2014 DOE Hydrogen and Fuel Cells Program Development of Advanced Manufacturing Technologies for Low Cost Hydrogen Storage Vessels

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Project ID # MN008

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Overview

Timeline

- Project start date: 09/2008
- Project end date: 09/2014

Budget

- Total Funding Spent*: \$5,068,361
- Total Project Value: \$5,068,361
- DOE Share: \$2,924,826
- Cost Share Percentage: 40%

Barriers

Hydrogen Storage

- M. Lack of Low-cost Carbon Fiber
- N. Lack of Low-cost
 Fabrication Techniques for
 Storage Tanks

Partners

- Quantum Technologies, Inc.
 (QT) Project lead
- The Boeing Company (Boeing)
- Pacific Northwest National Laboratory (PNNL)

* as of 3/31/14







Relevance

Objectives: To manufacture Type IV H₂ storage pressure vessels, utilizing a new hybrid process with the following features:

- Optimize elements of advanced fiber placement (AFP) & commercial filament winding (FW)
- Improve understanding of polymer liner H₂ degradation

With the aim of addressing the barriers by achieving a manufacturing process with:

- 1. lower composite material usage
- 2. higher manufacturing efficiency







Overall Approach Quantum, Boeing, PNNL

- QT modified the existing in-house software to support hybrid vessel designs for reducing carbon fiber usage
- QT designed the hybrid vessels
- Boeing built the AFP dome caps per QT designs
- QT installed the dome caps and manufactured the vessels with FW
- QT performed tests per EC79/2009 standard to verify the vessel designs using the latest software
- Test result confirmed the software was sufficient for hybrid vessel designs
- PNNL prepared cost model to compare baseline and hybrid vessels
- PNNL studied polymer liner compatibility in hydrogen













Approach

Quantum

Tests Completed per EC79/2009

Test	Passing Criteria
Burst	Burst pressure to exceed 157.5 MPa (2.25 x 70 MPa)
Ambient Cycle	Cycle count ≥ 15,000 times with no leakage
Accelerated Stress Rupture	Burst pressure to exceed 133.9 MPa (85% x 157.5 MPa)
	No rupture within the first 9,000 cycles (0.6 x 15,000 cycles) and may
Impact Damage	fail by leakage afterward
	No leakage during leak test,
Extreme Temperature Cycle	Burst pressure to exceed 133.9 MPa (85% x 157.5 MPa)

These tests are the most critical/influential to the hybrid design

Validated modeling software with burst test result







Approach Boeing

Continuous Quality Improvements on AFP Dome Caps

- Software re-programming
- Upgraded fiber creel system







Approach PNNL

- Hydrogen Compatibility In-situ Testing
 - PNNL built and tested an in-situ tensile rig for high pressure hydrogen
 - Motivation: Hydrogen degrades polymers
 - Degradation affects leak rate, durability, lifetime
 - Prior ex-situ testing demonstrates
 - o Blistering
 - Modulus, strength decreases
 - o Time dependent
 - Need in-situ device to achieve full understanding of actual liner environment



In-situ tensile testing







Accomplishments and Progress Quantum



Pacific Northwest NATIONAL LABORATORY

- Vessel 14
 - Reduced composite weight by 5.7% from previous design by
 - Reducing AFP dome cap layers
 - Optimizing FW layup
 - Aft AFP dome cap design had a dip (potentially cause composite voids)
 - Burst pressure was 90% of requirement



Dip

Composite layup redesign of Vessel 14 reduced composite usage and weight by 5.7%









BOEING Pacific Northwest

Accomplishments and Progress Quantum

- Vessel 15 & 16
 - Same AFP dome cap design as Vessel 14
 - Filled the dip on the AFP dome cap with carbon fiber woven fabric rings



Fabric rings

- CT scan showed no voids
- Vessel 15 Achieved 103% of required burst pressure in mid cylinder
 Confirmed the in-house software is sufficient for hybrid design



Vessel 16 – Achieved target cycle test count of 15,000

Test results showed the latest design meets EC79 burst and cycle requirements



Accomplishments and Progress Quantum

Test to be performed

Non-destructive verification method

Vessel 15: Burst Test Vessel 16: Cycle Test Vessel 15 and 16 Exceeded target burst pressure by more than 3% Achieved target cycle count of 15,000

Manufactured per Vessel 15 design

Vessel 17: Accelerated Stress Rupture Test Vessel 18: Impact Damage Test

Vessel 17 and 18 Exceeded target burst pressure after Accelerated Stress Rupture Test by more than 14% Achieved target cycle count of 11,658 before leak after Impact Damage Test







Computed Tomography (CT)

Scan

High Speed Camera

- Vessel 17 & 18
 - Identical design to Vessel 15
 - Vessel 17 (Accelerated stress rupture test) Achieved 114% of the required burst pressure



Vessel 17 showed the hybrid design is resistant to creep degradation at high temperature







Accomplishments and Progress Quantum

 Vessel 18 (Impact damage test) – Achieved cycle count of 11,658 before leakage



Vertical drop





Horizontal drop

45° drop

 Post test analysis shows large gap between fiber placed domes and liner, resulting in leakage

> Design was sufficient to meet drop requirement Process improvement required for better fit between AFP and liner







Accomplishments and Progress Quantum

Test to be performed

Vessel 17: Accelerated Stress Rupture Test Vessel 18: Impact Damage Test

Vessel 17 and 18 Exceeded target burst pressure after Accelerated Stress Rupture Test by more than 14% Achieved target cycle count of 11,658 before leak after Impact Damage Test

Continue manufacturing per Vessel 15 design

Vessel 19: Extreme Temperature Pressure Cycle Test

Vessel 19 Achieved cycle count of 3,679







Continuous Quality Improvements

- Improved fiber placement
 - Within 2° of the angle specified
 - Within 0.05 inch of polar openings
- Upgraded fiber creel system
 - New smart-motor control system
 - Newly designed dancer system
 - Dynamically-control, closed-loopactive tow tensioning
 - Allowing for consistent tension on each tow regardless of tow direction or speed





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High consistency from part to part





In-situ High Pressure Hydrogen Testing

- In-situ tensile tests of HDPE liner material in high pressure hydrogen
 - Upgraded in-situ tensile tester
 - 100% hydrogen at 4000 psi, 4500 psi, 5000 psi tests





In-situ tensile tester for high pressure hydrogen

Pulled HDPE mini tensile sample



As cut HDPE mini tensile sample

Noticeable drop in UTS with negligible change in modulus when hydrogen pressure increases







In-situ High Pressure Hydrogen Testing (Cont.)

- Results of high pressure tensile testing
 - Noticeable decrease in UTS with increasing pressure; ~ 6% decrease at 5,000 psi
 - Potential non-linear behavior with higher pressures
 - No dilation observed upon pressurization indicates increase in flow/lubricity
 - Small or no change in modulus



Cost Analysis of Advanced Hybrid Vessel Manufacturing Processes

- Cost model includes materials, labor, overhead, balance of system, manufacturing equipment, and factory space costs
- Quantum and Boeing experience provided manufacturing details to estimate \$/kg of FW and AFP composites
- Hybrid composite design and testing provided the mass of FW and AFP composites used in successful vessel designs
- Designs showed separate manufacturing of AFP dome reinforcements was successful
- FW manufacturing compared with hybrid FW+AFP manufacturing
- The added cost of AFP material, manufacturing equipment, and factory space is small compared to the savings in FW composite.

Hybrid vessels save up to 20% in cost and 32% in composite mass





Accomplishments and Progress: Response to Previous Year Reviewers' Comments

The project was not reviewed last year







Collaborations

					Within DOE	
					H ₂ and FC	
Partner	Prime	Sub	Industry	Fed Lab	Program	Collaboration
Quantum Technologies,						Design and test hybrid pressure
Inc.	v	100	v		V	vessels manufactured with
	XXX		~	combination of FW and AFP		
					1	
Boeing Research and						Develop AFP process for vessel
Technology		x	x	1		manufacturing and provide
			~			material testing capabilities
Pacific Northwest National					and the second	Develop cost model for hybrid
Laboratory						vessel manufacturing and study the
		Х		X	X	impact of H ₂ absorption in polymer
		1				liners







Proposed Future Work

- Replace AFP end caps with localized FW process
- Incorporate polar boss feature into foam tool to minimize gap between AFP end cap and liner
- Investigate load transfer between AFP and FW due to different resin systems at extreme temperatures
- Study potential non-linear behavior of HDPE with higher pressures







Project Summary

- Latest vessel design passed all planned tests per EC79
 - Burst test
 - Pressure cycle test
 - Accelerated stress rupture test
 - Impact damage test

With the exception of

- Extreme temperature cycle test
- Validated modeling software for hybrid design
- Load transfer between AFP and FW remains a challenge at extreme temperatures
- AFP process improvements to deliver parts with higher quality
- In-situ hydrogen tester built
- Approximately 6% decrease in UTS with hydrogen pressure increase from 0 to 5,000 psi
- Updated cost model with latest hybrid vessel design, showing a 20% cost and 32% composite mass savings compared to baseline vessel







Technical Back-Up Slides







Background on Hybrid Vessel Manufacturing



1. Highly-accurate foam mandrels. Three ¹/₄-inch tows are placed on mandrel.



3. Both forward and aft dome caps are then transferred and installed to the hydrogen storage liner.



2. AFP dome caps (forward and aft) are then removed from foam tooling and brought to wind cell.





4.



The final stage is to filament wound

over the forward and aft dome caps.

Comparison of Vessel Manufacturing Costs for 129L

Summary Table		Baseline 129L	Filament Wound + Advanced Fiber Placement			
		Filament Wound	Tank 1 Layup	Tank 7 Layup	Tank 15 Layup	
Composite Mass, kg	FW	76	63.4	56.2	49.6	
	AFP		1.5	2.4	1.9	
Total Composite Mass, kg		76	64.9	58.6	51.5	
Composite Mass Savings		0%	15%	23%	32%	
Composite	FW	13.2	13.2	13.2	13.2	
Placement Speed, kg/hr	AFP		0.9	0.9	0.9	
Composite	FW	5.75	4.80	4.25	3.75	
Placement Time, hr/tank	AFP		1.65	2.64	2.05	
Total Place Time, hr/tank		5.75	4.80	4.25	3.75	
# Manuf. Cells for 500K/yr	FW	191	159	142	125	
	AFP		165	264	205	
Tank Costs						
FW Composite		\$2,604	\$2,172	\$1,926	\$1,699	
AFP Composite			\$103	\$164	\$128	
End Boss		\$250	\$250	\$250	\$250	
Manuf. Equipment		\$36	\$41	\$45	\$40	
Factory Space		\$7	\$7	\$8	\$7	
Total Tank Cost		\$2,897	\$2,573	\$2,393	\$2,124	
% Tank Cost Savings		0%	11%	17%	27%	
DOE Measures						
Specific Energy, kWh/kg ¹		1.50	1.67	1.78	1.93	
Cost Efficiency, \$/kWh ²		\$25.34	\$23.40	\$22.31	\$20.70	
¹ 5 kg H2 * 33.31 kWh/kgH2 / (Tank+OtherComponents+H2 mass, kg) OtherCompMass=30kg						
² (Tank+OtherComponents \$\$) / (5 kg H2 * 33.31 kWh/kgH2)						



BOEING



Comparison of Vessel Manufacturing Costs Based on New DOE Record for 129L

Summary Table		Baseline 129L	129L Filament Wound + Advanced Fiber Placement			
		Filament Wound	Tank 1 Layup	Tank 7 Layup	Tank 15 Layup	
Composite Mass, kg	FW	76	63.4	56.2	49.6	
	AFP		1.5	2.4	1.9	
Total Composite Mass, kg		76	64.9	58.6	51.5	
Composite Mass Savings		0%	15%	23%	32%	
Composite	FW	13.2	13.2	13.2	13.2	
Placement Speed, kg/hr	AFP		0.9	0.9	0.9	
Composite	FW	5.75	4.80	4.25	3.75	
Placement Time, hr/tank	AFP		1.65	2.64	2.05	
Total Place Time, hr/tank		5.75	4.80	4.25	3.75	
# Manuf. Cells for 500K/yr	FW	191	159	142	125	
	AFP		165	264	205	
Tank Costs						
FW Composite		\$1,792	\$1,495	\$1,326	\$1,169	
AFP Composite			\$71	\$113	\$88	
End Boss		\$14	\$14	\$14	\$14	
Liner		\$23	\$23	\$23	\$23	
Balance of Plant		\$940	\$940	\$940	\$940	
Assembly		\$12	\$12	\$12	\$12	
Total Tank System Cost		\$2,781	\$2,554	\$2,428	\$2,246	
% Tank Cost Savings		0%	8%	13%	19%	
DOE Measures						
Specific Energy, kWh/kg ¹		1.5	1.7	1.8	1.9	
Cost Efficiency, \$/kWh ²		\$16.7	\$15.3	\$14.6	\$13.5	







Comparison of Vessel Manufacturing Costs Based on New DOE Record for 147.3L

Summary Table		DOE 2013, 147.3L	147.3L Filament Wound + Advanced Fiber Placement			
		Filament Wound	Tank 1 Layup	Tank 7 Layup	Tank 15 Layup	
Composite Mass, kg	FW	91	75.9	67.3	59.4	
	AFP		1.8	2.9	2.2	
Total Composite Mass, kg		91	77.7	70.2	61.6	
Composite Mass Savings		0%	15%	23%	32%	
Composite	FW	13.2	13.2	13.2	13.2	
Placement Speed, kg/hr	AFP		0.9	0.9	0.9	
Composite	FW	6.9	5.7	5.1	4.5	
Placement Time, hr/tank	AFP		2.0	3.2	2.5	
Total Place Time, hr/tank		6.9	7.7	8.3	6.9	
# Manuf. Cells for 500K/yr	FW	229	191	170	150	
	AFP		197	316	245	
Tank Costs						
FW Composite		\$2,146	\$1,790	\$1,588	\$1,400	
AFP Composite			\$85	\$136	\$105	
End Boss		\$14	\$14	\$14	\$14	
Liner		\$23	\$23	\$23	\$23	
Balance of Plant		\$940	\$940	\$940	\$940	
Assembly		\$12	\$12	\$12	\$12	
Total Tank System Cost		\$3,134	\$2,863	\$2,712	\$2,494	
% Tank Cost Savings		0%	9%	13%	20%	
DOE Measures						
Specific Energy, kWh/kg ¹		1.5	1.6	1.8	1.9	
Cost Efficiency, \$/kWh ²		\$16.8	\$15.3	\$14.5	\$13.4	





