

# Electrolyzer Component Development for the HyS Thermochemical Cycle

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2013 DOE Hydrogen and  
Fuel Cell Program Review  
**Project PD096**

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# Overview

## Timeline

**Start Date: June, 2004**

**End Date: October, 2013\***

(work suspended 2010-2012)

**50% Complete**

## Budget

- **Total Project Funding**
  - DOE Share = \$5.2 M
  - Industry Cost Share = \$140 K
- **Funding received in FY12: \$0**
- **Funding for FY13: \$300 K**  
(pending)

## Barriers

**T. Coupling Concentrated Solar Energy and Thermochemical Cycles**

**W. Materials and Catalyst Development**

**X. Chemical Reactor Development and Capital Costs**

## Partners

- **Project Lead: SRNL**
- **Univ. of South Carolina and Air Products and Chemicals**
- **Numerous industry and university partners from previous DOE-NE work**

# Project Objectives - Relevance

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**Goal:** Process development of solar-driven high-temperature thermochemical water splitting cycle to enable integrated laboratory-scale studies followed by demonstrations utilizing solar-based heat

**Relevance:**

- Overcome barriers leading to cost-effective centralized hydrogen production from renewable sources
- Coupling of solar energy and thermochemical cycles
- Resolve major technical challenges for Hybrid Sulfur thermochemical cycle to permit reliable, cost-effective process operation at high energy efficiency

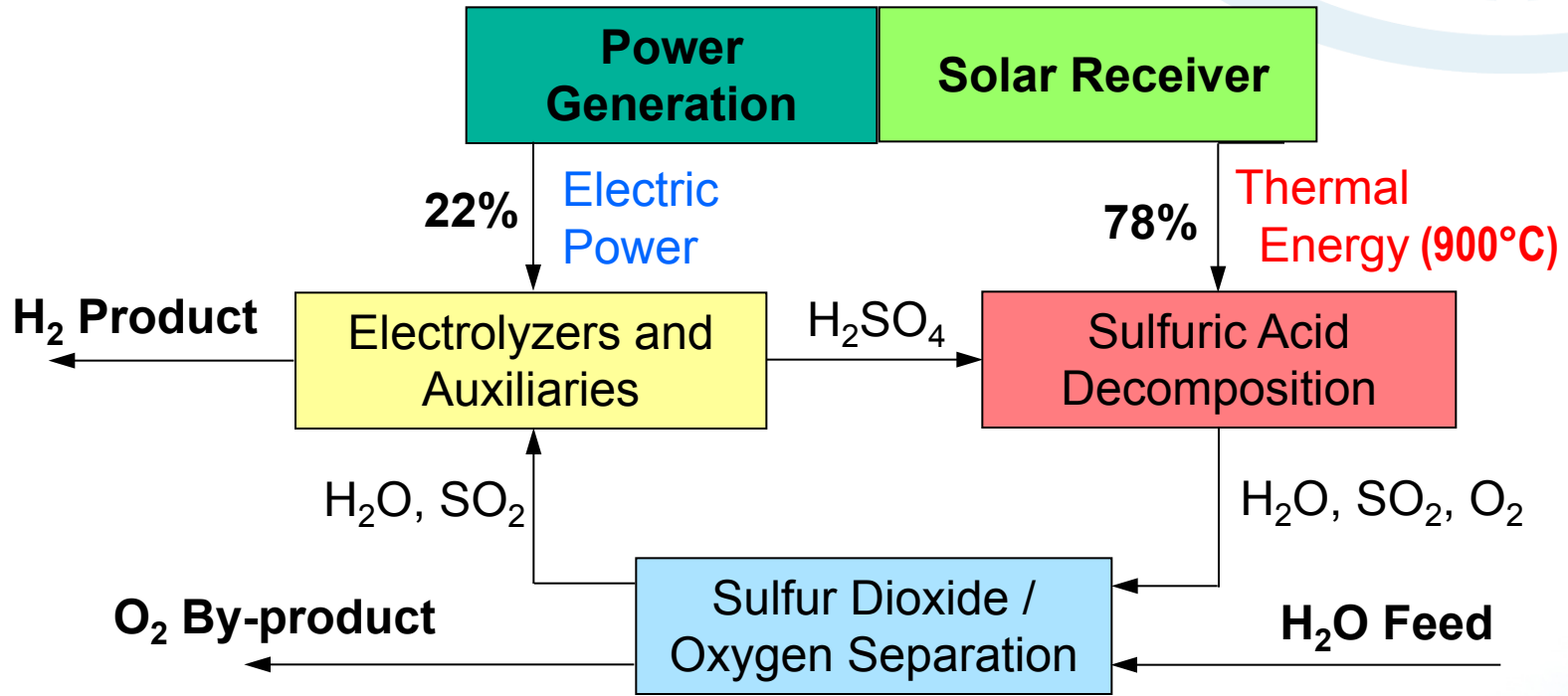
# FY13 Objectives - Relevance

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## Overcoming Barriers:

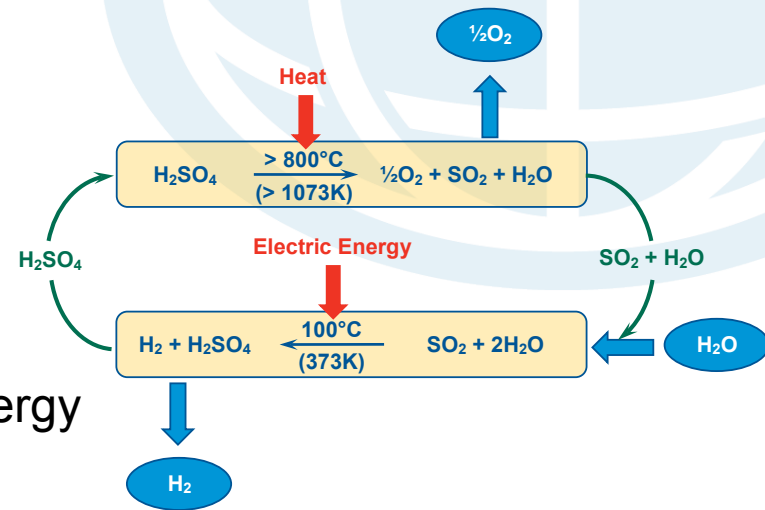
- Key Step in HyS Cycle is electrochemical water-splitting based on use of an SO<sub>2</sub> depolarized electrolyzer (SDE)
- FY13 Objectives are focused on addressing major challenges of reaction kinetics, high unit output (current density), sulfur formation, and operating lifetime of PEM-type SDE
  - Demonstrate liquid-fed SDE operation at increased T&P at button-cell scale
  - Characterize various advanced PEM membranes at >120°C
  - Develop electrocatalysts that lower cell voltage and increase efficiency
- Improved SDE will result in lower capital costs, improved overall solar-hydrogen plant performance and lower hydrogen costs

# HyS Process Simplified Flowsheet

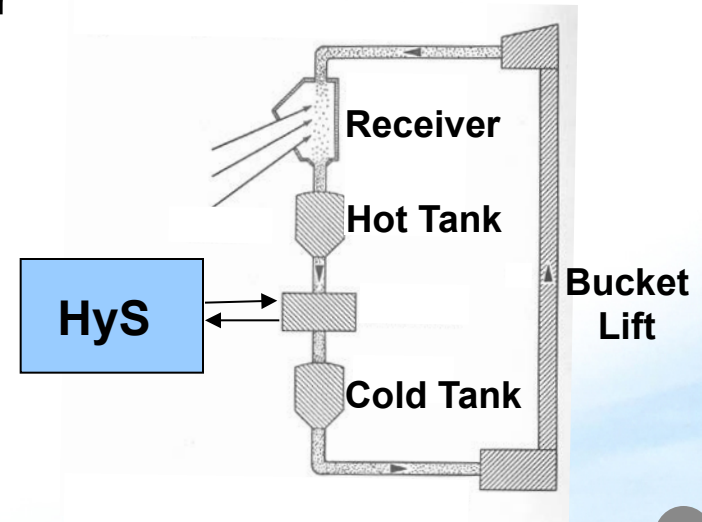


# Hybrid Sulfur Thermochemical Cycle

- Simple two-step, all-fluid cycle
- Sulfur chemistry (S-H-O species)
- Extensive development
  - R&D started in 1970's
  - Supported by DOE Office of Nuclear Energy
- Moderate peak temperature (900°C)
- Compatible with Solar Central Receiver
- Detailed flowsheets and cost analysis completed with positive results
- Key steps demonstrated at 100 lph; need integrated lab-scale process demonstration and development of solar receiver and solar interface



Receiver/Storage Concept





# Hybrid Sulfur Process (HyS)

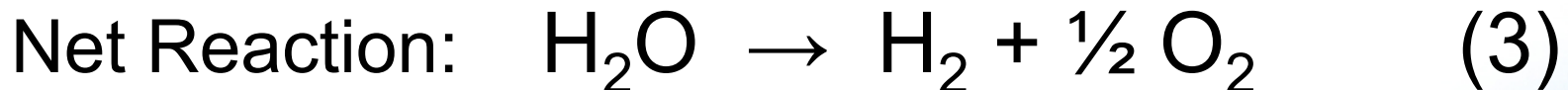
*The only practical **two-step, all-fluids** thermochemical cycle – based on sulfur oxidation and reduction; **only S-H-O compounds***



(thermochemical; 800-900 °C)



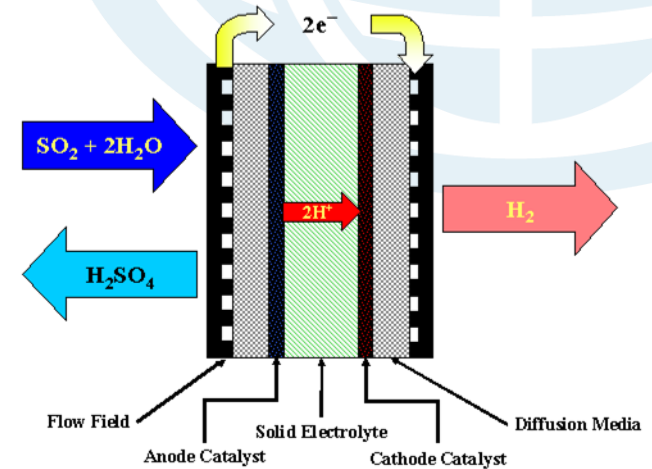
(electrochemical; 80-120 °C)



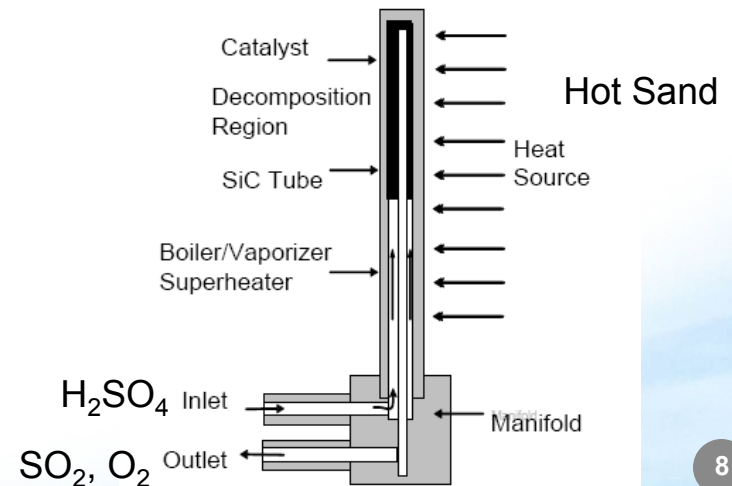
# Research Status

- **Electrolyzer based on PEM technology**
  - Focus on advanced membranes (>20 types tested)
  - Key issue is crossover of  $\text{SO}_2$  creating sulfur
  - Goal: 600 mV at 120-140  $\text{A cm}^{-2}$  and 2 MPa
  - Status: 760 mV at 80  $\text{A cm}^{-2}$  & 700 kPa w/o S formation
  - Largest unit: 3-cell, 160- $\text{cm}^2$ , 100 lph  $\text{H}_2$
- **Acid decomposer integrated skid completed**
  - Heated section constructed of SiC with recuperation
  - Metal/SiC joints at lower temperature
  - Integrated skid with electric heating tested at 100 lph
  - Key solar feature is solid particle heating
  - Future design could use direct solar heating
- **Falling particle receiver tested at SNL**
  - Permits simple high temp heat storage
  - Operate sand/HX continuously
  - Bucket conveyor to return hot sand up tower

## $\text{SO}_2$ -Depolarized Electrolyzer



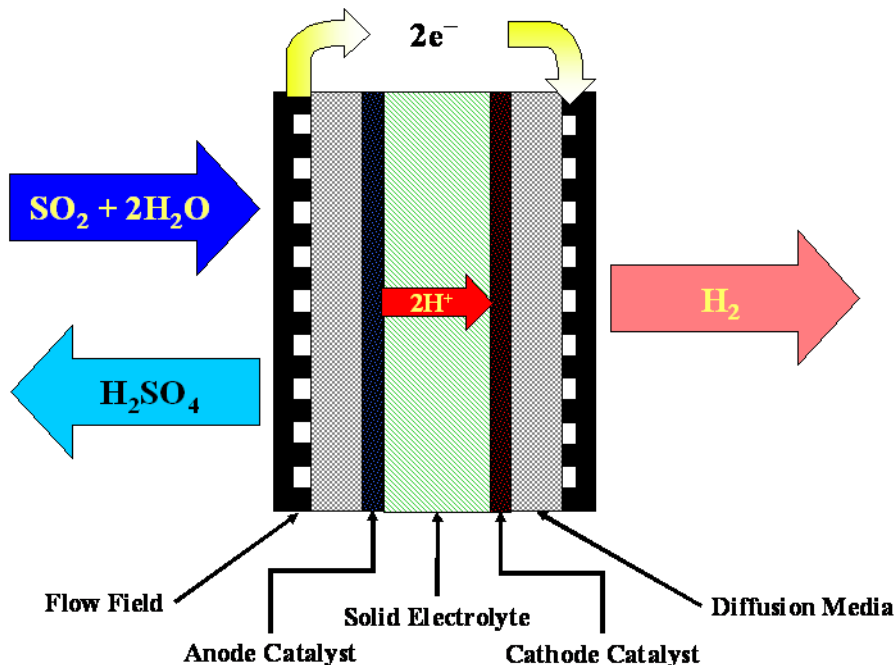
## Bayonet Acid Decomposer





# Step 1: SO<sub>2</sub>-Depolarized Electrolyzer

Proton Exchange Membrane (PEM) Electrochemical Cell



SO<sub>2</sub> oxidized at anode to form H<sub>2</sub>SO<sub>4</sub> and hydrogen ions

Reversible cell potential reduced by 87% vs water electrolysis (0.16 V vs. 1.23 V)

Practical cell voltage of 0.6 V versus 1.6-2.0 V for water electrolysis

Requires efficient thermal step to regenerate SO<sub>2</sub> and close the cycle

PEM cell concept permits compact design, reduced footprint, and lower cost versus earlier designs

Leverages extensive R&D and advances being done for PEM fuel cells by auto companies and others

**PROGRAM GOAL: 600 mV at 500 mA/cm<sup>2</sup>**

# Technical Approach – SO<sub>2</sub>-Depolarized Electrolyzer

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**Address key challenges for efficient, long-life operation (high current density, lower voltage, no sulfur formation):**

- Complete fabrication and assembly of Pressurized Button Cell Test Facility (PBCTF)
- Conduct rapid screening of membranes and electrocatalysts at elevated temperature and pressure

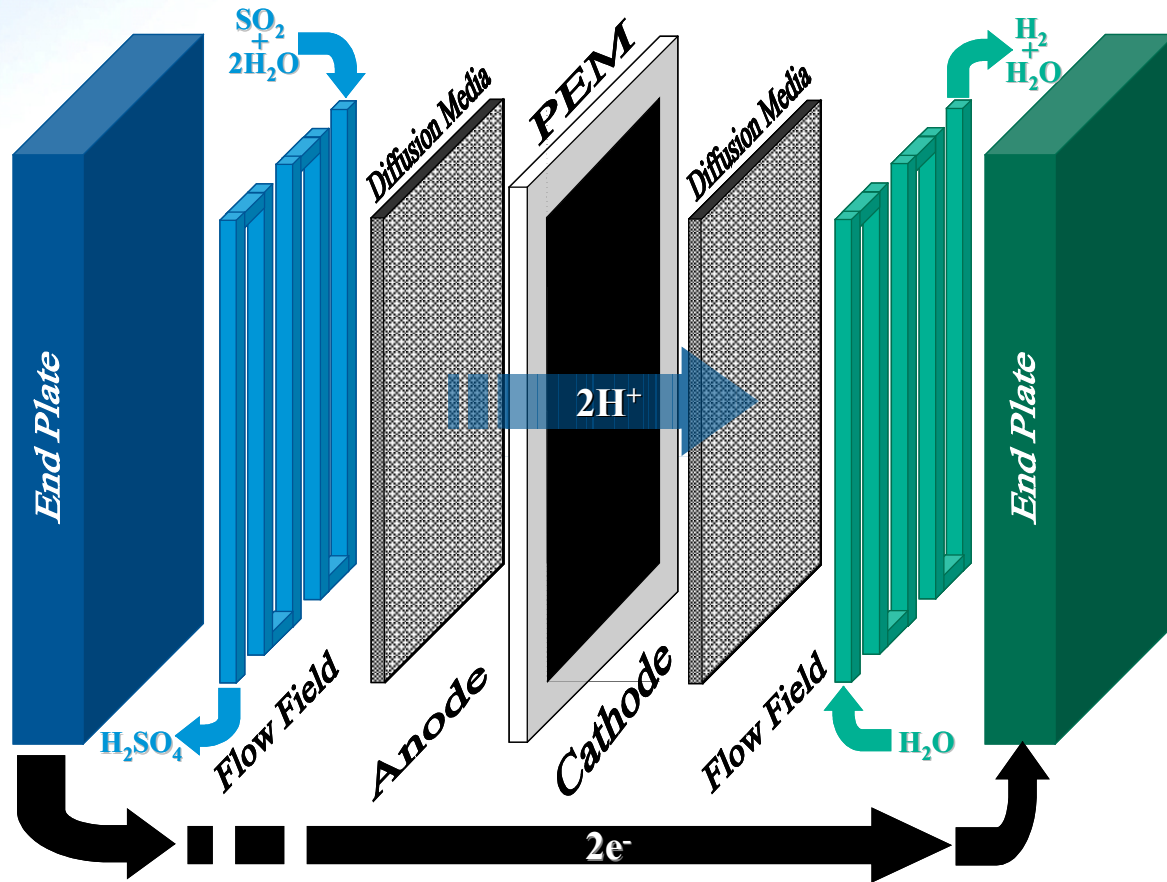
**Prepare and characterize improved electrocatalysts**

**Identify advanced membrane candidates that improve performance and prevent sulfur crossover**

- Work with industry and universities partners to leverage membrane developments for fuel cells and other applications

**Scale-up and test in larger Single-cell Test Facility at SRNL**

# PEM Electrolyzer Design Concept



Cathode      Membrane      Anode



← 100-150 μm →

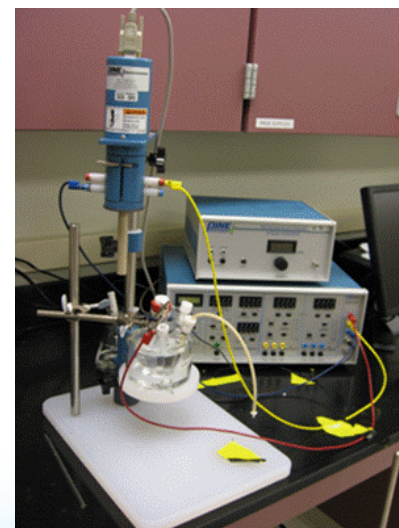
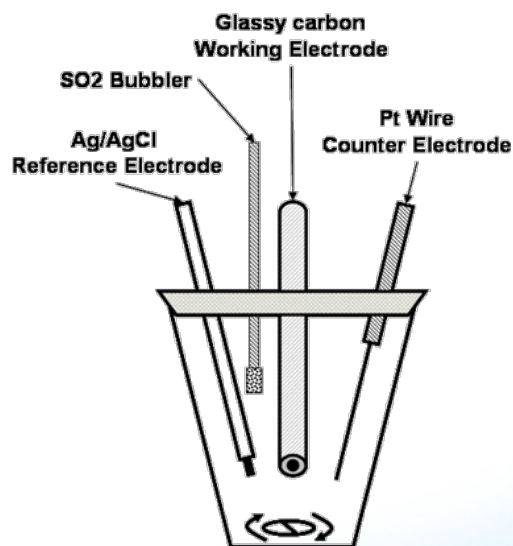
MEA Cross-section

## Prior Technical Accomplishments - Electrocatalyst

- Pt/C is more stable and has greater activity than Pd/C (converse to some previous results)
- Pt-transition metal alloy catalysts (Pt/Co, Pt/Co/Ni, Pt/Co/Cr) show improvement over Pt/C
- Activation of the catalyst surface is needed for optimum oxidation kinetics
- Higher acid concentrations decrease catalyst activity
- Higher temperatures increase catalyst activity
- **BASELINE DESIGN:** Pt/C with higher operating temperature

### Materials tested:

- Pt, Pd, Pt/transition metal alloys on carbon black
- Cyclic Voltammetry (50mV/s)
- Linear Sweep Voltammetry (5 mV/s)





# Prior Technical Accomplishments - Membranes

Membrane candidates included unmodified and modified PFSA (e.g. Nafion®) and hydrocarbon and fluorocarbon base membranes

Perfluorinated sulfonic acid (PFSA) – e.g. Nafion®

Polybenzimidazole (PBI)

Sulfonated Diels-Alder polyphenylene (SDAPP)

Stretched recast PFSA

Nafion®/fluorinated ethylene propylene (FEP) blends

Treated PFSA

Perfluorocyclobutane-biphenyl vinyl ether (BPVE)

Perfluorocyclobutane-biphenyl vinyl ether-hexafluoroisopropylidene (BPVE-6F)

DuPont

BASF (Germany);  
Univ. So. Car.

Sandia National  
Laboratories

CWRU; Vanderbilt

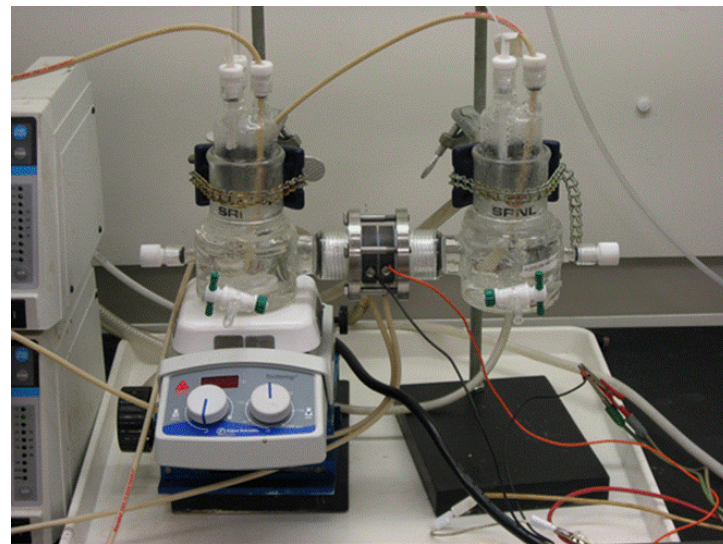
CWRU; Vanderbilt

Giner Electrochem.

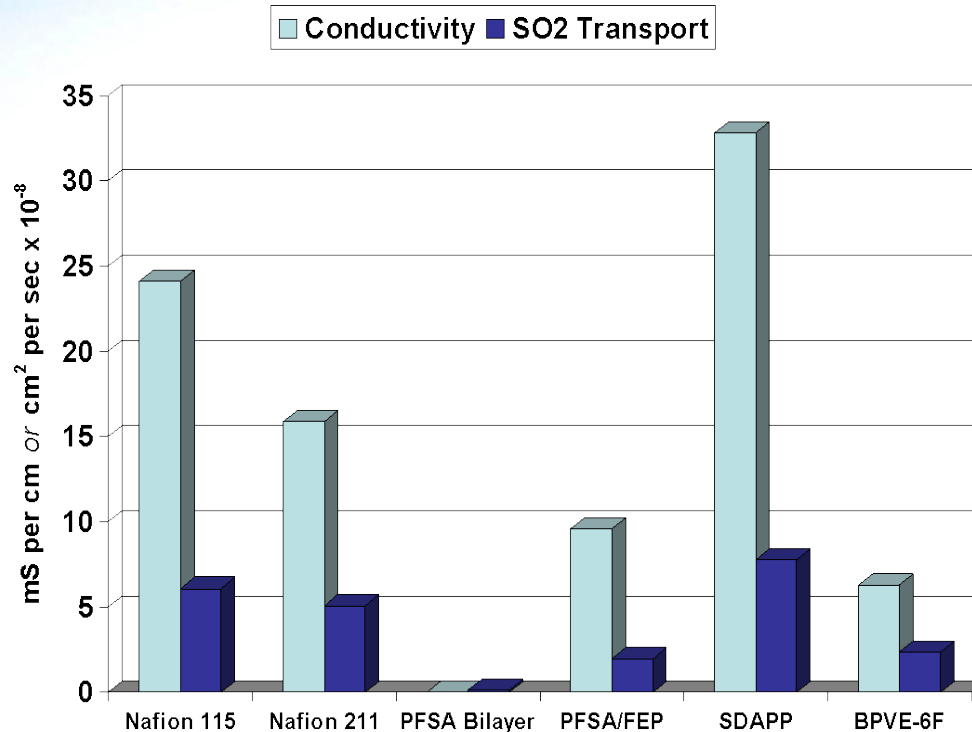
Clemson University

Clemson University

## SO<sub>2</sub> Transport Characterization Cell



# Prior Technical Accomplishments - Membrane Results



Membrane Characterization  
using button cells

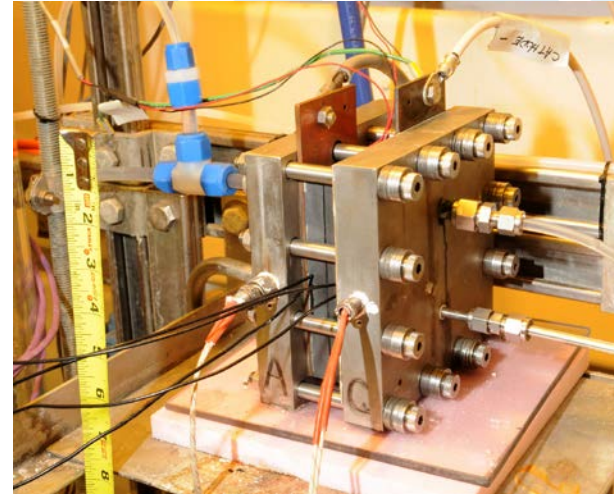
- Nafion® 115 serves as baseline
- PFSA/FEP blend and the BPVE-6F membranes exhibited lower SO<sub>2</sub> transport than Nafion®, but with somewhat lower ionic conductivity
- SDAPP had high conductivity, but also higher SO<sub>2</sub> transport
- PBI, BPVE, SDAPP, Modified PFSA, PFSI and S-PFCB membranes exhibit reduced SO<sub>2</sub> transport and potential for higher temperature operation (120-140°C)



# Prior Accomplishments - Single Cell Electrolyzer Testing

## Test Capabilities:

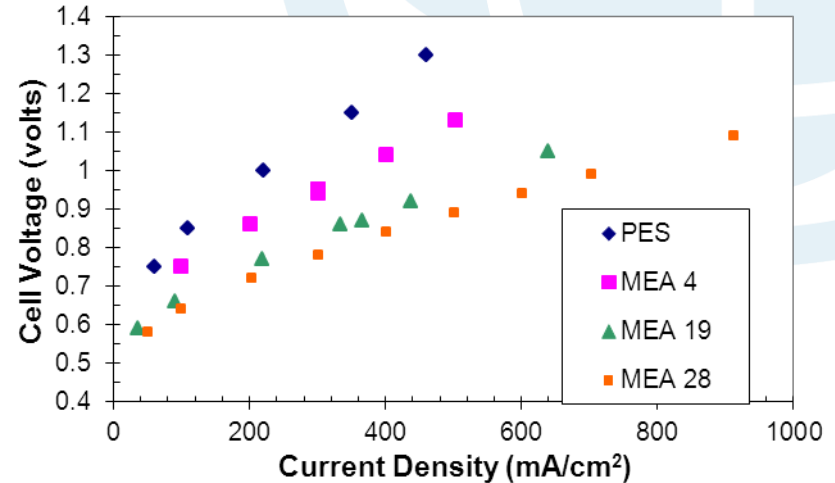
- Reconfigurable electrolyzer
- Nominal 60 cm<sup>2</sup> active cell area
- Pressurized test facility with liquid H<sub>2</sub>SO<sub>4</sub>/SO<sub>2</sub> feed
- Operation to 80°C and 600 kPa
- Unattended operation with remote monitoring
- Current density to 1100 mA/cm<sup>2</sup>
- Hydrogen output is 10-20 L/hr
- Over 40 MEA designs tested



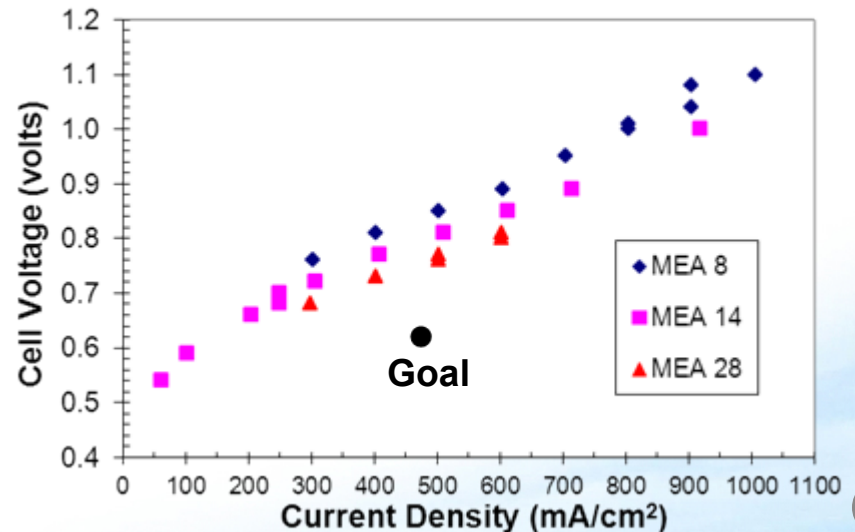
# Prior Accomplishments - Single Cell Electrolyzer Testing

- Tests conducted at ambient conditions and 80°C and up to 600 kPa
- 39 MEA configurations tested from 2007-2010
- Performance improved as the program progressed
- Current status is 760 mV (80°C) versus 600 mV goal
- Higher temperature and pressure operation results in lower voltages – requires new membranes
- Testing resumed in 2013 with industry support

Ambient Conditions Electrolyzer Operation



Electrolyzer Operation at 80C



## Prior Technical Accomplishments - Major Milestones

### Successfully completed Level 1 Milestones for DOE-NE three consecutive years

- M1: Demonstrate long-term operation (>100 hrs) for liquid-fed SO<sub>2</sub> Electrolyzer (5/15/07)
- M1: Complete multi-cell stack testing (3/31/08)
- M1: Demonstrate SDE operation without sulfur buildup limitations (6/30/09)
  - Completed two tests of 216 hours each; post-test examinations showed no signs of sulfur formation

Completed on Schedule

Completed on Schedule

Completed on Schedule

**DOE-NE Nuclear Hydrogen Program was discontinued in FY2010 due to redirection of high temp reactor program; work on HyS development was suspended**

## Technical Accomplishments – Non-DOE Funded

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### Ongoing collaborative research activities funded by others in FY 2013:

- **Long-term single cell testing (SRNL CRADA with industry partner Air Products and Chemicals)**

- Refurbish single cell test facility and demonstrate long-term operation up to 4400 hours (six month). In progress.

- **Advanced membrane testing using gas-fed SO<sub>2</sub> electrolyzer**

- Research at University of South Carolina (Dr. John Weidner) to demonstrate use of modified PBI membranes. See results.



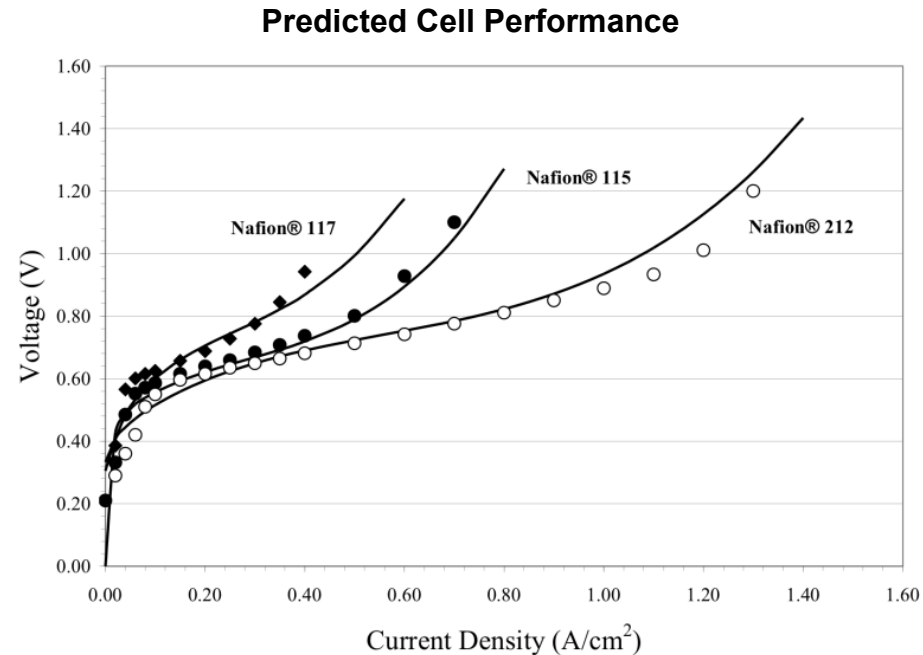
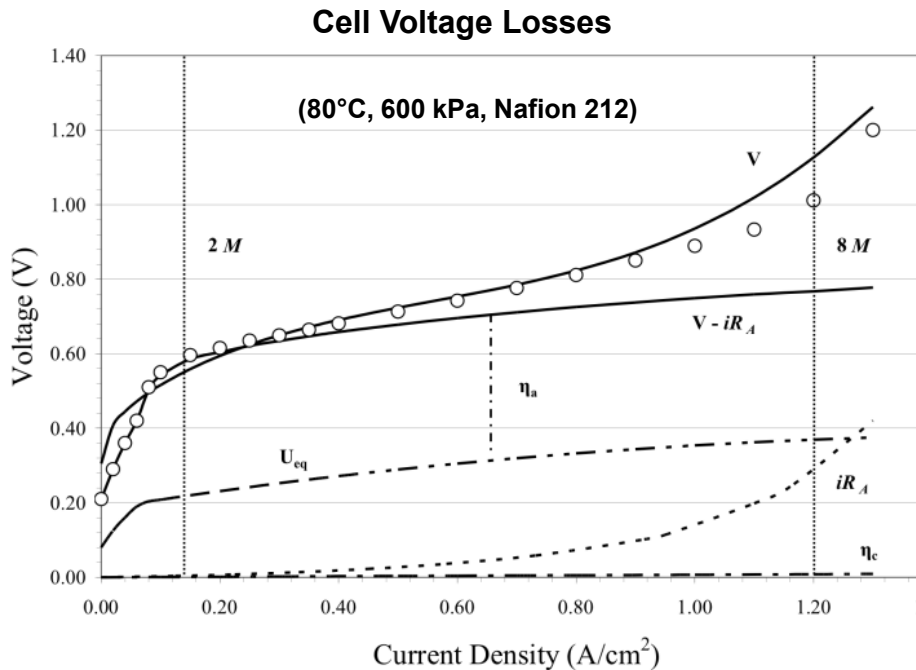
# Technical Accomplishments – University of South Carolina

Modeling and testing with SO<sub>2</sub> gas-fed button-cell

Individual components of cell voltage determined by experiments and mathematical modeling

Largest losses due to kinetics at anode. Membrane resistance increases at high current due to stronger acid

Good model fit with Nafion® membranes



# Technical Accomplishments – University of South Carolina

Comparison of Nafion® and PBI membranes

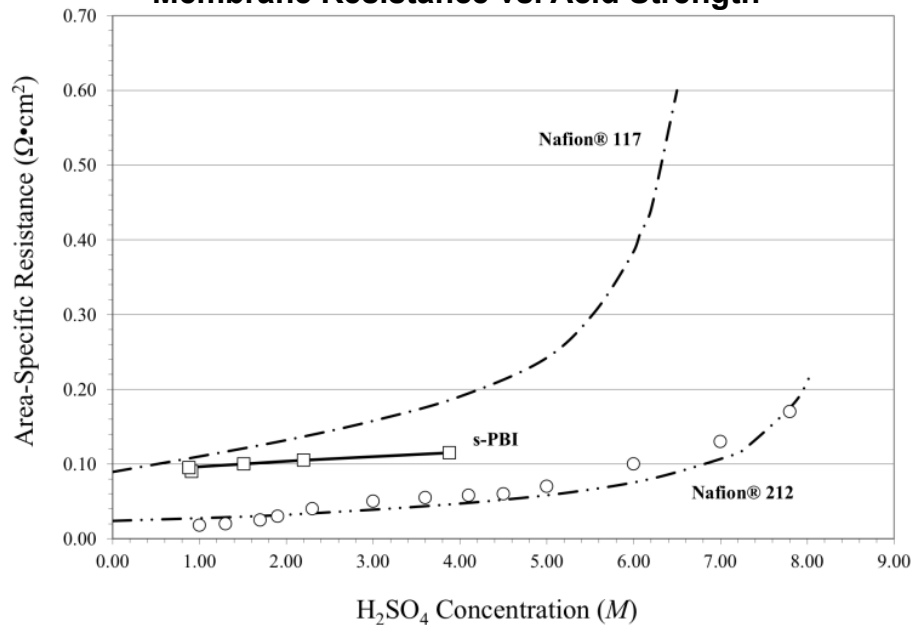
Water added to cathode for Nafion® and anode for sulfonated PBI (s-PBI)

Unlike Nafion®, s-PBI is not affected by high acid concentration

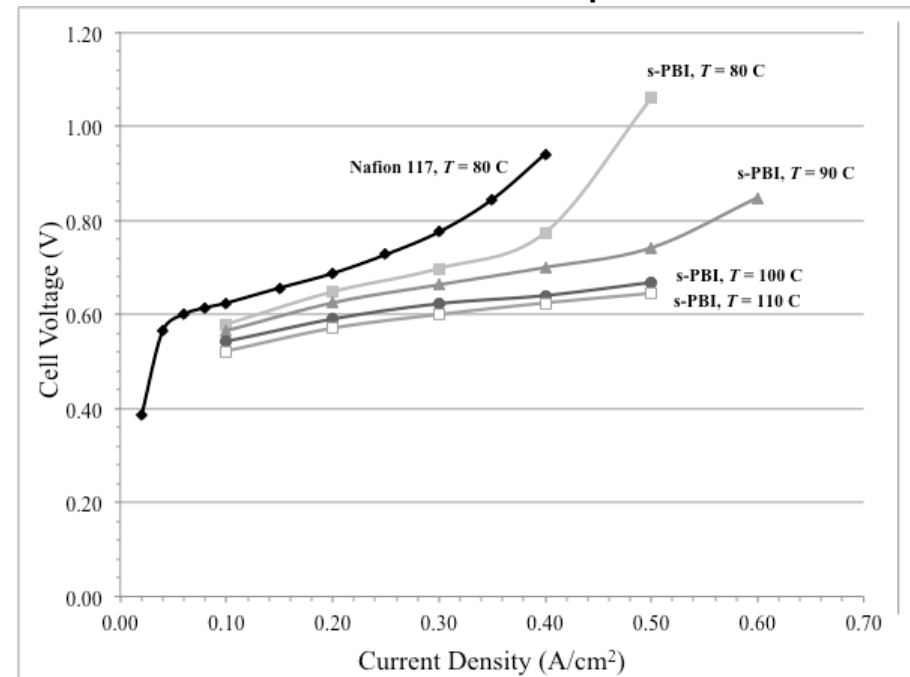
Increased temperature improves s-PBI performance

Product acid more dilute for s-PBI; may require alternative humidification process

Membrane Resistance vs. Acid Strength



Polarization Curve Comparison





# Collaborations

## Collaborations from DOE-NE work (2006-2010)

Sandia National Lab  
Idaho National Lab  
Univ. of South Carolina  
Clemson, Vanderbilt,  
Penn State, CWRU  
DuPont  
Giner Electrochemical

Westinghouse, PBMR,  
Shaw

Acid Decomposer – Bob Moore; Membranes – Mike Hickner  
Acid Decomposition Catalyst – Dan Ginosar  
Cell Design and Testing – John Weidner  
Advanced membrane electrolytes – various PIs

Advanced Nafion® membranes  
Electrolyzer design & manufacture; Gap cell development;  
membranes – Simon Stone  
Nuclear plant interface; process design & cost estimates

## Current Collaborations

Univ. of South Carolina

Cell Design and Testing, Modeling, Advanced membranes –  
Dr. John Weidner

Air Products & Chemicals

Single cell endurance testing – Dr. Steffen Zahn

**NOTE: SRNL designed/built our own electrolyzer and fabricates our own MEAs using membranes from partners.**

# Future Work

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## Proposed 2013 FCT Hydrogen Production Program

- Anticipated Funding = \$300 K
- Twelve month program beginning May 1, 2013
- Conduct R&D to overcome the main obstacles for successful deployment of the Hybrid Sulfur thermochemical cycle by:
  - Identify and test improved electrocatalysts to improve efficiency
  - Identify and test high-temperature, highly selective, long-lived proton-exchange membranes
  - Demonstrate liquid-fed button-cell operation at increased temperature and pressure in order to improve reaction kinetics, utilize advanced membranes, prevent sulfur formation and improve product acid strength

# Future Work – Longer Term

## ● Electrolyzer Development (near term)

- Complete high T&P button cell test facility
- Characterize advanced membranes
- Develop improved electrocatalysts
- Verify operation without sulfur build-up
- Lifetime testing without degradation

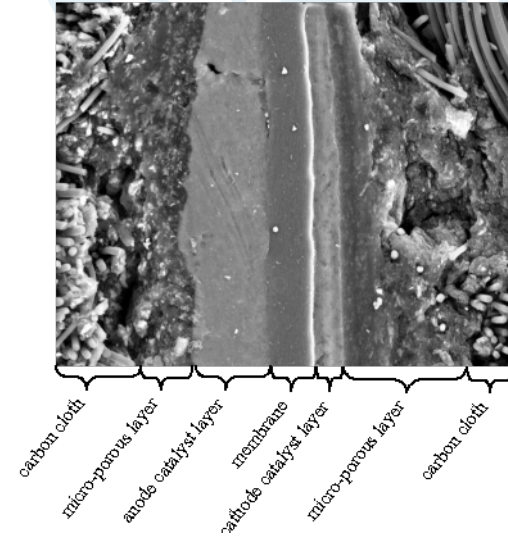
## ● HyS Process Development

- Integrated process demonstration
- Scale-up to pilot plant

## ● Heat Source Development

- On-sun demonstration with solar receiver
- Nuclear high temperature reactor

PEM Cell Cross-section



# Project Summary

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**Relevance** HyS combined with solar receivers (or advanced nuclear reactors) can be an important source of carbon-free hydrogen for industry and the transportation sector.

**Approach** Build on previous work funded by DOE-NE. Leverage ongoing PEM fuel cell work and collaborate with membrane developers. Focus near-term efforts on SO<sub>2</sub> electrolyzer.

**Technical Accomplishments** Previous work resulted in several major milestones, including multi-cell stack demonstration; high efficiency HyS commercial flowsheet; new membranes identified; test facility modified for unattended operation; successful method developed for sulfur-free operation.

**Collaborations** Active partnership with University of South Carolina and Air Products on electrolyzer development and testing; collaborations with other industry and university partners on membranes.

**Future Work** Restart electrocatalyst development; complete and operate pressurized button-cell test facility; test new high temperature membranes, including s-PBI from USC. Continue endurance testing under industry CRADA.