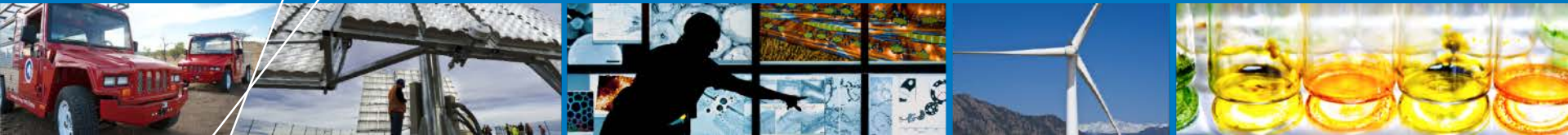


# 2015 DOE Hydrogen and Fuel Cells Program Review



## Renewable Electrolysis Integrated System Development & Testing

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June 11, 2015

Project ID: PD031

### \*Presenter

This presentation does not contain any proprietary, confidential, or otherwise restricted information

# Overview

## Timeline

Project start date: Sep. 2003

Project end date: Oct. 2015\*

## Budget

FY13 DOE Funding: \$460k

FY14 DOE Funding: Forward funded with  
FY13 funds

FY15 DOE Planned Funding: \$200k

Total Project Value: \$5,900k

## Barriers

G. System Efficiency

I. Grid Electricity Emissions (Distributed)

J. Renewable Electricity Generation  
Integration (Central)

L. Operations and Maintenance

## Partners

Xcel Energy (CRADA)

Proton OnSite

Giner Inc.

\* Project continuation and direction determined annually by DOE

# Relevance

- Hydrogen is a storage fuel enabling higher penetrations of renewable electricity sources
- Electrolyzer systems are rapidly increasing in size and are able to provide:
  - Renewable hydrogen for a near-zero carbon transportation fuel
  - Utility grid services and stabilization

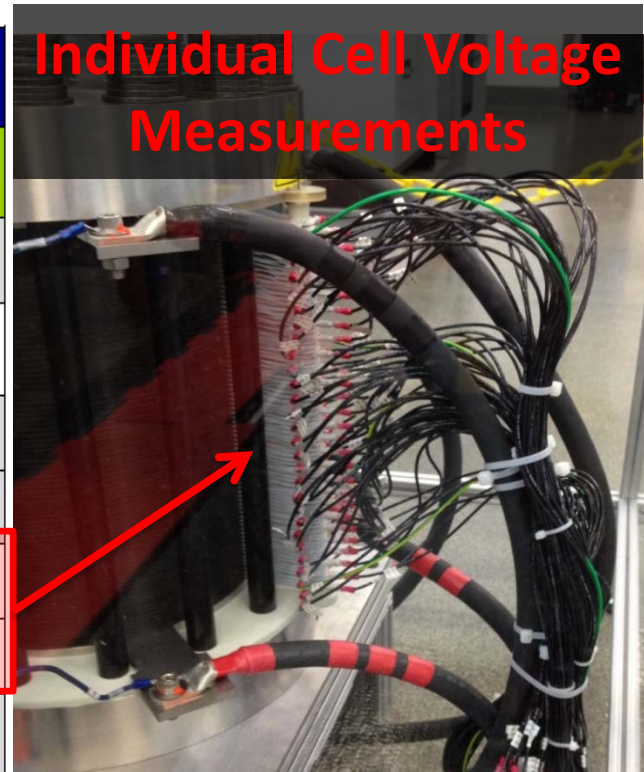


# Impact

- As electrolyzer systems size increase there is a need to validate large active area stacks to meet DOE targets
- System efficiency under varying power operation (e.g., solar, wind) needs to be optimized to account for the intermittency of renewable energy sources

**Table 3.1.4 Technical Targets: Distributed Forecourt Water Electrolysis Hydrogen Production<sup>a, b, c</sup>**

Characteristics	Units	2011 Status	2015 Target	2020 Target
Hydrogen Levelized Cost <sup>d</sup> (Production Only)	\$/kg	4.20 <sup>d</sup>	3.90 <sup>d</sup>	2.30 <sup>d</sup>
Electrolyzer System Capital Cost	\$/kg	0.70	0.50	0.50
	\$/kW	430 <sup>e, f</sup>	300 <sup>f</sup>	300 <sup>f</sup>
System Energy Efficiency <sup>g</sup>	% (LHV)	67	72	75
	kWh/kg	50	46	44
Stack Energy Efficiency <sup>h</sup>	% (LHV)	74	76	77
	kWh/kg	45	44	43
Electricity Price	\$/kWh	From AEO 2009 <sup>i</sup>	From AEO 2009 <sup>i</sup>	0.037 <sup>j</sup>



# Approach

- Provide independent performance testing of advanced electrolyzer stacks and systems for DOE and Industry
- Develop and optimize electrolyzer stack and sub-system performance using grid and renewable power systems
- Leverage large active area stack testing platform and balance of plant to develop system efficiency improvements

## Collaborate with other NREL projects and industry

- INTEGRATE project TV030 provided electrolyzer stack test bed and hydrogen dryer
- Quality results collected as part of 700 bar station operation
- Giner Inc. provided test stack to commission stack test bed



# Approach

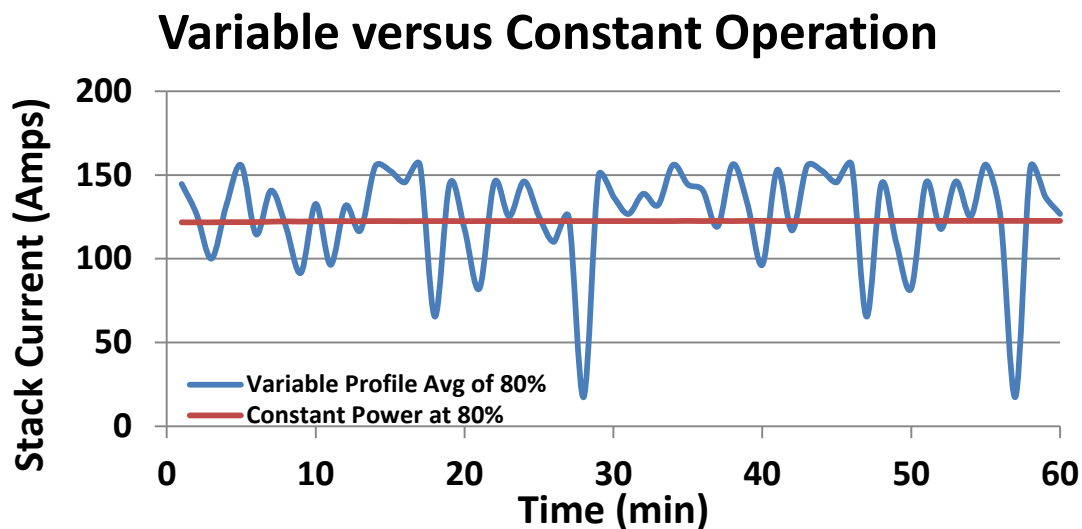
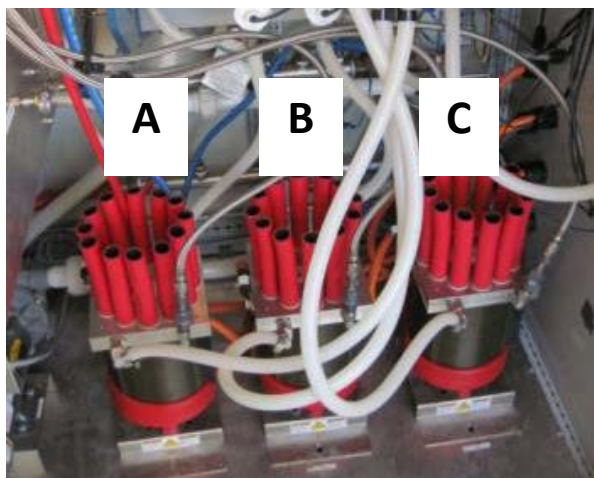
Milestone Description	Type	Due Date
Provide comparison of four different drying technologies, focusing on efficiency, capital cost and O&M cost of the different techniques. If there is a technique that has not been tested but shows promise in the Q1 detailed analyses, the technique may be designed, procured, implemented and tested.	Qtr Progress Measure (Regular)	31-Dec-14
Install and begin testing large active area stack drying system, comparing fixed flow versus variable flow desiccant drying systems. Confirm drying system removes moisture content below 5 parts per million of water in hydrogen (as per SAE J2719) for PEM stacks capable of hydrogen production in the 65+ kg/day range.	Qtr Progress Measure (Regular)	31-Mar-15
Collect 40 hours each on 3 different pressure swing adsorption drying techniques comparing the fixed flow (orifice) approach with two new linear actuated valves (variable flow) that vary in performance and price.	Annual Milestone (Regular)	30-Jun-15
Complete cumulative testing of 7500 h for two PEM electrolyzer stacks and 4500 h for a new stack under constant- and variable-powered operating conditions and compare stack decay rates of the two operational modes with results from FY14.	Qtr Progress Measure (Regular)	30-Sep-15



# Technical Accomplishment

## Compare Stack Lifetime: Wind vs. Constant Power Operation

- **Goal:** Analyze stack decay differences between constant- and variable-powered stack operation
  - Three 10 kW stacks under test
  - ~5,500 hour operation completed
- Proton Onsite (H-Series) – 40 kW, 13 kg/day PEM electrolyzer
- Instrumented electrolyzer and took control of AC/DC power supplies to operate stacks in variable power mode



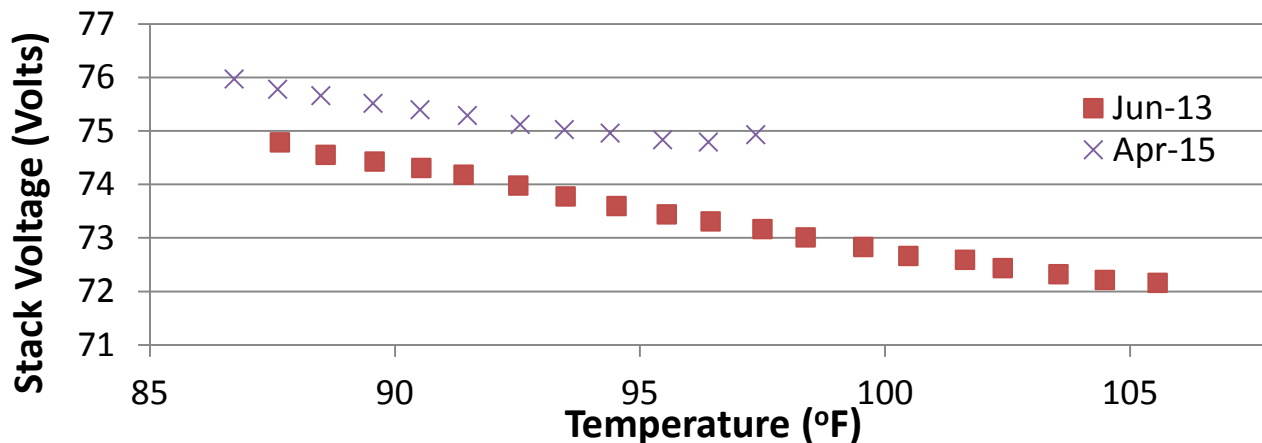
# Technical Accomplishment

## Long Duration Variable Stack Testing

- Stack A & B reached 5,500 hours of operation, newer stack C reached 2,500 hours of operation
- Stack decay rate calculated by running the stacks at steady-state (~155 Amps) and separating into temperature and voltage bins
- Voltage comparison of the three stacks at 104 °F is used to determine stack decay rate

Operating Mode	Stack Identifier	Decay Rate ( $\mu\text{V}/\text{cell-h}$ )
Variable Power	Stack A	11.5
Constant Power	Stack B	12.6
Constant Power	Stack C	21.6

Example of Sorted Steady-state Data





# NREL Electrolyzer Stack Test Bed

## Located at NREL's Energy System Integration Laboratory

- AC-DC power supplies capable of 2,000 ADC and 250 VDC
- Built as a collaboration with the INTEGRATE project

## System efficiency improvements in electrolyzer balance of plant

Goal is to improve system efficiency;

- Drying losses in variable operation with NREL's variable flow drying technique
  - NREL designed and Proton built research drying skid
- Optimize balance of plant based on variable stack power

## First testing completed with Giner Inc.

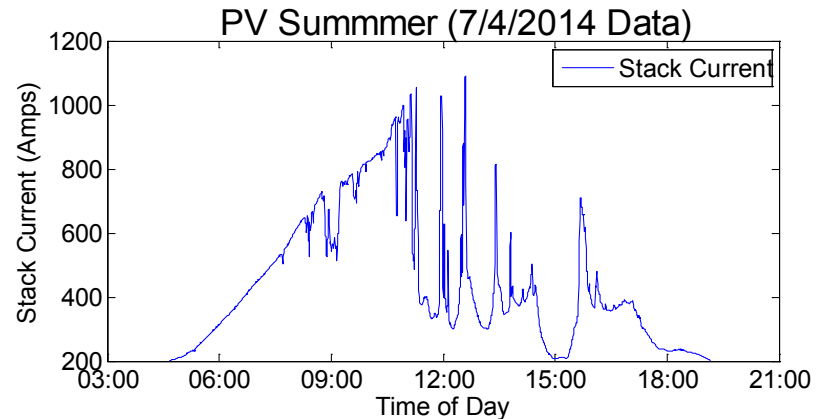
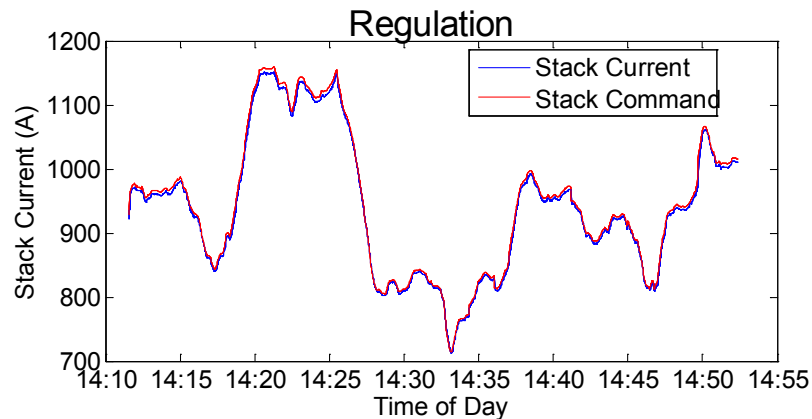
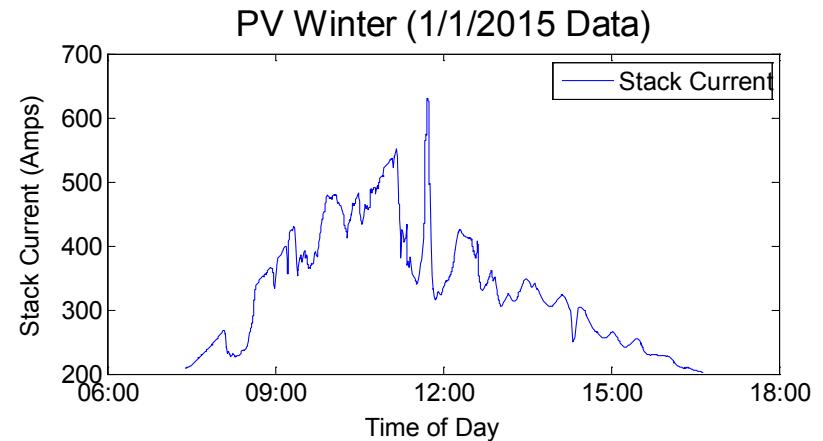
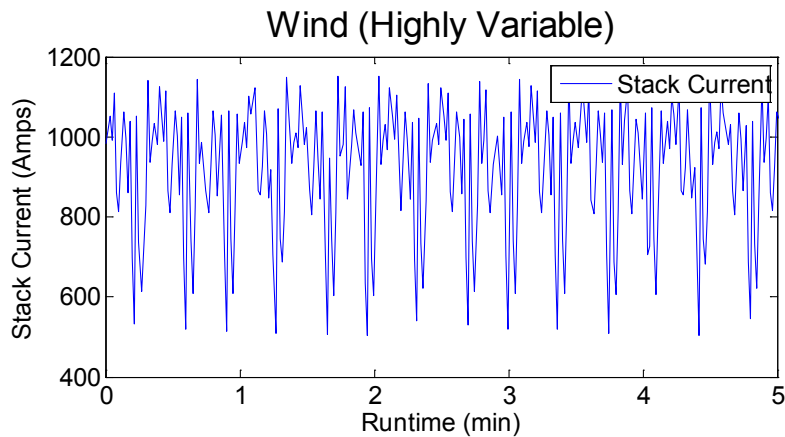
- Three 150 kW PEM stacks
- IV-Curves were collected at stack temperature of 70 °C
- Individual cell voltages were collected at different current and stack pressure levels



# Technical Accomplishments

## Ability to program profiles into the stack test bed

- Examples of renewable and regulation profiles
- Ran profiles with 120 kW stack from Proton



# Technical Accomplishments

## Large active area stack testing and hydrogen dryer improvements

- **Challenge:** Traditional  $H_2$  drying systems are designed to operate at full power with a fixed amount of  $H_2$  lost regardless of operating conditions
- **Goal:** Improve electrolyzer efficiency by optimizing electrolyzer balance of plant operation under variable conditions
- **Approach:** Reduce  $H_2$  drying losses in pressure swing adsorption dryers to less than 3.5% of flow using variable flow approach
- Testing aims to confirm  $H_2$  quality is not compromised with real time monitoring of water content in the  $H_2$





# Technical Accomplishments

## Measuring Dryer Performance

- Dew point sensors on outlet of dryer are used to track parts per million by volume (ppmv) of H<sub>2</sub>O in the H<sub>2</sub>
- SAE J2719 fuel quality standard is mandatory target, < 5 ppmv
- Dew point sensors are known to have issues during operation. Solutions to overcome dew point sensor challenges:
  - **Challenges:** Dew point sensors having erratic behavior, Dew point sensors drift over time
  - **Solutions:** Install multiple dew point sensors, filter data when needed, N<sub>2</sub> purge system to sweep any contaminants off of the sensors when needed

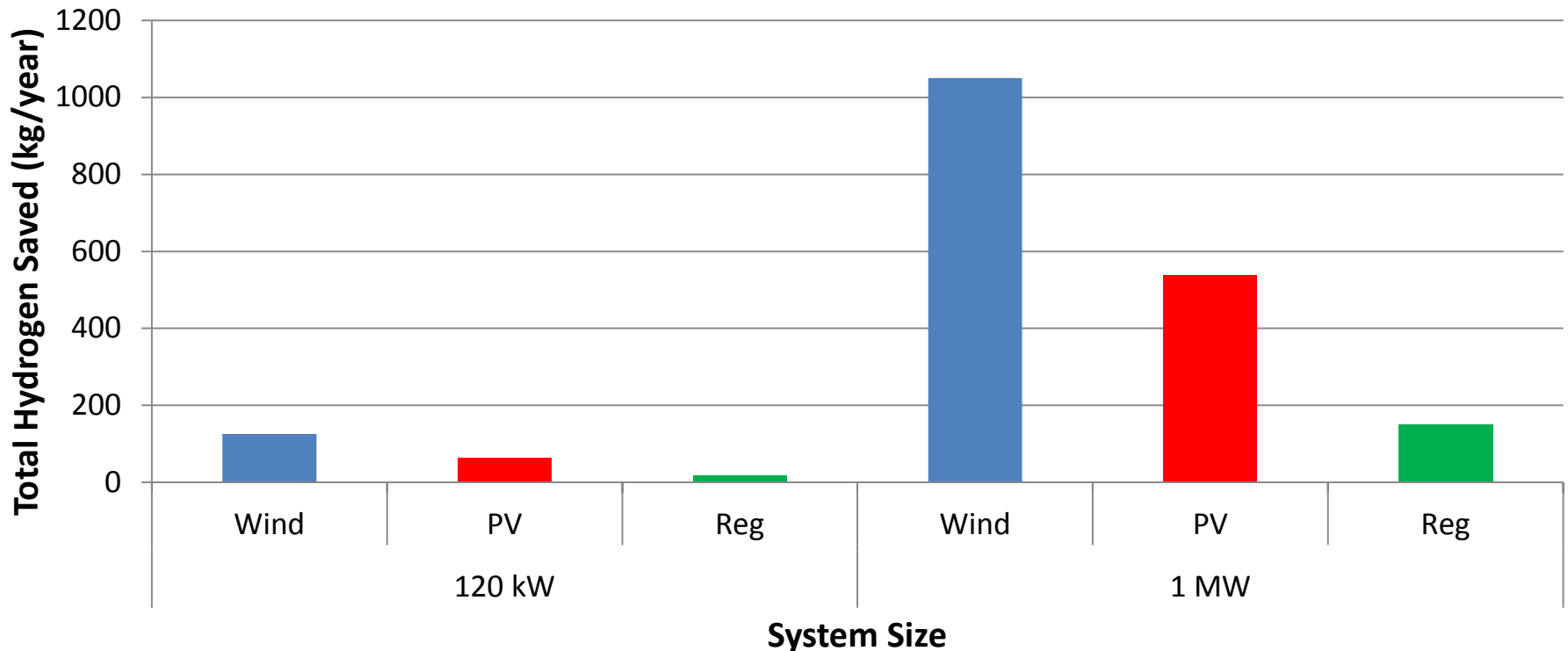


# Technical Accomplishments

## Hydrogen savings with variable flow

- Preliminary analysis of why these savings are important
- Systems are growing in size, real savings happen as larger systems come online

### Hydrogen Saved per Year with Variable Flow Approach





# Collaborations

## Formal

### Giner Inc.

- Work for Others
- Tested (3) 150 kW stacks

### Xcel Energy (CRADA)

- Wind-to-Hydrogen demonstration project since 2005

## Internal to NREL

### 700 bar hydrogen station

- Quality results

### INTEGRATE

- Large active area stack test bed
- H<sub>2</sub> drying system

# Future Work

- Finalize testing and report on on-going dryer testing to optimize drying losses
- Continue long duration testing comparing stack decay rates for variable power operation and constant power operation
- Find other opportunities to use the electrolyzer balance of plant to improve system efficiency
  - Capturing heat to warm up H<sub>2</sub> sweeping gas to lose less H<sub>2</sub> in drying
  - Using cooling system and H<sub>2</sub>O drop outs to improve dryer efficiency

# Responses to Previous Year Reviewers' Comments

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- This project was not reviewed last year

# Summary

**Relevance:** Goals consistent with reducing capital cost, improving stack and system efficiency and integrating systems with renewable energy sources

**Approach:** Develop and demonstrate advanced controls, novel sub-systems, system-level improvements and integrate with renewable energy sources to reduce the cost of hydrogen

## **Technical Accomplishments:**

- Reached 5,500 hours of operation on (3) 10 kW stacks to analyze stack decay differences between constant- and variable-powered stack operation
  - Stacks showed a decay rate of 11 - 22  $\mu\text{V}/\text{cell-h}$
- Collaborated with INTEGRATE to build electrolyzer stack test bed
- Purchased, installed, commissioned and began testing H<sub>2</sub> variable dryer concept
  - Installed linear valves and orifice in parallel paths for testing
  - Solved dew point challenges

## **Collaborations:**

- Giner Inc. - Large active area stack testing
- Internal - 700 bar station, INTEGRATE

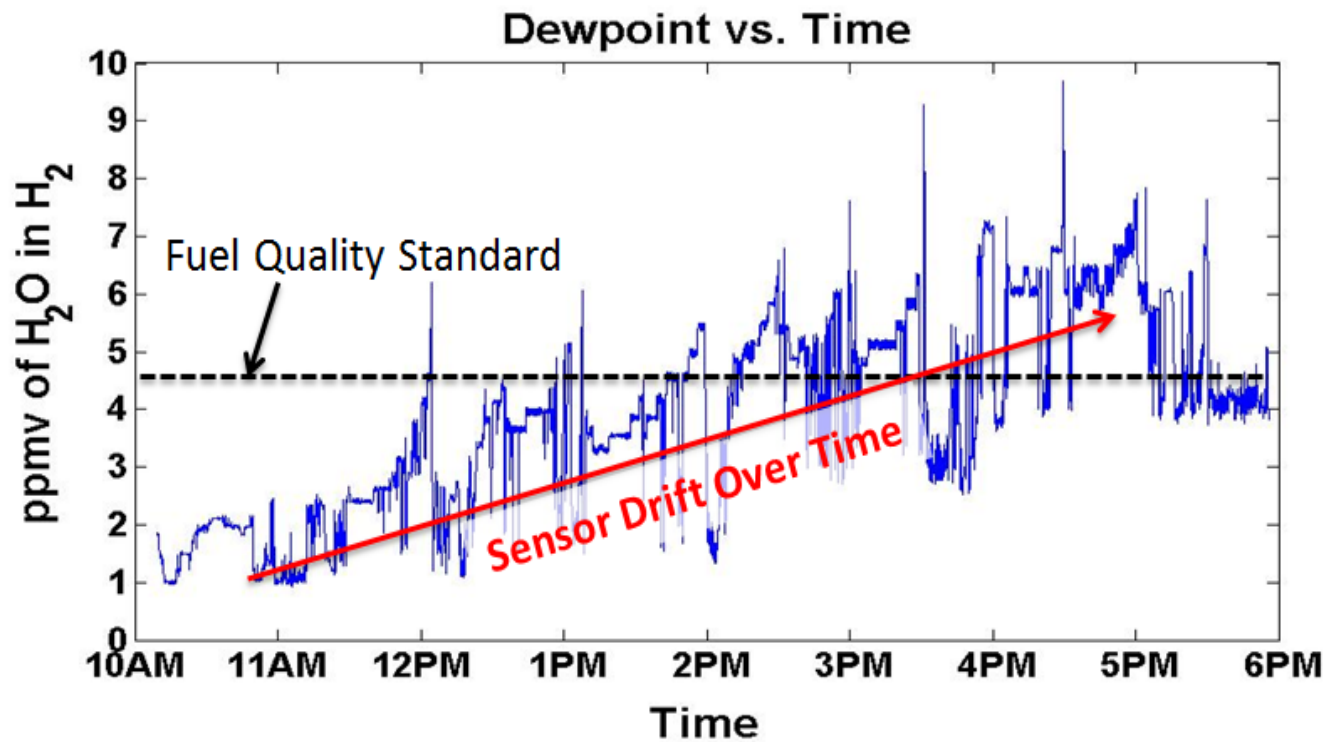
## **Proposed Future Research:**

- Finalize testing and report on on-going dryer testing to optimize drying losses
- Continue long duration testing comparing stack decay rates for variable power operation and constant power operation
- Find other opportunities to use the electrolyzer balance of plant to improve system efficiency

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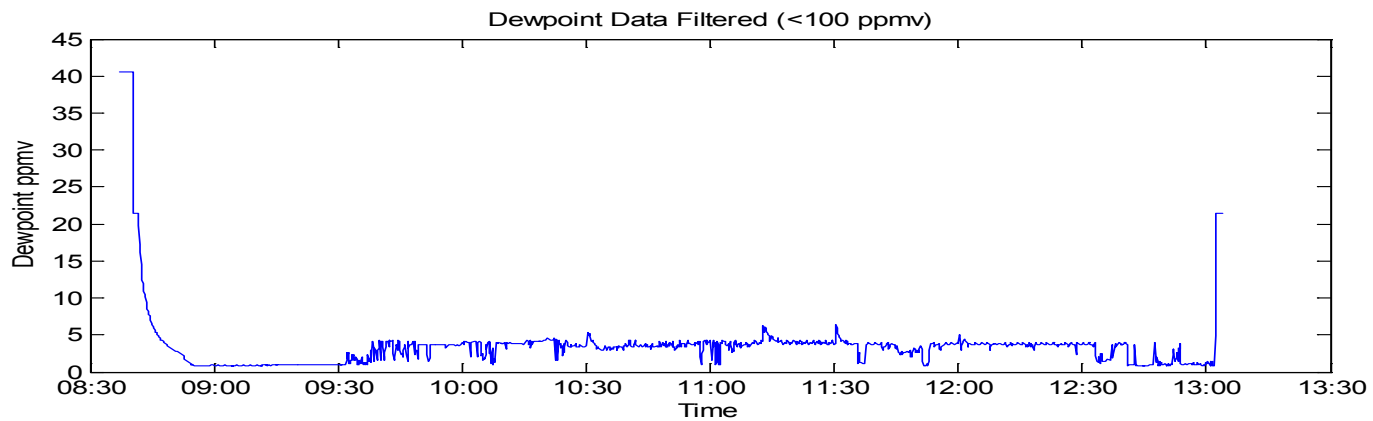
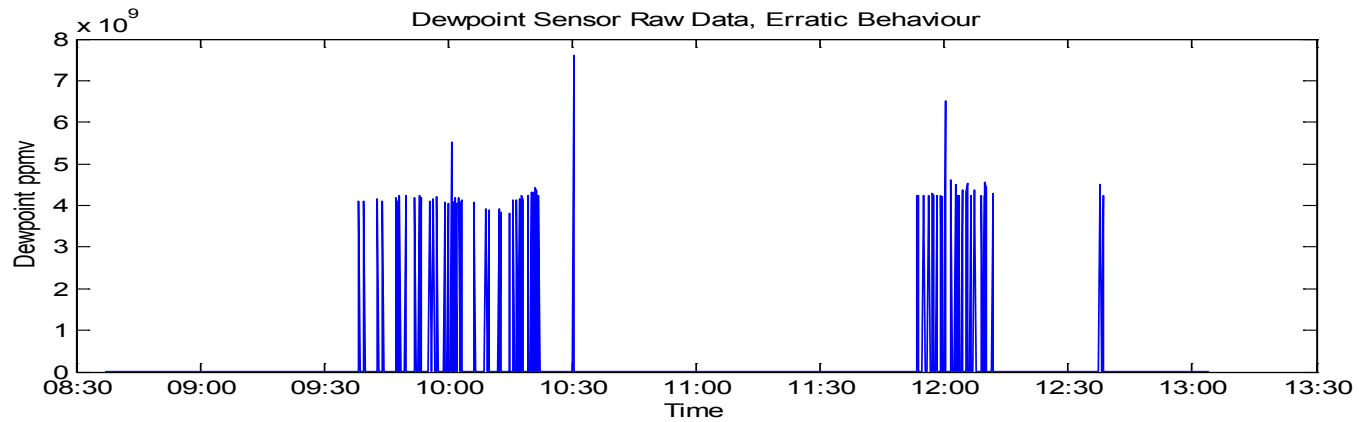
# Technical Backup Slides

# Dew Point Sensor Drift Over Time





# Dew Point Sensor Erratic Behavior

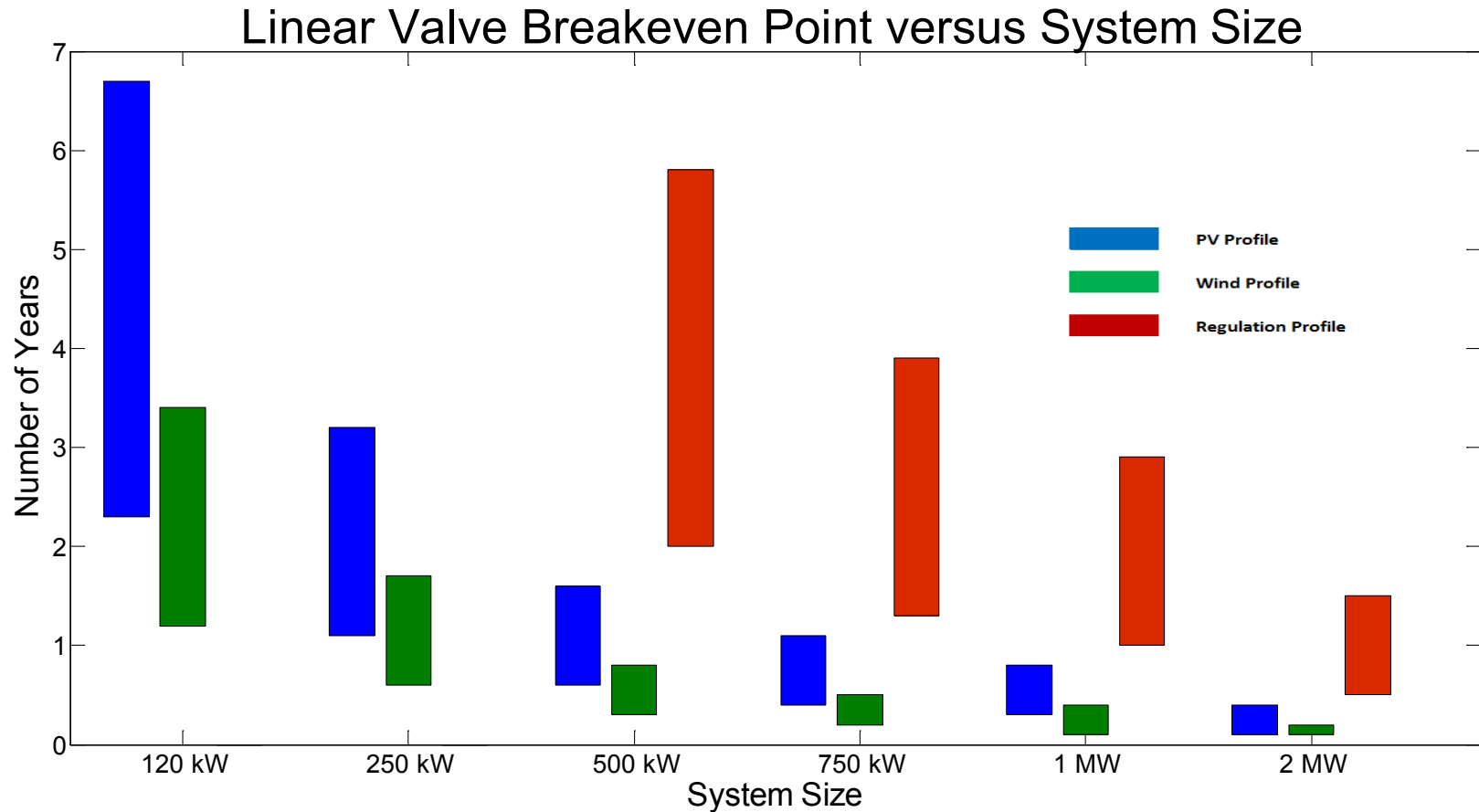


# Hydrogen Savings Analysis Details

## Assumptions

- Estimates on installing/implementing one linear actuated valve on one system based on experience. Cost would go down as more valves are implemented and controls are duplicated
- Price of H<sub>2</sub> 6 – 10 \$/kg
- Valve Costs Hardware:
  - Valve, Linear Actuator
- Valve Costs Labor:
  - Installation, Controls

# Linear Valve Breakeven



# Technical Accomplishments

## Dryer Characteristics

- Calculated flow based on stack current for the 120 kW stack from Proton
  - 52 kg/day
- Initial drying losses calculated at
  - 9 – 11 kg/day
  - 17 – 21% of H<sub>2</sub> lost
- Drying system designed for 135 kg/day
  - 6 – 8 % of H<sub>2</sub> lost theoretically
- Added control valve on vent line to reduce losses to < 10% at full operation

