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#### Project ID# ST063

OPERATED BY SAVANNAH RIVER NUCLEAR SOLUTIONS



### **Reversible Formation of Alane**

A High Hydrogen Density Material for Energy Storage

**Ragaiy Zidan** 

**Energy Security Directorate** 

Savannah River National Laboratory

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# Overview

### Timeline

Start: 10/1/06

End: Continuing

Percent complete of activities proposed for FY15: 50%

### **Barriers**

- A. System Weight and Volume
- B. System Cost
- C. Energy Efficiency

### Budget

- Funding received in FY14
  - \$400K
- Funding to be received in FY15
  - \$400K

### Collaborators

- Ardica (CRADA Partners)
- SRI

### **Overall Objectives**

 Develop a low-cost rechargeable hydrogen storage material with cyclic stability, favorable thermodynamics and kinetics fulfilling the DOE onboard hydrogen transportation goals.

Aluminum hydride (Alane - AlH<sub>3</sub>), having a gravimetric capacity of 10 wt.% and volumetric capacity of 149 g/L H<sub>2</sub> and a desorption temperature of ~60°C to 175°C (depending on particle size and the addition of catalysts) has potential to meet the 2020 DOE onboard system desorption targets

#### **Specific Objectives**

- Develop cheaper techniques to synthesize alane which avoids the chemical reaction route of AlH<sub>3</sub> that leads to the formation of alkali halide salts such as LiCl or NaCl.
- Utilize efficient electrolytic methods to form AlH<sub>3</sub>.
- Develop crystallization methods to produce alane of the appropriate phase, crystal size and stability.



 Current alane production techniques use AlCl<sub>3</sub> and LiAlH<sub>4</sub> in a solution based chemical reaction which is costly due to LiCl formation which is not easily reversible.

 $3LiAlH_4 + AlCl_3 \Leftrightarrow 4AlH_3 + 3LiCl$ 

Current price \$3,500/kg small scale

• Generating alane electrochemically allows for the exclusion of halide salts and simple aluminum recycling methods.

$$LiAlH_4 \Leftrightarrow AlH_3 + \frac{1}{2}H_2 + Li^+ + e^- \quad E^0 = -2.05 \text{ V vs. SHE}$$

$$Li^+ + \frac{1}{2}H_2 \Leftrightarrow LiH + e^ E^0 = -2.33 \text{ V vs. SHE}$$

$$LiH + Al + \frac{3}{_2}H_2 \Leftrightarrow LiAlH_4$$

Large scale production using electrochemical method expected to reduce cost below \$100/kg



#### Aluminum not recycled

Hydrogen Cost in AlH <sub>3</sub>	\$0.428	\$/kg
Aluminum Cost in AlH <sub>3</sub>	\$1.982	\$/kg
E-Chem Thermo Cost	\$0.103	\$/kg
E-Chem Kinetics Cost	\$0.096	\$/kg
E-Chem Ohmic Cost	\$0.114	\$/kg
Total E-Chem Cost from NAH	\$2.724	\$/kg

#### Aluminum recycled

Hydrogen Cost in AlH <sub>3</sub>	\$0.428	\$/kg
E-Chem Thermo Cost	\$0.103	\$/kg
E-Chem Kinetics Cost	\$0.096	\$/kg
E-Chem Ohmic Cost	\$0.114	\$/kg
Total E-Chem Cost from NAH	\$0.742	\$/kg

# **Approach: Electrochemical Generation of Alane Adduct**

#### **Before Electrolysis**



#### After Electrolysis



- Producing alane directly from the elements requires impractical hydrogen pressure
- Electrochemical alane adduct
  production significantly reduces the
  cost of manufacture compared to
  chemical methods
- The cost of alane production can be significantly reduced due the recyclability of the materials by the electrochemical method
- Electrochemical alane production avoids the production of alkali halides which require large amounts of energy to reverse



# Approach: Crystallization of Alane Adduct to α-Alane

- Alane adduct can be crystallized by various methods.
- The conditions used depend highly on the nature of the adduct ligand.
- Dry methods and solution based methods have been explored with the use of additives to assist in the formation of  $\alpha$ -alane.





## **Approach: Regeneration of Spent Alane to Electrolyte**

### **Regenerating LiAlH**<sub>4</sub> from dehydrogenated AlH<sub>3</sub>:

 $2 \text{ LiH} + 2 \text{ Al}_{c}^{*} + 3 \text{H}_{2} \rightarrow 2 \text{ LiAIH}_{4}$ 

(Al<sub>c</sub>\* = catalyzed and activated Al)



High pressure Parr-reactor used for the regeneration of electrolyte.

Yields above 80% have been achieved for both NaAlH<sub>4</sub> and LiAlH<sub>4</sub> regeneration.

- Regeneration of the electrolyte from spent alane allows for the reversible production of alane.
- This regenerated electrolyte (LiAlH<sub>4</sub> or NaAlH<sub>4</sub>) can then be used in the electrochemical cell to generate the alane adduct.



## **Current Progress: Electrochemical Alane Production**

### **Dendrite Reduction**

- Dendrites pose problems for the large scale production of alane since they can grow to an extent where shorting out the cell is possible.
- The dendrites are composed of (Na/Li)<sub>3</sub>AlH<sub>6</sub> and Al metal.
- The pulsing forms growth in a compact layer



Dendrites from typical 18 hour reaction.

Dendrites were significantly reduced by utilizing a reverse pulse technique during the electrochemical reaction.





Dendrites from reverse pulsed 24 hour reaction.



## Methods for Crystallization

- Both chemical and electrochemical production techniques generate the alane adducted to various ligands.
- Crystallization to the right phase and crystal size is essential for stability of the material and hydrogen capacity and release temperatures.
- The conversion of alane adduct to alane occurs in a very small temperature window (75 - 85 °C)
- The alpha phase with symmetrical crystals in the 4-50 µm range is most desired.
- The dry method produces large crystals, but with little symmetry and aluminum.





 $\alpha\text{-alane}$  crystals produced by the dry method.



# **Current Progress: Crystallization of Alane Adduct**

## *Identifying conditions to produce α-alane and avoid other phases using solution methods*



SEM image of  $\alpha^\prime$  alane

- Solution based methods can produce the alpha prime  $(\alpha^\prime)$  phase of alane
- This phase is found to predominate when the crystallization temperature is below 76 °C or the rate of diethyl ether removal is too slow
- While the alpha prime phase has a high hydrogen content, it's stability is much less than that of α-alane



## **Current Progress: Crystallization of Alane Adduct**



SEM image of Alpha Alane with residual gamma alane.



- The appropriate time, temperature, and ether removal rate must be optimized to produce pure alpha alane.
- Gamma alane will convert to alpha alane with additional heating.





## **Current Progress: Crystallization of Alane Adduct**





- The alpha alane produced contained 9.2 wt. % H<sub>2</sub> as shown in the TGA/RGA.
- The crystals are of excellent symmetry and size.
- Further work to reduce the agglomeration of these alpha alane crystals is underway.



# **Current Progress: Recycling Spent Alane for Reuse**



SEM image of the inside of a spent alane pellet pressed at 3 tons.



SEM image of the surface of a spent alane pellet pressed at 3 tons. Bright spots show electron build up (charging) which is indicated lower current flow (high resistivity).

- Our collaborators (Ardica) are developing an electrochemical system that regenerates electrolyte in situ.
- Their system is based on an electrochemical flow cell approach.
- Therefore, the use of spent alane for both electrodes would allow for in situ recyclability of spent alane.
- SRNL tested spent alane as electrodes in the production of alane
- Spent alane electrodes has a lower current.
- This was due to insufficient electrical contact between the compressed spent alane particles.
- This can easily be avoided by using higher pressure for compaction or electrically conductive binders.



## **Collaborations and Team members**



- Improve the conductivity of the electrolyte solution to increase the rate of alane production
- Eliminate the dendrite formation on the surface of the electrolyte
- Optimize the crystallization parameters for the large scale production of alpha alane



# Future Work: Electrochemical Production of Alane

- Insulate the electrode at the surface of the electrolyte solution to prevent dendrite formation at the location during the reverse pulse method
- Increase conductivity by reducing the distance between the electrodes once dendrites have be eliminated
- Develop efficient method for the crystallization of the alane THF adduct, so THF can be used as the solvent (higher conductivity than Diethyl Ether)
- Explore additives to the electrochemical cell which can increase the conductivity



- Develop techniques for the crystallization alane THF adduct with appropriate phase (α) and particle size
- Ensure current technique for the crystallization of alane diethyl ether adduct is reproducible on a larger scale
- Optimize the crystallization technique with toluene instead of benzene to improve commercial production opportunities



- Dendrites formed during the electrochemical generation of alane have been significantly reduced and a method for removal along the electrolyte surface has been identified.
- Crystallization of alane adduct to alpha alane with appropriate particle sizes has been accomplished.
- Regeneration of spent aluminum to the electrolyte has been achieved in high yields as reported previously.
- Feasibility of using spent alane as electrode in the electrochemical cell has been investigated.

