

Electrochemical Hydrogen Compressor

Ludwig Lipp FuelCell Energy, Inc. June 17, 2014

Project ID #PD048

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Overview

Timeline

- Project start date: 7/15/10
- Project end date: 10/14/14

Budget

- Total Funding Spent: \$1,517,000*
- Total DOE Project Value: \$1,993,642

Barriers

- Barriers addressed for gaseous hydrogen compression:
 - More reliable
 - Lower-cost
 - Higher efficiency

Partners

- Collaborations: Sustainable Innovations, LLC
- Project lead: FuelCell Energy





Relevance

Impact of EHC:

- Increases reliability/availability over current mechanical compressors
- Ensures "no possibility of lubricant contamination" (No moving parts) → Fuel Cell Quality H₂
- Increases Compression Efficiency to 95% (DOE 2015 Target)
- Potentially reduces cost of H₂ delivery to <\$1/gge (DOE Long Term Target)





Approach

- Use high-pressure electrolyzer experience for mechanically robust cell design
- Higher current density operation to minimize capital and operating costs
- Improved flow field design to increase H₂ recovery efficiency
- Simple system: Reduce capital cost by increasing cell size and reducing number of parts





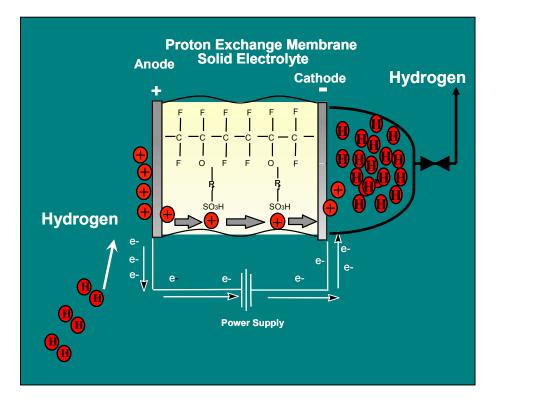
Approach

ITEM	APPROACH	
Increase Pressure, Life, Efficiency	-Cell & Stack Design Enhancements -MEA Improvements -Multi-Stage Operation -Very High Single Stage Compression	
Lower System Cost	 -Cell & Stack Design Enhancements -Increase Current Density -Increased Durability/Life -Increase Single-Stage Pressure Capability -Design for Mfg & Assembly -Lower Labor Rates -Lower Cost Materials of Construction -Lower Part Count -Leverage Economies of Scale -Increase Cell Active Area 	





Principle of Electrochemical Hydrogen Compressor



EHC does not follow P V = n R TRather Nernst Eqn: $RT = \begin{pmatrix} P_2 \end{pmatrix}$

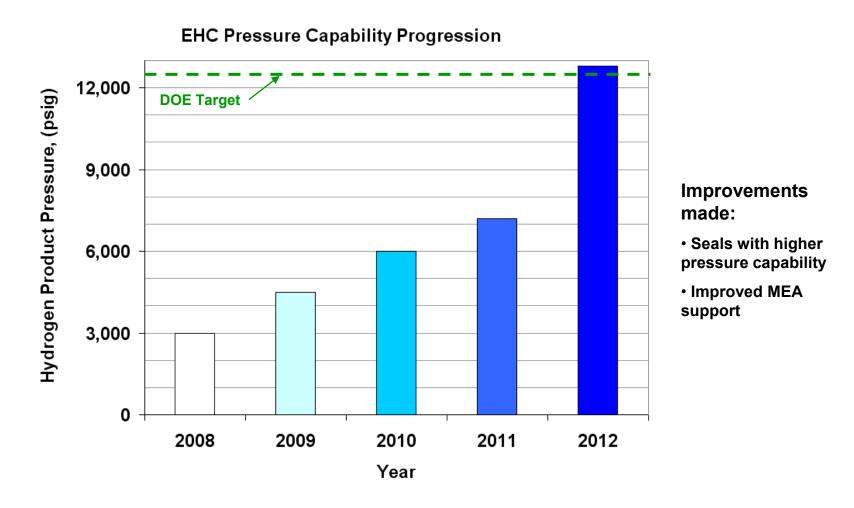
 $V_{\text{theor}} = \frac{RT}{nF} \ln \left(\frac{P_2}{P_1}\right)$

- Simple operating principle with no moving parts Solid State !
 - Use of hydrogen electrode for high compression efficiency





EHC Pressure Capability

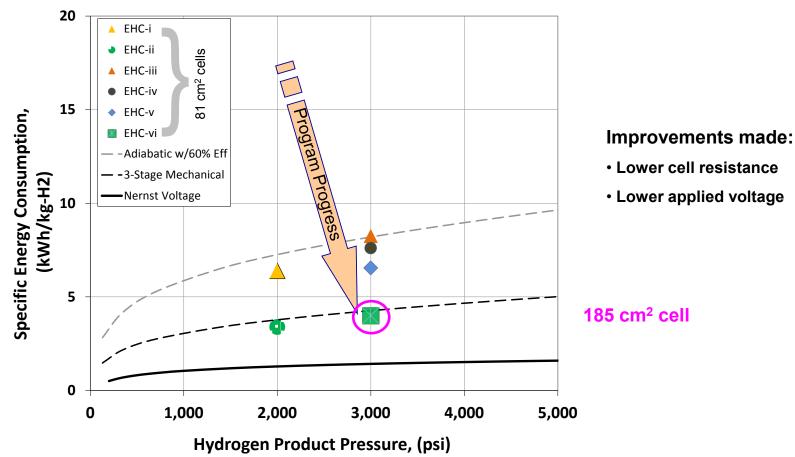


Met DOE 2015 pressure target for forecourt compressors





Reduction in the Energy Consumption of EHC

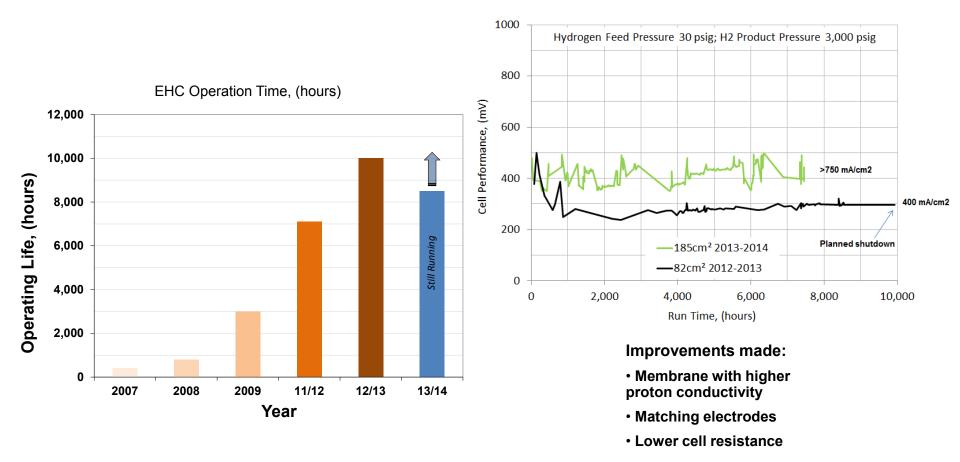


Improved cell design and materials for 3,000 psi





EHC Durability



10,000 hr operation at ~95% H₂ recovery

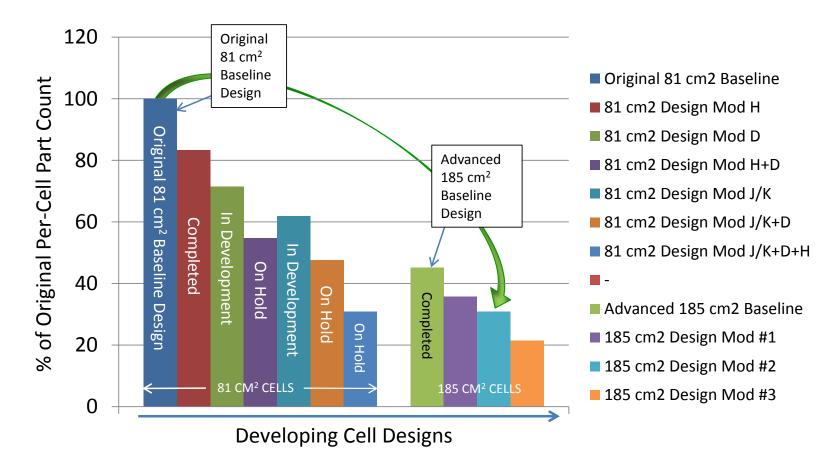
>8,500 hrs at elevated current density (≥750 mA/cm²) in 185 cm² cell





EHC Cost Reduction

Reduction in Parts per EHC Cell



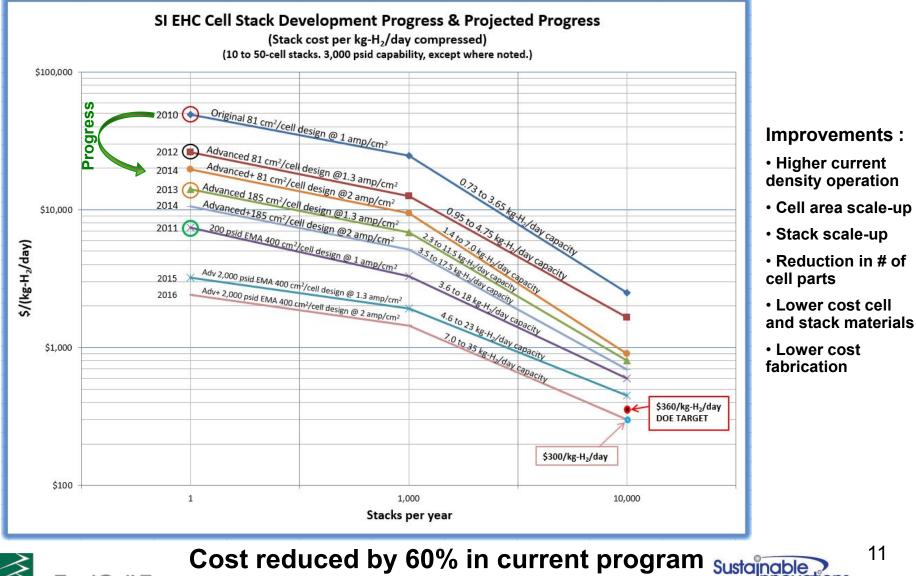
Reduced part count by 75% of original design





Opportunities for Cost Reduction

Stack Cost/H₂ Compression Capacity - \$/kg-H₂/day



FuelCell Energy

EHC Stack Development

	3-Cell Stack #1	3-Cell Stack #2	3-Cell Stack #3	5-Cell Stack	10-Cell Stack	8-Cell Stack 185 cm ²
Pressure, (psig)	4,550	Up to 1,000	2-3,000	Up to 3,000	Up to 3,050	3,000
Current Density, (mA/cm²)	≤500	Up to 2,200	≤500	≤450	≤500	≤720
Capacity, (lbs/day)	0.2	Up to 0.8	0.2	0.3	0.6	2.0
Operation, (hours)	150	~100	>2,000+	1,800	~400	>3,800

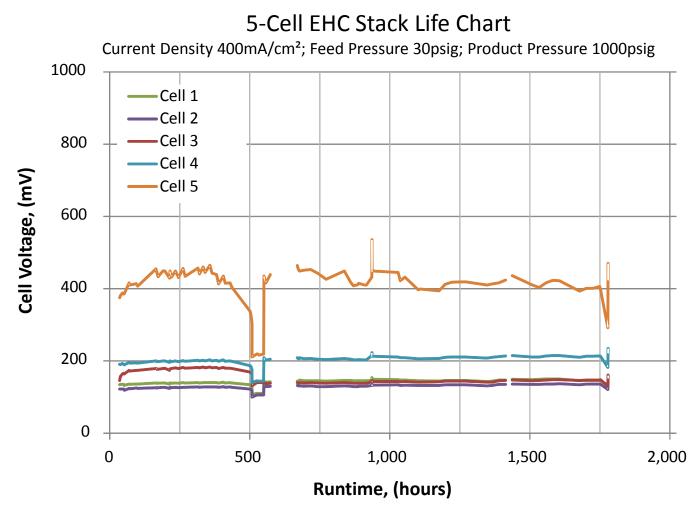
[†] At Sustainable Innovations

Cumulatively >8,000 hr operating experience





Subscale Stack Durability

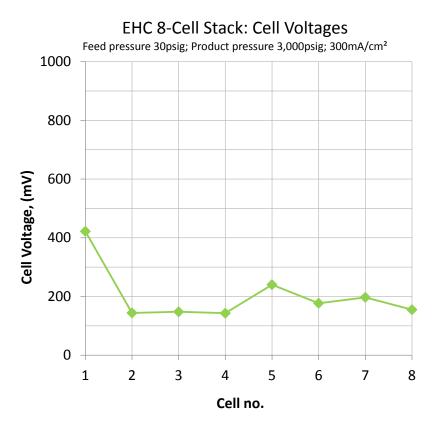


Met program target of 1,000 hr stable operation in EHC stack





Larger Area EHC Stack



Improved cell to cell performance variation by ~50%

Increasing Hydrogen Capacity by 7x

DC Load, (Amps)	133
Average Cell Voltage, (Volts)	0.373
Flux Rate, (SLPM H ₂)	7.6
Power, (Watts)	397
Production Rate, (lb H ₂ /day)	2

Met program target of 2 lb/day hydrogen at 3,000 psi





Collaborations

Prime

- FuelCell Energy, Inc. (Industry):
 - System development and application engineering
 - Membrane and electrode design and fabrication

Subcontractor

- Sustainable Innovations, LLC (Small Business):
 - Cell and stack design and fabrication
 - Scale-up design and fabrication
 - EHC stack cost reduction and estimates





Proposed Future Work

- Continue endurance tests of 10,000 hr and 8,500 hr cells
- Continue testing short stack
- Build and test taller EHC stack
- Complete test facility for larger capacity EHC stacks
- Demonstrate 1,000 hr operation at 2 lb/day H₂ capacity

compressing to 3,000 psi





Scale-Up Plan to Reach 8 lb/day

Activity Covered Under Current Funding			Activity Not Covered Under Current Funding	
			25 - Cell 185 cm ² Active Area 500 – 1000 mA/cm ² Up to 8 lb/day	
185 c 500 -		8 - Cell 185 cm ² Active Area 500 – 1000 mA/cm ² 2 - 3 lb/day		
	Single Cell 185 cm ² Active Area 500 - 1500 mA/cm ² Up to 0.5 lb/day			
400 mA/cm ² 0.3 lb/day		,		





Achievements in EHC Technology Development

Parameter	Program Goals	Current Status	DOE Goals
Hydrogen Product Pressure	Up to 3,000 psi building block, 6-12 kpsi	12,800 psi single stage 6,000 psi 2-stage	12,700 psi
Hydrogen Inlet Press.	5 - 300 psi	0 – 2,000 psi	300 psi
Compression Ratio	Up to 300:1	300:1	43:1
Hydrogen Recovery Efficiency	90 - 95%	>98%	99.5%
Hydrogen Flux	500 -1,000 mA/cm ²	≥750 mA/cm² for >8,500 hrs (185 cm² cell)	-
Hydrogen Capacity	2-4 lb/day at 3,000 psi	2 lb/day	Up to 1000 kg/day
Endurance Capability	1,000 hrs at 3,000 psi	>10,000 hrs at 3,000 psi	>5 years
Compression Efficiency	<10 kWh/kg at 3,000 psi	3-12 kWh/kg from <30 to 3,000 psi	6.2 kWh/kg from 300 to 12,500 psi



Project Summary

Relevance: Provide highly efficient, reliable and cost-effective hydrogen compression (up to 6,000/12,000 psi)

Approach: Develop electrochemical compressor – solid state device

Technical Accomplishments:

- Reduced capital cost by >60% by increasing current density, increasing cell active area and by design improvements (reduced cell part count)
- Operated >8,500 hrs in 185 cm² cell at \geq 750 mA/cm² at high H₂ recovery (\geq 95%)
- Demonstrated 2 lb/day capacity at 3,000 psi in 185 cm² stack

Collaborations: Active partnership with industry (Sustainable Innovations) on materials, design and fabrication

Proposed Future Work: Scale-up to taller stack to further increase throughput and lower the cost





Acknowledgement

- FCE: Pinakin Patel, Ray Kopp, Jonathan Malwitz, Paul Pinard
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