

### POWER GENERATION FROM AN INTEGRATED BIOMASS REFORMER AND SOLID OXIDE FUEL CELL

**SBIR Phase III Xlerator Program** 

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### INNOVATEK

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**Project ID: FC096** 

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## **Overview**

Timeline

Start: 10-01-2010 Finish: 03-31-2014

66% Complete

DOE Barriers: Cost, Durability & Performance DOE Targets: H2 production from diverse domestic sources; distributed power demo 2Q 2018

YearCost/kWEfficiencyLifetimeTechnology2015\$170042.5%40,000h5 kW Dist Gen Sys2020\$1500>45%60,000h5 kW Dist Gen Sys

#### Budget

Total: \$2.3M Received FY12: \$650K Expected FY 13: \$748K Partners Topsoe Fuel Cell

Fuel Cell Energy/Versa Power Impact Washington



### **Relevance:** Public Benefits; H<sub>2</sub> from Diverse Sources

Addressing DOE Barriers and Targets: Environmental Quality & Energy Security

The full benefits from fuel cells are possible only if the feedstock for hydrogen production is a renewable, domestically produced commodity that does not compete in the food chain, and does not increase the price of energy

Our technology will address these issues by:

- Helping shift the primary energy source for H<sub>2</sub> from fossil fuels to renewable non-food biomass, using natural gas as the bridge.
- Using less fuel through high system efficiency by effective thermal integration and off-gas recycling.
- Providing an alternative method for distributed power generation near the source of the feedstock, enhancing grid stability at competitive cost.





## **Relevance: Project Objectives**

Year	Objective	DOE Barriers Addressed
2011 Complete	Establish design to meet technical and operational needs for distributed energy production from renewable fuels	SOFC power using renewable non-food biomass fuel; codes & standards
2011/ 2012 Complete	Design, optimize, and integrate proprietary system components and balance-of-plant in a highly efficient design.	Demonstration; system efficiency; design for low cost manufacturing
2013/ 2014 Not started	Demonstrate the technical and commercial potential of the technology for energy production, emissions reduction, and process economics	<ul> <li>40,000 h lifetime</li> <li>99% availability</li> <li>&gt;40% efficiency</li> <li>\$1700/kW equipment cost</li> </ul>



# **Approach: Project Goal**

Develop and demonstrate a fuel cell distributed energy system that operates with 2<sup>nd</sup> generation biofuel.

- System based on InnovaTek's steam reforming process and SOFC
- Non-food biofuels include pyrolysis oil and bio-kerosene processed locally
- System to be demonstrated in Richland's renewable energy park and tied to grid



## **Approach: Milestones & Go/No Go**

Date	Milestone or Go/No Go	Status
Jan 2013	M4: Achieve 40% system operating efficiency with revised/optimized system design	41%
Feb 2013	M5: System performance proves superior energy efficiency & emissions reductions compared to conventional technology	Complete
March 2013	Go/No Go: Analysis of process economics supports commercial feasibility (Cost of power is competitive)	Complete
Oct 2013	Complete fabrication of Gen3 prototype for field demonstration	Not started
March 2014	Complete 6 months of field demonstration	Not started



### **Approach:** Optimization & Economic Analysis

- 1. Use simulation and modeling studies to optimize system design for performance and cost reduction.
  - Optimize process configuration using MathCAD and FEMLAB
  - Conduct FMEA to assess necessary redesign, determine maintenance requirements and costs, lifetime
  - Conduct DFMA analyses to identify design changes to improve manufacturability and reduce production & operation costs
  - Use HOMER model to assess cost of power
- 2. Translate dimensions, geometries, and flow patterns defined from optimization modeling to 3-D CAD images
- 3. Complete Bill of Materials & SolidWorks drawing libraries for all original hardware designs and BOP
  - Use this information to model capital equipment costs and parasitic power requirements



### **Approach:** Scale-up & Optimize Core Technology

#### InnovaGen® Fuel Processor for 4 kW power



#### 2012 2013 Size reduced, output increased

- Creates hydrogen from a range of liquid and gaseous fuels with high energy density
- Proprietary catalyst & hardware
- Water neutral steam reformer
- Compact and efficient

### Solid Oxide Fuel Cell



Transitioning to scaled-up SOFC





## **Approach: Economic Analysis Models**



## Accomplishments: Developed Highly Efficient Thermally Integrated System Design

#### **Process Flow Diagram**

Subdivided into 21 process streams

#### Mass and Energy Balance

- Completed for each process stream
- Determines input, output, efficiency

**Optimized Layout, Piping & Instrumentation** 

Solid Model of Integrated System Milestone 3

**Component Design and Analysis** 

- Process simulations
- Design trade-off analyses



5kW fuel cell system that operates on liquid bio-fuel



## Accomplishments: Solid Model 4 kW



## Accomplishments: 41% System Efficiency

Gross DC Power, kW	4.2
Current density, mA/cm <sup>2</sup>	390
Cell active area, cm <sup>2</sup>	550
Stack current, A	214.5
Cell voltage, volt	0.82
Number of cells	24
gross DC power, watt	4221
stack electrical efficiency	65.60%
parasitic power, watts	300
Net AC electrical efficiency	40.8%

# Improved from last year (37.5%) due to:

- Better stack efficiency
- Lower parasitic power due to lower stack pressure drop
- Less waste heat loss through improved thermal integration and heat transfer
- Higher methane content in reformate



## **Accomplishments: Catalyst Durability**



## **Accomplishments:** Analysis of Energy Cost

### Adapted EERE's HOMER Model for fuel cell system

- Examined several scenarios for delivering 5 kW electrical AC power for 10 years using InnovaGen FC power unit
- Compared bio-kerosene & natural gas
- Capitol and operating costs based on Bill of Materials and Testing
- Used projected production and fuel pricing data from DOE sources

#### **Significant Findings:**

- 1. Our fuel cell generator operating on natural gas could produce electricity at prices at or below current grid prices (<\$0.09/kWh) when volume production brings capital costs down.
- 2. The price for liquid bio-fuel, estimated at \$3.50 per gallon, is the dominant factor affecting cost of electricity when operating on bio-fuel.



## **Progress:** Economic Analysis for 5 kW FC

Cost of energy using InnovaTek's 5 kW fuel cell system with n.gas at current & forecasted spot price

Cost of energy using InnovaTek's 5 kW fuel cell system using bio-kerosene with Honeywell's projected price



DOE Program Review 5-14-13

### **Progress: 32% Cost Reduction Fuel Processor**



Old Design

New Design

System Cost Material Cost T	Total Cost	Parts	Approx volume (L)
ginal Design \$10,201 \$4951	\$15,152	159	13.87
/ised Design \$6,374 \$3997	\$10,371	66	6.88
/ised Design \$6,374 \$3997	\$10,371		66



### **Progress: 79% Cost Reduction Fluid Handling**

Air Handling Subassembly

Feed Handling Subassembly

Fuel Handling Subassembly







	Docian	Labor	Material	Total	Dorto
	Design	Cost	Cost	Cost	Fails
	Original	\$210	\$2,630	\$2,840	136
Air Delivery	Revised	\$22.50	\$762	\$785	16
Fuel & Fuel	Original	\$390	\$11,573	\$11,963	118
Delivery	Revised	\$60	\$2,230	\$2,290	25



# **Collaborations**

#### **Subcontractors**

- Fuel Cell Energy Versa Power SOFC (within DOE H<sub>2</sub> Program)
- Boothroyd Dewhurst Design for Manufacturing & Assembly training
- Manufacturing partners shift from welding to brazing

#### **Strategic Partners**

- Impact Washington manufacturing design support
- PNNL provided upgraded bio-oil made from non-food biomass (within DOE H<sub>2</sub> Program)
- Honeywell UOP provides bio-kerosene
- City of Richland Electric Utility providing site for field demo
- Mid-Columbia Energy Initiative

Education

Supported 3 student interns from WSU, U of WA, Delta HS in mechanical engineering and chemistry



## **Proposed Future Work**

**Objective 3. Prove the technical and commercial potential of the technology** 

**FY13** 

- Optimize performance by testing & adjusting operating parameters
- Further improve system efficiency & durability; reduce cost
  - Enhance FC-FP integration; evaluate BOP alternatives
- FY14
- Fabricate and assemble fully integrated grid-ready 5 kW system
- Verify performance and durability with 6 month field demo at City Utility
- Analyze process economics



# **Summary**

**Relevance:** Shift primary energy from fossil to renewable fuels

- Address codes & standards for fuel cells
- Increase system efficiency, lifetime and durability; decrease cost
- Distributed power production near source of feedstock to enhance grid stability
- Approach: Develop reformer that generates hydrogen from non-food biofuels
  - Develop highly efficient processing design of integrated SOFC and fuel processor
  - Prove technology in long-term field demonstration with utility partner

Accomplishments: Achieved 41% system efficiency

- Used simulation and modeling to optimize component & system designs
- Prepared solid model of system & complete Bill of Materials with P&ID
- Developed optimized catalyst for biofuel reforming; demonstrated >900hrs durability
- Determined capital and operating expenses; modeled process economics

**Collaborations:** Supported 3 students; Subcontractors for fuel cell & manufacturers;

- Partnerships with PNNL, WSU, Boeing, City of Richland, Regional Energy Initiative **Future:** Complete laboratory tests with 4 kW prototype
  - Fabricate prototypes for grid interconnect
  - Conduct field demonstration and long term operation
  - Complete further analysis of process economics









### **Technical:** System Efficiency Algorithms

system efficiency (electrical efficiency)

$$\begin{split} & P_{\text{parasitic}} \coloneqq 300W & \text{D}\mathcal{C}_{\text{gross}}(\mathbf{I}_d) = 4.221 \times 10^3 W \\ & \text{regulated DC power} & \eta_{\text{dc}\_dc} \coloneqq 95\% \\ & \mathcal{D}\mathcal{C}_{\text{reg}}(\mathbf{I}_d) \coloneqq \mathcal{D}\mathcal{C}_{\text{gross}}(\mathbf{I}_d) \cdot \eta_{\text{dc}\_dc} & \eta_{\text{dc}\_ac} \coloneqq 92\% \\ & \text{net DC power} & \mathcal{OCV}_{\text{HHV}} \coloneqq 1.48 \text{volt} \\ & \mathcal{D}\mathcal{C}_{\text{net}}(\mathbf{I}_d) \coloneqq \mathcal{D}\mathcal{C}_{\text{reg}}(\mathbf{I}_d) - \mathcal{P}_{\text{parasitic}} & \mathcal{OCV}_{\text{LHV}} \coloneqq 1.25 \text{volt} \\ & \text{net AC power} & \eta_{\text{volt}} \coloneqq \frac{\text{Volt800}_{\text{cell}}}{\mathcal{OCV}_{\text{LHV}}} = 0.656 \\ & \mathcal{A}\mathcal{C}_{\text{net}}(\mathbf{I}_d) \coloneqq \mathcal{D}\mathcal{C}_{\text{net}}(\mathbf{I}_d) \cdot \eta_{\text{dc}\_ac} & \eta_{\text{volt}} \coloneqq \frac{\text{Volt800}_{\text{cell}}}{\mathcal{OCV}_{\text{LHV}}} = 0.656 \\ & \eta_{\text{ele}} \coloneqq \frac{\mathcal{A}\mathcal{C}_{\text{net}}(\mathbf{I}_d)}{\mathcal{L}\text{HV}_{\text{spk}} \cdot (n_{\text{feed}} + n2) \cdot MW_{\text{spk}}} = 40.793 \cdot \% \\ & \eta_{\text{ele}} = 0.408 \\ \\ & \eta_{\text{fps}} \coloneqq \frac{\text{LHV}_{h2} \cdot N_{\text{anode}\_in_3} + \text{LHV}_{ch4} \cdot N_{\text{anode}\_in_0} + \text{LHV}_{co} \cdot N_{\text{anode}\_in_1}}{\mathcal{L}\text{HV}_{\text{spk}} \cdot (n_{\text{feed}} + n2) \cdot MW_{\text{spk}}} = 112.977 \cdot \% \end{split}$$

