



Biomass Fuel Cell Systems

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**Colorado School of Mines
Golden, Colorado, USA**

June 8, 2010



**Project ID:
FC076**

Overview: Improve robustness of hydrocarbon- and biomass-fueled solid-oxide fuel cells and systems



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■ Timeline

- Project start date: 10/1/2009
- Project end date: 9/30/2012
- Percent complete: 20%

■ Budget

- Total project funding:
 - DOE Share: \$1,665,125
 - CSM Share: \$425,018
- Funding received in FY09:
 - \$1,665,125
- Funding for FY10: \$0

■ Industrial Partners

- CoorsTek, Inc. (Golden, CO)
 - Tubular SOFC supplier
 - Integrated ceramic heat-exchanger / fuel-reformer

■ Project Lead:

- Colorado School of Mines

Barriers:

■ Durability

- Broaden SOFC operating windows under hydrocarbon / biomass fuels

■ Performance

- Increase efficiency through system optimization / BoP integration
- Optimize fuel-processing strategies
 - Biogas fuels of anaerobic digesters
 - Bio-derived liquid fuels (butanol)

■ Transient operation

- Develop model-predictive control algorithms

■ Balance-of-Plant costs

- Integrate BoP components
- Decrease BoP fabrication costs
- Decrease BoP materials costs

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Objectives / Relevance: Improve durability and performance of SOFC systems while lowering costs



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- **Task 1: SOFC materials for robust operation on bio-fuels**
 - Sulfur- and redox-tolerant materials to broaden SOFC operating windows
 - Develop Nickel-free, perovskite-based anodes w/ novel cell architectures
- **Task 2: Fuel processing of bio-derived fuels**
 - Utilize methane from anaerobic digesters of waste-water treatment plants
 - Develop fuel-processing for biomass-derived liquid fuels (butanol)
 - Decrease cost of fuel-processing balance-of-plant hardware
 - Integrated ceramic micro-channel heat exchangers / fuel reformer
- **Task 3: Modeling and simulation**
 - Develop chemically reacting flow models of fuel-processing hardware
 - Create design tools for micro-channel heat exchanger (HX) / reformer
 - Utilize model-predictive control to integrate system hardware
 - Improve APU dynamic response, reduce supplementary-storage need
 - Conduct thermal modeling of hot-zone system components
 - Employ system modeling: explore benefits of BoP-component integration

Task 1 Approach: Develop materials to improve SOFC durability under hydrocarbon / alcohol fuels



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- **Develop nickel-free, perovskite-based, next-generation SOFC anodes**
 - Perovskites more tolerant to sulfur, redox, and heavy hydrocarbons
 - Challenges in utilizing perovskites as anode materials in SOFCs
 - Materials stability during SOFC processing and cell operation
 - Electronic conductivity significantly lower than existing solutions
 - Catalytic activity may limit internal reforming of biomass fuels
 - Fabricate novel perovskites with unique material-doping strategies
 - Milestone: Synthesize first next-generation anode material (100%)
- **Evaluate perovskite anode performance relative to Ni-YSZ baseline**
 - Quantify stability, conductivity, and catalytic activity of new materials
 - Catalytic activity evaluated using unique Separated Anode Experiment
 - Decouples anode internal-reforming processes from electrochemistry
 - Materials conductivity currently under evaluation using 4-pt probe
 - Milestone: Demonstrate electronic conductivity $> 10 \text{ S / cm}$ (100%)
 - Materials stability measured using thermo-gravimetric analysis
 - Milestone: Demonstrate materials stability using TGA (10%)

Task 1 Results: Perovskite materials synthesized; conductivity baselined against Ni-YSZ materials



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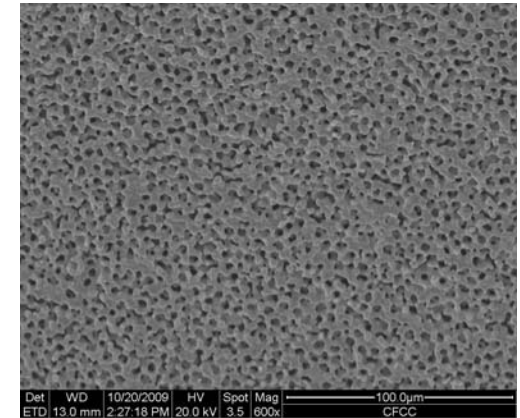
■ Perovskite anodes synthesized

- $\text{Sr}_{0.8}\text{La}_{0.2}\text{TiO}_3$ (SLT)
 - High electronic conductivity
- $(\text{La}_{0.75}\text{Sr}_{0.25})_{0.95}\text{Mn}_{0.5}\text{Cr}_{0.5}\text{O}_3$ (LSCM)
 - Internal reforming
- Multi-phase SLT / LSCM ceramic anode

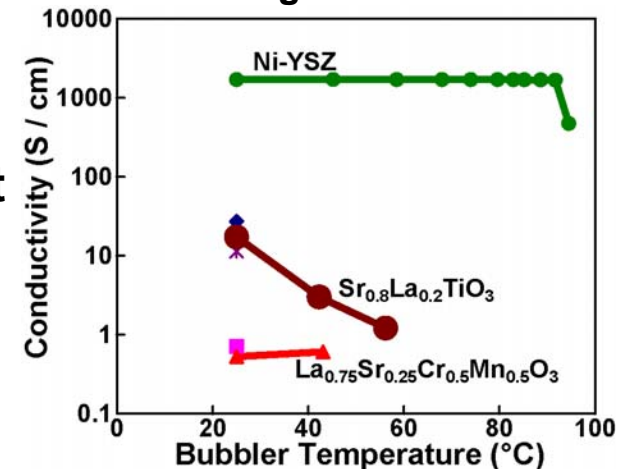
■ DC conductivity baselined against Ni-YSZ

- Materials-conductivity test stand commissioned
 - Vary temperature, gas composition
- Ni-YSZ conductivity > 1000 S / cm
 - Stable across wide range of steam content
- SLT conductivity > 17 S / cm
 - Decreases as steam content increases
- LSCM conductivity < 1 S / cm
 - Insufficient for SOFC-anode applications

Micrograph of porous perovskite anode structure



Conductivity under H_2 at 800°C increasing steam addition



Task 2 Approach: Develop bio-fuel processing strategies for optimal compatibility with SOFC



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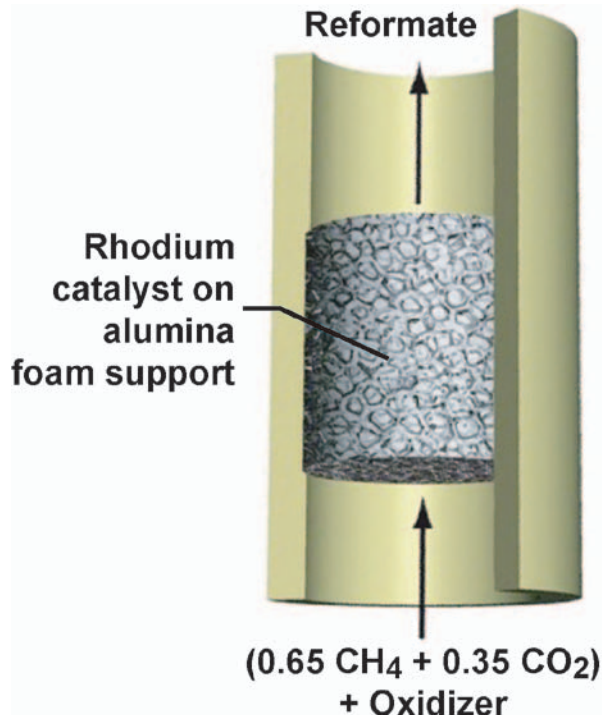
- **Biogas fuels: anaerobic digesters at waste-water treatment facilities**
 - Low-quality methane stream: 65% CH₄ / 35% CO₂
 - MW-scale power generation
- **Explore fuel-reforming options to convert biogas to syngas (H₂ + CO)**
 - Catalytic partial oxidation (CPOX - air and / or O₂)
 - Simplest approach, but lowers system efficiency
 - Steam and / or dry reforming (H₂O and / or CO₂)
 - Endothermic, but improves system efficiency and cell performance
- **Milestone: Demonstrate biogas-reforming reactor (100%)**
- **Milestone: Identify optimal reforming conditions (25%)**
- **Milestone: Demonstrate SOFC operation on biogas reformat (75%)**
- **Biomass-derived liquid fuels: butanol (C₄H₉OH)**
 - Butanol energy density 75% of diesel
 - Milestone: Demonstrate integrated liquid-fuel vaporizer / reformer (100%)

Task 2 Results: Kinetic model for biogas reforming on Rh-based catalyst developed and implemented

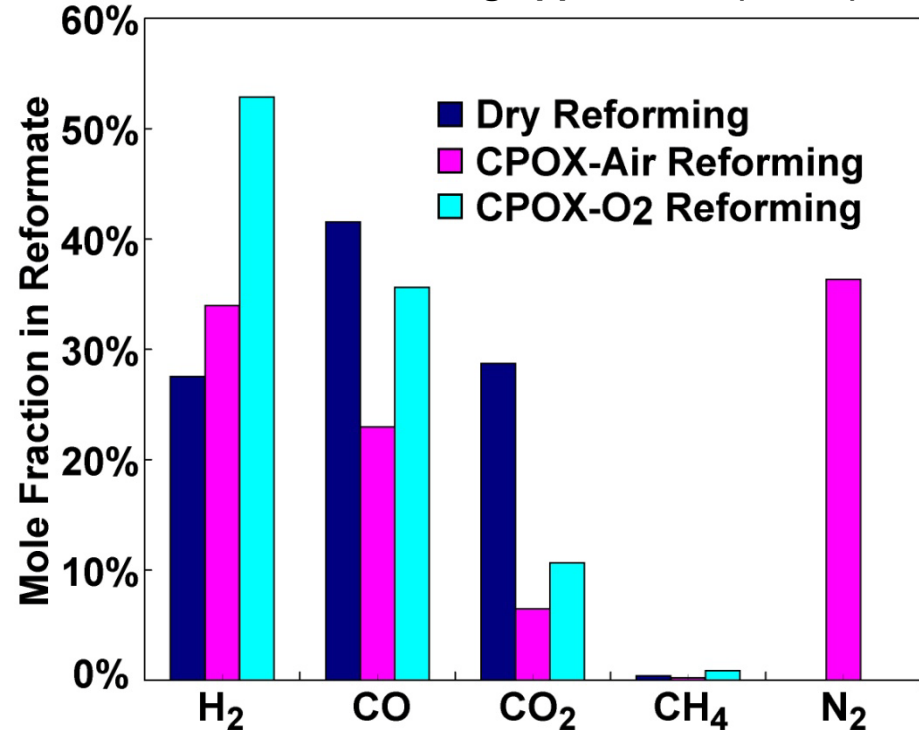


- Reacting-flow model with multi-step elementary reaction chemistry
- Exercised across numerous reforming approaches
- Excellent conversion of CH_4 and CO_2 to syngas at 900 C
 - Highest hydrogen content realized with CPOX using pure O_2

Illustration of reforming approach



Model-predicted biogas reformat composition for different reforming approaches (900 C)

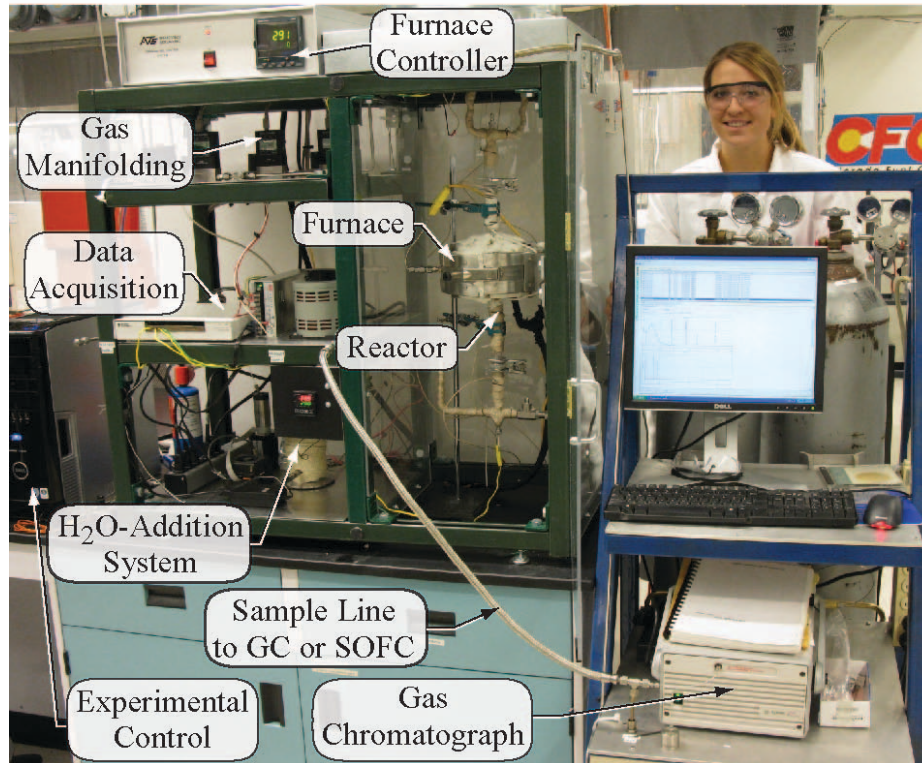
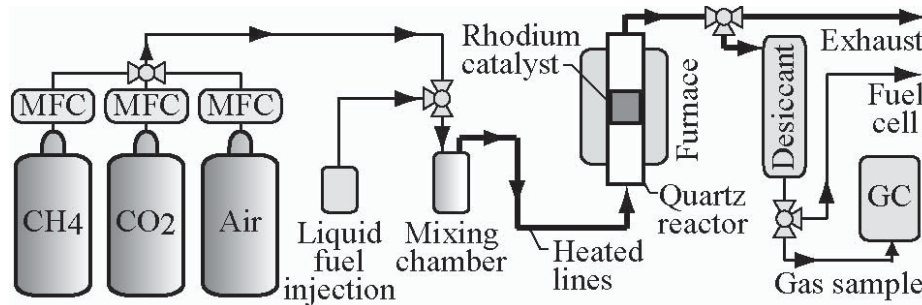


Task 2 Results: Bio-fuel reactor commissioned, integrated with SOFC-performance test stand

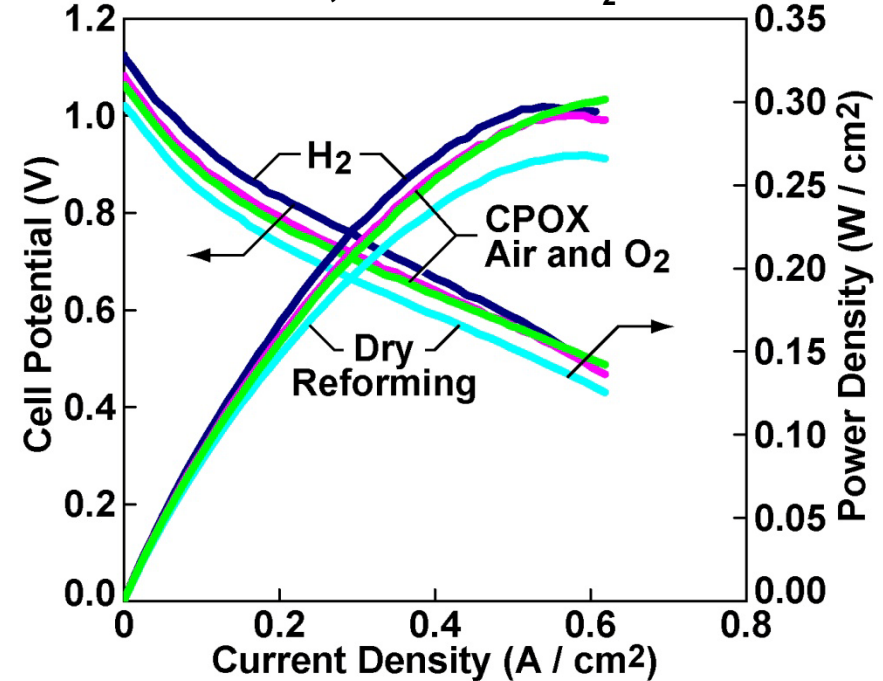


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Reforming experiment process flow diagram and photo



SOFC performance under biogas reformat, baselined to H₂ fuel

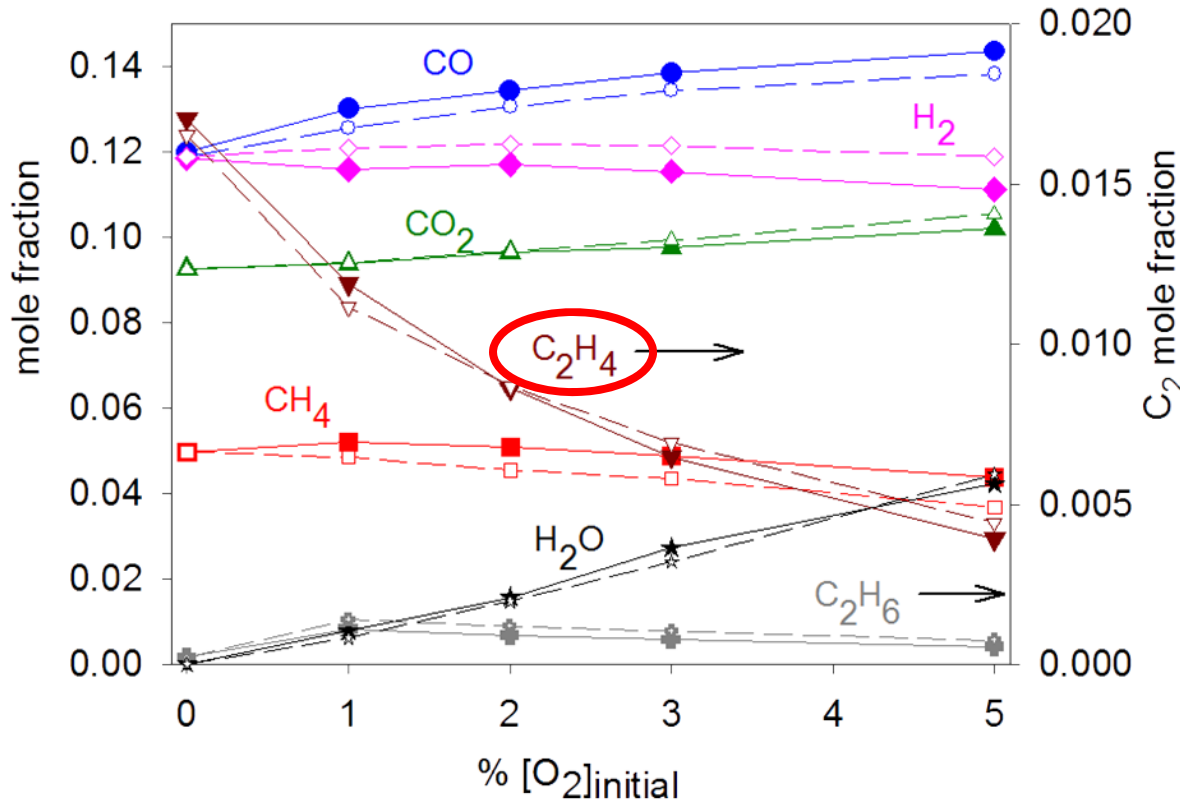


- Reforming approach strongly affects cell performance
- Cell performance under CPOX rivals H₂ fuel

Task 2 Results: Carbon-deposit precursors in biogas can be selectively reduced through O₂ addition



Gas composition changes with O₂ addition (810°C)



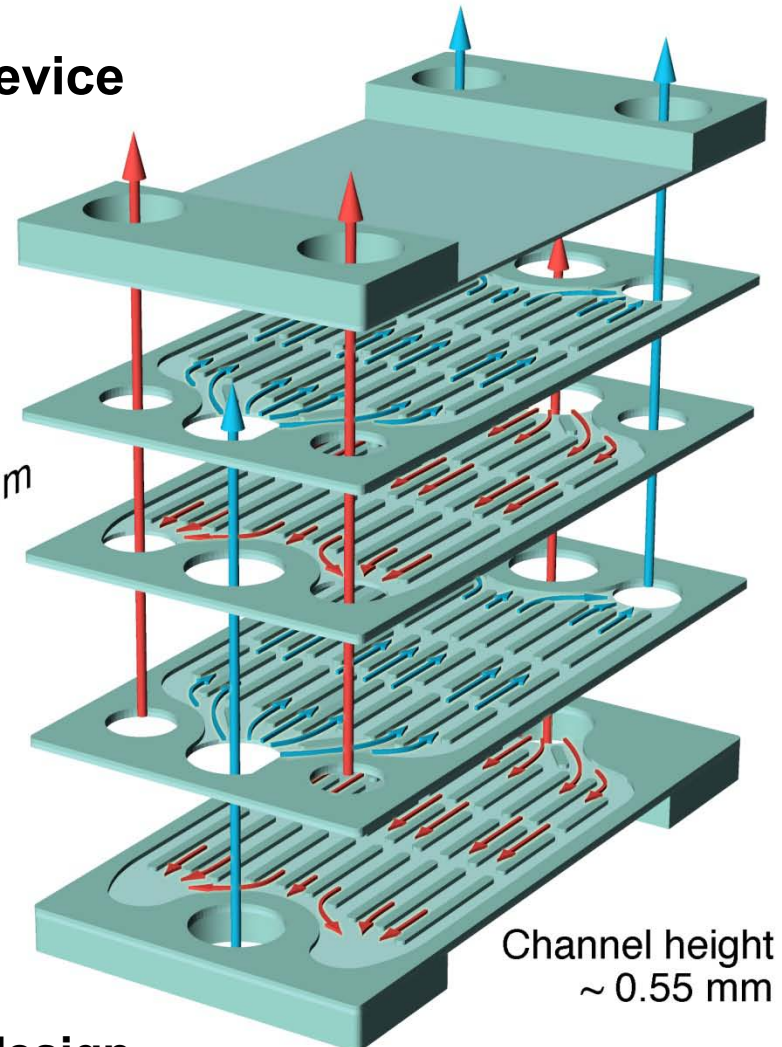
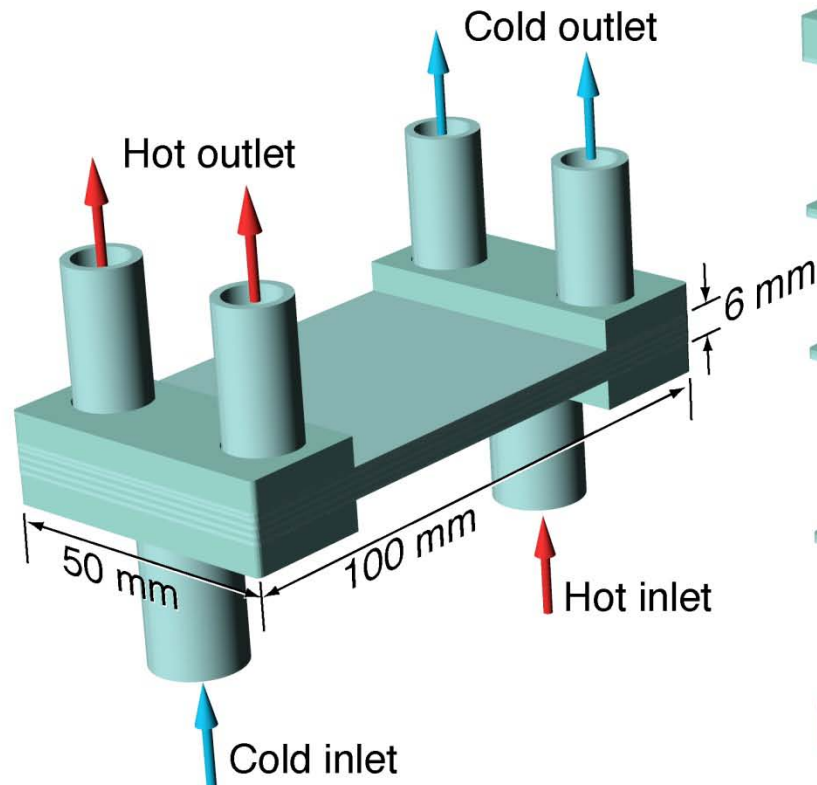
- Ethylene (C₂H₄) is the common precursor to deposits
- O₂ additional leads to significant reduction in ethylene
- H₂ and CH₄ concentrations are relatively unchanged
- CO preferentially formed over CO₂

Task 2 Approach: Develop low-cost ceramic micro-channel reactive heat exchangers for fuel reforming



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- Low-cost alumina materials
- Co-sintered layers: Single-body device
- Low-cost manufacturing



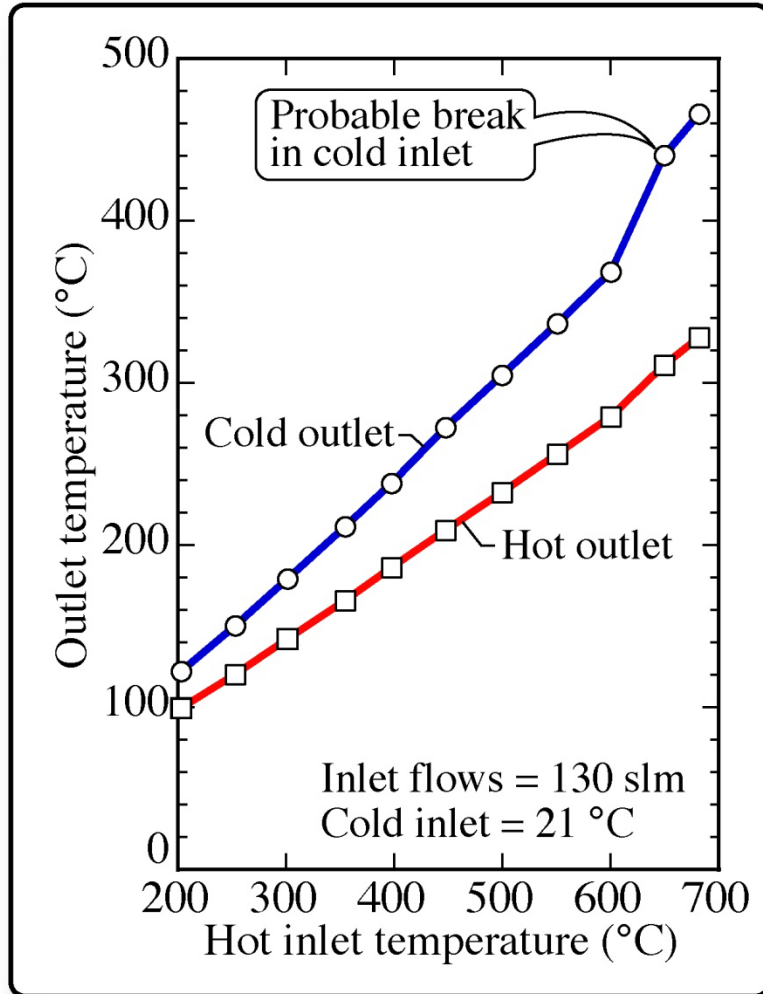
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Generation-3 design

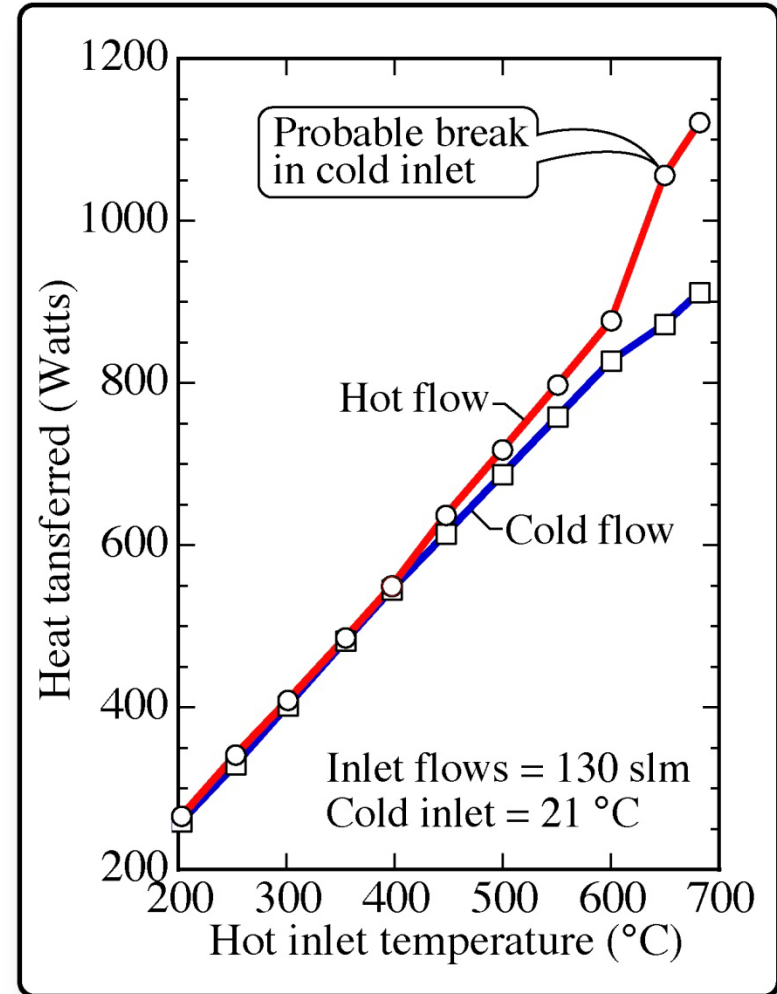
Task 2 Result: Experimental results demonstrate ceramic micro-channel HX at 700°C hot-inlet temp



Inlet and outlet gas temperatures



Total heat transferred



Task 3 Approach: Provide modeling support for Tasks 1 and 2 using CFD and chemically reacting flow tools



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- **Task 3a: Design tools for ceramic micro-channel reactive heat exch**
 - ANSYS-FLUENT Computational Fluid Dynamics software
 - Flow through complex heat-exchanger channel geometries
 - CANTERA chemically reacting flow software
 - Open-source code under development at Sandia National Labs
 - Elementary chemical kinetics for fuel-reforming simulations
 - Two models integrated through FLUENT “User-Defined Functions” feature
 - Enables high-fidelity chemically reacting flow with high-fidelity CFD
- **Task 3b: Model-predictive control for dynamic-load following**
 - Map high-fidelity CANTERA model results to rapid low-order linear models
 - Apply to fuel-reformer hardware for dynamic control of pump and blower
- **Task 3c: System-level modeling tools to advance thermal integration**
 - Map ANSYS-FLUENT results to lower-order hot-zone thermal models
 - Utilize system tools to estimate benefits of thermal-integration strategies
 - Integrated reactive heat exchangers

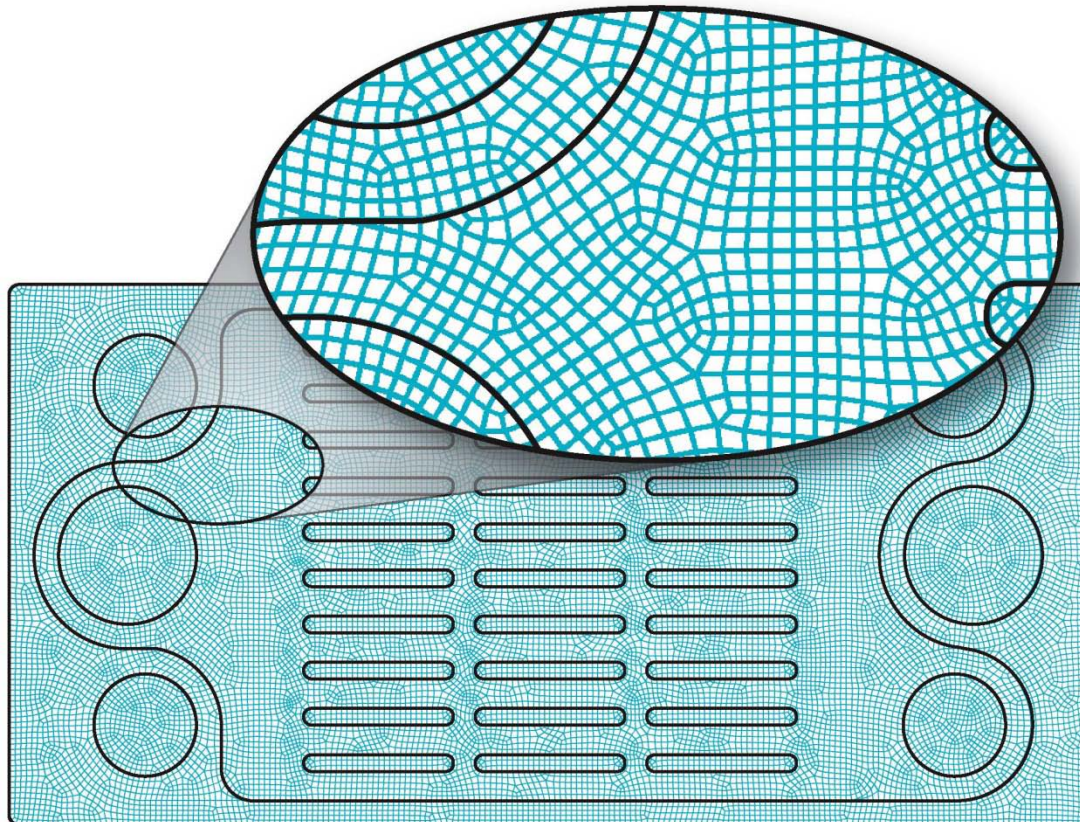
Task 3a Approach: CFD and chemically reacting flow models integrated to provide HX-design guidance



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- ANSYS-FLUENT software utilized for computational fluid dynamics
- CANTERA software developed for chemically reacting flow simulation
- Two models integrated in FLUENT “User-Defined Functions” feature

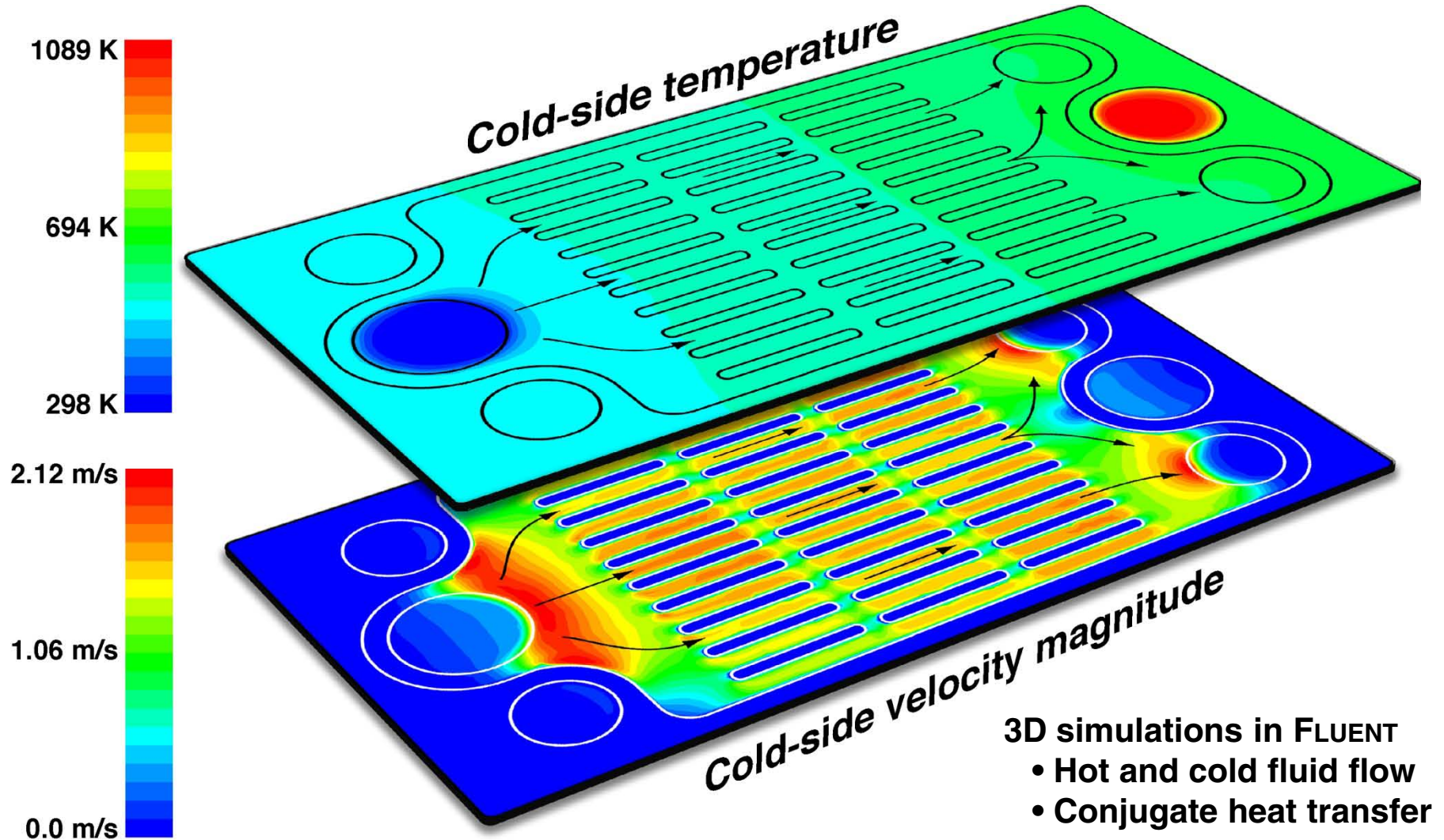
Numerical mesh used in FLUENT simulations



Task 3a Result: Models indicate that baseline design shows axially uniform flow and temperature fields



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Efforts leveraged by current NETL program at Colorado School of Mines

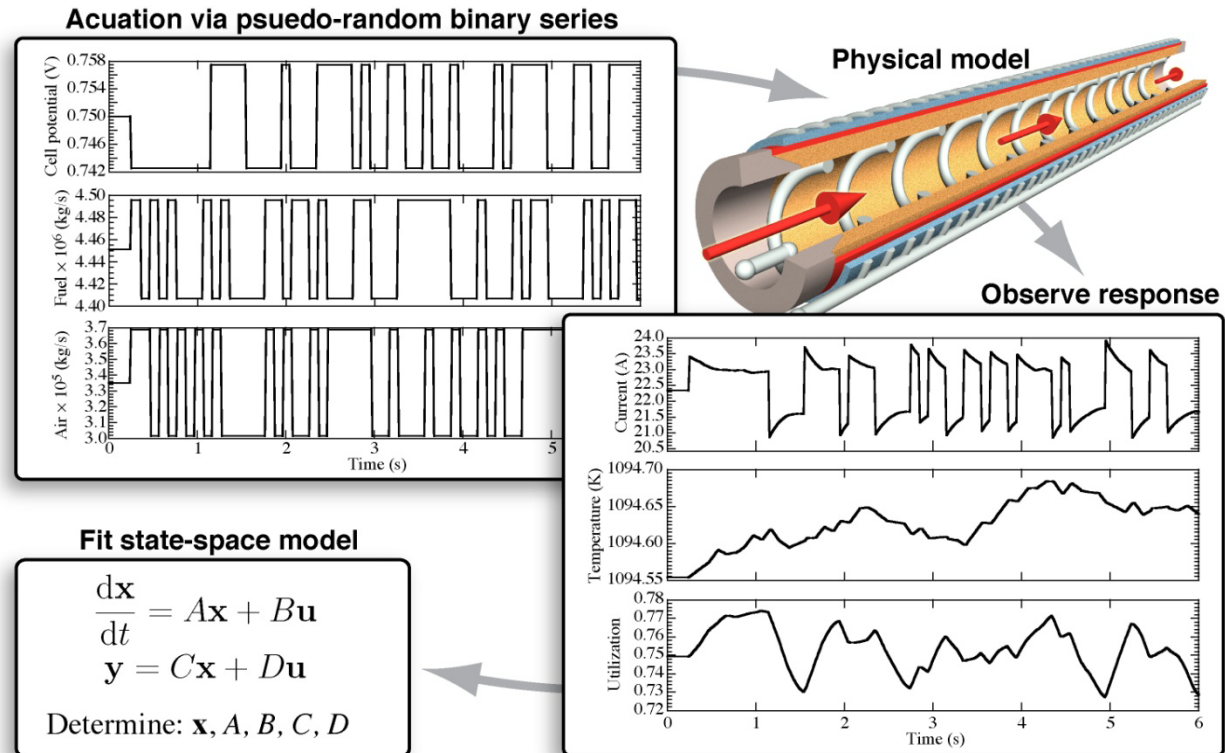
Task 3b Approach: Extend high-fidelity chemically reacting flow models to model-predictive control



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- Map high-fidelity CANTERA model results to rapid linear models
- Apply to dynamic control of fuel-reformer hardware
- Validate models with experimental apparatus
 - Milestone: Establish experimental fuel-reformer test bed (30% - Task 2)

Mapping of high-fidelity physical models to rapid low-order linear models

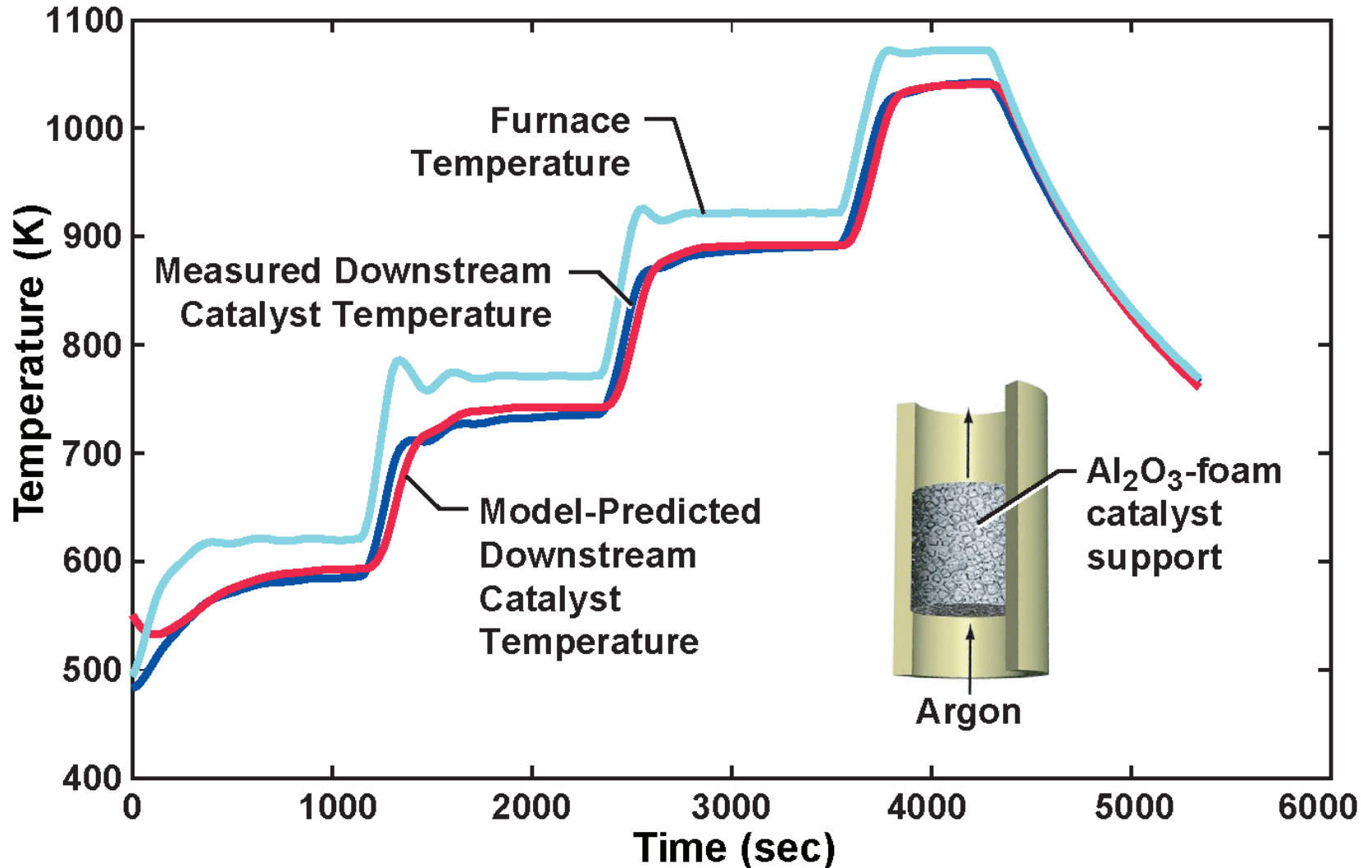


Task 3b Result: Dynamic model of reformer developed; tuned to thermal response of experiment



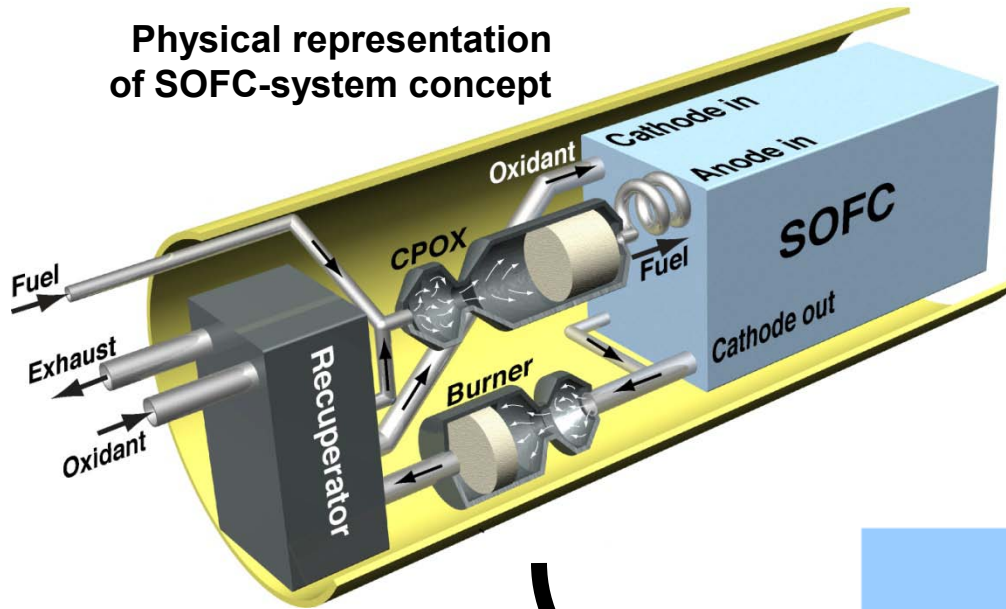
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Model-validation: reformer dynamic response (non-reactive conditions)



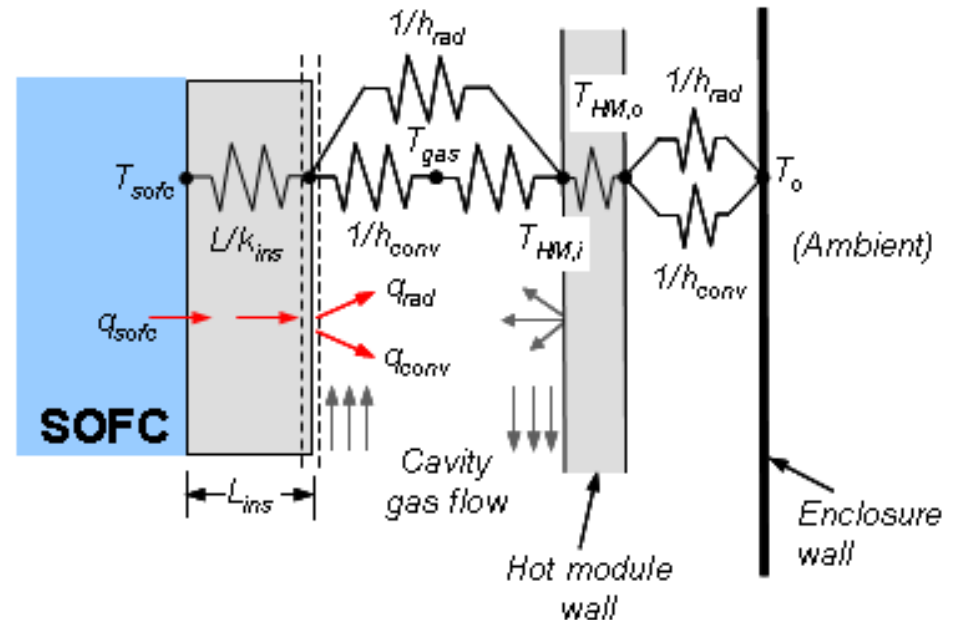
Task 3c Approach: Apply hot-zone modeling tools for creation of lower-order thermal networks

Physical representation of SOFC-system concept



- FLUENT high-fidelity CFD
 - Hot-zone thermal interactions
- Map to thermal networks
 - Rapid modeling tools

Thermal model resistive network

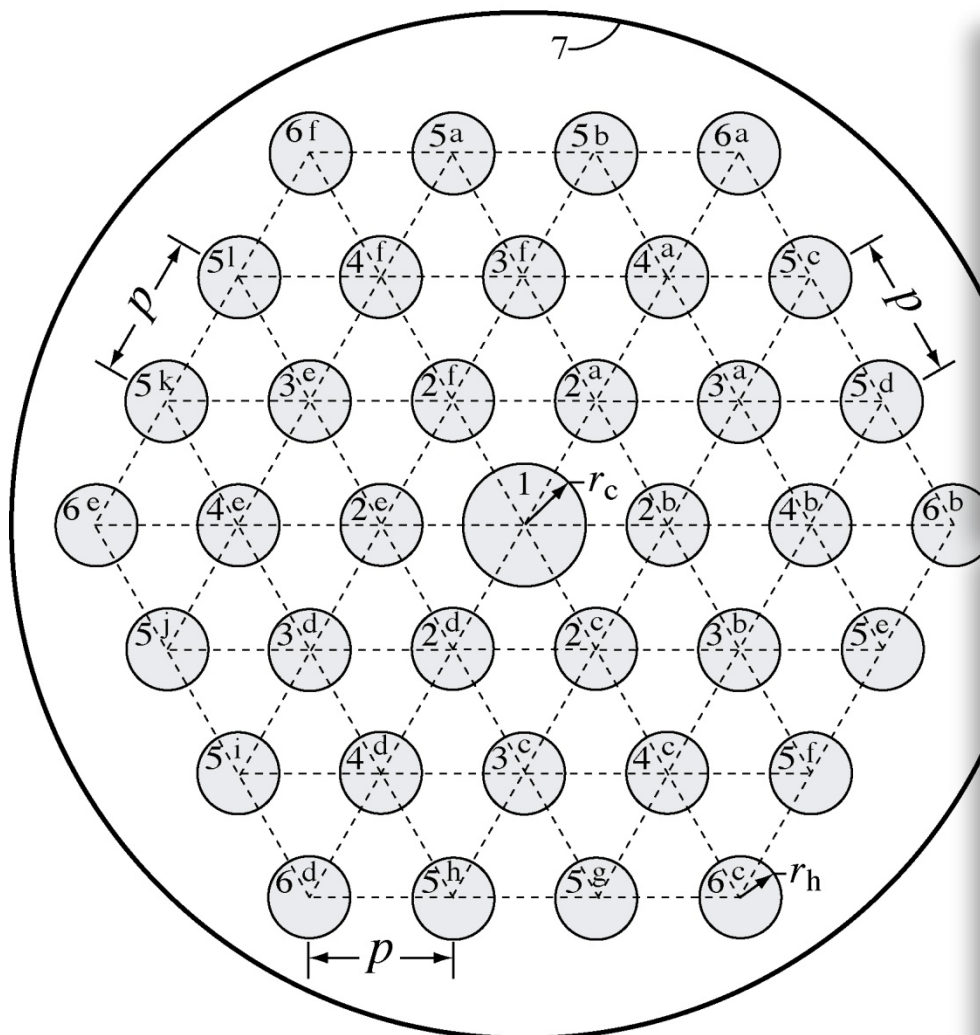


Task 3c Result: Radiative model of tubular SOFC hot zone shows impacts of cell pitch on temperature

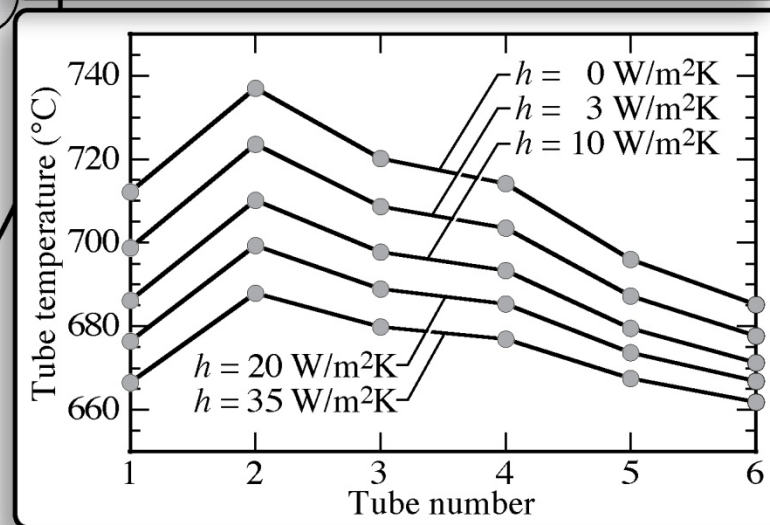
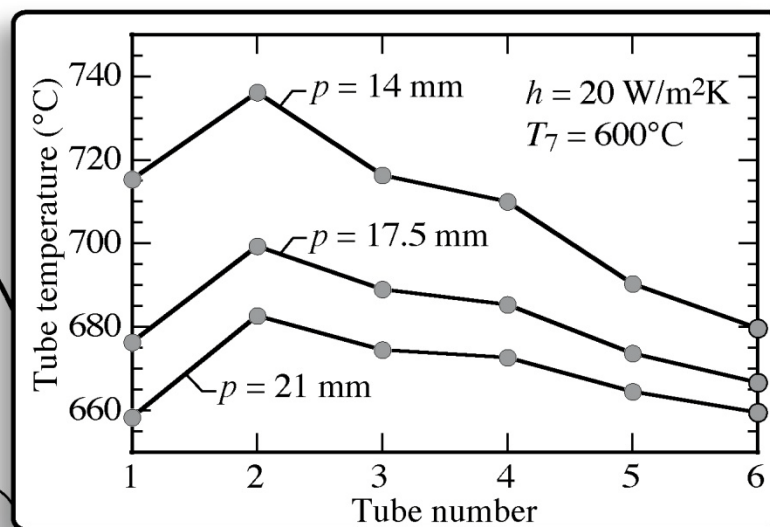


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Tubular stack geometry



Model predictions of tube temperature variations



- **Largest ceramics company in the United States**
- **Supplier of SOFCs and materials for use across multiple tasks**
 - **Task 1: Provider of baseline Ni-YSZ materials**
 - **CSM compares Ni-YSZ to next-generation perovskite anodes**
 - **Task 2: Supplier of tubular SOFCs**
 - **CSM adds cathode layer to CoorsTek anode-electrolyte assemblies**
 - **CSM evaluates cell performance under bio-fuels reformat streams**
 - **Task 2: Fabricate ceramic micro-channel heat exchangers**
 - **CSM adds catalyst to reactive side of micro-channel heat exchanger**
 - **CSM develops test protocol, evaluates performance of reactive HX**
 - **CSM develops computational modeling to provide design guidance**

Future work



- **Task 1: Next-generation SOFC materials and architectures**
 - Use Ni-free perovskite anode materials in fabrication of complete cells
 - Use proton-conducting materials in fabrication of complete cells
- **Task 2: Reforming of biomass-derived fuels**
 - Widen biogas operating windows: steam reforming, anode recycle
 - Establish fuel-processing of biomass-derived liquid fuel (butanol)
 - Validate processing strategies on operational SOFCs
- **Task 3: Modeling and simulation**
 - Task 3a: Ceramic micro-channel reactive heat exchanger
 - Add chemically reacting flow to established FLUENT CFD model
 - Exercise model; explore integrated reformer-HX operating windows
 - Task 3b: Model-predictive control of fuel-reforming BoP hardware
 - Expand mapping of high-fidelity models to rapid linear models
 - Develop control algorithms; validate on experimental facility
 - Task 3c: Thermal modeling of SOFC stack and system
 - Predict impacts of integrated reformer / HX on system efficiency

Summary: CSM program is focused on improving system robustness, decreasing BoP costs



■ Relevance

- Improve durability: advanced materials, improved control strategies
- Decrease costs: Develop low-cost integrated reactive heat exchangers

■ Approach

- Create next-generation SOFC materials
- Optimize fuel-reforming strategies for biomass-derived fuel sources

■ Results

- Demonstrated processing of next-generation SOFC-anode materials
- Demonstrated modeling and experimentation for trouble-free SOFC operation on biogas reformat
- Demonstrated operation of low-cost ceramic micro-channel heat exch.

■ Future work

- Establish SOFC operation using nickel-free perovskite anode materials
- Define trouble-free cell operation on biomass-derived liquid fuel (butanol)
- Extend heat-exchanger models to include chemically reacting flow
- Explore effect of integrated reactive heat exchanger on system efficiency