

# 2007 DOE Hydrogen Program Review

## MEA & Stack Durability for PEM Fuel Cells

3M/DOE Cooperative Agreement  
No. DE-FC36-03GO13098

Project ID # FC10



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3M Company  
May 16, 2007



# Overview

## Timeline

- 9/1/2003 – 12/31/2007
- 90% complete

## Budget

- Total \$10.1 M
  - DOE \$8.08 M
  - Contractor \$2.02 M
- Funding received in FY06: \$1.895 M
- Funding (estimated) for FY07: \$1.604 M

## Barriers & Targets

- Durability:
  - Demonstrate: 2k hrs
  - Target: 40k hrs

## Team Members

- Plug Power
- Case Western Reserve University
- University of Miami

## Consultant

- Iowa State University

# Objectives

Develop a pathway/technology for stationary PEM fuel cell systems to meet the DOE's 2010 objective of 40,000 hour system lifetime.

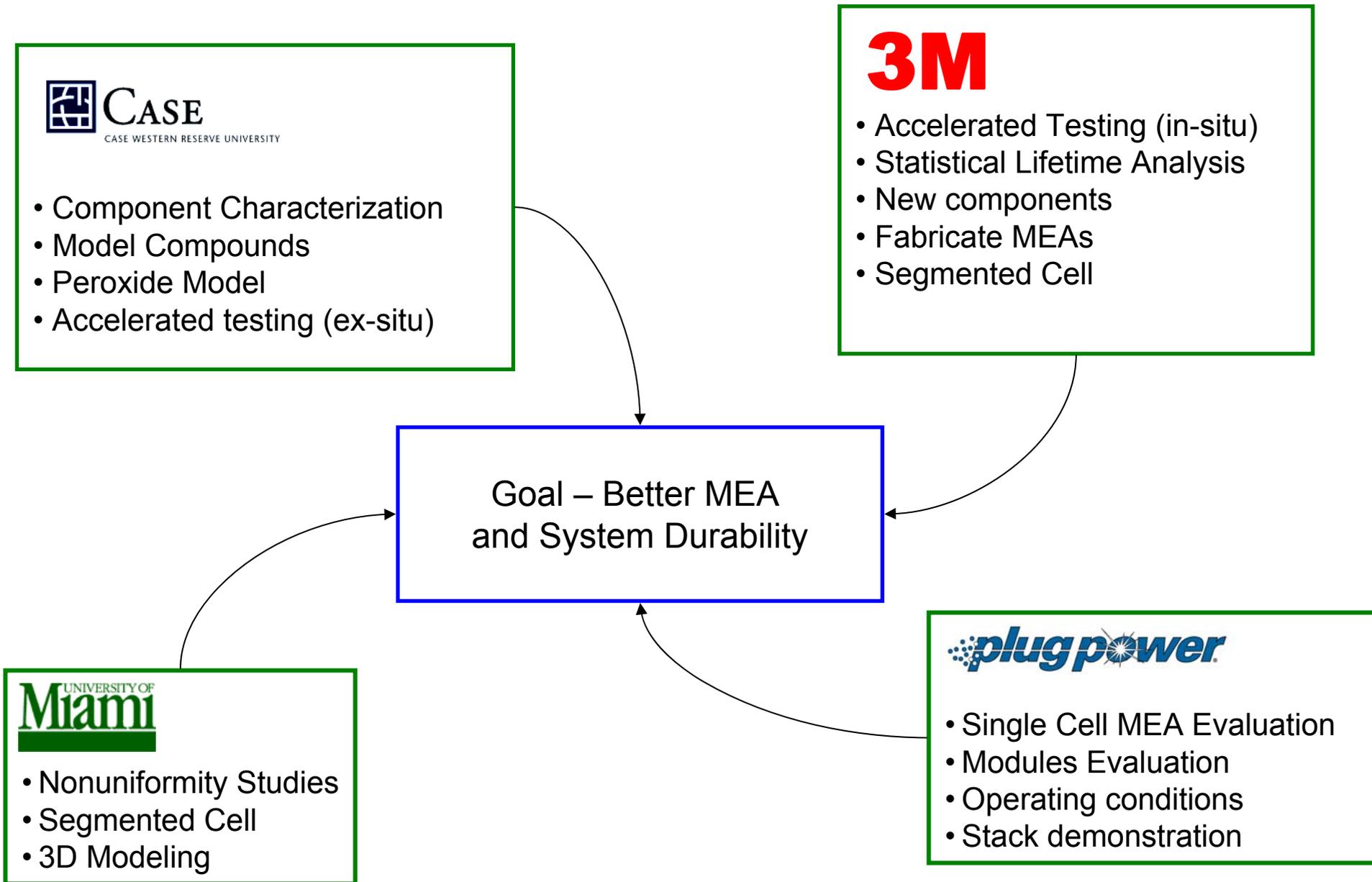
**Goal:** *Develop an MEA and System with enhanced durability*

- Manufacturable in a high volume process
- Capable of meeting market required targets for lifetime and cost
- Optimized for field ready systems
- 2,000 hour system demonstration

## **Focus to Date**

- MEA characterization and diagnostics
- MEA component development
- MEA degradation mechanisms
- MEA nonuniformity studies
- Hydrogen peroxide model
- Defining system operating window
- MEA and component accelerated tests
- MEA lifetime analysis
- Stack testing with intermediate developments
- Final Stack Demonstration Started

# Approach



# Accomplishments ('07)

## Membrane Degradation Mechanism

- Utilized ionomer model compounds to identify likely 'points of attack' and confirmed degradation pathway
- Developed initial hydrogen peroxide model to study peroxide in operating fuel cell

## GDL Characterization

- Demonstrated new test equipment to measure capillary pressure in GDLs

## MEA Nonuniformity Studies

- Utilized 121-channel segmented cell to investigate current uniformity as a function of load setting, flow rate and flow configuration.
- Completed a series of durability experiments with segmented cell
- Segmented cell fabricated to run in full stack

## Membrane

- Developed film edge protection technology
- Ongoing monitoring of membrane properties in accelerated tests

## MEA Lifetime Modeling

- Developed initial lifetime prediction model to estimate MEA lifetime relative to DOE's 2010 stationary system goals
- Related initial fluoride ion to lifetime

## System Test

- Ongoing Saratoga system test with a preliminary, durable MEA design
- Initiated 'Final' MEA and system test

# Membrane Degradation Model

**Objective** – Predict degradation pattern and Fluoride release rate

## Source terms:

- $H_2O_2$  production rate from  $O_2$  x-over
  - ORR side reaction
- } well-known from previous work

## Reaction terms:

- $H_2O_2$  decomposition rate in electrodes (Multidecker sandwich cells)
- peroxide reaction rate with PFSA (Model compounds w/kinetic analysis)

## Transport Terms:

- $H_2O_2$  diffusion rate through each MEA component (GDL, CL, membrane) (Multidecker sandwich cells)

$$\begin{aligned} \frac{d}{dt}(C_{H_2O_2}) = & \text{Rate of production (electrochemical + Chemical recombination)} \\ & + \text{Rate of consumption} \left( \begin{array}{l} \text{Ionomer degradation + catalytic disproportionation} \\ + \text{electrochemical reduction} \end{array} \right) \\ & + \text{Transport through the electrode (Diffusion + Convection)} \end{aligned}$$



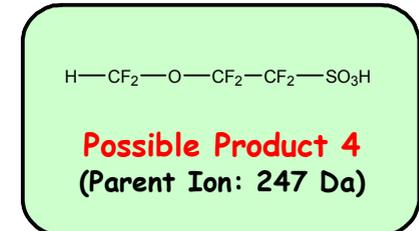
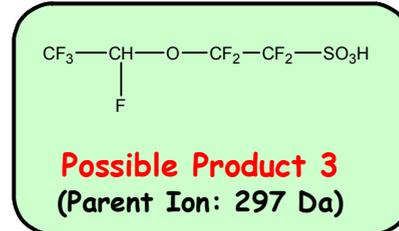
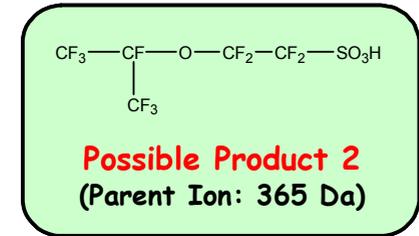
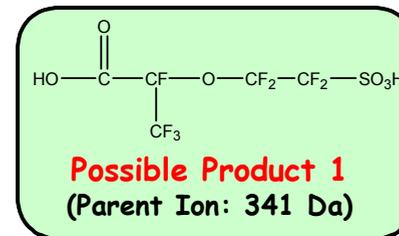
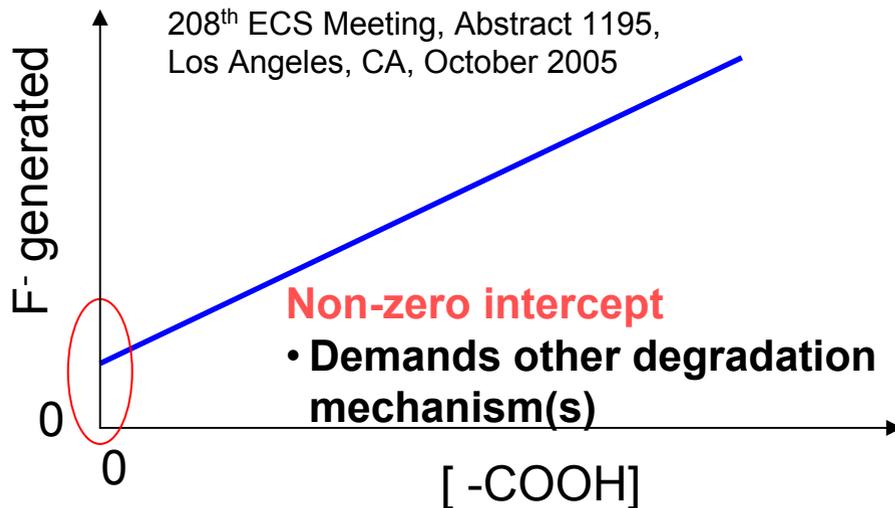
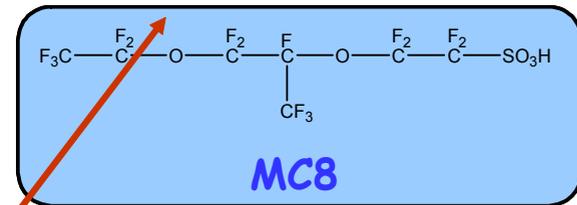
# Model Compound Studies

## LC-MS System



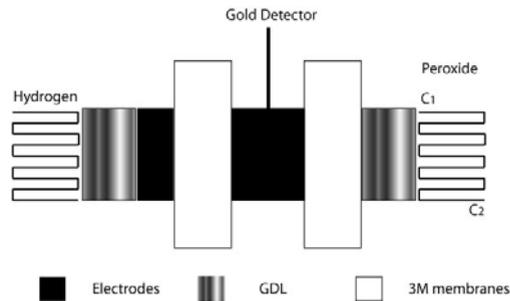
Peroxide degradation

“Side chain” cleavage appears to occur with the model compound



# H<sub>2</sub>O<sub>2</sub> Transport and Reaction Processes

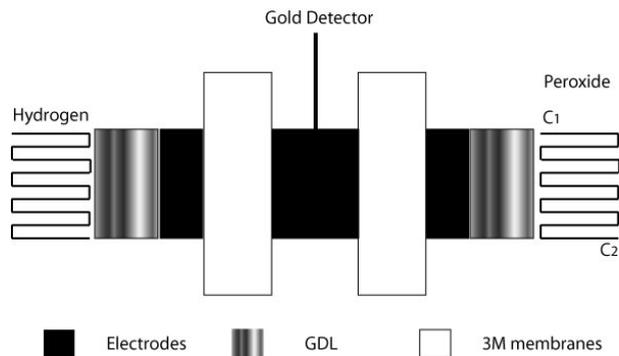
## Half MEA Setup



### Allows us to measure:

- H<sub>2</sub>O<sub>2</sub> diffusion through GDL layer
- Diffusion+Reaction(?) through the membrane
- $I_d$  --- for H<sub>2</sub>O<sub>2</sub> redox at center electrodes

## Full MEA Setup



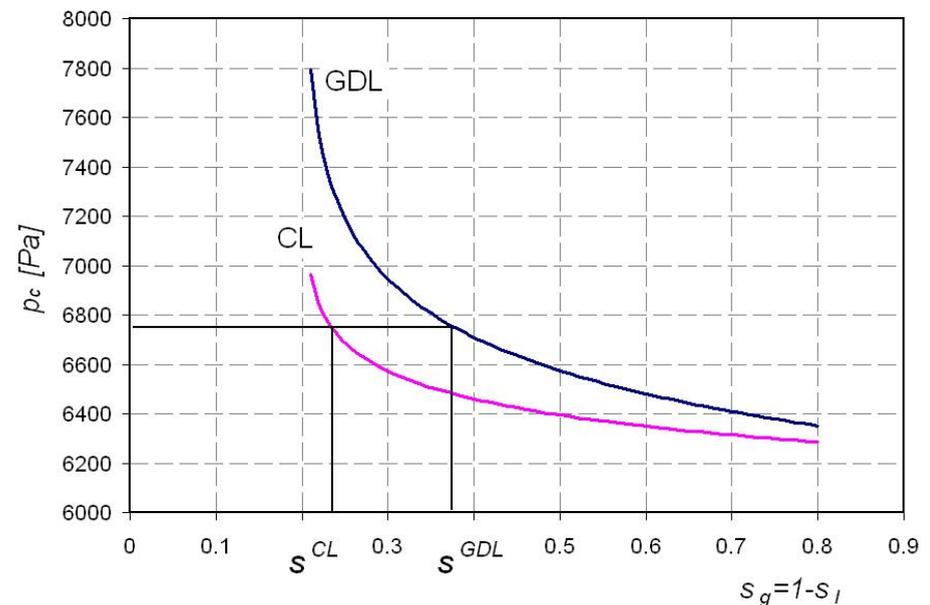
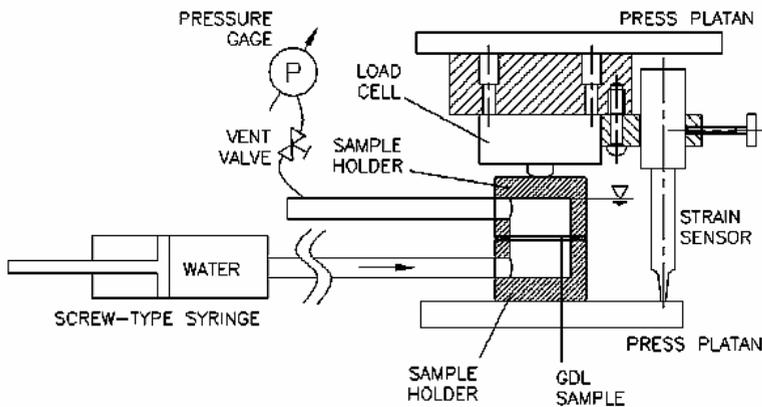
### Allows us to measure:

- Mass transfer through GDL
- Mass transfer+disproportionation through catalyst layer

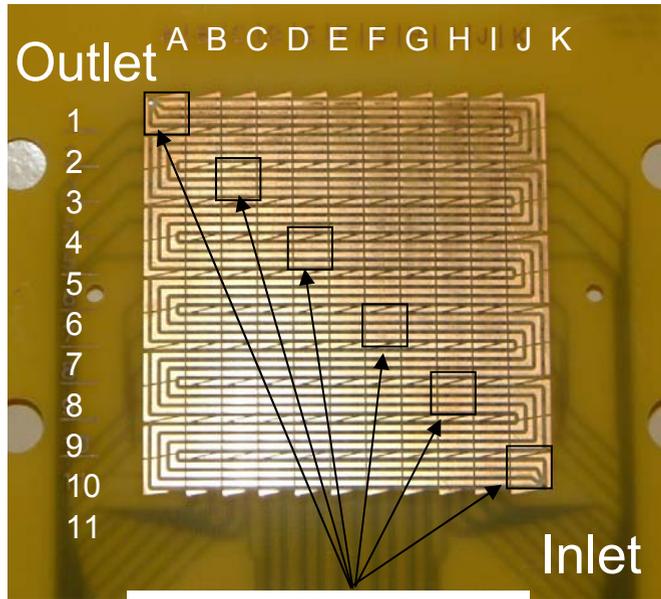
# GDL Characterization – Capillary Pressure

## Motivation:

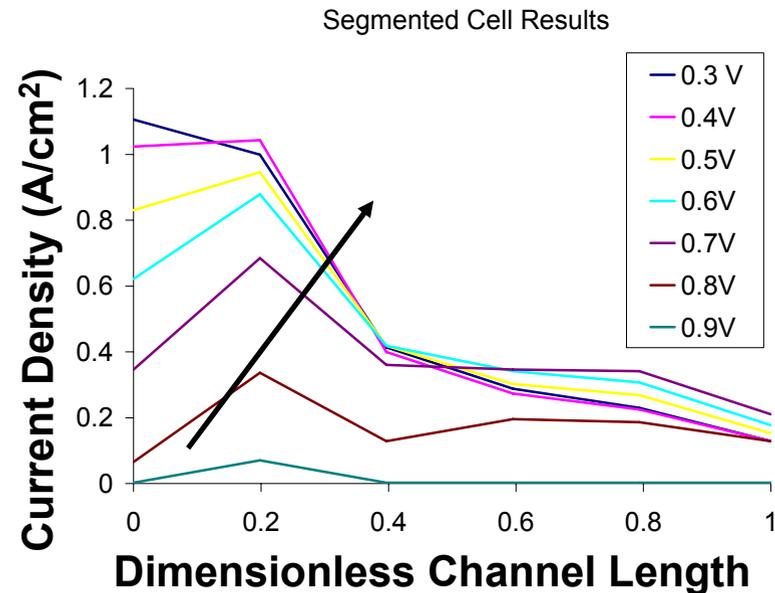
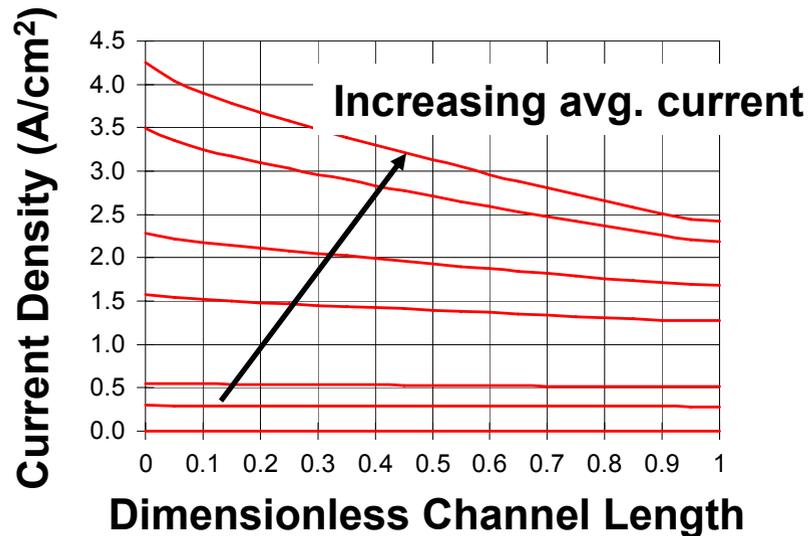
- Inherently, catalyst layers lack the flexibility to control the amount of water that resides in its pores during fuel cell operation;
- GDLs may be designed to promote or inhibit water flow out of the catalyst layer pores; to achieve this, one needs to be able to assess the capillary pressure as function of water saturation  $P_c(s)$  in the GDL;



# Segmented Cell - Update

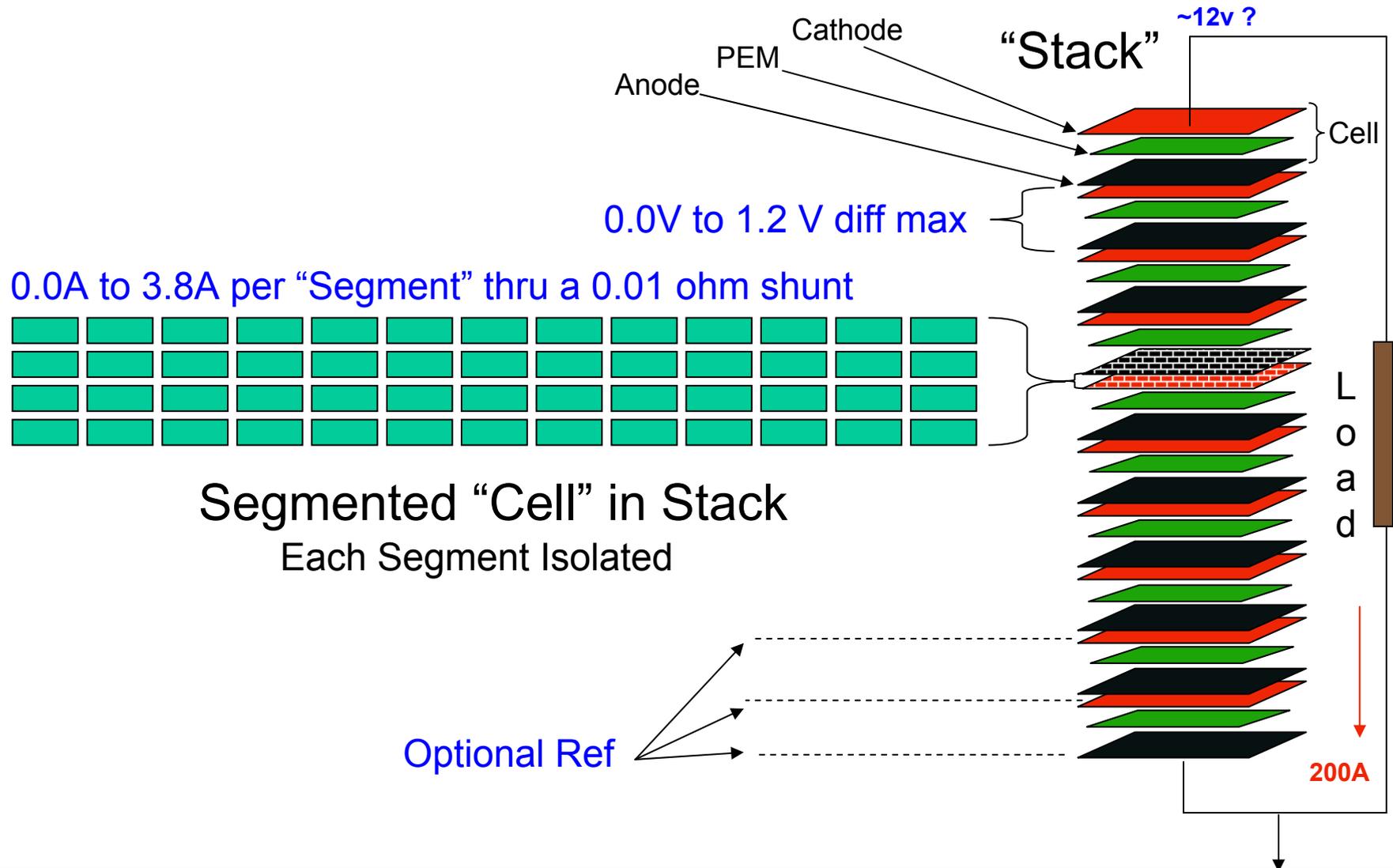


- Recently completed 121 channel load
- Cell design validated
- Design fuel cell systems to operate at high stoichiometry for uniformity
- Cell for Plug Power under fabrication



# Segmented Cell for GenSys Stack

**Objective** – Study cell uniformity in real system. Optimize operating parameters for performance and durability



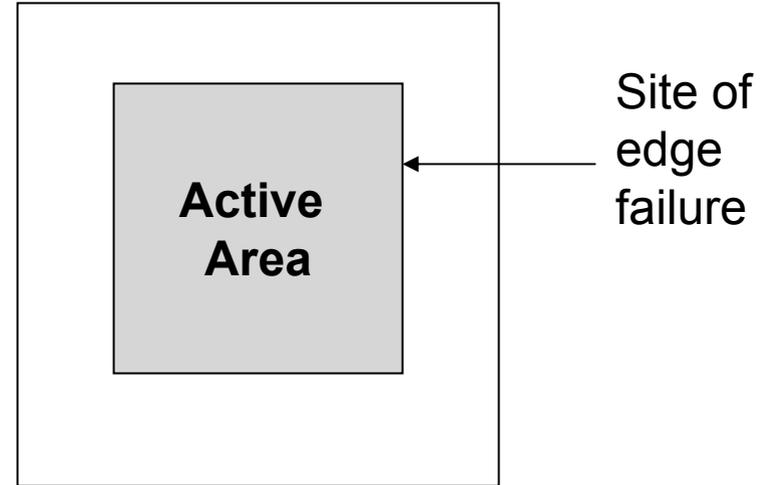
# Film Edge Protection

## Problem

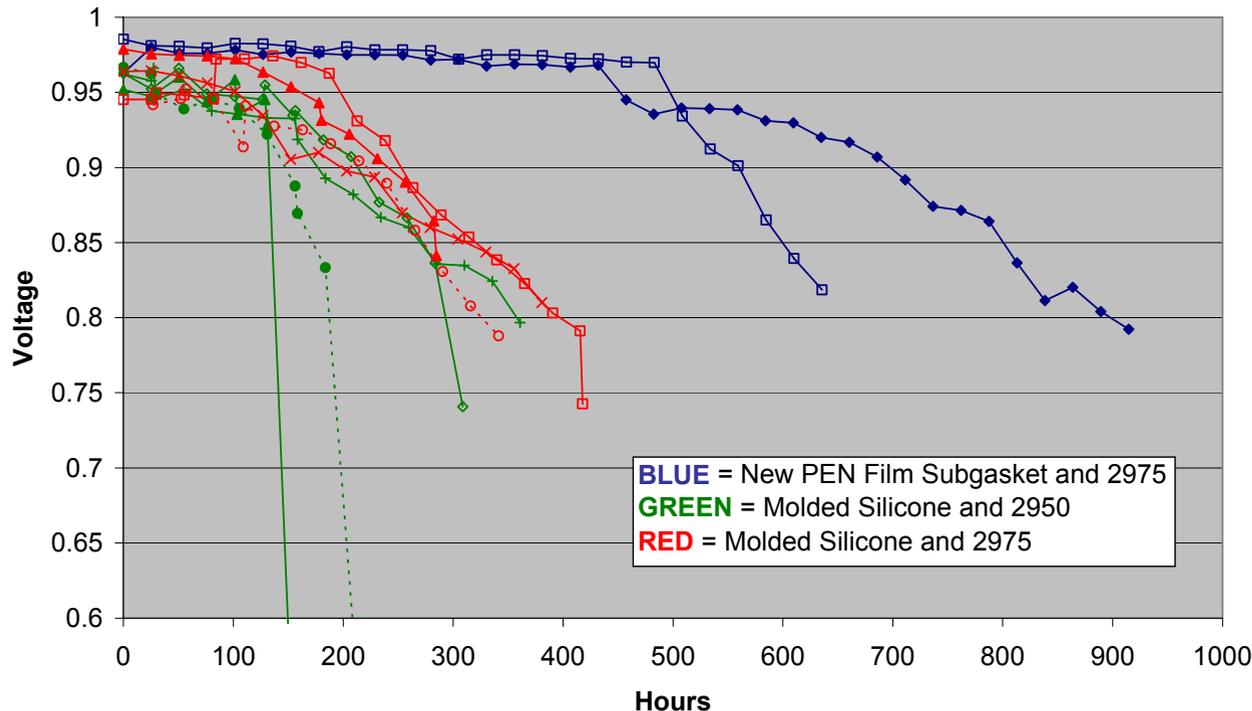
- In module testing, observe infant mortality of MEAs due to edge failure at the membrane – catalyst interface

## Solution

- Developed edge protection component for MEA

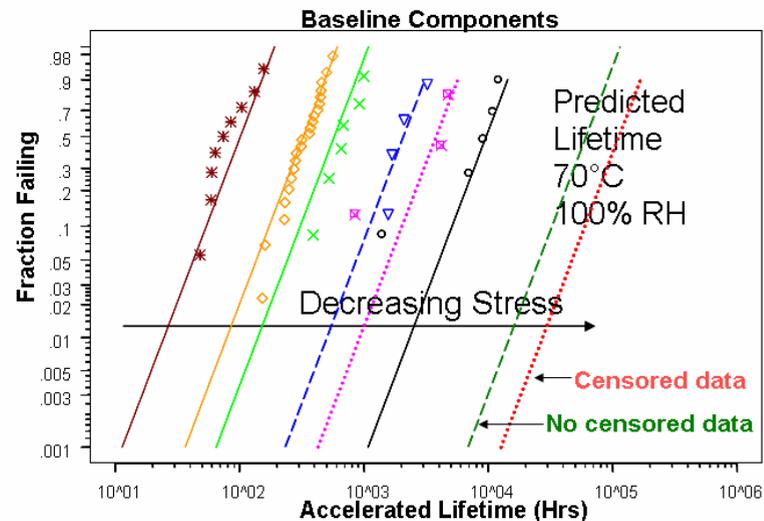
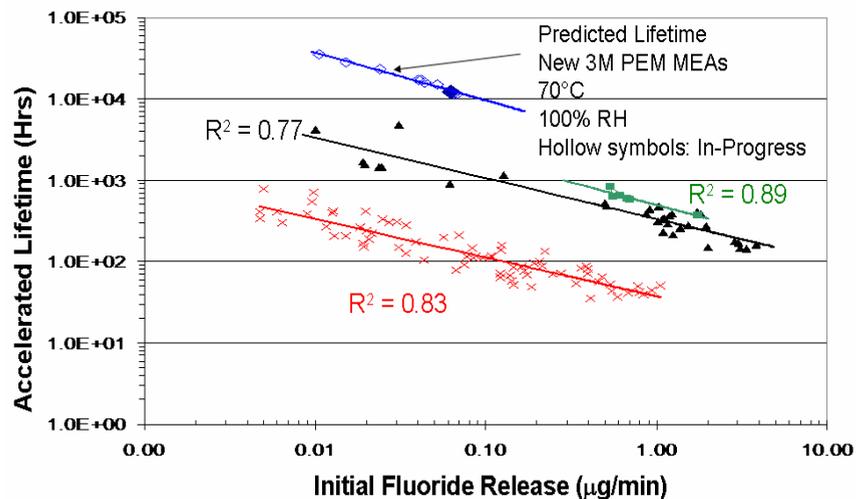


Gasket Comparison  
New Film Subgasket with Overlap GDL VS Silicone Molded Gaskets



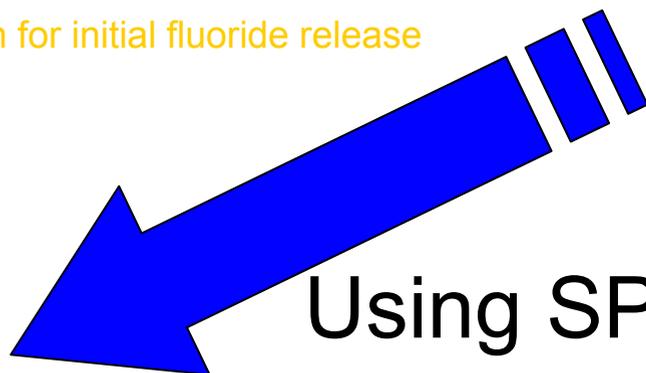
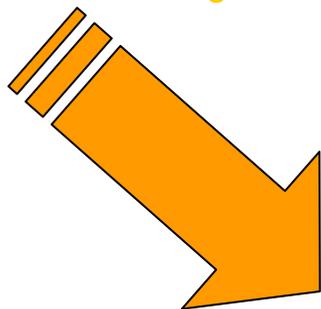
- Identified MEA failure mode
- Increased Lifetime Observed in Accelerated tests
- Reduced infant mortality in non-accelerated tests

# Combine Fluoride Ion Mapping and Statistical Lifetime Modeling



## Fluoride Release and Lifetime Correlation

- Uses Strong correlation for initial fluoride release



## SPLIDA Statistical Modeling Using

- Lognormal distribution
- Arrhenius for temp
- Humidity model for RH

## Using SPLIDA Software

### Unified Prediction Equation

$$Lifetime = \frac{A}{T + 273} + H * LN\left(\frac{RH}{100 - RH}\right) + F * LN(FRR) + I$$

Where:

- A = Arrhenius Constant
- H = Humidity Constant
- F = Fluoride Release Constant
- I = Intercept

\* Load cycle differences not included yet

# Statistical MEA Lifetime Model Unified Equation

## Equation Predictions

Conditions	Fluoride Release	Equation Prediction Lifetime	95% Lower Confidence Interval	95% Upper Confidence Interval	Actual Lifetime
90°C 30%RH	0.46	63	56	70	56
90°C 44%RH	1.11	329	291	372	347
70°C 93%RH	0.04	11,314	9,272	13,817	10,984
90°C 93%RH	0.50	5,633,891	1,079,697	29,410,394	Not Run

Predictions reasonable within oval design space

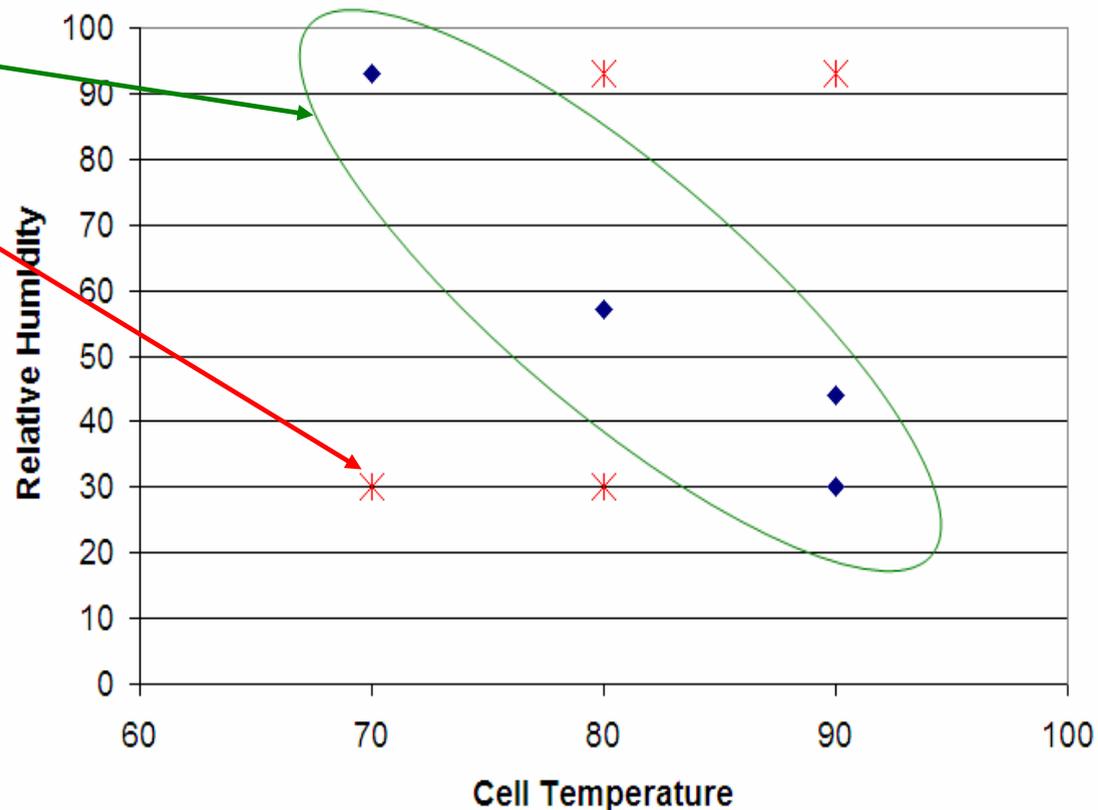
Predictions unreasonable due to poor temperature correlation

### Unified Prediction Equation made by SPLIDA Software

- Reasonable predictions for data within design space that has been tested
- Unreasonable predictions outside the design space due to inaccurate temperature dependence
- Need data at different temperatures with same RH

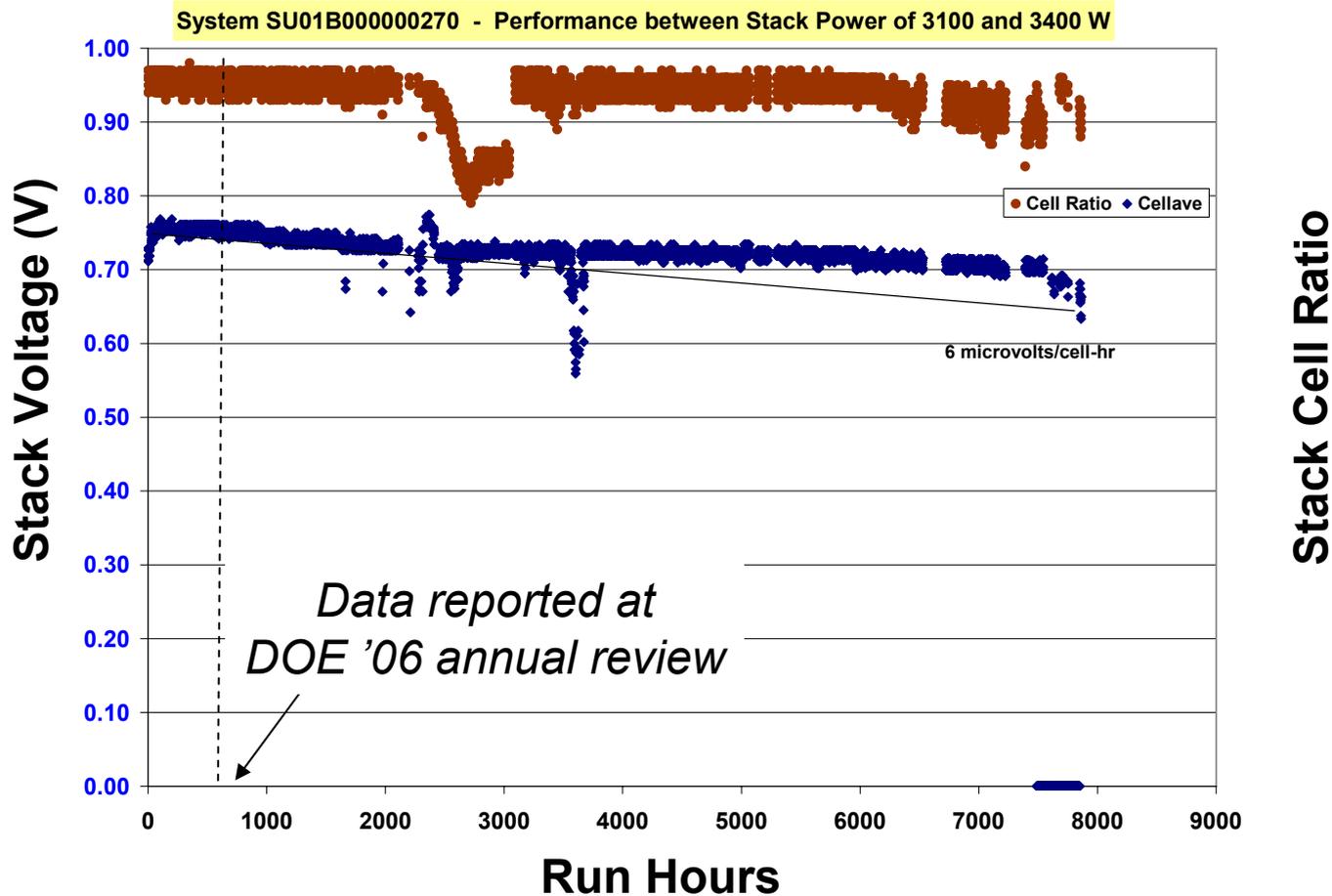
### Fuel Cell Conditions Model Design Space

- ◆ Conditions Tested Within the Model
- ✖ Conditions Not Tested (Want to Predict Lifetimes)
- Design Space



# DOE4 MEA in SU1 System

**Objective** – Demonstrate Intermediate advances

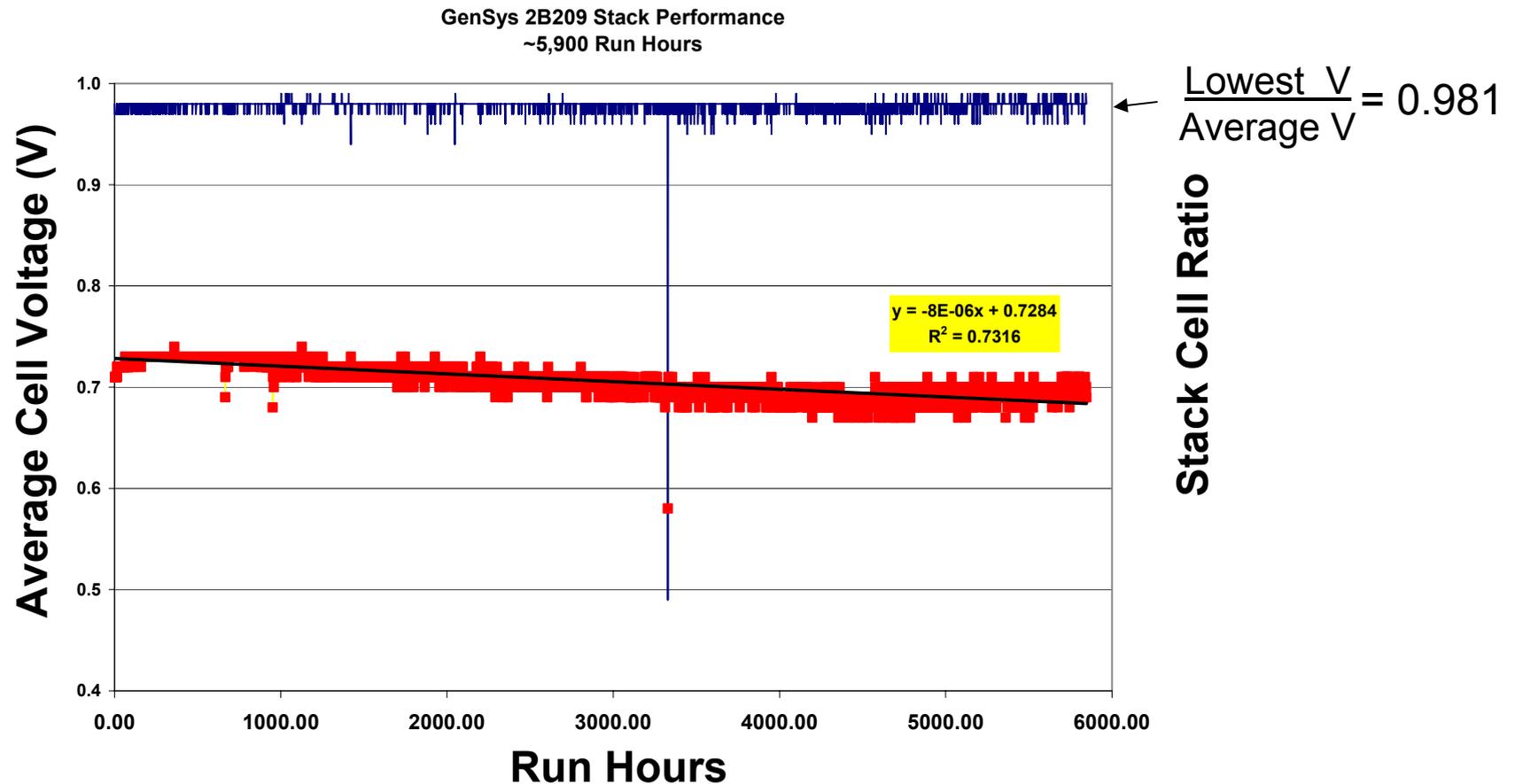


- New Membrane
- New Catalyst
- New GDL
- First Generation System



# DOE4 Membrane in GenSys System

**Objective** – Demonstrate Intermediate Advances



- New Membrane
- Improved System
- First Generation Catalyst
- *No low cell shut downs*
- *No maintenance for 257 consecutive days*



# DOE4 MEA in Final GenSys System

**Objective** – Demonstrate Final Components and System for 2,000 hours per statement of work

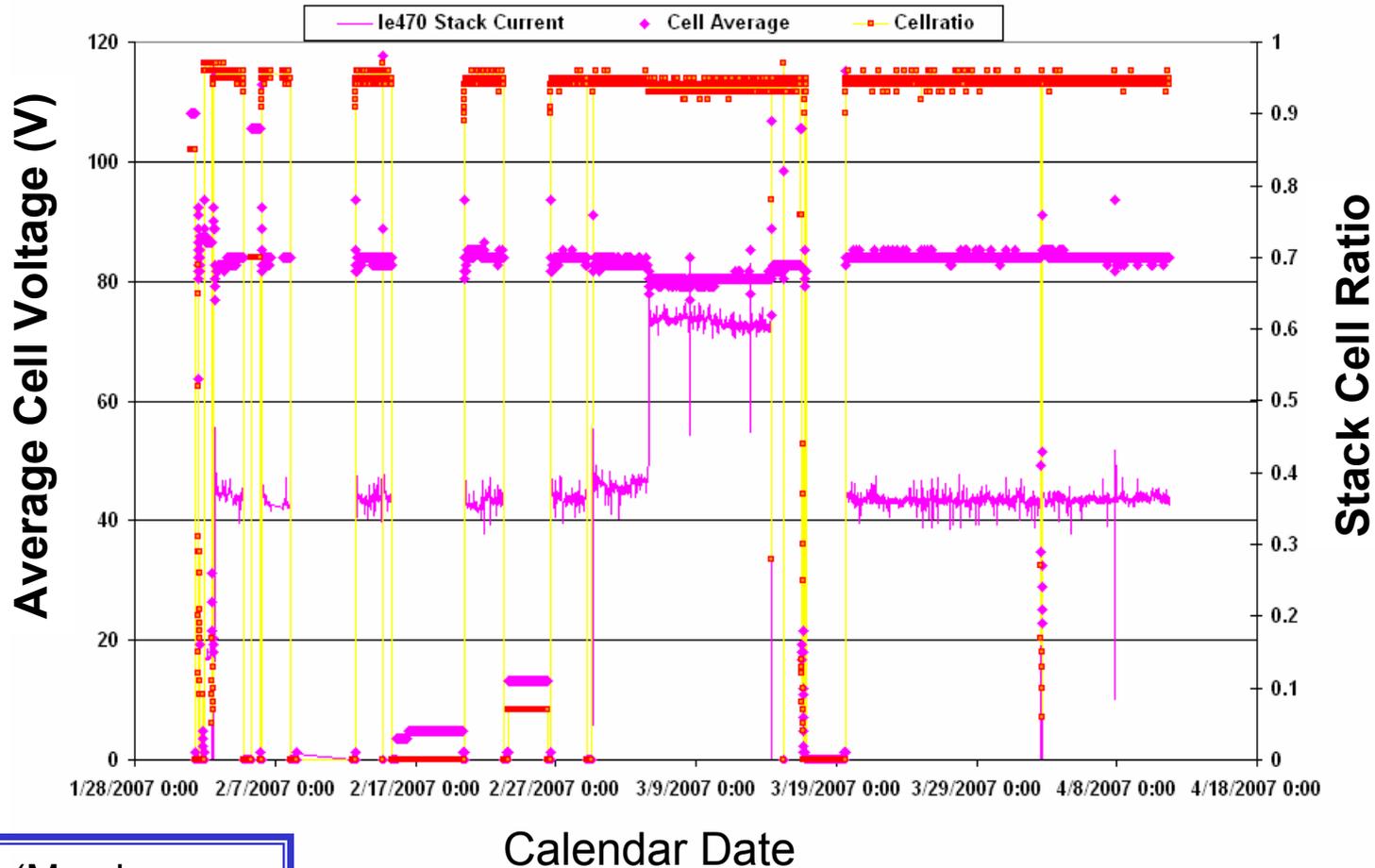
- Installed DOE Final 4 stack in GenSys Unit 2B304 on 2/1/2007.
- Total stack hours as of 3/31/2007 = 996 hrs (3374 kw-hrs)
- System Efficiency actual 28.69% vs goal of 28.5 to 30%
- Low Degradation
  - - 3.02 microvolts/cell hr Entire 59 day run
  - 0.151 microvolts/cell hr last 10 days (3/20/07 to 4/3/07)
- High Number of low cell trips 10 to date vs goal of 0
- Low Cell Trips: Perform Stack Testing to confirm System Delta T Model
- *Anticipating 2000 stack hours will be achieved by early June*



# DOE4 MEA in Final GenSys System

**Objective** – Demonstrate Final Components and System for 2,000 hours per statement of work

## Final Demonstration Stack



- Final MEA (Membrane, Catalyst, GDL)
- Improved System



# Future Work – To the End of the Project

## MEA & Stack Development & Testing

- Run until failure Saratoga stack tests – Plug Power
- Run until failure 'Final' stack and MEA design and test – Plug Power/3M
- Module testing on continual component improvements

## MEA Degradation Studies (update based upon CASE data)

- Peroxide model – CASE
  - Incorporate realistic kinetic and transport parameters
- Model compounds – CASE
  - Determine degradation kinetic constants
- MEA nonuniformity studies – 3M/Plug/University of Miami
  - Determine operating conditions/MEA designs that yield current distribution uniformity
- Post mortem analysis – CASE/Plug Power
- Mechanical properties-morphology relationship – CASE

## MEA Statistical Lifetime Predictions

- Continue to update MEA lifetime modeling – 3M/Plug Power
- Add temperature and humidity conditions to balance model
- Final MEA design started

# Project Summary

**Relevance:** Developing MEA and system technologies to meet DOE's year 2010 stationary durability objective of 40,000 hour system lifetime. Providing insight to MEA degradation mechanisms.

**Approach:** Two phase approach (1) optimize MEAs and components for durability and (2) optimize system operating conditions to minimize performance decay.

**Progress:** Demonstrated pathway towards 20,000 hour MEA lifetime with 3M PEM MEAs under accelerated 'near-OCV' load cycle test conditions. Initiated durable MEA-stack system tests.

	FY '05	FY '06	FY '07	DOE 2010 Goal (hrs)
<b>Accelerated Lifetime Predictions (hrs)</b>	16,000	> 20,000	> 20,000	40,000

**Technology Transfer/Collaborations:** Active partner with CWRU, Plug Power and the University of Miami. Presented 9 presentations and 2 papers on work related to this project in last 12 months.

**Future Work:** Continue system tests