

Development and Validation of a Two-phase, Three-dimensional Model for PEM Fuel Cells

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FC027

Overview

Timeline

- Project start date: 10/1/09
- Project end date: 9/30/12
- Percent complete: ~85%

Budget

- Total project funding (over 3 years)
 - DOE share: \$2.246M
 - Contractor share: \$238K
- Funding received in FY11:
\$798K
- Funding for FY12:
\$400K

Barriers

- Barriers addressed
 - Performance
 - Cost

*The validated PEM fuel cell model can be employed to **improve** and **optimize** PEM fuel cells **design** and **operation** and thus address these two barriers.*

Partners

- Direct collaborations with Industry, University and other National Labs:
Nissan (no cost), Ballard
Penn State University
LANL, LBNL.
- Project lead: Sandia National Labs



Objective/Relevance

- The project objective is twofold:
 - 1) to **develop** and **validate** a **two-phase, three-dimensional** transport **model** for simulating **PEM fuel cell** performance;
 - 2) to **apply** the validated PEM fuel cell **model** to **improve fundamental understanding** of key phenomena involved and to **identify performance-limiting phenomena** and **develop recommendations** for improvements so as to **address technical barriers** and **support DOE objectives**.
- The **coupled DAKOTA/PEMFC model** computational capability can be employed to **improve** and **optimize PEM fuel cell design** and **operation**. Consequently, the project helps **address** the **performance** and **cost** technical barriers since **improving performance** will **reduce cost**, for example, by **using less materials** (e.g., catalyst) or **minimizing operation cost** (e.g., reduce pumping power).

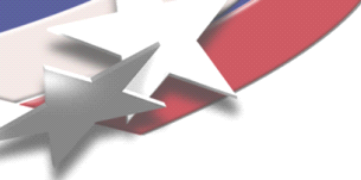
Approach

Our approach is both **computational** and **experimental** with active **participation from industrial partners**:

- Numerically, develop a **two-phase, 3-D, transport model** for simulating PEM fuel cell performance.
- Experimentally, measure **model-input parameters** and generate **model-validation data**.
- **Perform model validation** using data available from literature and those generated within the team.
- Apply the validated model **to identify performance-limiting phenomena** and **develop recommendations** for improvements.

What distinguishes the present work and previous efforts?

- Couple the **PEMFC model** with **DAKOTA** (toolkit for design/optimization) to perform **computational DOE** (design of experiments) and **3-D detailed probing, sensitivity** and **variability** analyses, and **parameter estimation**.
- **Collaboration** with and **participation** by industry partners, **Ballard & Nissan**, **ensure** that the PEMFC model can be used as a **practical design tool**.

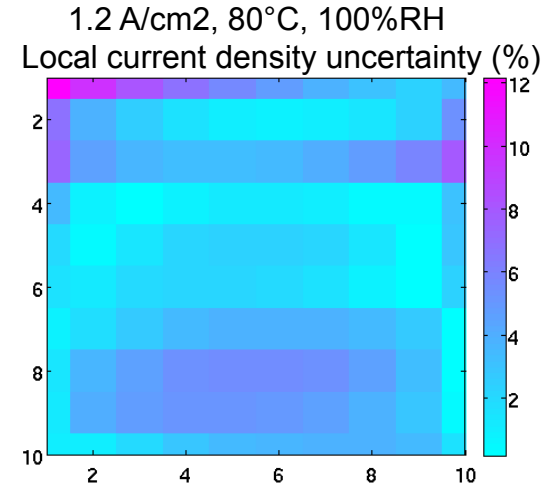
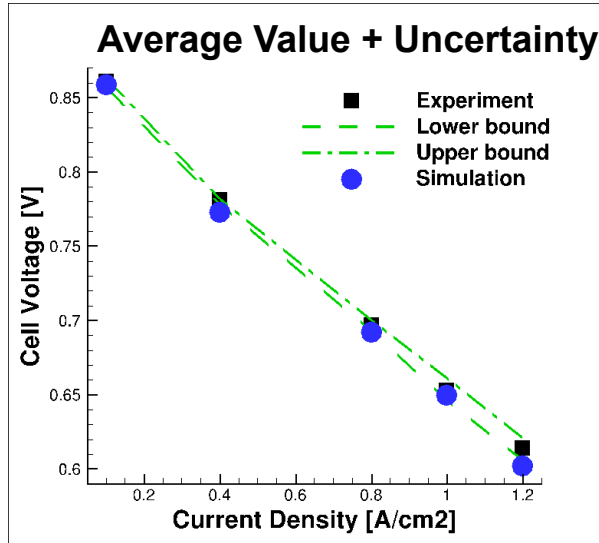
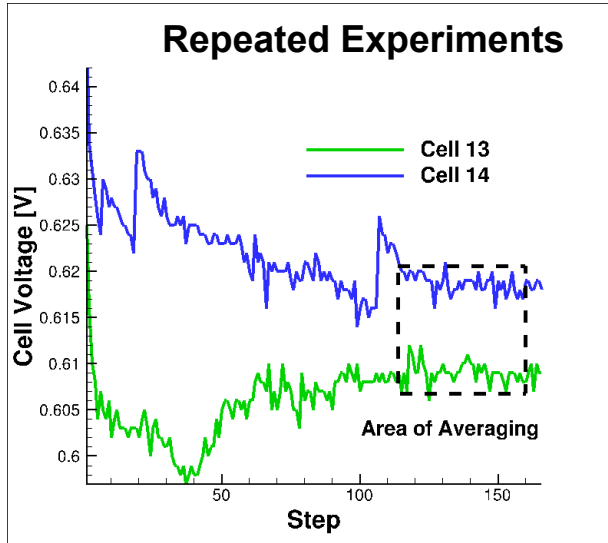


Approach

FY12 Milestones, and Current Status

M/D/Y	Milestone Descriptions	Comments
1/31/12	Perform the validation of the 3-D, partially two-phase, single-cell PEM fuel cell model. Status: completed .	At 80 C validation was acceptable. At 60 C some current over-prediction at high current density (slide 9)
5/31/12	Validate model under real-world conditions and architectures using data from Ballard and Nissan for non-automotive and automotive applications. Goal is to predict experimental current, temperature and cell voltage within 20% or as defined otherwise by Ballard and Nissan. Status: 50% complete .	Nissan collaboration resulted in new sub-models for low Pt loading. Ballard model validation will measure model capability under realistic operating conditions.
7/31/12	Validate fully two-phase, 3-D cell model with microporous layer effect using neutron imaging data. Status: 50% complete .	Direct validation of through-plane liquid water predictions will increase model credibility.
9/30/12	Generate test suite for PEM fuel cell model and create user manual. Status: 25% complete .	These deliverables will enable the model to be run by researchers and industry.

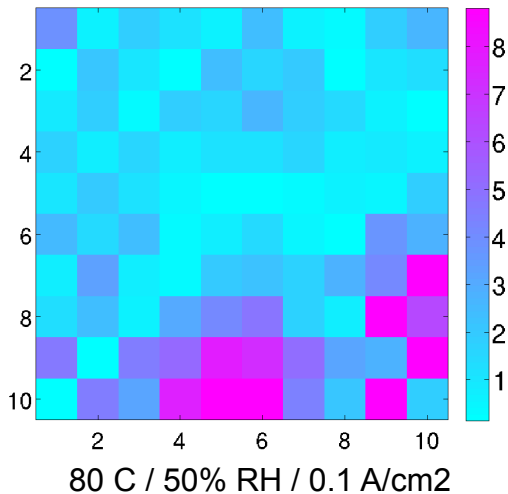
Technical Accomplishment: Uncertainty Quantification of Experiments / Simulations



Repeated experiments (80°C, 100%RH) enables estimation of **uncertainty bounds** on cell voltage and current density

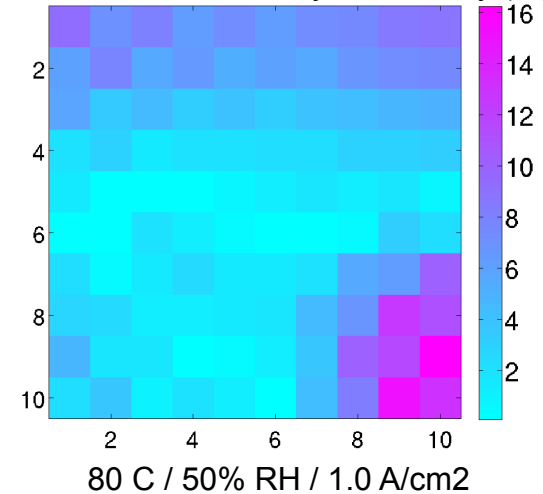
Uncertainty (percent difference) from numerical errors in computations was also quantified using multiple meshes

Local current density uncertainty (%)



Uncertainty (variability between repeated experiments) in local quantities like **local current** (10-15%) can be much higher than for integrated quantities like cell voltage (<5%). Numerical uncertainty (error) can be up to 10-15%.

Local current density uncertainty (%)



Technical Accomplishment: Validation of Segmented Cells: Cell Voltage

Operating Conditions: (Co-flow)

$I = 0.1, 0.4, 0.8, 1.2 \text{ A/cm}^2$

$T_{\text{cell}} = 60, 80 \text{ C}$, $P_a = P_c = 25 \text{ psig}$

Inlet %RH(a/c) = 25, 50, 75, 100

$St(a/c) (H_2/air) = 1.2/2.0$

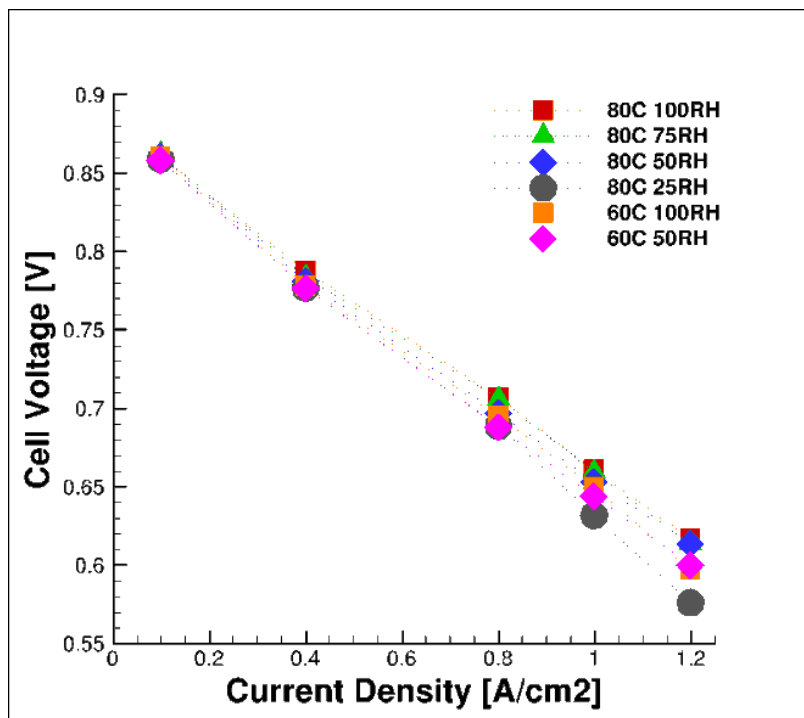
Cell Geometry:

Membrane: 18 μm CL(a/c): 7/12 μm

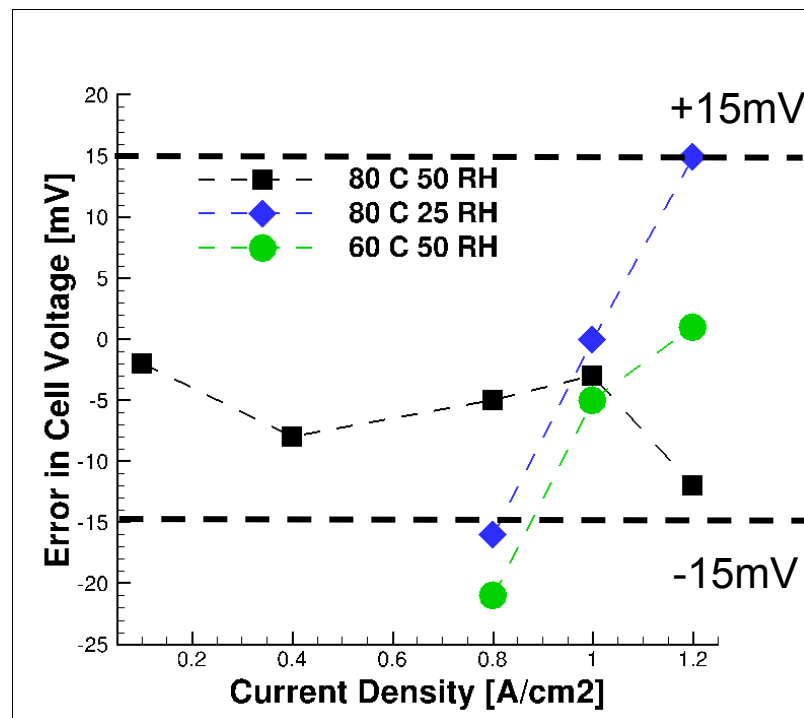
MPL: 40 μm GDL: 160 μm

GFC: 1 \times 1mm Land: 1.1mm

Cell active area: 50 cm^2



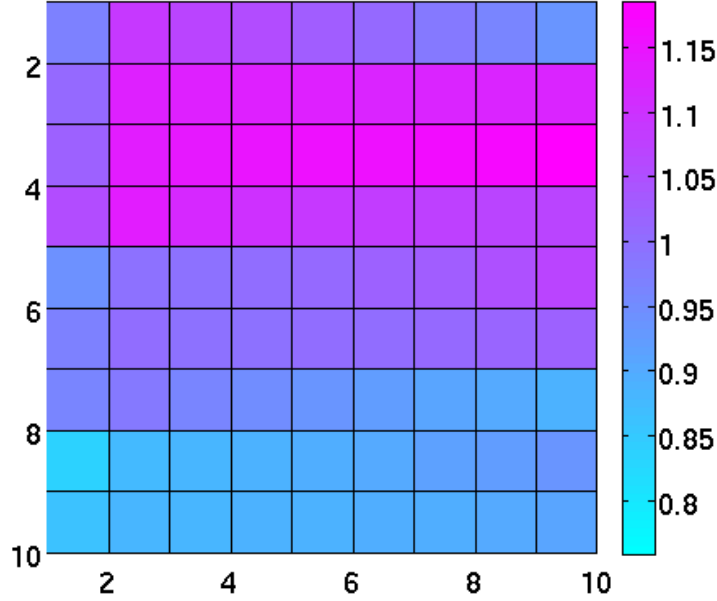
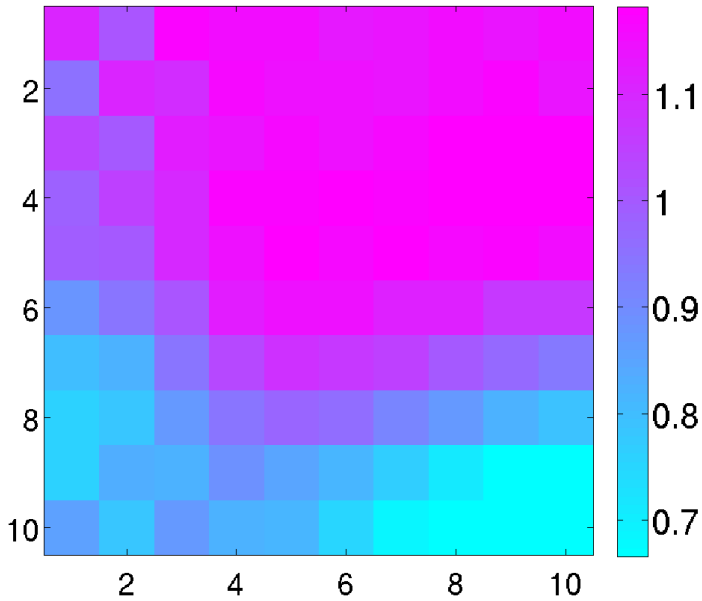
Experimental polarization curves for all 6 operating points. Based on averages of two repeated experiments.



Model validation estimated the cell voltage to within +/-15 mV. Largest errors occurred at high current and at low temperature and relative humidity (RH).



Technical Accomplishment: Qualitative Validation of Segmented Current Density

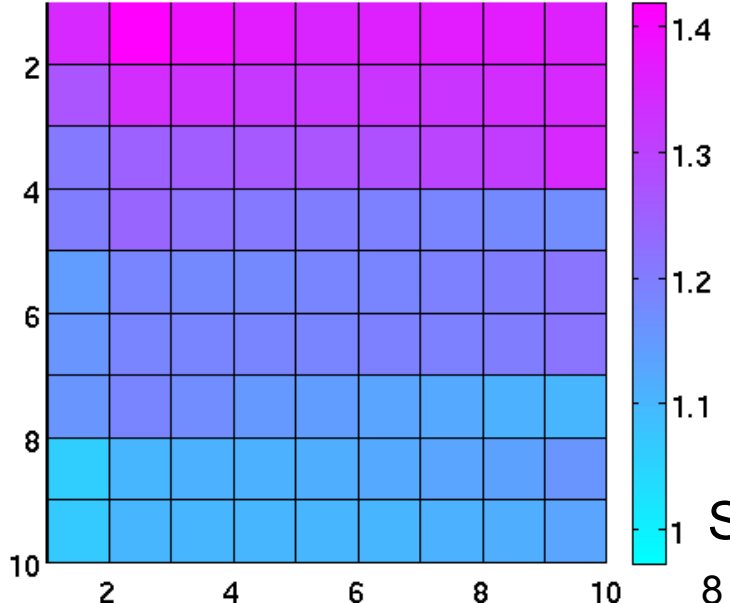
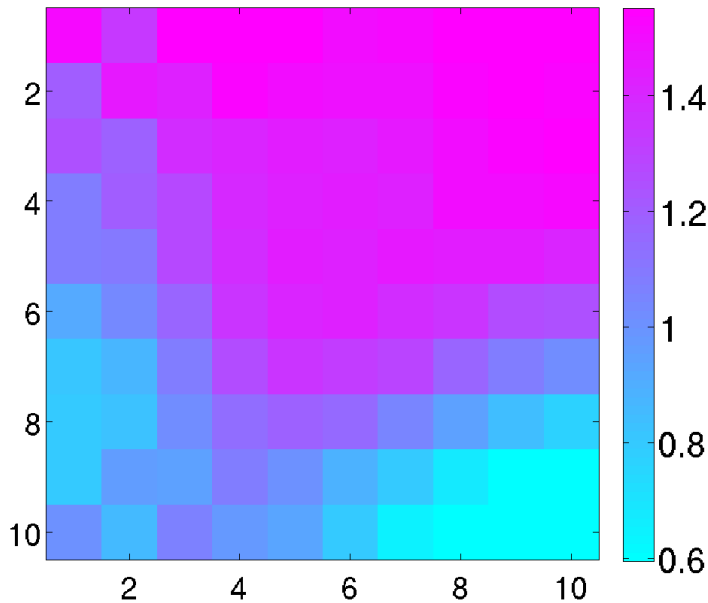


Comparison of local current density profiles at 80C / 50RH / 1.0 A/cm². Note the similar location of the maximum current

Sim

Exp

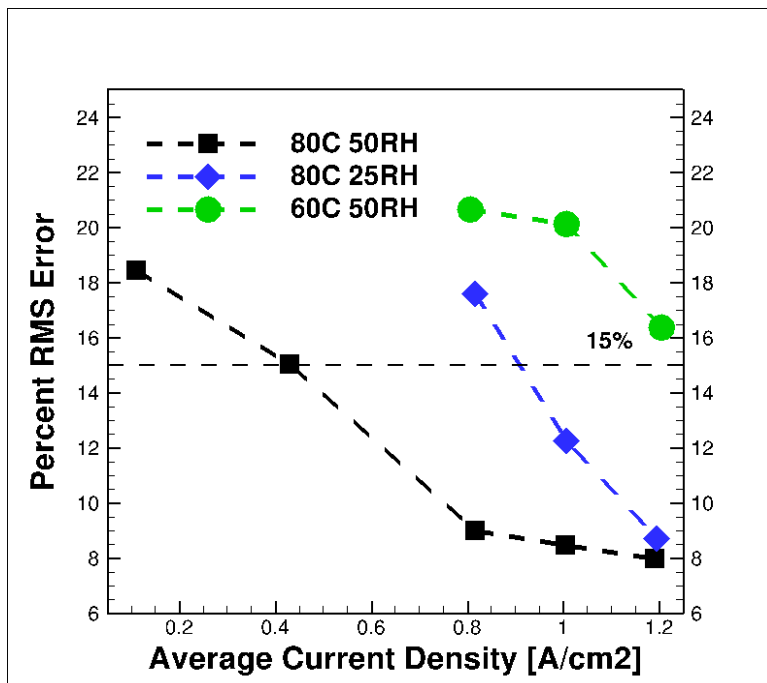
Comparison of local current density profiles at 60C / 50RH / 1.2 A/cm². Note the similar location of the maximum current



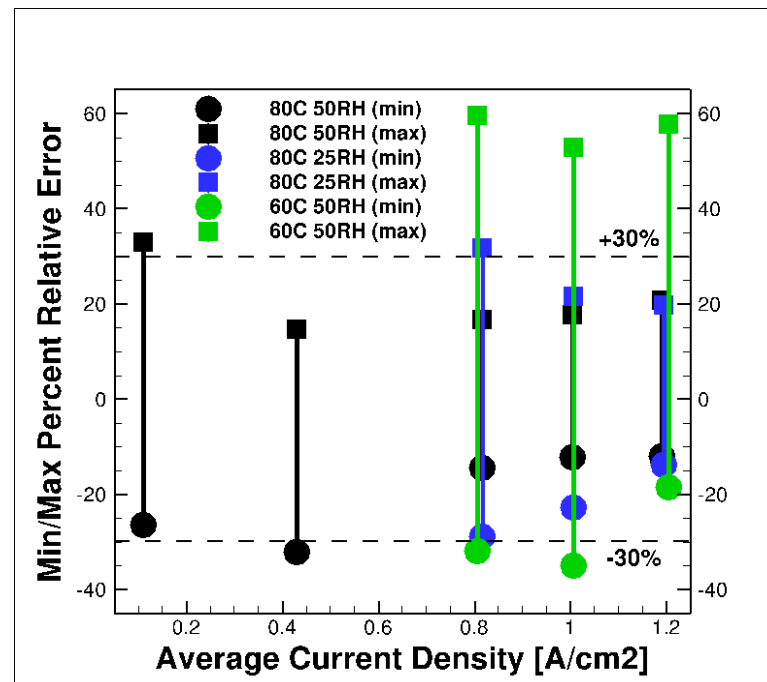
Exp

Sim

Technical Accomplishment: Quantitative Validation of Segmented Current Density



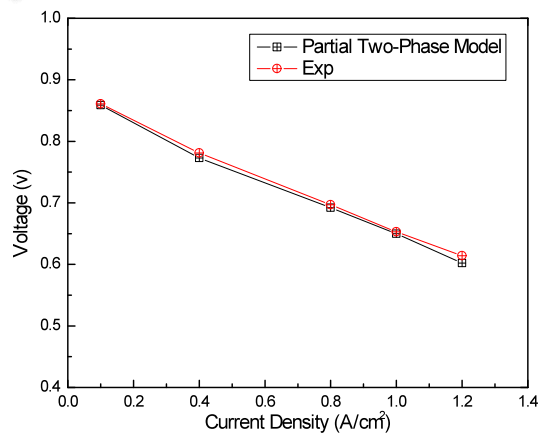
Validation using **RMS error in local current density** between simulation and experiment at multiple operating conditions.



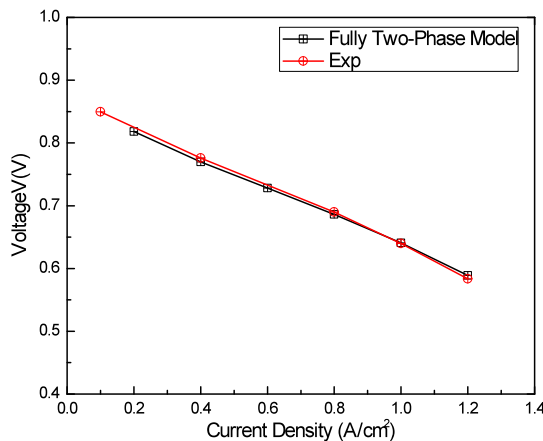
Validation using **min/max local error** (5/95 percentile) at multiple operating conditions. This shows the largest local error, with over- or under-prediction indicated by a positive or negative sign.

Local current density model predictions were **validated at 80C / 50RH and 80C / 25RH** (within acceptable bounds). At 60C / 50RH the model may over-predict the local current density. Further work is needed for validation under low temperature operation.

Technical Accomplishment: Comparison Between Partial and Fully Two-Phase Model



(a) Partial Two-phase Model



(b) Fully Two-phase Model

Polarization comparison between model predictions and measurement

Operating Conditions:

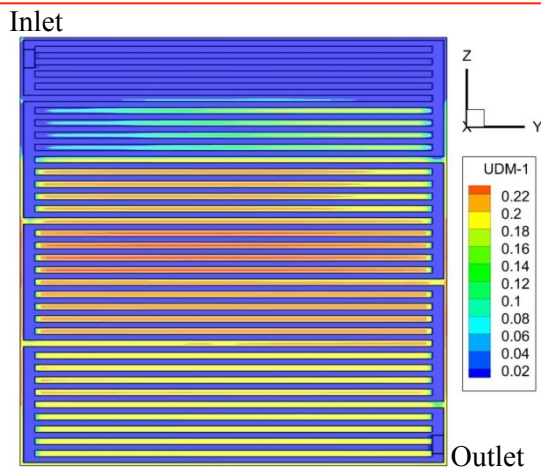
$$St(a/c) = \underline{1.2/2.0} \text{ (H}_2\text{/air)}$$

$$P_a = P_c = \underline{200\text{kPa}}$$

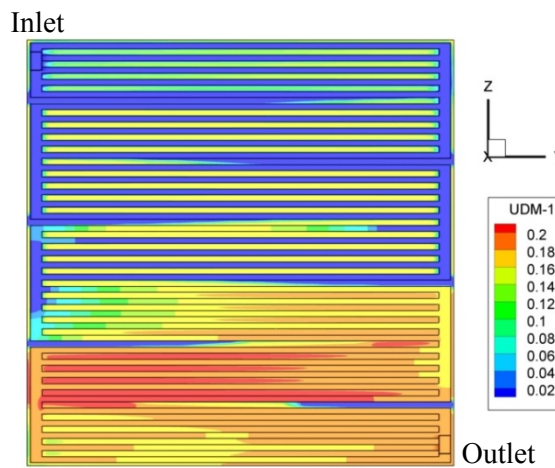
$$T_{\text{cell}} = \underline{80\text{ }^\circ\text{C}}$$

$$\text{Inlet \%RH(a/c)} = \underline{50.0/50.0}$$

- ◆ Only small difference in polarization prediction between the two models for this 50 cm² cell.
- ◆ However, the fully two-phase model predicts liquid water in the gas channels comparing to partially two-phase model.
- ◆ Liquid water predicted by partial two-phase model covers regions only under the bipolar plate.
- ◆ While liquid water predicted by fully two-phase model appears under both bipolar plate and gas flow channel, especially in the downstream regions near the outlet.



(a) Partial Two-phase Model

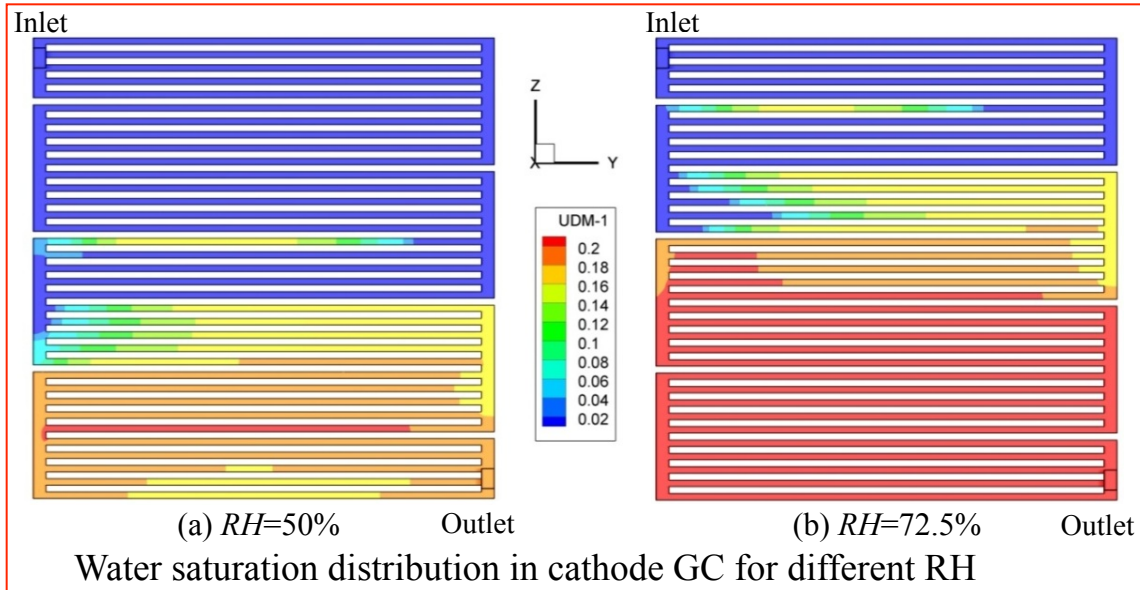


(b) Fully Two-phase Model

Water saturation distribution at cathode gas flow channel/GDL interface

Technical Accomplishment: Case Study

Using Fully Two-Phase Model For Segmented Cell

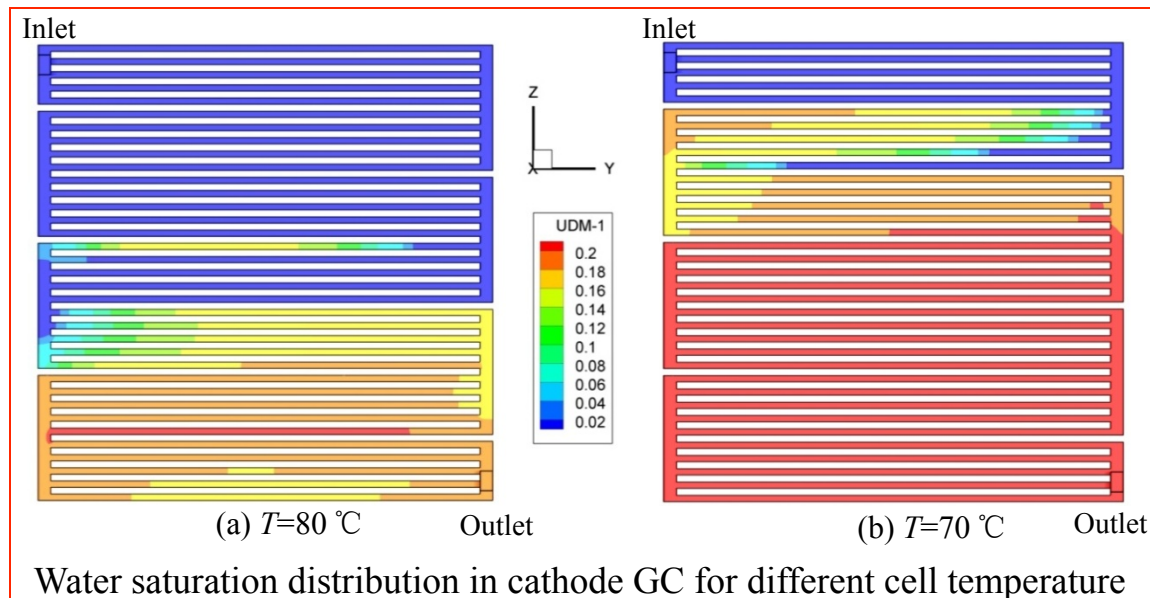


Operating Conditions:

$$St(a/c) = 1.2/2.0 \text{ (H}_2\text{/air)}$$

$$P_a = P_c = 200\text{kPa}$$

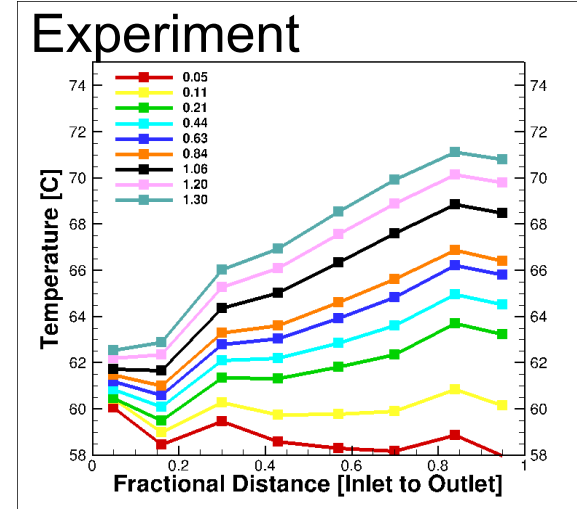
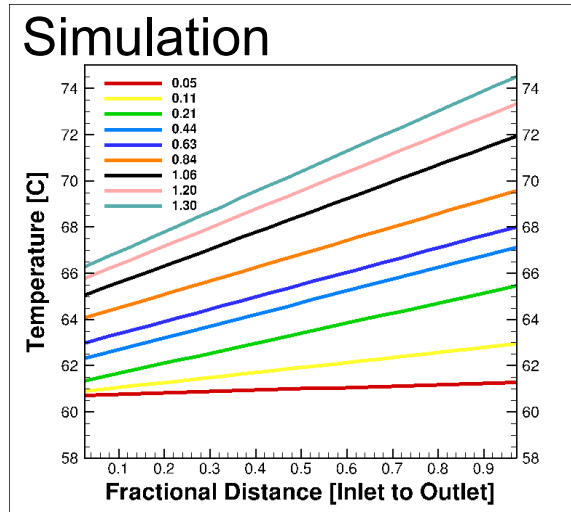
$$CD = 0.8\text{A/cm}^2$$



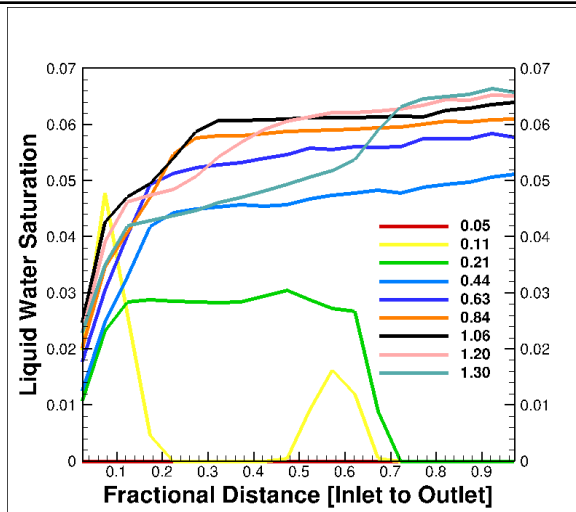
- ◆ **More liquid water appears in the gas flow channel with higher inlet relative humidity.**
- ◆ **For lower operating temperature, more liquid water is accumulated inside gas flow channels since low temperature are prone to condensation.**

Technical Accomplishment: Ballard Stack Model (Single Channel)

Validation of
average
temperature
down the
channel at
various current
densities



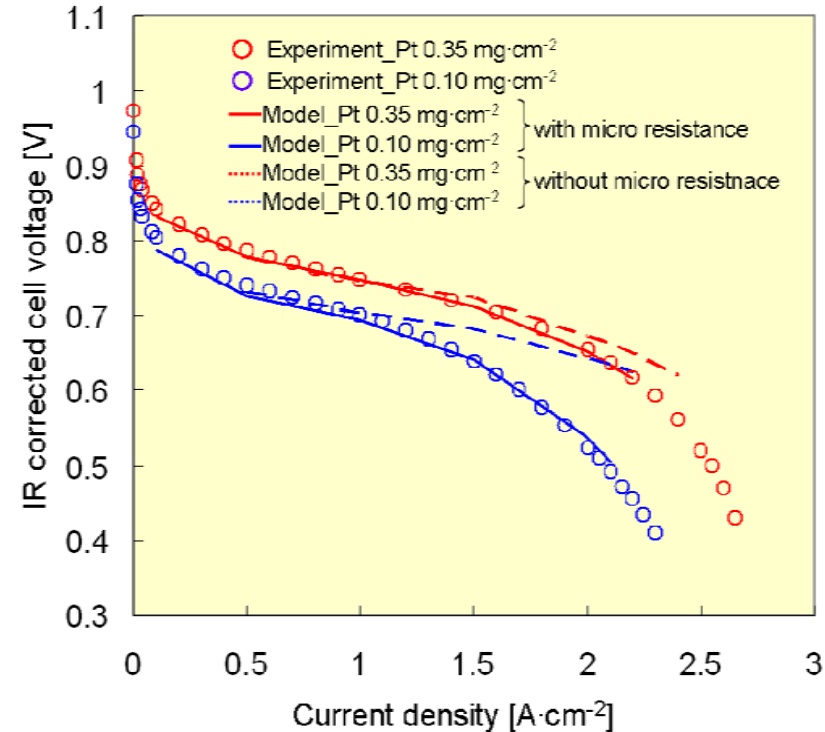
Simulation of average saturation
(cathode catalyst layer) at various current densities



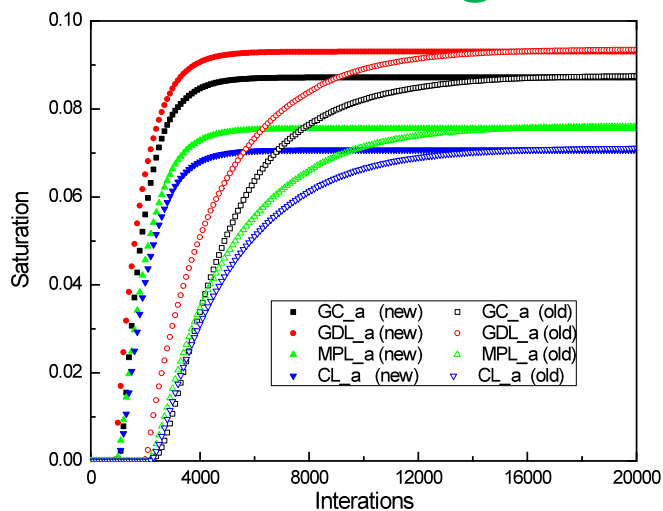
- Current model is complete and being run by Ballard.
- Prediction of main variables (voltage, local current, temperature, and reactants) has been demonstrated.
- **Validation** of the model predictions for local current, local temperature and polarization is **on track** for completion this year.
- Model for neutron imaging is currently being built.

Technical Accomplishment: Nissan Collaboration and Model Validation

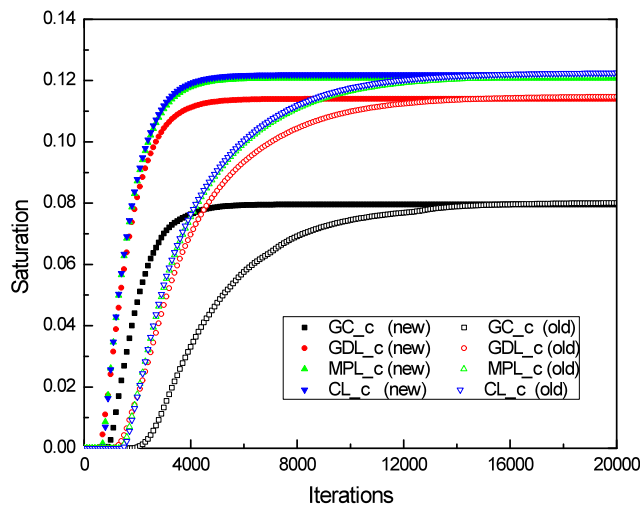
- The team is working closely with Nissan to explore the model application to automobiles.
- Nissan sent a visiting scientist to stay at PSU for one year to collaborate on this project.
- Preliminary success has been achieved by Nissan engineers to modify PSU's two-phase code for predicting fuel cell performance with low-Pt loading catalyst layer, as shown in the figure on the right.



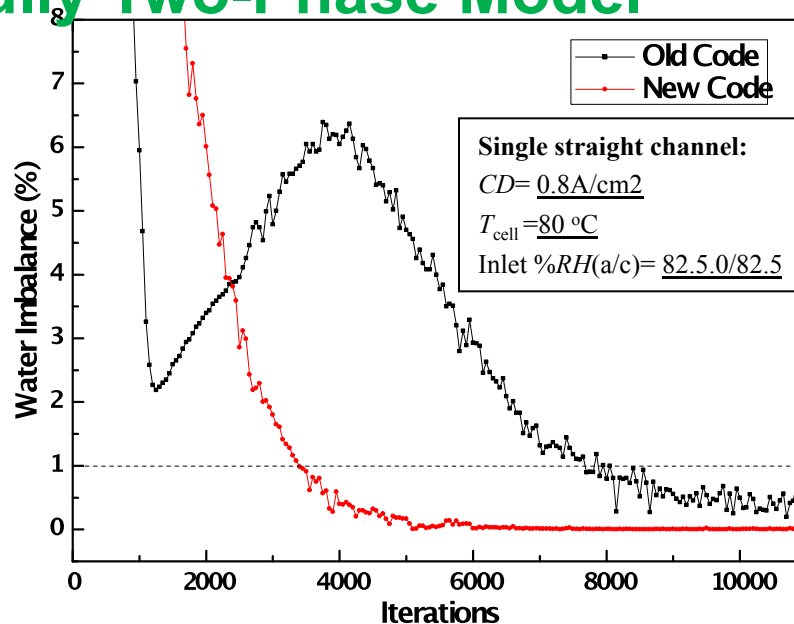
Technical Accomplishment: Improved Convergence for Fully Two-Phase Model



Avg. saturation vs. iteration at **Anode side**



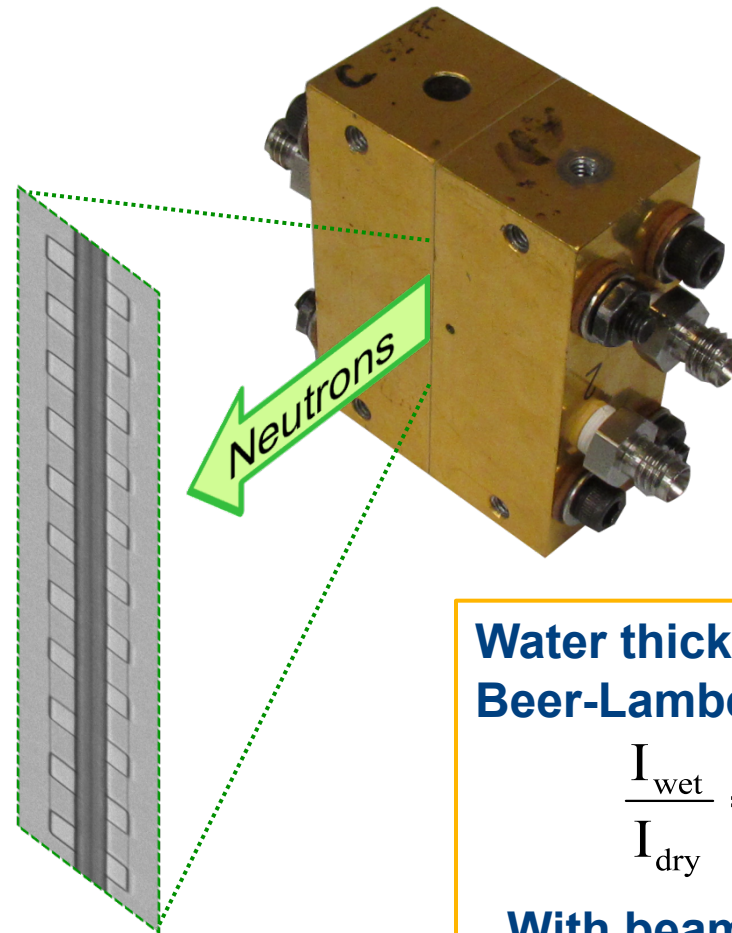
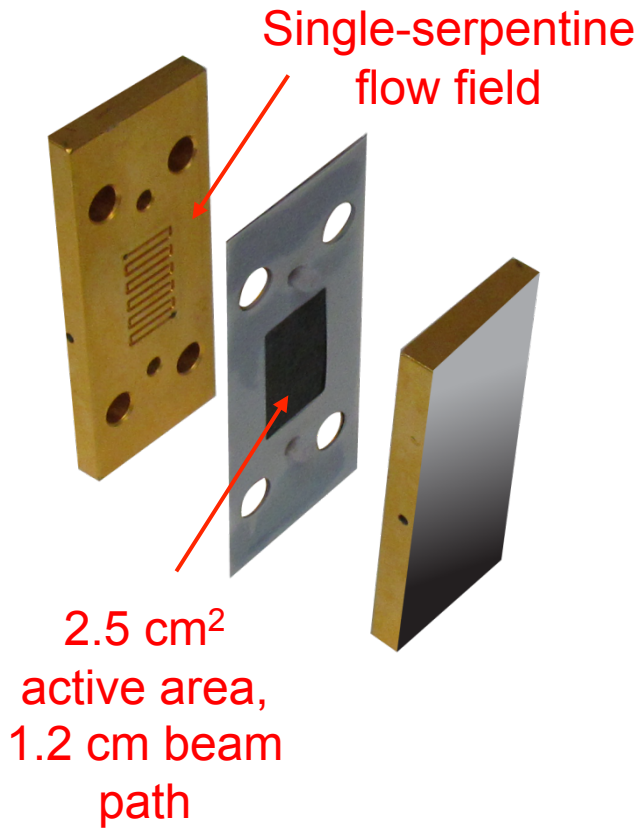
Avg. saturation vs. iteration at **Cathode side**



Water Balance for Channel M2 Model

- ◆ Water saturation convergence at both anode and cathode sides is greatly improved for the latest code.
- ◆ For a typical case, water saturation converges within about 4,000 iterations for latest code, while it needs about 12,000 iterations for previous version. Thus the simulation time is cut by two thirds.
- ◆ The water imbalance reaches 1% around 3500 iterations for the latest code, while it needs more than 8,000 iterations for previous code.

Technical Accomplishment: High-resolution (13 μm) Through-Plane Neutron Imaging



In situ evaluating water
content through the
thickness.
Varied current density
(0.4, 0.8, 1.2 A/cm²) and
RH (50 and 100%)

Water thickness “t” from
Beer-Lambert law:

$$\frac{I_{\text{wet}}}{I_{\text{dry}}} = e^{-\mu t}$$

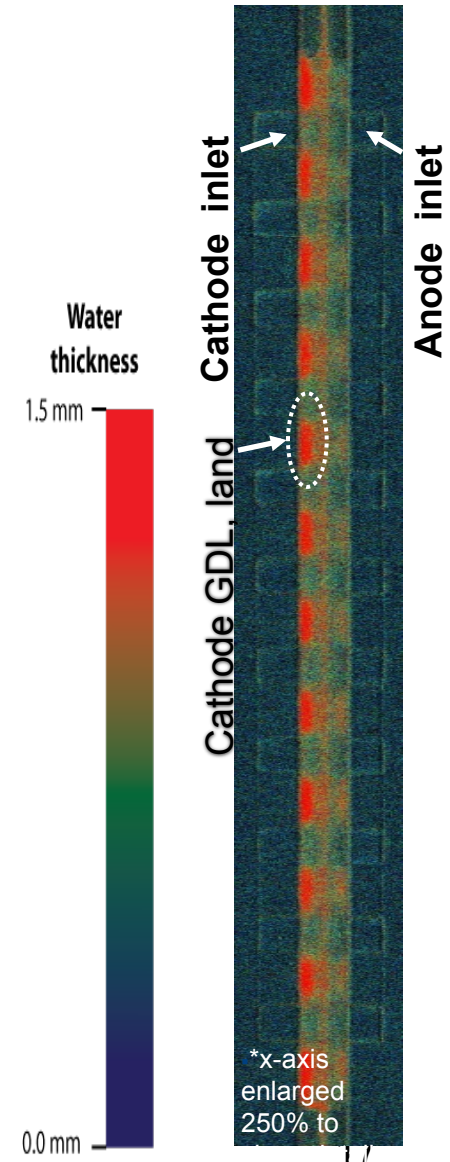
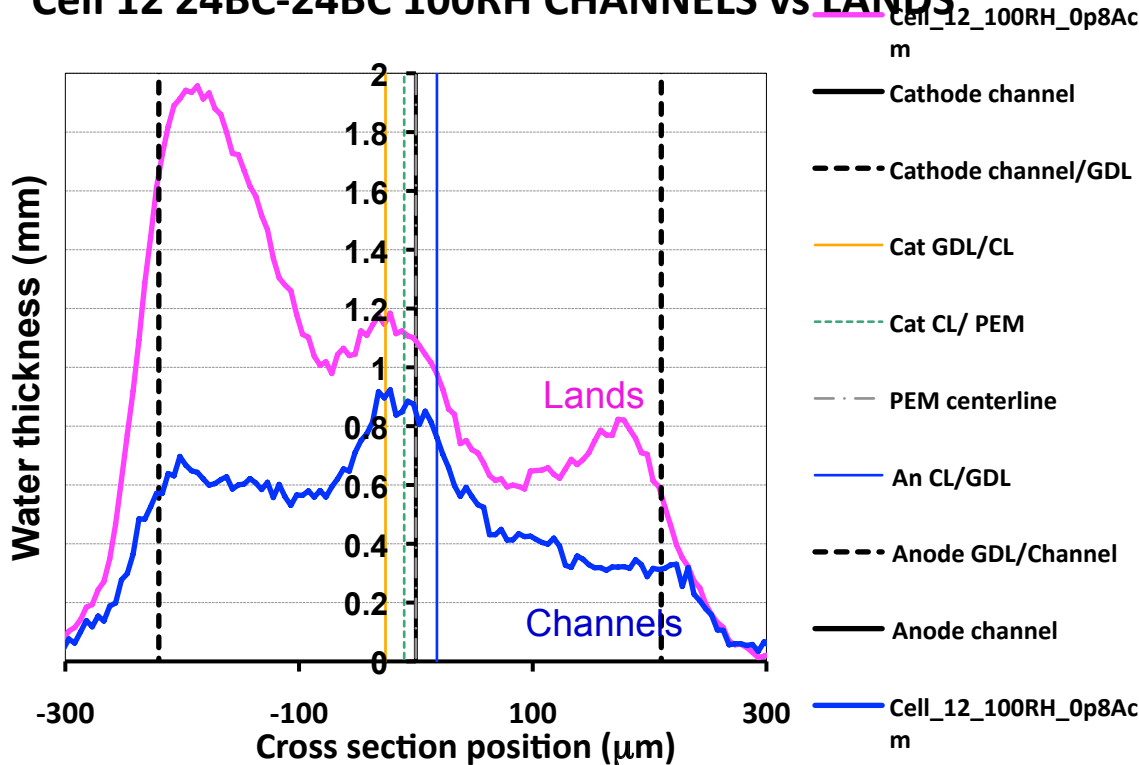
With beam hardening:

$$\frac{I_{\text{wet}}}{I_{\text{dry}}} = e^{-\mu t - \beta t^2}$$

Technical Accomplishment: High-resolution (13 μm) Through-Plane Neutron Imaging

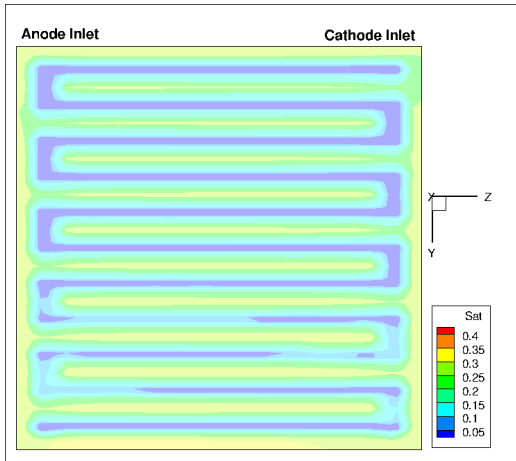
0.8 A/cm², 80°C, 100%RH

Cell 12 24BC-24BC 100RH CHANNELS vs LANDS

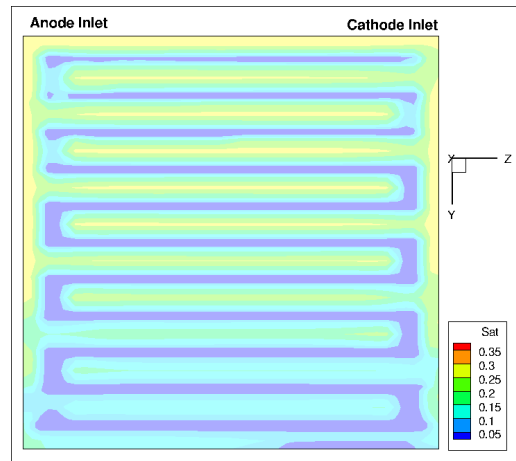


High resolution **through-plane** liquid water measurements are used for validating predictions of multi-phase models in different layers (GDL/MPL/CH). Separate liquid water data for **lands** & **channels** can be directly compared to model predictions.

Work in Progress: Preliminary Validation of Liquid Water Predictions Using Neutron Imaging

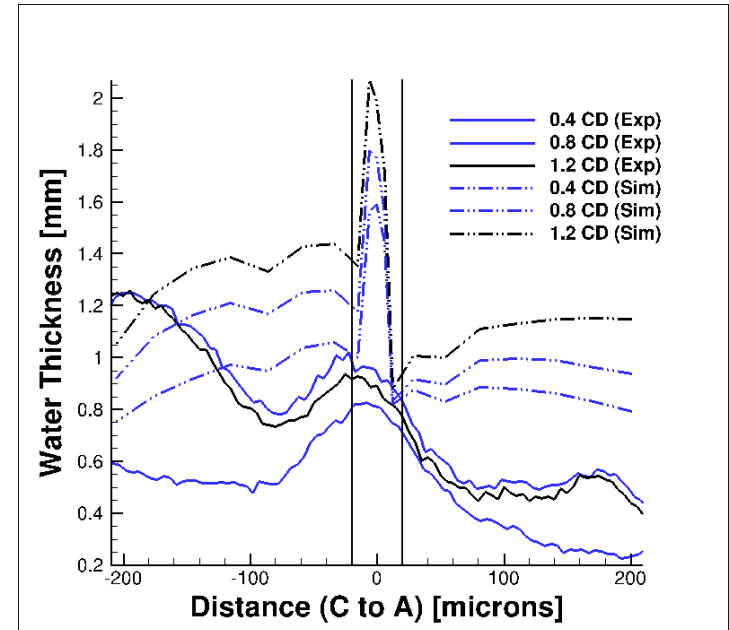


1.2 A/cm², 50% RH



1.2 A/cm², 100% RH

Liquid water saturation model predictions at Cathode GDL/Channel Interface



Preliminary model validation of water thickness at 100% RH

- ◆ Simulated liquid water saturation was converted to a through-plane water thickness by dividing the cell into small segments (cathode to anode)
- ◆ The water thickness in each segment was computed by the formula below using saturation (S), cross-sectional area (A), volume (V), porosity (ϵ):

$$W = \frac{1}{|A|} \int_V \epsilon S dx$$

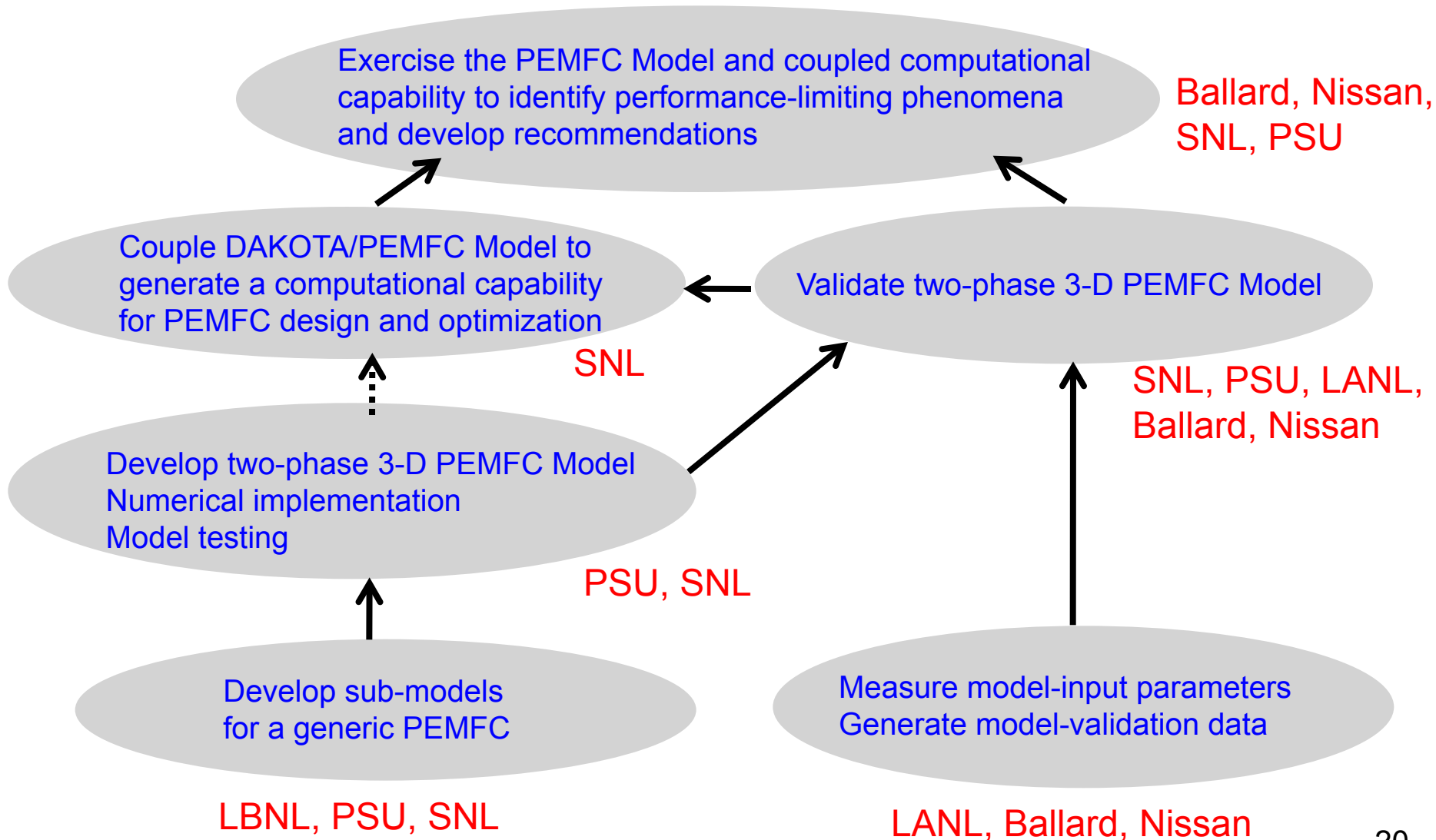
Model validation is **on track**. We expect to publish a paper this year on model validation using neutron imaging for data measured by LANL at the NIST facility.

Code Dissemination

- A user manual has been documented for the two-phase code we developed over the past decade and further improved in this project.
- The code is currently under testing by project partners, Sandia, Ballard, and Nissan.
- After further development and completion of the project, the software will be made available to the general public under licensing agreements.
- For further information about the two-phase model and computer code, contact Prof. Chao-Yang Wang at cxw31@psu.edu.
- For further information about the DAKOTA interface and scripts, contact Brian Carnes (bcarnes@sandia.gov)

Collaborations

Team partners: SNL(prime), PSU(sub), LBNL(sub), LANL(sub), Ballard(sub), Nissan(no cost)



Remaining FY12:

1. Complete **model validation** in the **fully two-phase** regimes using **neutron imaging data** obtained by **LANL** at NIST
2. Complete validation studies using **test data** from **Nissan** and **Ballard**.
3. Complete code manual and test problems.
4. Submit journal articles on model validation for neutron imaging data.



Summary of Technical Accomplishments

- **Model validation** using polarization and **current distribution data** obtained by LANL using a 10×10 segmented cell was performed. Year 3 **milestone M5** (“Perform validation of the 3-D, partially two-phase, single-cell model”) was **completed**.
- Model **validation of liquid water prediction** using LANL/NIST neutron imaging data is underway and Year 3 model-validation milestone M3 (“Validate fully two-phase, 3-D cell model ... using neutron imaging data”) is **on track**.
- Nissan/Ballard milestone M2 (“Validate model under real-world conditions”) has resulted in **model testing under realistic operating conditions**.
- Other accomplishments include:
 - **Channel liquid water predictions** were demonstrated using the fully two-phase model on the LANL 10×10 segmented cell flow field.
 - Demonstration of the two-phase model for **predicting liquid water** in a form comparable to neutron imaging studies of liquid water for *in situ* fuel cells.
 - A **model for micro-resistance** was applied for performance prediction of low-Pt loaded catalyst layers for Nissan.
 - Ballard **validation of stack data** for down-channel current/temp is on track.
 - Validation of Ballard neutron imaging experiments is also **on track for completion**.