

### WØ<sub>3</sub> and HPA based systems for durable Pt catalysts in PEMFC cathodes



2014 DOE Hydrogen and Fuel Cells Program Review

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FC084

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### **Overview**

### Timeline

- Start date: 05/01/2010
- End date: 04/30/2014
- Percent complete: 100%

#### **Budget**

- Total funding spent: \$2.9M
- Total Project value: \$2.9M
- Cost Share percentage: 9%

### **Barriers**

- Durability
- Cost
- Performance

#### **Partners**

- S. George: UC Boulder
- A. Herring: CSM
- S. Hamrock: 3M
- K. Adjemian: NTCNA
- Tanaka Kikinzoku Kyogo (TKK)

#### **Project lead – NREL**

(John Turner, <u>Anne Dillon</u>,

Katie Hurst, Bryan Pivovar,

K.C. Neyerlin, Jason Zack, and Shyam Kocha)

### **Relevance: Objectives**

Improve electrocatalyst, MEA durability, and activity through the use of  $Pt/WO_3$  and Heteropoly Acid (HPA) modification of carbon support to approach automotive PEMFC activity (**0.44 mA/mg**<sub>Pt</sub>) and durability targets (5000h/10y).

#### **Enhance Pt anchoring to support**

- Suppress loss in Pt ECA under load cycling operations
- Enhance electrocatalytic activity

#### Lower support corrosion

- Increased durability under automotive startup/shutdown operation.
- Suppress Pt agglomeration/electrode degradation

#### Simplify and lower system cost



Polymer Electrolyte Fuel Cell Degradation, Editors: Matthew M. Mench, Emin Caglan Kumbur, T. Nejat Veziroglu, Chapter 3, S. Kocha, Electrochemical Degradation: Electrocatalyst and Support Durability (2012)

### **Develop Accelerated Tests for Durability Support- Protocols**

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#### **RDE Accelerated Test for Support Corrosion**



|                                 | Nissan      | NREL        | DOE        |
|---------------------------------|-------------|-------------|------------|
| Тетр                            | 60°C        | Room Temp   | Room Temp  |
| Scan Rate                       | 500 mV/s    | 100 mV/s    | 1.2 V Hold |
| No of<br>Cycles                 | 5000 Cycles | 6000 Cycles | No Cycles  |
| Time to<br>complete<br>the test | ~ 8 Hrs     | ~ 24 Hrs    | ~ 402 Hrs  |

### **Protocol Comparisons – Pt/C Results**



- Nissan and NREL protocols result in comparable losses for ECA, i<sub>s</sub> and i<sub>m</sub>.
- Nissan protocol (60°C) takes only 8h due to higher temperature accelerant
- NREL protocol is conducted at RT and takes 24 h using low scan rate accelerant.

## Approach





## **Pt/WOx Electrocatalysts**



### Accomplishments

Other oxides, carbide and nitrides were also screened.

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#### **HWCVD Production of Tungsten Oxide Nanostructures**

Synthesis at 150 Torr 4%  $O_2$  in Ar, filament temperature ~ 2000°C.



300 °C

30 °C

30 °C 4 sequential depositions

Dramatic change in particle morphology
 Lower furnace temperature

Sequential depositions lead to rod growth

A.H. Mahan, P. A. Parilla, K.M. Jones and A.C. Dillon, Chem. Phys. Lett. 413 (2005) 88.



# Controlling the stoichiometry of WO<sub>x</sub> by subsequent oxidation in air.





#### Samples are heterogeneous

- Different oxide phases are made upon oxidation
- Sub-stoichiometric material should have higher conductivity
- The stoichiometry of WO<sub>x</sub> may impact subsequent Pt deposition

### **Tungsten Oxide Wet Chemistry Synthesis**



## **Pt Colloid Synthesis (outcome)**

- A literature recipe\* was modified significantly to synthesize Pt nanoparticles of controlled size by:
  - Decreasing the temperature to 80°C
  - Bubbling dilute CO into solution
  - Gradually adding 0.25M NaOH over 3h





\*Wang, Y.; Ren, J.; Deng, K.; Gui, L.; Tang, Y. Chem. Mater. 2000, 12, 1622.

#### Tungsten Bronze Formation Interferes with Standard Electrochemical Surface Area Measurements Techniques



### Cu UPD on Pt/WO<sub>x</sub> Electrocatalysts



Adding carbon (graphite nanofibers – GNF) improves conductivity, but still far short of baseline



#### From NREL ALD

## **Challenges: Electronic Conductivity**

- Oxides supports have low electronic conductivity
- Addition of carbon matrix enhances the overall conductivity
- 3 electron pathways
  - Contact point between Pt and support:
    RA
  - Electronic conductivity through the support: **RB**
  - Electronic conductivity through the added carbon matrix: **RC**
  - Coating of Nafion<sup>®</sup> ionomer on Pt and WO<sub>x</sub> and C not shown: R<sub>Nafion</sub>



Actual Micrograph RA, RB not addressed with GNF

## Mass Activity of Pt/C vs. ALD Pt/WO<sub>x</sub>



#### WOx based electrocatalysts did not meet Pt/C baseline activity

## **WO<sub>3</sub> Semiconductor Energetics**



### Strategy for Continuous Pt ALD Films Using W Adhesion Layer



Continuous film of Pt would help conductivity, but needs a continuous W adhesion layer. Attempted to make a W film via a hydrogen plasma, but didn't work for mesostructured WO<sub>3</sub>

### Results for Pt ALD on WO<sub>x</sub> Particles in Plasma Reactor used for Flat Substrates

#### 200 cycles - MeCpPt(IV)Me<sub>3</sub> with H<sub>2</sub> plasma at 120<sup>o</sup>C



Attempt to produce a W film via a hydrogen plasma to make a continuous film of Pt, but didn't work for mesostructured  $WO_3$  Pt particles are still the result.

#### Atomic Layer Deposition of Platinum Nanoparticles on Titanium Oxide and Tungsten Oxide Using Pt(hfac)<sub>2</sub> and Formalin as the Reactants

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## **Corrosion Currents on Au disk (Corrected)**



#### **Results:**

E (V vs. RHE)

- TiC is the worst. From the inset WC is also less than ideal, and TiN is questionable
- TiO<sub>2</sub>, TaC, and WO<sub>3</sub> appear to be the best for corrosion resistance.

### Pt/SnO<sub>2</sub> Electrocatalysts: SEM



#### Better dispersion



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### Pt/SnO<sub>2</sub> Electrocatalysts: ORR Activity





## Lower electronic conductivity—one of the causes for lower activity of Pt/SnO<sub>2</sub> electrocatalysts; the other being electrode dispersion.

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## **Results**—Pt/SnO<sub>2</sub>



Nafion-free results are better due to Nafion blocking or slowing down oxygen diffusion. Note: this only works for an RDE.

### **Pt/SnO<sub>2</sub> Electrocatalysts: Cyclic Durability**



- Protocol (0.6–1.0V, RT, 500 mV/s) applied to baseline Pt/C and Pt/SnO<sub>2</sub> show similar losses in ECA. Losses are likely to be due to Pt dissolution which is independent of the support.
- Protocol (1.0V–1.6V, RT, 100 mV/s) applied to baseline Pt/C and Pt/SnO<sub>2</sub> show higher losses for Pt/C catalysts since the SnO<sub>2</sub> support is more corrosion resistant.

![](_page_25_Picture_0.jpeg)

## Pt/HPA-Graphitized C Electrocatalysts

![](_page_25_Picture_2.jpeg)

Based on FY13 work on Pt/Ketjen Black-HPA, Fuel Cell Tech Team and DOE recommendation was to evaluated Pt/graphitized carbon-HPA.

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### HPA Functionalization to C, Pt/C, WO<sub>3</sub> and Pt/WO<sub>3</sub>

- Stabilize nano-metallic particles
- Decompose peroxide
- Alter electrochemistry on Pt surface
- Conduct protons

#### Immobilized HPAs as Catalyst Supports

![](_page_26_Picture_6.jpeg)

![](_page_26_Figure_7.jpeg)

HPA functionalization of Carbon black confirmed by EDX spectra.

Carbo

### **Pt/HPA-C EXAFS**

![](_page_27_Figure_1.jpeg)

The strong effect on the Pt edge with increasing HPA loading implies to us that Pt is preferentially binding at the HPA locations. In contrast, there is very little change in the W edge implying that the Pt-W interaction remains approximately unchanged as HPA loading is increased.

The maximum observed in Pt mass activity is likely a result of competing effects of the Pt-W interactions shown here and occupation of preferential binding sites by the HPA.

## **Pt/HPA-C Durability**

![](_page_28_Figure_1.jpeg)

The 0.6-1.0 V cycling (30,000 cycles, 500 mV/s) was used to evaluate Pt dissolution, while 1.0-1.6 V cycling (6,000 cycles, 100 mV/s) evaluated support corrosion. HPA loading was chosen such that initial activity was near equal to Pt/C (blue bars). In both cases, HPA helped maintain catalyst activity by slowing particle growth (red bars).

J. Electrochem. Soc. Volume 159 (12) Pages F871-879 (2012)

![](_page_28_Figure_4.jpeg)

\*All scale bars are 20 nm. \*\*Insets show Pt particle size distribution in 0.5 nm increments starting from 1.5 nm.

### Electrochemical Activity for ALD Catalyst (ALD—Pt/V)

#### Mass Activity Target = 275 mA/mg<sub>Pt</sub>

![](_page_29_Figure_2.jpeg)

In this next set of experiments (to slide 34) however, this data shows a decrease in the activity after HPA modification. The reason for the difference is not clear.

#### Electrochemical Activity for Wet Chemistry Catalysts (Pt/V, Pt/HT-V)

#### Mass Activity Target = 275 mA/mg<sub>Pt</sub>; 380 mA/mg<sub>Pt</sub>

![](_page_30_Figure_2.jpeg)

#### Electrochemical Activity for Wet Chemistry Catalysts (Pt/G-KB)

#### Mass Activity Target = 275 mA/mg<sub>Pt</sub>

![](_page_31_Figure_2.jpeg)

#### Electrochemical Activity for Wet Chemistry Catalysts (Pt/GCNF)

#### Mass Activity Target = 275 mA/mg<sub>Pt</sub>

![](_page_32_Figure_2.jpeg)

## **Cyclic Durability of Pt/C and Pt/C-HPA**

### ECA (m<sup>2</sup>/g<sub>Pt</sub>); ECA Loss (%)

**Pt/Ketjen Black <u>Baseline</u>:** BOL= 100 m<sup>2</sup>/g<sub>Pt</sub>; EOL= 46 m<sup>2</sup>/g<sub>Pt</sub>; 39.5% Loss **Pt/GCNF:** BOL= 82 m<sup>2</sup>/g<sub>Pt</sub>; EOL=71 m<sup>2</sup>/g<sub>Pt</sub>; 13.4% Loss

**Pt/GCNF-HPA:** BOL= 68 m²/g<sub>Pt</sub>; EOL=52 m²/g<sub>Pt</sub>; **23.5% Loss** 

EOL @ 5000 cycles

Pt/GCNF exhibits improved durability compared to baseline, <u>but for post-HPA</u> <u>treatment, the losses are slightly higher</u>.

For these samples, the HPA treatment does not result in an improvement of the durability of the catalyst system.

## FY 2014 1<sup>st</sup> Quarter Milestone

 Meet the Pt/C baseline activity of 275 mA/mg<sub>Pt</sub> mass activity at 0.90 V, 100 kPa with either the HPA modified carbons or the non-carbon supports, but show a 2x greater cyclic durability in RDE tests.

Milestone has been met; but HPA treatment itself does not cause any improvement in durability of a graphitized carbon support.

## 2<sup>nd</sup> and Final Quarter Milestone

• Evaluate remainder of the Pt/HPA treated carbons with RDE

MEA testing was a no-go and the program was ended early with some cost saving to DOE