## High performance PEFC electrode structures



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# **Overview**

## Timeline

Project Start:	October 2016	
	2016Q4 = "Q0"	
Project Q1:	Jan-March 2017	

Project End:

December 2019 39 months

### Budget

\$3,019K Total Project Budget:

- \$2,415K Federal Share
- Cost Share (20%) \$604K

\$23K Total DOE Funds Spent\*:

\* as of 3/31/2017

### **Key Barriers**

Achieve DOE's 2020 Targets for MEAs

Characteristic	Units	2015	2020
		Status	Targets
Platinum-group metal (PGM) total loading (both electrodes)	mg PGM /cm²	0.13	≤ 0.125
Performance @ 0.8 V	mA/cm <sup>2</sup>	240	300
Performance @ rated power (150 kPa <sub>abs</sub> )	mW/cm <sup>2</sup>	810	1,000

**Partners** 





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# <u>Relevance</u>

**Objective:** Develop *improved fundamental understanding of transport limitations* in a SOA MEA and use this know-how to *develop and demonstrate high-performance MEAs with ULCLs* 

- High-activity ORR catalysts have been developed & demonstrated
  - MEAs with ultra-low catalyst loadings (ULCLs) can meet activity targets
  - Transport losses are major barrier
    - Flux rate per catalyst site is increased
      - Transport losses increase
    - MEAs with ULCLs cannot yet meet power density (high current) targets



- Need to reduce transport losses in MEAs with ULCLs
  - *First step is to determine actual root-cause mechanisms* (*e.g.,* not CCL thickness)
  - Fundamental understanding is currently lacking

New electrocatalysts require new MEA architectures to realize their full potential



# **Technical Approach**

### Develop Detailed Geometric (*i.e.*, microstructure) Model of CCL



- Cathode catalyst layer (CCL) contains multiple length scales
- Agglomerates in CCL probably contain more than one carbon particle
- If there is an ionomer shell around agglomerates, then need to determine:
  - Thickness of ionomer shell and number of carbon (and catalyst sites) per agglomerate
- Different transport-limiting mechanisms result in different limiting currents
  - Use microstructure model to help discern different transport limitations
  - Make CCLs that can help to probe these differences, as guided by model

#### Multiple possible transport-limiting mechanisms within CCL





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## **Collaborations**

### Core Project Team (i.e., subcontractors)





- Modeling
- Cell testing
- Cell diagnostics

### ion Power

- SOA MEAs
  - 1. C-supported catalysts
  - 2. Novel catalysts

Mike Perry (Project) Rob Darling (Modeling) J.V. Yang (Experimental)

#### Stephen Grot

#### Tansel Karabacak

Novel catalyst

structures

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Core team has capability to lead modeling and fabricate key materials required

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# **Accomplishments & Progress**

### **Key Project accomplishments in Q1:**

- Completed sub-contracts (both done by 4/7/2017)
- Made progress on micro-structural CCL model
- Began to assess diagnostic methods at UTRC based on model cases
- Obtain MEAs from *Ion Power* and completed initial diagnostic testing in cells at UTRC
- Prioritized catalyst-architecture options with UALR
- Begin to engage appropriate FC PAD Consortia members
  - Assigned primary contact (R. Borup, LANL)
  - Completed FC-PAD SOW for this project
  - Obtained MEAs from LANL
  - Began to work with LBNL on modeling tasks

UTRC has recently begun to work with all of the project partners



**WE** United Technologies **Research Center** 





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### Technical Progress: Initial microstructure model has been developed

- CCL geometry depends on multiple factors:
  - Composition of the component materials (e.g., Pt/C wt%, Ionomer EW, I/C ratio)
  - Arrangement of these key components (e.g., agglomerate size, ionomer film distribution)



• **One possible arrangement** is an agglomerate structure with an outer shell of ionomer:

- For a assumed agglomerate size, can estimate number of C and Pt per agglomerate
- Can also estimate ionomer film and electrode thickness from I/C ratio
- These estimates can be verified with SEM and other electrode-characterization tools

UTRC has begun to construct and verify some microstructure CCL models



### **Technical Progress: Some Limiting Cases have been identified**

- Different transport-limiting mechanisms result in different limiting currents
  - Can make CCLs that help to probe these differences



Case 3



 $I_{L,1} = \frac{4F\varepsilon_b DPy}{\tau lRT} = \frac{4F\varepsilon_b (1-\varepsilon) DPy}{\tau RTL_{Pt}G(\omega,\gamma)}$  $I_{L,2} = I_f r_a = \frac{24FDHPyL_{Pt}G(\omega,\gamma)}{\delta d_a}$  $I_{L,3} = I_f r_{Pt} u_{Pt} = \frac{24FHDPy}{\tau_f \delta} \frac{L_{Pt}u_{Pt}}{\rho_{Pt}d_{Pt}}$  $I_{L,4} = I_a r_a = \frac{48FDcL_{Pt}G(\omega,\gamma)}{d_a^2}$ 

L<sub>Pt</sub> = amount of platinum in electrode, mg/cm<sup>2</sup> ω = mass fraction Pt in Pt/C catalyst γ = ionomer to carbon ratio by mass

		Limiting current varies as			
Case	Limiting transport through	$L_{Pt}^{n}$ , n=	G(ω,γ) <sup>n</sup> , n=	d <sub>a</sub> <sup>n</sup> , n=	d <sub>Pt</sub> <sup>n</sup> , n=
1	Electrode thickness in gas pores	-1	-1	0 < <i>n</i> < 1*	0
2	lonomer film, uniform consumption in agglomerate	1	1	-2	0
3	lonomer film, consumption near perimeter	1	0	-1	-1
4	Agglomerate	1	1	-2	0

\* The diffusion coefficient increases with agglomerate diameter.

UTRC has already begun to engage FC-PAD (LBNL) on modeling work



### **Technical Progress: Established relevance of Pt-only MEAs**

- Have utilized key results from previous DOE project to assess:
  - Best in-cell diagnostic techniques
  - Initial MEA compositions
- Comparison of Pt/Ni to Pt-only MEAs with ultra-low loadings:
  - Pt/C catalyst with similar catalystparticle size as Pt-Ni/C exhibit very similar mass-transport losses
    - Pt-only MEAs offer simple path for initial transport studies

BOL	#1 PtNi	#2 Pt (HSA)	#3 Pt
ECA (m²/g-Pt)	58	82	56
Mass activity (A/mg-Pt)	0.53	0.37	0.28

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**Project builds on UTRC's extensive modeling & diagnostics capabilities** 



iR-drop (V)

### Technical Progress: Initial Results with Ion Power MEAs

- Comparison with state-of-the-art (SOA) Pt-only MEA
- Ion Power MEA exhibited:
  - Similar Pt catalyst activity
  - Superior performance at low current densities
    - Higher catalyst loading
  - Lower *iR*-drop, but higher H2pump resistance
    - Indicative of lower protonconductivity in electrodes
  - Slightly lower limiting currents at low O<sub>2</sub> concentrations
    - Appears to indicate slightly lower oxygen-transport



current density (mA/cm<sup>2</sup>)

POL	B1240	B1286
BOL	<b>SOA Baseline</b>	IP MEA
Pt Size &	5-nm Pt	4-nm Pt
Loading	0.1 mg	0.3 mg
H2-Xover	4.5 mA/cm <sup>2</sup>	3.5 mA/cm <sup>2</sup>
Mass activity	312 A/g-Pt	304 A/g-Pt
H2-pump	$61 \text{ m}\Omega^*\text{cm}^2$	80 m $\Omega^*$ cm <sup>2</sup>

Very good initial result, some further work required to match SOA performance





### **Technical Progress: Non-Conventional Catalysts**

#### **Density-modulated Pt and Pt-alloy thin film electrocatalysts**

Tansel Karabacak's Group, University of Arkansas at Little Rock Collaboration with Deborah Myers' Group at ANL



Goal:

> Developing an ORR electrocatalyst with high performance and durability.

#### Approach:

- > High pressure sputtering (HIPS) to modulate the density of the thin film (TF) catalyst. Pressure change results in a change in porosity, density, and strain.
- High density bottom: Strong adhesion to the substrate leading to enhanced physical and electrochemical stability of the TF by preventing leaching of Pt at the bottom and the detachment of large regions of TF from the substrate.
- Porous top: Effective transportation of oxygen, improved catalyst utilization, reduced Ptloading, and enhanced ORR activity.

#### Preliminary results:

Electrochemical activity of Pt-TFs with different densities/porosities is shown. UALR will investigate the effect of density, thickness, strain, and crystal structure on the ORR activity.





Cyclic voltammetry curves of Pt-TFs with different densities after 3000 cycling between 0.05-1 V in N<sub>2</sub> saturated 0.1 M HClO<sub>4</sub>.

Phys./Chem. Stability



RDE profile of Pt-TFs with different densities in O<sub>2</sub> saturated 0.1 M HClO₄ at sweep rate 20 mV/s and rotation rate 1600 rpm.



Electrochemical activity of Pt-TFs with various densities \* Mass and specific activity of Pt-TFs are compared only for three films (19, 15 and 14 g/cm<sup>3</sup>).

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# **Proposed Future Work**

### Major goals for the next year of this project:

- Completion and validation of microstructural model using stateof-the-art MEAs with ultra-low catalyst loading (Pt/C)
- Use improved understanding of mass-transport loss mechanisms to improve CCLs & fabricate MEAs with improved performance

Milestone I.D.	Tasks	Task Title	Brief Milestone Description
Q1	1	Program Management	All subcontracts completed
Q2	3, 4	Carbon-supported MEA Fabrication	Demonstrate SOA performance at low PGM loading
Q3	2	Model development and validation	Microstructural electrode model framework complete
Q4 <u>Go/No-Go</u>	2	Model development and validation	Initial carbon-supported catalyst-layer model complete and validated with SOA MEA data
Q5	6	Novel catalyst MEA Fab	Fabricate thin-film graded catalyst
Q6 (2Q2018)	3, 4	Carbon-supported MEA Fabrication	Meet 2020 performance targets with high stoichiometric flow rates

Major focus in first year will be on MEAs/CCLs with conventional electrocatalysts



## **Summary**



- *Major barrier* to meeting DOE's 2020 MEA Targets is *mass-transport losses in CCL*
- Sources of these losses are currently not well understood
- This project should enable improved understanding
- Utilize this understanding to develop MEAs that meet all of DOE's performance targets
- Both conventional and thinfilm catalysts are included



- Raw in blue,
- Transport-corrected in red.

Develop MEAs w/ ultra-low catalyst loadings & minimal transport losses

## **TECHNICAL BACK-UP SLIDES**

### Technical Background: Non-Conventional Catalysts

**Fabrication Technique:** 

#### **High Pressure Sputtering (HIPS)**







#### **Technical Progress: Non-Conventional Catalysts**



#### Summary of electrochemical activity vs. porosity/density

Density (g/cm³)	Porosity %	Mass Activity (A/mg)	Specific Activity (µA/cm²)
21	4	-	-
19	9	0.023	1159
15	30	0.046	1311
14	36	0.034	1331

#### Additional Preliminary results:

- Electrochemical activity of Pt-TFs with different densities/porosities.
- UALR is currently investigating the effect of density, thickness, strain, and crystal structure on the ORR activity.





Make electrodes to probe model



 Fabrication of CCLs with sufficient differentiation to uniquely identify model parameters and/or sufficiently uniform ULCLs



- FC PAD Consortia has additional capabilities that can be used here
- LANL has already provided UTRC with ULCL MEA samples
- NREL also has MEA-fabrication capabilities
  - Thrust 2: "Electrode Layers" Coordinator: Shyam Kocha



Figure from: R. Borup, 2016 AMR: "FC-PAD Consortium Overview" (FC135)



# Key Risk



- Capability to *adequately characterize structures* for accurate input into the geometric models
- FC PAD Consortia has world-class capabilities that can be used here
- Especially valuable in assessing:
  - Ionomer-film dimensions and primary pore sizes & volume
    - Example: HAADF-STEM
  - Pt particle sizes and pore structures in thin-film catalysts
    - Ex: Electron Tomography



Figures from: K. More, 2016 AMR Presentation (FC020) showing ionomer dispersion in CCLs



# <u>Key Risk</u>

Non conventional catalysts

- Availability of *sufficient quantities* of alternative catalysts (e.g., thinfilm and/or nanoframe structures) to support the fabrication of MEAs by conventional techniques
- FC PAD Consortia has world-class capabilities that can be used here
- NREL has experience in fabricating MEAs with Thin-Film catalysts
  - Use MEA fabrication methods that work with relatively small quantities of catalysts
- ANL also has extensive capabilities to make alternative electrocatalysts
  - This is *not* part of FC-PAD Consortia, but is still a possible source of materials



#### "FC-PAD Consortia Overview" 2016 AMR (FC135)

Shyam.Kocha@nrel.gov



Figure from: V. Stamenkovic, 2016 AMR (FC140)

