2011 Hydrogen Program

Annual Merit Review Meeting

Unitized Design for Home Refueling Appliance for Hydrogen Generation to 5,000 psi

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Project ID# PD065

This presentation does not contain any proprietary or confidential information

Overview

Phase II SBIR Program

Timeline

- **Project Start:** 08/15/2010
  Project End: 08/14/2012
- **Percent Complete:** 12%

Budget

- **Total Project Budget: $999k**

Barriers

Hydrogen Generation by Water Electrolysis

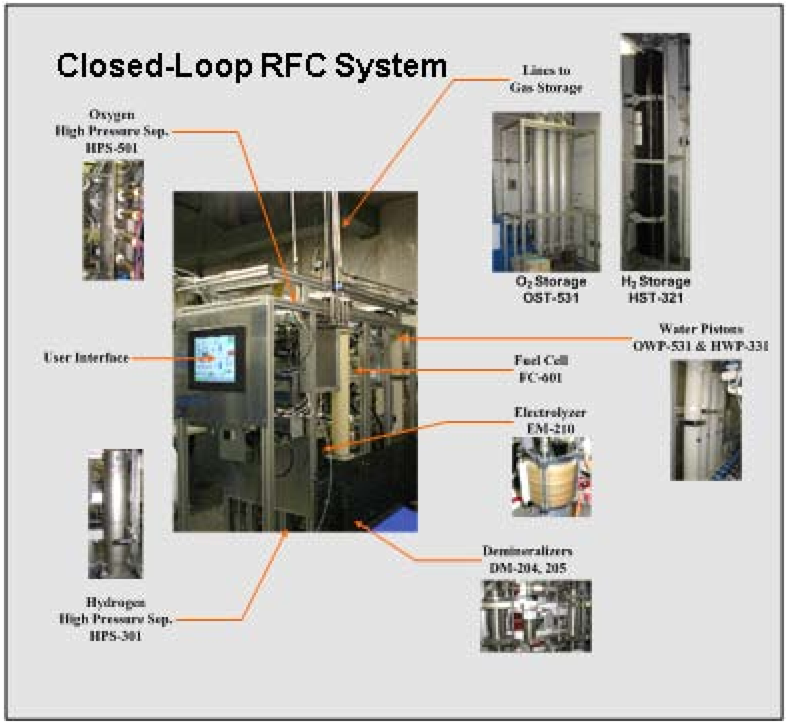
- **G. Capital Cost**
- **H. System Efficiency**

Targets

DOE TARGETS: Distributed Water Electrolysis			
Characteristics/units	**2006**	**2012**	**2017 - 2020**
Hydrogen Cost ($/kg-$H_2$)	4.80	3.70	2.00 – 4.00
Electrolyzer Cap. Cost ($/kg-$H_2$)	1.20	0.70	0.30
Electrolyzer Efficiency (%LHV) (%HHV)	62 (73)	69 (82)	74 (87)

Partners

- **Prof. R. Zalosh –** Hydrogen Safety Codes
- **IAS, Inc. –** System Controls Design
- **3M Fuel Cell Components Program (Manufacturer) –** NSTF Catalyst & Membrane
- **Entegris –** Carbon Cell Separators
- **DE-FC36-08GO18065 -** PEM Electrolyzer Incorporating an Advanced Low-Cost Membrane



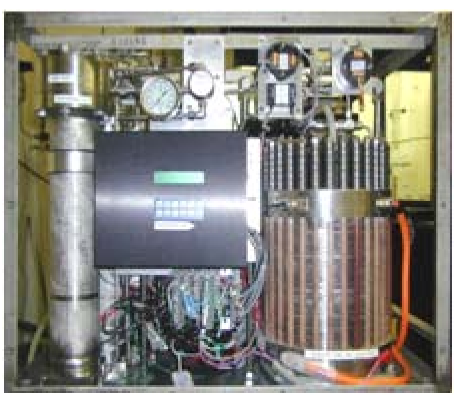
S-10 Electrolyzer System

6 kW Electrolyzer
~ 40 SCFH-H2 (~0.1 kg-H2/hr)
1500 ASF
1250 psi H2 / Ambient O2
Volume ~ 6 ft3

GES PEM Electrolyzer Systems

UUV Applications (V = 12.5 Ft^3)

12 Cells - 0.17 ft2 Cells/Stack
6-kW Electrolyzer
~ 40 SCFH-H2 (~0.1 kg-H2/hr)
High Current Density (1300-1500 A/ft2)
1000 psi H2/Ambient O2
No High-Pressure Water Feed Pump or Containment Vessel
UUV Applications



EP-1
On-Site H2 Generators

20 kW Electrolyzer
0.35 kg H2 / hr
1500 ASF
1250 psi H2 / Ambient O2
Volume ~ 16 ft3

Relevance/Project Objectives

Overall Project Objectives

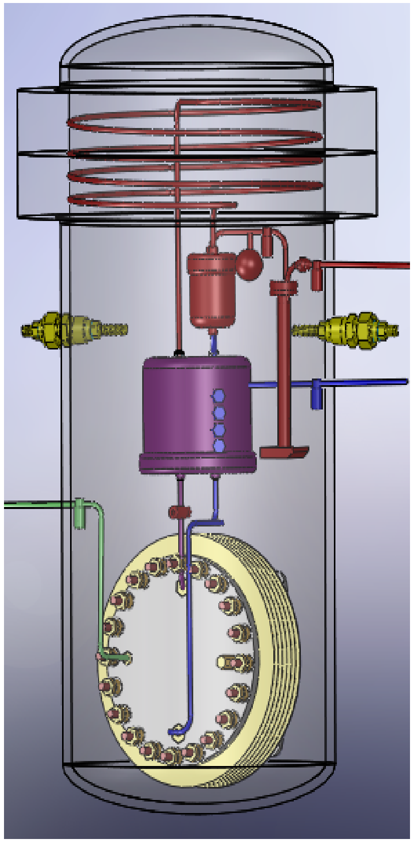
- Detail design & demonstrate subsystems for a unitized electrolyzer system for residential refueling at 5,000 psi to meet DOE targets for a home refueling appliance (HRA)
- Fabricate & demonstrate unitized 5,000 psi system (Year 2)
- Identify & team with commercialization partner(s)

Relevance

- Successfully developing a low-cost residential refueling appliance will enable early adoption of fuel cell vehicles

Impact

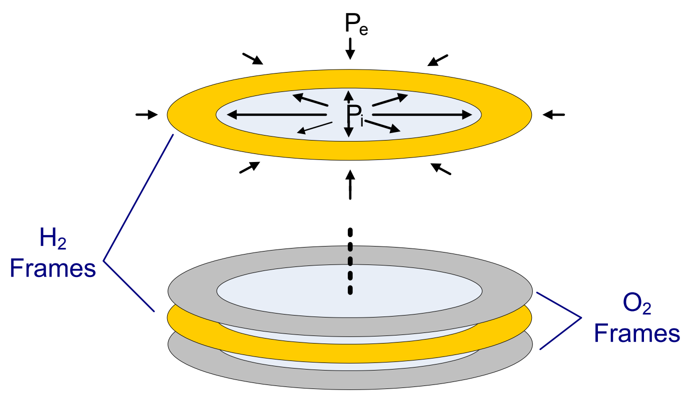
- Successfully developing a low-cost residential refueling appliance will overcome Barriers G. Capital Cost and H. System Efficiency



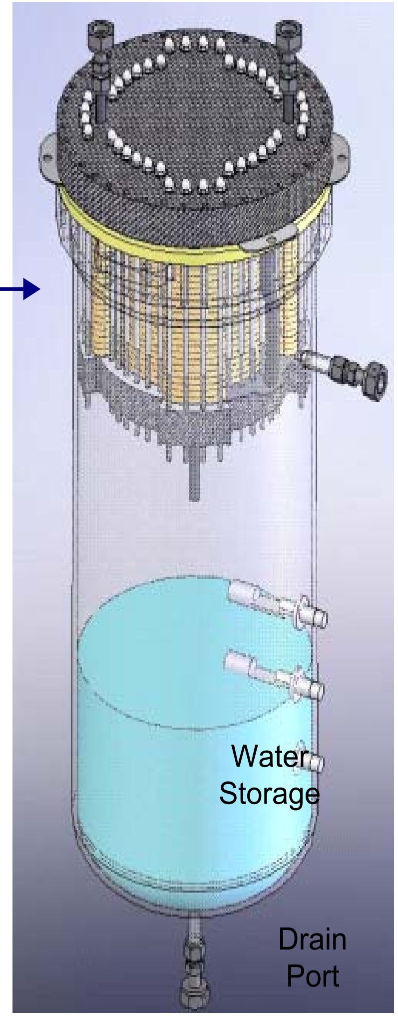
Innovative Approach to High Pressure Electrolyzer Operation

- Innovation Required to Overcome Significant Issues
  - Improve Efficiency
    - Good voltage performance
    - Reduce high gas cross-over rates
  - Supported MEA (long life)
  - Reduce Expense of High-Pressure Components
    - Stack
    - Phase separators
    - Valves, pumps, and piping
  - Engineer a Safe System
    - High pressure compressible gases
    - High pressure flammable hydrogen
    - High pressure high purity oxygen
- PEM Electrolysis Proven Under Balanced Pressure Conditions
  - To 3,000 psi with Gen 1 Navy stacks
  - Aerospace stacks at 400, 1,200, and 2,000 psi

Proposed Approach: Unitized Design Concept



Electrolyzer Cell Frames



GES Electrolyzer Stack-Dome Assemblies

Approach: Utilize a Low-Cost Cell Design

- Take Advantage of Advances & Developments on Related Giner/DOE Projects
- Carbon Cathode
  - Multi functional part
  - One piece replaces two subassemblies
    - Eliminates 20+ component parts
  - Enables high pressure operation
  - Demonstrated to 2,000 psi (balanced and differential)
- Low Precious Metal Loadings (3M)
  - 10x reduction
  - Demonstrated performance comparable to standard anode and cathode catalysts
- Single Piece Separator (Entegris)
  - Eliminates hydrogen embrittlement
  - One subassembly reduces cell part count by 30%

Approach: High Pressure Electrolyzer Membrane

PEM Electrolyzer Efficiency

- Increase Ionomer's Conductivity (Low EW)
- Thin MEA – reduces membrane resistance
- Operate at High Temperature – reduces MEA resistance
- Reduce Ionomer's Permeability
- Enabling Technology: DSM™

Approach/Milestones

Task	Progress Notes	% Complete
Task 1: Preliminary Performance of Thermosiphon-Based Electrolyzer Stack	**Completed:** ▪ Test Stand modifications complete ▪ Initial tests showed importance of cathode compartment height ▪ Special components designed, fabricated and ready ▪ Testing underway on first cathode height	**60%**
Task 2: Detailed Analysis of Hydrogen Safety Codes and Standards	**Completed:** ▪ Phase I codes and standards work updated ▪ Preparing to conduct HAZOP/FMEA after P&ID is finalized	**10%**
Task 3: Design/Build/Test Full-Scale Home Refueling Appliance (HRA) Electrolyzer Stack	**Completed:** ▪ Performed 50 cm^2 2000 psig (pumped cathode feed) electrolysis tests in a pressure dome ▪ Task 3 will use full-scale 160 cm^2 hardware tested in Task 1 ▪ Preparing to down-select optimum cathode compartment height	**20%**

Approach/Milestones (Cont.)

Task	Progress Notes	% Complete
Task 4: Optimize Selection of Protective Coating for Pressure Containment Dome Internals	**Completed:** ▪ Corrosion testing of Parylene completed ▪ Awaiting coated coupon samples from other vendors	**20%**
Task 5: Design/Build/Test 5,000 psig Pressure Swing Absorber Dryer	**Completed:** ▪ Earlier thermal swing dryer results reviewed ▪ Selected pressure swing sorbent materials ▪ Awaiting delivery of sorbents	**10%**
Task 6: Design PEM Electrolyzer HRA Breadboard System	**Completed:** ▪ Began preliminary system layouts	**10%**
Tasks 7 - 9	**Completed:** ▪ Not scheduled to start yet	**0%**

Technical Accomplishments and Progress: Membrane

System requires a high-efficiency membrane - DSM™

- **Superior Mechanical Properties**
  - No x-y dimensional changes upon wet/dry or freeze-thaw cycling
- Much Stronger Resistance to tear propagation
  - Superior to PTFE-based supports 10x stronger base properties
- **Improve MEA Mfg**
  - Ease of handling
  - Direct catalyst inking onto membranes
  - Low-cost, chemically-etched support
- **Improve Stack Seals**
  - Potential to bond support structures into bipolar frame to eliminate sealing issues
- **Customized MEAs**
  - Vary ionomer and thickness
  - Provide more support at edge regions and/or at ports
- **Related GES Project**
  - DE-FC36-08GO18065

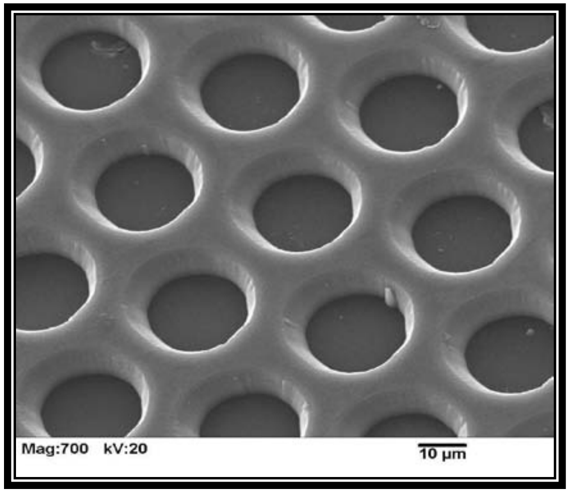


Figure 1. Scanning Electron Microscope (SEM) micrograph of the polymer membrane support structure with definable straight hole pattern

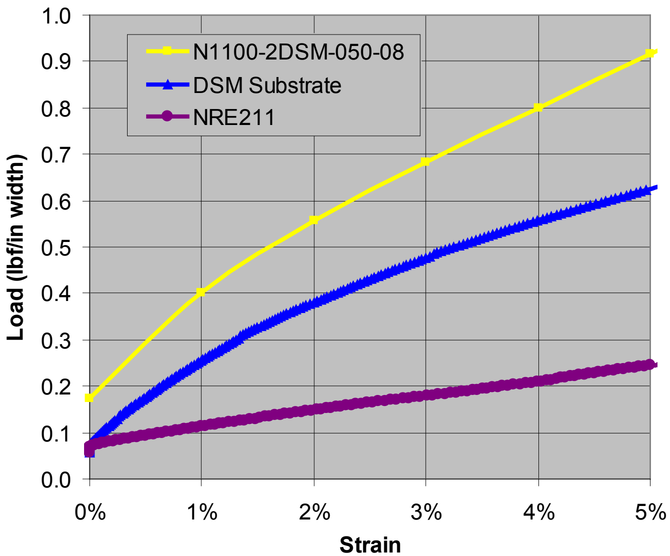
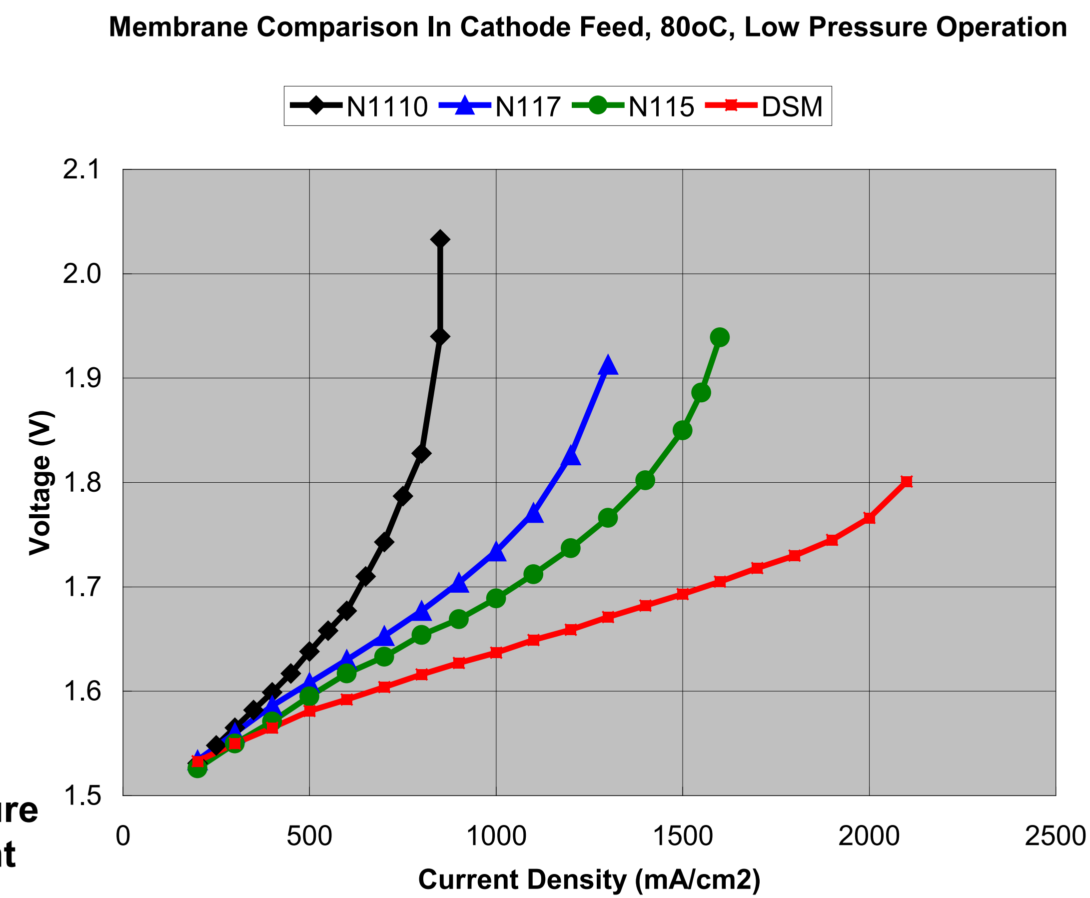


Figure 2. Dynamic Mechanical Analysis (DMA) shows the increased tensile strength of the DSM™ versus its components (wet at 80°C)

Demonstration of DSM™ in Cathode Feed

- **Cathode Feed**
  - System configuration advantages
  - Limits Max. current density
- **Performance of the Advanced DSM™ is superior to that of Nafion® 117 and 115**
- **Current Density Limits**
  - N1110 = 600 mA/cm^2
  - N117 = 900 mA/cm^2
  - N115 = 1200 mA/cm^2
  - DSM = 2000 mA/cm^2
- **High Pressure Operation**
  - Similar performance benefits measured at balanced pressure
  - Anticipate higher Max. current with differential pressure operation

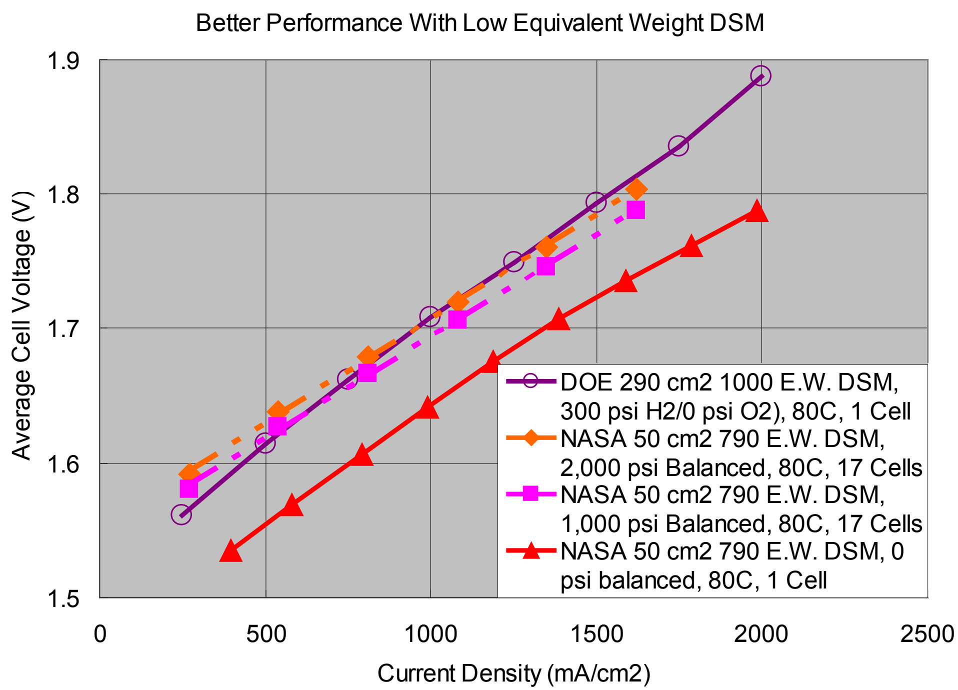


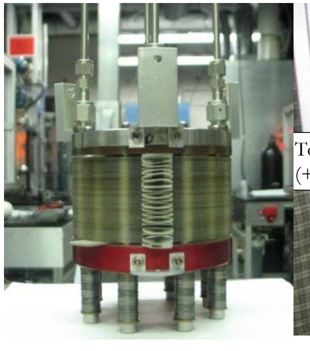
Demonstration of DSM™ in Pressure Dome

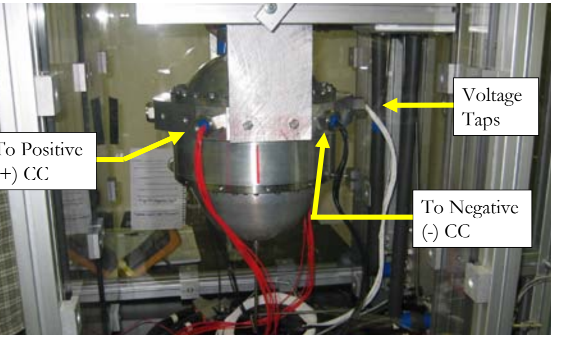
- **Successful Pumped Cathode Feed Operation of 50 cm^2 17-Cell Stack in 2000 psig Pressure Dome**

- **2 DSM™ Structures Shown**
  - **1 is "Standard" 1100 Equivalent Weight (E.W.) ionomer (for differential pressure operation)**
  - **1 is low-resistance 790 E.W. ionomer (for better electrical efficiency with no differential pressure operation)**

- **Results in Graph Show Lower Voltage At 1,000 mA/cm^2 With Low E.W. Ionomer at 1,000 psi Operation Than At Ambient Pressure**
  - **Equal performance at 1,000 mA/cm^2 and 2,000 psig operation**
  - **Over 500 mV better performance at 1,000 mA/cm^2 and 0 psig operation**







Preliminary Performance:
System Pressure Drop

- **Top Figure Illustrates High Pressure Drop in Cathode of Conventional Electrolyzer**
- **3 Features of HRA Low-Pressure Drop Operation**
  - **Efficient electrolyzer operation, to minimize heat generation**
  - **External cooling of stack, to minimize catholyte heating**
  - **Larger, low pressure-drop cathode compartment design, compared to anode compartment**
- **Results in Lower Figure Show Predicted Lower Pressure Drop**
  - **Natural convection supplies circulating water**
  - **Low resultant pressure drop**

Figure 1. Pressure Drop In Conventional (Pumped) Cathode-Fed Electrolyzer

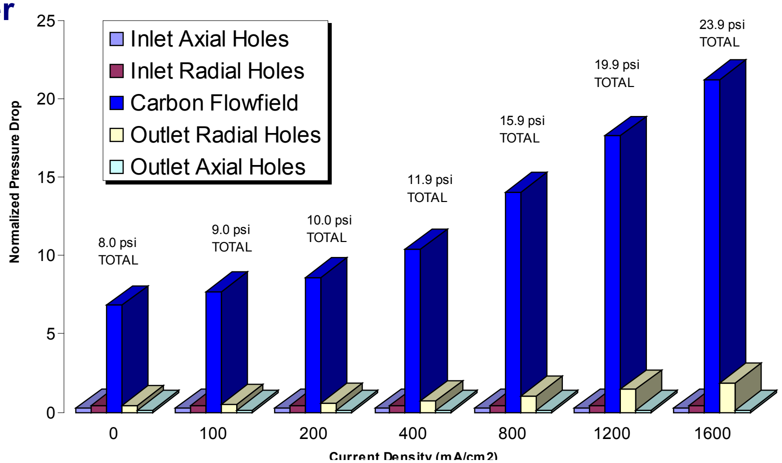
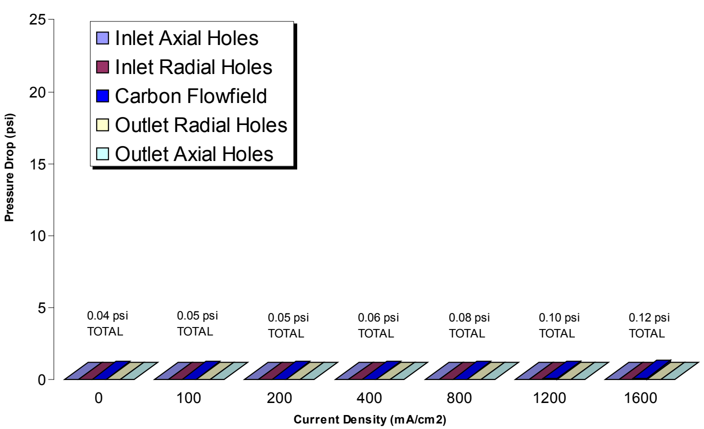
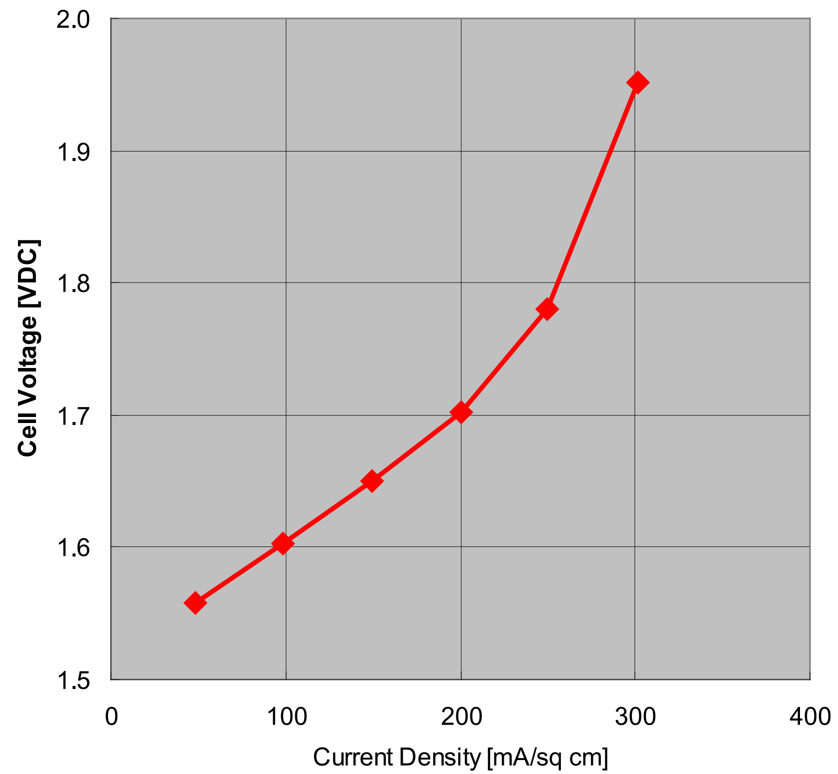


Figure 2. Predicted Pressure Drop In Natural Convection Cathode-Fed Electrolyzer



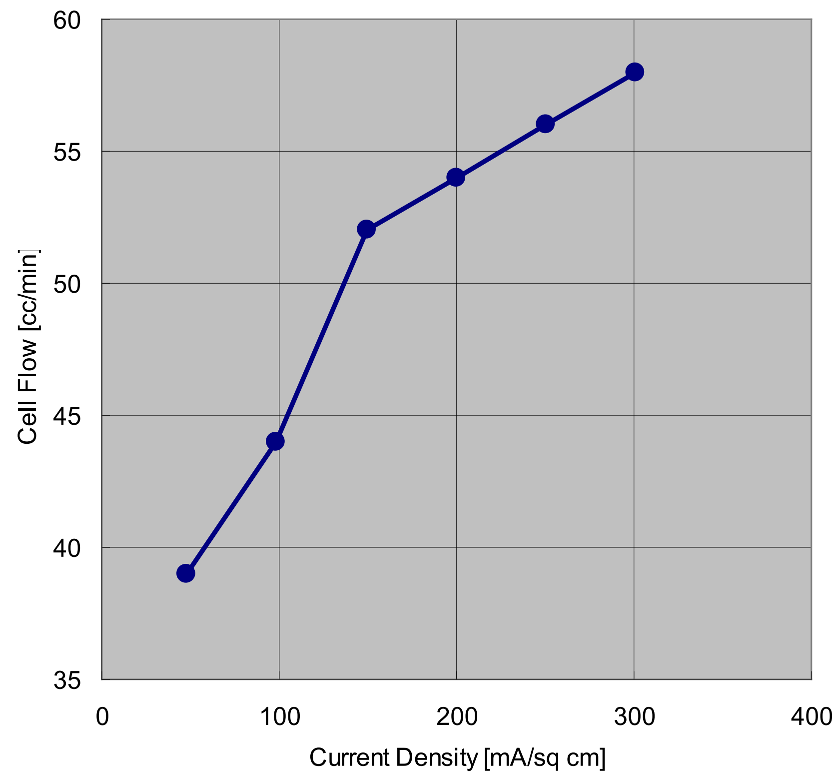
Thermosiphon HRA Single-Cell Tests

- Single-Cell Testing at 160 cm^2 Underway
  - GES-Treated Nafion® 115 Membrane, Standard Catalyst, Room Temperature Operation
- Maximum Current Density ≈ 300 mA/cm^2
  - Investigating Low Maximum Current Density
- Cathode Compartment Height Being Varied
  - 90 mil thick
  - 120 mil thick
- Increased Height Will
  - Decrease Pressure Drop
  - Permit Operation at Higher Current Densities



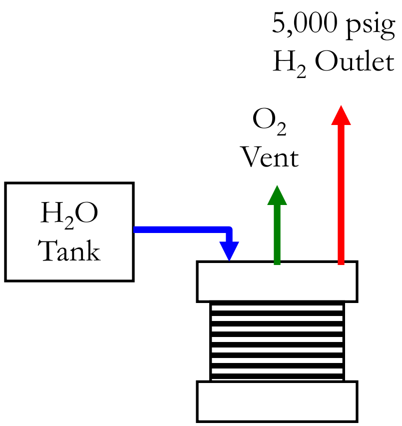
Thermosiphon HRA Single-Cell Tests

- Single-Cell Testing at 160 cm^2 Underway
  - No Circulation Pump – Thermosiphon Only
  - 90 mil Cathode Height
- Water Circulation Measured by Capturing Cathode Effluent Water ("Bucket Test")
- Relative Water Circulation Rate Decreases above 150 mA/cm^2
- Could Explain Low Limit to Current Density
- Increased Height Will
  - Decrease Pressure Drop
  - Permit Operation at Higher Current Densities



Static-Feed WaMM Membrane Development for HRA

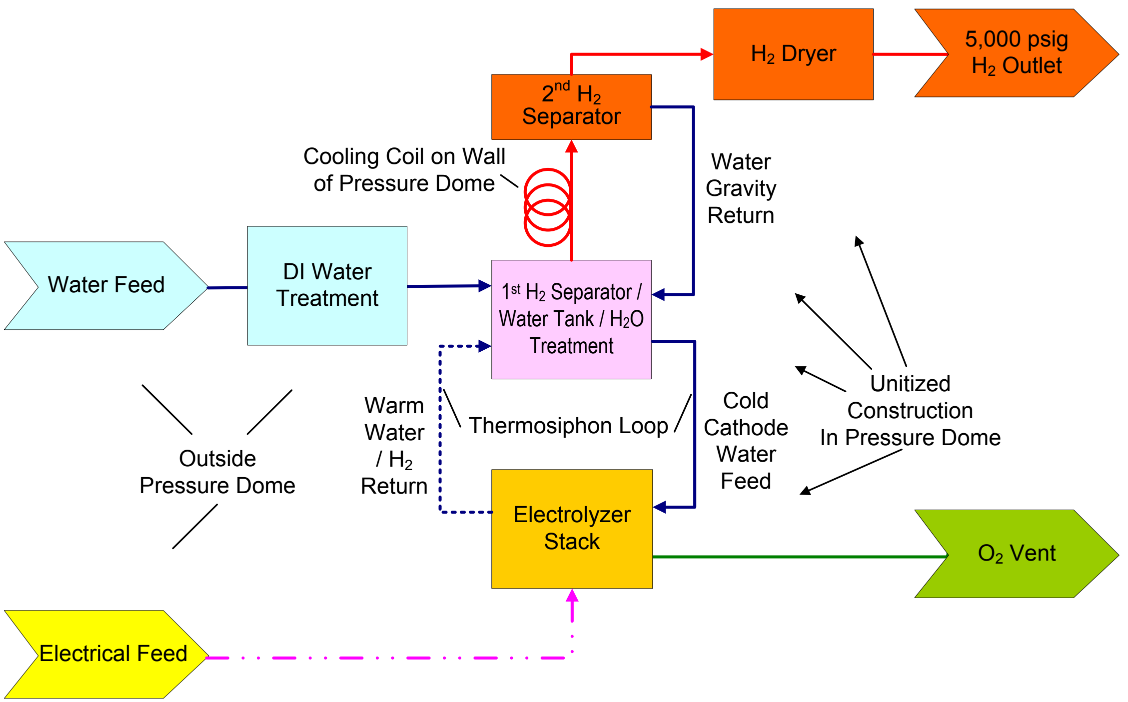
- NASA is Funding GES to Develop a Water Management Membrane (WaMM) Technology
  - WaMM originally for unitized regenerative fuel cell
- Advantages
  - No electrolyzer circulation pump – static water feed
  - Dry H_2 outlet – no separator required
  - Can use lower-quality water
- This Program Will Further Its Development As Risk Mitigation for Thermosiphon-Fed Electrolyzer
- Currently Fabricating 50 cm^2 Hardware to Test at 2,000 psig in Pressure Dome
- Testing Later in 2011



Static Water Feed Electrolyzer

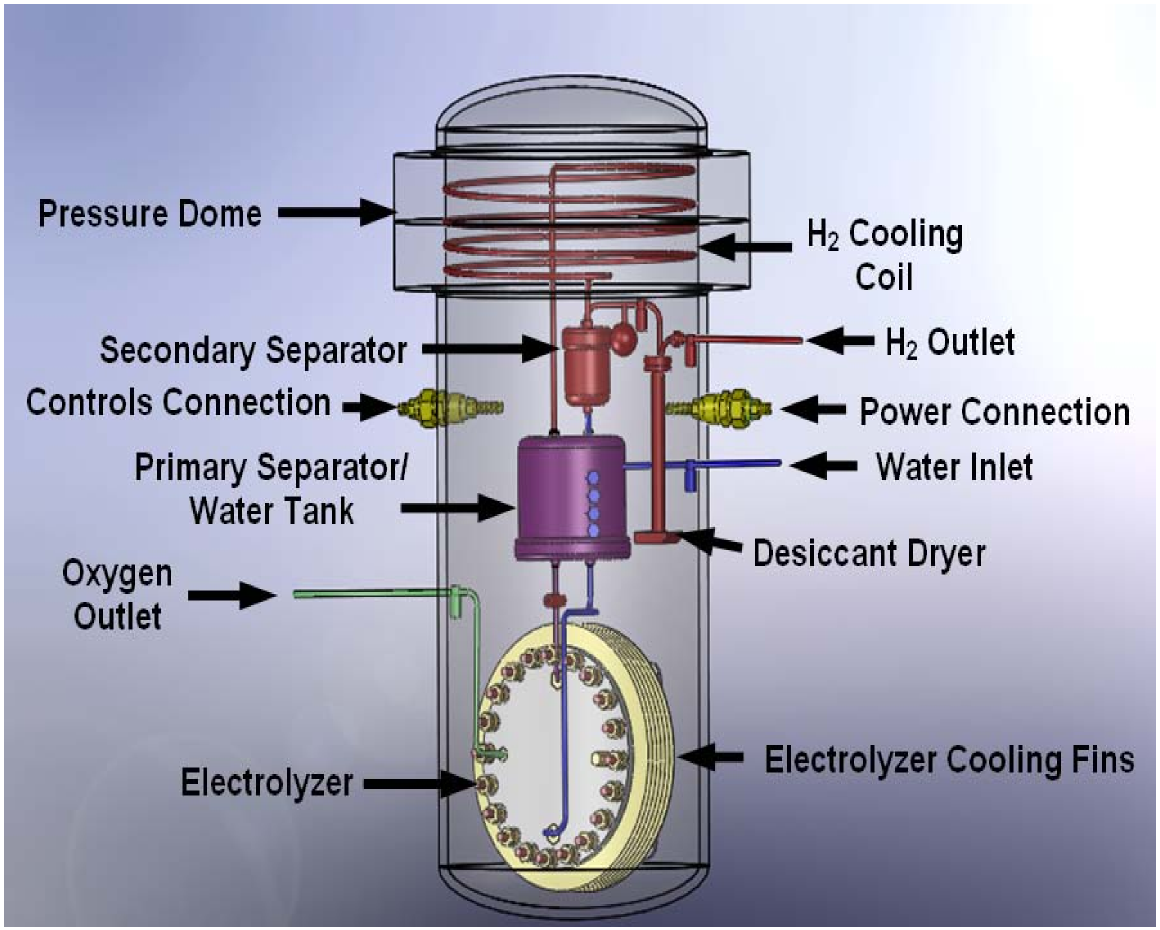
Progress: Preliminary System Design

- Preliminary P&ID, PFD Completed
  - Equipment and Flow Paths Determined
  - Instrumentation Selected
  - Flow Rates and Conditions Calculated
- System Layout Started
- Component Studies Planned
  - Electrolyzer Stack
  - Passive Stack Cooling
  - Prelim. Pressure Containment Dome
  - Passive Hydrogen Cooling
  - Regenerative Dryer
  - Cathode Circulation Thermosiphon (Natural Circulation)



Cathode Feed Process Flow Diagram

Progress: Phase I System Design
(Unitized Packaging Layout)



- Operates in Thermosiphon Cathode Feed Mode
- Low-Pressure Stack Hardware
  - Thin end plates
  - Machine bolts not specialty metal parts
  - Thermoplastic frames
- Utilize Pressure Inside Pressure Containment Dome
  - Minimizes stack compression needs
  - Benefits contact resistance
  - Allows use of unreinforced plastic frames
  - Enhances safety
  - Use unreinforced, low-cost components and piping

Progress: Inert Coating for Pressure Dome Internal Components

- To Provide Protective Coatings Over Low-Cost HRA Components (i.e. Carbon Steel Pressure Dome)
- Parylene Coated Samples from Speedline
  - Poly-para-Xylylene coating film formed by the chemical vapor deposition (CVD) process
  - Claimed to be pinhole-free
- Corrosion Test
  - Place SS coupon with 1 mil thick Parylene coating in 3 N H_2SO_4 and polarize sample to +1.3 V anodic vs. DHE
- Corrosion Test Results Showed Corrosion and Activity after 380 hours of exposure

Additional Inert Coating Work

- Thin Parylene Coating (1 mil) Not Adequate
- Thicker (25 – 40 mil) Coatings Used for Ultra-Pure Chemical Industry (i.e. Semiconductor)
  - PFA and E-CTFE offer low permeabilities
  - Flame spraying PEEK does not require an oven to cure coatings
- Thicker Coatings being Procured

Progress: Hydrogen Dryer

- Earlier Giner Dryers Used Type 4A Molecular Sieves as Sorbent
  - Require excessive (>400°F) regeneration temperatures
  - Results in long cycle times and excessive hydrogen purge loss during regeneration
- Alternate Sorbents Being Down-Selected
  - Lower regeneration temperatures/shorter cycle times
  - Type 3A Molecular Sieves, aluminosilicates
- Currently Preparing For Pressure-Swing Adsorbtion (PSA) Tests
  - Heat-free regeneration
  - Aluminosilicates are primary candidate sorbents (on order)
  - Hardware being procured/assembled
- Lab Tests Will Use Helium as a Surrogate Gas
  - Testing will cover 290 – 5000 psig gas pressure (full range of allowed vehicle tank pressure)
  - Brassboard prototype will dry product hydrogen

Progress: Residential H_2 Refueling Appliance Applicable Codes & Standards

- Prof. Zalosh – H_2 safety expert
- Reviewed National & International Codes & Standards
- Giner Invited to Contribute Comments to ISO/DIS 22734-2 Draft
- One Significant Concern
  - NFPA 52-2100, Chapter 9 (no indoor refueling)
  - International fire code – no impediment to indoor refueling
  - NFPA will be approached to resolve discrepancy

Design Progress: Codes Pertinent to Residential Hydrogen Refueling Systems

Component Examples

IEC 60335 Parts 1, 2, 3, 5
Household and Similar Electrical Appliances

IEC 60079-10-1: Explosive Atmospheres, Classification of Areas

ISO 4126-1, -2: Safety Devices for Protection Against Excessive Pressure: Valves & Rupture Disks

CSA America HGV 4.7-2009: Automatic Valves for Use In Gaseous Hydrogen Fueling Stations

SAE J2600: Compressed Hydrogen Fueling Receptacles

Electrolyzer System

ISO/DIS 22734-2:
Hydrogen Generators Using Water Electrolysis Process; Part 2: Residential Systems

Eventual UL and CSA Versions of **ISO/DIS 22734-2**

Residential Installation

NFPA 52-2010, Chapter 9:
GH2 Compression, Gas Processing, Storage, and Dispensing Systems

International Fire Code Section 2209:
Hydrogen Motor Fuel Dispensing and Generation Facilities

Vehicle Refueling

CSA America HGV 4.1-2009:
Hydrogen Dispensing Systems

International Fire Code Section 2209:
Hydrogen Motor Fuel Dispensing and Generation Facilities

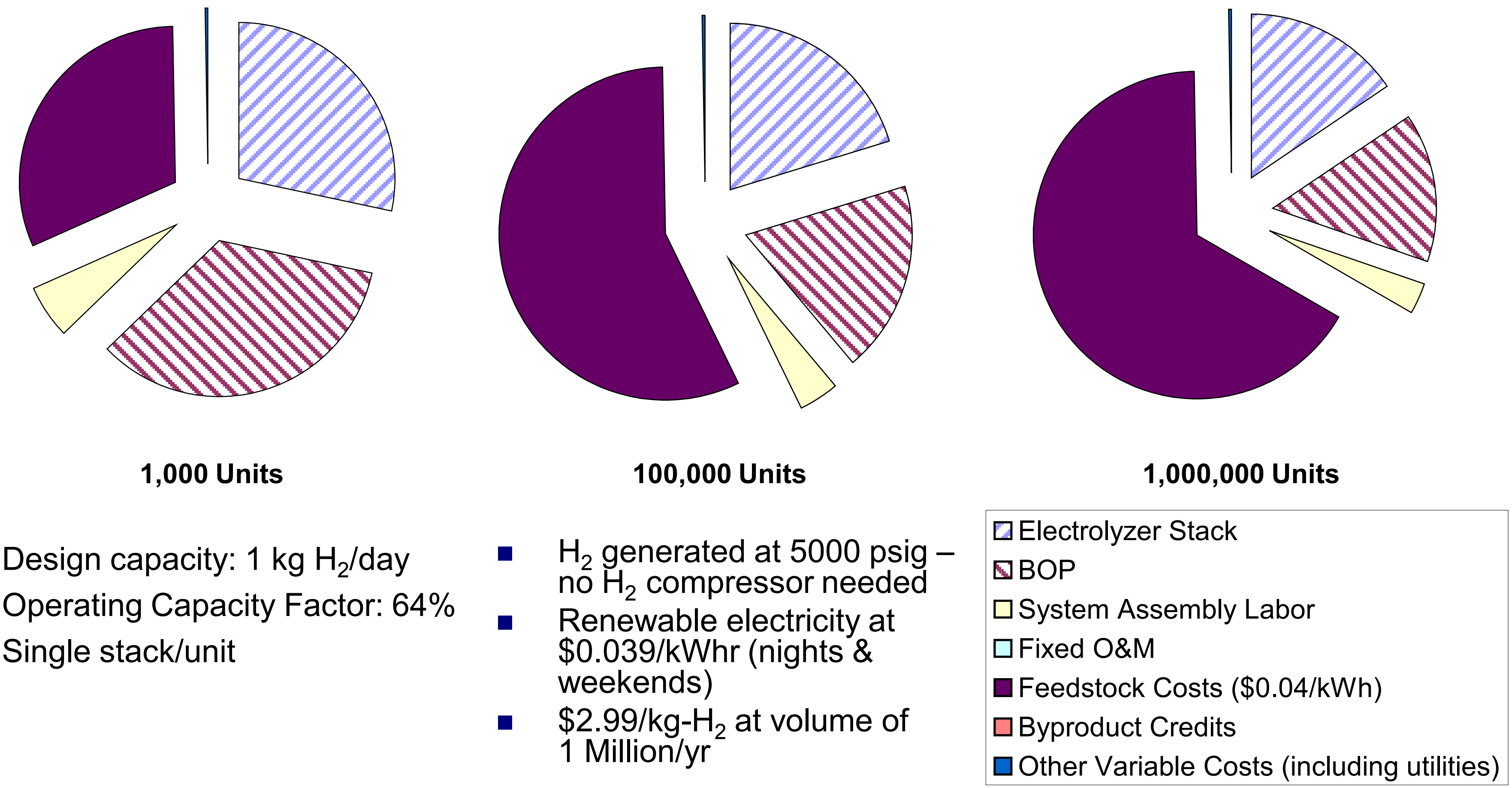
SAE TIR J2601
Compressed Hydrogen Fueling Protocol

Additional Codes/Standards

- Residential Installation and Vehicle Refueling
  - NFPA 55, Standard for Storage, Use and Handling of Compressed Gases and Cryogenic Fluids in Portable and Stationary Containers, Cylinders and Tanks
  - International Fire Code Section 3005, Use and Handling of Compressed Gases
  - International Fire Code Section 3503, General Requirements, Flammable Gases
  - CGA G-5.4, Standard for Hydrogen Piping Systems at Consumer Locations (Compressed Gas Association)
  - CGA G-5.5, Hydrogen Vent Systems (Compressed Gas Association)
  - SAE J2600, Compressed Hydrogen Surface Vehicle Refueling Connection Devices
  - ISO 17268:2006, Gaseous Hydrogen Land Vehicle Refueling Connection Devices
- Additional Codes Need Consideration
  - Proposed ASTM Analysis Methods for Hydrogen Purity, etc.

Design Progress: Projected H_2 Cost

H2A Model Analysis (Forecourt Model rev 2.1.1)



- Design capacity: 1 kg H_2/day
- Operating Capacity Factor: 64%
- Single stack/unit

- H_2 generated at 5000 psig – no H_2 compressor needed
- Renewable electricity at $0.039/kWhr (nights & weekends)
- $2.99/kg-$H_2$ at volume of 1 Million/yr

Collaborations

- Professor Robert Zalosh
  - Vendor
  - University
  - Review of applicable codes and standards
  - Assist with HAZOP/FMEA safety analysis
- IAS, Inc.
  - Vendor
  - For-profit company
  - Will develop low-cost controller prototypes
  - Will assist with control system development and projecting production costs
- GES, LLC (DOE Cost-Shared Grant DE-FC36-08GO18065)
  - Same Company
  - For-profit company
  - Within DOE H_2 program
  - Multiple overlapping components and subsystems [also Parker, 3-M (NSTF Catalyst & Membrane) and Entegris (Carbon Cell Separators)]
- GES, LLC (Government and Private Electrolyzer Development Programs)
  - Same Company
  - For-profit company
  - Outside DOE H_2 program
  - Several NASA programs, one DARPA Prime Contractor, electrolyzers for several private companies

Proposed Future Work (This Year and Next)

- Detailed HAZOP/FMEA Analysis of Hydrogen Refueling Appliance
- Test Full-Scale Home Refueling Appliance (HRA) Electrolyzer Stack
- Optimize Selection of Protective Coating for Pressure Containment Dome Internals
- Build/Test 5,000 psig Pressure Swing Absorber Dryer
- Complete Design, Fabrication & Demonstration of Unitized HRA System
- Preliminary Design and Economic Analysis of Commercial HRA System
- Identify & Team With Commercialization Partner(s)

Summary

- Innovative System Design
  - No compressors, pumps, or fans required; only one pressure vessel
  - Reduces costs (capital, operating & maintenance)
  - Improves reliability, safety, efficiency
- Innovative High-Strength Low-Permeability Supported Membrane Required
  - Advanced DSM™
  - High efficiency
- Testing Progress
  - Thermosiphon feed electrolyzer testing underway (testing at full-scale 160 cm^2 unit size)
  - 2,000 psig pumped cathode feed electrolyzer tests in pressure containment dome complete
  - Hardware being fabricated for WaMM static feed electrolyzer tests at 2,000 psig in pressure dome (risk mitigation and cost comparison)
  - Protective coating coupon tests ongoing
  - Pressure swing dryer components/sorbent being procured
- Codes & Regulations & HAZOP/FMEA Analysis Ongoing
- "Unitized" Breadboard HRA System Design Begun
- Hydrogen Costs Meet DOE Target of $2 - $4/kg
  - Will require significant sales volumes