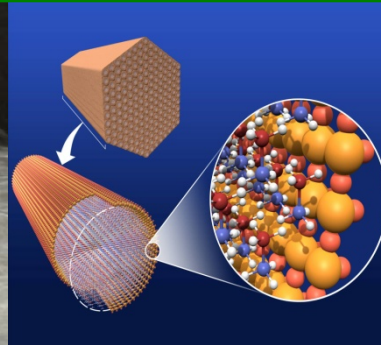




U.S. DEPARTMENT OF  
**ENERGY**

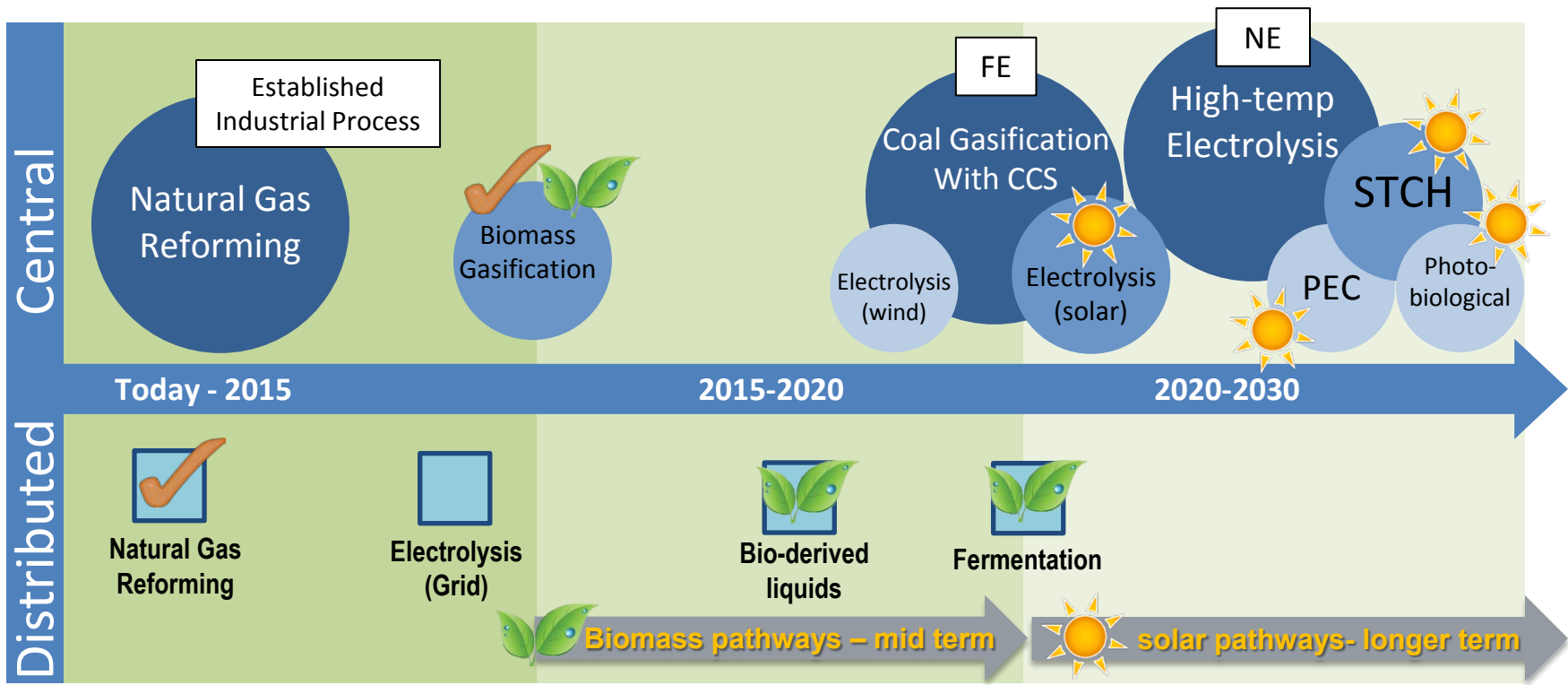


# Hydrogen Production and Delivery

*Sara Dillich*

*2013 Annual Merit Review and Peer Evaluation Meeting  
May 13, 2013*

# Technology Readiness of DOE Funded Production Pathways



Estimated Plant Capacity (kg/day)

Up to 1,500

50,000

100,000

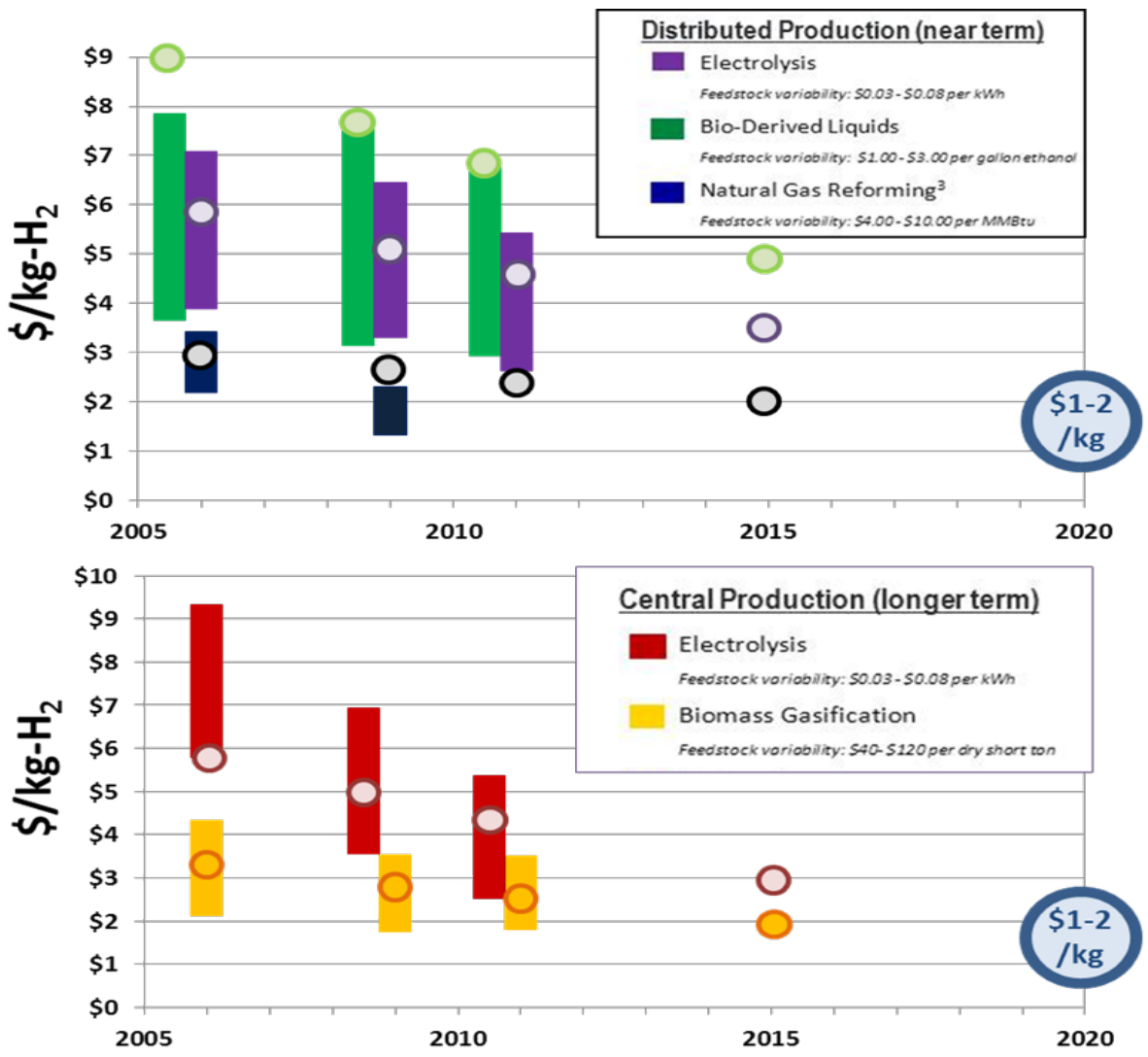
≥500,000

P&D Subprogram R&D efforts successfully concluded

*FE, NE: R&D efforts in DOE Offices of Fossil and Nuclear Energy, respectively*

# Hydrogen Production — Status & Pathways

## Projected High-Volume Cost of Hydrogen for Near-Term Production Pathways



- Status of hydrogen cost (production only, does not include delivery or dispensing costs) is shown in vertical bars, reflecting values based on a range of assumptions (feedstock/capital costs).
- Targets for hydrogen cost are shown in circles.
- Targets shown are normalized for consistency in feedstock assumptions and year-cost basis (2007 dollars)
- *Targets prior to 2015 are extrapolated based on 2015 and 2020 targets in the FCT Office's Multi-year RD&D Plan.*
- Cost ranges are shown in 2007 dollars, based on projections from H2A analyses, and reflect variability in major feedstock pricing and a bounded range for capital cost estimates.
- Projections of costs assume Nth-plant construction, distributed station capacities of 1,500 kg/day, and centralized station capacities of ≥50,000 kg/day.

## Hydrogen Production from Natural Gas: Bridge to Longer-Term, Low-Carbon Technologies

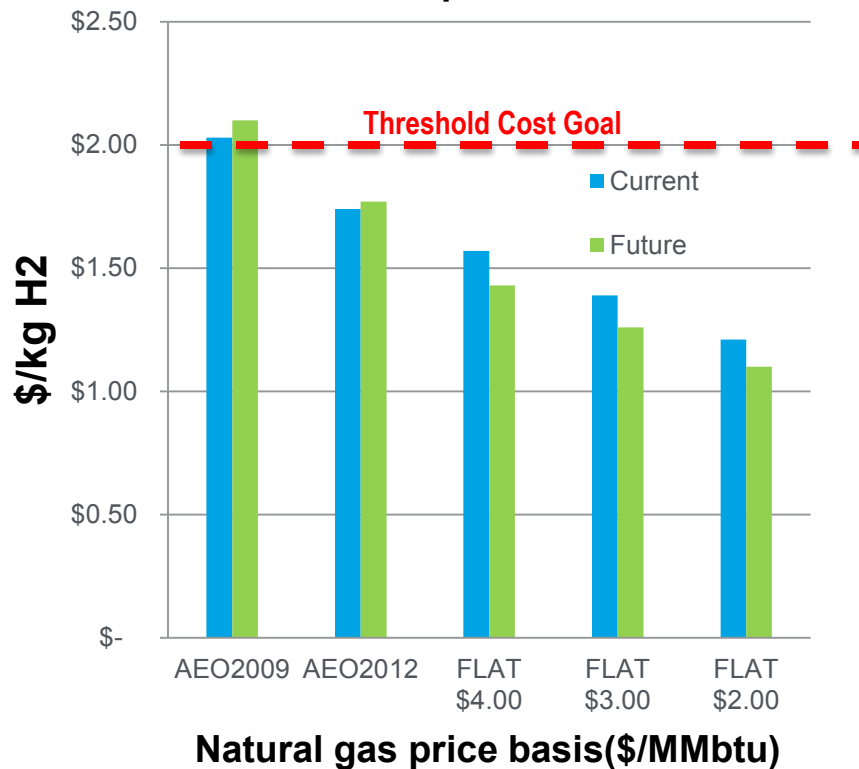
Distributed H<sub>2</sub> production from natural gas steam methane reforming

(high volume/economies of scale, 1500 kg/day production)

- Cost of H<sub>2</sub> production not limiting factor
- Cost goals can be met by a wide range of NG prices\*
- Focus shifting to longer term, early development, renewable pathways

\*Production Cost Using Low-Cost Natural Gas, September, 2012, [http://hydrogen.energy.gov/pdfs/12024\\_h2\\_production\\_cost\\_natural\\_gas.pdf](http://hydrogen.energy.gov/pdfs/12024_h2_production_cost_natural_gas.pdf)

**\$/kg H<sub>2</sub> (produced & untaxed, today's technology) for Varying Natural Gas Spot Prices**



Based on H2A v3 Case Studies @ [http://www.hydrogen.energy.gov/h2a\\_production.html](http://www.hydrogen.energy.gov/h2a_production.html)  
 AEO2009 avg NG prices (HHV, \$/MMBtu): \$7.10 (Current, 2010-2030); \$8.44 (Future, 2020-2040)  
 AEO2012 avg NG prices (HHV, \$/MMBtu): \$5.28 (Current, 2010-2030); \$6.48 (Future, 2020-2040)

**GOAL: Develop technologies to produce hydrogen from clean, domestic resources at a delivered and dispensed cost of \$2-\$4/gge H<sub>2</sub> by 2020**

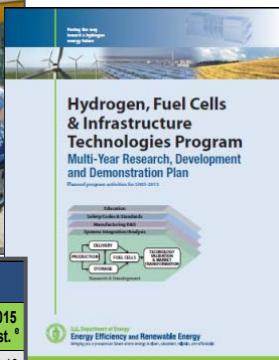


Table 3.1.1 Distributed Forecourt Natural Gas Reforming <sup>a, b, c</sup>

Characteristics	Units	2010 Status <sup>d</sup>	2015 est. <sup>e</sup>
Hydrogen Levelized Cost (Production Only) <sup>f</sup>	\$/kg H <sub>2</sub>	\$2.03	\$2.10
Production Equipment Total Capital Investment	\$M	\$1.5	\$1.2
Production Energy Efficiency <sup>g</sup>	%	71.4	74
Production Equipment Availability <sup>c</sup>	%	97	97
Industrial Natural Gas Price <sup>h</sup>	average \$/mmBtu	\$7.78	\$8.81

2013 2014

2012

**H2A Case Studies  
&  
MYRD&D  
Updates**

2011

- Update of analysis models
- Apportionment of cost threshold goal

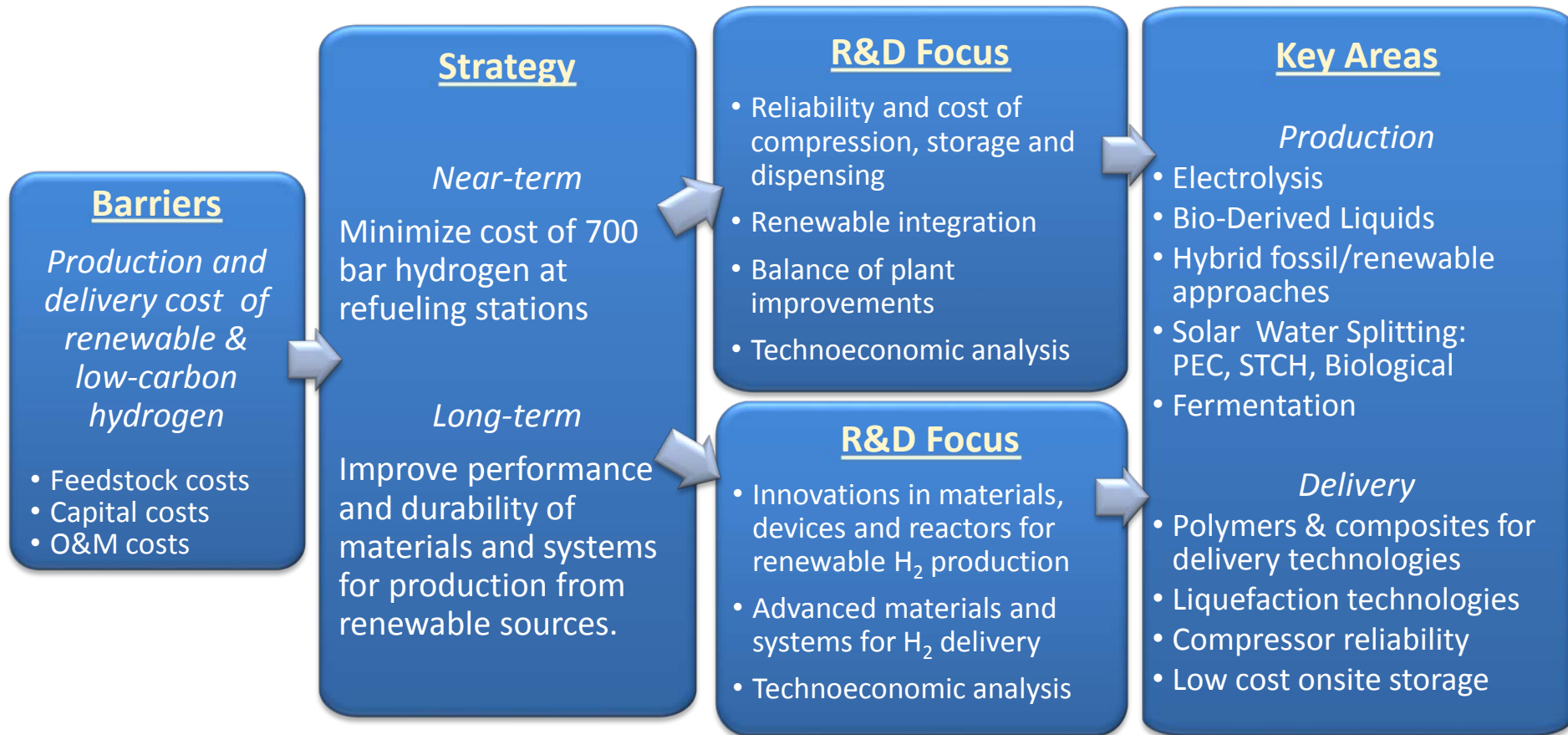
**FOA for  
new  
starts in  
FY2014**

- Updated MYRD&D Chapters posted online
- Updated Production and Delivery Roadmaps submitted to U.S. DRIVE
- Analysis FOA & Project Initiation
- MOU: FCTO & NSF MOU prepared for joint funding of hydrogen and fuel cells R&D
- Hydrogen Production Expert Panel (HPEP) Report prepared
- Independent Panel Review of Compression, Storage, and Dispensing (CSD) Costs
- Workshop on CSD Cost Reduction March, 2013, ANL
- 2013 SBIR topic: H<sub>2</sub> Dispensers



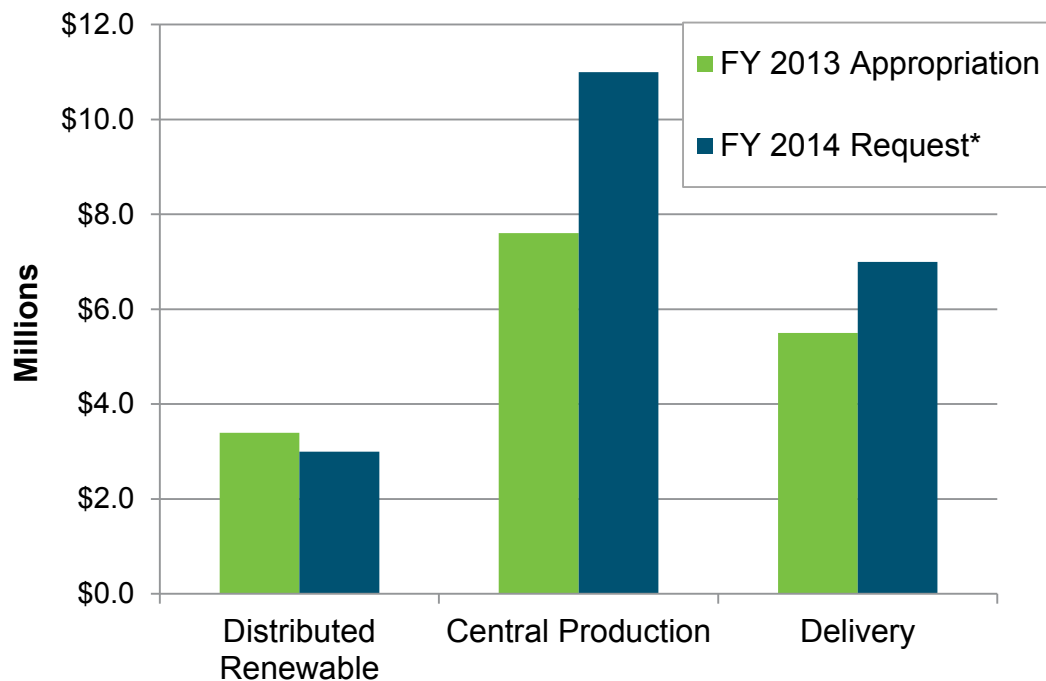
# H<sub>2</sub> Production and Delivery Challenges & Strategy

*Materials durability, efficiency improvements, and capital cost reductions are key challenges for all production and delivery pathways*



*FY 2013 Appropriation: \$16.5M*

*FY 2014 Request: \$21M*



\* Subject to appropriations, project go/no go decisions and competitive selections. Exact amounts will be determined based on R&D progress in each area and the relative merit and applicability of projects competitively selected through planned funding opportunity announcements (FOAs).

## 2013/14 Emphasis

- FOAs for FY14 new starts: based on updated MYRD&D, Roadmaps and HPEP report

### Distributed Production

- Develop production and forecourt CSD technologies for improvements in
  - Cost
  - Balance of plant
  - Reliability

### Central

- Innovations in materials, devices and reactors for renewable H<sub>2</sub> production.
- Advanced polymers and composites for H<sub>2</sub> delivery systems

Nuclear Hydrogen Initiative was discontinued at end of FY2009 as a separate program. Funding of high temperature electrolysis continued under the NGNP project through FY2011. After INL demonstration of pressurized stack operation in FY 2012, technology readiness will be sufficiently advanced (TRL5) to allow for further development by industry. Congressional direction to DOE for FY2012 was to focus on conversion of coal and biomass to liquid fuel. No funding for H<sub>2</sub> production from coal was provided.

## New Project Initiated

### Team:

*Strategic Analysis, Inc.*

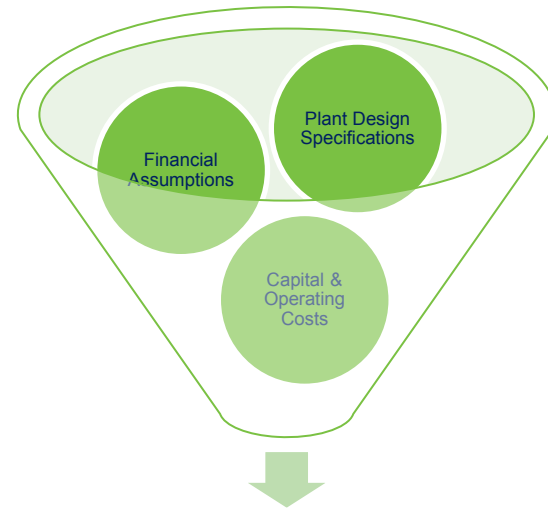
PI: Brian James

Partners: NREL, ANL

### Scope:

- Establish cost and performance baselines and track progress for R&D projects (with R&D project teams)
- Update pathway cases and develop new pathway case studies as needed
- Standardize assumptions & metrics for longer term pathways (with DOE and project teams)

### Hydrogen Analysis Model



### Required Selling Price of H2 (\$/kg)

	\$/kg (production costs only)	2011 Status	2015 Target	2020 Target	Ultimate Production Target
Distributed	Electrolysis from grid electricity	\$4.20	\$3.90	\$2.30	\$1-\$2
	Bio-derived Liquids (based on ethanol reforming case)	\$6.60	\$5.90	\$2.30	
Central	Electrolysis From renewable electricity	\$4.10	\$3.00	\$2.00	
	Biomass Gasification	\$2.20	\$2.10	\$2.00	
	Solar Thermochemical	NA	\$14.80	\$3.70	
	Photoelectrochemical	NA	\$17.30	\$5.70	
	Biological	NA	NA	\$9.20	



## Hydrogen yields depend on composition and properties of bio-oil

Feed-stock	H <sub>2</sub> g/100g bio-oil
Poplar	11.0
Oak	8.5
Pine	10.5
Oak, lignin-free	3.0 (12)*

\*hydrogen yield on water-free basis (lignin-free oak bio-oil fraction contained 74.6% water)

Reforming of poplar and pine bio-oils delivered > 10g H<sub>2</sub> per 100 g bio-oil.

Lower yield from oak bio-oil due to lower carbon and higher oxygen contents, and lower carbon-to-gas conversion

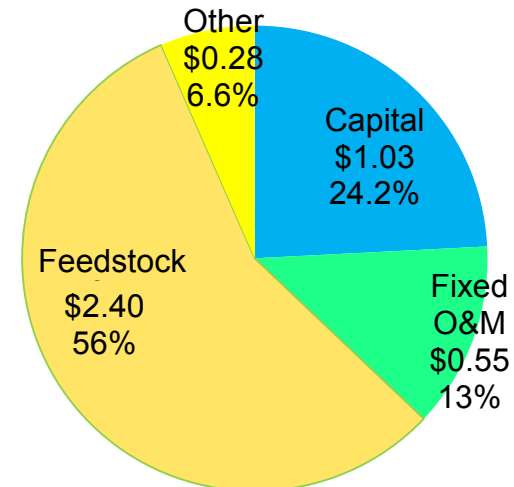
### Optimum Process Conditions Identified:

800-850 C, steam-to-carbon ratio of 2.5-3.5,  
Pt/Al<sub>2</sub>O<sub>3</sub> catalyst, Space velocity ~ 2000 h<sup>-1</sup>

### H2A v3: \$4.26/kg H2

(Production only, CSD not included)

Distributed Production: 1500 kg/day

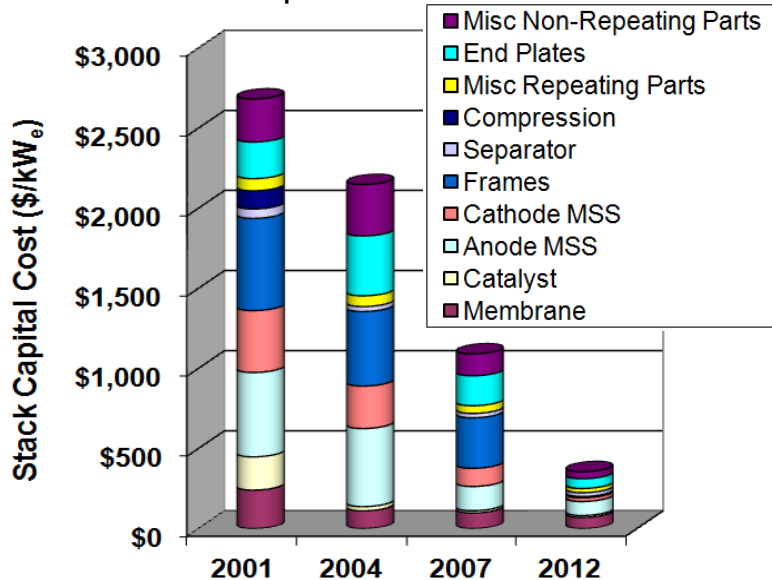


Production Cost Break-down  
for Poplar bio-oil: \$236/ton

**NREL**

## Greater than 60% reduction in cost of PEM electrolyzers stacks achieved since 2007 (Giner Inc.)

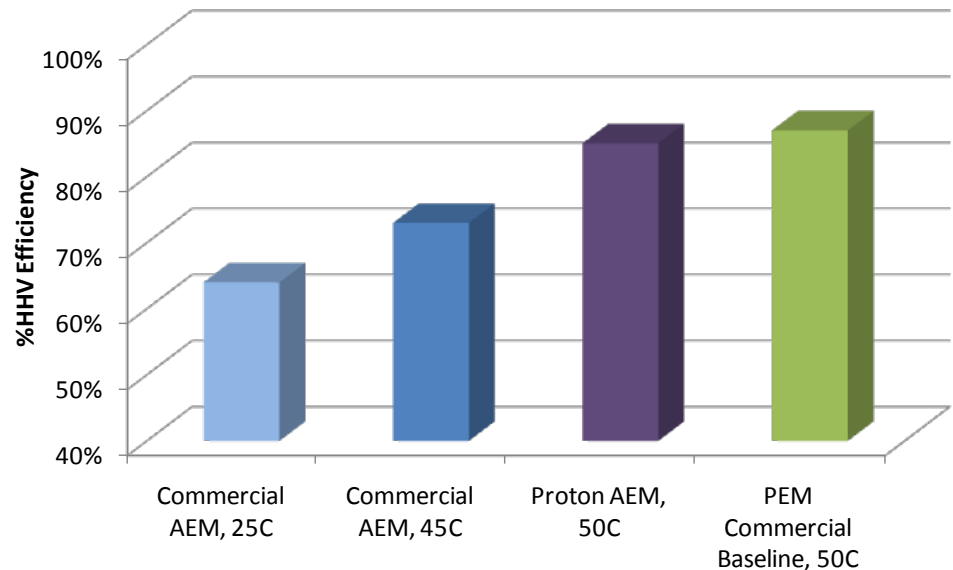
- ✓ 75% reduction in part count leading to a 50% reduction in manufacturing labor
- ✓ 30% thinner frame reduce cathode and anode support material
- ✓ 90% cost reduction of DSM MEA's through fabrication with chemically etched supports
- ✓ 66% end plate material cost reduction by using carbon steel in place of stainless steel



## Alkaline exchange membrane (AEM) technology offers potential for efficiency & small footprint of PEM stacks, but at lower cost (*Proton OnSite*)

- ✓ Developed OER catalysts for AEM electrolysis
- ✓ Demonstrated performance over >100 h of operation
- ✓ > 80% HHV AEM efficiency shown at bench scale
- ✓ Material cost savings potential of > 80% using AEM technology are projected
- ✓ Leveraging ARPA-e project on AEM technology for regenerative fuel cell systems

Electrolyzer Performance, 400 mA/cm<sup>2</sup>



## Innovative chemical reaction materials and reactor designs used to produce hydrogen from sunlight and water through thermochemical processes

### R&D Focus

- Materials efficiency and durability (SNL, U of CO)
- Reactor design (SNL, Univ. of Colorado)
- Membranes and electrocatalysts (ANL, SAIC, SRNL)
- Technoeconomic analysis to establish efficiency and durability requirements for meeting DOE cost goal

### High Temp 2-Step cycles

- Metal oxides, Perovskite compounds (SNL)
- Nanostructured hercynite (Univ. of Colorado)

### Hybrid Cycles wt Electrolysis Step

- Cu-Cl cycles (ANL/GTI/Penn State)
- Sulfur-ammonia (SAIC)
- Hybrid sulfur (SRNL)

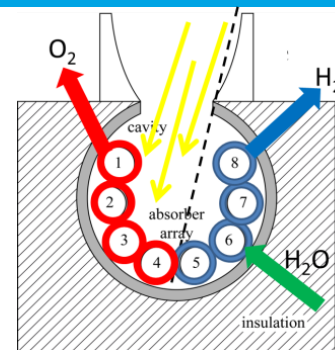
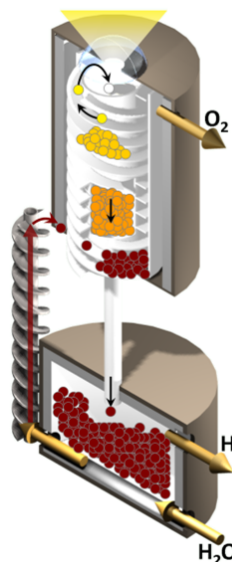
### Reactor Designs

- Particle receiver-reactor (SNL)
- Absorbing cavity w/ multi-tubular fixed beds (Univ. of Colorado)
- Bayonet-type reactor (SAIC)

### Field Concepts

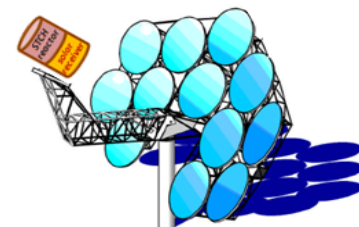
- Central tower/Heliostat field
- Central tower/Heliostat with molten salt storage (SAIC)
- Dish field -- one reactor/dish (SNL)

SNL reactor design



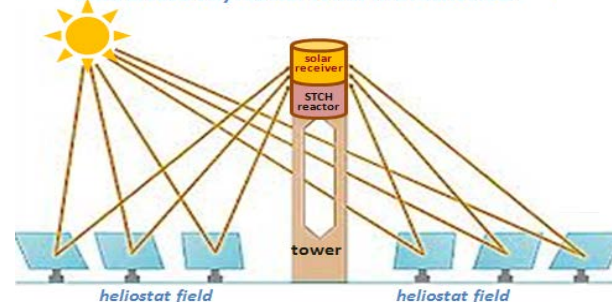
Univ. of Colorado reactor design

modular dish-mounted receiver/reactor



dish mirrors

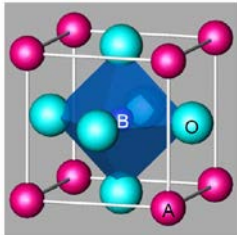
central receiver/reactor tower with heliostats



# 2013 Progress: Solar-Thermochemical

## Novel perovskite compounds, nanostructured hercynite, split H<sub>2</sub>O in 2-step thermochemical cycles

- Synthesized 45 perovskite compounds from 9 elements (Al, Cr, Ce, Fe, La, O, Sr, Ti, Zr) using Sol-gel or Solid State Reactive Sintering (SNL)

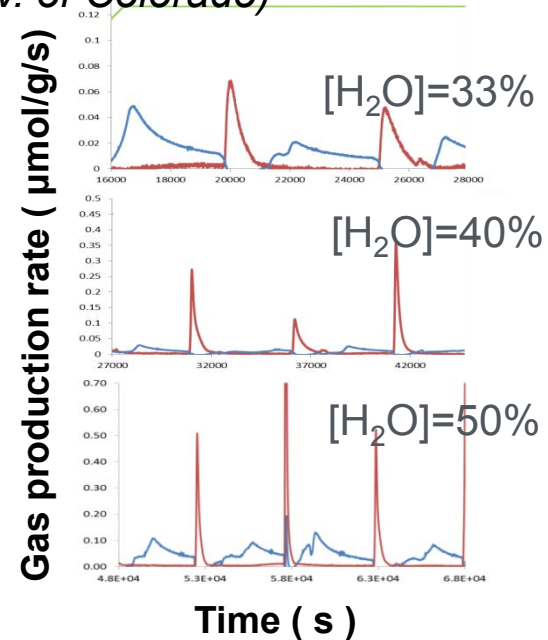


Perovskite structure  
 $ABO_3$

property	ceria (CeO <sub>2</sub> )	perovskite (ABO <sub>3</sub> )	ideal
redox kinetics	<b>FAST</b>	<b>TBD</b>	<b>FAST</b>
redox capacity	<b>LOW</b>	<b>HIGH</b>	<b>HIGH</b>
reduction T <sub>H</sub>	<b>HIGH</b>	<b>LOW</b>	<b>LOW</b>
durability	<b>HIGH</b>	<b>TBD</b>	<b>HIGH</b>
earth abundance	<b>LOW/MED</b>	<b>HIGH</b>	<b>HIGH</b>

Patent filed on a perovskite family of Sr - and Mn- substituted LaAlO<sub>3</sub>.

- Verified stability of Hercynite redox activity via Raman analysis and >150 cycles testing
- Increased H<sub>2</sub>O pressure increases total H<sub>2</sub> produced and peak rates of H<sub>2</sub> production (Univ. of Colorado)

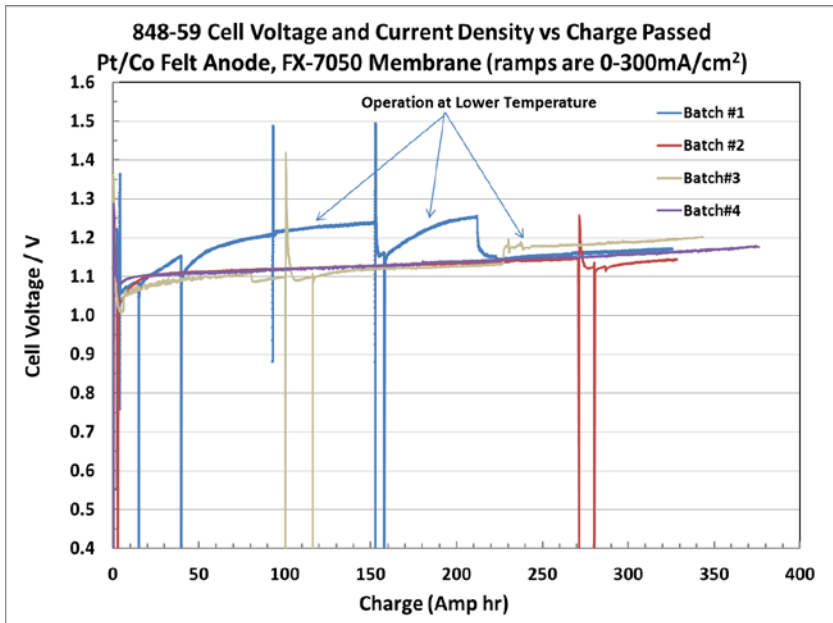


U.S. Patent Issued on Coated Redox Materials for Chemical and Thermochemical Reduction

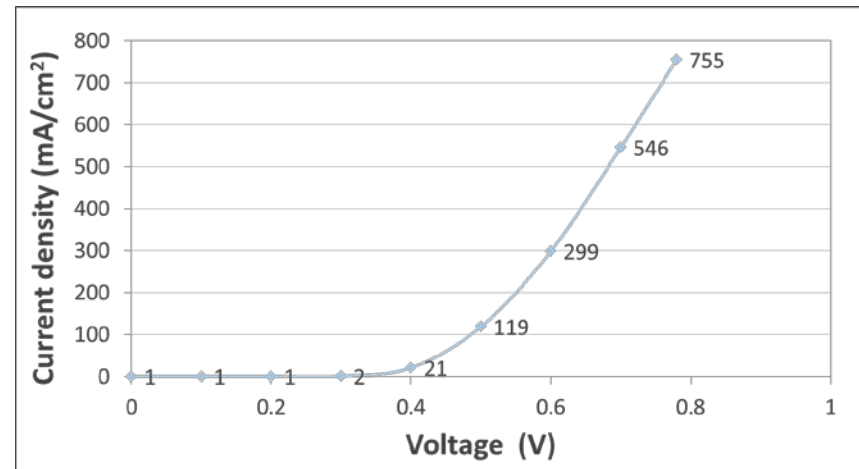
*High performance membranes and electrocatalysts are key for hybrid cycles*

## Sulfur Ammonia Cycle (SAIC)

- Demonstrated long term voltage stability of complete electrochemical system (500+ hour extended run)
- Identified new membranes with up to 2 orders of magnitude lower sulfite crossover fluxes



## Cu-Cl Cycle (ANL /GTI/Penn State)



- 5cm<sup>2</sup> electrolyzer ran successfully for 168 h at milestone value of 300 mA/cm<sup>2</sup> at 0.7V
- One cell, 300 cm<sup>2</sup>, electrolyzer ran at >500 mA/cm<sup>2</sup> at 0.7V (exceeding 2015 design target)

## Innovative wide band gap semiconductor material systems to produce hydrogen from sunlight and water through low-temperature photoelectrochemical processes

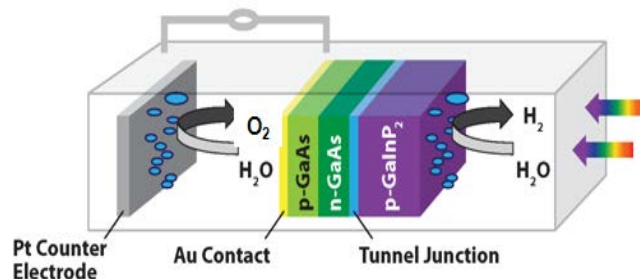
### R&D Approach and Focus

- Innovative crystalline, thin-film and nano-structured material systems to meet efficiency, durability and cost requirements
- Technoeconomic analysis to establish efficiency and durability requirements for meeting DOE cost goal

### Efficient Crystalline Systems

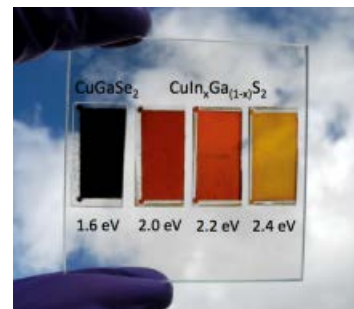
- III-V materials and integrated tandem devices (*NREL*)
- Stabilization of III-V PEC interfaces (*NREL, LANL*)

*III-V material systems R&D utilizing advanced theory, synthesis and characterization capabilities*



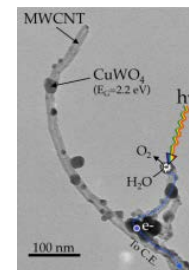
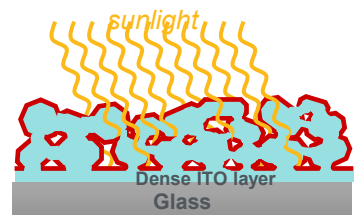
### Durable, low-Cost Thin-Film systems

- Novel metal oxide, copper chalcopyrite and silicon carbide thin-film materials and devices (*MVSystems, UH*)
- Large-scale integrated thin-film PEC electrode device fabrication (*MWOE*)



### Innovative Nano-structured Systems

- Quantum-confined MoS<sub>2</sub> photocatalysts on nano-structured support scaffold (*Stanford, LBNL*)
- Mixed oxide photocatalyst particles (*UH*)



### Cross-Cutting PEC Materials R&D Efforts

- Theoretical modeling of PEC interfaces and bulk bandgaps (*LLNL, UTA*)
- Advanced spectroscopic characterization (*UNLV*)
- Standardized PEC protocols (*PEC WG*)

*Thin-film and nano-structured materials R&D leveraging theory, synthesis and characterization tools*

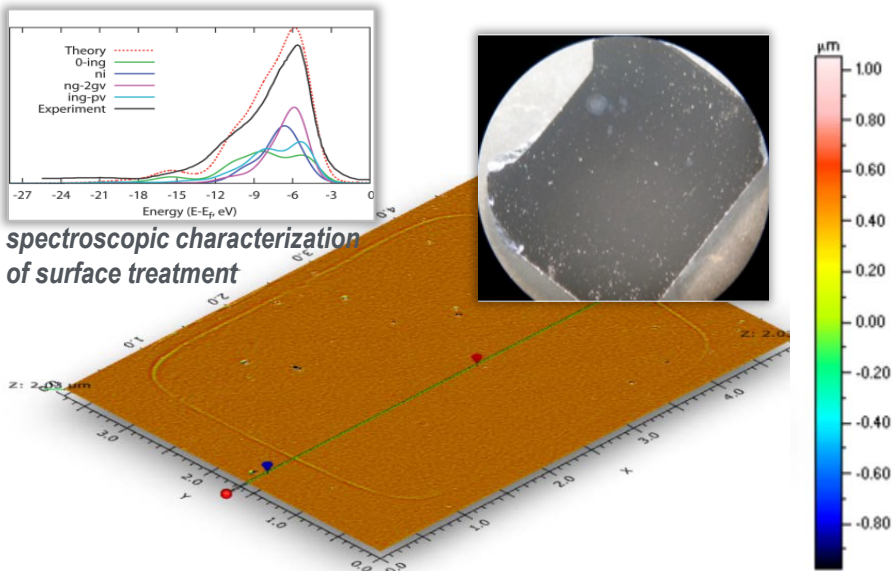
# 2013 Progress: Photoelectrochemical

**Significant new PEC progress this year in stabilizing high-efficiency crystalline materials and in developing new lower-cost thin films**

**Developed reproducible process to extend III-V durability at high production rates**  
(NREL / UNLV / LLNL)

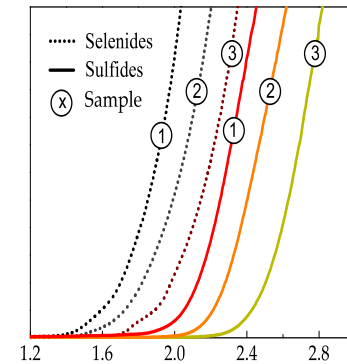
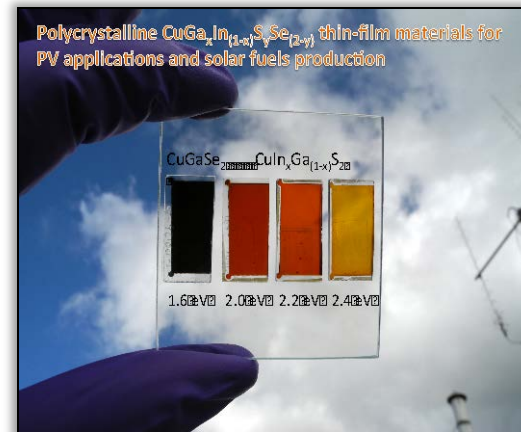
Reproducible  $N_2^+$  ion treatment to protect high-efficiency GaInP<sub>2</sub>/GaAs tandem PEC devices from corrosion achieved.  
Durability demonstrated under operating conditions comparable to 25% STH

*No detectable etching in treated tandem photoelectrodes after 24 hours at high current density of  $\sim 20\text{mA}/\text{cm}^2$*



**Demonstrated bandgap tuning to optimize a promising thin-film material class**  
(MVSystems / U. Hawaii)

Reproducible control over bandgap achieved in copper chalcopyrite material systems is critical to the design and development of efficient PEC tandem devices based on lower cost thin-films



- Chalcopyrites with bandgap ranging from 1.1eV (selenides) to 2.5eV (sulfides) successfully fabricated,
- In/Ga ratio in sulfides adjusted to match 2.0eV  $E_g$  target
- PEC tests show significant charge carriers generation.

## Innovative reactor configurations and genetic engineering used to improve microbial hydrogen production

### R&D Approach and Focus

- Development of strains with improved hydrogen production capacity
- Technoeconomic analysis to establish efficiency and production duration requirements for meeting DOE cost goal

### Develop O<sub>2</sub>-tolerant photolytic organisms

- Engineered cyanobacterial strains with non-native, oxygen-tolerant hydrogenases (NREL, JCVI)
- Algae with modified or replaced hydrogenases to reduce oxygen sensitivity (NREL)

### Improved photo-biological activity

- Increase light utilization by reducing collection of excess photons (UC-Berkeley)
- Improved energy flow from photosynthesis to hydrogen production pathways (NREL, JCVI)

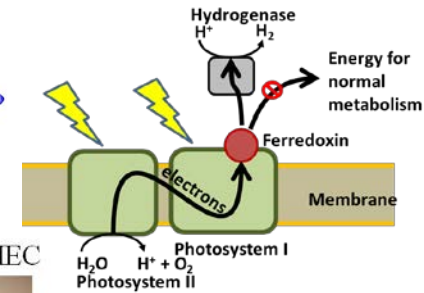
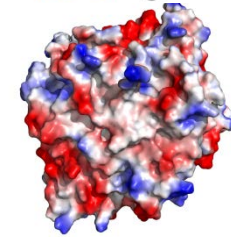
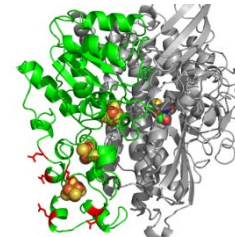
### Feedstocks

- Improved utilization of less refined biomass feedstocks (cellulose, corn stover) through genetic engineering, optimized mixtures of strains (NREL)
- Optimized Microbial Electrolysis Cells (MEC) to produce hydrogen from fermentation wastewater (Penn State)

### Reactor designs

- Improved sequence-batch bioreactor systems (NREL)
- Innovative MEC designs to reduce or eliminate external power requirements (Penn State)

Genetic engineering to improve strain's hydrogen production capacity



single-chamber MEC



Cathode  
Brush anode



Improved reactor designs for better feedstock utilization, hydrogen production rates

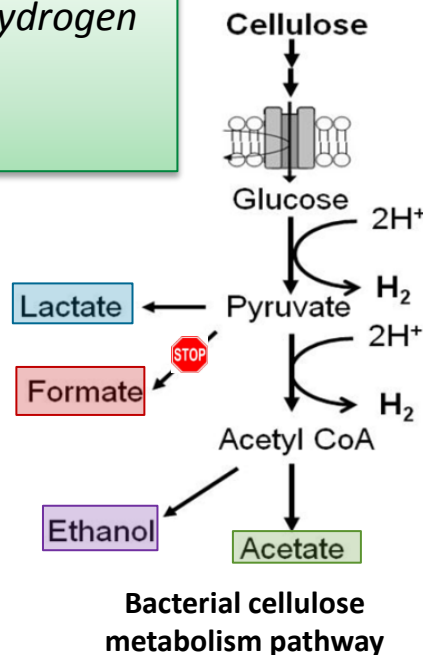
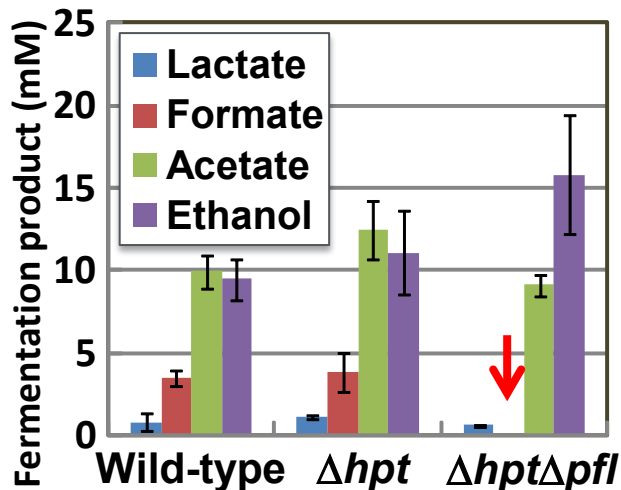


## Genetic engineering to improve biological hydrogen production

### Eliminating competing metabolic pathways (NREL)

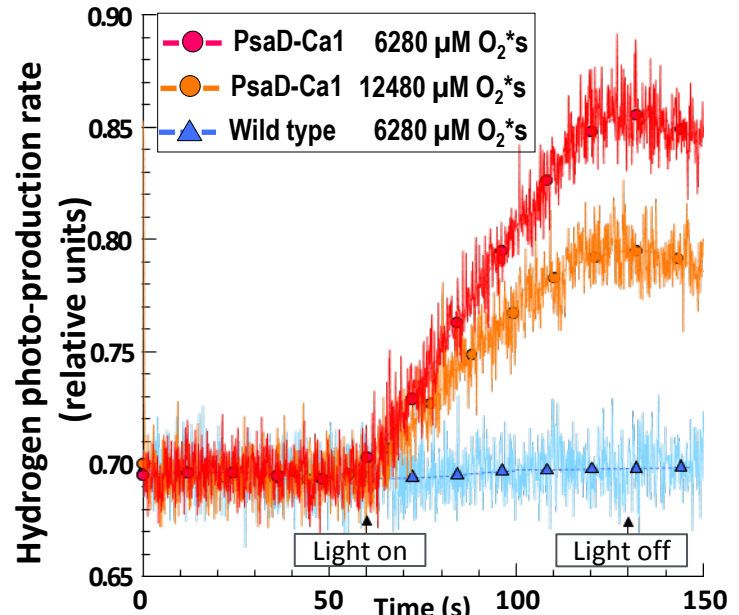
- Developed *Clostridium thermocellum* strain ( $\Delta hpt$ ) for improved mutant generation method
- Generated strain missing the pyruvate-to-formate pathway ( $\Delta hpt\Delta pfl$ ), which consumes pyruvate that could be used for hydrogen production

Next steps: determine effect on hydrogen production, and knock-out other competing pathways



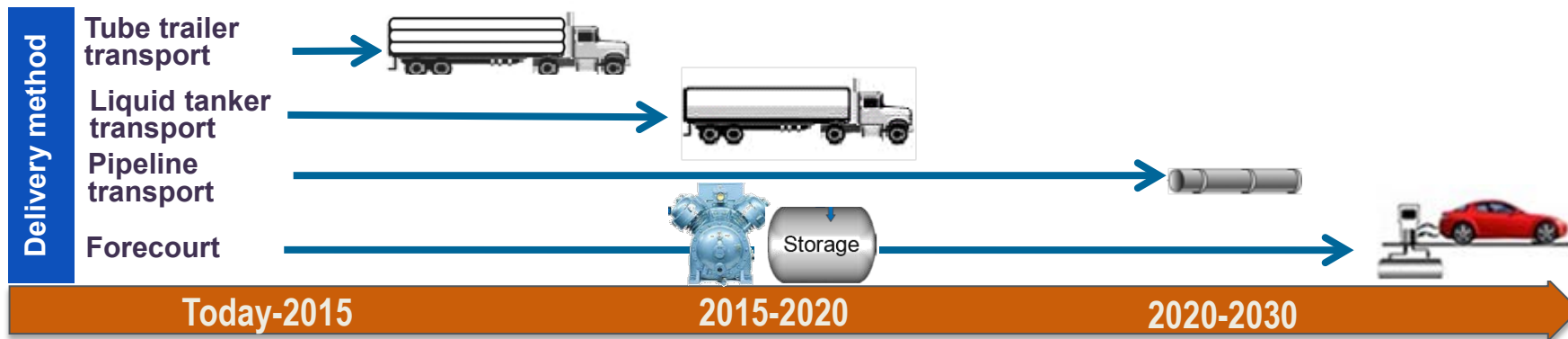
### Improving oxygen tolerance (NREL)

- Demonstrated light-induced hydrogen production in algae with bacterial Ca1 hydrogenase at oxygen concentrations equivalent to 80% of air, more than double the oxygen that wild-type algae can tolerate

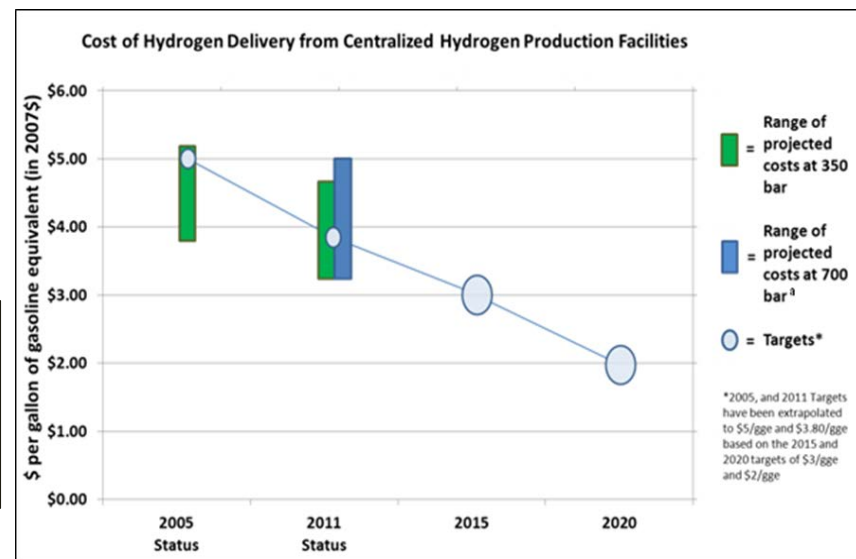
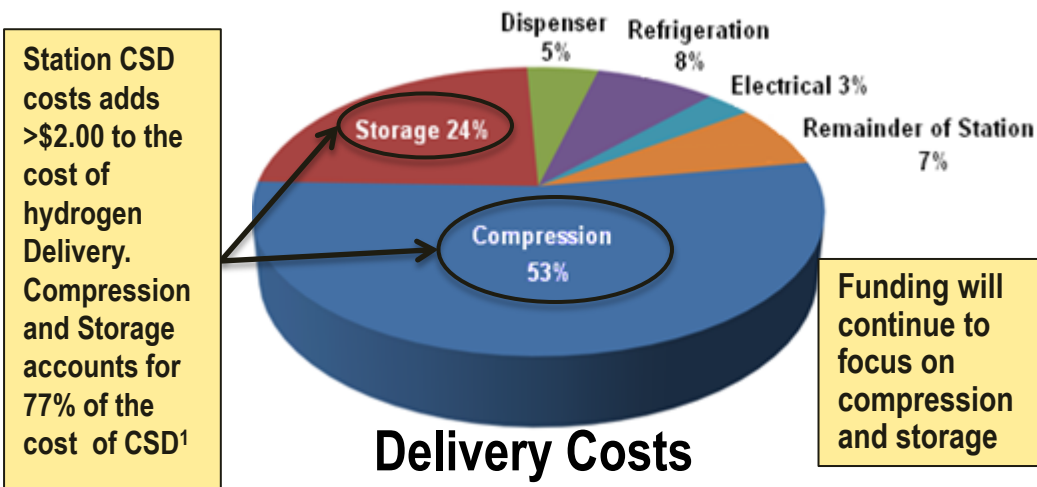


Next steps: genetic engineering for high, stable Ca1 hydrogenase expression

# Delivery: Compression, Storage and Dispensing (CSD) Cost Reduction



- Advanced tube trailer GH<sub>2</sub> transport
- Conventional LH<sub>2</sub> transport
- Mobile re-fuelers
- Forecourt GH<sub>2</sub> production
- Improved liquefaction
- Cold GH<sub>2</sub> transport
- Improved, low-cost forecourt technology (compression & storage)
- Pipeline GH<sub>2</sub> transport
- Advanced energy efficient liquefaction
- Dedicated forecourts with advanced compression/ storage/dispensing technology



\*Based on 2011 advances projected to high volume

## *Lowering the Cost of Forecourt CSD is a top priority for FY13/14*



### Near-term

- Improve forecourt compressor cost, reliability & efficiency through improved seals and other R&D advancements
- Address dispenser cost and reliability through SBIR projects and investigation of existing failure modes
- Decrease the footprint and cost of storage at the forecourt through advanced composite designs

### Longer-term

- Focus on materials research to enable high volume hydrogen delivery (FRP pipelines, High-pressure composite tube trailers, Carrier technologies...)
- Research and develop advanced compression technologies for high reliability and through-put

***CSD Workshop Proceedings posted on FCTO website!***

*Direct fills from high pressure tube trailers can reduce capital at the forecourt by ~40%*

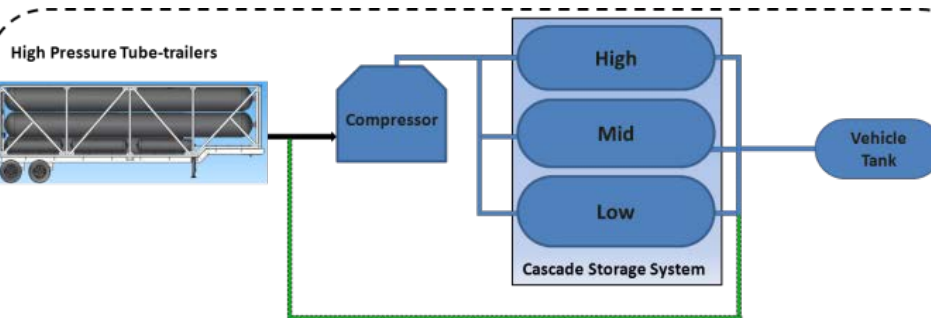
**Compression, Storage, and Dispensing (CSD) Independent Panel review of the assumptions used by the hydrogen delivery scenario analysis model (HDSAM) V2.32. Report finalized Q3 FY13**



FLOW-250 SCFM  
150 HP



ANL



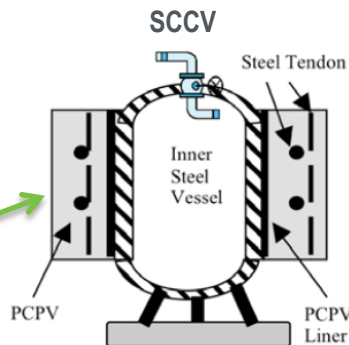
**CSD cost minimized by:**

- ✓ **Optimized compression to storage capacity**
- ✓ **4-5 cascade storage banks**
- ✓ **Direct fills from high-pressure tube trailers**

*Demonstrated that high pressure steel-concrete composite vessels (SCCV) for hydrogen storage can exceed the relevant cost targets (ORNL)*

## Near Term Forecourt Storage (ORNL)

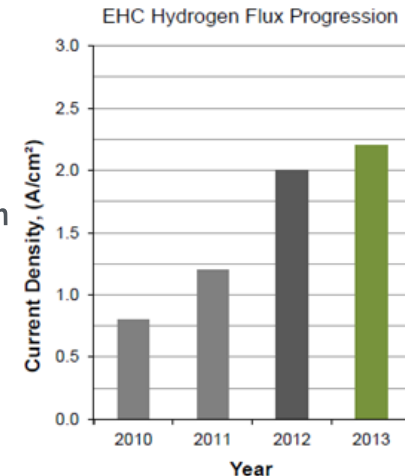
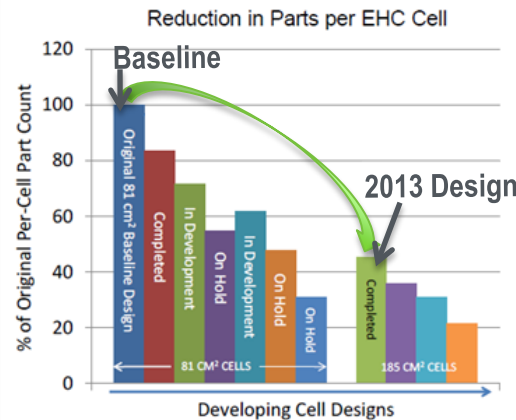
- ✓ Validated ability to meet 2020 target of \$1000/kg of hydrogen stored at 860 bar using optimized design (target exceeded).
- ✓ Successfully demonstrated ability to use Friction Stir Welding (FSW) to lower manufacturing cost
- ✓ Completed a manufacturing study – posted on OSTI: *ORNL/TM-2013/113*



50/50 split between steel and concrete was selected as the optimal design for cost and strength.

## Long Term Forecourt Compression (FCE)

- ✓ Reduced electrochemical compressor cell part count through design innovations by >50%
- ✓ Increased operating current density by ~3X over the 2010 baseline
- ✓ Combined, this results in a greater than 50% cost reduction over the 2010 baseline

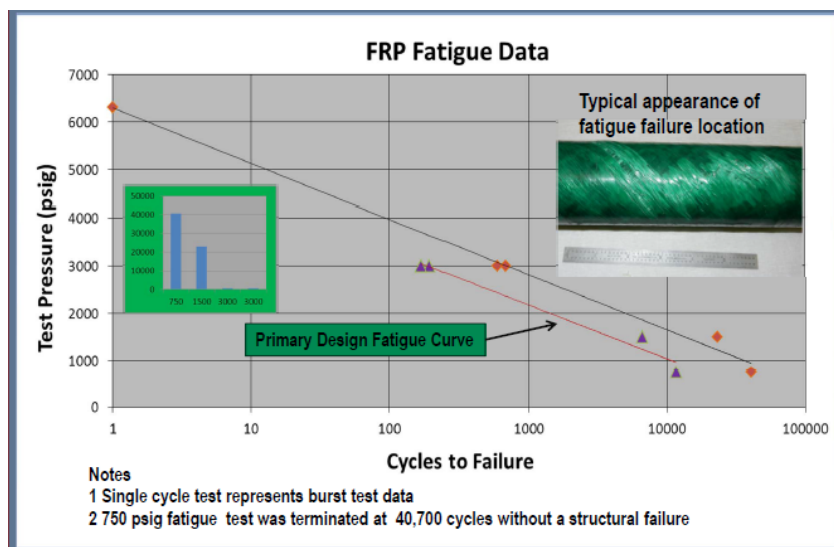


## Fiber reinforced polymer (FRP) pipelines and new compressor technology can reduce cost

### FRP pipeline testing (SRNL)

**Can reduce installation costs by 20– 40%**

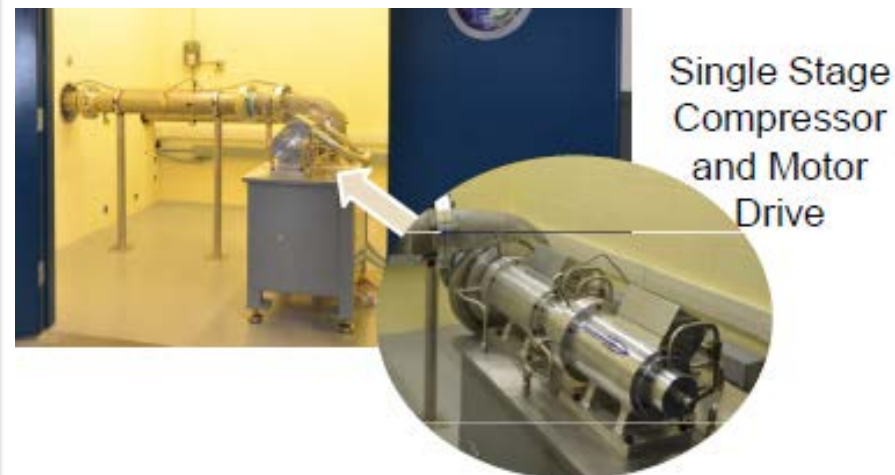
- ✓ Fatigue testing completed over the range of 750 to 3000 psig
- ✓ Calculated FRP fatigue design curve from data
- ✓ Report submitted to ASME for inclusion in B31.12



### Detailed designs for high speed centrifugal H<sub>2</sub> compressors (Mohawk)

**Potential to reduce capital cost by 20% and O/M costs by 30%**

- ✓ Selected double-entry design over single-entry
- ✓ Completed single stage prototype fabrication and verified achievement of performance goals through testing in air and He at 55,000 RPM

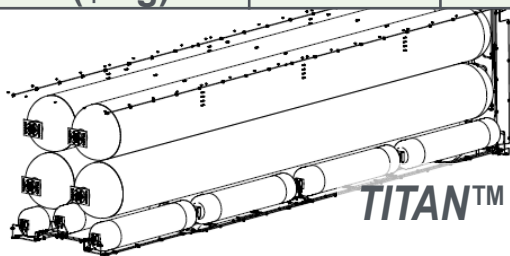


*High pressure composite tube trailers show significant potential to meet the 2020 tube trailer delivery targets*

## Tube Trailer Delivery (Hexagon Lincoln)

- ✓ Exceeded DOE 2015 delivery capacity target using Hexagon Lincoln's TITAN™ V Magnum Trailer System (originally designed for the 2010 targets)
- ✓ 350 bar design shows promise toward the 2020 targets.

	250 Bar (Available)	350 bar (Designed)	DOE 2015 Target	DOE 2020 Target
<b>Delivery Capacity (Kg)</b>	720	907	700	940
<b>Capital Cost (\$/kg)</b>	744	710	730	575

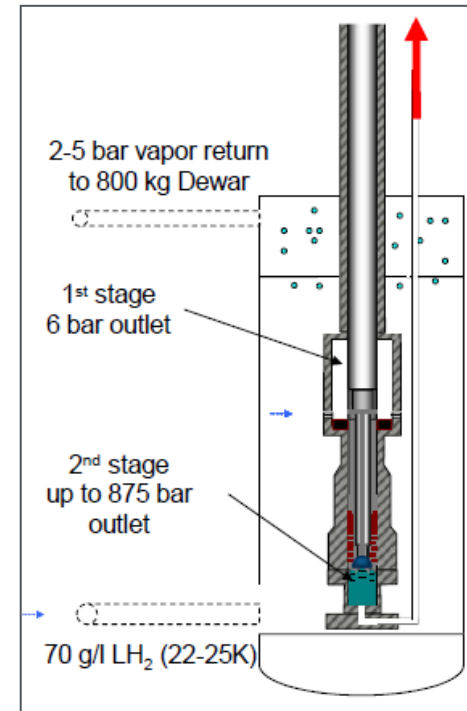


**TITAN™ V Magnum Trailer**

## Liquid Delivery (LLNL)

*Cryogenic liquid pumps have the potential to reduce energy consumption and capital cost at the forecourt*

- ✓ Pump installation in progress, efficiency validation to follow
- ✓ Successful test of high pressure cryogenic 3 ft. hose segment
- ✓ Completed electrical and civil work necessary for pump installation



**Pump rated at 900 bar**

## INTERNATIONAL ACTIVITIES

### Examples:

- IEA HIA Tasks 21, 23-28
- Infrastructure Workshop
- IPHE

## I<sup>2</sup>CNER - Japan

Director: Dr. Petros Sofronis

Focus on H<sub>2</sub> production, delivery, and FC technologies

## DOE/EERE

### H<sub>2</sub> Production and Delivery Applied R&D

- > 30 projects
- 14 SBIR projects:
  - Home Refueling
  - Electrochemical Process Intensification
  - Large Scale PEM Electrolysis
  - Sorbents for Biofueled SOFCs
  - Hydrogen Fueling Station Cost Reduction

## INDUSTRY

- U.S. DRIVE Partnership
  - Tech teams:
    - H<sub>2</sub> Production
    - H<sub>2</sub> Delivery
- Codes & Standards Organizations

## TECHNOLOGY VALIDATION (DOE EERE)

>180 vehicles & 25 hydrogen stations

## National Collaboration (*inter- and intra-agency efforts*)

DOE Basic Energy Sciences

Over 25 Projects

DOT/NIST

DOE Bioenergy Technologies Office

National Science Foundation

DOE Fossil Energy

DOE Nuclear Energy

ARPA-E



## *Hydrogen Production & Delivery Team*

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