

# Solar Hydrogen Production with a Metal Oxide Based Thermochemical Cycle

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DOE Annual Merit Review

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**Project ID: PD081**

Sandia is a multi-program laboratory operated by Sandia Corporation, a Lockheed Martin Company, for the United States Department of Energy's National Nuclear Security Administration under contract DE-AC04-94AL85000.

## Timeline

- Project Start Date: 10/2008
- Project End Date: 10/01/2012\*
- Project Complete: 75%

## Budget

- Total project funding to date  
DOE share: \$4002K (2008-2012)  
Contractor share: \$548K
- Funding for FY11  
\$175K (SNL)
- Planned Funding for FY12  
\$625K (SNL ~\$408K) (CU ~\$217K)

## Barriers Addressed

- U: High temperature thermochemical technology.
- V: High temperature robust materials.
- X: Coupling solar and thermochemical cycles.

## Partners

- University of Colorado, Boulder CO  
Prof. Alan Weimer  
Mr. Darwin Arifin
- Bucknell University, Lewisburg PA  
Prof. Nathan Siegel

\*Project continuation and direction determined annually by DOE.

- **DOE Objective**: Develop high-temperature thermochemical cycles driven by concentrated solar energy to produce hydrogen that meet the DOE threshold cost goal of <\$2.00/gge at plant gate.

- **Project Objective**: Develop a high-temperature solar-thermochemical reactor for efficient hydrogen production. The successful development of this reactor will provide a solar interface for most two-step, non-volatile metal oxide cycles.
- **2011-2012 Objectives**:
  - Discover and characterize suitable materials for two-step, non-volatile metal oxide thermochemical cycles.
  - Establish a screening protocol for candidate reactive materials and structures.
  - Design particle receiver-reactor concepts and assess feasibility.
  - Construct and test reactor prototypes.

# Technical Efforts Target Three Key Areas

- Materials discovery and characterization.

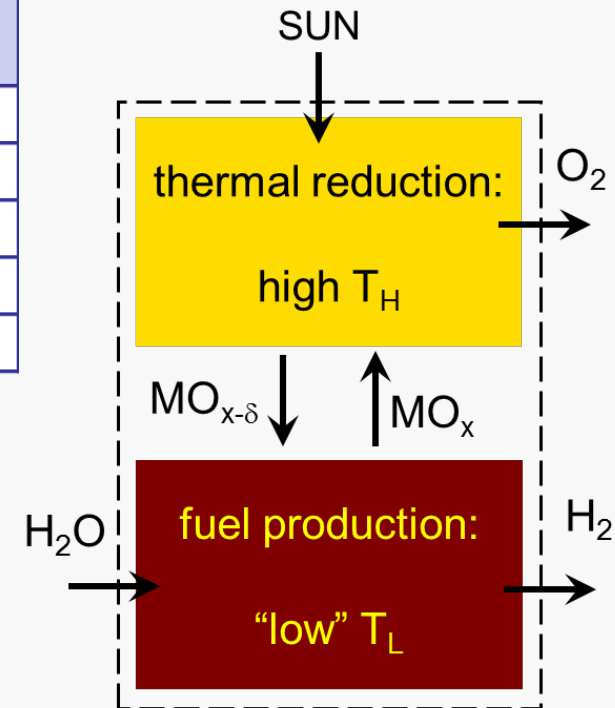
property	ferrite (Fe <sub>2</sub> O <sub>3</sub> )	ceria (CeO <sub>2</sub> )	hercynite (FeAl <sub>2</sub> O <sub>4</sub> )	perovskite (ABO <sub>3</sub> )	ideal
redox kinetics	<b>SLOW</b>	<b>FAST</b>	<b>SLOW/MED</b>	?	<b>FAST</b>
redox capacity	<b>HIGH</b>	<b>LOW</b>	<b>HIGH</b>	<b>HIGH</b>	<b>HIGH</b>
reduction T <sub>H</sub>	<b>MED/HIGH</b>	<b>HIGH</b>	<b>MEDIUM</b>	<b>LOW</b>	<b>LOW</b>
durability	<b>MEDIUM</b>	<b>HIGH</b>	<b>HIGH</b>	?	<b>HIGH</b>
earth abundance	<b>HIGH</b>	<b>LOW/MED</b>	<b>HIGH</b>	?	<b>HIGH</b>

- Reactor design and development.

- Direct solar absorption by redox material
- Efficient heat recovery between T<sub>H</sub> and T<sub>L</sub> >75%
- Continuous ON-SUN operation
- Intrinsic gas and pressure separation (H<sub>2</sub> from O<sub>2</sub>)

- Systems analysis.

- Derive REALISTIC estimate for H<sub>2</sub> production cost
- THEORETICAL performance must meet DOE cost targets



Two-step metal oxide cycle

- **MATERIAL and REACTOR DESIGN are critically linked.**
- **Good reactor design compensates for non-ideal material.**

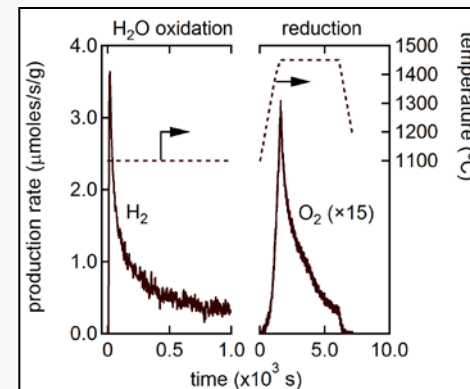
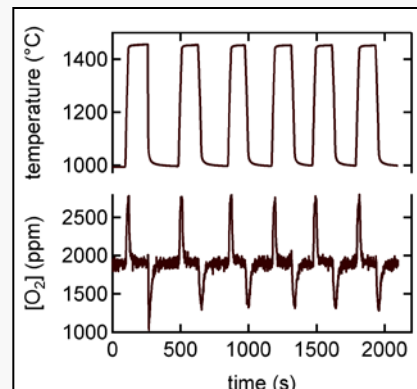
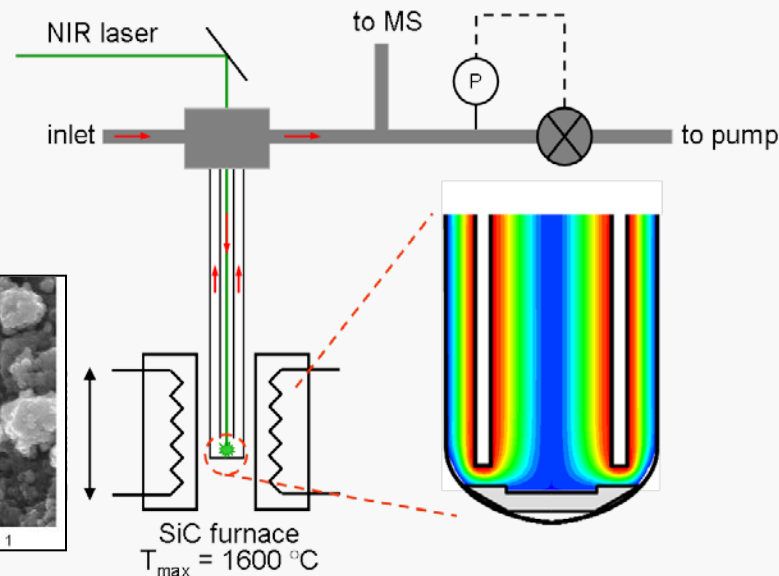
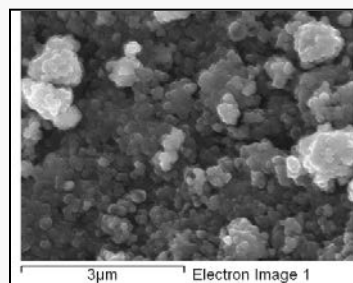
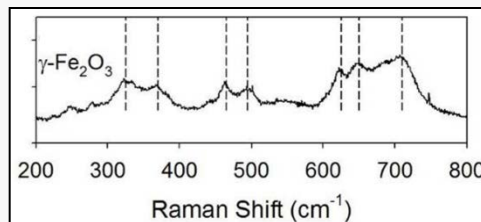
# Milestones and Progress

## 03.2011-03.2012 Accomplishments

ACTIVITY	MILESTONE	COMPLETE
Develop a protocol for material characterization	evaluated oxidation behavior (water splitting) of ferrite, ceria, and hercynite cycles	<b>50%</b>
Develop and validate a kinetic model for ceria	model used to establish theoretical cycle performance metrics for ceria in Sandia reactors	<b>100%</b>
Synthesize and characterize doped ceria materials	decreased thermal reduction temperature for ceria ( $T_H$ ) below 1450°C	<b>50%</b>
Theoretically analyze particle reactor performance	demonstrated that Sandia particle reactor has the potential to achieve >30% solar-to-H <sub>2</sub> thermal efficiency	<b>100%</b>
Design and test particle conveyor concept	validated conveyor concept by demonstrating a sustained mass flow rate of 30 g/s particles for 1 hour	<b>100%</b>
Evaluate reactor materials for high-temperature chemical compatibility with ceria, with no adverse reactivity, during lab-scale, short duration tests	no reactivity with Al <sub>2</sub> O <sub>3</sub> at 1550°C after 3 hours no reactivity with SiC at 1400°C after 3 hours no reactivity with coated SiC at 1450°C after 3 hours	<b>75%</b>
Design, construct, and test a “cold” reactor prototype	demonstrate mechanical operation at $T < 200^\circ\text{C}$ for 10 hours	<b>30%</b>

# Experimental Methods for Characterizing Redox Materials

- Surface analysis.
  - Surface Raman, XPS
- Material properties.
  - BET surface area
  - SEM-EDX, TEM-EELS, XRD
- Kinetic measurements.
  - Stagnation flow reactor
    - 500 W CW NIR laser heating
    - Modulated beam mass spectrometer
- Screen for O<sub>2</sub> uptake and release.
  - Assess redox viability
- Resolve thermal reduction behavior.
- Resolve water splitting behavior.
  - Variable T, P, [H<sub>2</sub>O]
- Analysis.
  - Resolve rate limiting mechanisms
  - Develop kinetic models
  - Evaluate material stability
  - Test cycle performance



- Assess material behavior at heating rates  $> 10^\circ\text{C/s}$ .
- Expose material to many rapid heating cycles.

# Packed Particle Bed Reactor Design and Operation

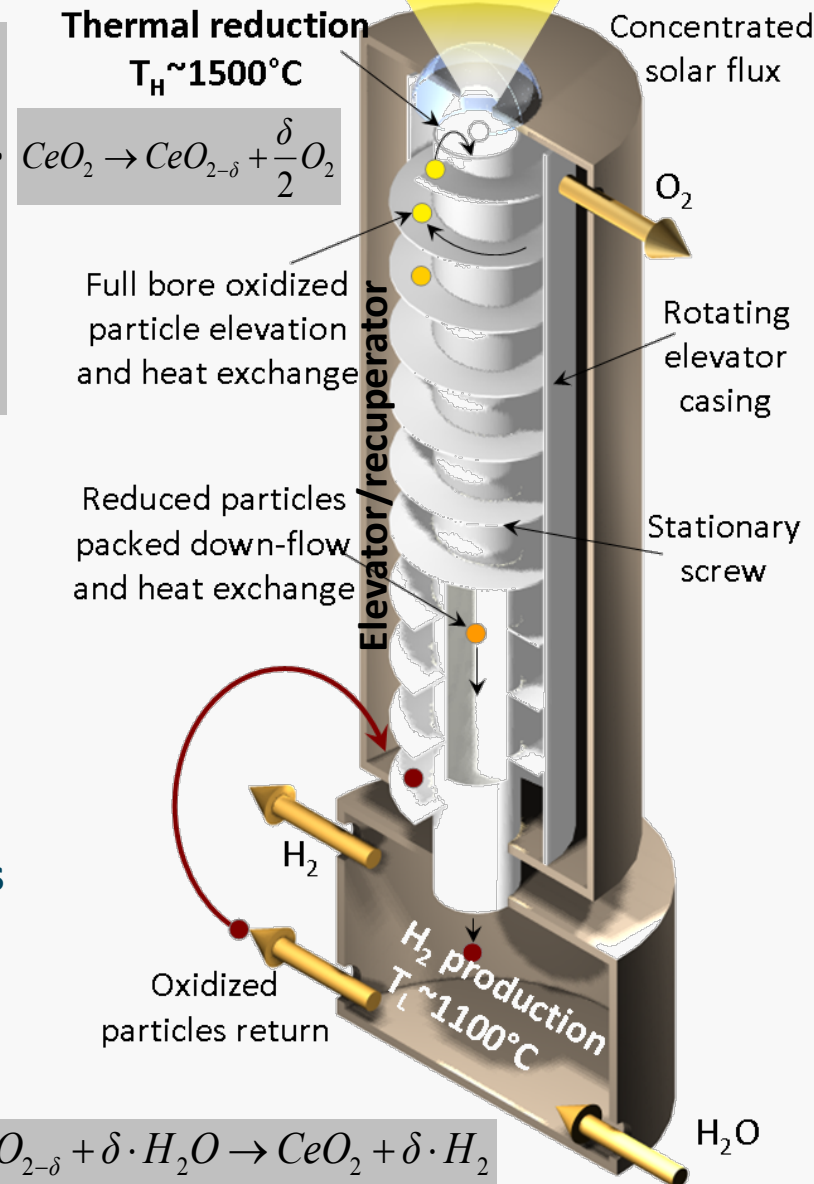
## Key efficiency attributes:

- DIRECT solar absorption by working material (>90%).
- EFFICIENT heat recovery between  $T_H$  &  $T_L$  (>75%).
- CONTINUOUS on-sun operation.
- INTRINSIC gas and pressure separation ( $H_2$  from  $O_2$ ).

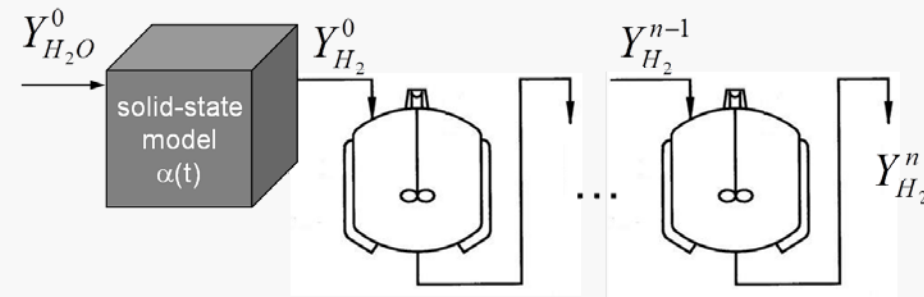
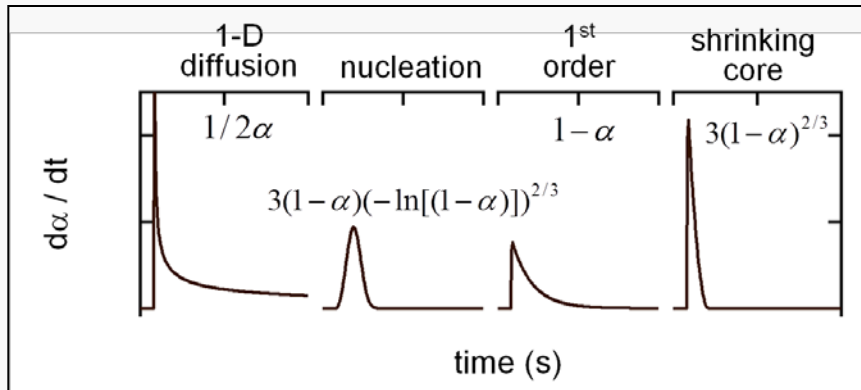
## Specific design advantages:

- Small reactive particles (~100 $\mu$ m)
- Only particles are thermally cycled
- Only one high T moving part: a ceramic tube
- Independent component optimization
- Straightforward material replacement
- Uses established high T and vacuum techniques  
[Cement kiln: 1450 $^{\circ}$ C; LPCVD: <150 Pa]

- High performance particle receiver reactor embodies ALL key efficiency attributes.



## Developed Model-based Data Reduction Protocol



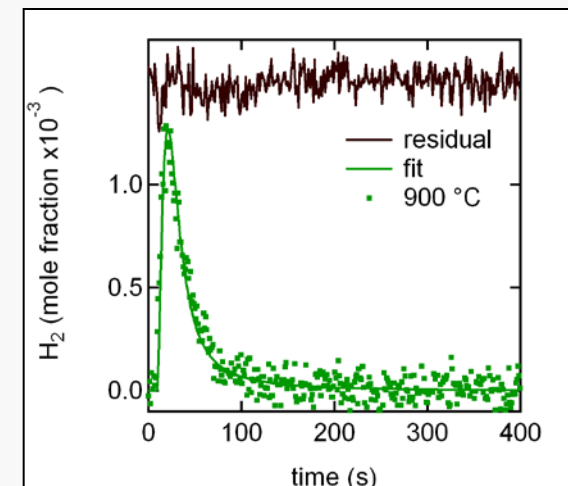
$$\frac{d\alpha}{dt} = k[Y_{H_2O}^0 (t - t_{shift})]^\gamma \exp[-E/RT] \cdot f(\alpha)$$

$$Y_{H_2}^0 \propto \frac{d\alpha}{dt}$$

$$\frac{dY_{H_2}^n}{dt} = \tau \cdot (Y_{H_2}^{n-1} - Y_{H_2}^n)$$

- Solid state kinetic theory.
  - Use 14 validated expressions for  $f(\alpha)$
  - Resolve rate-governing mechanism
- Numerical procedure.
  - Coding is Mathematica® based
    - Stiff integrators
    - Global least squares optimization
  - Correct experimental artifacts

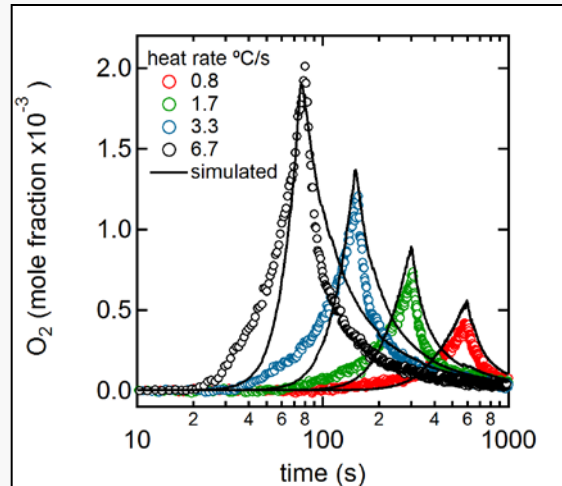
- Analytical approach new to this field of research.
- Generate high fidelity predictions of kinetic behavior.
- Establish and test performance metrics.
  - Both materials and reactor design





## Developed Validated Kinetic Model for $\text{CeO}_{2-\delta}$ Redox

### thermal reduction at 1500 °C

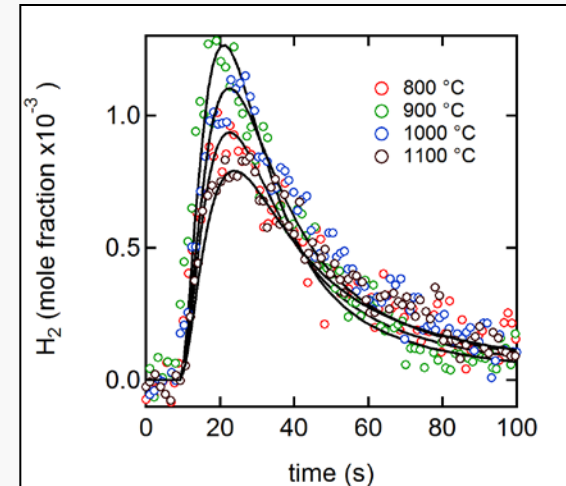


$$\frac{d\delta}{dt} = k_1 \left( \frac{T}{T_1} \right)^{\beta_1} \exp[-E_1 / RT] \cdot (\delta_{eq} - \delta)^{m_1}$$

- Reduction kinetics very rapid.
  - Solid-state dynamics at *mm length scales* does not limit kinetics

- **CeO<sub>2</sub> is a good model material.**
- **Use to evaluate reactor performance metrics.**
  - Mass flow, reactor geometry
  - Reaction time and temperature

### H<sub>2</sub>O oxidation



$$\frac{dY_{H_2}^0}{dt} \propto \frac{d\alpha}{dt} = k_2 [Y_{H_2O}^0 (t - t_{shift})]^\gamma \exp[-E_2 / RT] \cdot (1 - \alpha)^2$$

- H<sub>2</sub> production rate exhibits 2<sup>nd</sup> order behavior.
- 90% conversion in 100 s @ 900°C.
  - 10- 100 μm size particles

property	ceria (CeO <sub>2</sub> )	ideal
redox kinetics	<b>FAST</b>	<b>FAST</b>
durability	<b>HIGH</b>	<b>HIGH</b>

## Synthesized and Characterized Doped Ceria Materials

ferrites		ceria	perovskites	
$\text{Fe}_2\text{O}_3$	$\text{CoFe}_2\text{O}_4$	$\text{MO}_x:\text{CeO}_{2-\delta}$	$\text{La}_{1-x}\text{Sr}_x\text{Cr}_{1-y}\text{Mn}_y\text{O}_{3-\delta}$	
YSZ m-ZrO <sub>2</sub>	m-ZrO <sub>2</sub>	10 mol% Mn, Ni, Co, Mo, & Fe	$\underline{X}$ 0.9	$\underline{Y}$ 0.5
CeO <sub>2</sub>			0.8	
			0.7	
Al <sub>2</sub> O <sub>3</sub>	Al <sub>2</sub> O <sub>3</sub>		0.6	
			0.5	

- Current material chemistries under consideration.

- Chemical systems

$\text{M}^{+n}/\text{M}^{+(n+1)}$  redox couples

$\text{MO}_{n-\delta}$  non-stoichiometric oxides

CU “hercynite”

- Supports

m-ZrO<sub>2</sub>, YSZ, CeO<sub>2</sub>, Al<sub>2</sub>O<sub>3</sub>

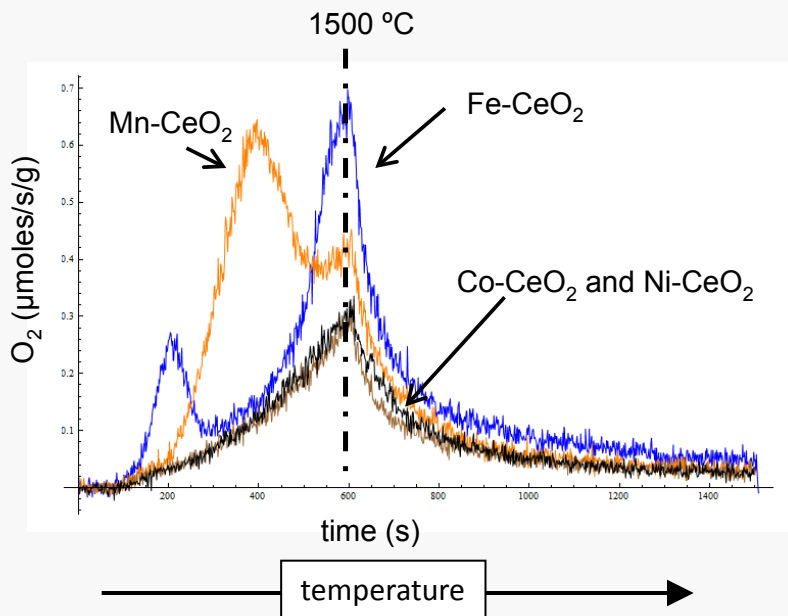
property	ceria (CeO <sub>2</sub> )	ideal
redox capacity	<b>LOW</b>	<b>HIGH</b>
reduction T <sub>H</sub>	<b>HIGH</b>	<b>LOW</b>

- **Destabilized CeO<sub>2</sub> more likely to achieve DOE performance targets.**

- **Improve material performance through chemical modification.**
  - Create solid solutions with transition metals
- **Increase oxygen non-stoichiometry (redox capacity).**
- **Decrease thermal reduction temperature (T<sub>H</sub>).**

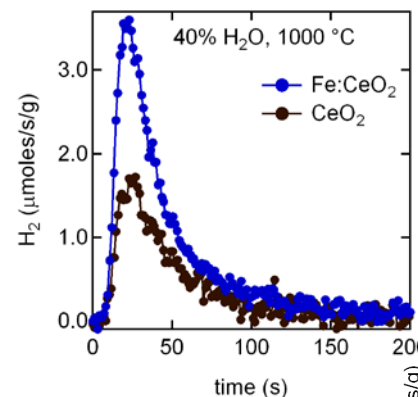
## Characterized Effects of Transition Metal Doping on $\text{CeO}_{2-\delta}$

### thermal reduction at 1500 °C

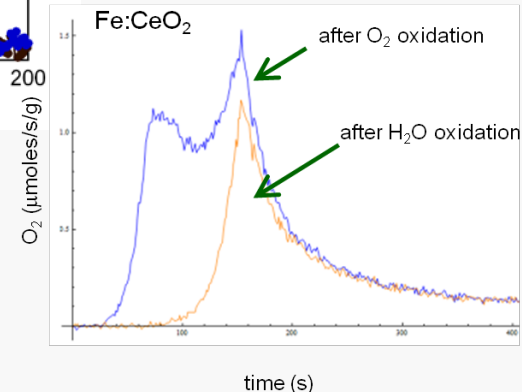


- $\text{O}_2$  evolution complex for Mn and Fe.
  - More  $\text{O}_2$  evolved per unit mass of material than undoped  $\text{CeO}_2$
  - Multiple valence states for Mn and Fe cations likely in doped system
- $\text{O}_2$  evolution unchanged for Co and Ni.

### $\text{H}_2\text{O}$ oxidation



TR to 1500 °C @ 3.3 °C/s



- $\text{FeO}_x$  doping increases net  $\text{H}_2$  production.
- Active sites in Fe-doped  $\text{CeO}_2$  oxidize at different rates.

- **Fe and Mn change  $\text{CeO}_2$  material behavior.**
  - More  $\text{O}_2$  evolves at lower temperature (increase capacity at lower  $T_H$ )
- **Difficult to re-oxidize added capacity by water splitting chemistry.**

# Iron Doping Induces Morphological Instability

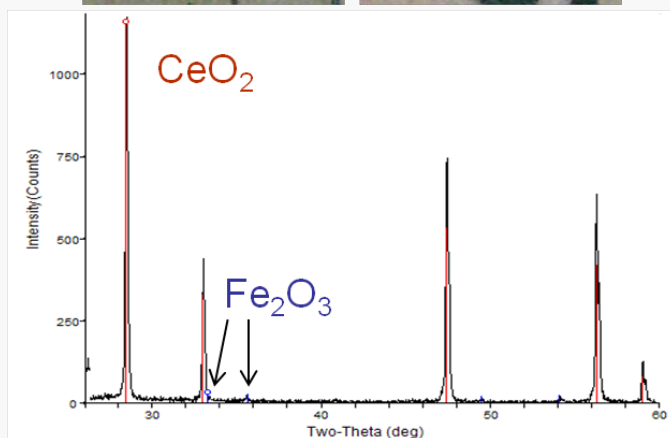
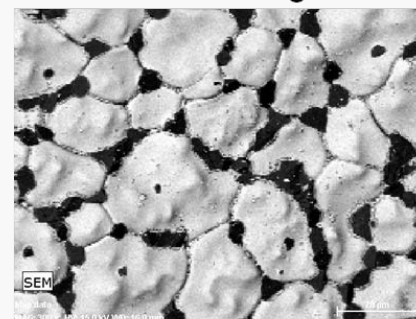
before redox



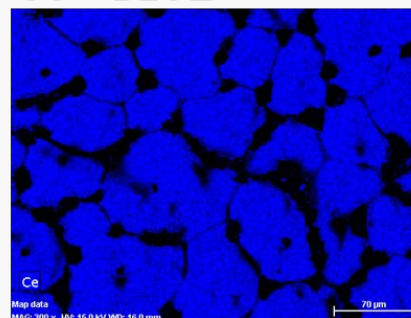
after redox



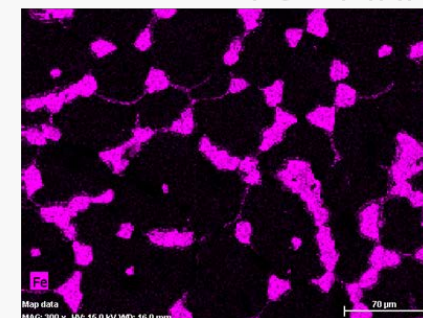
SEM image



Ce = BLUE



Fe = PINK



- Reduction in helium at 1500°C followed by H<sub>2</sub>O oxidation at 1000°C.
  - Severe problems with sintering and reactivity with other ceramics
  - Fe phase segregation evident in SEM-EDS despite lack of evidence in XRD
  - Slow kinetics on “low temperature” O-site

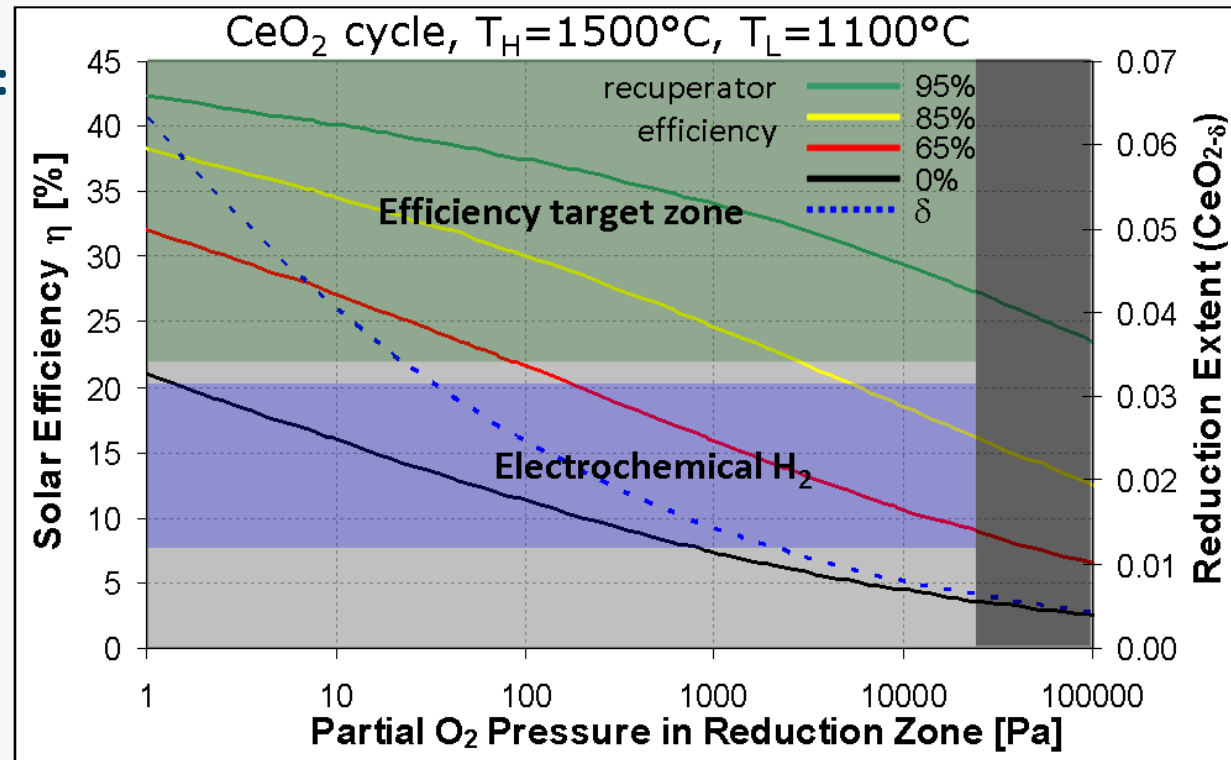
- **Fe doping not likely a viable strategy despite greater redox capacity.**
  - Other doping strategies may work!

## Theoretical Analysis of Sandia Reactor Concept: Solar-to-H<sub>2</sub> Efficiency

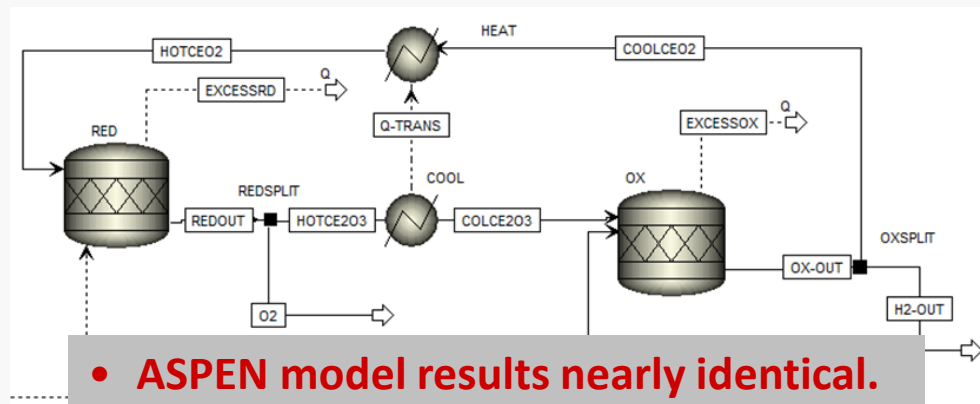
### All-inclusive efficiency metric:

- Collection losses.
  - Concentrator & re-radiation
- Oxide heating.
- Oxide thermal reduction.
- Feedstock heating (steam).
- Pumping.
- Electrical/mechanical work.

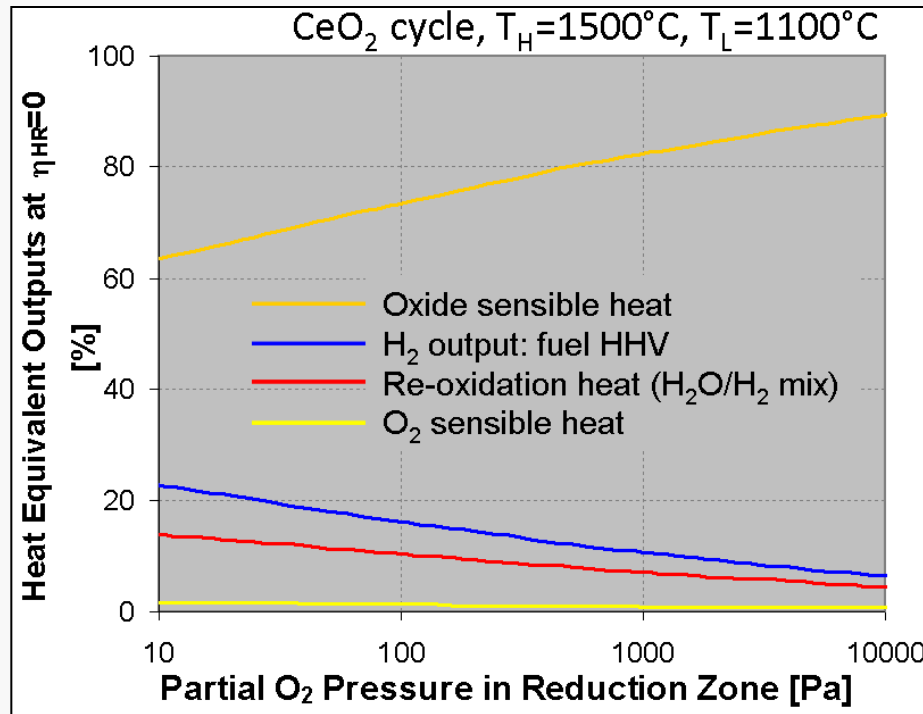
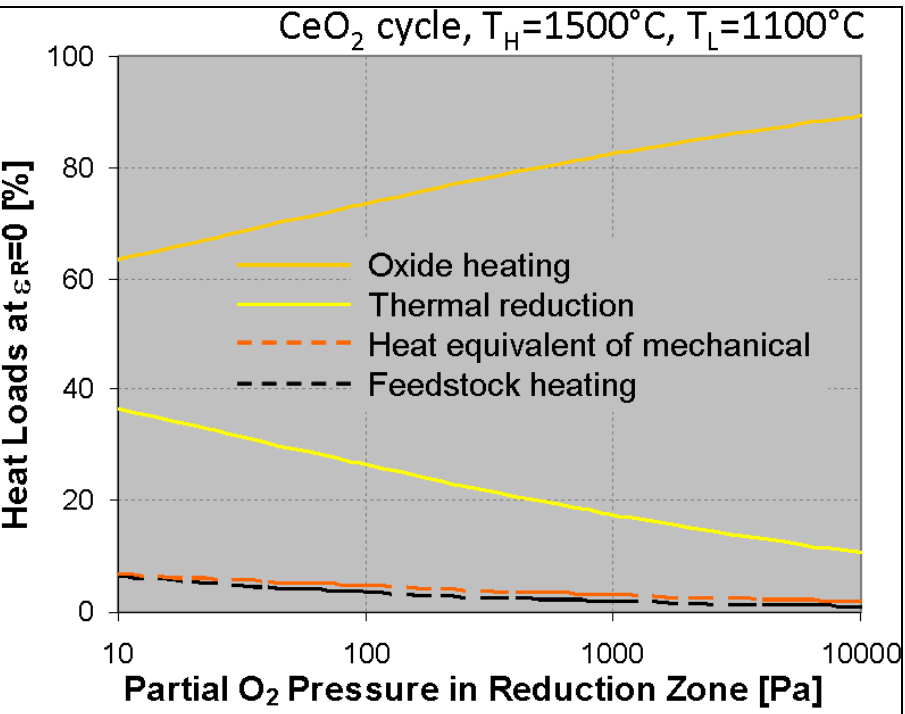
$$\eta = \frac{\dot{n}_{H_2} \cdot HHV_{H_2}}{P_S}$$



- **Theoretical Solar-to-H<sub>2</sub> efficiency >30% possible with CeO<sub>2</sub>.**
- **Must haves:**
  - Heat recovery (recuperation)
  - Low O<sub>2</sub> pressure in reduction zone



# Heat Recuperator Effectiveness Critically Important



- Oxide heating and reduction.
  - Must be driven by direct solar input
- Other loads can use waste heat.

- Heat (or equivalents) of reactor output.

• Heat recovery critical to efficient system operation.  
 • Recuperator effectiveness >65% required to meet DOE performance goals.

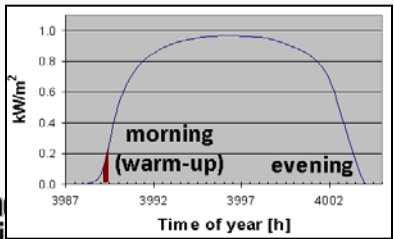
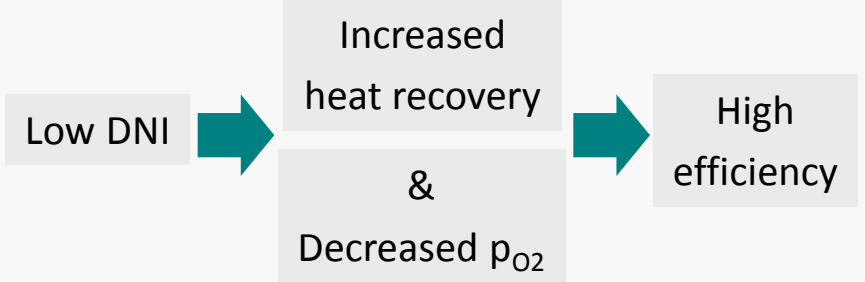
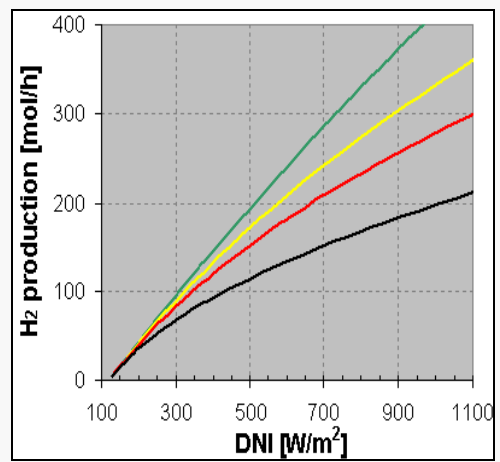
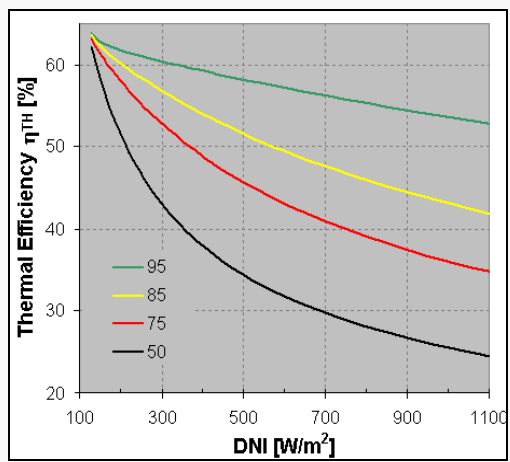
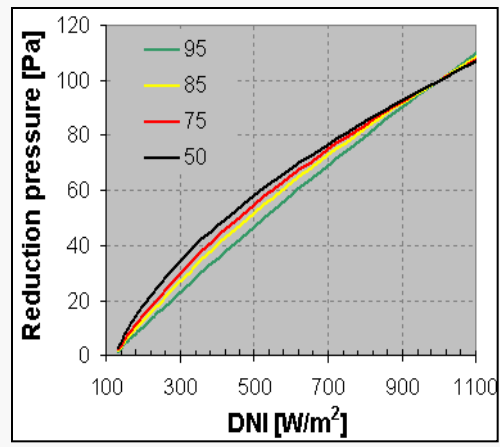
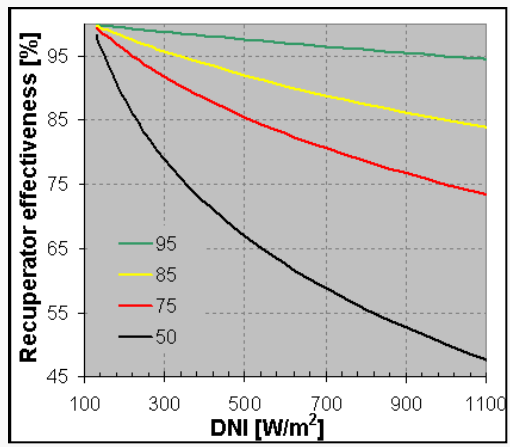
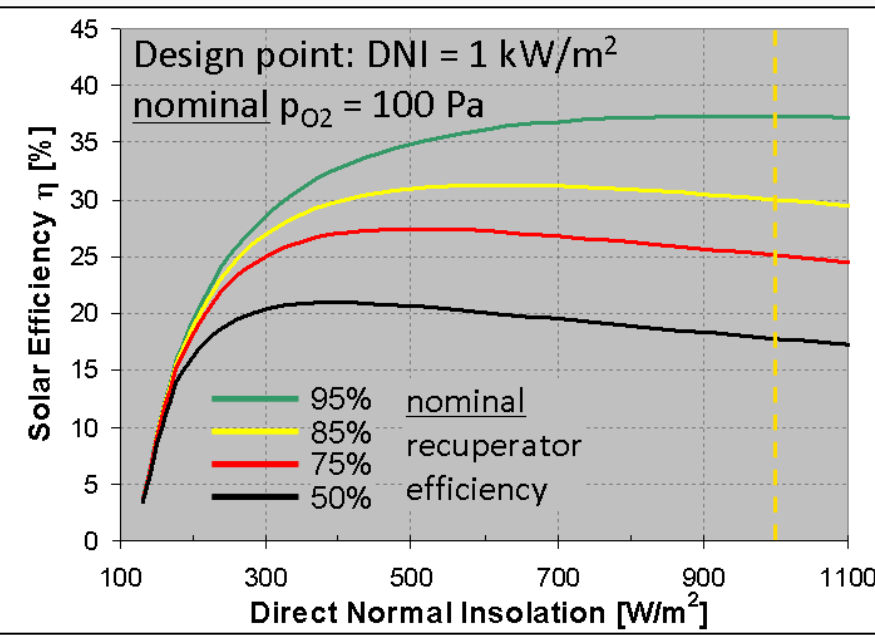
## Achieving Effective Heat Recuperation in a Particle Elevator

- Innovative reactor design (Sandia patented).
  - Stationary screw with rotating casing
- Internal fins used for enhanced heat recovery.
- Use multiple screw design to increase heat recovery.
  - Single standard-pitch elevator screw inefficient



- **Nested multi-screw design is most promising elevator/recuperator concept we have tested to date.**
  - Move 30 g/s particles at 20 RPM
- **Building prototypes to assess heat recuperation effectiveness.**

## Sandia Reactor Also Operates Efficiently at Low DNI

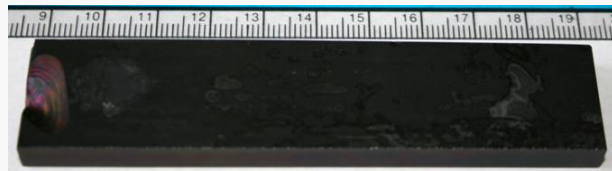


- High solar utilization under most operating conditions.
  - 25% solar-to-H<sub>2</sub> annual average efficiency expected
- Use low DNI in the morning for system warm-up.



## Materials Compatibility and Manufacturing

- Reactor parts and reactive oxide must not react with each other, even at  $T_H$ .
- Multiple bare and coated materials tested under realistic conditions.
- Alumina compatible with ceria to at least 1550°C.
- SiC compatible with ceria to 1400°C.
- Alumina-coated SiC compatible to 1450°C (coating thickness, method, and stability critical).
- Ceramic component manufacturers identified.



CeO<sub>2</sub>/SiC Hexoloy, 1400°C  
stagnant air, 3h



CeO<sub>2</sub>/Al<sub>2</sub>O<sub>3</sub>, 1550°C  
stagnant air, 3h



paint CeO<sub>2</sub>/Al<sub>2</sub>O<sub>3</sub>/SiC, 1450°C  
stagnant air, 3h

- **For a ceria reactive oxide, no showstoppers in prototype manufacture are expected.**

- Currently working with Prof. Alan Weimer's group at the University of Colorado.
  - Several students are working at SNL/CA in the area of materials discovery and characterization
- Currently working with Prof. Nathan Siegel at Bucknell University.
  - Optics, particle conveyance, systems and economic analysis
- Jenike and Johanson Inc. contracted to help develop particle conveyor concepts.

- Find perovskite materials that exhibit low thermal reduction temperature, fast exchange kinetics, and increased redox capacity.
  - Synthesize novel, substituted  $ABO_3$  perovskites
    - Future collaboration with Colorado School of Mines
    - Future collaboration with North Western University via an NNSA fellow
  - Develop a method to use simple thermodynamic assessments to guide search
    - Use structure-property and structure-performance relationships as descriptors
- Build a reactor prototype platform to test various functionalities at increasing temperatures (<200°C, ~900°C, ~1500°C). Target power ~5 kW<sub>thermal</sub>
  - Develop a manufacturing process for  $CeO_2$ 
    - Correctly-sized particles and quantities (~100 kg needed for 5kW)
  - Evaluate particle flow and attrition as a function of particle and elevator dimensions
  - Evaluate steam flow through particle bed in the  $H_2$  production chamber
  - Measure particle bed permeability and gas flow between reactor chambers
  - Test reactor performance in a solar furnace or solar simulator ( $T > 1400^\circ C$ )
- Systems analysis.
  - Critically evaluate central receiver performance
  - Detailed annual average performance analysis

- Developed a novel analytical approach to characterizing reactive materials.
  - Used to generate high fidelity predictions of  $\text{CeO}_2$  kinetic behavior
  - Used to establish and test performance metrics for both reactor designs and materials
- Synthesized and characterized the redox behavior of several transition-metal doped  $\text{CeO}_2$  compounds (Mn, Fe, Co, Ni, and Mo).
  - Chemical modification of  $\text{CeO}_2$  may improve material performance
- Designed and theoretically analyzed new solar thermochemical reactor that embodies four key high-efficiency attributes: direct solar absorption, efficient heat recovery, continuous on-sun operation, and intrinsic gas and pressure separation.
  - Design can attain a solar-to- $\text{H}_2$  conversion efficiency >30%
  - Determined that heat recovery (recuperation >65%) critical for efficient performance
  - Determined that efficient operation possible even in low DNI  
25% solar-to- $\text{H}_2$  annual average efficiency expected
- Prototyped a novel particle elevator/recuperator reactor concept.
  - Particle conveying experimentally validated using a unique nested-screw design
  - U.S. patent filed in 2011

# Technical Back-Up Slides

# System Level: Many Losses and High Annual Efficiency

**Resource efficiency = 95%** for Daggett, CA (DNI > 300W/m<sup>2</sup>)

**Operational ~ 94%**

Equip. Availability = 97%, Blocking&Shading = 98%, Wind Outage = 99%

**Optical ~ 79%**

Reflectivity = 93% (two reflections)

Dirt = 95%

Window = 95%

Tracking = 99%

Intercept = 95%

**Receiver ~ 82%**

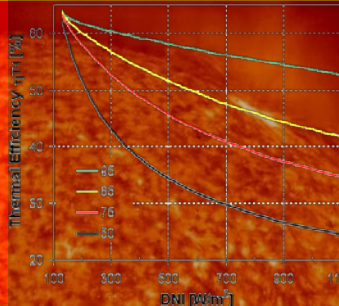
Radiation = 82%

Conduction/Convection = 0 %

Solar-to  
heat:  
~58%



Thermal  
~44%



**~25% solar to H<sub>2</sub>  
annual average**

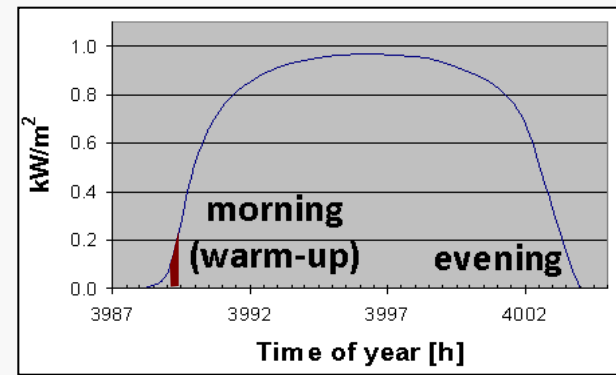
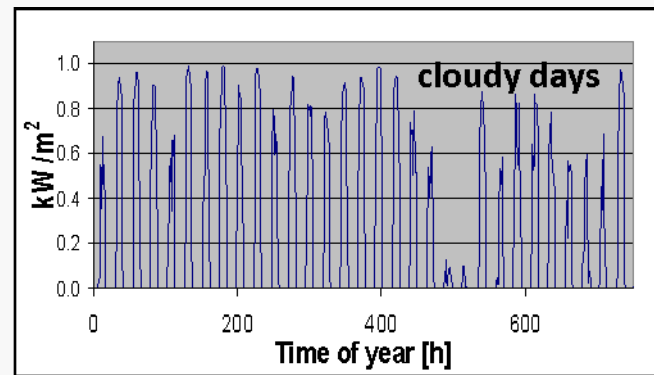
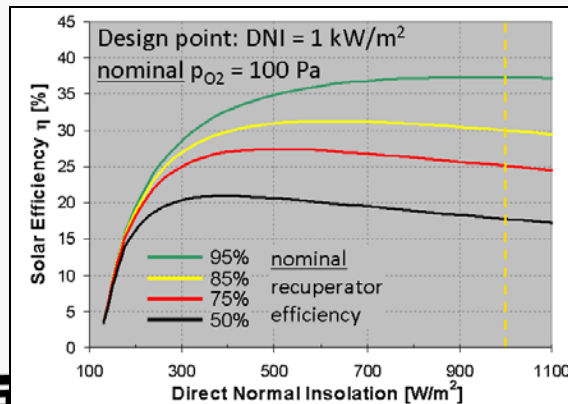
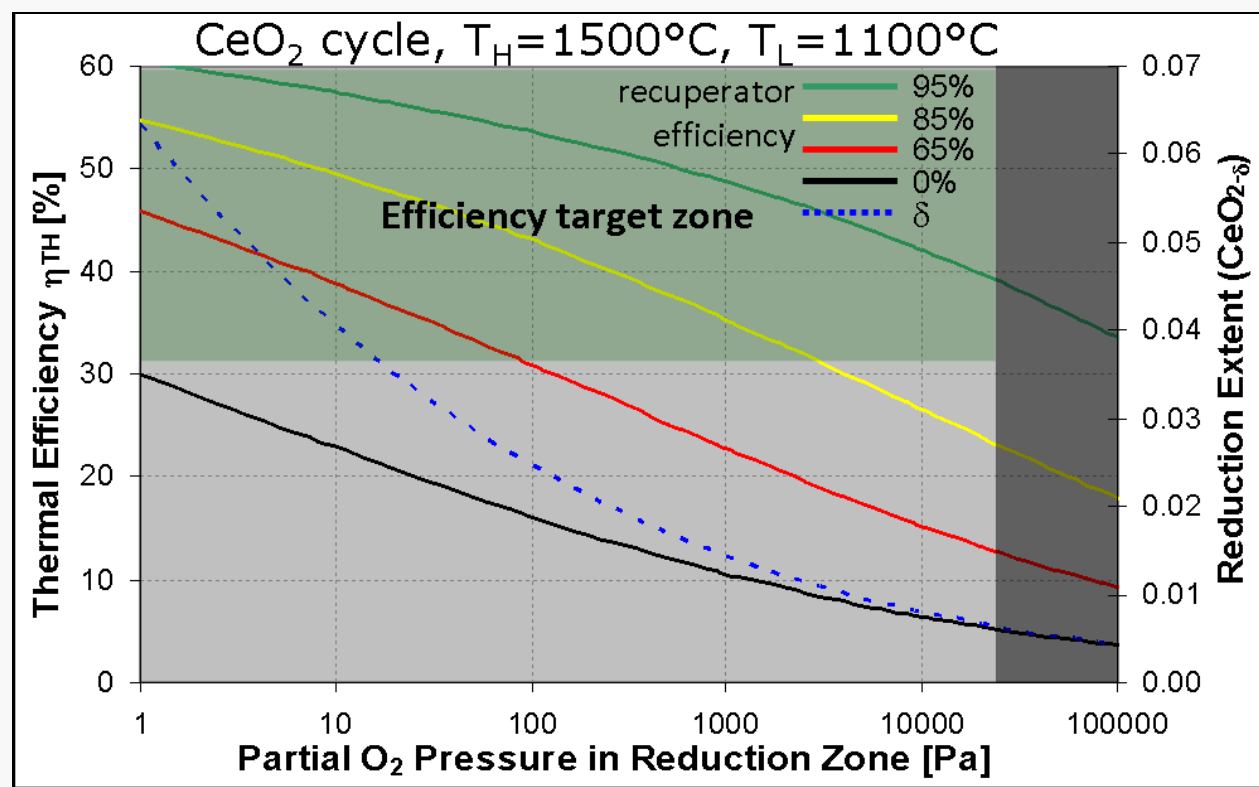
## Reactor Performance Model: Thermal Efficiency

Reactor-only metric includes:

- Oxide heating.
- Oxide thermal reduction.
- Feedstock heating (steam).
- Pumping.
- Electrical/mechanical.

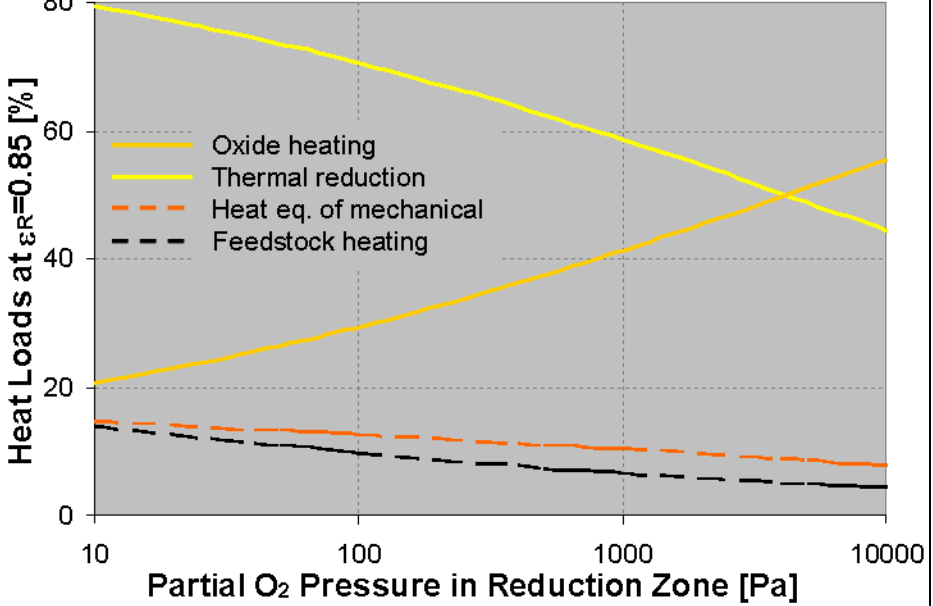
$$\eta = \frac{\dot{n}_{H_2} \cdot HHV_{H_2}}{P_{TH}}$$

- **Thermal efficiency >40% attainable.**
- **Excellent low-DNI efficiency**

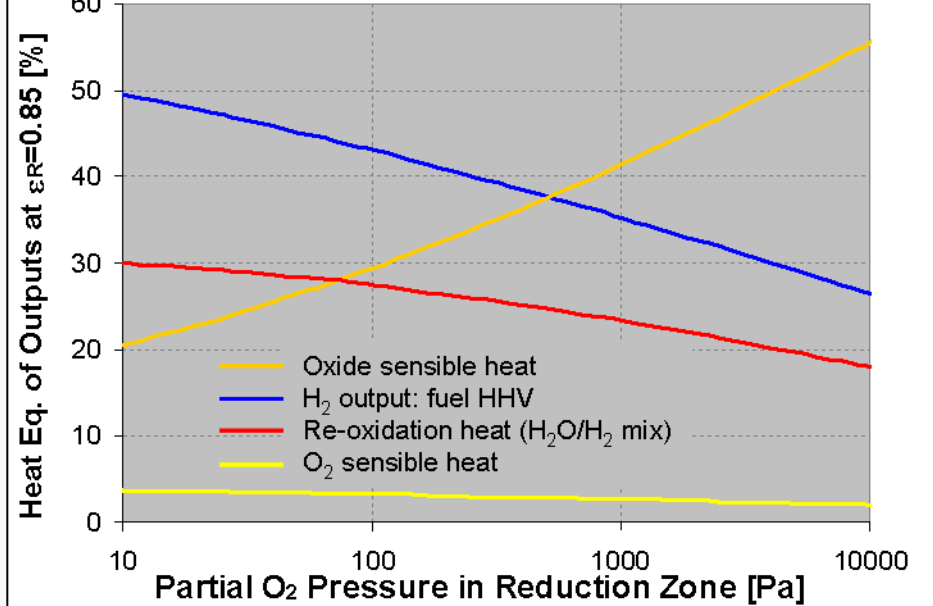


# Heat Recuperator Effectiveness Critically Important

CeO<sub>2</sub> cycle, T<sub>H</sub>=1500°C, T<sub>L</sub>=1100°C



CeO<sub>2</sub> cycle, T<sub>H</sub>=1500°C, T<sub>L</sub>=1100°C



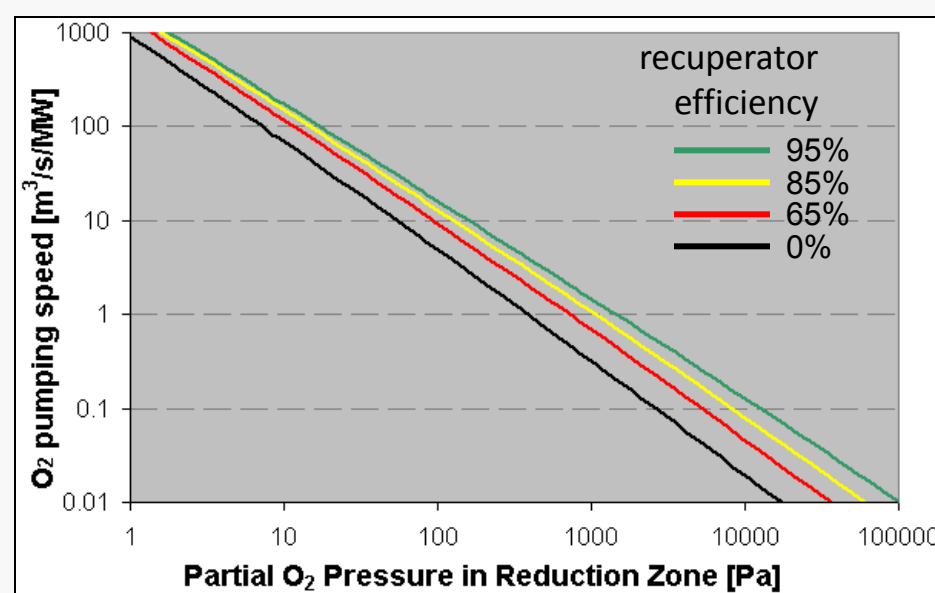
- Oxide heating and reduction.
  - Must be driven by direct solar input
- Other loads use waste heat.

- Heat (or equivalents) of reactor output.

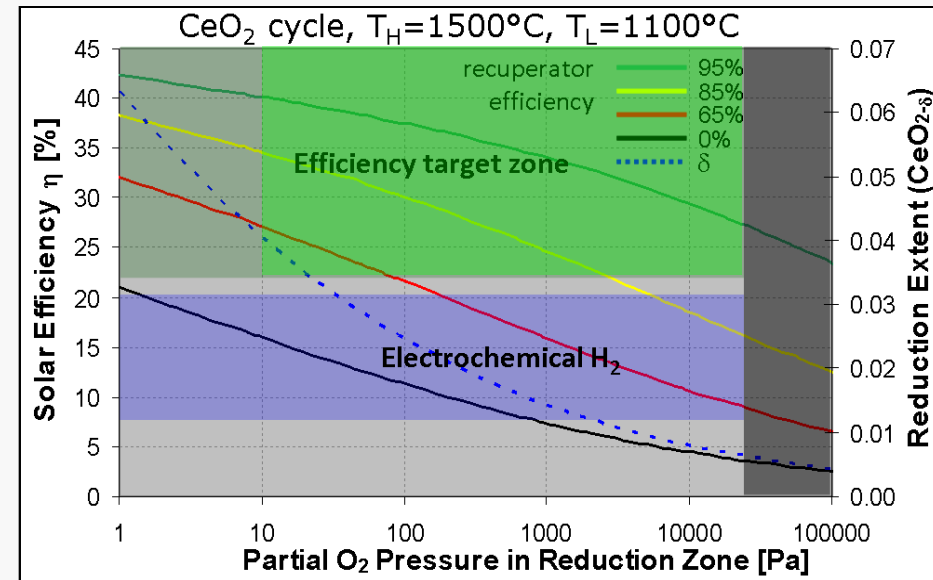
• Heat recovery critical to efficient system operation.  
 • Recuperator effectiveness >65% required to meet DOE performance goals.



## Low Pressure Limit: Pumping Speed



Required pumping speed for 1 MW<sub>solar</sub> device



- Pumping speed requirement is a likely limit to minimum design-point p<sub>O<sub>2</sub></sub> or maximum solar power input per device.