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# **CORROSION-RESISTANT NON-CARBON ELECTROCATALYST SUPPORTS FOR PEFCs**

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**Illinois Institute of Technology**

**Date: 6/7/2016**

**Project ID # FC145**

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## Timeline and budget

### Competitively selected project

- **Project start date:** 03/01/16\*
- **Project end date:** 02/28/19
- **Total project budget:** \$ 3,397,431
  - **Total recipient share:** \$ 397,431
  - **Total federal share:** \$ 3,000,000
  - **Total DOE funds spent\*\*:** < \$ 50,000

### Partners

- Project lead: **IIT, Chicago**
- Partners (sub-contractors):
  - **Nissan Technical Center, North America**
  - **University of New Mexico**

\* Official date of contract from DOE. Issue of sub-contracts were finalized on April 15<sup>th</sup> 2016. Kick-off meeting held on April 21<sup>st</sup> 2016

\*\* As of 3/31/16

## Barriers and DOE target

- Barriers to be addressed:
  - Durability
  - Performance
- Technical targets:

	Units	2020 Target
Loss in catalytic (mass) activity <sup>a,b</sup>	% loss	<40
Loss in performance at 0.8 A/cm <sup>2</sup> <sup>a</sup>	mV	30
Loss in performance at 1.5 A/cm <sup>2</sup> <sup>b</sup>	mV	30
Mass activity @ 900 mV <sub>iR-free</sub> <sup>c</sup>	A/mg <sub>PGM</sub>	0.44

<sup>a</sup>-Table E1, <sup>b</sup>-Table E2; Appendix E of FOA; <sup>c</sup> DOE protocol per appendix E of FOA

# Relevance

## Impact of carbon corrosion on PEFCs

Carbon is mainly used as an electrocatalyst support due to its:

- High electrical conductivity ( $> 20 \text{ S/cm}$ )
- High BET surface area :  $200 - 300 \text{ m}^2/\text{g}$
- Low cost

Electrochemical oxidation of carbon occurs during fuel cell operation

- $\text{C} + 2\text{H}_2\text{O} \rightarrow \text{CO}_2 + 4\text{H}^+ + 4\text{e}^-$   $E^\circ = 0.207 \text{ v vs. SHE}$

Carbon corrosion is accelerated:

- During start/stop operation (cathode carbon corrosion)
- Under fuel starvation conditions (anode carbon corrosion)

Kinetic and ohmic losses result due to:

- Pt sintering and loss of contact between Pt and C

Mass transport losses occur due to

- Formation of hydrophilic groups => flooding

# Relevance

## Research objectives

- Conducting, doped, non-PGM metal oxides (electron conductivity  $>0.2$  S/cm)
- High surface area ( $>70$  m<sup>2</sup>/g)
- Exhibits SMSI with Pt
- Corrosion resistant (DOE 2020 targets)
- High electrocatalyst performance (DOE 2020 targets)

Metal oxide	Stable potential window (vs. SHE) (pH 0-1)	Manifestation of SMSI	Possible dopants
TiO <sub>2</sub> (4+, 60.5 pm)	-0.4 - 2.2 V	Yes	Nb (5+, 64 pm), Ta (5+, 64 pm), Mo (6+, 59 pm), W (6+, 60 pm)
Nb <sub>2</sub> O <sub>5</sub> (5+, 64 pm)	-0.2 - 2.2 V	Yes	Mo (6+, 59 pm), W (6+, 60 pm), Tc (7+, 56 pm), Re (7+, 53 pm)
Ta <sub>2</sub> O <sub>5</sub> (5+, 64 pm)	-0.7 - 2.2 V	Yes	Mo (6+, 59 pm), W (6+, 60 pm), Tc (7+, 56 pm), Re (7+, 53 pm)

## Research objectives: Technical targets

Metric	Units	SoA (Pt/C) *	SoA (Pt/RTO)	Proposed approach status (Pt/TiO <sub>2</sub> -Ta)**	End target	DOE 2020 target
Total PGM content	g kW <sup>-1</sup>	0.55	0.55	Not Available	0.25	<0.125
Total PGM loading	mg cm <sup>-2</sup>	0.4	0.4	0.6	0.25	<0.125
Voltage at 1.5 A cm <sup>-2</sup> (air)	mV	0.45	0.48	0.3	0.55	N/A
Loss in mass activity <sup>a,b</sup>	% loss	32	33	<10%	<5%	<40
Voltage loss at 0.8 A cm <sup>-2</sup> a	mV	81	9	< 15	<10	30
Voltage loss at 1.5 A cm <sup>-2</sup> b	mV	182 <sup>+</sup>	20	N/A; 20 mV at 1Acm <sup>-2</sup>	<20	30
Mass activity@900 mV <sub>ir-free</sub> <sup>c</sup>	A mg <sup>-1</sup> <sub>PGM</sub>	0.07	0.07	ca. 0.05	0.3	0.44

<sup>a</sup>-Table E1, <sup>b</sup>-Table E2; Appendix E of FOA; <sup>c</sup> DOE protocol per appendix E of FOA; \*Pt/C refers to Pt/Graphitized Ketjen Black tested at NTCNA; \*\*Results from entirely un-optimized MEAs run primarily to test stability. <sup>+</sup>Pt/HSAC durability is much worse – MEA does not run beyond 0.5 A cm<sup>-2</sup> after start-stop cycling.

Data from MEA in a PEFC

# Relevance

## Research objectives: 1<sup>st</sup> year milestones

Q1

- 2g Ta-doped TiO<sub>2</sub>
- B.E.T. surface area >30 m<sup>2</sup>g<sup>-1</sup>; Electronic conductivity > 0.2 S cm<sup>-1</sup>

Q2

- 2g stable doped metal oxide
- B.E.T. surface area > 30 m<sup>2</sup> g<sup>-1</sup>; Electronic conductivity >0.2 S cm<sup>-1</sup>

Q3

- 2g TiO<sub>2</sub> using SSM
- B.E.T. surface area >50 m<sup>2</sup> g<sup>-1</sup>; Particle size <70nm

Q4

- 2g Ta-doped TiO<sub>2</sub> support using SSM
- B.E.T. area >50 m<sup>2</sup> g<sup>-1</sup>; Particle size <70nm, conductivity > 0.2 S cm<sup>-1</sup>

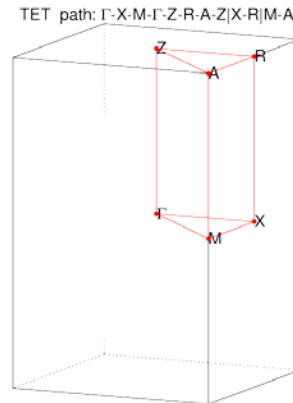
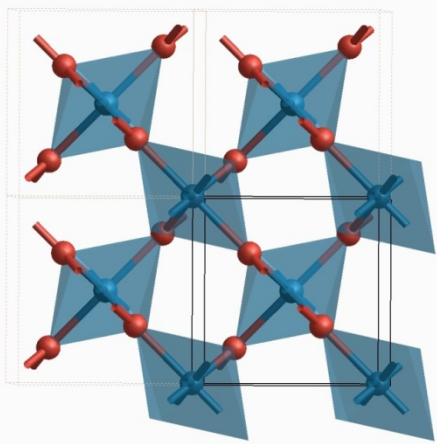
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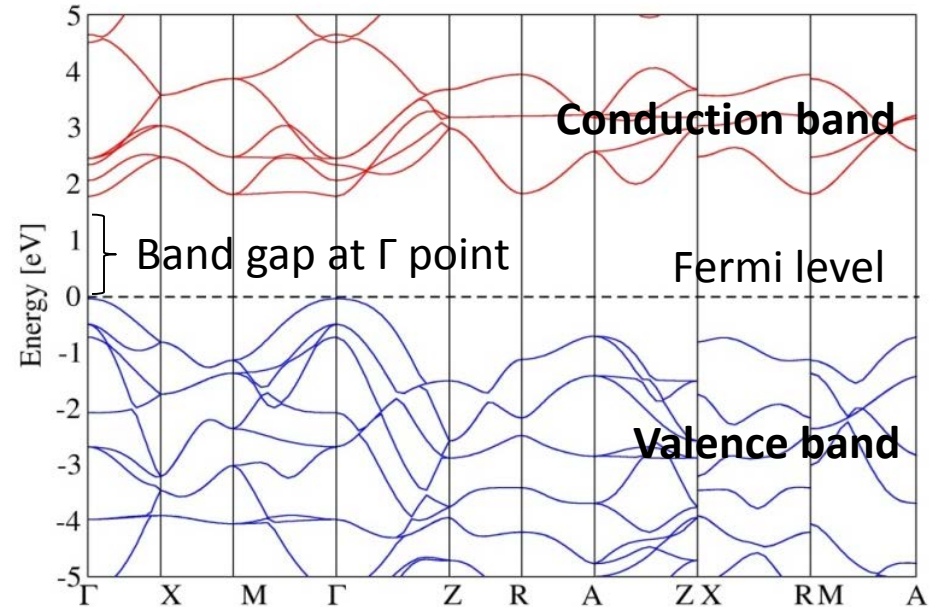
# Approach

## Density Functional Theory - Doping of $\text{TiO}_2$ with Ta

Change in the electronic structure of supports as a result of doping



DFT optimized structure of  $\text{TiO}_2$  (PBEsol functional). Cell parameters  $a=4.56$ ,  $b=4.56$ ,  $c=2.93$  Å  
red – oxygen, blue - Ti



DFT calculated band structure of  $\text{TiO}_2$ . Top HSE06 level, bottom PBEsol level

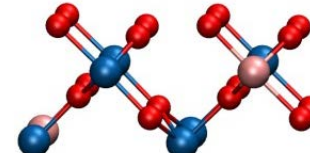
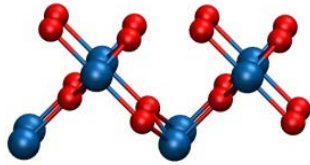
- $\text{TiO}_2$  is a **semiconductor, absorbs in UV**.
- Direct B-G of 1.82 eV at PBEsol level, 3.44 eV at HSE06 level (hybrid functional needed).
- Experimental reports 3.3-3.6 eV (UPS-IPS spectroscopy).



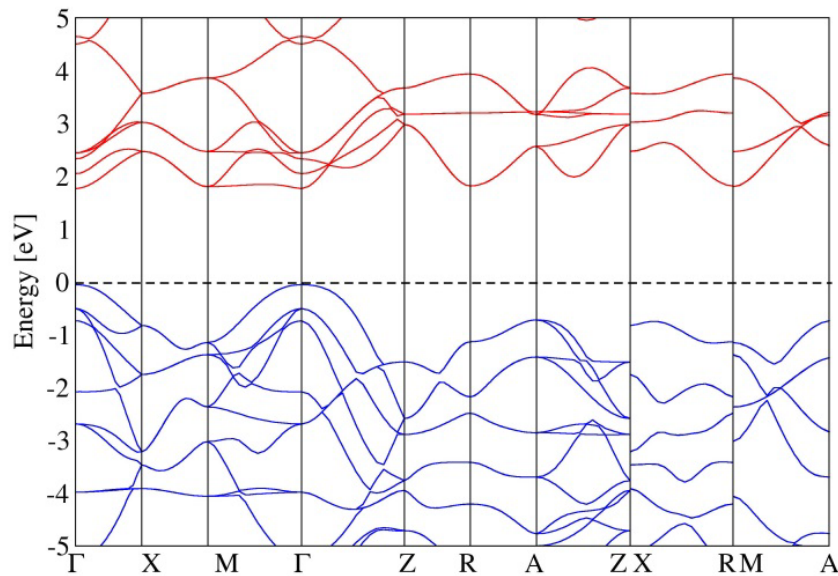
# Approach

## Density Functional Theory - Doping of TiO<sub>2</sub> with Ta

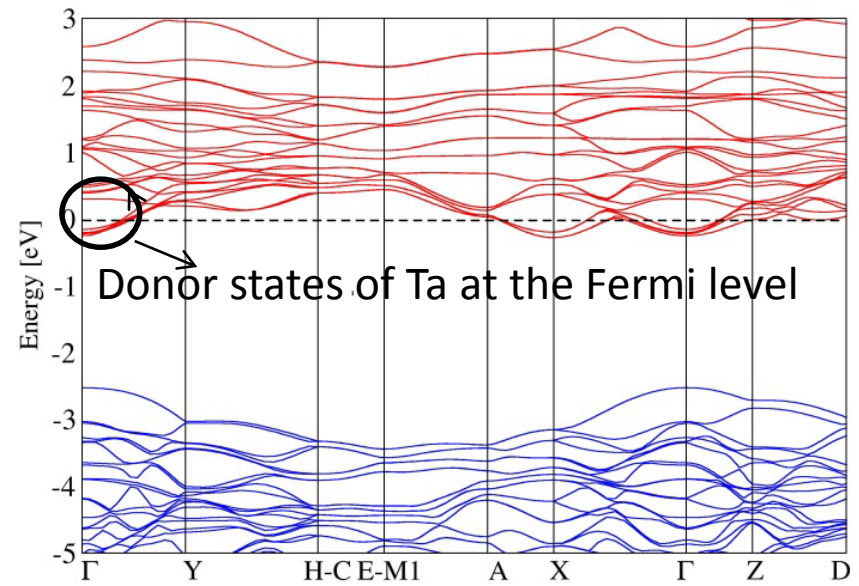
Change in the electronic structure of supports as a result of doping



Blue - Ti  
Pink - Ta  
Red - O



TiO<sub>2</sub>

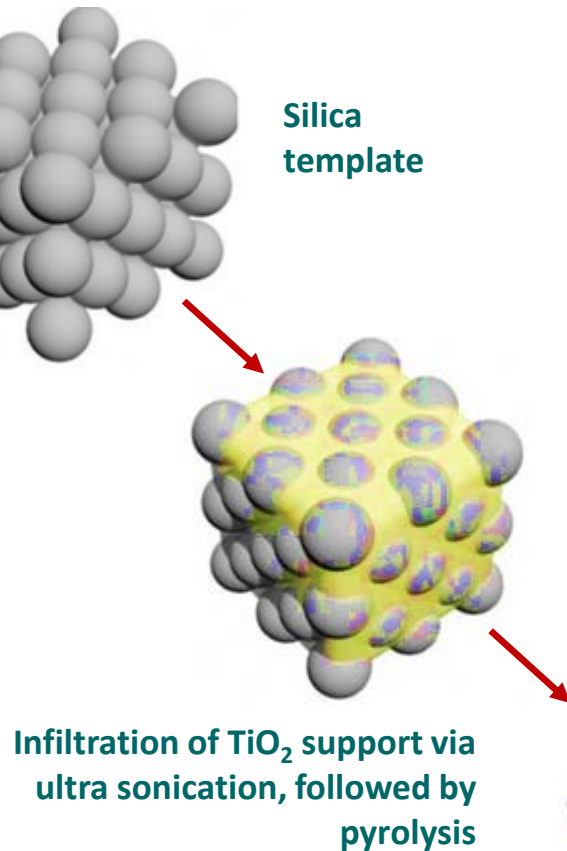


TiO<sub>2</sub> with 12.5% Ta (model concentration)

- TiO<sub>2</sub> is a **semiconductor**, while doping of Ta creates a ***n*-type semiconductor** with **increased conductivity** - leads to “metallization”

# Approach

## Design Porous TiO<sub>2</sub> supports



### Synthesis and characterization of high surface area TiO<sub>2</sub> supports.

#### (i) Synthesis of TiO<sub>2</sub> support.

- sol-gel technique
- alkoxides titanium as precursors

#### ii Sacrificial support method (Templating)

- Cab-O-Sil L90 surface area ~90 m<sup>2</sup> g<sup>-1</sup>, 0.22 μm
- Cab-O-Sil EH5, surface area ~400 m<sup>2</sup> g<sup>-1</sup>, 0.14 μm
- pyrolyzed at 850°C followed by leaching with 40 wt.% HF

#### iii Characterization of TiO<sub>2</sub> support

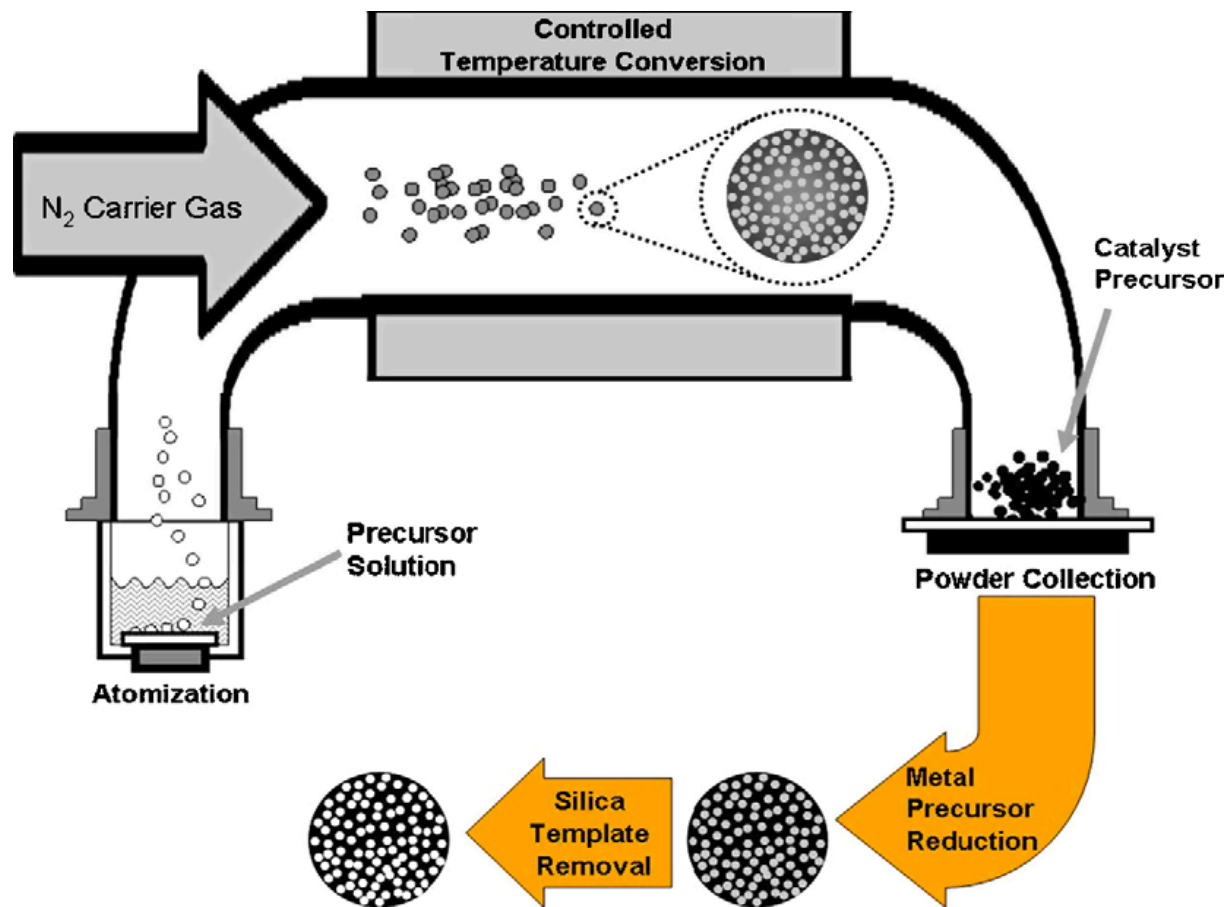
- Morphology: SEM, N<sub>2</sub>-sorption BET surface area, pore size analysis
  - Composition: EDS, XPS, Elemental Mapping
    - Structure : XRD
  - electron conductivity (in-house test cell)



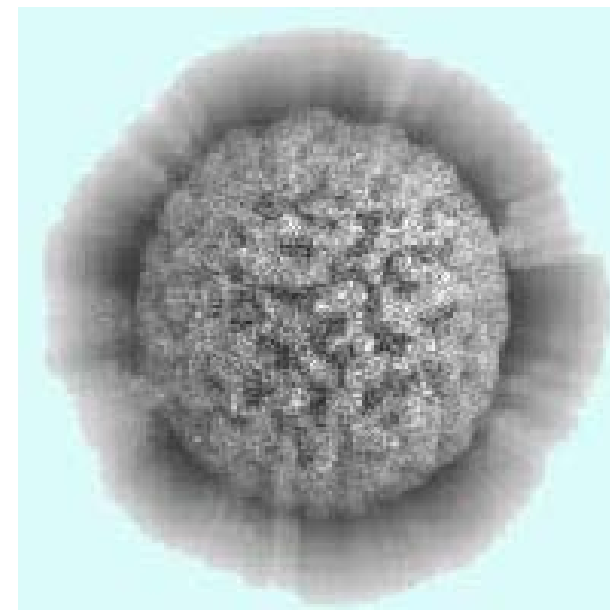
Leaching the sacrificial silica support: Porous TiO<sub>2</sub> support

# Approach

## Scale-up of templated materials



Combination of spray pyrolysis with SSM method



E. Switzer, P. Atanassov A.K. Datye, Nanostructured Anode Pt-Ru Electrocatalysts for Direct Methanol Fuel Cells, *Topics in Catalysis*, 46 (2007) 334-338

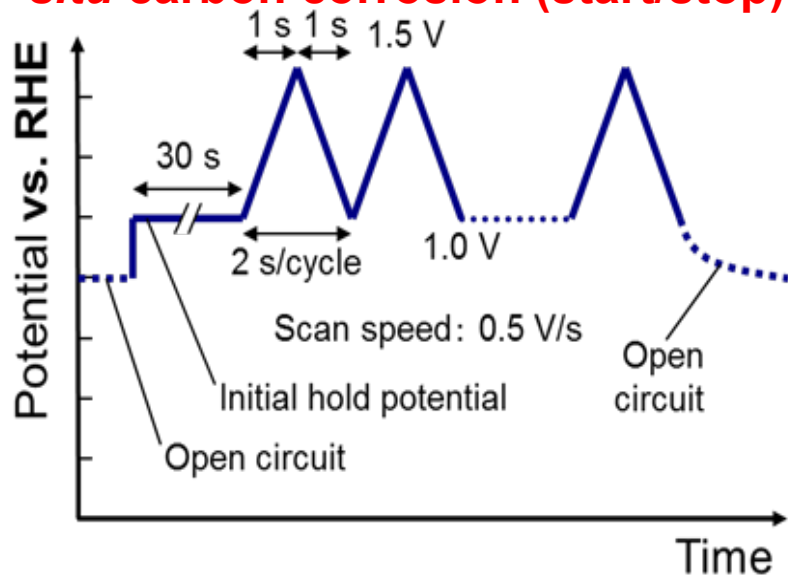
E. Switzer, T.S. Olson, A. K. Datye, P. Atanassov, M.R. Hibbs and C.J. Cornelius, Templated Pt-Sn Electrocatalysts for Ethanol, Methanol and CO Oxidation in Alkaline Media, *Electrochimica Acta* 54 (2009) 989-995

A. Falase, K. Garcia, C. Lau, and P. Atanassov, Electrochemical and *in Situ* IR Characterization of PtRu Catalysts for Complete Oxidation of Ethylene Glycol and Glycerol, *Electrochemistry Communications*, 13 (2011) 1488-1491

# Approach

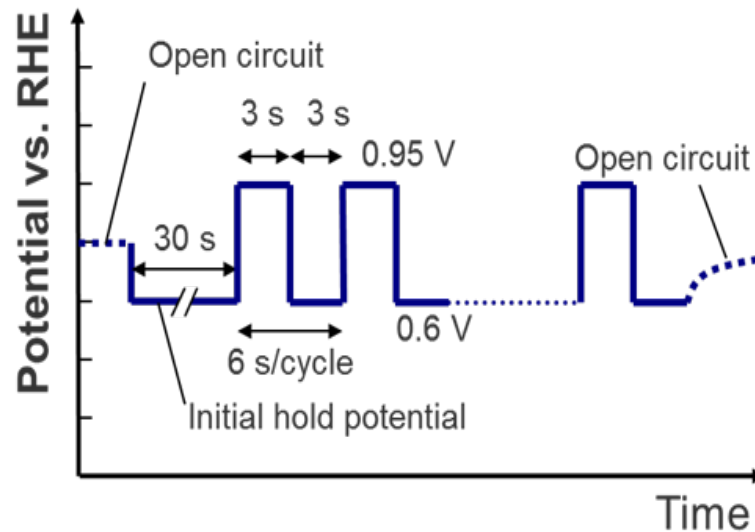
Potential cycling to evaluate support and electrocatalyst electrochemical stability/durability

**Catalyst durability: *Ex-situ* and *in situ* carbon corrosion (start/stop)**



Protocol for simulating start-up/shut-down phenomena

**Catalyst durability: *Ex-situ* and *in situ* Pt dissolution (load cycling)**



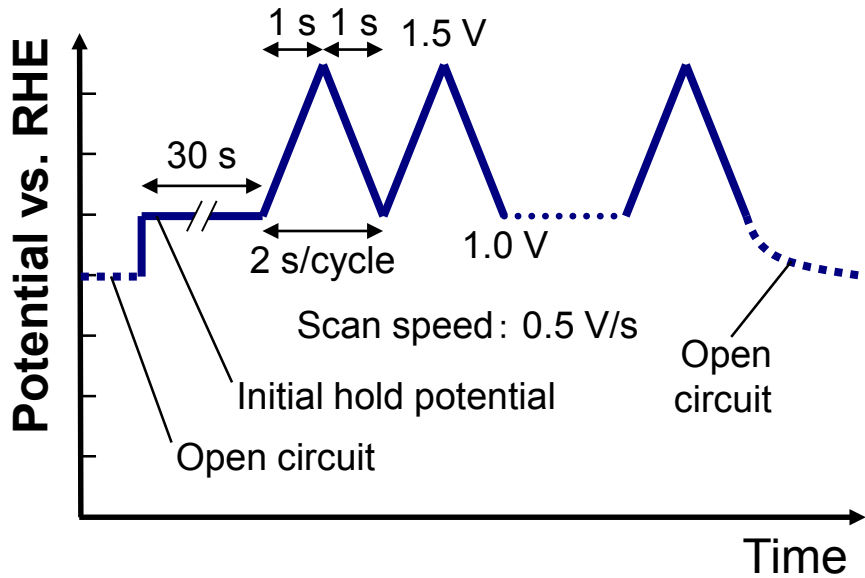
Protocol for simulating load cycling phenomena.

The protocols recommended in solicitation **DE-FOA-0001224 (next slide)** will also be employed.

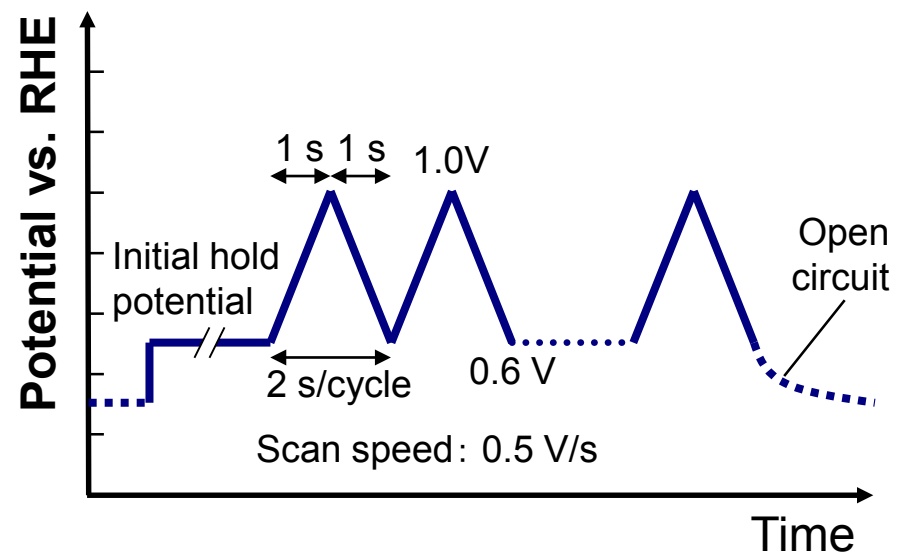
# Approach

Potential cycling to evaluate support and electrocatalyst electrochemical stability/durability

**Catalyst durability: *Ex-situ* and *in situ* carbon corrosion (start/stop)**



**Catalyst durability: *Ex-situ* and *in situ* Pt dissolution (load cycling)**



**Support durability — support corrosion**

**Catalyst durability — Pt dissolution**

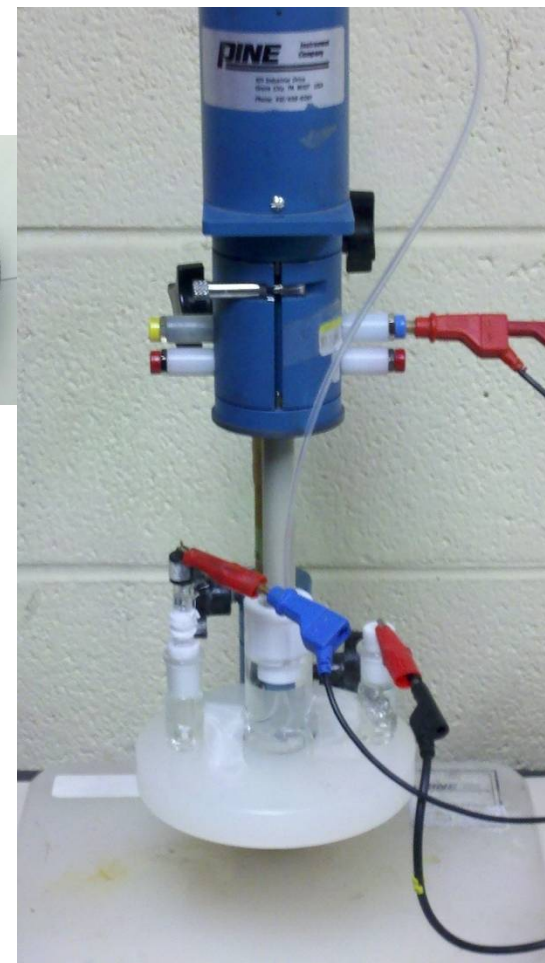
Electrolyte: 0.1 M HClO<sub>4</sub>  
Temperature: 60°C at NTCNA, RT at IIT  
CV sweep rate of 20 mV/s; Room temperature CV



# Approach

Potential cycling to evaluate support and electrocatalyst durability

- Three electrode cell with rotating disk electrode
  - Working electrode (WE) : Glassy carbon coated with catalyst support
  - Counter electrode : Pt foil
  - Reference electrode : Saturated calomel electrode (SCE)
  - Electrolyte :  $N_2$  saturated 0.1M  $HClO_4$
- Support loading on W.E.: 200-600  $\mu g/cm^2_{geo}$  (material dependent)
- Pt loading:  $20\mu g_{Pt}/cm^2_{geo}$
- Potential cycling protocol



# Approach

## MEA fabrication and optimization



Homogenizer (IKA)

- ❑ NTCNA has extensive expertise in the fabrication of catalyst-coated membranes (CCMs) and catalyst-coated gas diffusion layers (GDLs).
- ❑ High performance dispersing homogenizers for uniformly dispersed catalyst ink preparation.
- ❑ Automated robotic spray system for catalyst layer deposition on GDL/membrane.

### MEA fabrication



Spray system (Asymtek)

### Design and optimization of catalyst layers (CL)

Estimation of ionomer volume fraction

$$\varepsilon_i \equiv \frac{V_{I,wet}}{V_{cath}} = \left( \frac{I}{C} \right) \frac{10}{f_I d_{I,dry}} \left( 1 + \frac{M_w d_{I,dry} \lambda}{d_w EW} \right)$$

Estimation of ionomer film thickness

$$\sigma \text{ (ionomer film thickness)} = \frac{V_{Nafion}}{A_{eff}} = \frac{V_{Nafion}}{(1 - \gamma) A_{BET} \cdot 10^4 \cdot m_{cat}}$$

# Approach

## Performance Evaluation

MEA conditions (electrochemical diagnostics)		
<b>Temperature</b>		80 °C
<b>Anode</b>	Gas	H <sub>2</sub>
	Relative humidity	100%
	Flow rate (NLPM)	0.5
<b>Cathode</b>	Gas	N <sub>2</sub>
	Relative humidity	100%
	Flow rate (NLPM)	0.5

MEA conditions (iV performance)	
<b>BoL and EoL iV performance</b>	H <sub>2</sub> -O <sub>2</sub> /Air, 80°C, RH 40%, RH 100%, ambient pressure, and 101 kPa (gauge pressure)

- ❑ Fuel cell performance evaluation under standard DOE-protocols
- ❑ To better understand mass transport properties.
- ❑ Using dilute oxygen concentrations (~0.5-2% O<sub>2</sub>) to obtain gas transport resistances ( $R_{diff}$  and  $R_{other}$ ) in the catalyst layer.



# Approach

## 1<sup>st</sup> year milestones and GNG

Task number	Milestone	Milestone description	Milestone verification process	Anticipated Date/Quarter	Current status
1	Milestone 1.1	2g of TiO <sub>2</sub> -Ta*	B.E.T. surface area >30 m <sup>2</sup> g <sup>-1</sup> ; electronic conductivity > 0.2 S cm <sup>-1</sup>	M3/Q1	20 m <sup>2</sup> g <sup>-1</sup> ; 0.1 S cm <sup>-1</sup>
4	Milestone 4.1	2g of stable doped-metal-oxide support	B.E.T. surface area > 30 m <sup>2</sup> g <sup>-1</sup> ; electronic conductivity >0.2 S cm <sup>-1</sup>	M6/Q2	Not started
5	Milestone 5.1.1	2g of TiO <sub>2</sub> using SSM	B.E.T. area >50 m <sup>2</sup> g <sup>-1</sup> ; particle size <70nm	M9/Q3	Not started
5	Milestone 5.1.2 Go/No-Go	2g of TiO <sub>2</sub> -Ta support material using SSM	B.E.T. area >50 m <sup>2</sup> g <sup>-1</sup> ; particle size <70nm, conductivity > 0.2 S cm <sup>-1</sup>	M12/Q4	Not started

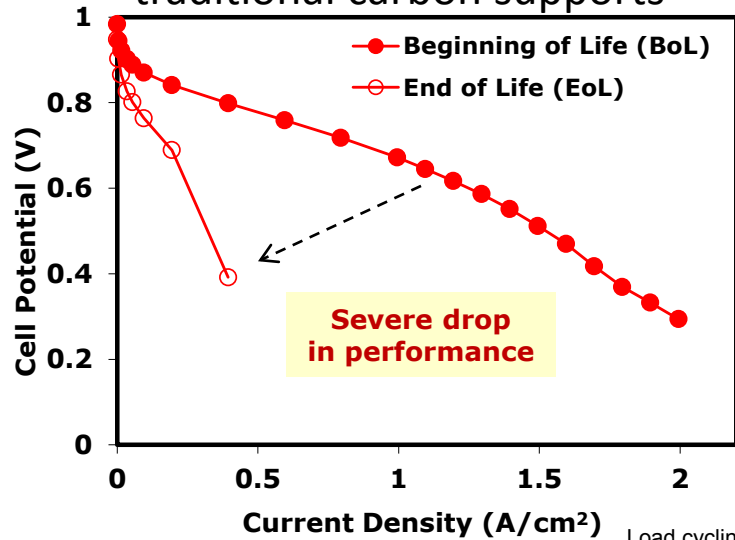
\* Or any other conducting and stable doped-metal-oxide support exhibiting SMSI and meeting the milestone targets

# Technical accomplishments

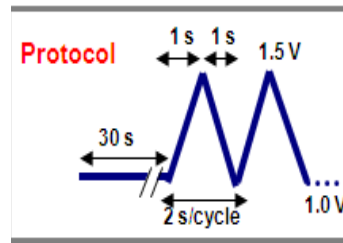
IIT-Nissan Pt/non-carbon support research:

Example of previous results

■ Problem: Poor durability of traditional carbon supports



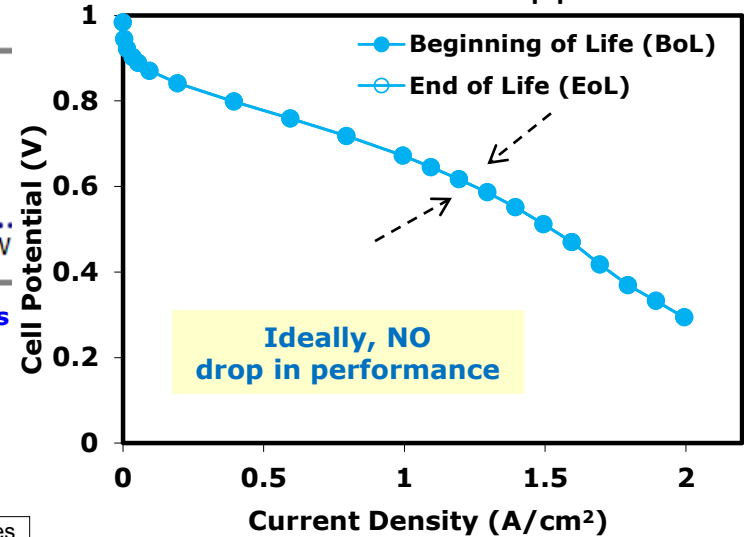
FCCJ (Japan)



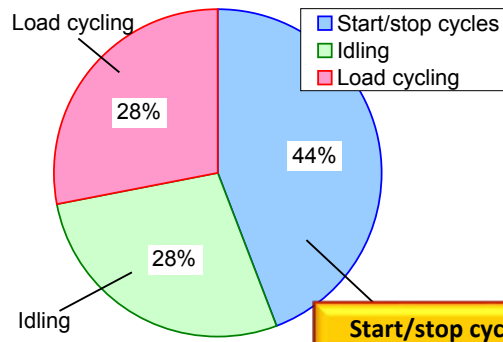
1000 cycles

Start-stop potential cycling protocol

■ Approach: Development of non-carbon supports

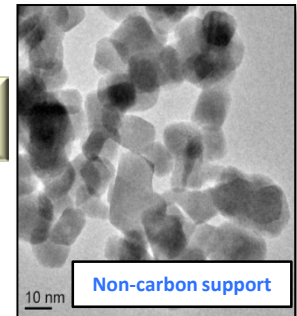


Nissan study on fuel cell degradation modes



Shimoi et al, JSAE Spring Meeting (2009)

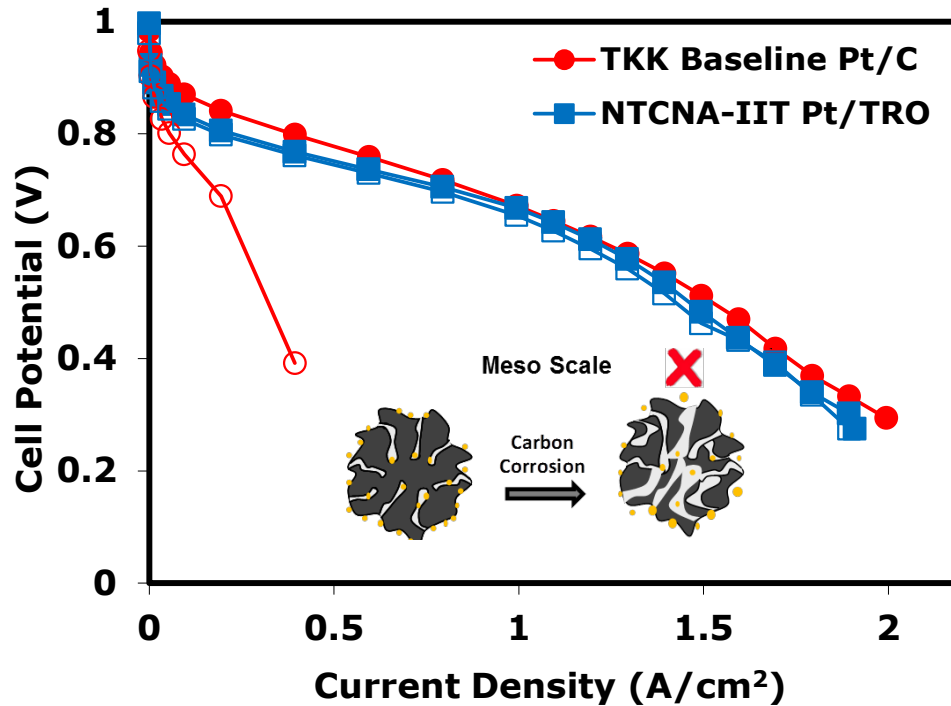
Example: TiO<sub>2</sub>-RuO<sub>2</sub>, SnO<sub>2</sub>-In<sub>2</sub>O<sub>3</sub> metal oxides



# Technical accomplishments

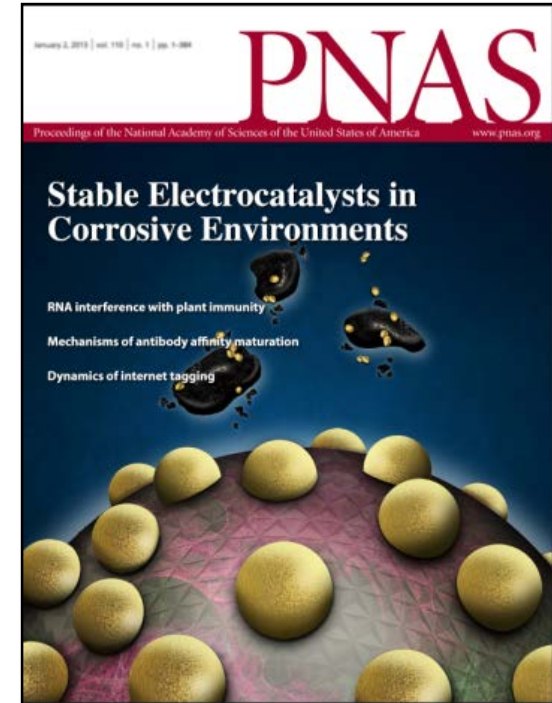
## Pt/TRO as cathode support – *Prior DOE Project*

- Pt/TRO showed excellent durability under start-stop protocol



**Durability of Pt/TRO is much better than the Pt/C baseline catalyst**

- Published in PNAS\*

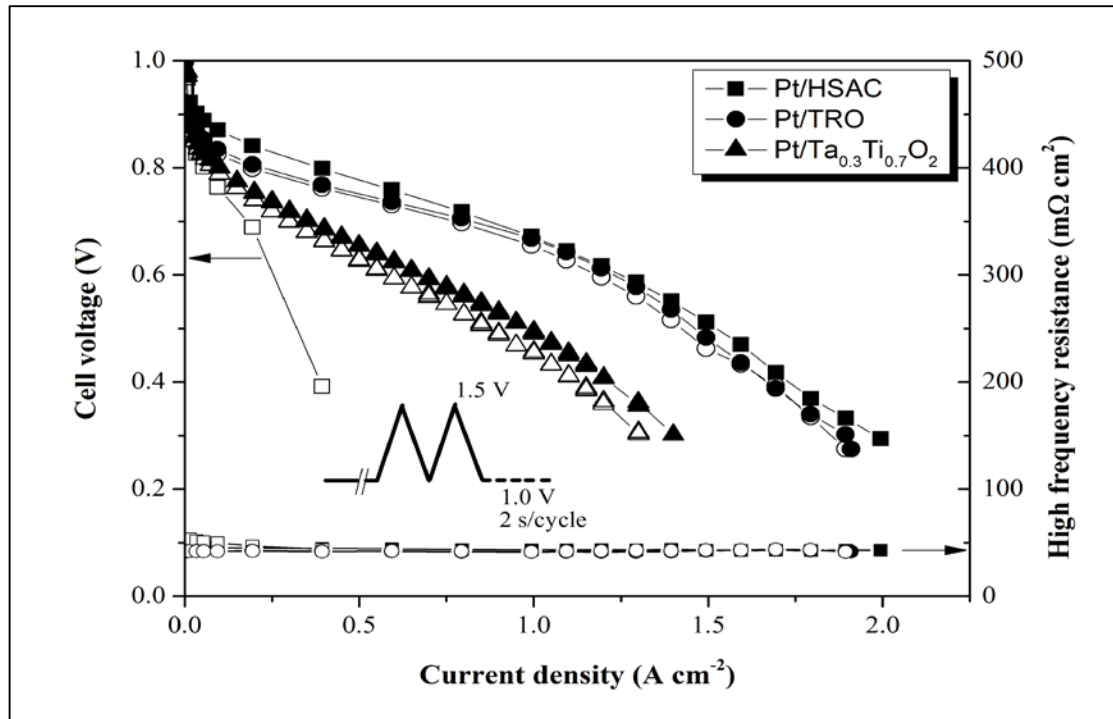


**Breakthrough durability of Pt/TRO Results published in PNAS**

- \* Illustrative cover only!

# Technical accomplishments

## Start-stop stability of Ta doped TiO<sub>2</sub> in a PEFC



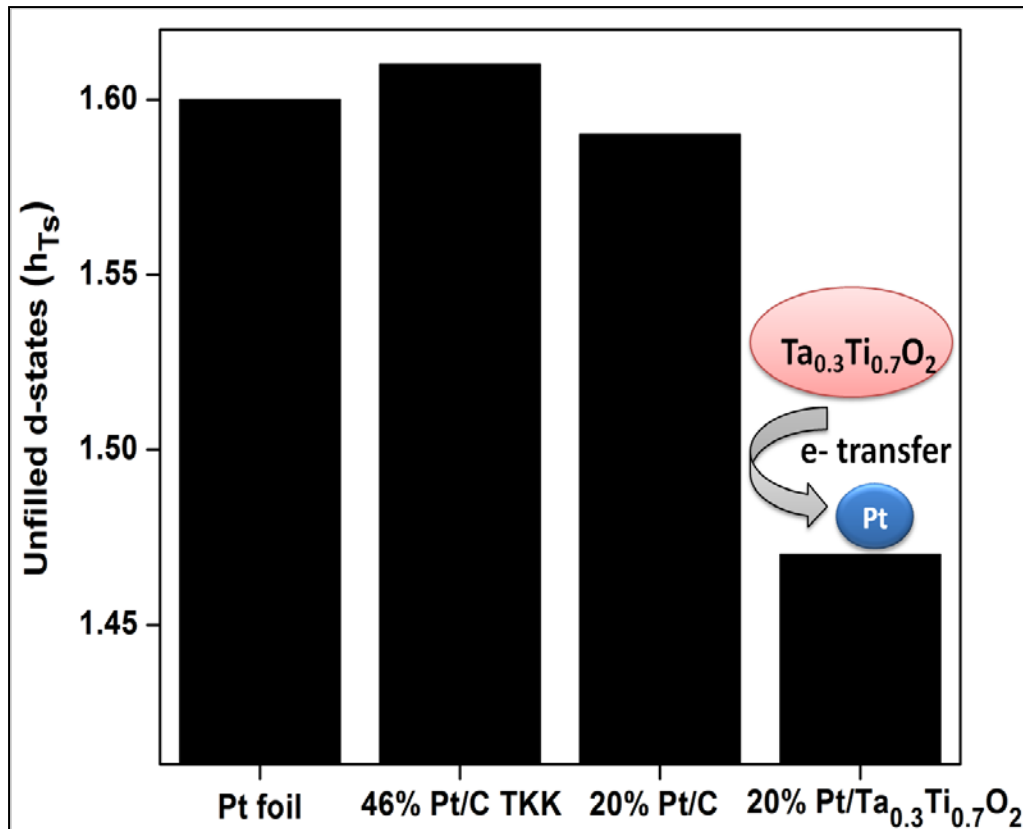
**Figure .** Comparison of fuel cell performance obtained with Pt/ HSAC, Pt/TRO, and Pt/ (TiO<sub>2</sub>-Ta) before (closed symbols) and after (open symbols) exposure to the start-stop protocol specified in FOA (1,000 cycles). 25 cm<sup>2</sup> fuel cell; 80°C and 100% RH.

- Pt/TiO<sub>2</sub>-Ta shows remarkable start-stop stability
- Ability to achieve respectable performance (though short of Pt/TRO or Pt/C) with *essentially zero optimization* of the Pt/TiO<sub>2</sub>-Ta electrode.

Note: TRO is TiO<sub>2</sub>-RuO<sub>2</sub>, developed in our previous project

# Technical accomplishments

## Demonstration of SMSI in Ta doped TiO<sub>2</sub>



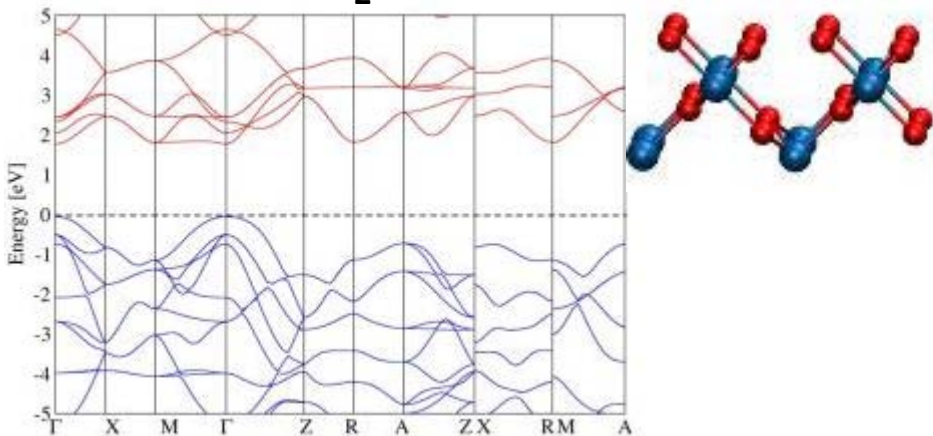
**Figure.** Variation in unfilled d-states for 20% Pt/TiO<sub>2</sub>-Ta, 46% Pt/C, 20% Pt/C catalysts and Pt foil.

- The existence of SMSI on Pt/TiO<sub>2</sub>-Ta was ascertained by XPS and XAS.
- The decrease in the number of unfilled d-states confirms electron donation from the TiO<sub>2</sub>-Ta support to Pt nanoparticles.
- SMSI mitigates Pt dissolution under load cycling conditions

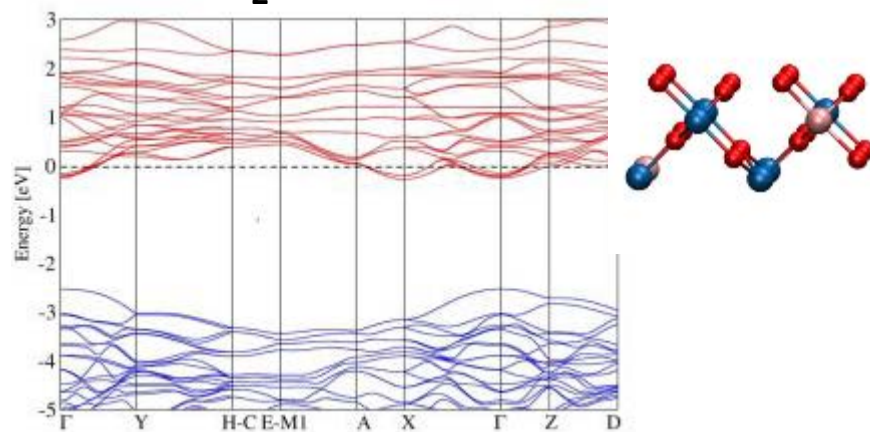
# Technical accomplishments

## DFT calculations for Ta-TiO<sub>2</sub> support

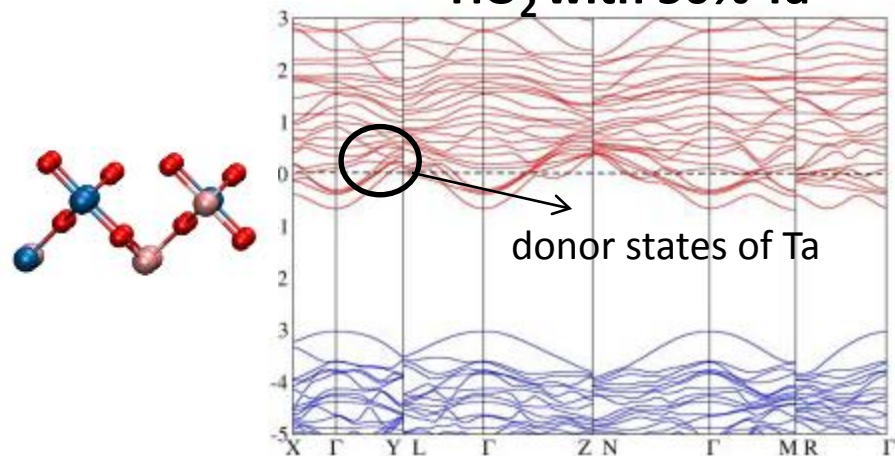
TiO<sub>2</sub>



TiO<sub>2</sub> with 25% Ta



TiO<sub>2</sub> with 50% Ta

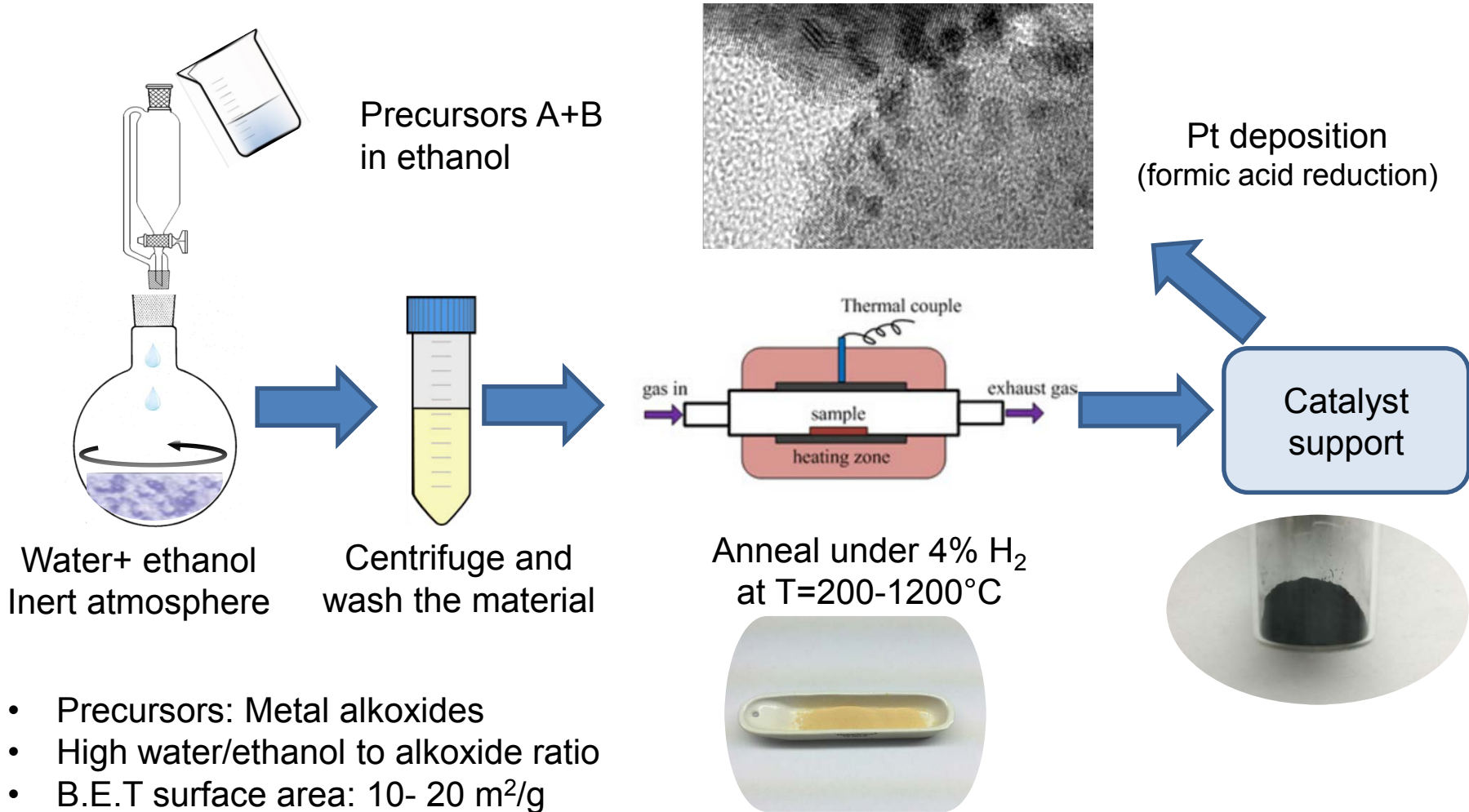


- DFT calculations show that doping TiO<sub>2</sub> with Ta from 25-50% reduces the B-G
- Ta-TiO<sub>2</sub> becomes increasingly metallic and conductive.



# Technical accomplishments

## Sol-gel synthesis



# Technical accomplishments

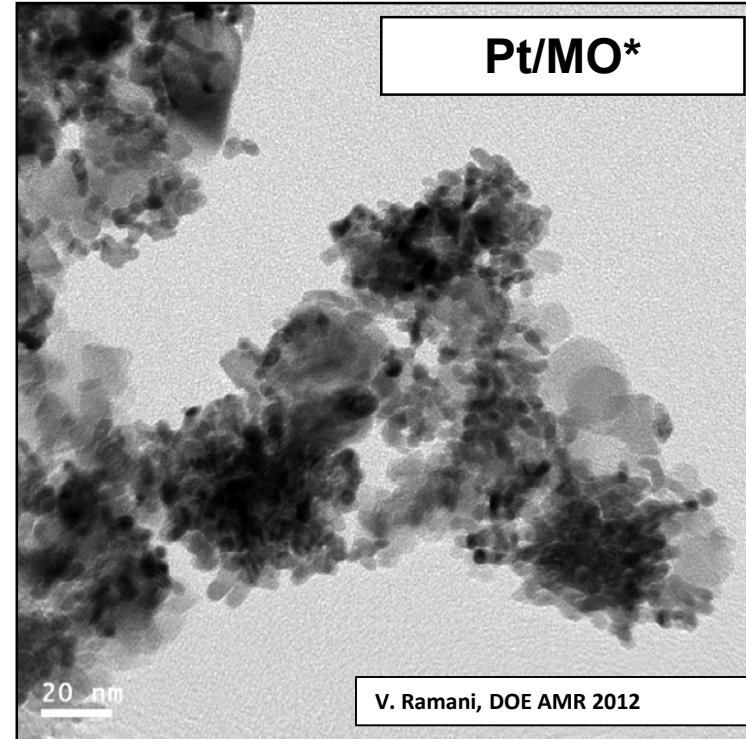
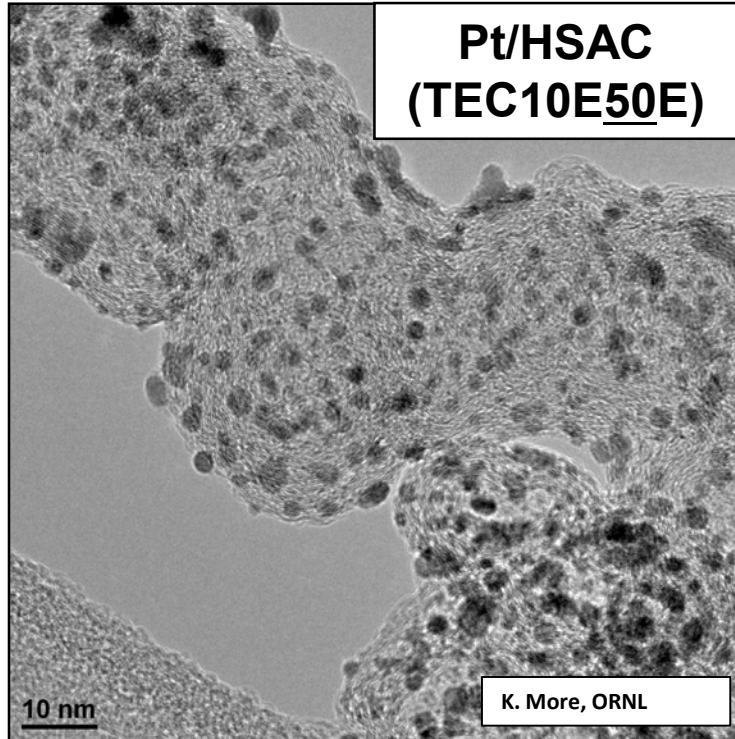
## Sol-gel synthesis

Oxide	Precursor A	Precursor B	Annealing temperature	BET m <sup>2</sup> /g	Conductivity S/cm
Nb-doped TiO <sub>2</sub>	Nb <sub>2</sub> (OC <sub>2</sub> H <sub>5</sub> ) <sub>10</sub>	Ti[OCH(CH <sub>3</sub> ) <sub>2</sub> ] <sub>4</sub>	650°C	14.6 ± 2.4	0.102 ± 0.01
Nb-doped TiO <sub>2</sub>	Nb <sub>2</sub> (OC <sub>2</sub> H <sub>5</sub> ) <sub>10</sub>	Ti[OCH(CH <sub>3</sub> ) <sub>2</sub> ] <sub>4</sub>	550°C	21.2 ± 3.1	Non Conductive
Ta-doped TiO <sub>2</sub>	Ta <sub>2</sub> (OC <sub>2</sub> H <sub>5</sub> ) <sub>10</sub>	Ti[OCH(CH <sub>3</sub> ) <sub>2</sub> ] <sub>4</sub>	1000°C	3.4 ± 0.5	0.043 ± 0.007
Ta-doped TiO <sub>2</sub>	Ta <sub>2</sub> (OC <sub>2</sub> H <sub>5</sub> ) <sub>10</sub>	Ti[OCH(CH <sub>3</sub> ) <sub>2</sub> ] <sub>4</sub>	850°C	10.3 ± 1.3	0.024 ± 0.005
Ta-doped Nb <sub>2</sub> O <sub>5</sub>	Ta <sub>2</sub> (OC <sub>2</sub> H <sub>5</sub> ) <sub>10</sub>	Nb <sub>2</sub> (OC <sub>2</sub> H <sub>5</sub> ) <sub>10</sub>	850°C	12.1 ± 1.7	Non Conductive



# Remaining Challenges and Barriers

## TEM images of Pt/C and Pt/MO\*

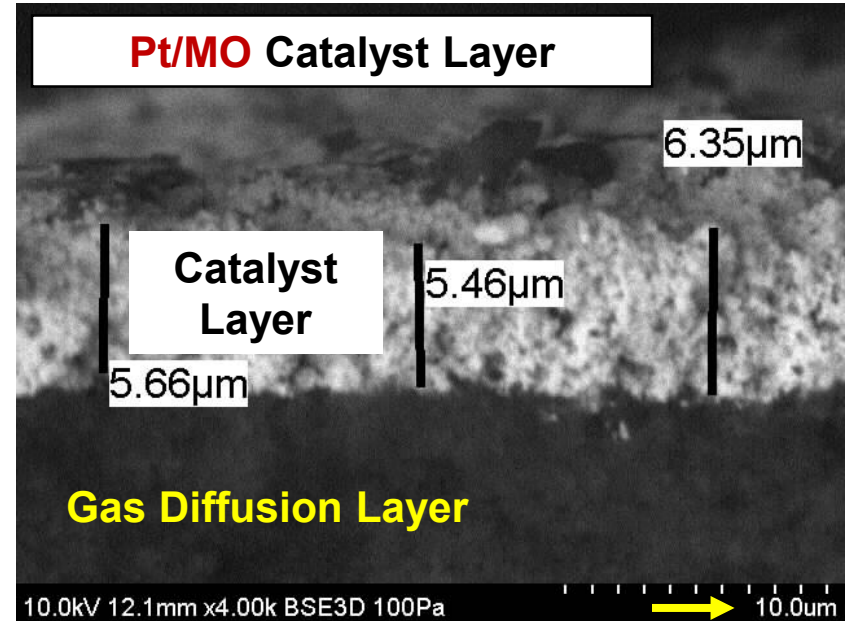
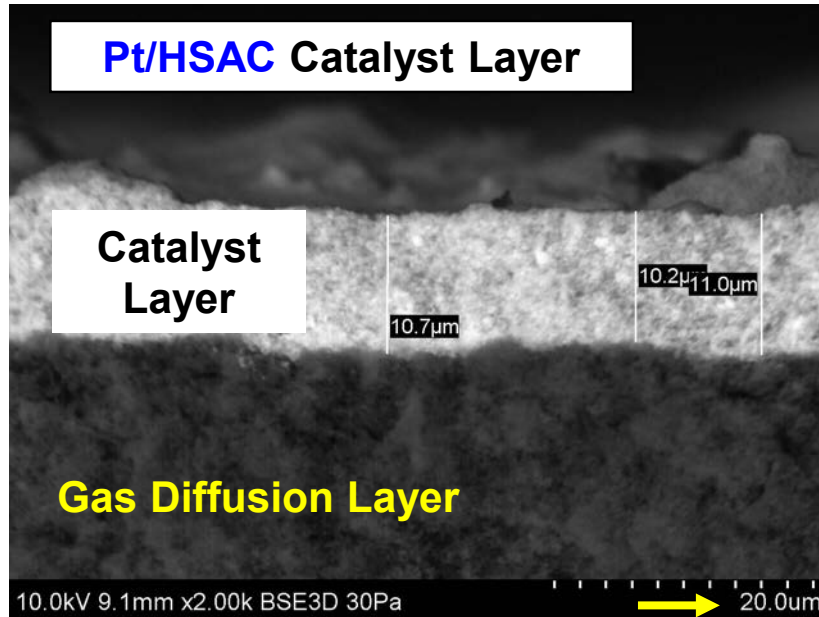


- ❑ There are significant differences between Pt/C and Pt/MO
- ❑ Pt particle size, Pt dispersion/agglomeration, Pt particle density.
- ❑ **Engineer wettability**

\* MO= metal oxides

# Remaining Challenges and Barriers

## SEM pictures of Pt/C and Pt/MO\* catalyst layers



	Pt/HSAC	Pt/MO
CL thickness (μm)	11	5.5
I/C mass ratio	0.9	0.9
B.E.T. surface area(m <sup>2</sup> /g)	313	39
ε <sub>i</sub> (ionomer volume fraction)	0.21	0.66

$$\varepsilon_i \equiv \frac{V_{I,wet}}{V_{cath}} = \left( \frac{I}{C} \right) \frac{10}{f_t d_{I,dry}} \left( 1 + \frac{M_w d_{I,dry} \lambda}{d_w EW} \right)$$

- MO is denser than carbon
- The Pt/MO CL is much thinner than Pt/HSAC.
- The ionomer volume fraction (ε<sub>i</sub>) is higher in Pt/MO
- Optimize MEA composition and design**

# Remaining Challenges and Barriers

Project just started!!!

Task number	Milestone	Milestone description	Milestone verification process	Anticipated Date/Quarter
1	Milestone 1.1	2g of TiO <sub>2</sub> -Ta*	B.E.T. surface area >30 m <sup>2</sup> g <sup>-1</sup> ; electronic conductivity > 0.2 S cm <sup>-1</sup>	M3/Q1
4	Milestone 4.1	2g of stable doped-metal-oxide support	B.E.T. surface area > 30 m <sup>2</sup> g <sup>-1</sup> ; electronic conductivity >0.2 S cm <sup>-1</sup>	M6/Q2
5	Milestone 5.1.1	2g of TiO <sub>2</sub> using SSM	B.E.T. area >50 m <sup>2</sup> g <sup>-1</sup> ; particle size <70nm	M9/Q3
5	Milestone 5.1.2 Go/No-Go	2g of TiO <sub>2</sub> -Ta support material using SSM	B.E.T. area >50 m <sup>2</sup> g <sup>-1</sup> ; particle size <70nm, conductivity > 0.2 S cm <sup>-1</sup>	M12/Q4

# Remaining Challenges and Barriers

Task Number	Milestone	Milestone Description	Milestone Verification Process*	Anticipated Date/Quarter
7	Milestone 7.1	2g of Pt/DS catalyst (SMSI)	Demonstrate SMSI; Meets Table 2 durability targets in RDE	M15/Q5
8	Milestone 8.1	Pt/DS catalyst	Demonstrate 10% increase in mass activity	M18/Q6
5	Milestone 5.2.1	2g of at least one doped oxide using SSM	B.E.T. area $>70 \text{ m}^2\text{g}^{-1}$ ; particle size $<70\text{nm}$ ; conductivity $> 0.2 \text{ Scm}^{-1}$ ; Stability and durability in RDE per DOE metrics	M21/Q7
6	Milestone 6.2.1 <b>Go/No-Go</b>	Deliver 2g of Pt/DS catalyst to NTCNA	20-40wt%Pt; $> 70 \text{ m}^2\text{g}^{-1}$ ; Pt particle size 3-6nm; meets DOE 2020 durability targets	M24/Q8

# Remaining Challenges and Barriers

Task Number	Milestone	Milestone Description	Milestone Verification Process*	Anticipated Date/Quarter
10	Milestone 10.1	Pt/DS catalyst	Demonstrate “End Project” durability metrics and at least 80% of mass activity metric	M27/Q9
6	Milestone 6.2.2	Pt/DS catalyst	In addition to Milestone 6.2.1, meet “End Project” BoL mass activity target	M30/Q10
11	Milestone 11.1	Deliver cost model	Specify cost of best 2 Pt/DS materials	M33/Q11
12	Milestone 12.1 Go/No-Go	Deliver six 50 cm <sup>2</sup> active area MEAs to DOE	Meet “End Project” durability, activity, and performance targets in Table 2	M36/Q12

# Collaboration

## Illinois Institute of Technology

- Lead PI and Technical PoC: **Vijay K. Ramani**
- Metal oxide synthesis and characterization, RDE testing (ORR activity and electrochemical stability), PEFC diagnostics



## Nissan Technical Center, North America

- PI and Technical PoC: **Nilesh Dale**
- Evaluation of the catalysts in RDE and PEFC, Cost modeling



## University of New Mexico

- PI and Technical PoC: **Plamen Atanassov**
- Modeling of doped MO conductivity and SMSI (DFT), scale-up of doped metal oxide synthesis

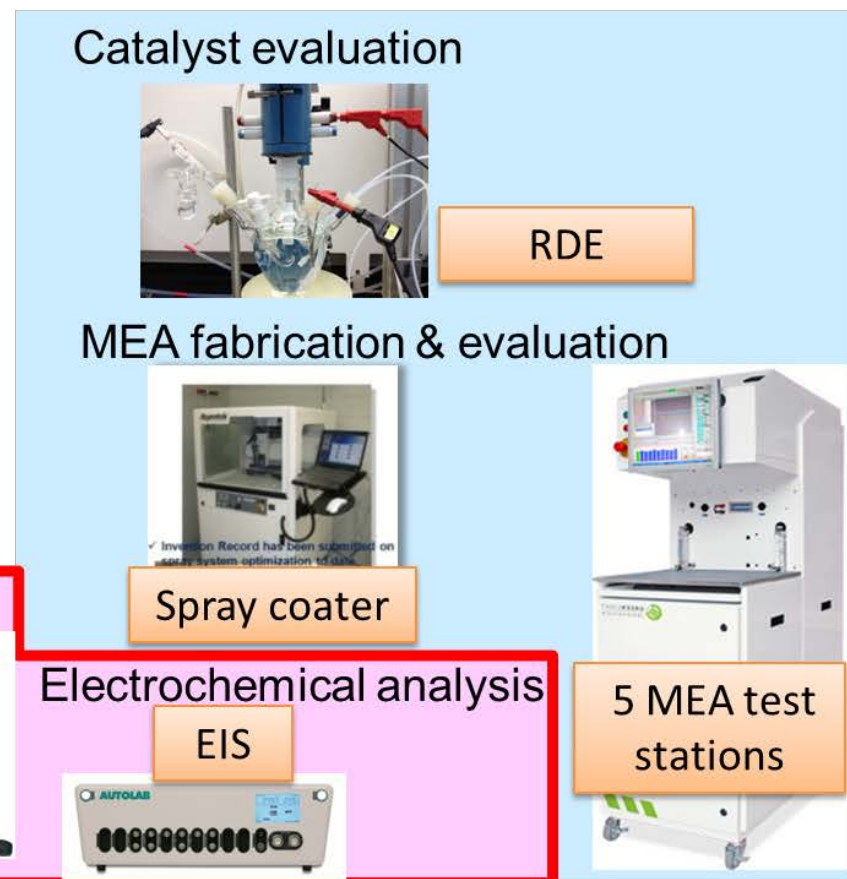




# Collaboration

## Facility and Equipment Capabilities

- ❑ **Scanning Electron Microscope** (SEM, EDS)
- ❑ **X-ray Fluorescence spectrometer** (XRF): To determine the Pt loading.
- ❑ **5 fuel cell test test-stations** (Hydrogenics)
- ❑ Expertise in the fabrication and characterization of catalyst layer (CL): **ionomer volume fraction, proton transport resistance, and oxygen transport resistance.**
- ❑ **Rotating Disk Electrode: *ex-situ* catalyst performance and durability**



# Proposed Future Work

**FY 2016**

- IIT: materials synthesis and characterization
  - ✓ Synthesis and characterization of Ta doped  $\text{TiO}_2$  and other doped metal oxides using wet chemistry
  - ✓ Electrochemical evaluation of support and Pt/MO stability
  - ✓ Investigation of SMSI in Pt/doped-metal-oxide systems
  - ✓ Measurement of BoL ECSA and ORR activity of selected catalysts
- Nissan North America Inc.: durability/performance testing
  - ✓ Accelerated test protocols on materials provided by IIT
  - ✓ Fabrication / testing of sub-scale and 50  $\text{cm}^2$  MEAs
- University of New Mexico
  - ✓ DFT calculations: conductivity and SMSI of relevant doped metal oxides
  - ✓ Characterization of the doped metal oxides and derived catalysts
  - ✓ High surface area support synthesis by SSM.



# Summary

- **Objectives and Approach:**
  - Synthesize doped metal oxides for catalyst supports
  - High conductivity and BET surface area
  - Exhibits SMSI and corrosion resistant (attaining DOE 2020 targets )
- **Relevance**
  - Material-level mitigation strategies can solve cathode durability issues
- **Accomplishments**
  - DFT framework in place to study effect of doping on conductivity
  - Successfully synthesized doped metal oxides with conductivities of 0.1 S/cm
- **Collaborations**
  - Illinois Institute of Technology
  - Nissan Technical Center, North America
  - University of New Mexico