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Non-Platinum Group Metal OER/ORR Catalysts for Alkaline Membrane Fuel Cells and Electrolyzers

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Organization: Proton OnSite

Date: May 15, 2015

Project ID: FC-133

Overview

Timeline

- Project Start: 15 Feb 2015
- Project End: 15 Nov 2015
- Percent complete: ~30%

Budget

- Total project funding
 - DOE share: \$150,000

Partners

- Rutgers University:
 - Charles Dismukes (PI)
 - Graeme Gardner
 - Karin Calvino

Barriers

- Barriers addressed
 - G: Capital Cost (Electrolyzer + Fuel Cell)

Table 3.4.7.a Technical Targets: Portable Power Fuel Cell Systems (<2 Watt)^a

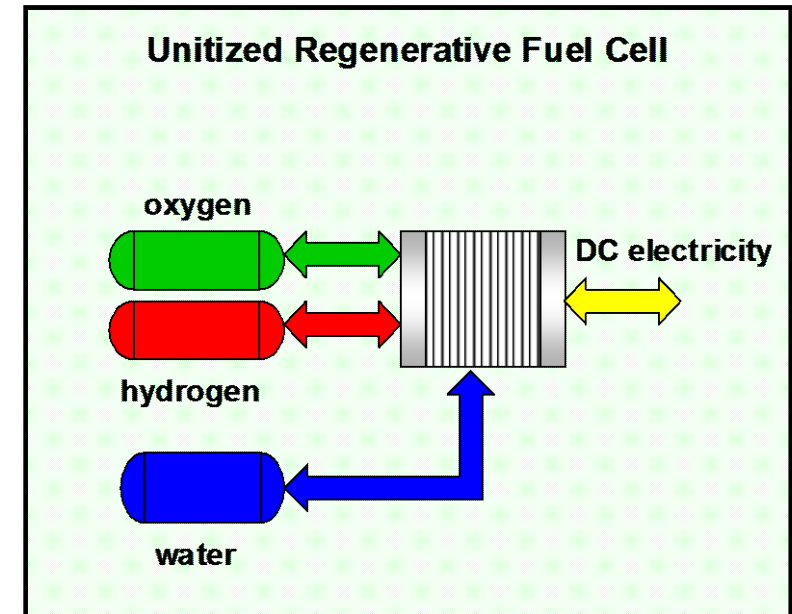
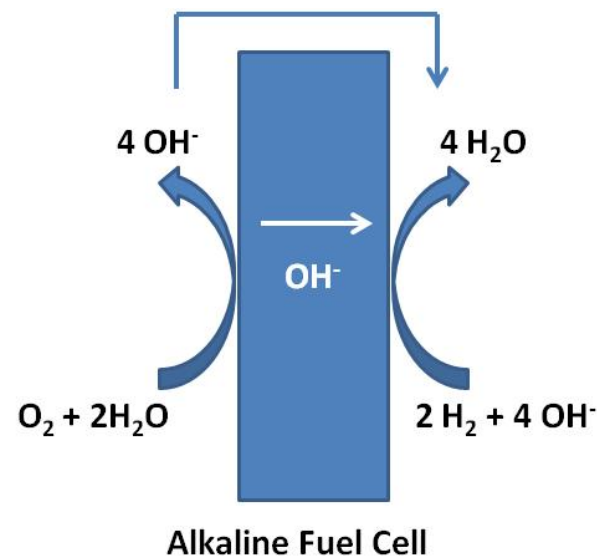
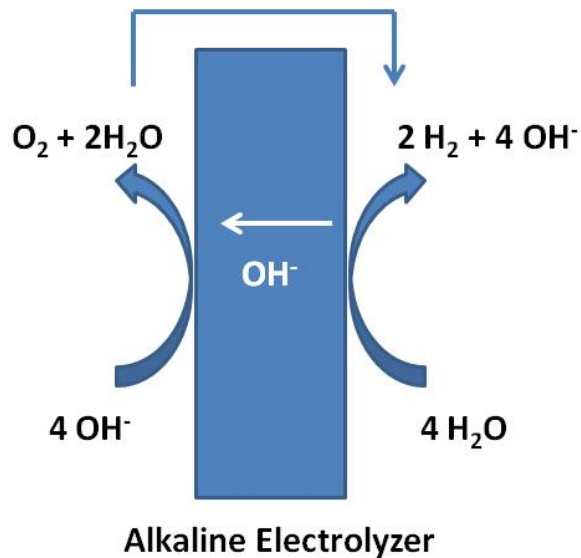
| Characteristic | Units | 2011 Status | 2013 Targets | 2015 Targets |
|---|-----------|-------------|--------------|--------------|
| Specific power ^b | W/kg | 5 | 8 | 10 |
| Power density ^b | W/L | 7 | 10 | 13 |
| Specific energy ^{b,c} | Wh/kg | 110 | 200 | 230 |
| Energy density ^{b,c} | Wh/L | 150 | 250 | 300 |
| Cost ^d | \$/system | 150 | 130 | 70 |
| Durability ^{e,f} | hours | 1,500 | 3,000 | 5,000 |
| Mean time between failures ^{f,g} | hours | 500 | 1,500 | 5,000 |

Table 3.1.4 Technical Targets: Distributed Forecourt Water Electrolysis Hydrogen Production^{a, b, c, l}

| Characteristics | Units | 2011 Status | 2015 Target | 2020 Target |
|--|---------|----------------------------|----------------------------|--------------------|
| Hydrogen Levelized Cost ^d (Production Only) | \$/kg | 4.20 ^d | 3.90 ^d | 2.30 ^d |
| Electrolyzer System Capital Cost | \$/kg | 0.70 | 0.50 | 0.50 |
| | \$/kW | 430 ^{e, f} | 300 ^f | 300 ^f |
| System Energy Efficiency ^g | % (LHV) | 67 | 72 | 75 |
| | kWh/kg | 50 | 46 | 44 |
| Stack Energy Efficiency ^h | % (LHV) | 74 | 76 | 77 |
| | kWh/kg | 45 | 44 | 43 |
| Electricity Price | \$/kWh | From AEO 2009 ⁱ | From AEO 2009 ⁱ | 0.037 ^j |

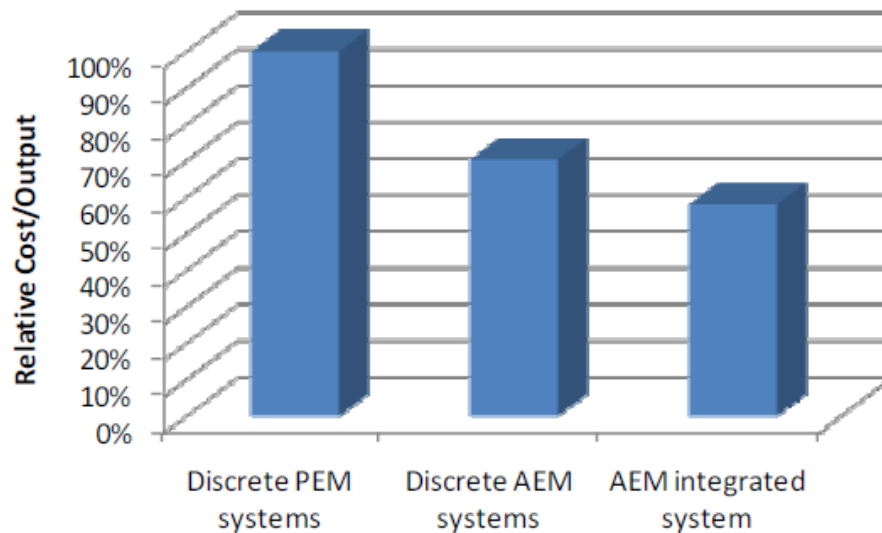
Project Goal

- Anion exchange membrane (AEM) based unitized regenerative fuel cell (URFC)
- Non-platinum group metal (PGM)-based oxygen electrode



Relevance

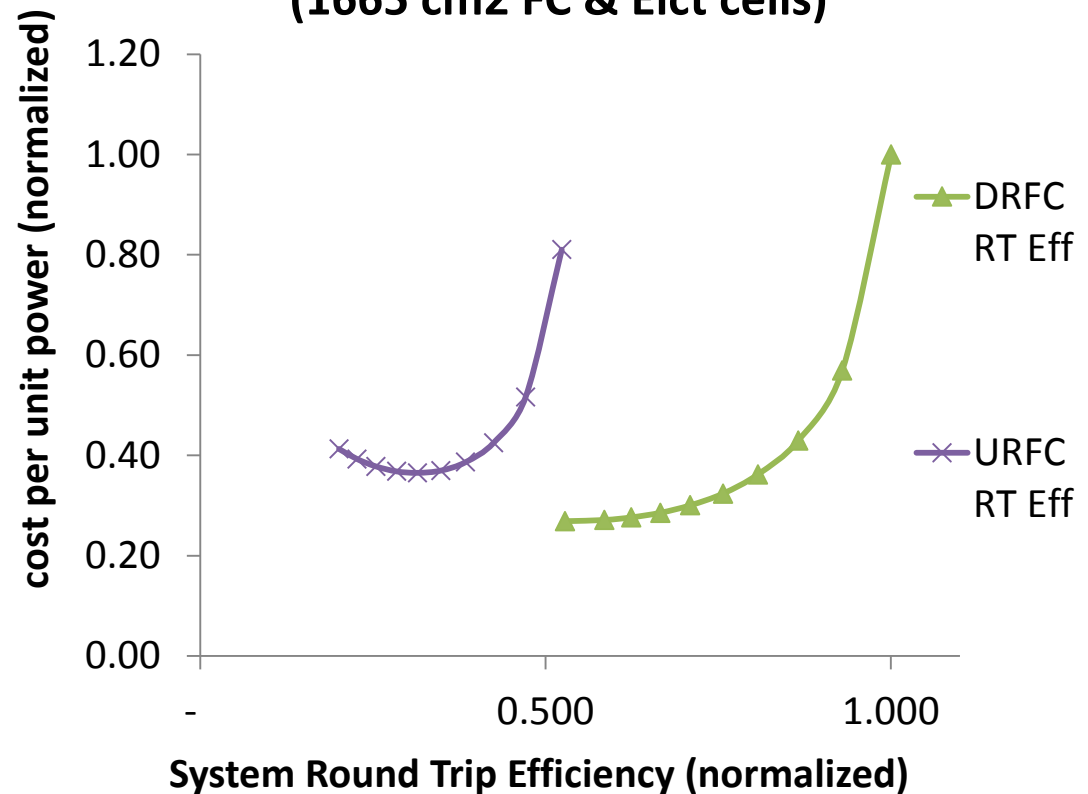
- Stacks are the largest cost components of RFCs
 - Integrated approach should make significant \$ impact
- Precious metal content
 - Decrease or eliminate PGM metals in electrodes
- Membrane electrode assembly cost
 - Anion exchange (AEM) vs proton exchange (PEM) membranes
- Balance of stack component cost
 - Reduction in cost using stainless steel vs valve metal components



Relevance: Energy Storage

- Costs need to be significantly reduced to enable energy markets
 - Energy capture and supply
 - Auxiliary power units
 - Backup power
 - Load leveling
 - Peak shaving
- URFC traditionally sacrifices operating efficiency for capital cost
 - AEM chemistry opens up broader range of catalysts

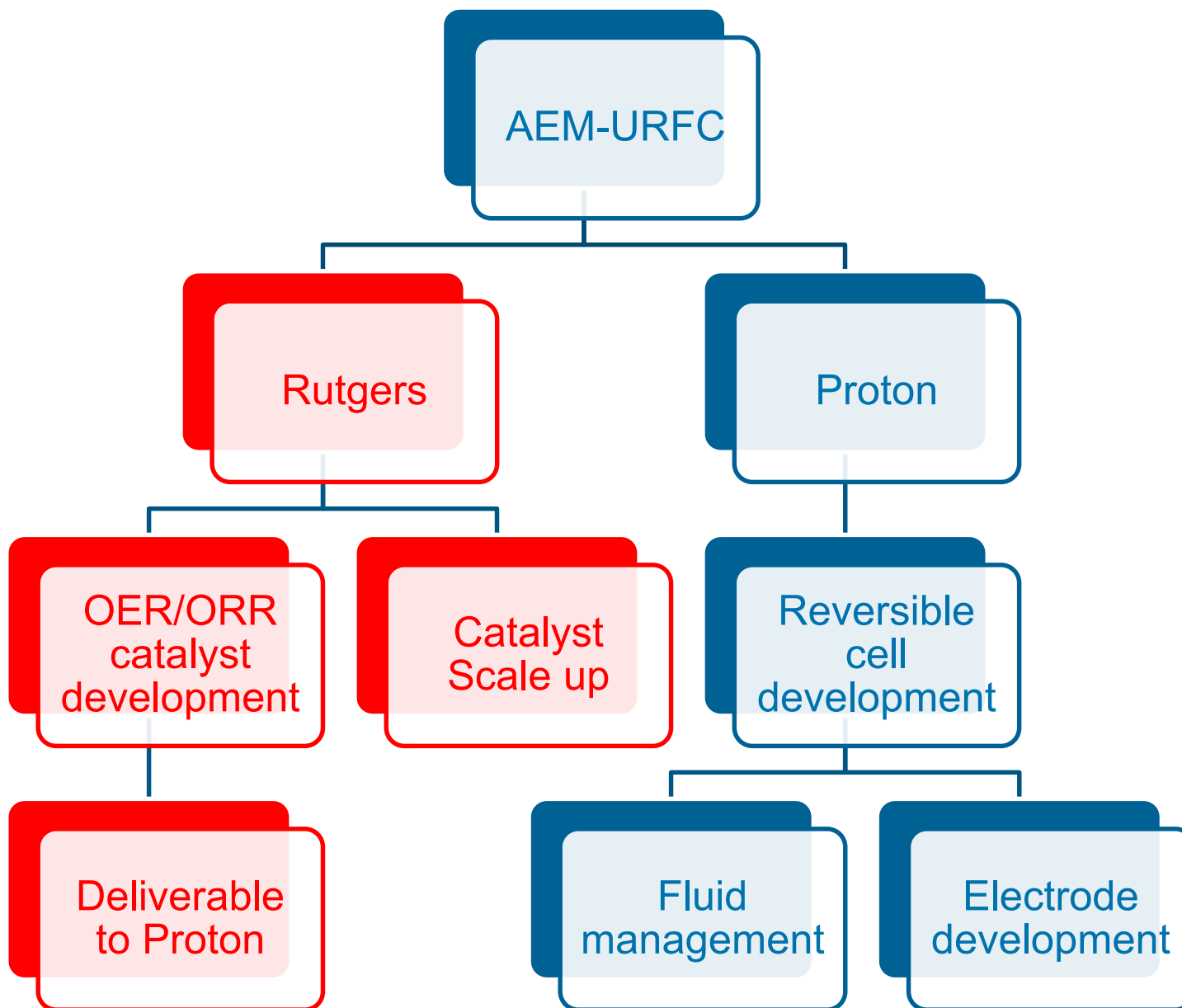
DRFC vs. URFC System Cost
1MW System, 1h:1h FC:Elct Timing
(1665 cm² FC & Elct cells)



Relevance: Project Objectives

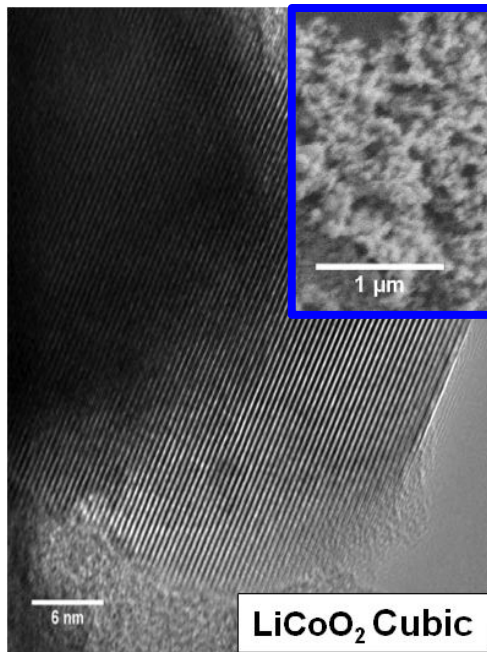
- Baseline AEM-URFC cell
 - Optimize flow fields and gas diffusion layers (GDL)
 - Optimize catalyst layers (O₂ and H₂)
- Develop non-PGM bifunctional oxygen catalyst
- Demonstrate feasibility
- Demonstrate cyclability (fuel cell ↔ electrolysis)
- Demonstrate stability
 - 200 hrs of run time

Approach

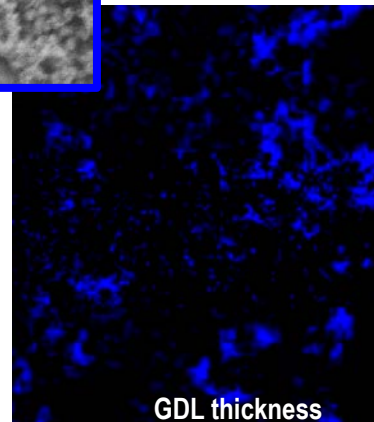
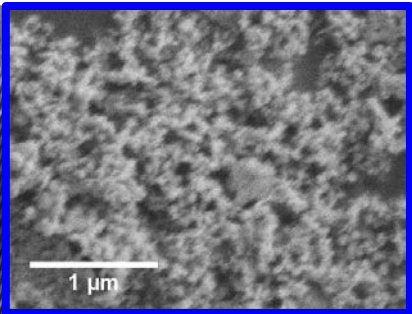


Approach

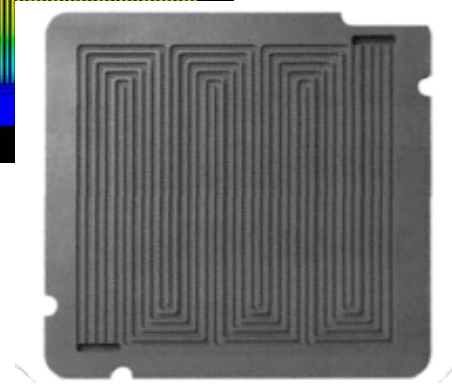
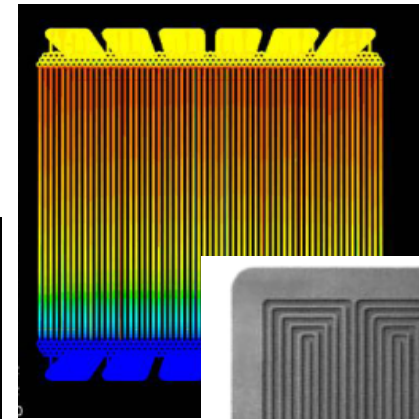
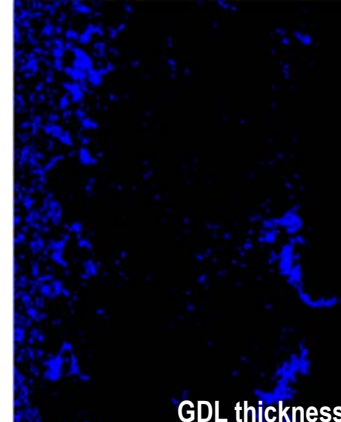
- Catalyst (Rutgers):
 - Based on cubic LiCoO_2
 - Tune OER/ORR activity by varying A and B site dopants
- AEM-URFC cell (Proton)
 - Water management
 - Flowfield
 - Wetproofing
 - Catalyst layer integration



Preliminary data on LiCoO_2



Water management optimization



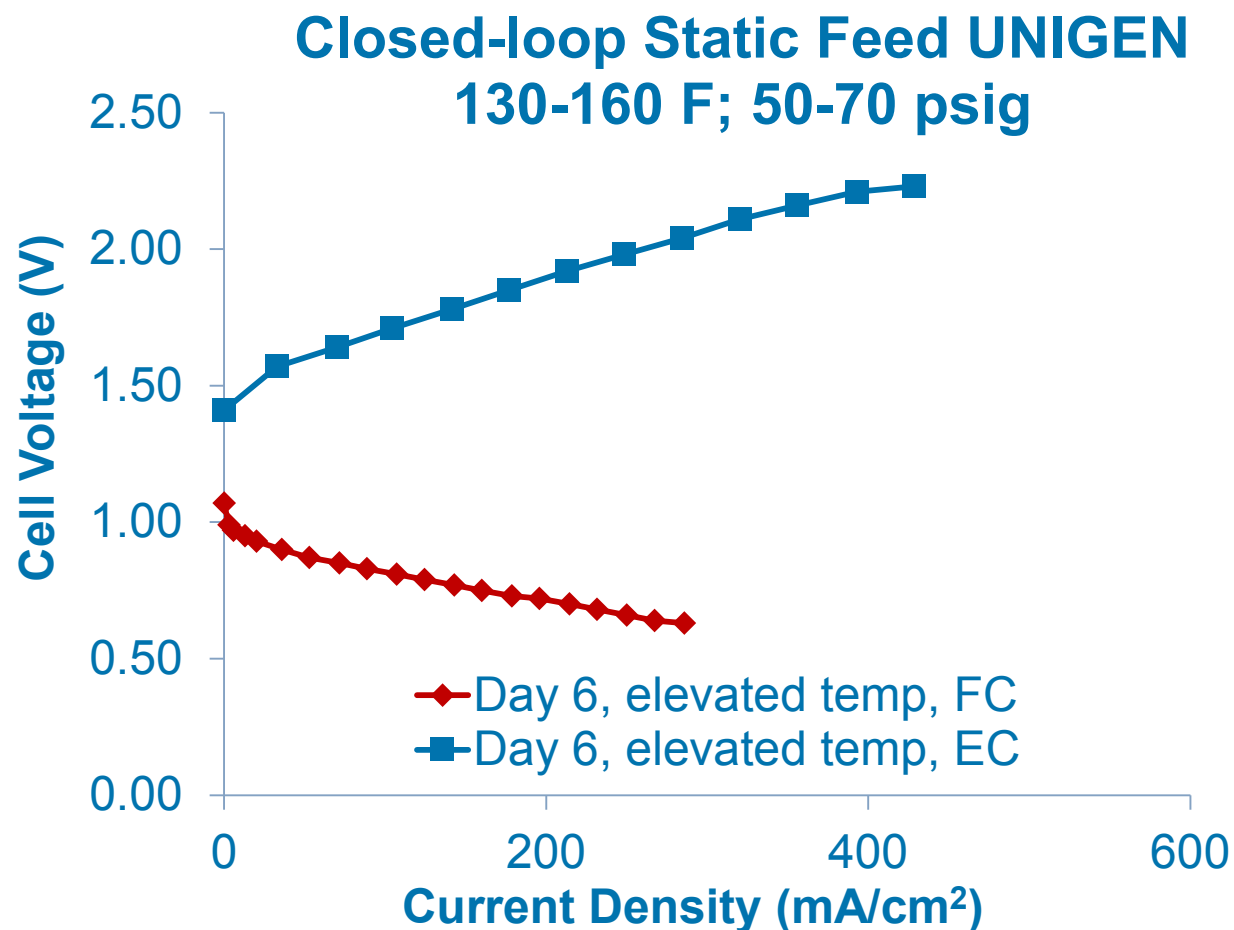
Flowfield Design

Approach: Leveraging Previous Work

- Leverage Proton PEM URFC experience from DARPA/NASA/NSF programs in AEM application:

- Flowfields
- Wetproofing
- OER/ORR catalyst philosophy
- Test stands

- Leverage AEM experience from ARPA-E and other programs



Objectives

| Task description and significance achievements | Completion |
|---|------------|
| Cubic phase $LiBCoO_2$ ($B=Mn^+$, etc) synthesized and screened | 25% |
| Electrochemical screening of synthesized materials in RDE | 25% |
| Development of URFC cell | 100% |
| Optimization of flowfields for fuel cell and electrolysis operation | 50% |
| Baselining PGM catalyst materials in fuel cell and electrolysis | 100% |
| Evaluation of non-PGM O_2 electrodes | 10% |
| Durability testing of non-PGM O_2 electrodes | 10% |

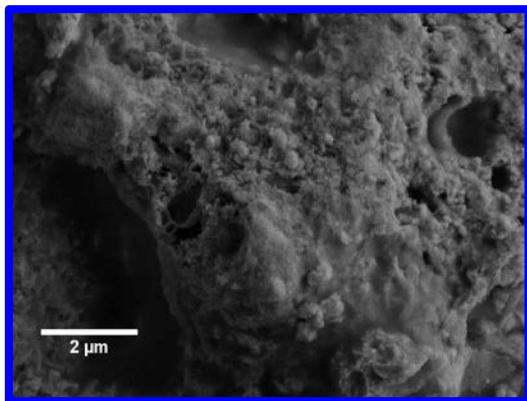
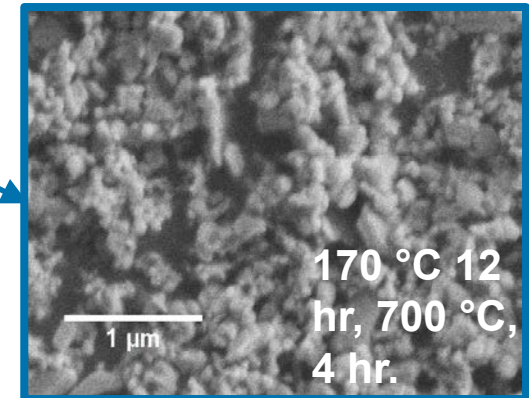
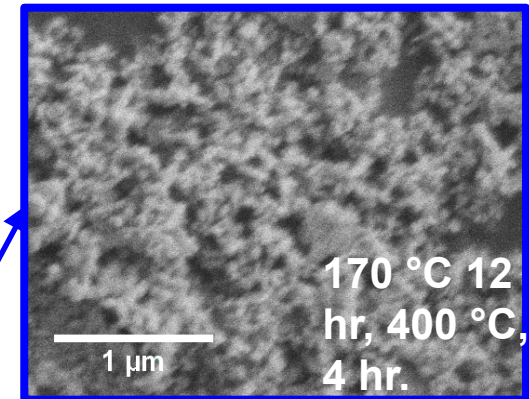
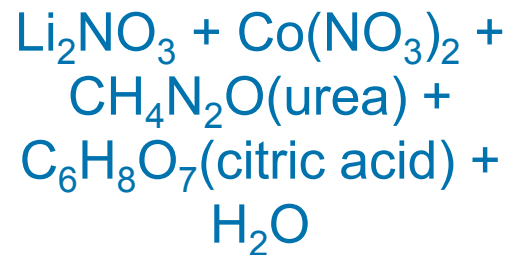
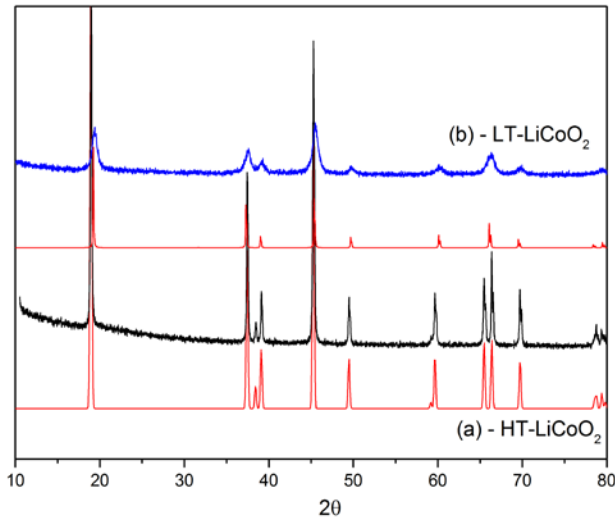
Technical Accomplishments

- **Catalyst Development**
 - Scaled up synthesis of LiCoO_2
 - Performance verified at Proton
 - Multiple B-site doped LiBCoO_2 (B=Mn...) synthesized and characterized by RDE
- **Cell Development**
 - Cell geometry and architecture defined for 25 cm² cells
 - Verified to function in fuel cell and electrolysis operation
 - Flowfield optimization and wet proofing initiated
- **URFC Testing**
 - Baseline performance obtained in fuel cell and electrolysis mode for Pt | Pt catalyst (PGM baseline)
 - Baseline electrolysis performance for LiCoO_2 and 600 hrs stability test completed

Technical Accomplishments: Synthesis

- Sol-gel synthesis employed for high phase purity and higher surface area catalysts

Sol-Gel Synthetic Routes

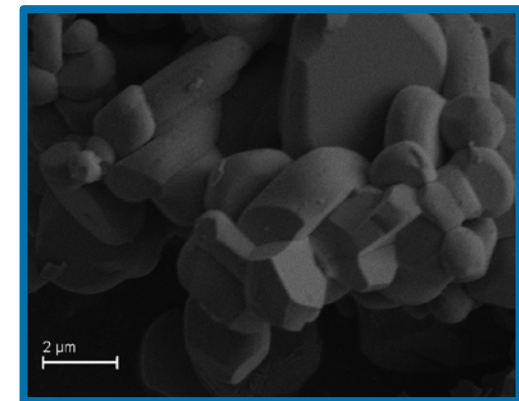


Solid State Synthesis



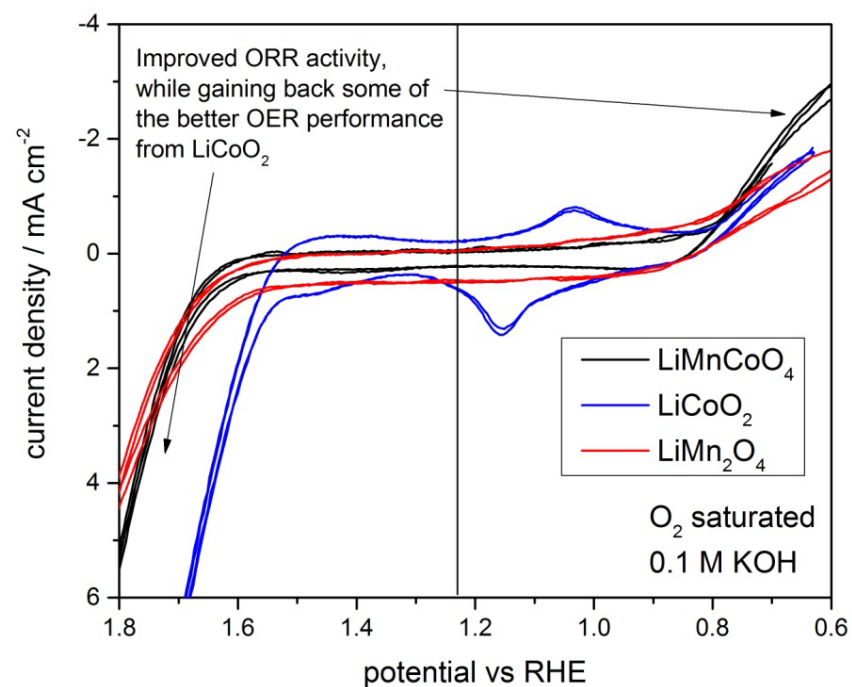
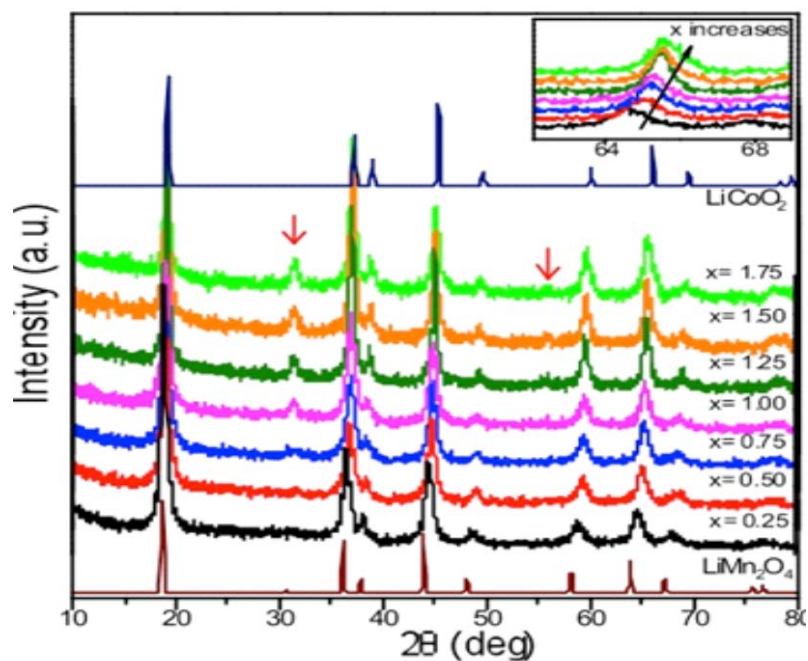
400 °C, 72 hr.

800 °C, 12 hr.



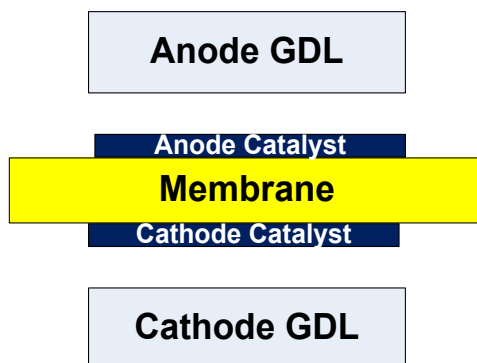
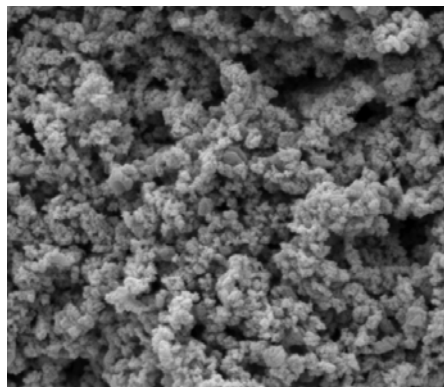
Technical Accomplishments: Non-PGM OER/ORR catalysts

- Synthesized well-defined non-PGM O₂ catalysts based on LiCoO₂ and LiMn₂O₄ families
 - Large batches by sol-gel method achieved high surface area
- Tuned OER and ORR activity by B site substitution
 - LiMn_{2-x}Co_xO₄ (0 < x < 1.5)

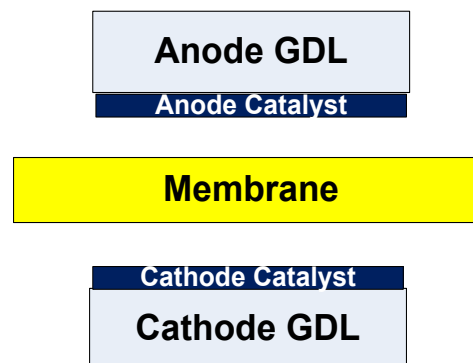


Technical Accomplishments: GDE Manufacture and Integration

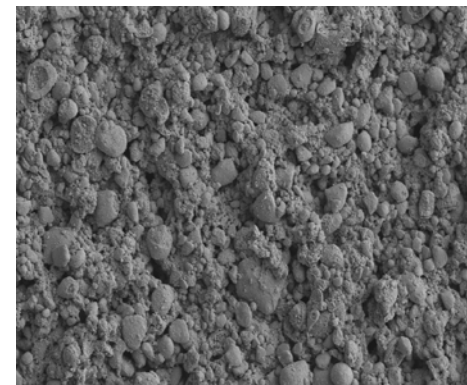
- Rutgers non-PGM materials integrated in GDE ink and sprayed to make electrodes for electrolysis testing
- CCM based approach pending



Catalyst coated
membrane (CCM)

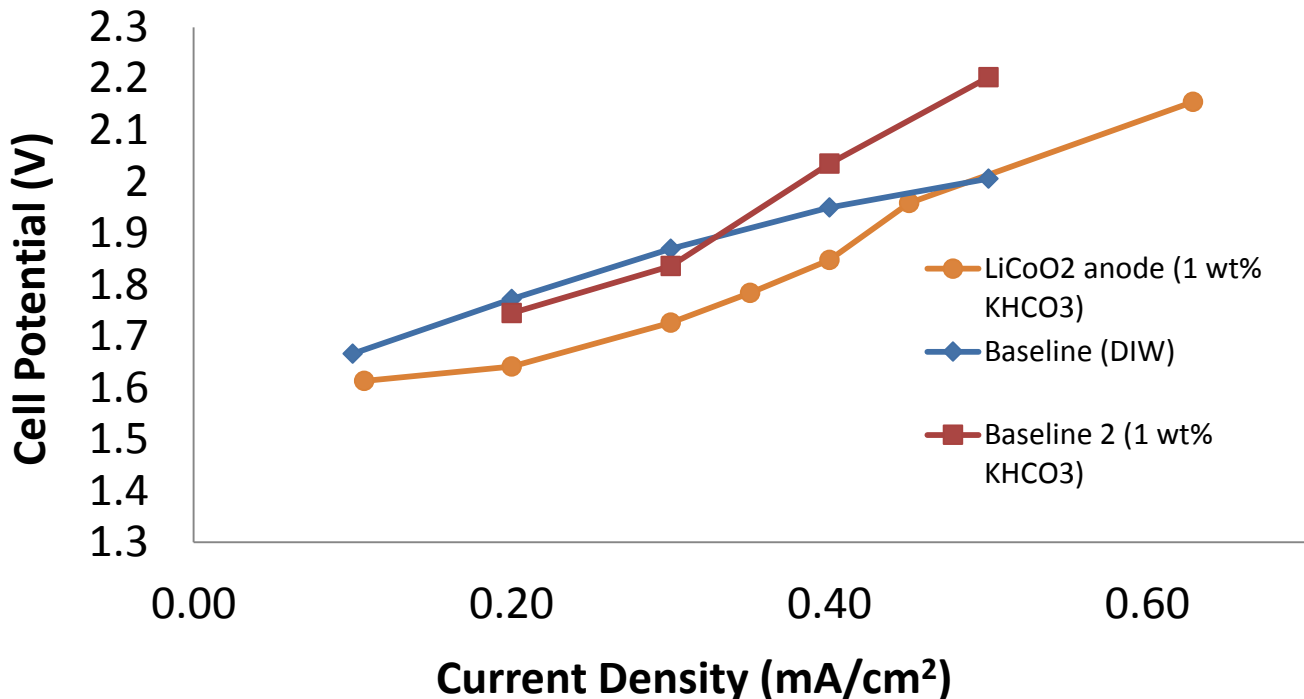


Gas diffusion
electrodes (GDE)



Technical Accomplishments: Non-PGM OER Performance Screening

AEMWE Polarization Curve 28cm² Stack 50°C

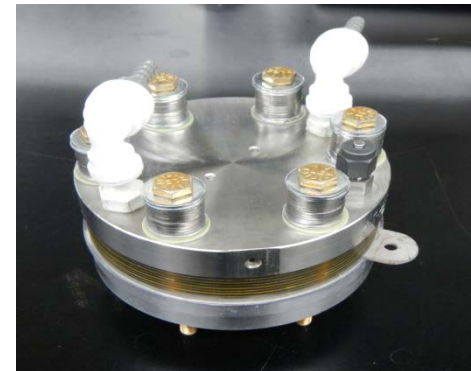
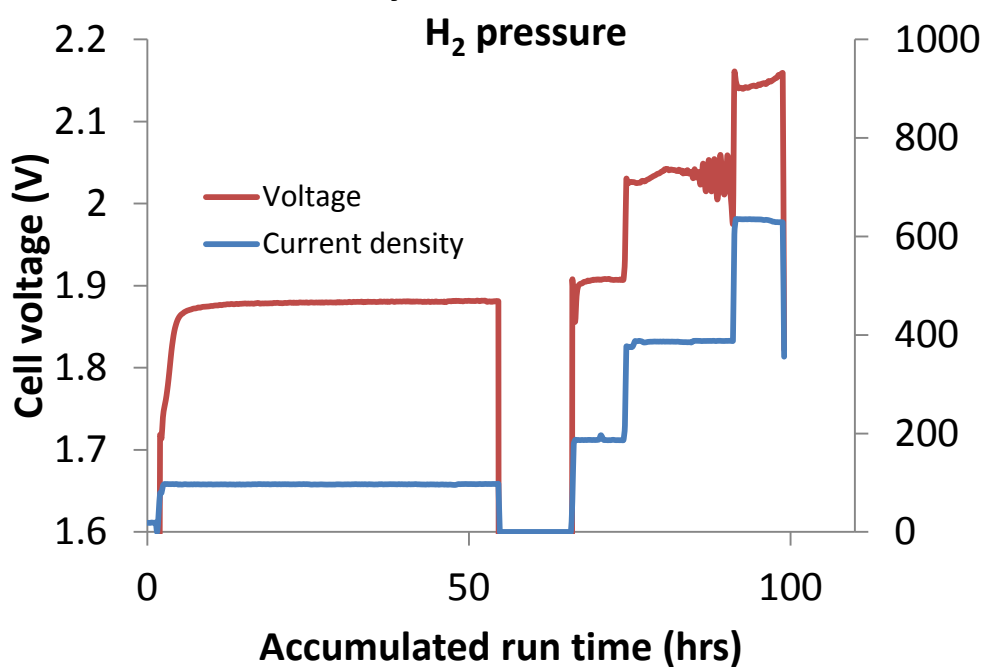


- Anode DI water or bicarbonate feed
- Equivalent Pt cathodes
- Improved performance over baseline anode catalyst

Technical Accomplishments

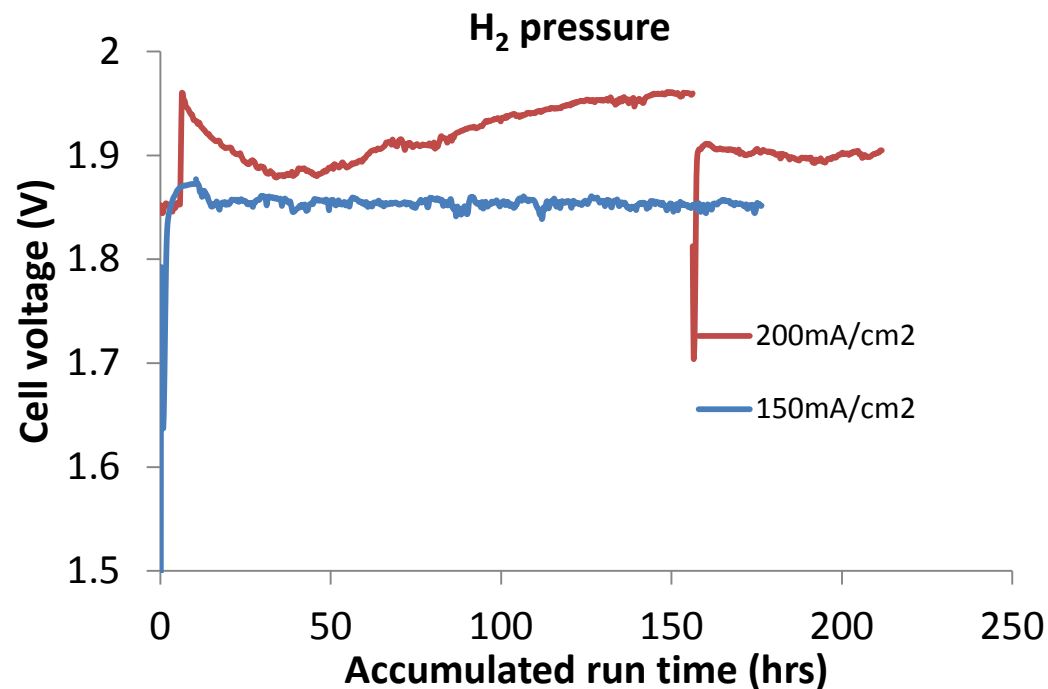
Non-PGM O₂ Catalyst Durability Test

AEMWE Stability test, 28cm² stack, 45°C, 45 PSI



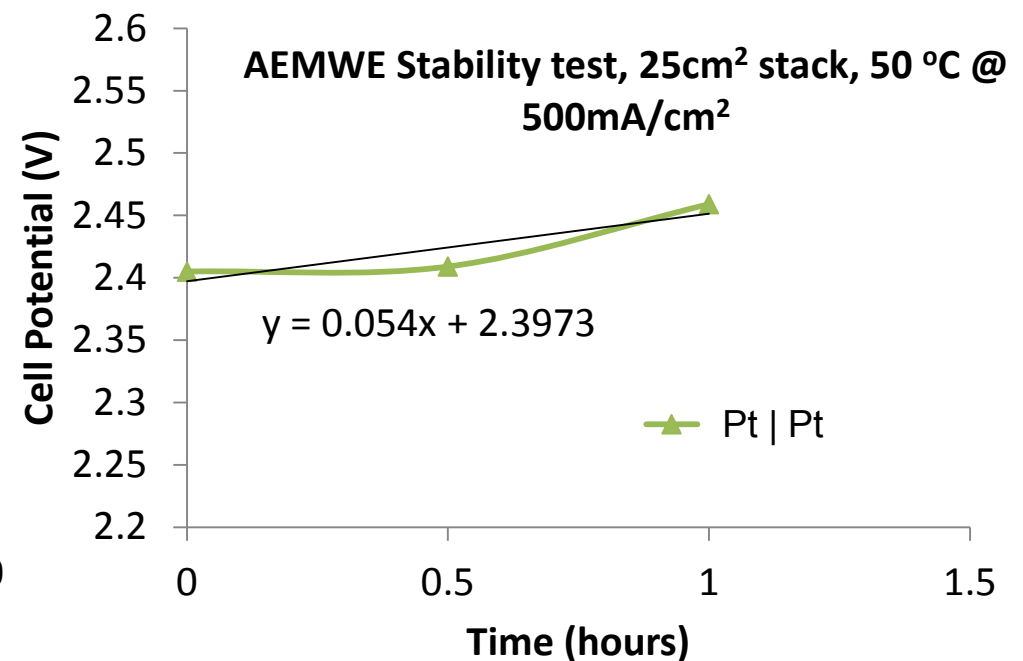
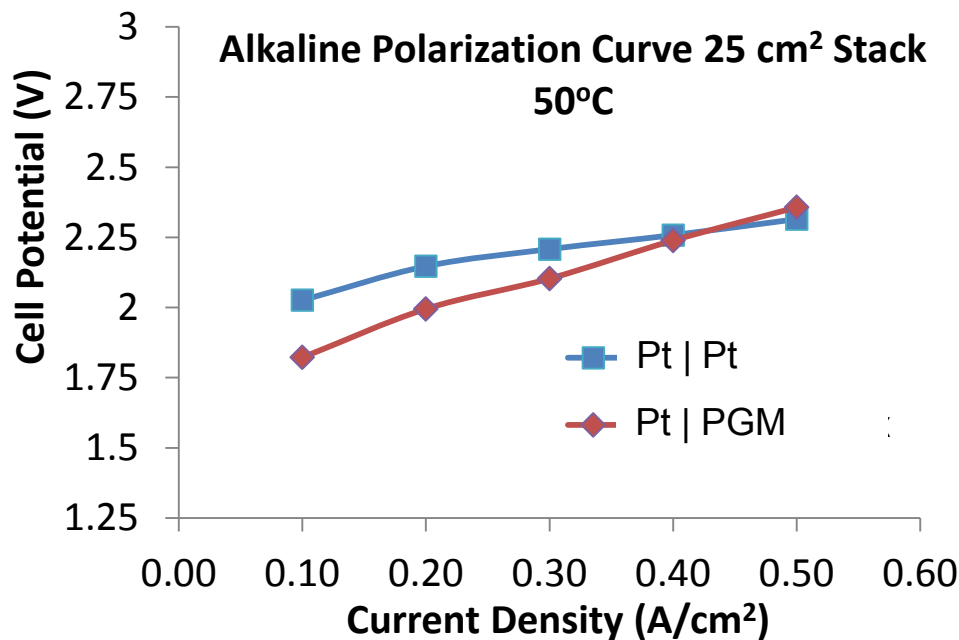
- 28cm² cell commercial platform
- Stainless steel and carbon BOP
- 1wt% KHCO₃ anode feed
- Cumulative run time of 550 hrs
- Apparent drift at high current densities

AEMWE Stability test, 28cm² stack, 45°C, 45 PSI

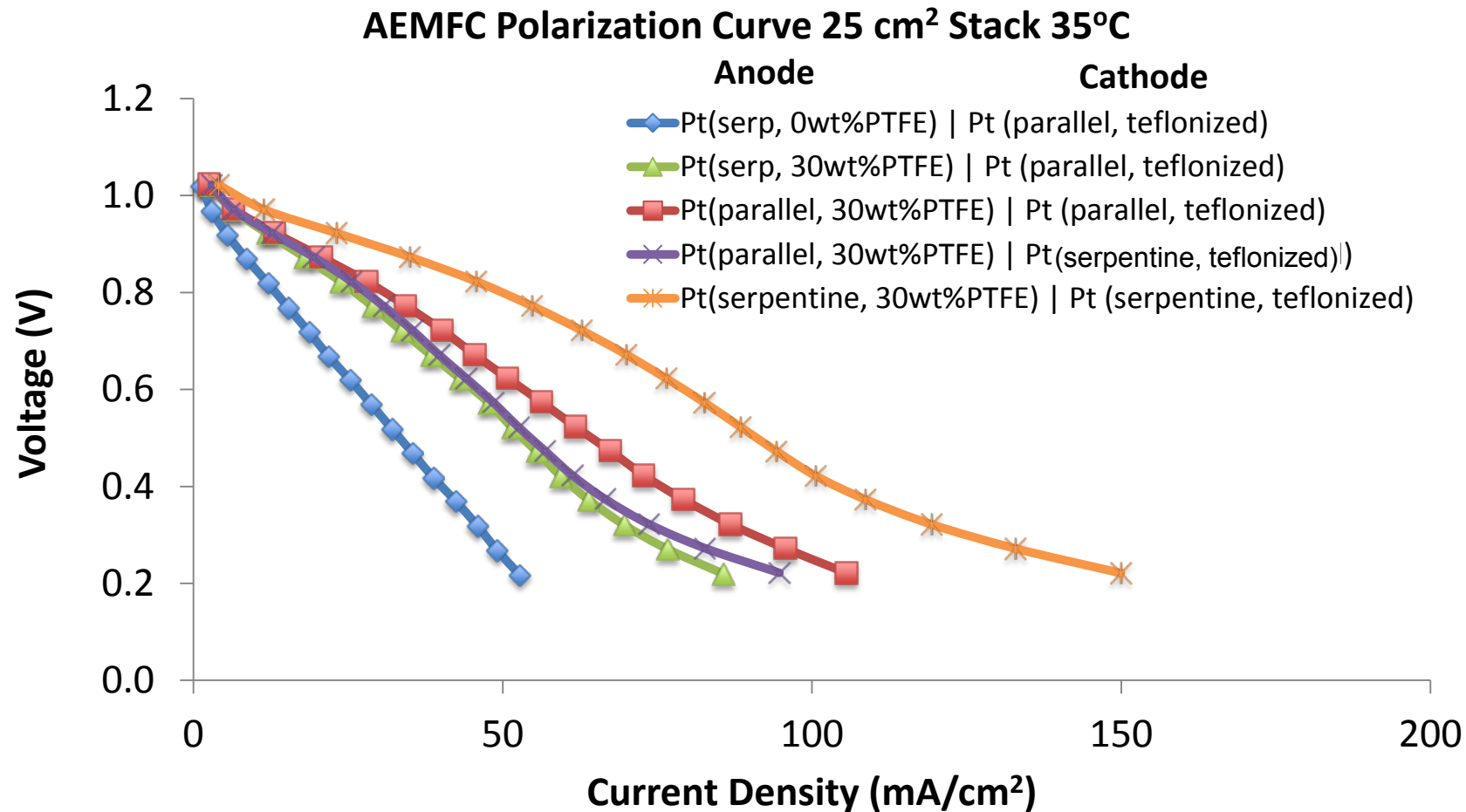


Technical Accomplishments: URFC cell baselining - Electrolysis

- 25cm² non-proprietary cell platform
- Deionized water feed on the anode side (O₂ electrode)
- Baseline vs conventional PGM anode catalyst
- Little difference at higher current densities points to other rate limiting steps



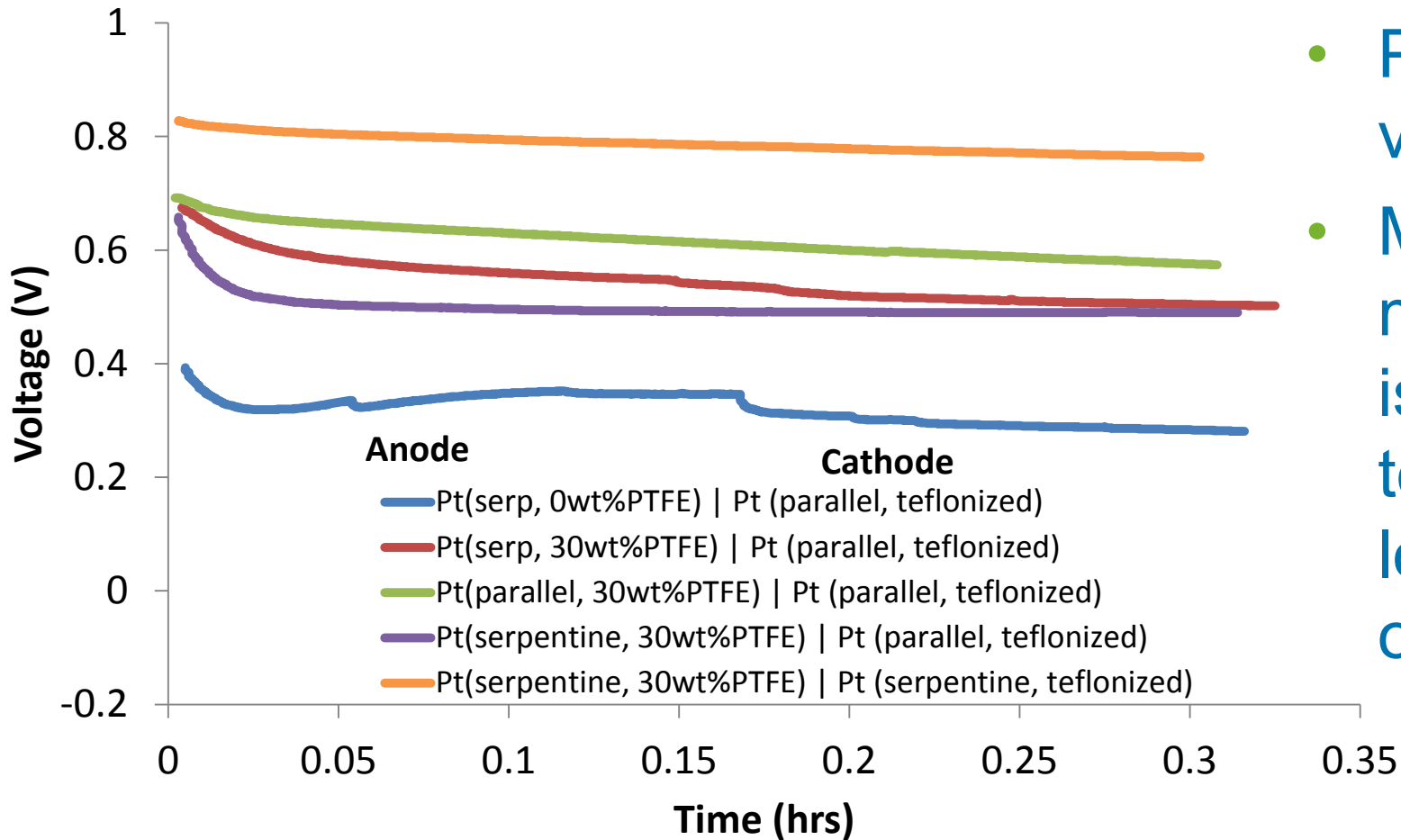
Technical Accomplishments: URFC cell baselining – Fuel Cell



- 25 cm² non-proprietary cell platform
- Underhumidified H₂, overhumidified O₂: high flow rates

Technical Accomplishments: URFC cell baselining – Fuel Cell

AEMFC Stability test, 25cm² stack, 35 °C @ 50mA/cm²



- Performance vs. stability
- May have water management issues - need to resolve for longer term operation

Future Work

- **Balance of Phase I:**
 - Test non-PGM Rutgers catalyst in URFC
 - Stability and cyclability data
 - Investigate CCM based approach
 - Incorporate advanced H₂ electrode catalyst
 - Investigate alternative membranes
- **Proposed work for Phase II:**
 - Development of 28cm² URFC platform
 - Multi cell stack
 - Scale up fabrication of non-PGM catalyst materials
 - Long term cycling and stability performance

Collaborations

- Rutgers University
 - Synthesis of ~ 2 gram batches of non-PGM oxygen catalysts
 - Cubic LiCoO_2 and spinel LiMn_2O_4
 - B site dopants (transition metal cations)
 - N doping into O site
 - OER/ORR activity and stability screening with RDE in near neutral, NaOH (pH 14) and potassium bicarbonate
 - Supplemental characterization

Summary

- **Relevance:** Demonstrates non-PGM AEM based URFC for reduced capital cost system and higher market penetration
- **Approach:** Optimize cell design and non-PGM catalyst activity for fuel cell and electrolysis operation with an anion exchange membrane
- **Technical Accomplishments:**
 - >500 hour durability test successfully completed for non-PGM electrolysis anode GDE
 - Baseline PGM feasibility demonstrated in 25 cm² test cell in both electrolysis and fuel cell operation
- **Collaborations:**
 - Rutgers University: non-PGM catalyst synthesis and screening
- **Proposed Future Work:**
 - Test non-PGM Rutgers catalyst in URFC
 - Investigate CCM based approach
 - Incorporate advanced H₂ electrode catalyst
 - Incorporate membrane improvements