



Fuel-Cell Fundamentals at Low and Subzero Temperatures

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Lawrence Berkeley National Laboratory

Solicitation Partners:

United Technologies Research Center

Los Alamos National Laboratory

3M Company

The Pennsylvania State University

Project ID #

FC 026

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Overview

Timeline

- ↩ Project initiated FY09
 - ☞ Start **September 2009**
- ↩ 4 year project duration
 - ☞ End **September 2013**
- ↩ ~85% complete

Budget

- ↩ Total Project Funding: \$5,145k
 - ☞ DOE share: \$ 4,700k
 - ☞ Contractor share: \$ 445k
- ↩ Funding Received in FY11: \$812.5k
- ↩ Funding Received in FY12: \$1,290k
- ↩ Planned Funding for FY13: \$1,095k
 - ☞ LBNL \$510k
 - ☞ Partners \$585k

Barriers

- ↩ A. Durability
- ↩ C. Performance
 - ☞ Cell Issues
 - ☞ Stack Water Management
 - ☞ System Thermal and Water Management
 - ☞ System Start-up and Shut-down Time and Energy/Transient Operation

Partners

- ↩ Project lead: **Lawrence Berkeley NL**
- ↩ Direct collaboration with Industry, National Laboratories and University (see list)
- ↩ Other collaborations with material suppliers and those with unique diagnostic or modeling capabilities
- ↩ Discussion with related project leads



Collaboration: Organizations/Partners

3

* Lead

↳ **Lawrence Berkeley National Laboratory:** Adam Weber, Ahmet Kusoglu, Clayton Radke, Alastair MacDowell, Alexander Hexemer, Frances Allen

* Subcontractors

↳ **Los Alamos National Laboratory:** Rod Borup, Rangachary Mukundan

↳ **3M Company:** Mark Debe, Andy Steinbach

↳ **United Technology Research Center:** Michael Perry

↳ **The Pennsylvania State University:** Chao-Yang Wang

* Other relationships (directly funded through other DOE projects)

↳ **Ion Power:** Stephen Grot (membrane and MEAs)

↳ **NIST:** Daniel Hussey, David Jacobson (neutron imaging of water)

↳ **The Pennsylvania State University:** Michael Hickner (membrane thin films)

↳ **Oak Ridge National Laboratory:** Karren More (GDL imaging)

* Other relationships (no cost)

↳ **UC Berkeley/JCAP:** Rachel Segalman (Nafion® scattering and other studies)

↳ **General Motors:** Craig Gittleman (Nafion® conductivity data)

↳ **Queens\Calgary University:** Kunal Kuran (Nafion® thin-film data and samples)

↳ **University of Michigan:** Massoud Kaviany (Nafion® MD simulations, ESEM)



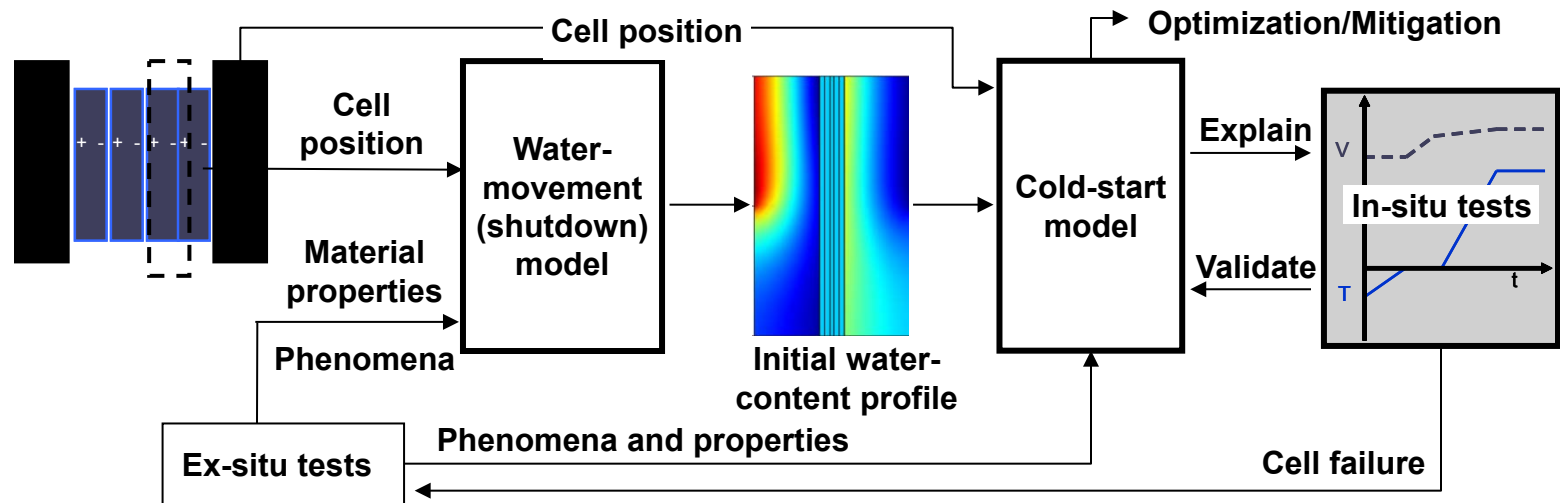
Relevance: Objectives

- * Fundamental understanding of transport phenomena and water and thermal management at low and subzero temperatures using state-of-the-art materials
 - ↳ Examine water management with thin-film catalyst layers (NSTF)
 - ↳ Examine water management and key fundamentals in the various fuel cell components
 - ↳ Enable optimization strategies to be developed to overcome observed bottlenecks
 - ↳ Operational
 - ↳ Material

- * Elucidate the associated degradation mechanisms due to subzero operation
 - ↳ Enable mitigation strategies to be developed

Improved understanding will allow for the DOE targets to be met with regard to cold start, survivability, performance, and cost

* Synergistic effort of modeling and experimental characterization



↪ Multi-scale, multi-physics continuum-based modeling

- ☞ Develop, validate, and refine a series of models for cell performance including cold and cool operation, startup, and shutdown

↪ Experimentally characterize component, cell, and stack properties and performance

- ☞ Measure critical properties including visualizing water and ice distributions
- ☞ Utilize various assemblies and components to elucidate governing phenomena

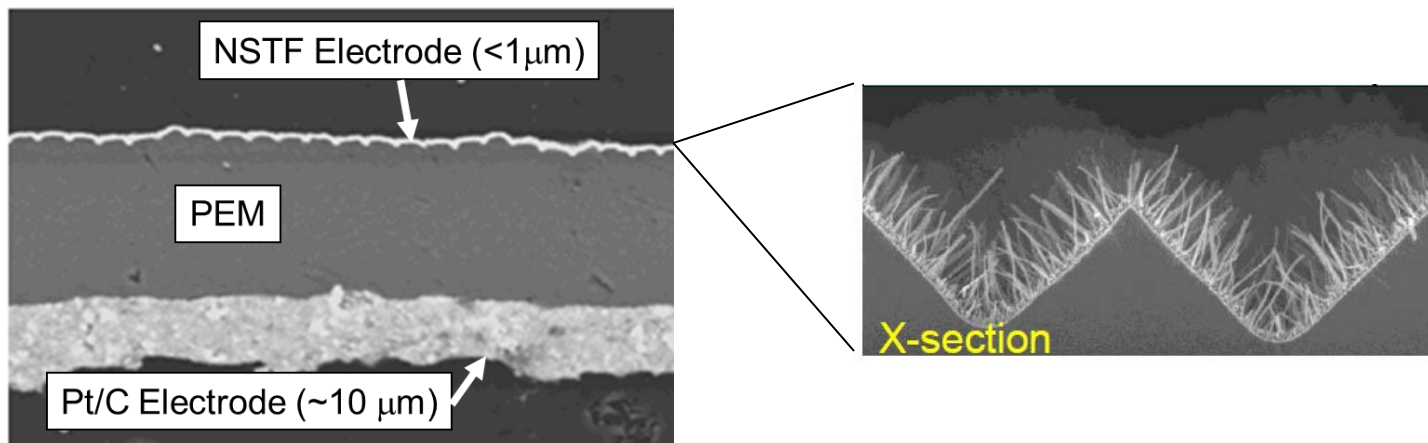
↪ Durability and degradation

- ☞ Elucidate and mitigate critical failure mechanisms related to cold and cool operation
- ☞ Experimentally observe and characterize failed cells

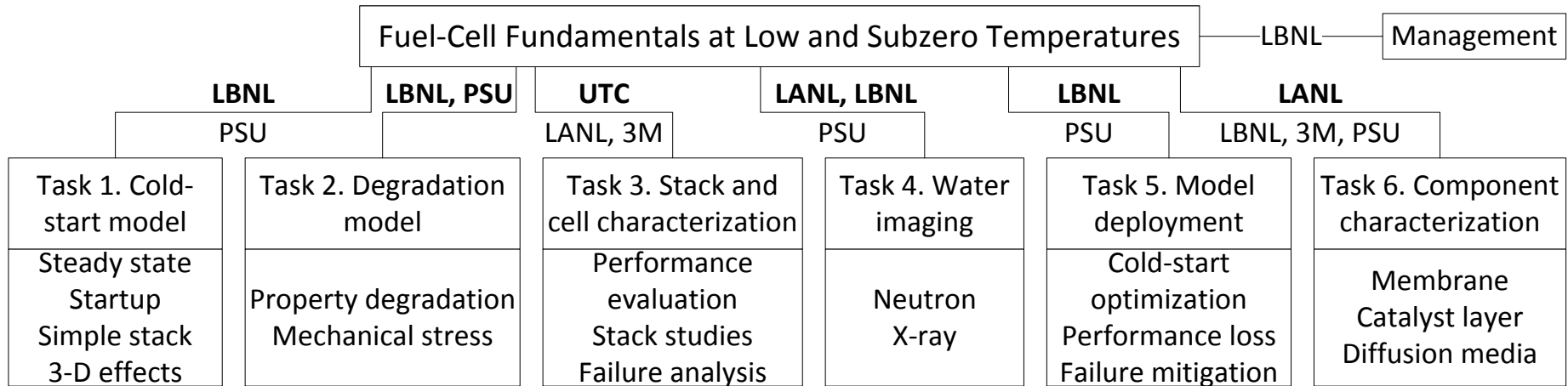
Approach: Cell Assemblies

- Utilize various assemblies to elucidate governing and controlling phenomena

Material	Baseline	Alternative 1	Alternative 2
Membrane	3M 850 EW		
Catalyst layer	NSTF PtCoMn	Low-loaded traditional	
GDL	MRC	SGL	Freudenberg
MPL	Hydrophobic	None	
Flow field	Quad serpentine		
Bipolar plate	Solid	Hybrid (one WTP)	



Workplan/Organization



LBNL

- ↪ Project management and coordination
- ↪ Model development
- ↪ GDL and membrane characterization

LANL

- ↪ Ex-situ component characterization
- ↪ Single-cell durability tests
- ↪ Neutron imaging

3M

- ↪ Material supplier, single-cell testing, and testing knowledge including conditioning procedures

UTRC

- ↪ Cell parametric studies
- ↪ Identify failure mechanisms
- ↪ Real-world guidance

PSU

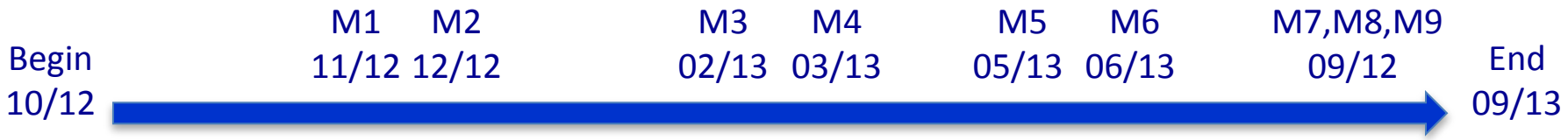
- ↪ Develop 3-D scaling expressions and mechanical stress model

Other

- ↪ Provide unique materials and diagnostics



Approach: FY13 Project Timeline

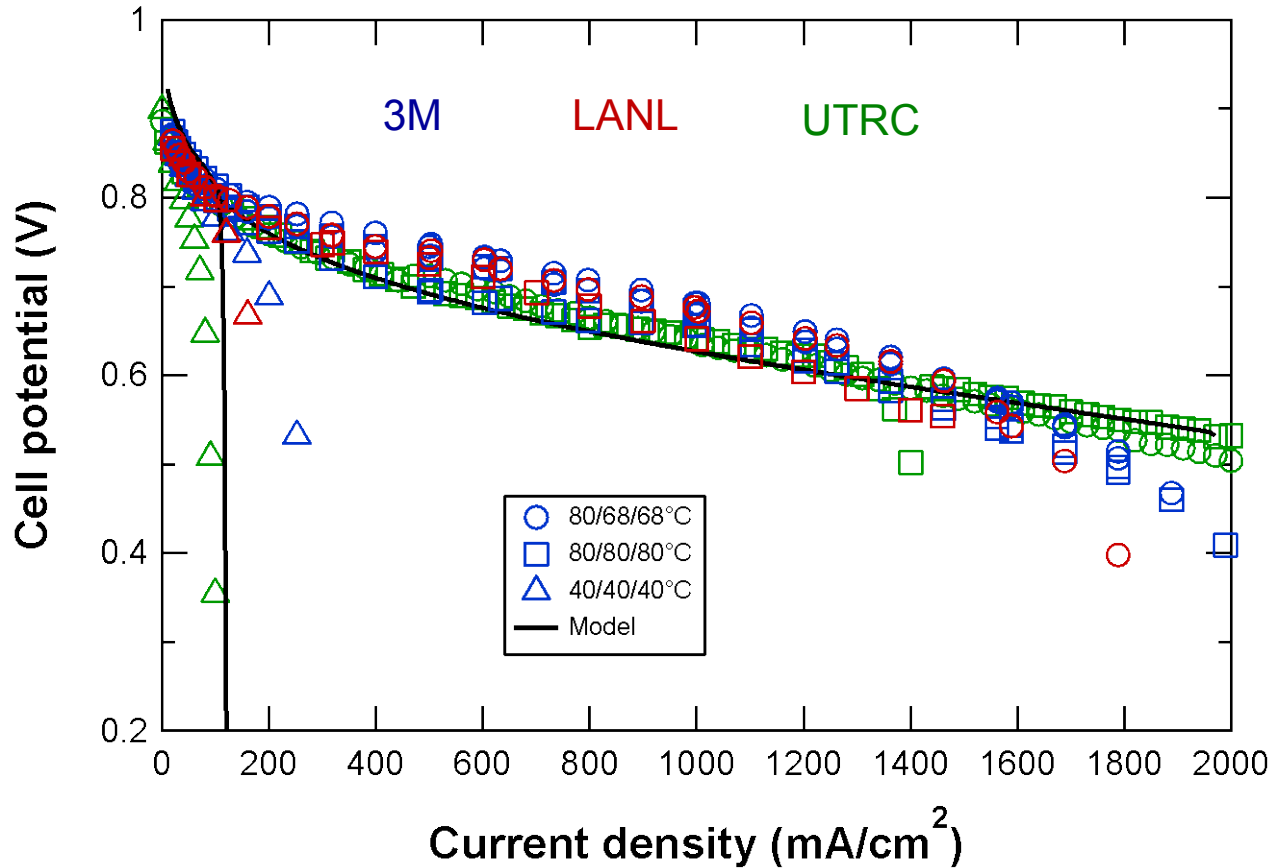


Major Milestones/Deliverables

- M1:** Correlation developed between isothermal start and freeze/thaw with observed catalyst-layer cracking under ESEM and in-situ cell studies. (*completed, NSTF has much greater durability*)
- M2:** Impact of 3 different GDLs on cell performance with two different cell-compression levels. (*completed*)
- M3:** Agreement (<10% deviation) between model analogs and real MPLs in terms of breakthrough pressure and capillary-pressure – saturation behavior. (*delayed due to issues of finding appropriate model materials*)
- M4:** Results of impact of water balance on startup performance for both NSTF and low-loaded traditional MEAs. (*slight delay due to experimental reproducibility that appear to be resolved*)
- M5:** Report of rainbow short-stack results with different cell diffusion media and baseline MEAs. (*changed to studies using the adiabatic cell based on reviewer and Tech Team feedback*)
- M6:** Complete low and high resolution imaging of 3M cells and report results to LBNL. (*on track, some high resolution studies already completed*)
- M7:** Report on optimum operating conditions and material properties for NSTF catalyst layers operating below 55°C. (*on track, model agreeing with experiments and now looking at parameter space*).
- M8:** Impact of 3 different NSTF peak heights on cell performance. (*on track, 1 of 3 peak heights completed*)
- M9:** Model results showing importance of compressive loads and mechanically induced degradation by layer including experimental comparison with ice-front propagation. (*on track, initial mechanical model completed*)

Baseline Performance

- * Baseline system is 3M NSTF “2009 best of class” MEA including 2009 GDLs



2/2.5 stoichiometry for H₂/Air
150/150 kPa outlet pressures

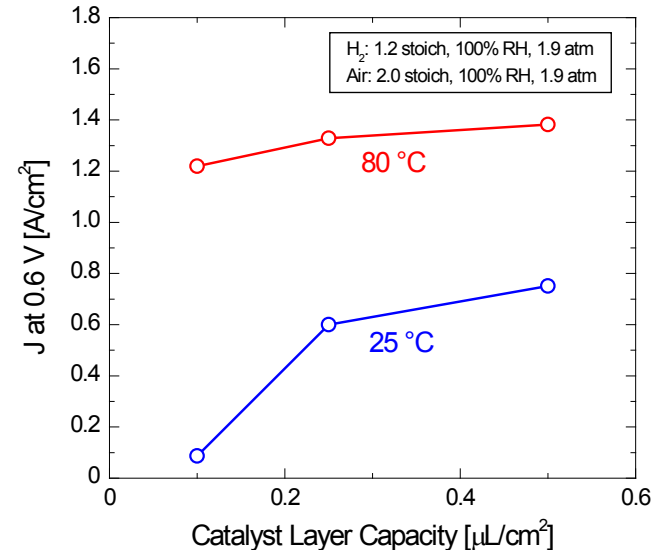
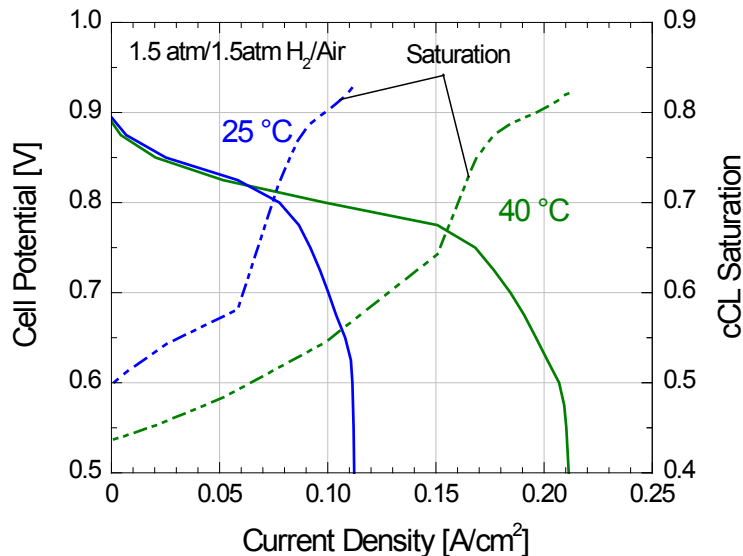
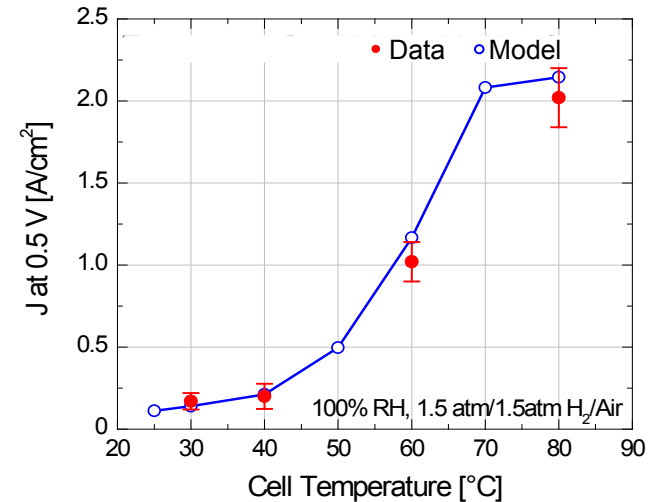
- * Performance among the three cell-testing sites is converged

↳ Lessons learned

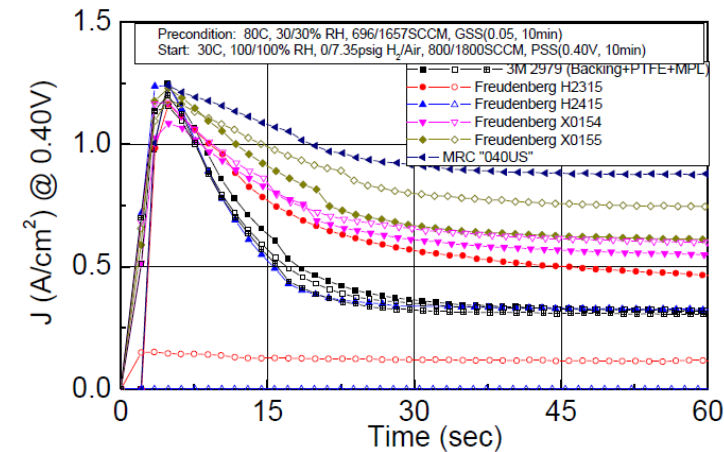
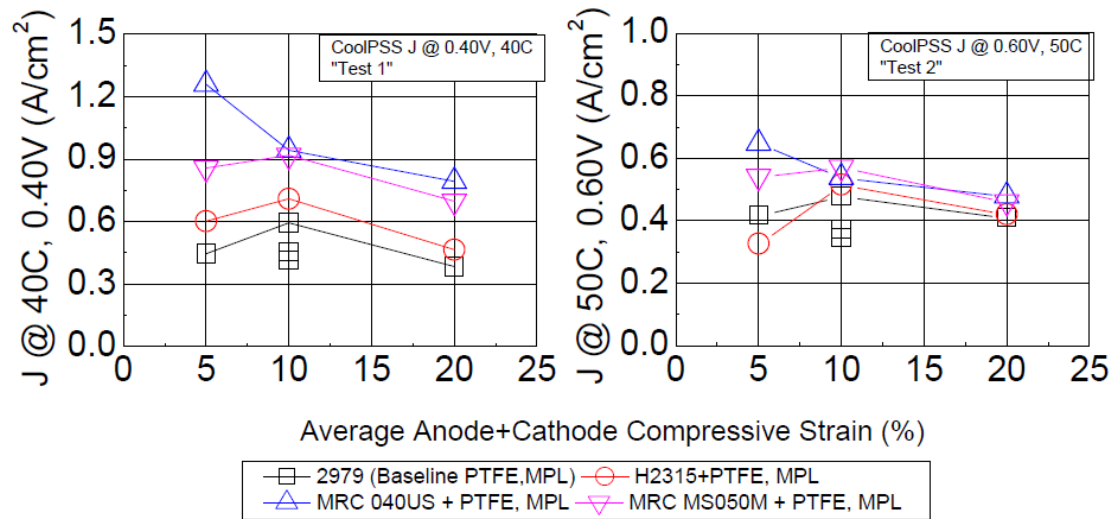
- ↳ Compression and cell assembly/hardware uniformity is critical
- ↳ Need to run and condition NSTF properly

✳ Use 2-D mathematical model to examine performance with NSTF

- ↪ Good agreement with experimental data
- ↪ Significant reduction in limiting current as temperature drops from 70 to 40°C
 - ↪ At higher temperatures the CL temperature is high enough to remove water through vapor phase by phase-change-induced flow
 - ↪ Near room temperature, severe CL flooding reduces the limiting current due to low water-capacity of NSTF CL



- * Evaluation of 4 anode GDLs (backing+PTFE, MPL) as a function of GDL strain
 - ↳ Transient and steady state show better low-temperature performance with MRC 040US
 - ↳ MRC 040US resistance remains too high

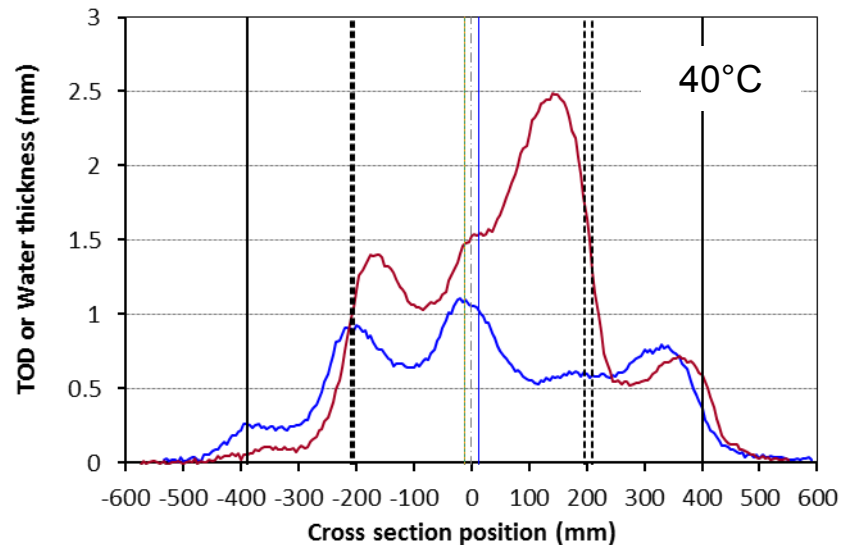
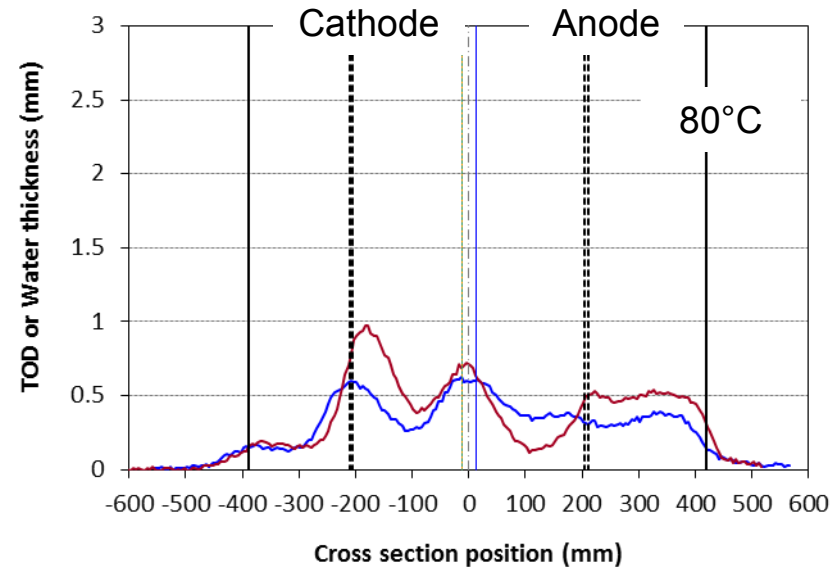


- ↳ Response generally decreases as compression increases from 10 to 20%, less consistent results for 5 to 10%

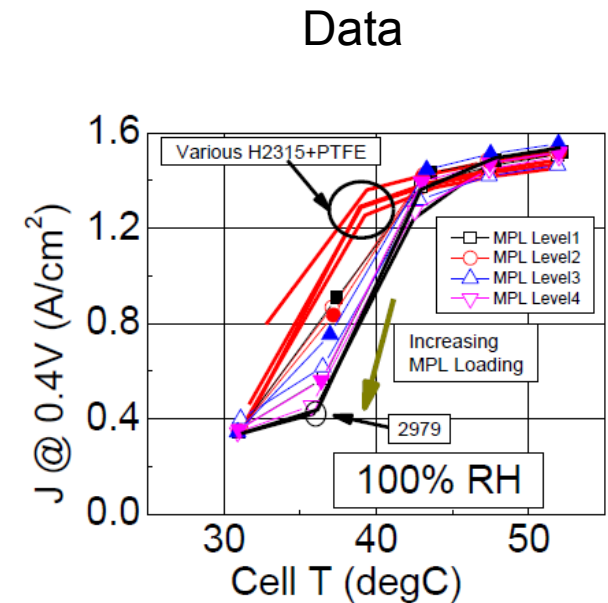
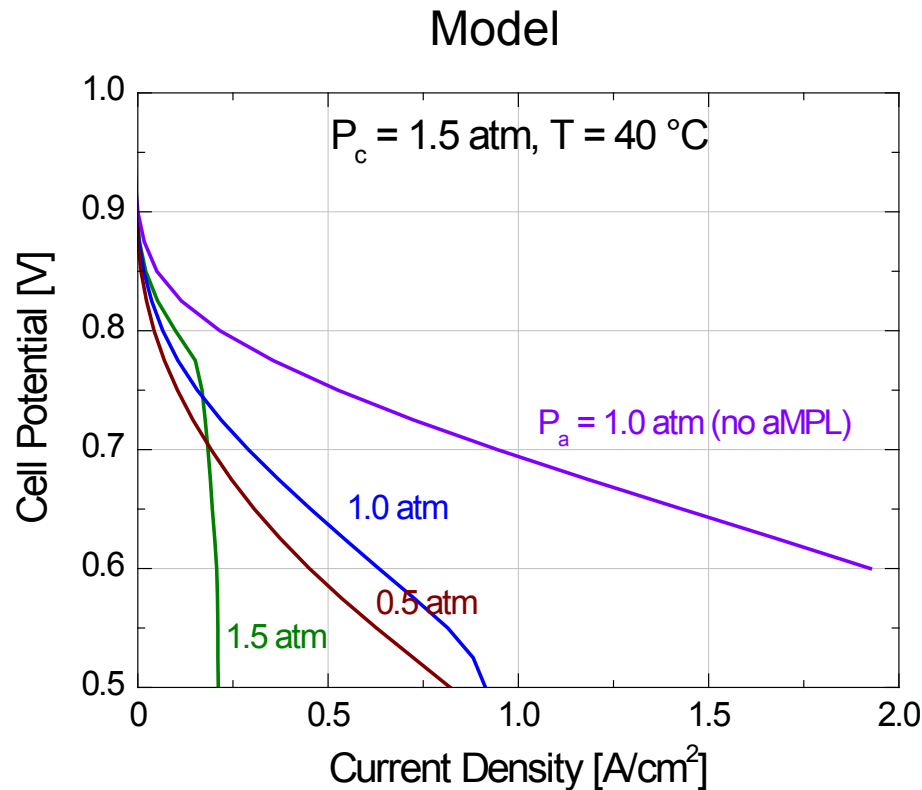
- * Drop off of performance as approach 40 to 50°C

Anode GDL Studies

- * Use high-resolution neutron imaging to compare water profiles between NSTF with **2979** and **MRC 040US** anode GDLs at 0.3 V
 - ↳ Less water at 80°C than 40°C
 - ↳ MRC 040US anode GDL consistently has less water in the MEA



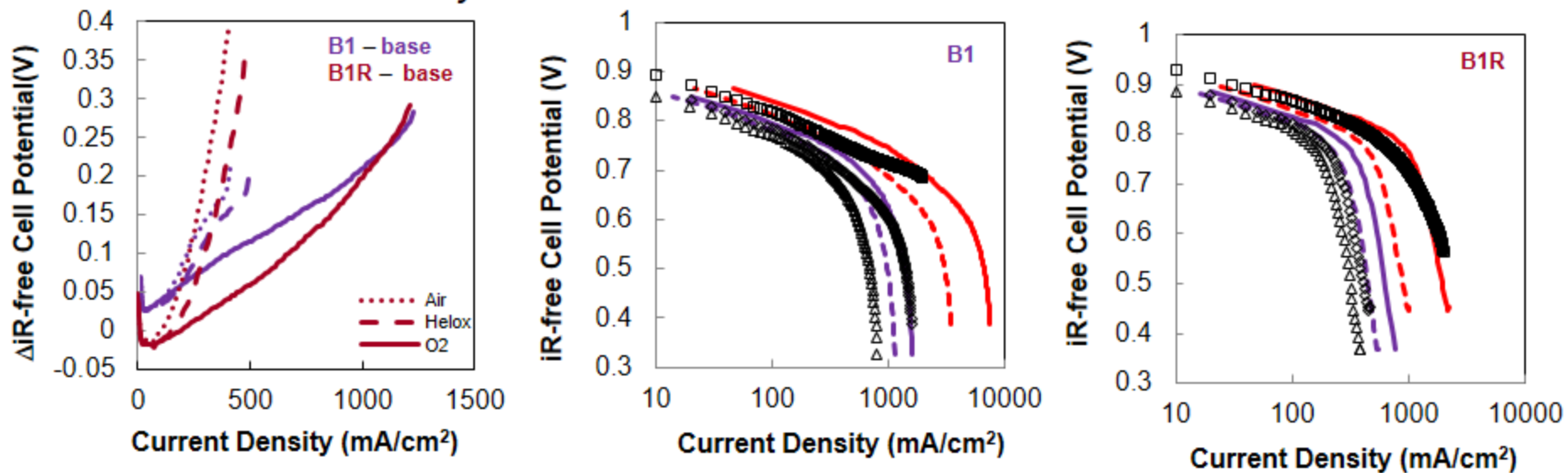
- * NSTF MEA low temperature performance is very sensitive to anode backing
 - ↪ Specific material factors responsible currently unknown



- ↪ Model shows the importance of reducing liquid-water transport resistance and enhancing back transport

Oxygen-Gain Analysis

Examine hybrid cells at 35°C with one NSTF and one Pt/C



* Performance loss at low T appears to be due to transport limitations

- ↳ Ionic limitation and not O₂?
- ↳ Change in H₂ kinetics

↳ Anode NSTF

- ↳ Performance a function of oxidant
- ↳ Ohmic limited at moderate current; limiting currents are ~ 1st order

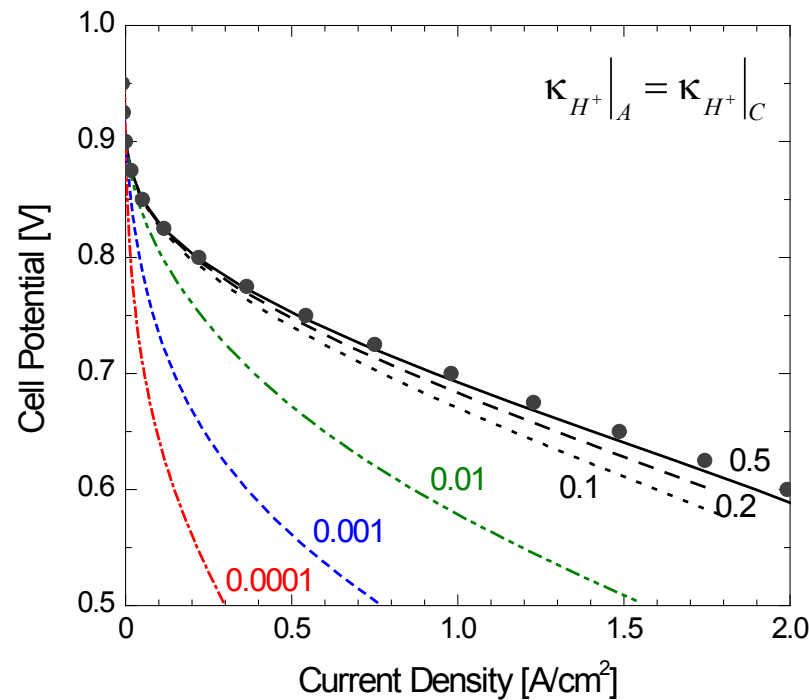
↳ Cathode NSTF

- ↳ Different behavior on different oxidants 1st order on O₂, ~ 1/2 order on air

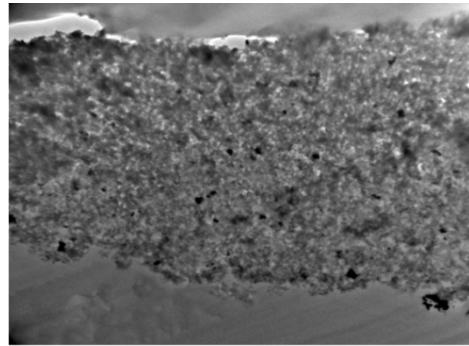
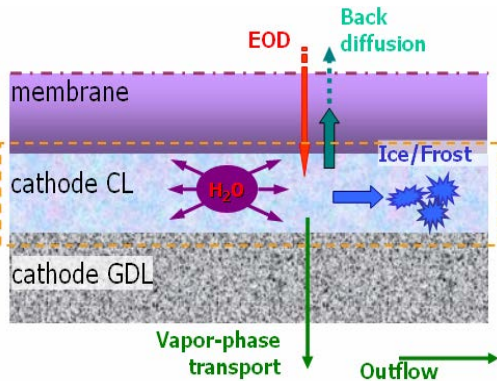
	Anode (mg/cm ²)	Cathode (mg/cm ²)
B1	0.05 Pt/C	0.10 NSTF
Base	0.05 NSTF	0.10 NSTF
B1R	0.1 NSTF	0.05 Pt/C

- H₂/O₂
- ◇ H₂/Air
- △ H₂/Half Air
- Air, (J x 4.75)
- - - Air, (J x sqrt(4.75))
- 1/2Air to Air, (J x 2)
- - - 1/2Air to Air, (J x sqrt(2))

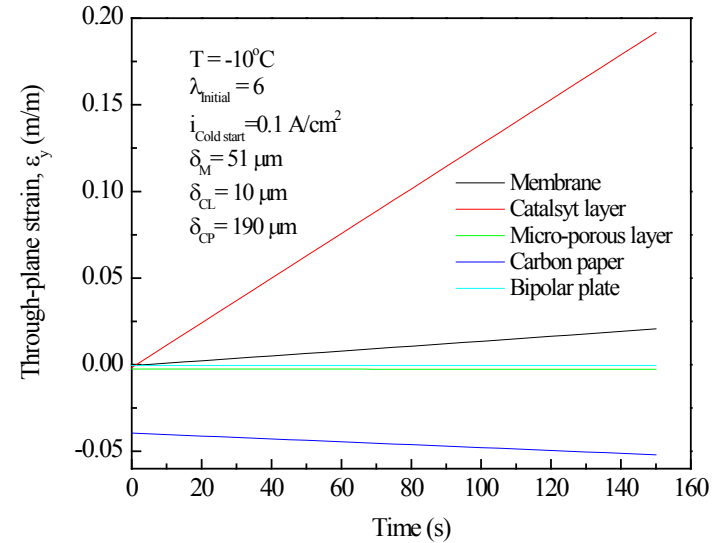
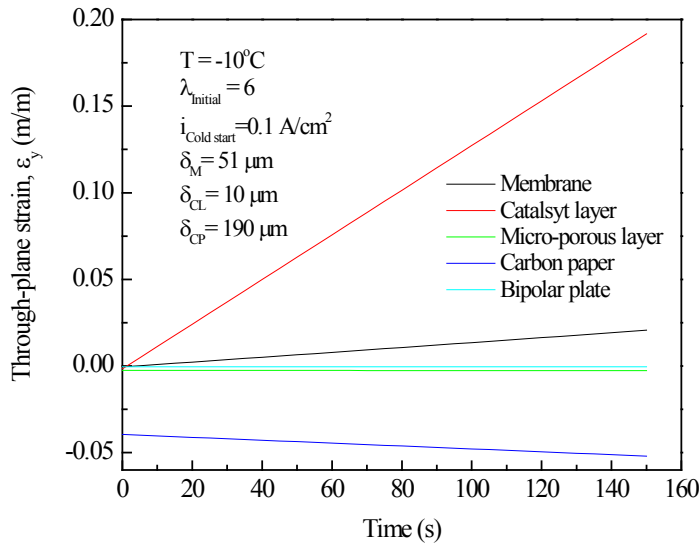
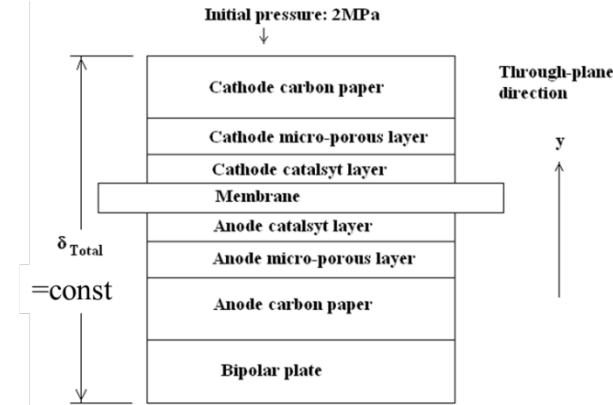
- * Parametric study using **model** without aMPL at 40°C
 - ↳ NSTF proton conductivity has strong influence on the cell performance when conductivity is below 0.1 S/m



* Stress model of fuel-cell sandwich for purge and cold start



Interfacial delamination after 110 cycles of cold-start at 500 mA/cm²

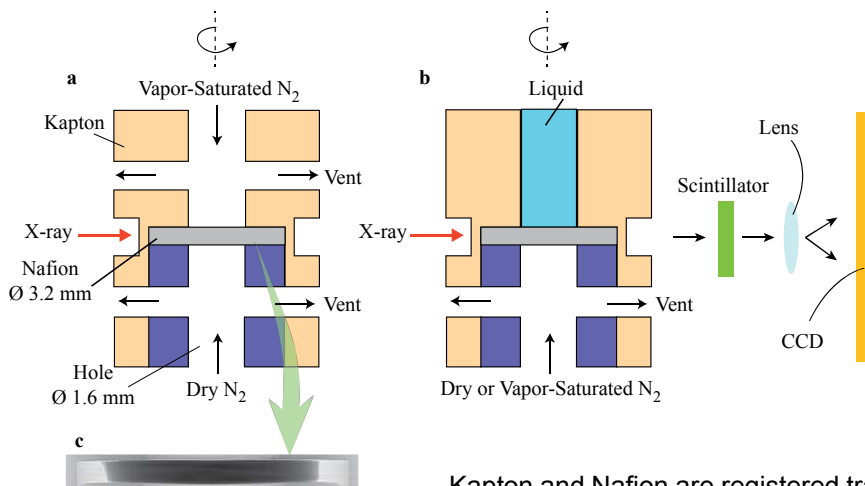
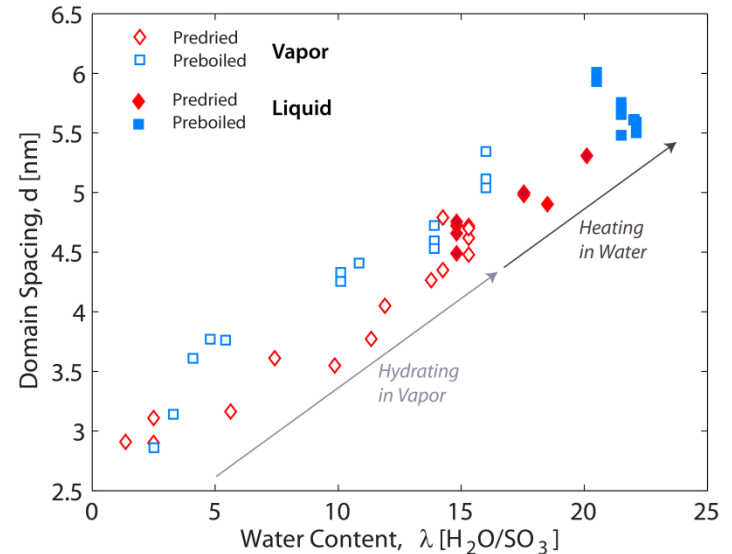


⚡ During cold start, ice production yields very large strain in CL, which could cause CL/mem delamination and CL pore structure collapse

⚡ Cold start from low temperatures leads to large mechanical stress, and high start current density leads to large strain in CL

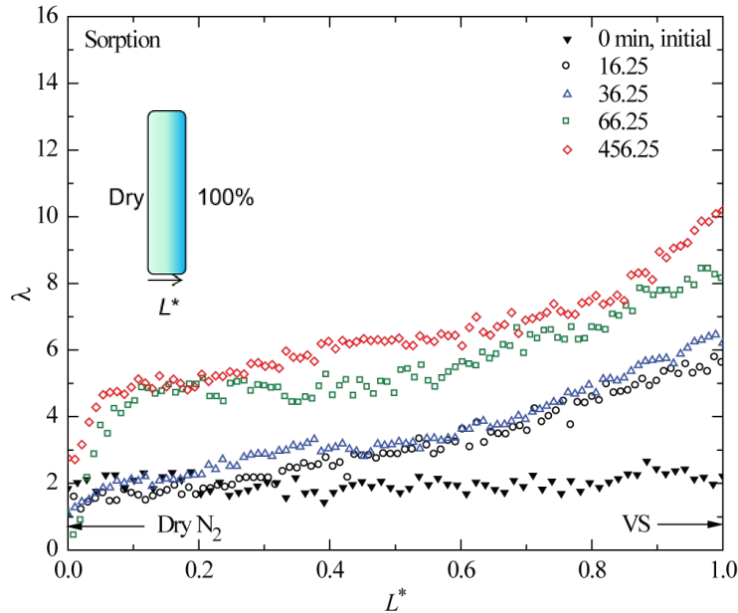
* Understand that pretreatment, crystallinity, and humidity effects are controlled by same chemical/mechanical energy balance

- ↪ Have seen some existence of interfacial phenomena
- ↪ Unknown whether Schroeder's paradox occurs during a gradient
- ↪ The water diffusion coefficient in literature varies, especially its dependence on water content
 - ↪ Expect different concavity in water profiles for dynamic versus steady state

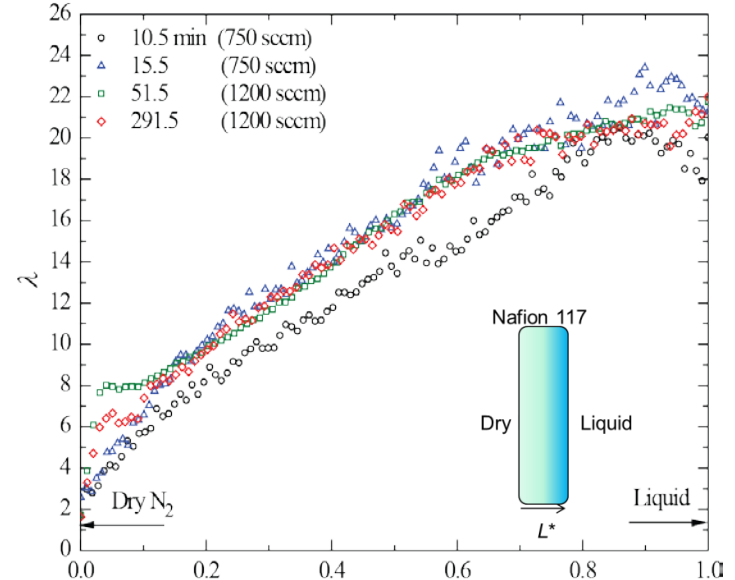


- * Measure membrane water profile
 - ↪ Use x-ray computed microtomography
 - ↪ Good combined temporal (\sim min) and spatial (\sim μm) resolution

Sorption from Dry to 100% RH



Sorption from Dry to Liquid

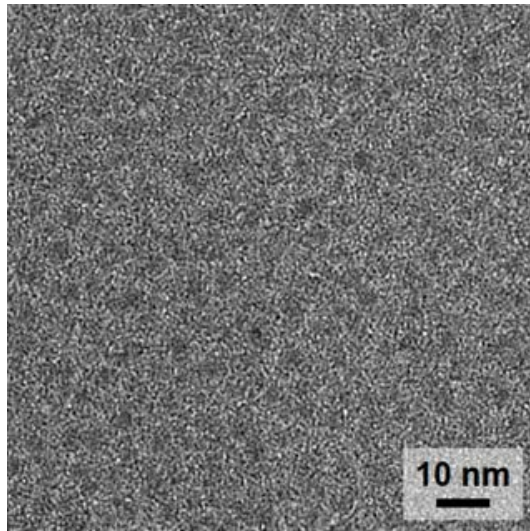


- * With saturated vapor/dry, complex transient and steady-state profile
 - ↳ Shape changes from concave to convex with time
 - ↳ Agrees with different dependence of diffusion coefficient for dynamic and steady state
 - ↳ Lower values at boundaries suggest interfacial resistance
- * With liquid/dry, rapid approach to steady-state profile
 - ↳ Profile is continuous from $\lambda = 22$ to 4
 - ↳ No liquid interfacial resistance
 - ↳ No evidence of sharp transition from liquid to vapor value

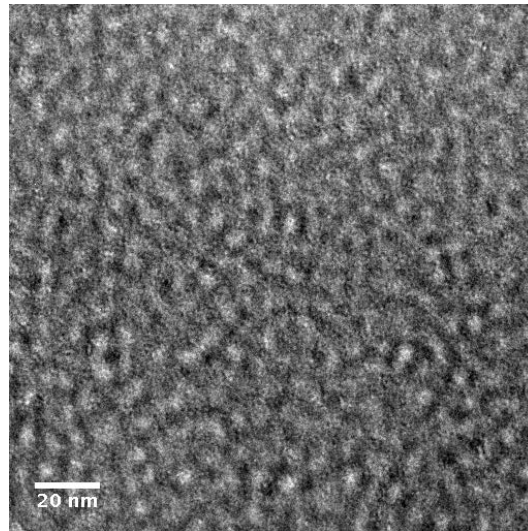
Membrane Morphology

- * Examine morphology using SAXS and also TEM

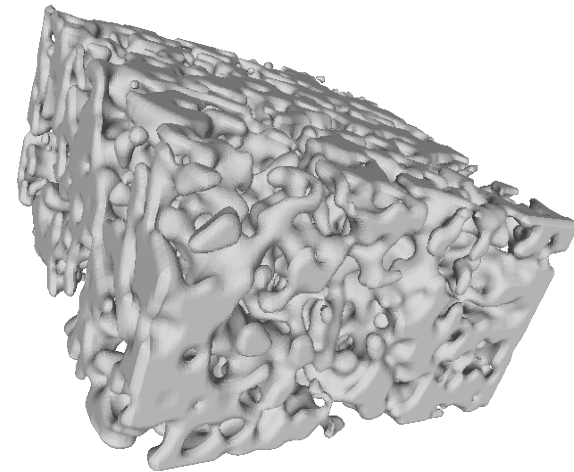
Dry (TEM)



Hydrated (cryoTEM)



Simulated from SAXS

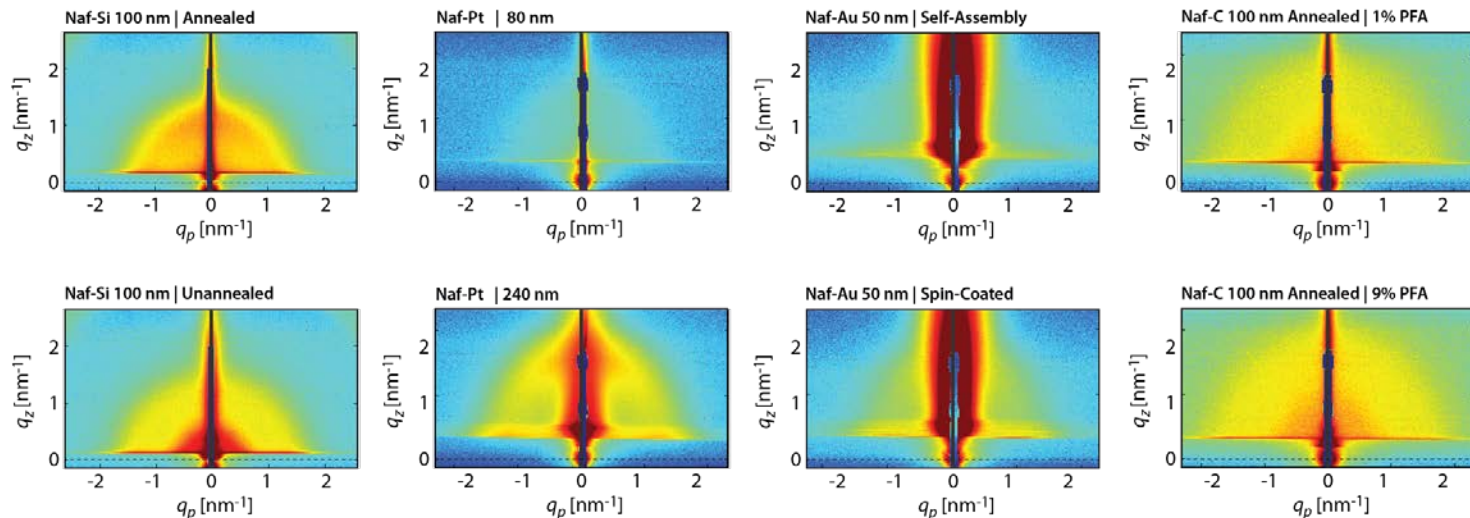


- ↪ Need to determine what the phases are using low-loss EELS
- ↪ Next would be to model transport through the morphology

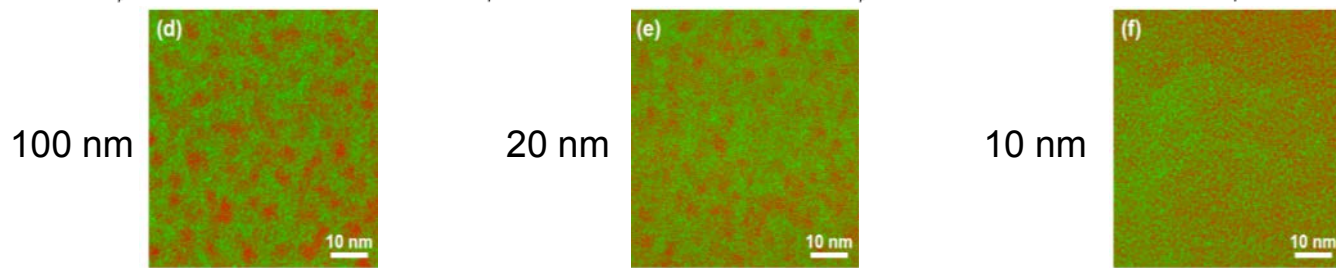
- * Thin-film Nafion[®] shows different morphology
 - ↳ Structure depends on interfacial interactions and film thickness
 - ↳ Correlating structure with mass uptake and swelling

Nafion-Si	Nafion-Pt	Nafion-Au	Nafion-C
Annealing induces crystallinity in films	Thinner films lose phase separation	Sample preparation affects nanostructure	Carbon preparation method has no effect

GISAXS



TEM



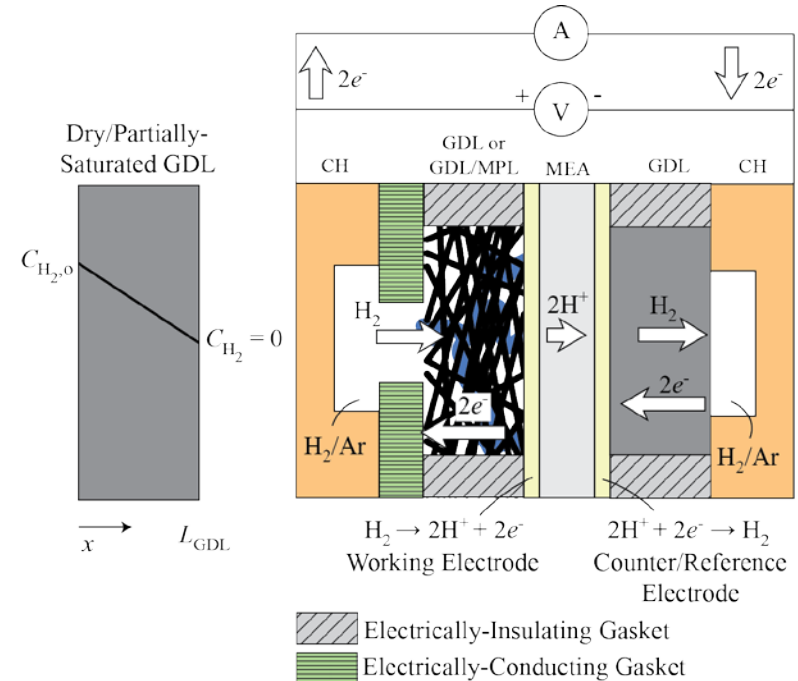
- * Effective diffusivity under saturated conditions is a key transport property that has not been adequately measure
- * Designed a hydrogen-pump setup to measure the hydrogen-limiting current for different saturations

$$\langle D_{\text{H}_2\text{-Ar}} \rangle = \frac{i_o L_{\text{GDL}}}{2F c_{\text{H}_2,0}}$$

- ↳ Exploiting the no spontaneous water-rejection properties of GDLs

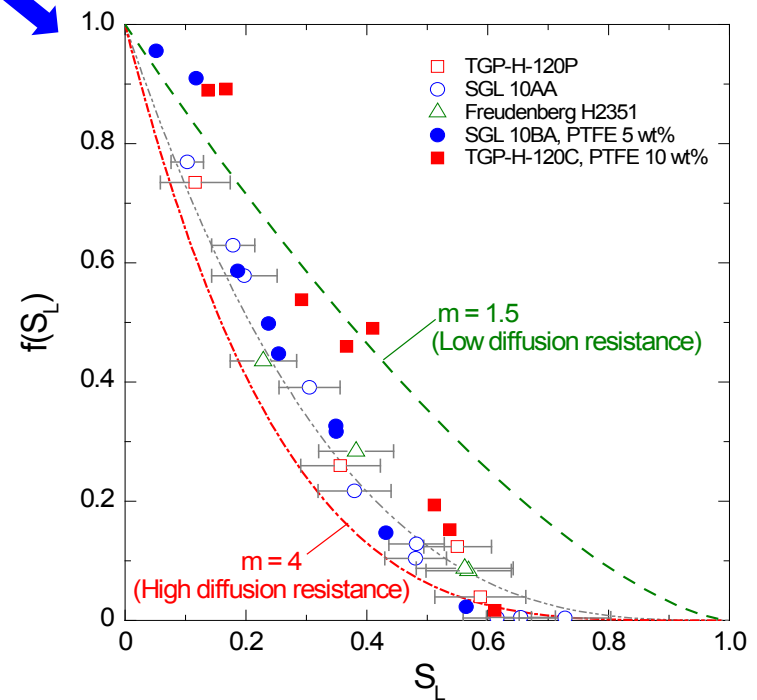
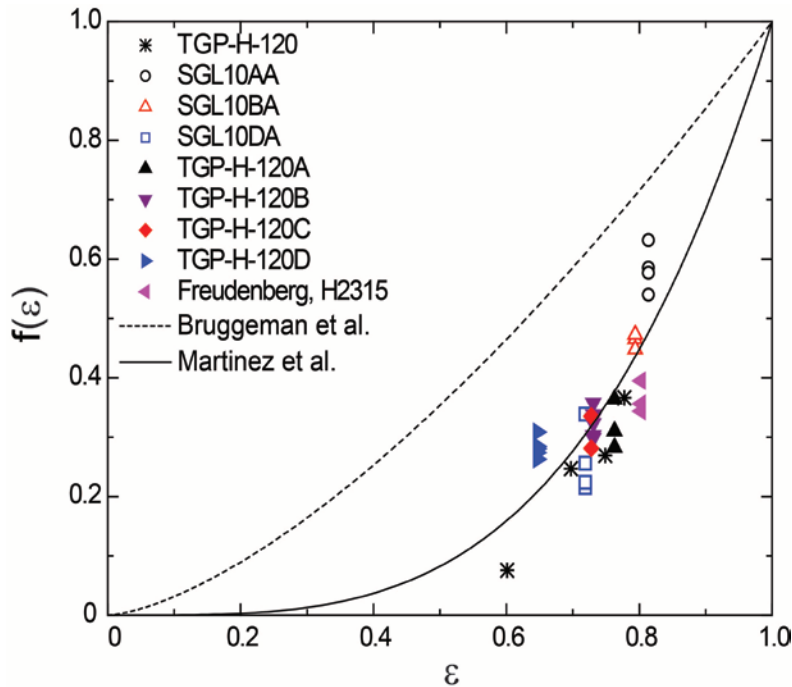
- * Effective diffusivity is composed of dry and wet contributions

$$\frac{\langle D \rangle}{D} = f(\varepsilon) f(S_L)$$



GDL Effective Diffusivity

$$\frac{\langle D \rangle}{D} = f(\varepsilon) f(S_L)$$



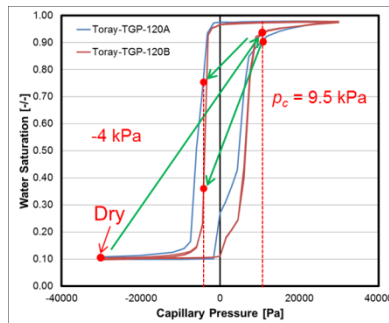
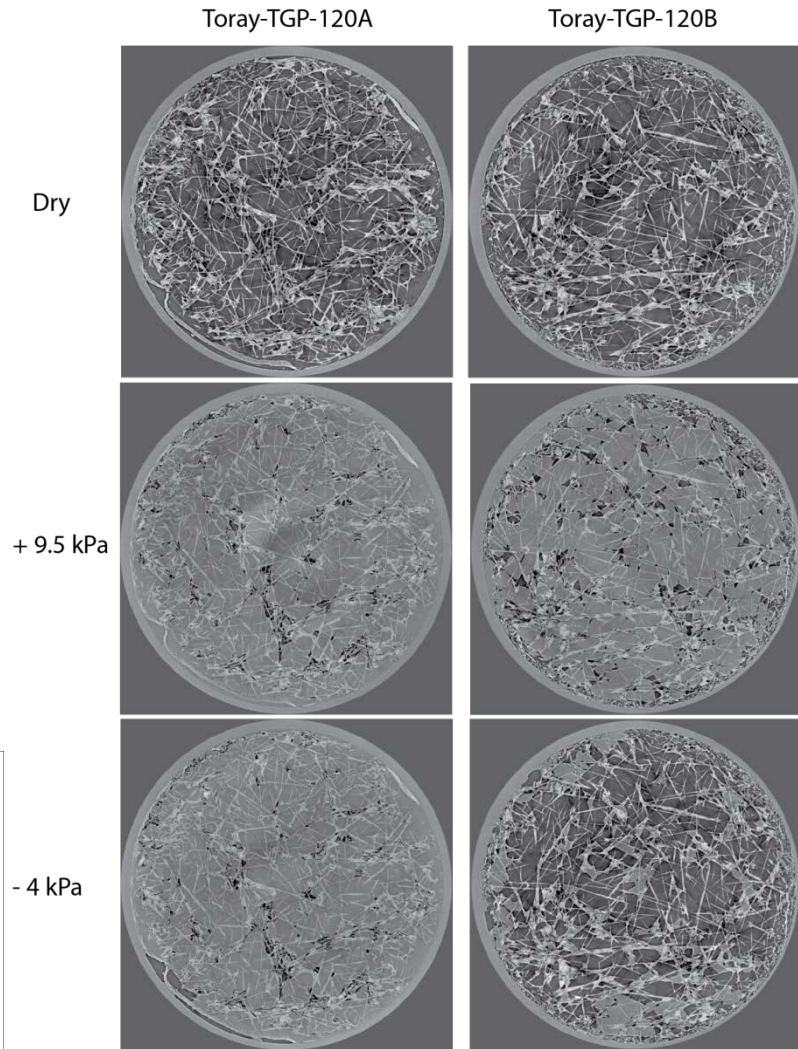
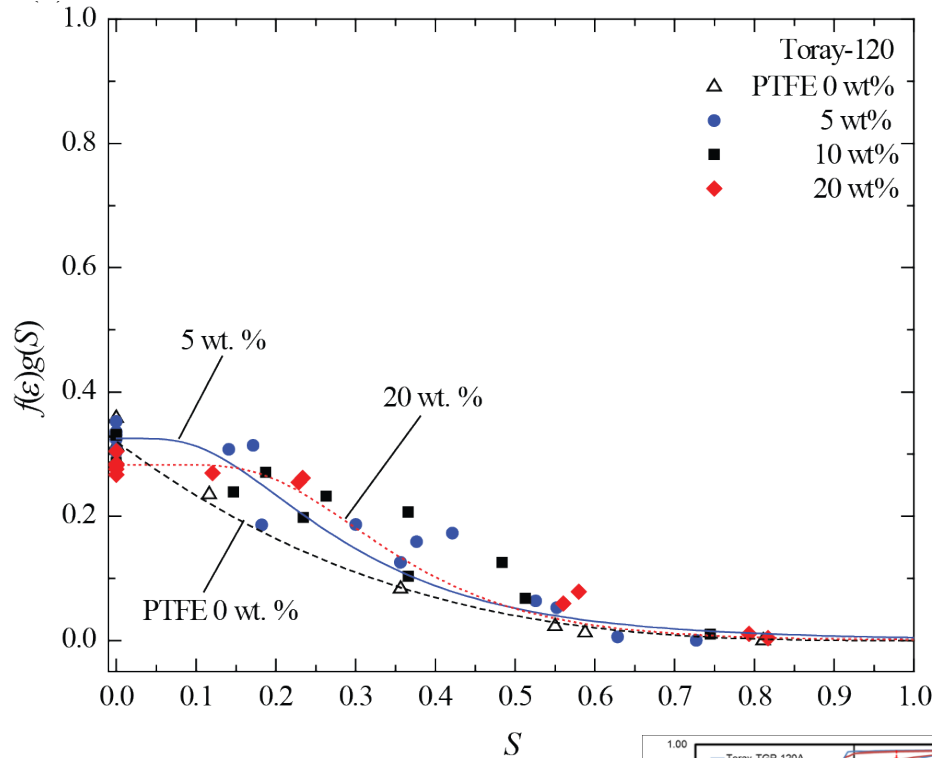
$$f(S_L) = (1 - S_L)^3$$

$$f(S_L) = \frac{1}{2} \left\{ 1 + \operatorname{erf} \left[-\frac{\ln(S_L) + a}{b} \right] \right\} \quad \text{with PTFE}$$

- * Much higher tortuosity than expected
- * Similar dependences for different papers
- ↳ There is an impact of PTFE

* PTFE coatings favorably change liquid distribution for diffusivity at $S_L < 0.6$

↳ More heterogeneous wetting

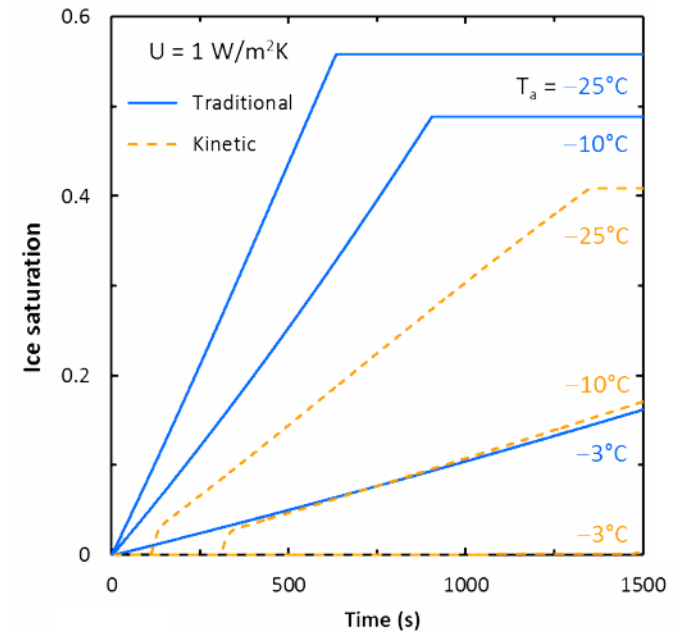
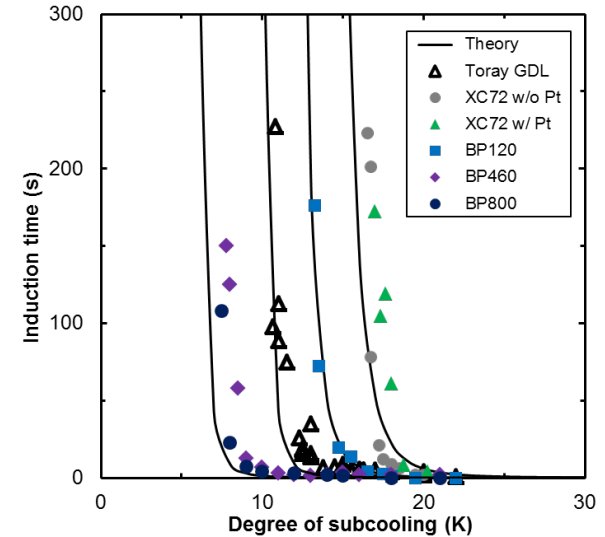


Freezing in Catalyst Layers

- * Use dynamic-scanning-calorimetry (DSC) to measure freezing time
 - ↪ Cast catalyst layer inside DSC pan
 - ↪ Vary catalyst-layer properties

- * Water takes longer to freeze in typical catalyst layers than in the gas-diffusion layer

- * Use developed rate expression in isothermal freeze model
 - ↪ Induction time results in much different performance compared to traditional thermodynamic-based rate expressions
 - ↪ Currently correlating to experimental data



* Cell Performance

- ↪ UTRC to run cool and cold starts including adiabatic and temperature transients
 - ↪ NSTF and low-loaded traditional CLs
 - ↪ Run hybrid WTP cells
- ↪ LANL to run NSTF cells including various tests
 - ↪ Segmented cell
 - ↪ Power transients
 - ↪ NIST high and higher resolution imaging
- ↪ 3M to run cells to determine water balance and impact of NSTF structure

* Component characterization

- ↪ Traditional CLs
 - ↪ Examine thin-film membrane morphology
- ↪ NSTF CLs
 - ↪ Proton migration on platinum
- ↪ GDLs
 - ↪ Liquid-water movement out of the GDLs by droplets
 - ↪ Measurement of effective diffusivities, thermal conductivities, and relative permeabilities
- ↪ MPLs: how do they work with liquid water?
- ↪ Membrane
 - ↪ Interfacial resistance and membrane morphology with different environments

* Modeling

- ↪ Use data from all partners and understand the anode GDL and water-out-the-anode scheme for NSTF
- ↪ Develop transient model and examine CL water capacity versus water removal fluxes as a function of CL thickness
- ↪ Optimize schemes and structures to increase low-temperature performance

* Examine failed MEAs and cyclical isothermal cold starts for durability concerns

* Understand and increase the operating window with thin-film catalyst layers

* Relevance/Objective:

- ↗ Help enable, optimize, and mitigate failure in state-of-the-art materials through fundamental understanding of operation at low and subzero temperatures

* Approach/Collaborations:

- ↗ Use synergistic combination of cell and component diagnostic studies with advanced mathematical modeling at various locations (national laboratories, industry, and academia)

* Technical Accomplishments:

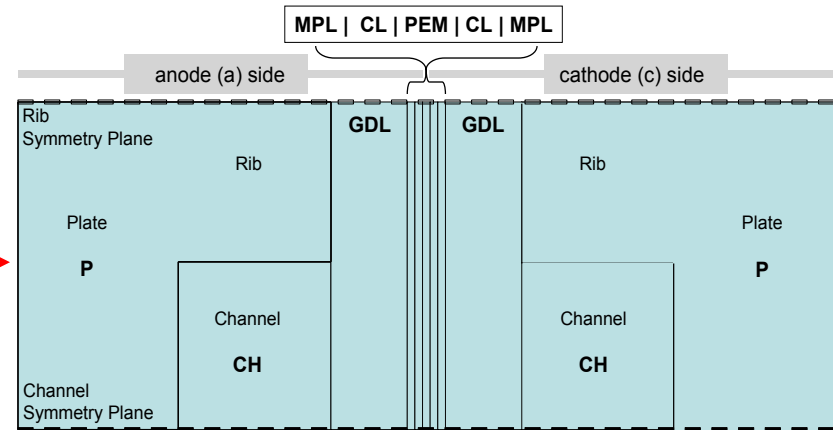
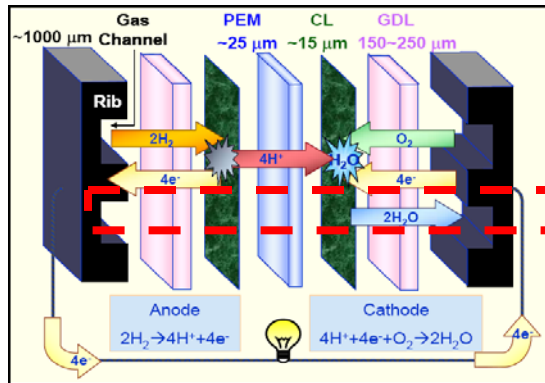
- ↗ Combined modeling and experiment to understand low-temperature performance of NSTF
 - ↗ Examining impact of different anode GDLs
 - ↗ Hybrid cell assemblies to determine limiting layers and phenomena
- ↗ Measured effective diffusivities as a function of saturation for GDLs
 - ↗ Shows roughly cubic and not Bruggeman power-law dependence on saturation and porosity
- ↗ Developed mechanical stress model for cold start and ice formation and membrane swelling
- ↗ Investigated membrane morphology and transport, especially as thin films
 - ↗ Thin films below 50 nm exhibit different and more resistive properties and is dependent on the interfaces
 - ↗ Measured water profiles across the membrane with good temporal and spatial resolutions

* Future Work:

- ↗ Understand liquid-water movement, interactions, and freeze in fuel-cell components
- ↗ Benchmark cell performance and durability with different assemblies

Technical Back-Up Slides

* Model Geometry



* Model physics

Thermodynamics

Standard cell potential
Equilibrium H_2O content
membrane, liquid, vapor, ice

Kinetics

Butler-Volmer for HOR, ORR
 H_2O phase change between
ionomer, vapor
liquid, vapor

Transport

Stefan-Maxwell diffusion
for gas-phase components
Darcy's law for liquid, gas phases
Ohm's law for e^- current
Modified Ohm's law for H^+ current
 H_2O transport by proton drag
 H_2O diffusion in membrane

Conserved quantities

Mass; Charge; Energy

Constitutive relations

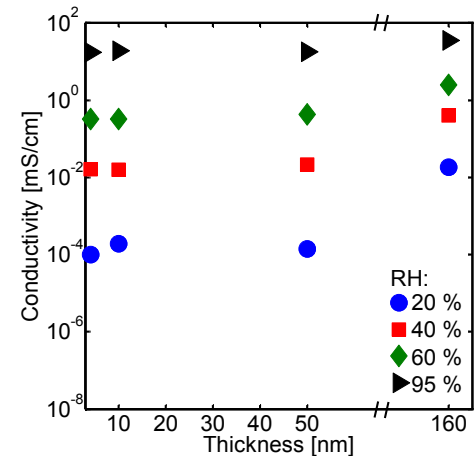
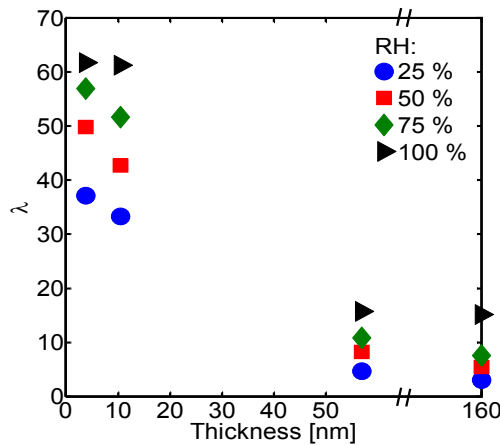
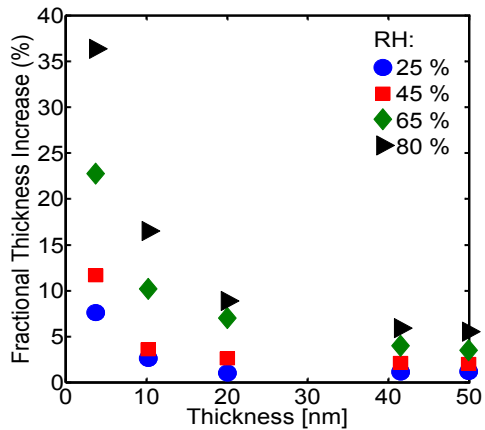
Faraday's law
Ideal-gas law

Properties

Function of T
and H_2O content

Equations (12): 7 2nd-order PDEs; 5 Algebraic equations

- ✧ From both ellipsometry and QCM, the thinner films have more swelling and higher water uptake
- ✧ Conductivity decreases due to loss of phase mixing and extreme hydration



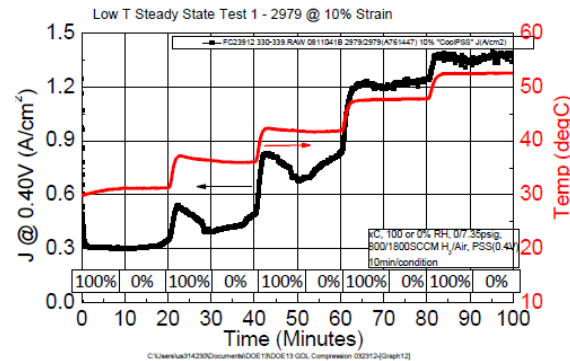
* Anode work consisted of 3 basic series (28 MEAs, 22 constructions)

1. Anode Backing Screening (9 types)
2. Anode Backing/GDL – Compression Effects (4 types @ 3 levels)
3. Periodic Baseline Checks (3 MEAs)

* Most evaluated over wide range of conditions.

- ↪ Peak Power (80C).
- ↪ Temp. Sensitivity Steady State (2 tests)
- ↪ Low Temp Cool Start Transient vs. T, RH

QTY	Anode GDL	Cathode GDL	Comp	Series
1	Freudenberg H1410	3M 2979	10%	Anode Backing Screening
2	Freudenberg H2315	3M 2979	10%	Anode Backing Screening
2	Freudenberg H2415	3M 2979	10%	Anode Backing Screening
1	Freudenberg X0090	3M 2979	10%	Anode Backing Screening
2	Freudenberg X0154	3M 2979	10%	Anode Backing Screening
2	Freudenberg X0155	3M 2979	10%	Anode Backing Screening
1	MRC MS050M	3M 2979	10%	Error
1	MRC 040US	3M 2979	10%	Anode Backing Screening
1	3M 2979	3M 2979	5%	Anode GDL - Compression
1	3M 2979	3M 2979	20%	Anode GDL - Compression
1	Freudenberg H2315+PTFE,MPL	3M 2979	5%	Anode GDL - Compression
1	Freudenberg H2315+PTFE,MPL	3M 2979	10%	Anode GDL - Compression
1	Freudenberg H2315+PTFE,MPL	3M 2979	20%	Anode GDL - Compression
1	MRC 040US	3M 2979	5%	Anode GDL - Compression
0	MRC 040US	3M 2979	10%	Anode GDL - Compression
1	MRC 040US	3M 2979	20%	Anode GDL - Compression
1	MRC 040US+PTFE,MPL	3M 2979	5%	Anode GDL - Compression
1	MRC 040US+PTFE,MPL	3M 2979	10%	Anode GDL - Compression
1	MRC 040US+PTFE,MPL	3M 2979	20%	Anode GDL - Compression
1	MRC MS050M+PTFE,MPL	3M 2979	5%	Anode GDL - Compression
1	MRC MS050M+PTFE,MPL	3M 2979	10%	Anode GDL - Compression
1	MRC MS050M+PTFE,MPL	3M 2979	20%	Anode GDL - Compression
3	3M 2979	3M 2979	10%	Baselines
28				
MEA: Roll Good CCM, one lot (Anode: 0.05mgPGM/cm2 PtCoMn/NSTF; Cathode: 0.15mgPGM/cm2 PtCoMn/NSTF; PEM: 3M 825EW 24u). Single cell and test station.				



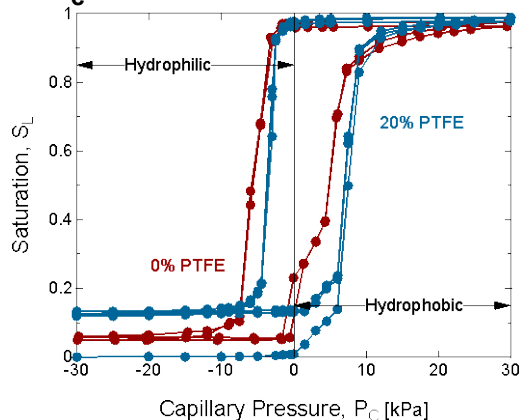
* Kinetic parameters

- ↗ 3M and UTRC (NSTF MEA); Los Alamos (Pt/C MEA)
- ↗ Literature (R.K. Ahluwalia et al., J. Power Sources, 215, 2012)

* Transport properties

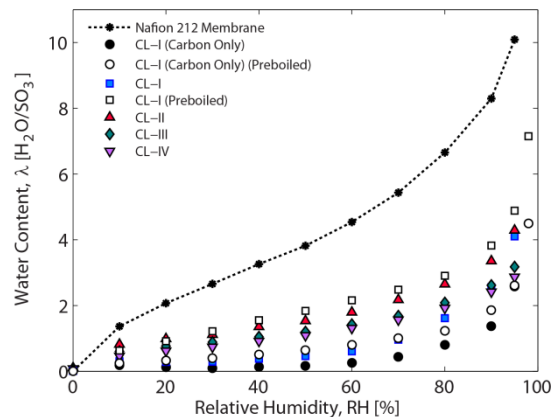
- ↗ Measured at LBNL (P_c – saturation relation, ionomer water uptake, effective gas diffusivity, effective thermal conductivity, etc.)
- ↗ Also taken from literature

P_c – Saturation Relation



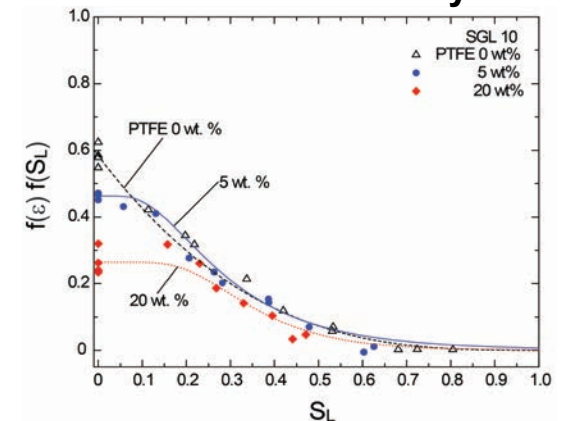
P.K. Das, A. Gripping, A. Kwong, and A.Z. Weber, *JES*, 159, B489-B496, 2012.

Ionomer Water Uptake



A. Kusoglu, A. Kwong, K.T. Clark, H.P. Gunterman, and A.Z. Weber, *JES*, 158, F530-F535, 2012.

Effective Diffusivity



G.S. Hwang and A.Z. Weber, *JES*, 159, F683-F692, 2012.

✦ Similar water contents at 80C

➡ Need to do tests at 40C

3M cells: NSTF MEA, cathode GDL fixed, **vary anode GDL.**

2.5 cm² cell, 100/200 sccm H₂/Air (fixed flows), **10.5 psig backpressure, 80 C (or 40 C)**, 100% RH

Co-flow, inlets high

Gore MEA: 0.2/0.4 mg Pt/cm² loading, Pt/C, 710 Membrane (18 microns thick).

VARY cathode GDL (same substrate, vary MPL only), anode GDL fixed.

The GDLs are from SGL Carbon.

2.5 cm² cell, 100/200 sccm H₂/Air (fixed flows), **zero backpressure, 80 C only**, 100% RH

Co-flow, inlets high

