



Novel Fluorinated Ionomer for PEM Fuel Cells

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Giner Inc.
Newton, MA

Project ID #
FC328

Project Overview

The logo for GINER, consisting of the word "GINER" in white capital letters inside a blue oval with a black border.

Timeline

- Project Start Date: 5/28/2019
- Project End Date: 5/27/2021

Budget

- Total Project Value: \$ 1 Million
- Spent: \$ 394k

Collaborators

- Compact Membrane Systems, Inc.
- University of Connecticut
- University of California Irvine

Barriers Addressed

- PEM fuel cell transport loss at low Pt and high power

Technical Targets

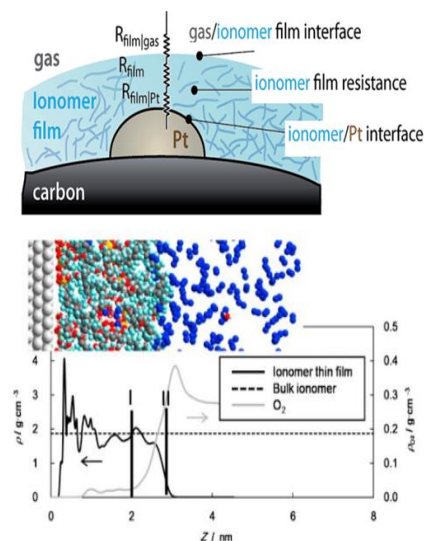
Develop next generation of fluorinated ionomers for PEM fuel cell cathodes to reduce local transport loss

- Improve O₂ permeability by 5x
- Increase polymerization scale by 10x per batch
- Evaluate fuel cell performance, durability and local transport resistance

Relevance

DOE Fuel Cell Catalyst Technical Targets

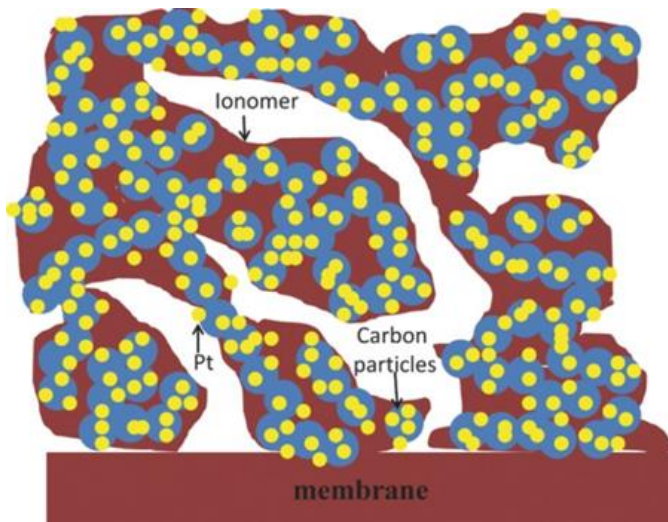
Characteristic	Units	2015 Status	2020 Targets
Platinum group metal total content (both electrodes) ^a	g / kW (rated, ^b gross) @ 150 kPa (abs)	0.16 ^{c,d}	0.125
Platinum group metal (pgm) total loading (both electrodes) ^a	mg PGM / cm ² electrode area	0.13 ^c	0.125
Mass activity ^e	A / mg PGM @ 900 mV _{IR-free}	>0.5 ^f	0.44
Loss in initial catalytic activity ^e	% mass activity loss	66 ^c	<40
Loss in performance at 0.8 A/cm ² . ^e	mV	13 ^c	<30
Electrocatalyst support stability ^g	% mass activity loss	41 ^h	<40
Loss in performance at 1.5 A/cm ² . ^g	mV	65 ^h	<30
PGM-free catalyst activity	A / cm ² @ 0.9 V _{IR-free}	0.016 ⁱ	>0.044 ^j



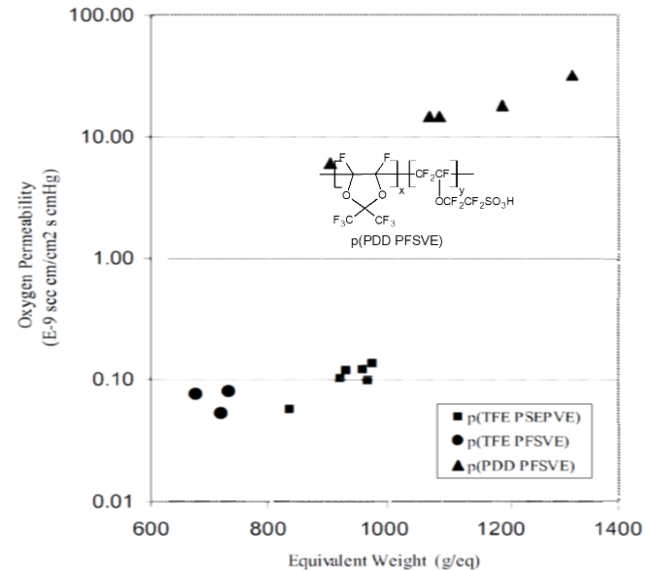
- **Electrode design is crucial to maximize the catalyst performance**
- Thin ionomer film formed in ultra-low Pt electrodes
- High local oxygen transport resistance due to thin ionomer film surrounding Pt particles
- Inferior performance at low-Pt loading due to local oxygen transport resistance

GOAL: Increase ionomer permeability to reduce local oxygen transport resistance

Approach



Cathode with ionomer layer

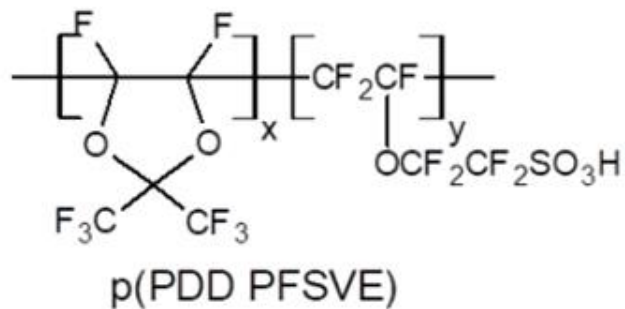


Dry O₂ permeability of PDD copolymers vs. p(TFE PSEPVE) "Nafion®" or p(TFE PFSVE) "Aquivion®"

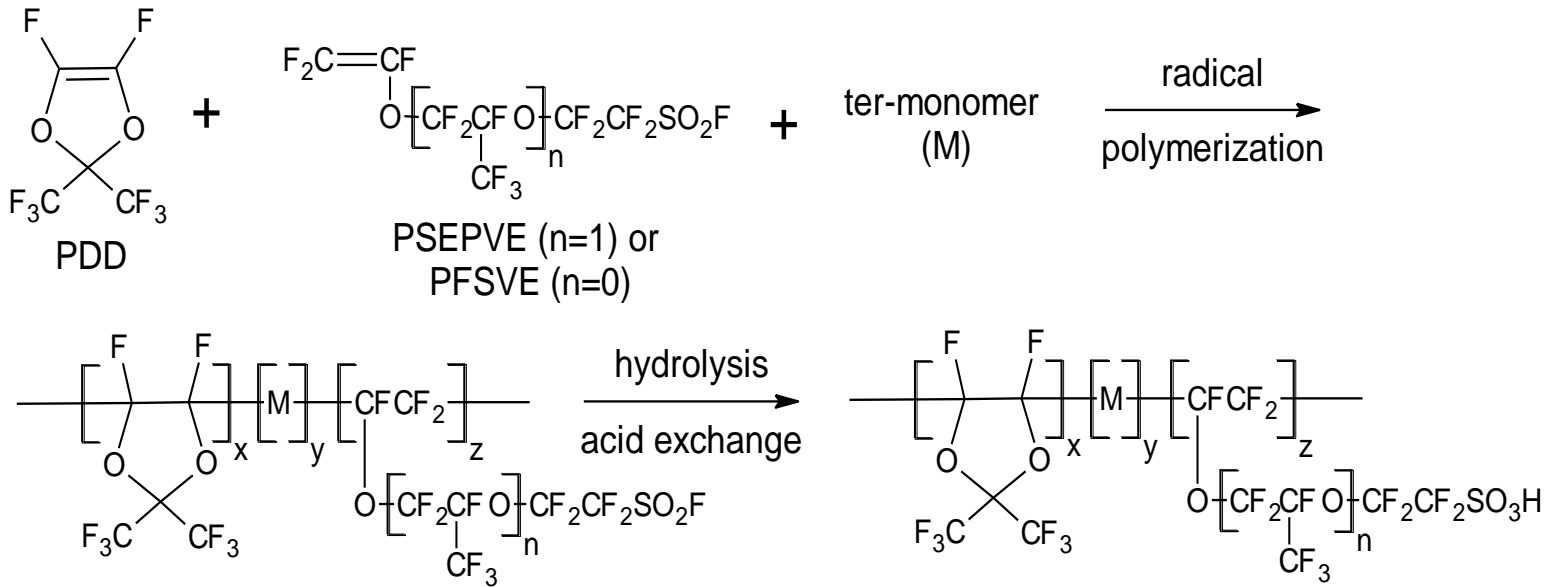
Amorphous ionomers (fluoropolymers) that are highly conductive like Nafion® but also have higher free volume may enhance oxygen permeance to the PGM catalyst and improve overall PEMFC cathode kinetics

GOAL: Higher ionomer oxygen permeability at lower equivalent weight

Fluoro-ionomers comprising perfluoro-2,2-dimethyl-1,3-dioxole (PDD) were known to have higher **dry** O₂ permeability from increased free volume imparted by the PDD repeat unit.



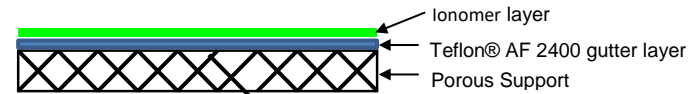
- Synthesize and characterize new fluorinated amorphous ionomers with varied composition, EW, and molecular weight
 - Measure humidified oxygen permeability
 - Measure ionomer conductivity
 - Perform fuel cell testing
- Scale up the most promising high-PDD content ionomer



Copolymerization of PDD, PFSVE (or PSEPVE), **and** a ter-monomer (M) for higher molecular weight (intrinsic viscosity) and better film-forming properties at low equivalent weight (EW)

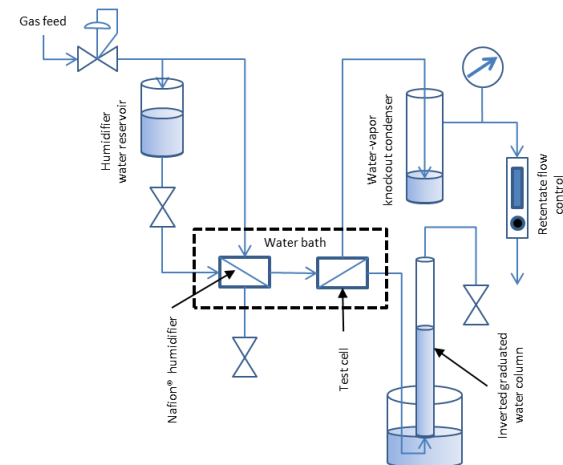
O₂ permeability from dilute solution casting on a high-permeance support to form a thin ionomer layer

- Thin ionomer layers (<5- μm) have realistically measurable gas fluxes over practical and manageable areas
- Gravimetric and helium permeability estimation of ionomer layer thicknesses
- Support + gutter layer resistance \ll ionomer layer resistance



Permeance testing design features

- Temperature-controlled water bath for consistent humidification ($\geq 95\%$ RH) and cell temperature
- Graduated and inverted water column for very low permeate-flow measurement by displacement

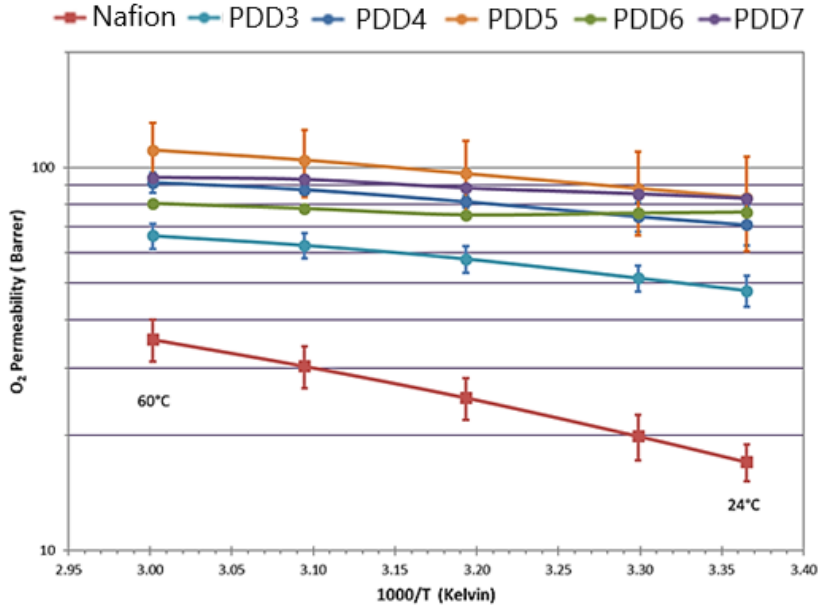


- Explored multiple variations of PDD content and equivalent weight
- Relative molecular weight (M_v) characterization through intrinsic viscosity (η) of copolymers prior to hydrolysis ($\eta \sim M_v^{0.5}$ in theta solvent systems)
- Equivalent weight measurement by titration after hydrolysis

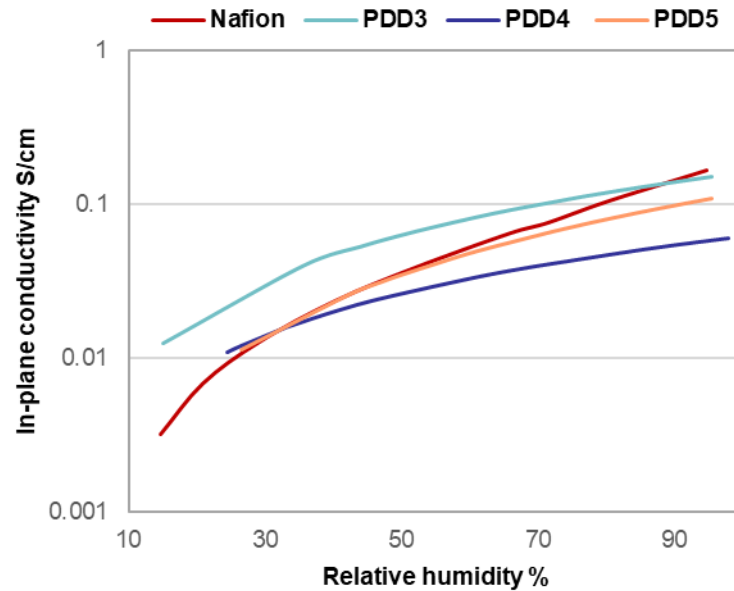
Ionomer	Composition	Estimated PDD content (mole%)	EW (g/mole)	Intrinsic Viscosity (dL/g)	O ₂ Permeability (Barrer)	
					24°C	60°C
PDD3	PDD/PFSVE/M	62 – 68	754	0.20	48	66
PDD4	PDD/PFSVE/M	67 – 73	863	0.31	71	91
PDD5	PDD/PFSVE/M	67 – 73	859	0.31	84	111
PDD6	PDD/PFSVE/M	70 – 76	953	0.20	77	81
PDD7	PDD/PFSVE/M	70 – 76	951	0.38	85	94
Nafion™ (control)	PSEPVE/TFE	0	930	n/a	17	36

High PDD content (low M) required for O₂ permeability significantly higher than Nafion™

Ionomer Permeability



Proton conductivity (80°C)

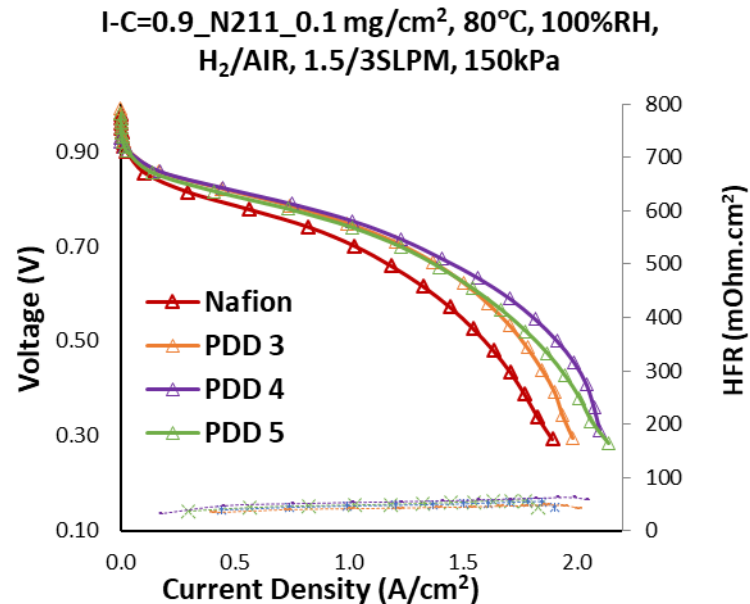
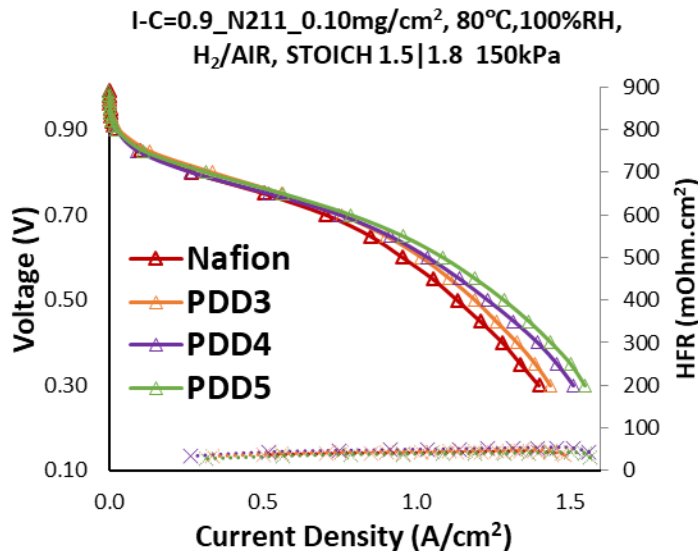


Permeability improvement vs Nafion

T (°C)	PDD 3	PDD 4	PDD 5	PDD 6	PDD 7
24	3x	4x	5x	5x	5x
60	2x	3x	3x	2x	3x

- PDD5, PDD6 and PDD7 display **5x** the permeability of Nafion
- PDD3 has higher conductivity than Nafion
 - Lowest equivalent weight

Accomplishment: PtCo/HSC Performance

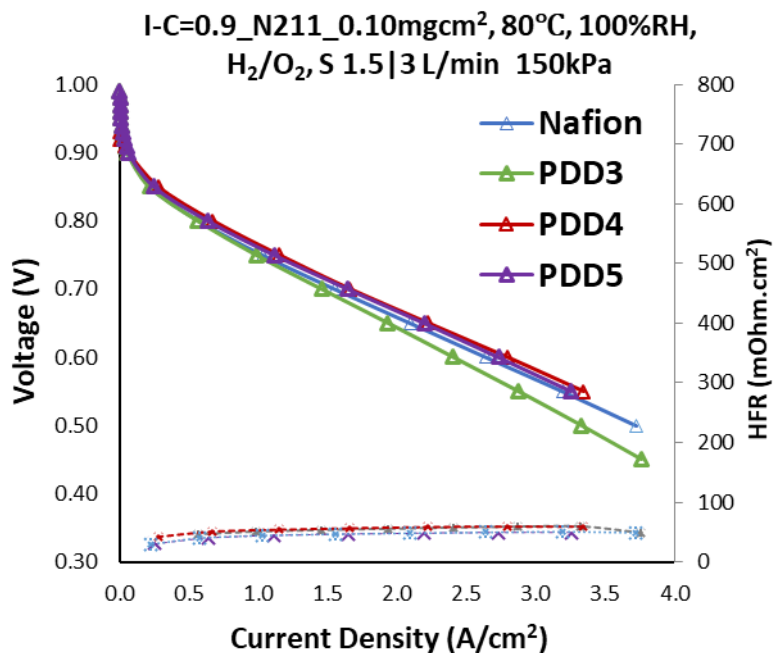


- All PDD MEAs outperform Nafion in the high current density region in good agreement with ionomer permeability values at 60°C
- MEA PDD5 has highest performance with stoichiometric flows; PDD5 has higher permeability & conductivity than PDD4
- MEA PDD4 shows highest performance with fixed flows; may be correlated with 10% higher secondary porosity
- MEA PDD3 has low high current density performance due to low EW = more SO₃⁻ groups attract water making ionomer swell and causing mass transport resistance

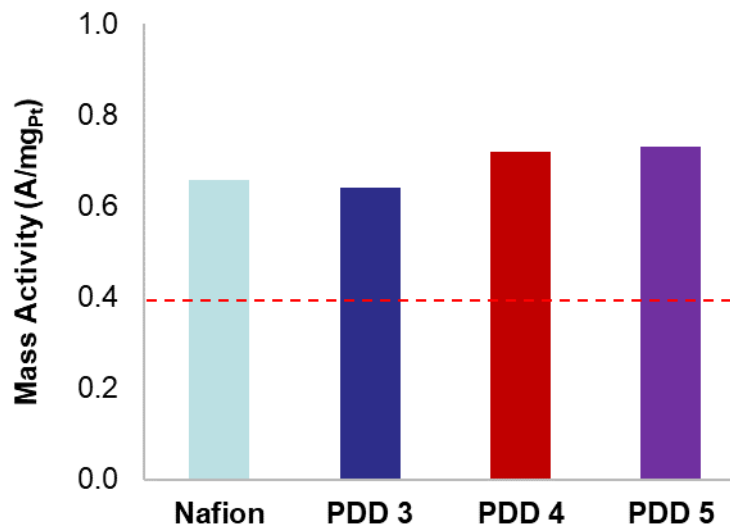
PtCo/HSC H₂/O₂ Performance and Mass Activity



25 cm² and 29BC SGL GDL

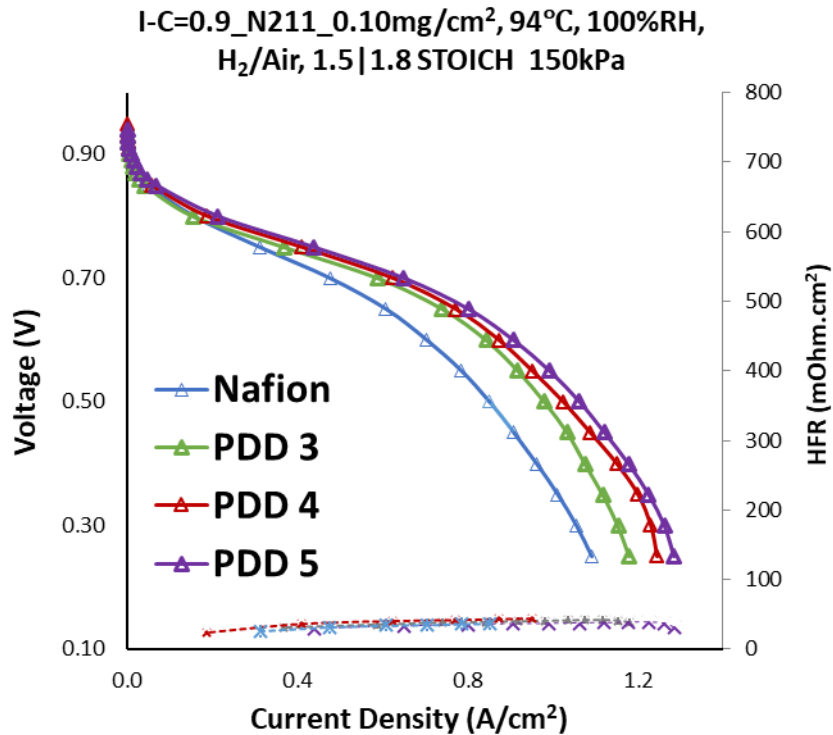


Mass Activity @ 0.9V IR Corr



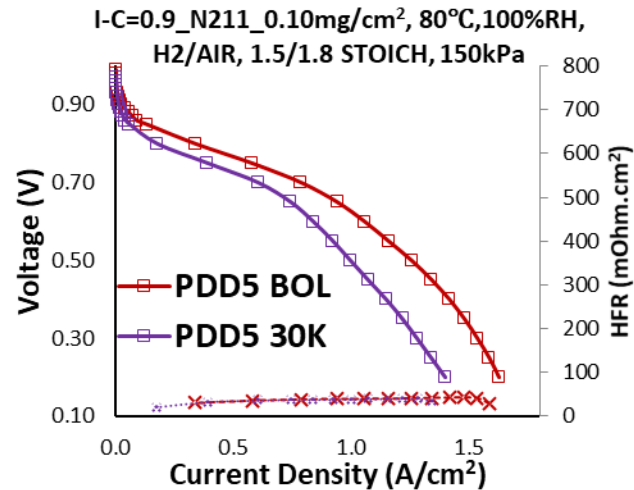
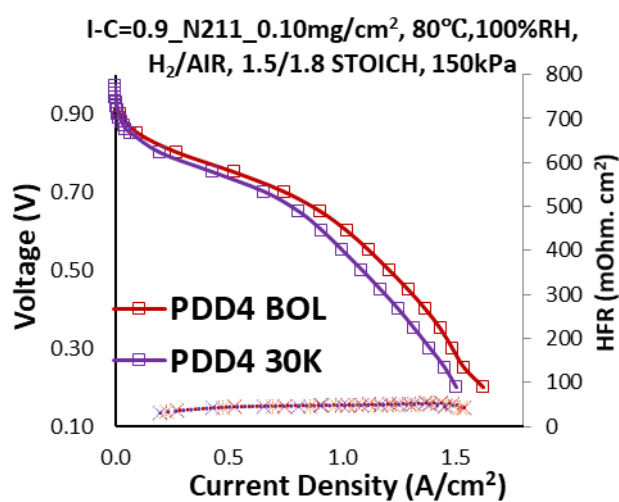
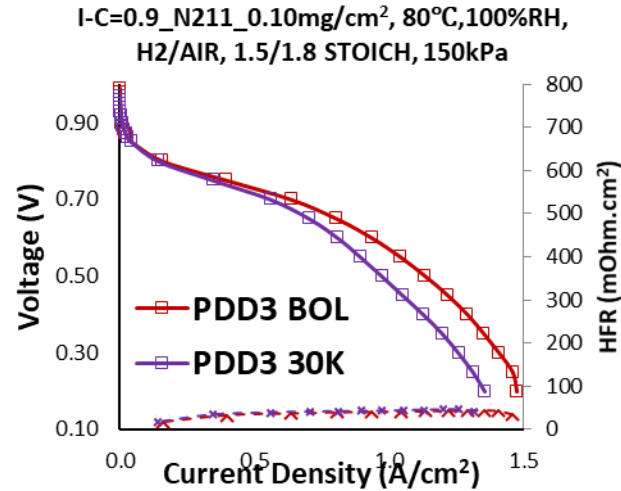
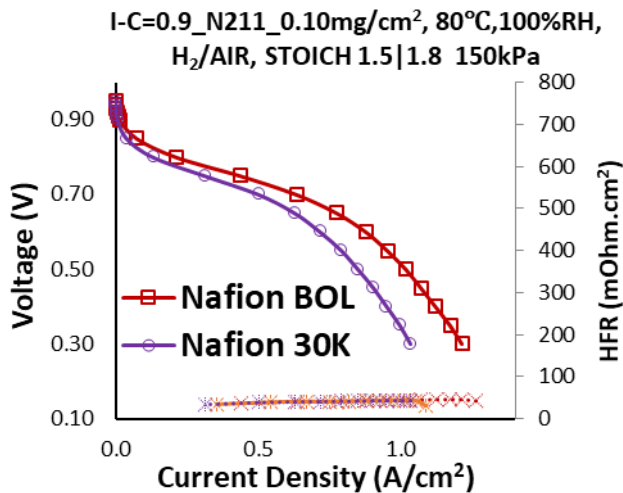
- MEAs **PDD4** and **PDD5** show improved performance in oxygen and higher mass activity vs. Nafion
- Differences in the triple phase boundaries, and Pt accessibility for O₂
- MEA **PDD3** has lowest MA and oxygen performance

PtCo/HSC 94°C 100% RH Performance



- MEA performance is worse at 94 °C than at 80 °C for all MEAs
 - Ionomers may have different water uptake capability in ionomer film at 94 °C than at 80 °C
- All PDD MEAs outperform Nafion MEA
 - PDD structure with bulky molecule in the backbone poses an advantage at high temperatures leading to even better performance of PDD MEAs vs Nafion MEA at 94 °C
 - PDD ionomers may hold more water due to lower EW
- At 94 °C MEA PDD5 performs better than MEA PDD4
 - Produced in different solvent (NPA vs IPA)
 - NPA dries faster than IPA
 - May have slightly different pore structure

PtCo/HSC Durability in 30K Square Wave AST

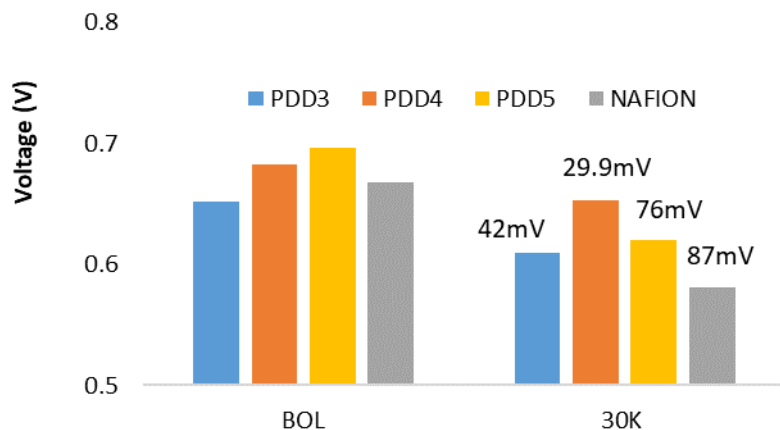


- **PDD4** MEA displays best durability
- MEA **PDD3** shows performance loss high current density region
- MEA **PDD5** shows performance loss in low and high current density region

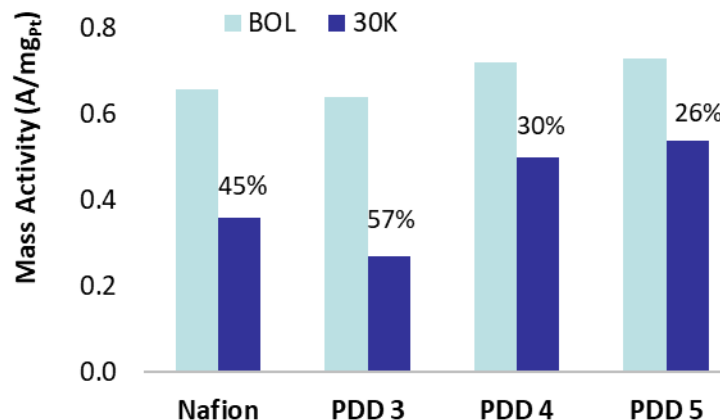
PtCo/HSC Durability w Nafion vs PDD



Voltage loss @ 0.8A/cm², 80°C, 100%RH, H₂/AIR,
STOICH 1.5|1.8 150kPa



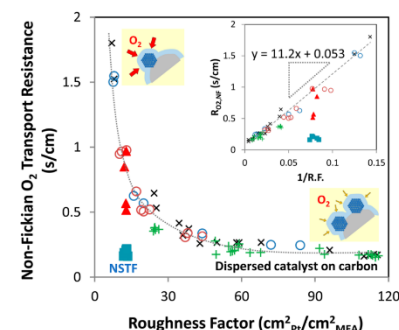
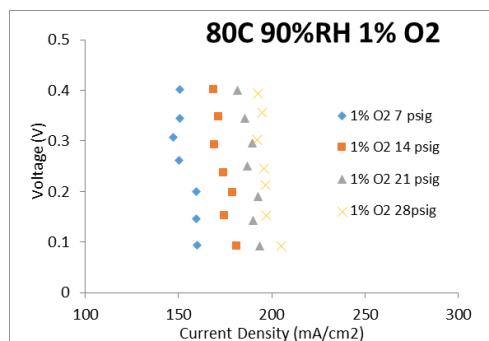
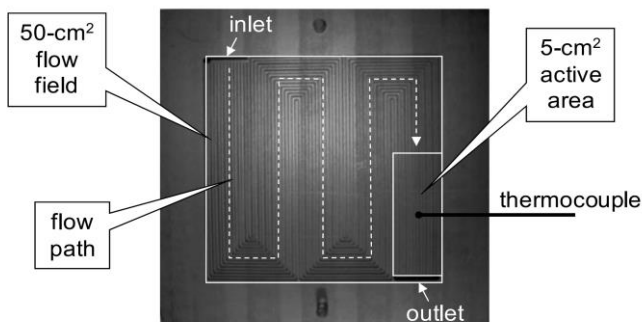
Mass Activity @ 0.9V IR Corr



- MEA **PDD4** displays **30 mV** performance loss 0.8 A/cm² meeting DOE durability target
- MEAs **PDD4** and **PDD5** meet DOE mass activity durability target < 40%
- MEA **PDD4** lost 86 mV at 1.5 A/cm² not meeting DOE target of < 30mV yet

Accomplishment: Isolate Local O₂ Transport Resistance

5cm² GM Differential cell



Baker et al, J. Electrochem. Soc. 156, B991 (2014)

- A limiting current approach was used to measure the transport resistance.

$$R_T = R_{Ch} + R_{DM} + R_{MPL} + R_{other}$$

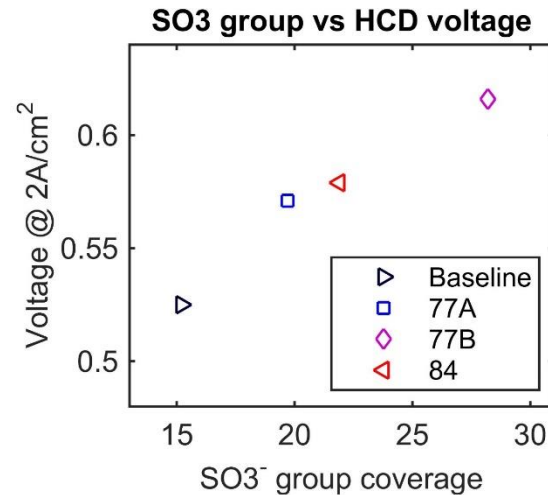
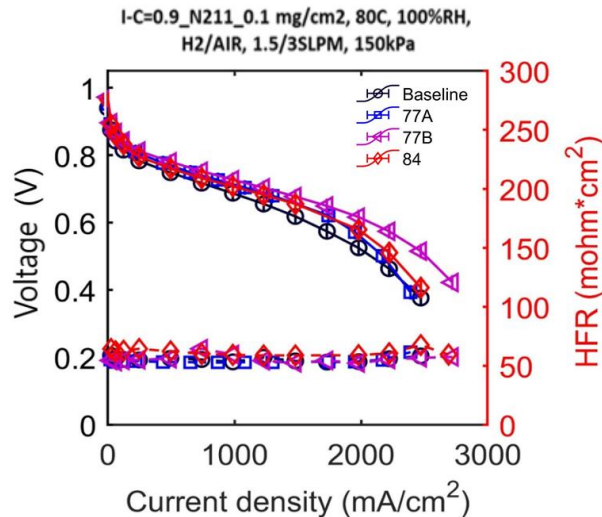
- 1%, 2% and 4% O₂ balanced with helium and variety in oxygen partial pressure was used to analyze the transport resistance from various sources
- Current densities at 0.2 V were used for local oxygen transport analysis

Pt/Vulcan	Nafion	PDD4
RO ₂ NF BOL (s/cm)	0.2096	0.0913

- PDD4** has **2x lower local O₂** resistance than Nafion
- Bulky PDD molecule may create void space for O₂ transport
- Absence of micropores in the carbon



Accomplishment: SO_3^- Group Coverage



- Calculated using charge transfer theory which is based on CO replacing the SO_3^- groups adsorbed on Pt particles

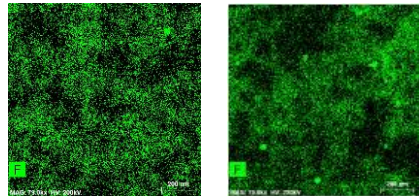
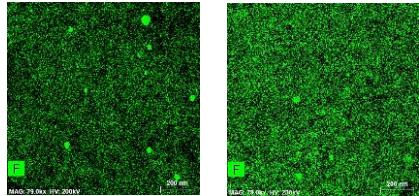
$$\theta_{\text{SO}_3^-} = \frac{2 \cdot \text{displacement charge}}{\text{stripping charge}} * 100\%$$

- SO_3^- group coverage should correlate with RO_2 local – ionomer backbone near Pt surface can block O_2 transport – also depends on number of mesopores vs micropores vs macropores because ionomer cannot enter micropores smaller than 2 nm Relevant for high surface area carbon
- Increasing SO_3^- group coverage correlated well with high current density performance – linked to RO_2 transport & hydration
- Nafion has higher EW than both PDD4 and PDD5 and therefore lower SO_3^- group coverage

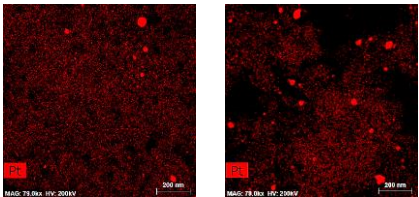
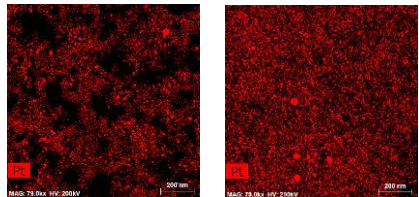
BOL = Beginning of Life

EOL = End of Life

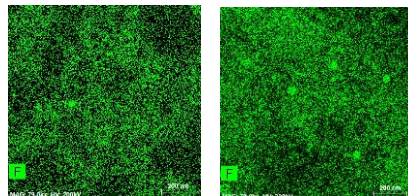
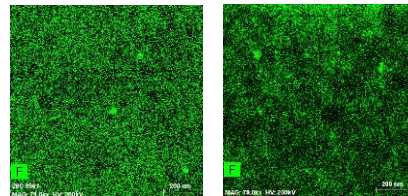
BOL → EOL



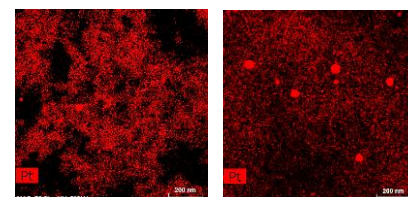
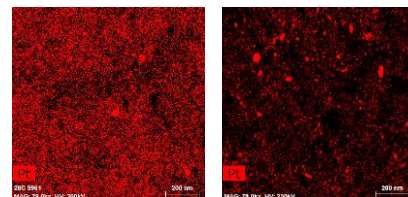
PDD3



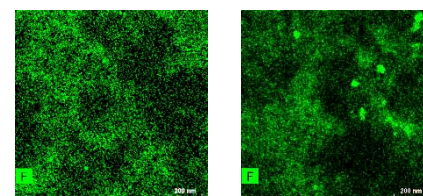
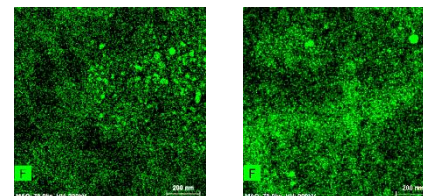
BOL → EOL



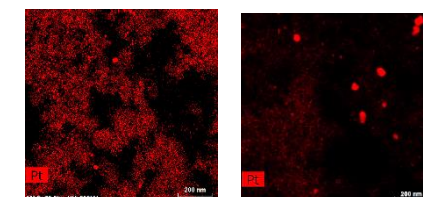
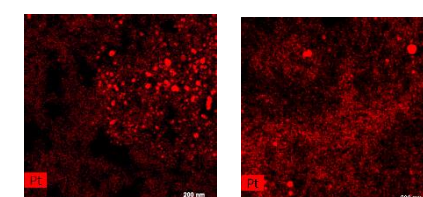
PDD4



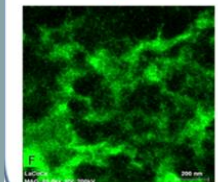
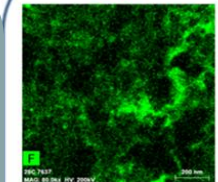
BOL → EOL



PDD5



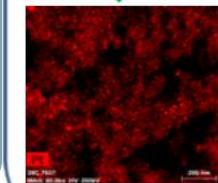
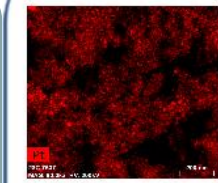
BOL



EOL

Nafion

BOL



EOL

- All MEAs have regions with non-uniform ionomer distributions at BOL and EOL
- Ionomer and Pt distributions become more agglomerated and non-uniform at EOL
- **PDD3** and **PDD5** display more visible agglomeration at BOL



MEA Microstructure Comparison



Sample ID	Primary porosity	Secondary porosity	Total porosity	Pt loading (mg/cm ²)	Pt/Co Atomic	Average Particle size (nm)	Co count
PDD3 BOL	37%	47%	84%	0.08	7.91	3.13 ± 1.07	0.008
PDD3 EOL	37%	45%	82%	0.05	14.48	4.63 ± 1.15 (+48%)	0.005 (-37%)
PDD4 BOL	25%	64%	89%	0.07	8.43	3.98 ± 1.25	0.007
PDD4 EOL	36%	47%	83%	0.05	16.99	4.43 ± 1.04 (+11%)	0.004 (-43%)
PDD5 BOL	28%	53%	81%	0.06	5.73	3.69 ± 1.31	0.01
PDD5 EOL	24%	44%	69%	0.05	14.11	4.72 ± 1.17 (+28%)	0.005 (-50%)
Nafion BOL	39%	45%	85%	0.1	6.3	6.25 ± 1.86	0.0326
Nafion EOL	39%	44%	83%	0.06	19.5	9.04 ± 3.93 (+45%)	0.015 (-53%)

- MEA **PDD4** has the highest secondary porosity of 64% and best performance
- MEA **PDD5** has the highest porosity loss
- MEA **PDD3** has the highest particle size growth and highest mass activity loss of 57%
- MEA **PDD4** has the smallest particle size growth and lowest mass activity and performance loss
- Cobalt leaching is evident from the increase in Pt/Co atomic ratio after degradation
- Nafion MEA lost the most cobalt from catalyst layer of 53% and has of 82 mV at 0.8 A/cm²

Collaboration and Coordination

The logo for GINER, consisting of the word "GINER" in white capital letters inside a blue oval with a gradient.

Giner (Lead): Hui Xu, Natalia Macauley, and Shirley Zhong: Oversee the project direction and progression. Electrode design and data analysis, and MEA commercialization.

CMS (Subcontractor): Dan Lousenberg. Synthesize ionomer samples and provide ionomer permeability data.

UCI (Subcontractor): Iryna Zenyuk. Analyze ionomer and SO_3^- group coverage, and O_2 transport resistance.

UConn (Subcontractor): Jasna Jankovic. Perform microstructure analysis with SEM and TEM.

Responses to Previous Year Reviewers' Comments

The logo for GINER, consisting of the word "GINER" in white capital letters inside a blue oval with a gradient effect. A horizontal blue line with a gradient extends from the left edge of the slide to the left side of the oval.

GINER

This project was not reviewed in 2019

Summary

- ❑ Novel PDD ionomers with 2-5x higher O₂ permeability than Nafion have been synthesized
- ❑ PDD ionomers show fuel cell performance and durability improvement compared to Nafion
- ❑ PDD ionomers show 2x lower local transport resistance than Nafion
 - DOE Mass Activity and Durability targets met with PDD Ionomers
- ❑ PDD ionomers in catalyst layers has more SO₃⁻ groups in contact with Pt than Nafion
- ❑ Microstructural analysis is in agreement with performance and durability results in porosity changes, Pt and Co loss

Future Direction

❑ Performance Improvement

- Use higher quality membranes from 3M
 - 15 μm supported membrane with doped Ce
 - 20 μm unsupported membrane
- Further optimize I/C ratio to better suit PDD ionomer
- Adopt advanced flow field and GDL

❑ Understanding ionomer durability

- Detect fluoride emission rate from ionomer during AST with ion chromatography by use of hydrocarbon membrane
- NMR: Fenton's test to identify ionomer breakage point

❑ Evaluate MEAs by OEMs and FC-PAD

- Send 50-100 cm^2 MEAs with best ionomer
- Extensive and harsh FC vehicle operation conditions (Transients, Sub-freezing operations)
- FC-PAD for ionomer/MEA evaluation

❑ Commercialization Strategies

- License ionomer technology to provide products to fuel cell and other community
- Utilize CMS ionomer for Giner's products

Any proposed future work is subject to change based on funding levels

Acknowledgments



- ❑ Financial support from DOE SBIR/STTR Program under award DE-SC001859

- ❑ Technical Manager
 - Dr. Dimitrios Papageorgopoulos

- ❑ Collaborators
 - Jasna Jankovic (Univ. of Connecticut)
 - Iryna Zenyuk (Univ. of California, Irvine)
 - Hannah Murnen and Dan Lousenberg (CMS)
 - General Motors (flow field to measure local O₂ transport resistance)