

	NaSi	NaSi (no over- stoich water)	Adv. Silicide	Adv. Silicide (no over- stoich water)
System Engineering for H250 Hydrogen				
Powder Weight (kg)	0.50	0.50	0.50	0.50
Theoretical Powder Performance	9.8%	9.8%	13.0%	13.0%
Estimated Powder Performance	9.5%	9.5%	12.5%	12.5%
H2 Weight (gm)	48	48	63	63
Water				
Water Stoich (kg)	0.42	0.42	0.56	0.56
% Recapture	50%	50%	50%	50%
Water Weight, Recaptured (kg)	0.21	0.21	0.28	0.28
Net Stoich Water (kg)	0.21	0.21	0.28	0.28
Over. Stoich Water (kg)	0.27	0.00	0.27	0.00
Total Water Required (kg)	0.48	0.21	0.55	0.28
Weight				
Canister Weight (kg)	0.20	0.20	0.20	0.20
Canister + Water + Powder (kg)	1.18	0.91	1.25	0.98
Energy/Density				
Chemical Energy (W-Hr), LHV	1,582	1,582	2,081	2,081
Specific Energy, Powder (W-Hr/kg), LHV	3,164	3,164	4,163	4,163
Specific Energy, Powder + Stoich. Water w/ 50% Recapture + Over-Stoich. Water + Canister (W-Hr/kg), LHV				
	1,336	1,734	1,664	2,125

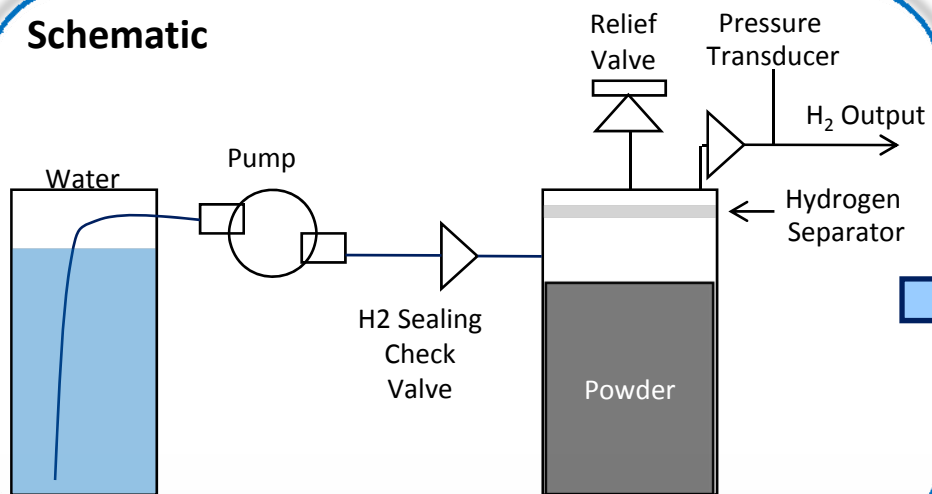
- Approaching DOE Targets Even for Small, Portable Hydrogen Storage Applications
 - Specific Energy
 - Current Tech.: 1336 W-Hr/kg, LHV
 - Next Gen. Tech.: 1664 W-Hr/kg, LHV
 - Cost
 - Sodium and Silicon are only production material cost
 - \$4.47 / kW-Hr
- Biggest Unknown: Over-Stoich Water
 - Assumptions based on purchased sodium silicate / water solution
 - NaSi reactivity and sodium silicate solubility will compete for water
 - Temperature control and water feed system under development to perform detailed study

Cost Analysis*

	2010	2011	2013	2015
Sodium (\$/kg)	\$ 3.08	\$ 3.08	\$ 3.08	\$ 3.08
Silicon (\$/kg)	\$ 6.42	\$ 6.42	\$ 6.42	\$ 6.42
Sodium Silicide Production (\$/kg)	\$ 90.00	\$ 50.00	\$ 20.00	\$ 7.00
Sodium Silicate Use (\$/kg)	\$ (2.38)	\$ (2.38)	\$ (2.38)	\$ (2.38)
Total (\$/kg)	\$ 97.13	\$ 57.13	\$ 27.13	\$ 14.13
\$/kWh powder	\$ 30.70	\$ 18.06	\$ 8.58	\$ 4.47

*Prices for Sodium & Silicon Based on Quotes From US Vendors

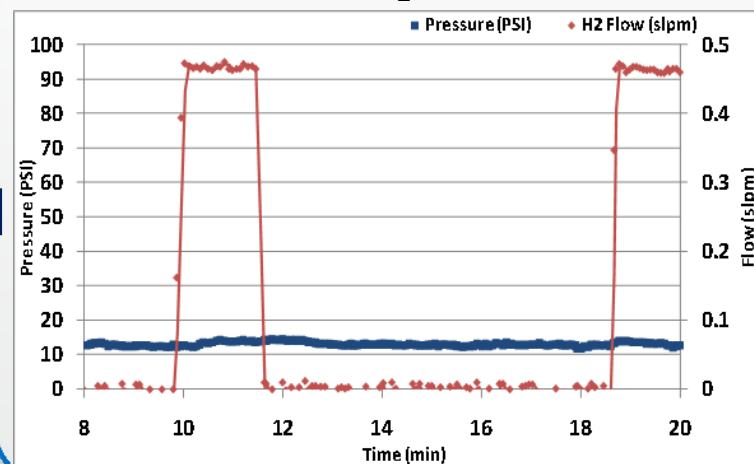
Schematic



Laboratory Unit



Controlled H₂ Generation



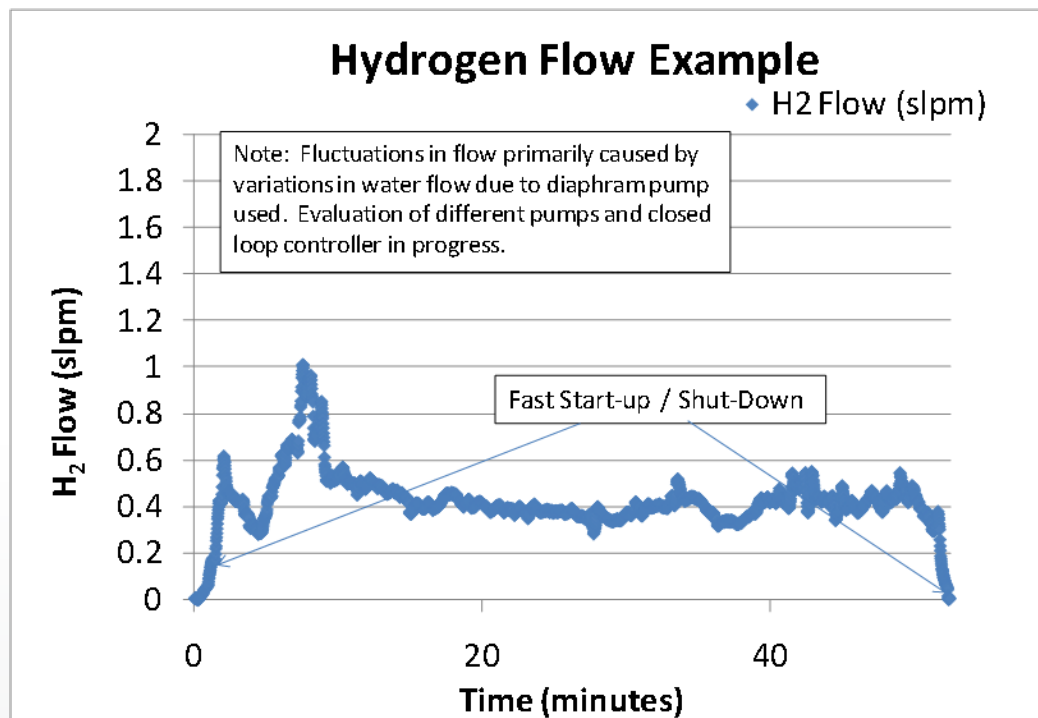
Beta Systems
October 2009



**General Purpose H₂ Generator For Fuel Cell
Partner Evaluation and Industrial Use**

Breadboard Testing Overview

- Repeated demonstration of high flows / fast reaction times in a small system
- Powder Energy Density: ~3200 W-Hr/kg (LHV of H₂)
- Maximum of 48 gm Tested in a Single Fixture
- Demonstrated 3 Re-starts



Date	Serial	Test #	Powder Type	Mass (g)	H ₂ (std L)	Grams H ₂	Correct mL H ₂ O	Watt-Hrs/Kg Powder
1/29/2009	BB4Ni	23	NaSi	26	28.6	2.4	82.9	1586.0
1/30/2009	BB4Ni	24	NaSi	21.4	23.8	2.0	77.2	1603.2
2/2/2009	BB4Ni	27	NaSi	17.9	19.5	1.6	59.6	1568.8

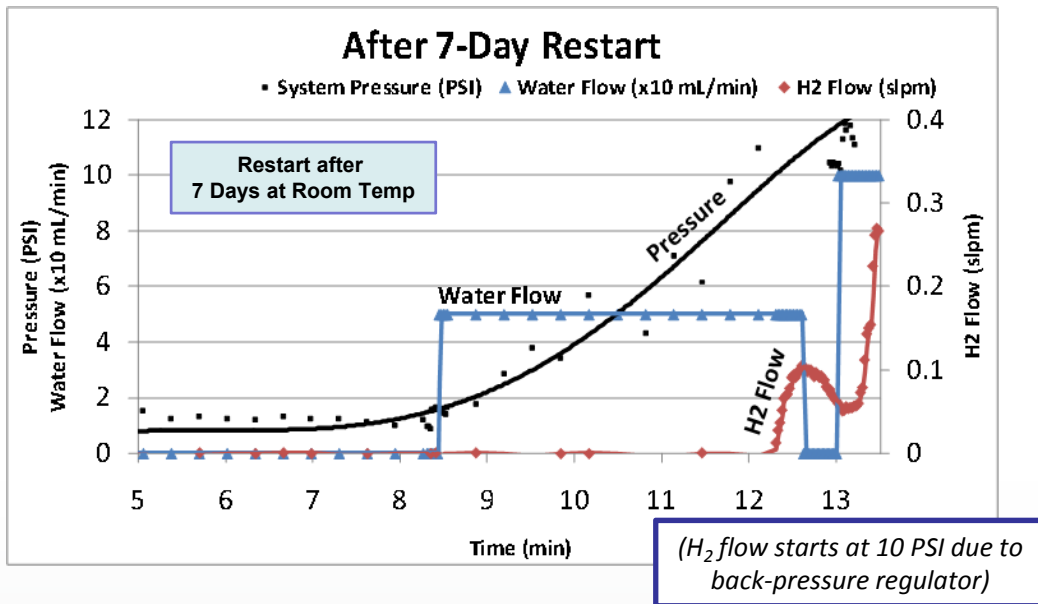
Net: assumes 50% fuel cell conversion efficiency

•**Issue:** Sodium Silicate Waste Product Can Slow Restarting

•**Solution:** Multiple Water Injection Ports Distributed Through Powder

•**Initial Results**

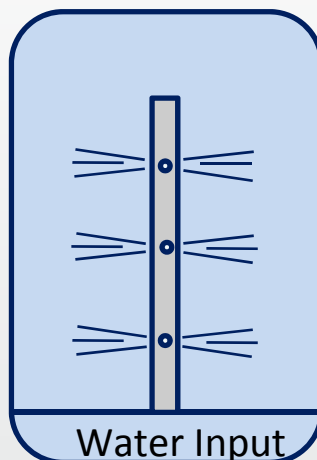
- Significant decrease in system restart time
- 3 Re-starts Demonstrated on 48 gm of powder
 - Start #2: > 24 hrs off time
 - Start #3: > 168 hours off time
- Approximately 1/3 consumed per use = 25 W-Hrs (net fuel cell)



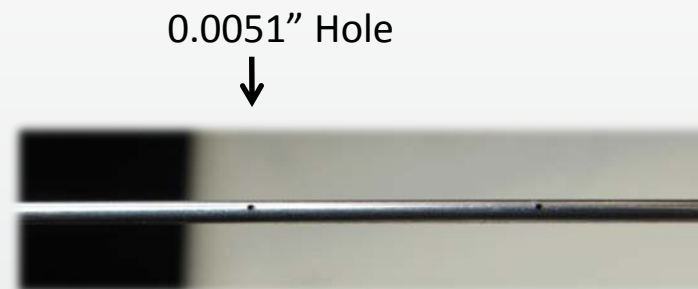
Spiraled water feed network tube



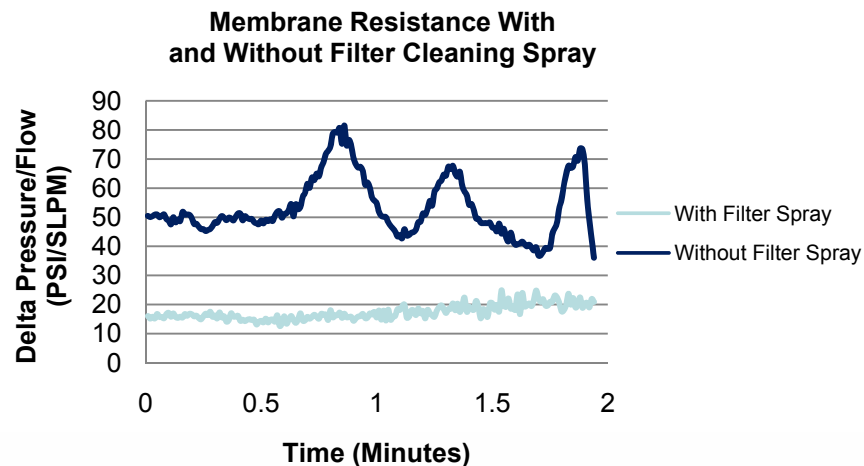
Water feed tube spraying inside Canister



Close-up of laser drilled holes in water feed tube



- Significant foaming observed in test reactor with cross-sectional area of $\sim 1.5 \text{ in}^2$
- Almost zero foaming observed in test reactor with cross-sectional area of $\sim 6 \text{ in}^2$
- Using small / low volume reactor: a cleaning nozzle is required
- All spray water runs-off to reaction sites and utilized
- Initial testing was done with crude holes spraying on the filter in isolated areas
- Current laser drilled precision holes with controlled spray patterns are under evaluation



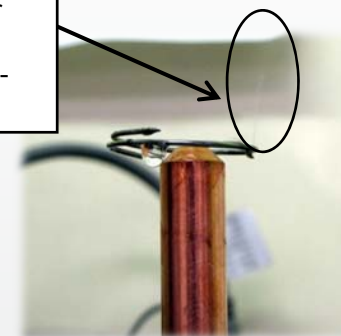
No Filter Cleaning



Filter Cleaning
Nozzles Used

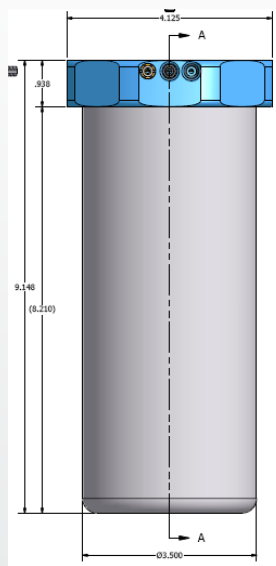
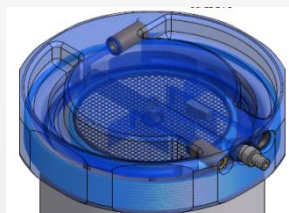
Fine Water
Spray
From Micro-
Nozzle

Only Two
Nozzles Used



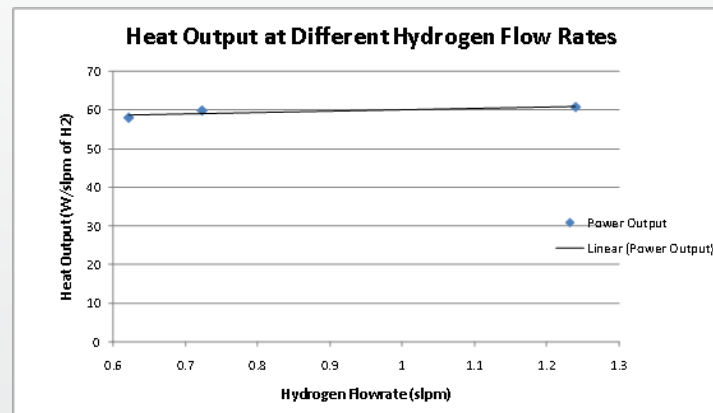
Design Characteristics

- Up to 500 gm Per Cartridge (Limit Set by DOT Shipping Regulations)
- Stores all waste product
- Net Fuel Cell Energy
 - >800 W-Hr / Cartridge
- Low Pressure
 - Nominal: 30 psi
 - Max. Continuous Design: 100 psi
 - Expected Burst: >300 psi
- Dimensions: 3.5" Dia X 9" Length
- Weight
 - 0.28 kg in 2009
 - 0.20 kg in 2010
- Thin Walled Canister Designed for Heat Removal
 - 60 W / slpm_{H₂}



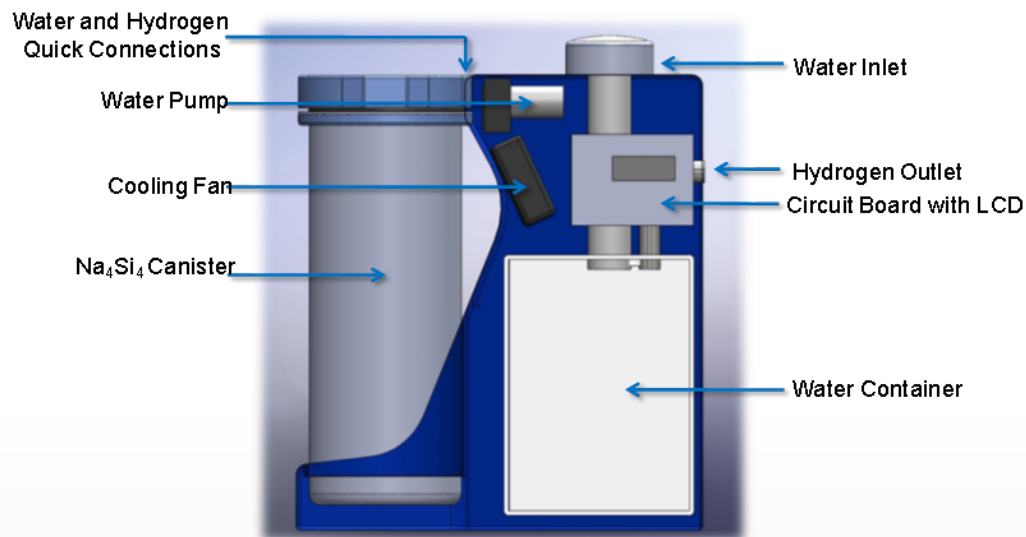
Weight Balance

Canister Part Description	Pre-Production Weight (kg)	Estimated Production Wt (kg)
Can	0.11657	0.09909
Cap/Can Capture Ring	0.02082	0.01770
Cap	0.10718	0.06431
O-Ring (cap to can ID seal)	0.00091	0.00091
Dip Tube (reaction chamber pressure relief)	0.00272	0.00204
O-Ring (pressure relief valve seal)	0.00091	0.00091
Pressure Relief Valve	0.00925	0.00925
Retaining Ring, Internal Self Locking (relief valve)	0.00091	0.00091
Filter Capture Ring	0.00590	0.00000
O-Ring (H ₂ output filter ID)	0.00091	0.00000
O-Ring (H ₂ output filter OD)	0.00091	0.00000
Filter (H ₂ output)	0.00136	0.00136
Screen (H ₂ output)	0.00741	0.00000
RFID Transponder	0.00045	0.00045
Fitting (center fluid feed)	0.00045	0.00045
Tube (center fluid feed)	0.00272	0.00272
Tube (H ₂ filter sprayer)	0.00091	0.00091
O-Ring (H ₂ /H ₂ O I/O ports)	0.00091	0.00091
Check Valve (H ₂ /H ₂ O I/O ports)	0.00454	0.00454
Total Weight (kg) (Less NaSi and Water)	0.28	0.20



Specifications

- Dimensions: 9" X 9" X 10" (height)
- Approx. System Weight: <2 kg
- H₂ Flow Rate (Continuous): 3 slpm
- H₂ Flow Rate (Peak): 8 slpm (0.25 Seconds every 2 minutes)
- Watt-Hrs/Cartridge: >1500 W-Hr (LHV)
- Regulated Output Pressure: 25 psi
- Initial Target Operating Temp: -5 to 40°C
- Start-up Time: 1 min
- Restarts: >5 / cartridge (expect >10 to 20)



Seeking Development Partners for Beta System Evaluation: October 2009



- Subcontract to Trulite Inc.

- Development of a 250W Fuel Cell System with Water Recirculation
- Status: Subcontract has been awarded. Early stages of development.
- Principal Investigator: Ken Pearson



- Subcontract to the University of Texas Austin, Center for Electromechanics

- Alternative reaction mechanism development and control
- Status: Subcontract has been awarded. Early stages of development.
- Principal Investigators: Richard Thompson and Michael Lewis

The University of Texas at Austin • Center for Electromechanics





- FY2009
 - Complete hydrogen purity verification
 - Complete development of prototype system
 - Demonstrate technology in an end customer application (late FY2009 – Early FY2010)
 - Research and develop high volume manufacturing methods for sodium silicide
 - Conduct additional experiments with additives to improve low temperature operability (below freezing)
 - Initiate research on ultra-high density sodium silicides
- FY2010
 - Deliver ~10 systems for Hydrogen Generator beta testing (early FY2010)
 - Improve hydrogen generation system performance and robustness
 - Work with development partners for end system integration
 - Demonstrate high volume manufacturing process for sodium silicide
 - Continued research on ultra-high density silicides



- Sodium silicides enable real-time hydrogen generation for portable applications that require low weight and cost
- Sodium silicides have unique technical attributes that enable simple systems with significant benefits over competitive hydrogen storage technologies
 - Fast starting
 - Low temperature
 - Low pressure
 - Long term storage
 - High temperature stability
- Continued research on ultra-high density sodium silicides will enable packaged fuel to approach doe targets of 2 kW-Hr/kg and \$4/kW-Hr for mobile power solutions