

System Level Analysis of Hydrogen Storage Options

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Project ID: ST01

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Overview

Timeline

- Project start date: Oct 2009
- Project end date: N/A
- Project continuation and direction determined annually by DOE

Budget

- FY16 DOE Funding: \$480 K
- FY17 DOE Funding: \$600 K

Barriers

- H₂ Storage Barriers Addressed:
 - A: System Weight and Volume
 - B: System Cost
 - C: Efficiency
 - E: Charging/Discharging Rates
 - J: Thermal Management
 - K: Life-Cycle Assessments

Partners/Interactions

- Hexagon Lincoln (HL), Matera, PNNL
- BMW, LLNL
- Ford, LANL
- ORNL
- Delivery Team, Hydrogen Interface Taskforce (H2IT)
- Strategic Analysis



Develop and use models to analyze the on-board and off-board performance of physical and material-based automotive hydrogen storage systems

- Conduct independent systems analysis for DOE to gauge the performance of H₂ storage systems
- Provide results to material developers for assessment against system performance targets and goals and help them focus on areas requiring improvements
- Provide inputs for independent analysis of costs of on-board systems.
- Identify interface issues and opportunities, and data needs for technology development
- Perform reverse engineering to define material properties needed to meet the system level targets

Impact of FY2017 work

- Demonstrated that 2-mm stainless steel (SS) liner is preferable to aluminum liner in cryo-compressed H₂ (CCH₂) storage systems for buses
- Compared to the baseline 350-bar compressed hydrogen (CH₂) tanks currently in use, 500-bar CCH₂ can achieve 66% improvement in gravimetric capacity, 132% increase in volumetric capacity, and 36% saving in carbon fiber (CF) composite
- Determined >7 d loss free dormancy with 95% full 500-bar CCH₂ tanks

Approach

- Develop thermodynamic and kinetic models of processes in physical, complex metal hydride, sorbent, and chemical H₂ storage systems
 - Address all aspects of on-board and off-board storage targets, including capacity, charge/discharge rates, emissions, and efficiencies
 - Perform finite-element analysis of compressed hydrogen storage tanks
 - Assess improvements needed in materials properties and system configurations to achieve storage targets
- Select model fidelity to resolve system-level issues
 - On-board system, off-board spent fuel regeneration, reverse engineering
 - Conduct trade-off analyses, and provide fundamental understanding of system/material behavior
 - Calibrate, validate, and evaluate models
- Work closely with DOE technology developers, national labs and others in obtaining data, and provide feedback
- Participate in meetings and communicate approach and results to foster consistency among DOE-sponsored analysis activities



FY2017 Tasks and Progress

1. Cryo-compressed H₂ Storage (FY2017 Q1)
 - Analyzed autofrettage process and liner fatigue using ABAQUS FE-SAFE
 - Conducted GCTool simulations of supercritical CcH₂ storage with off-board LH₂ pump and dormancy at different storage pressures and fill levels
2. Compressed H₂ storage (FY2017 Q2)
 - Setting up models for carbon fiber damage in impact tests
3. H₂ storage in sorbents (FY2017 Q3)
 - Update heat transfer model and absorption isotherms for compacted pellets
 - Revisit H₂ storage using high-pressure LH₂ pumps
4. H₂ storage in high-pressure metal hydrides (FY2017 Q4)
 - Revise analysis and publish paper on target material and transport properties

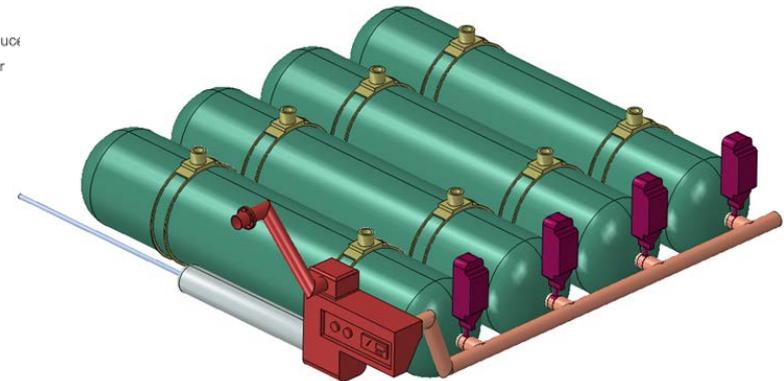
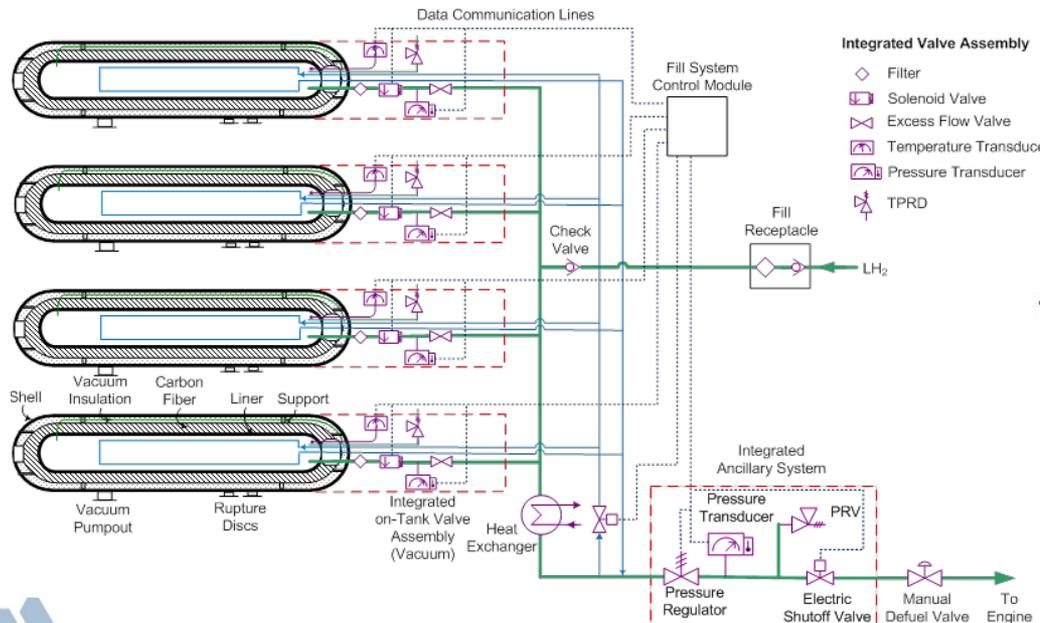
1	Conduct system analysis of CcH ₂ storage for FC buses and garbage trucks with emphasis on dormancy, durability and capacity	12/16
2	Conduct ABAQUS simulations to determine reduction in CF usage and system cost with recent improvements in materials and designs, relative to the current benchmarks of 97 kg CF composite and 15 \$/kWh for 5.6 kg usable H ₂ at 700 bar.	03/17
3	Conduct system analysis for H ₂ storage in sorbents utilizing data validated models for best-of-class framework materials relative to the 2020 system targets for gravimetric capacity (5.5 wt%), volumetric capacity (40 g/L), and WTE efficiency (60%).	06/17
4	Update system analysis for H ₂ storage in high-pressure, low-enthalpy metal hydrides and determine material properties needed for meeting 2020 system targets for refueling rate (1.5 kg/min), gravimetric capacity (5.5 wt%), volumetric capacity (40 g/L), and WTE efficiency (60%).	09/17

Cryo-Compressed (CCH₂) Hydrogen Storage for FC Buses

	Current Practice	Future Candidate
Storage Option	350-bar cH ₂	350-700-bar CcH ₂
H ₂ Tank	Type 3, T700 CF	Type 3, T700 CF
Liner	Aluminum	Aluminum or Stainless Steel
H ₂ Storage Capacity	40 kg	40 kg
Number of Tanks	8	4
L/D	5	5
H ₂ Density	24 kg/m ³	LH ₂ : 71 kg/m ³ at 20 K, 1 bar
Refueling Rate	5 kg/min	TBD

Issues to be addressed

1. Cryogenic liner behavior
2. CcH₂ system parameters
3. Operating pressures and temperatures
4. Realizable storage capacities
5. Loss-free dormancy



ABAQUS WCM and FE-SAFE Models

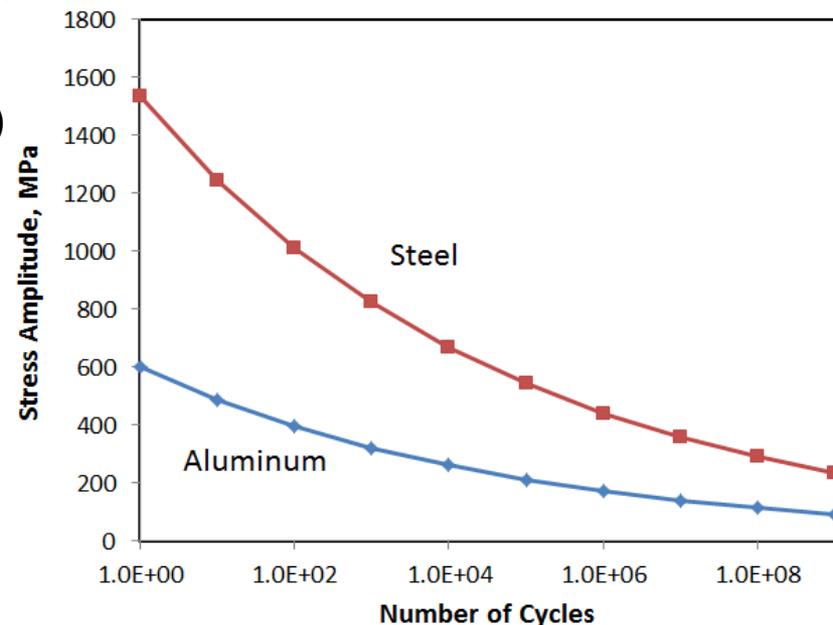
- Autofrettage process to induce residual compressive stress in liner and increase the fatigue life of the composite tank
- Thermal stresses during service at cryogenic temperatures

Process and Material Options

- Autofrettage at ambient temperature or at cryogenic temperature
- Autofrettage (proof) pressure
- Minimum tank pressure to prevent separation
- Aluminum or stainless steel liners
- Fatigue SN curves* for aluminum (Al) and stainless steel (SS)

Applicable Codes and Standards

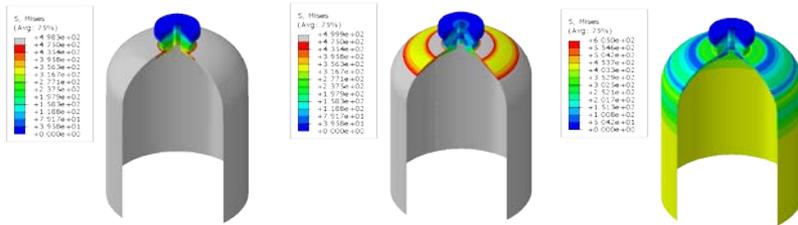
- SAE durability test cycles: 5500 for light duty vehicles, 15000 for commercial heavy duty vehicles



* Military Handbook, 2003, MIL-HDBK-5H, and Muralidharan UU, Manson SS, *ASME J. Eng. Mater. Technol.* 1988;110(1):55-58

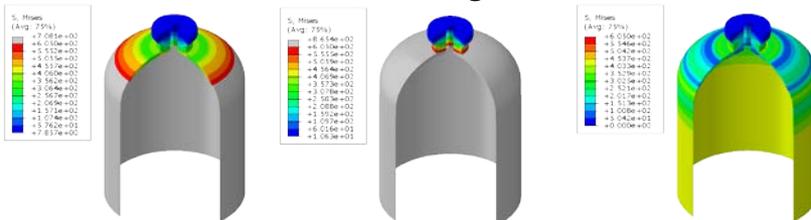
Autofrettage Process – Axial Stresses

- Process option AF1: autofrettage at RT, then cool tank to service temperature
 - Liner is in compression after autofrettage, but thermal stress induced during cool-down places it in tension
 - Entire liner undergoes plastic deformation during loading (as expected)

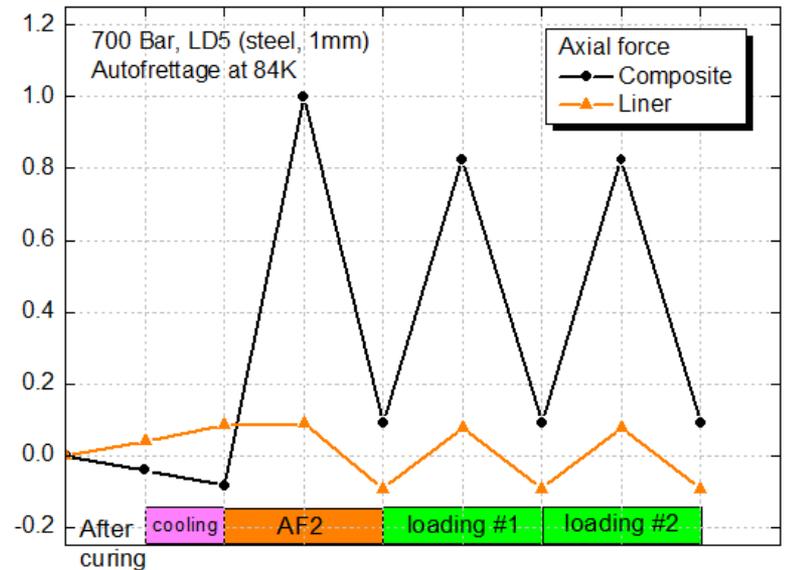
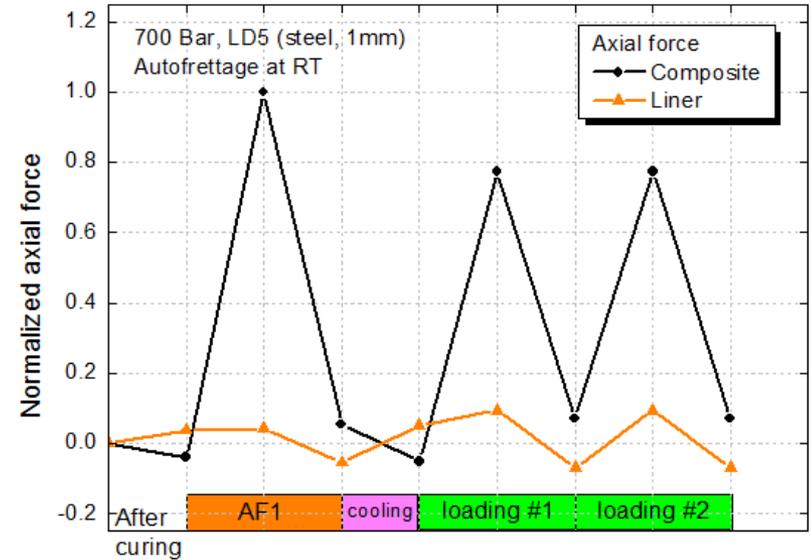


After proof loading After unloading After Cooling

- Process option AF2: cool tank to service temperature, then autofrettage
 - Liner is in tension after cool down, but in compression after autofrettage
 - The cylinder section has undergone plastic deformation after cooling

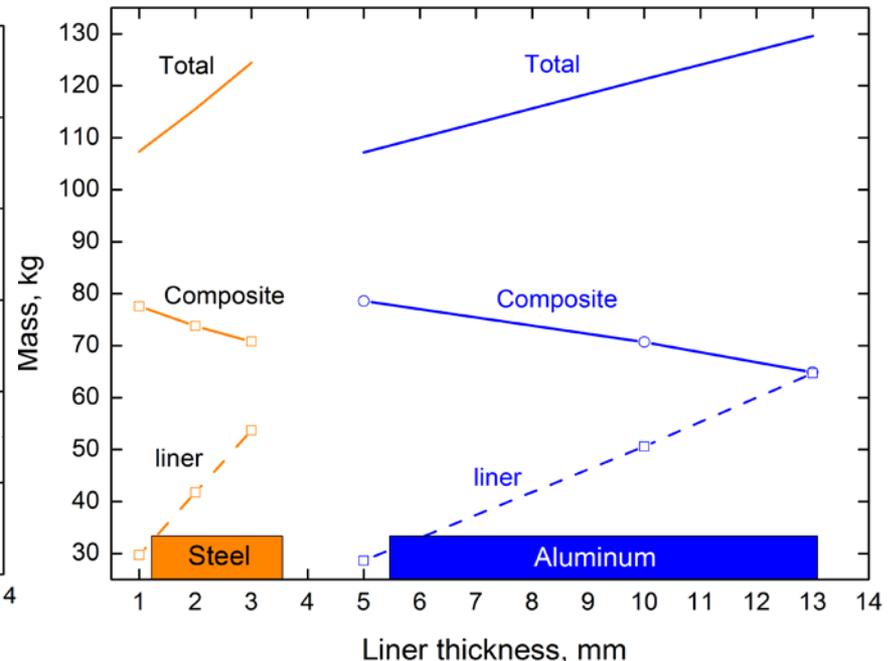
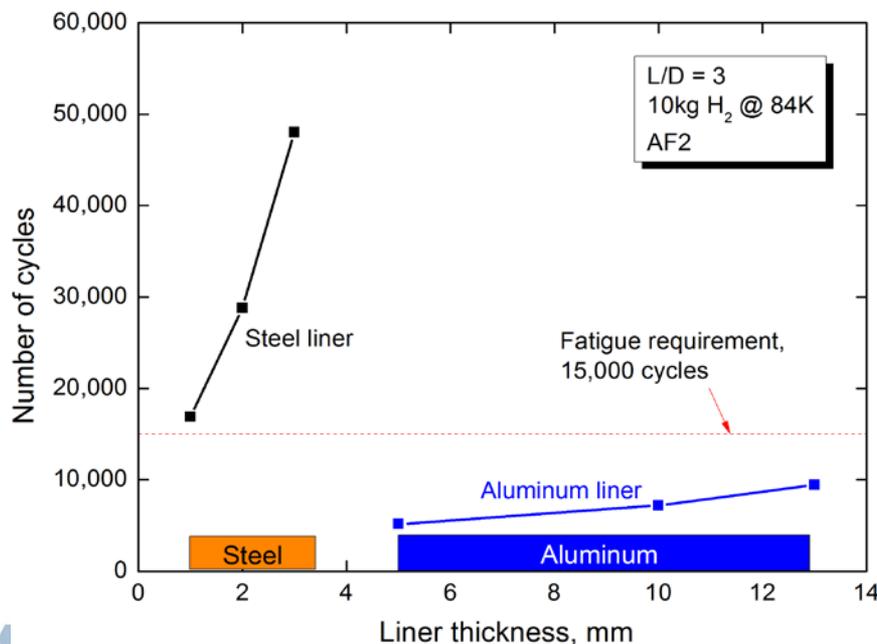


After cooling After proof loading After unloading



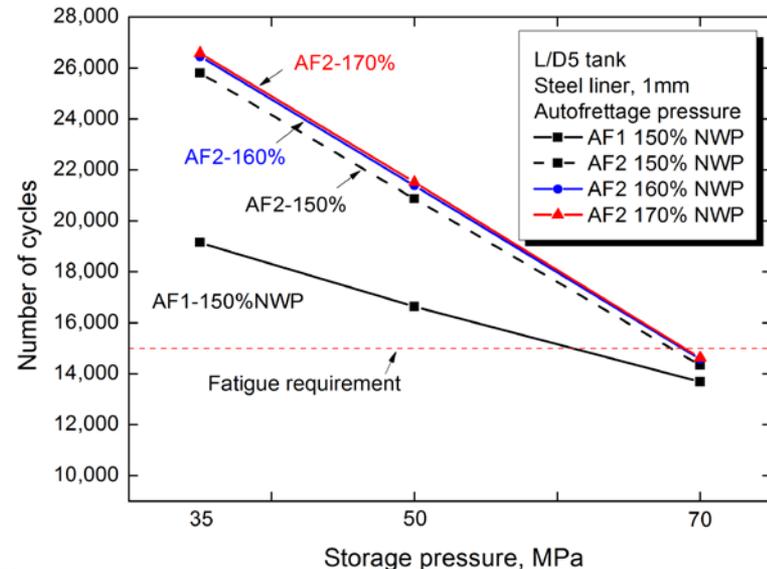
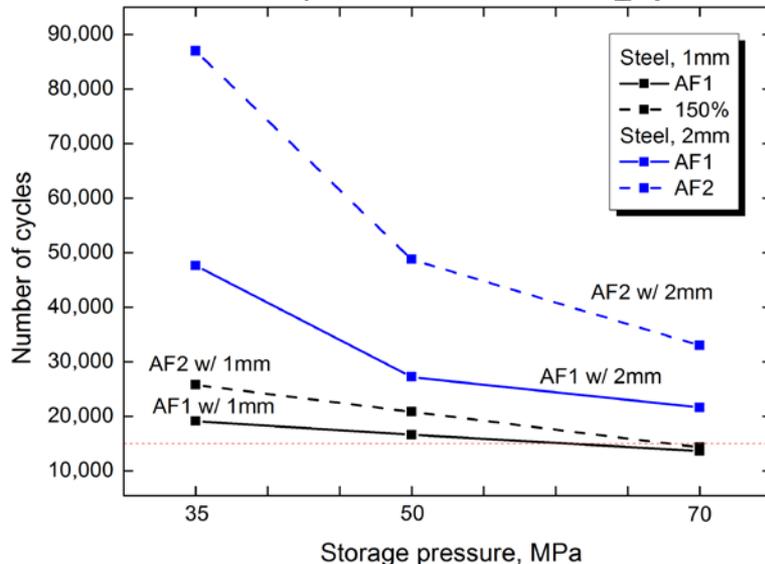
Fatigue Life: Aluminum vs. Steel

- 10-kg H₂ tanks with L/D = 3, nominal T = 84 K, P = 70 MPa, SF = 2.25
 - Autofrettage performed at 84 K
- Steel liner meets fatigue life requirement with thickness as small as 1 mm**
 - 1 mm liner weighs 29.7 kg, about 28% of total tank weight
- Aluminum liner fails before 15,000 cycles for thicknesses up to 13 mm (9500 cycles)**
 - Al liner weighs 64.7 kg, about 50% to total tank weight
 - Tank weight ~130 kg, 22 kg heavier than a 1-mm steel-lined tank



Fatigue Life: AF1 vs. AF2

- 10-kg H₂ tanks with L/D = 5, nominal T = 84 K, P = 35 – 70 MPa, SF = 2.25
- Longer cycle life if autofrettage performed at cryogenic temperature (AF2)**
 - Improvement is more pronounced with thicker liner
 - AF2 not necessary since AF1 can produce sufficient fatigue life**
- Lower CF and liner material cost with 2-mm rather than 1-mm liner**
 - P = 50 MPa, $\Delta(\text{CF}) = -4.0 \text{ kg}$, $\Delta(\text{liner}) = 15.0 \text{ kg}$, $\Delta(\text{cost}) = -\$85$
- Autofrettage performed at low temperature may be subjected to higher autofrettage pressure because yield stress and modulus of the metal are higher at lower temperature
 - Small enhancement in fatigue life by raising autofrettage to 170% NWP from 150% NWP (normal working pressure)



Performance of CcH₂ System for Fuel Cell Buses

GCtool model for CcH₂ storage: Ahluwalia, R. K. and Peng, J. K., Int. J. Hydrogen Energy, Vol. 33, Issue 17, pp. 4622-4633, Sep. 2008; Int. J. Hydrogen Energy, Feb. 2010, Vol. 35, 4171-4184, 2010; Int. J. Hydrogen Energy, Vol. 38, 13664-13672, 2013.

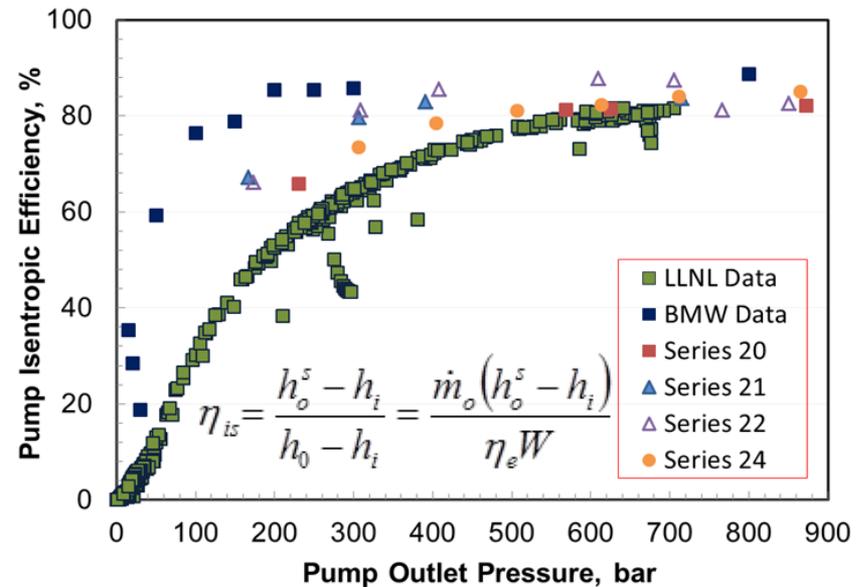
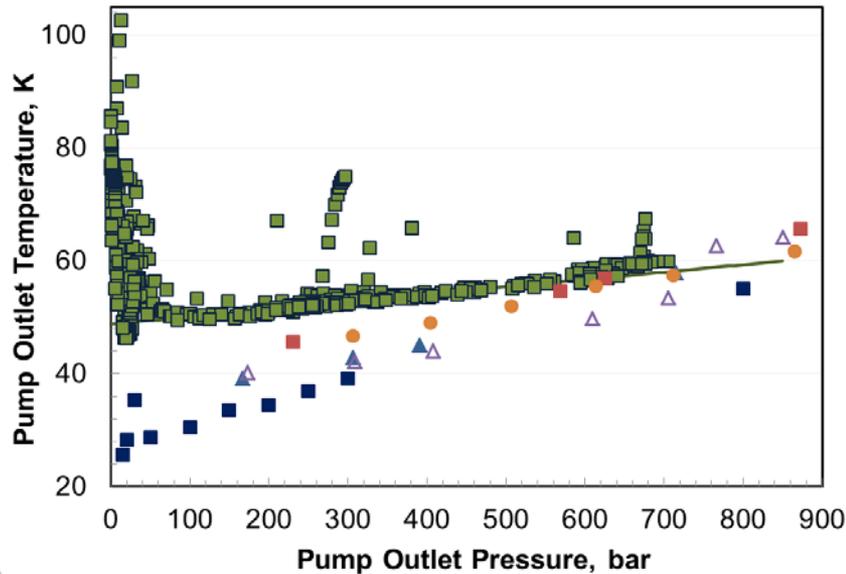
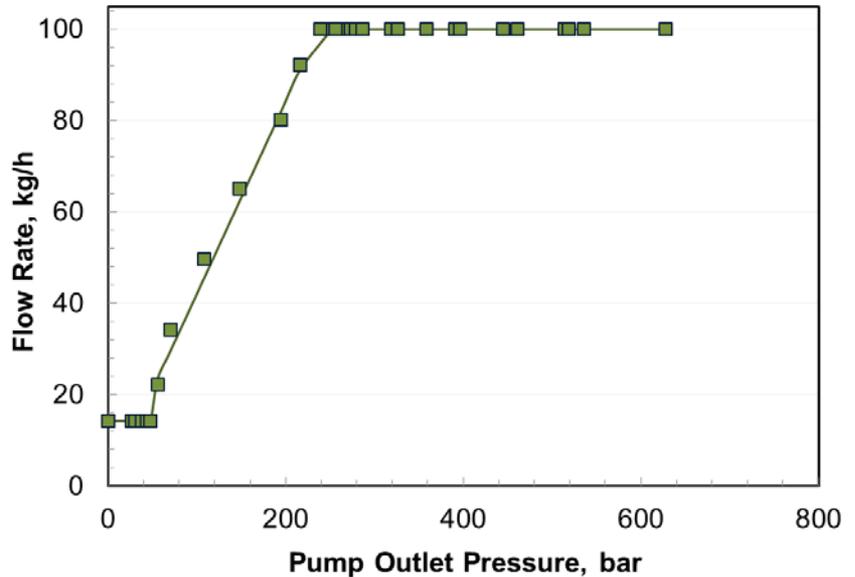
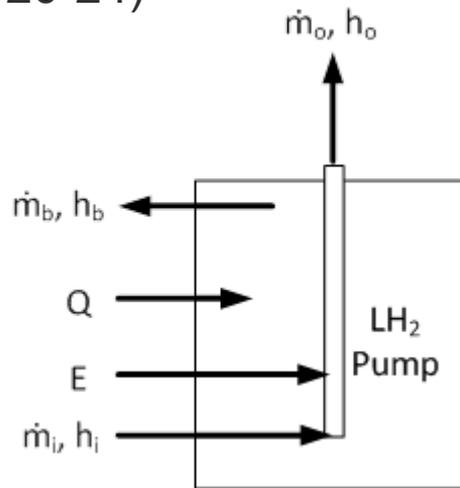
System Parameter	Reference Value ¹	Range ¹	Comment
Storage Pressure	500 bar	350-700 bar	Type-3 carbon fiber wound tank
Empty Pressure	5 bar	5-10 bar	Minimum delivery pressure set by FCS
Storage Volume ²	4 x 169 L	4 x 155-183 L	40 kg usable H ₂
Storage Temperature	107.9 K	93-123 K	Determined by LH ₂ refueling and LH ₂ pump efficiency
Discharge Temperature	47.1 K	47.1-49.5 K	Function of duty cycle, 1-3 day discharge time
Heat Rate	4 x 53 W	4 x 52-70 W	Repeat charge-discharge cycle
Refueling Rate	1.6 kg/min	5 kg/min target	Set by LH ₂ pump capacity
Tank Aspect Ratio	L/D = 5	L/D = 3-5	
Liner Thickness	2-mm SS	9.5-15.2 mm Al	SAE J2579: 11,250 duty cycles; ABAQUS FE-SAFE Model
Autofrettage Pressure	1.5 x NWP		Same as proof pressure
Carbon Fiber Amount	4 x 64.2 kg	4 x 43.2-96.2 kg	T700 CF; SAE J2579: 2.25 Safety Factor; ABAQUS-WCM Model.
Insulation Thickness	7.4 mm	6.9-8.1 mm	10 W heat gain, MLVSI

¹ Unless noted otherwise, results are for SS liner and high-efficiency LH₂ pump

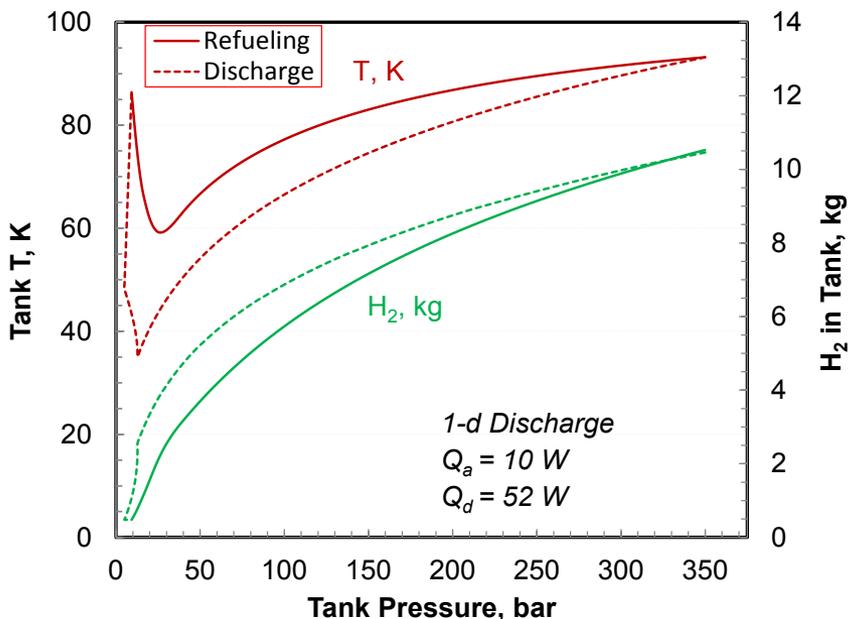
² Refers to gas (empty tank) volume

LH₂ Pump Performance

Data Sources: LLNL (880 bar pump),
 BMW (350 bar pump, high efficiency),
 Linde (Series 20-24)

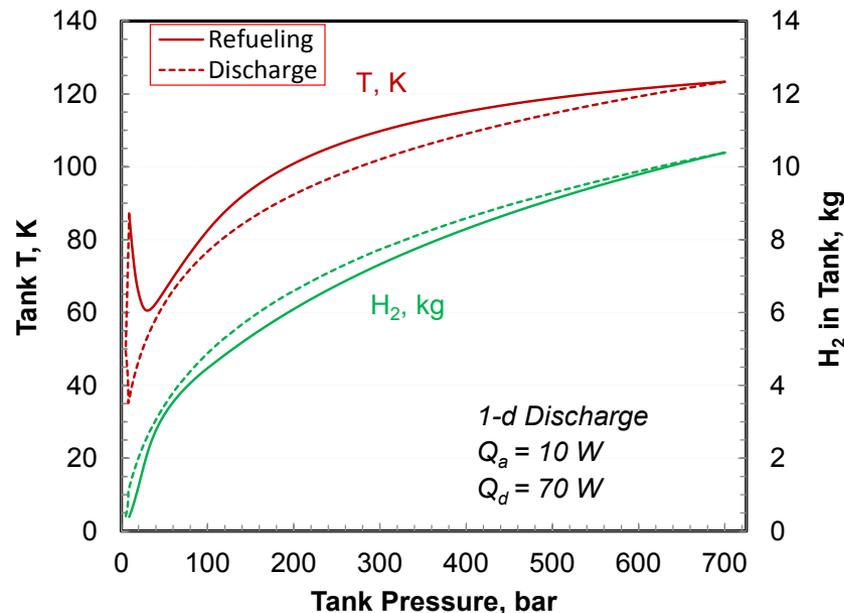
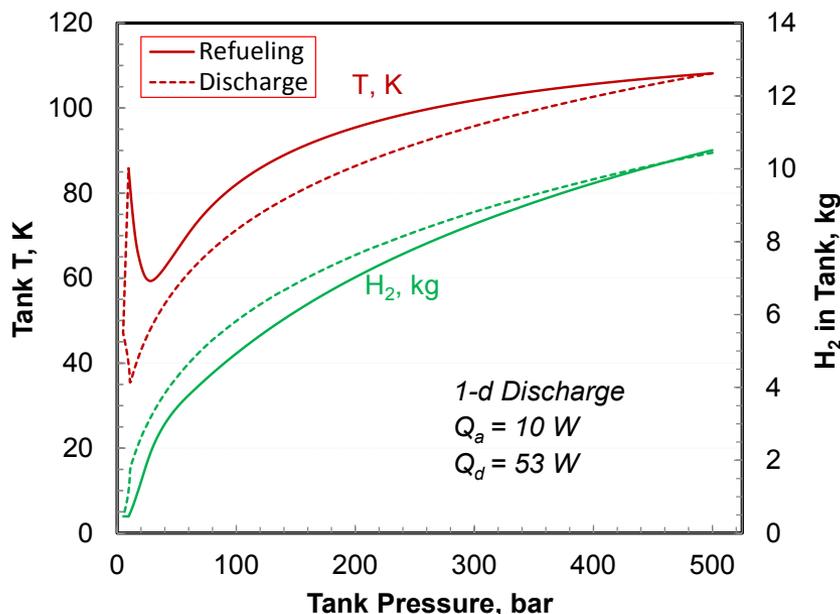


Repeat Charge-Discharge Cycle: 2-mm SS Liner, 350-700 bar



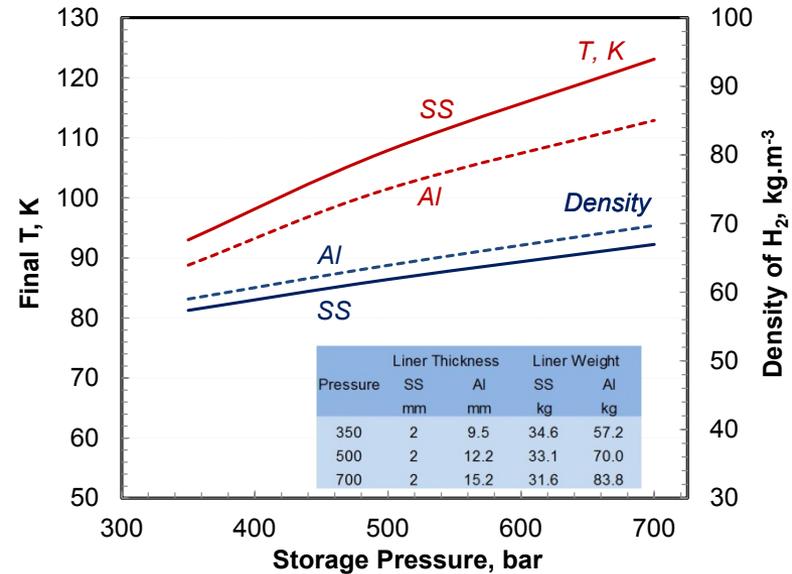
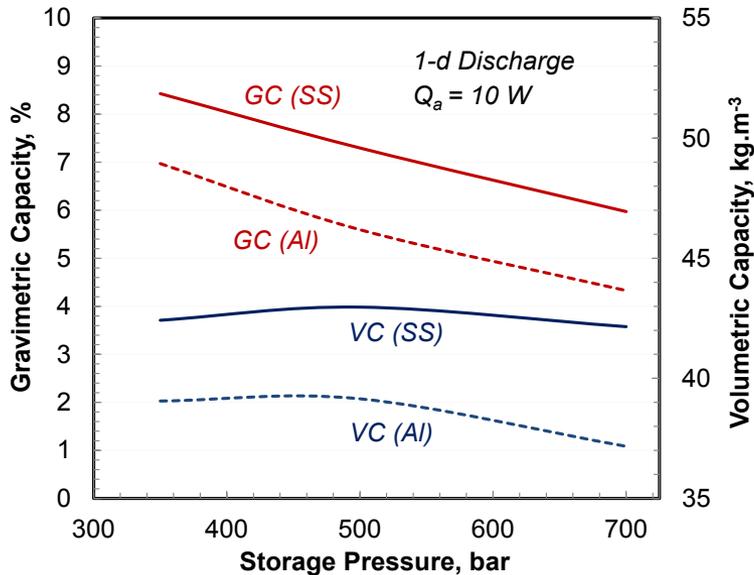
Supercritical CcH_2 storage: small heater or heat exchanger (HX) to prevent liquid formation
Volumetric capacity highest at intermediate P

Storage Pressure	350 bar	500 bar	700 bar
Storage Temperature	93 K	108 K	123 K
Storage Density	57.4 g/L	61.9 g/L	67.0 g/L
Usable H_2	95.5%	95.6%	96.2%
Gravimetric Capacity	8.4%	7.3%	6.0%
Volumetric Capacity	42.4 g/L	43.0 g/L	42.2 g/L
Storage Volume	4x183 L	4x169 L	4x155 L

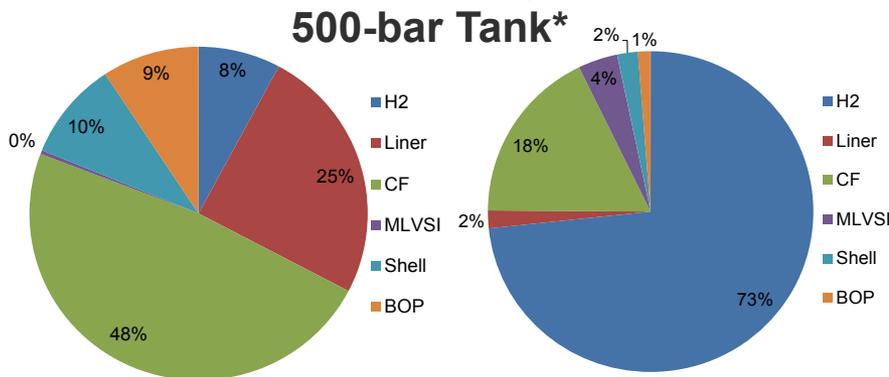


Storage Capacities: Stainless Steel vs. Aluminum Liner

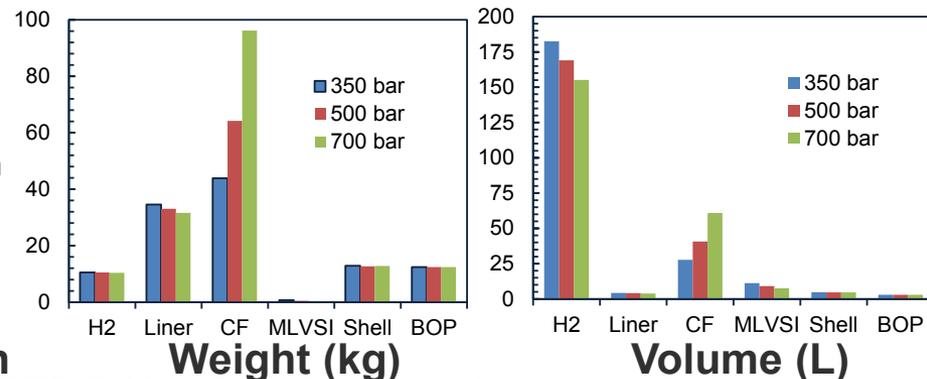
In spite of higher material density and storage temperature, gravimetric and volumetric capacities are higher with stainless steel liner.



At 500 bar, CF composite and SS liner account for 73% of the tank* weight, the volumetric efficiency is 73%.



Effect of Pressure on Weight and Volume



Weight Distribution

Volume Distribution

Weight (kg)

Volume (L)

*Includes components associated with each tank, excludes components common to all tanks

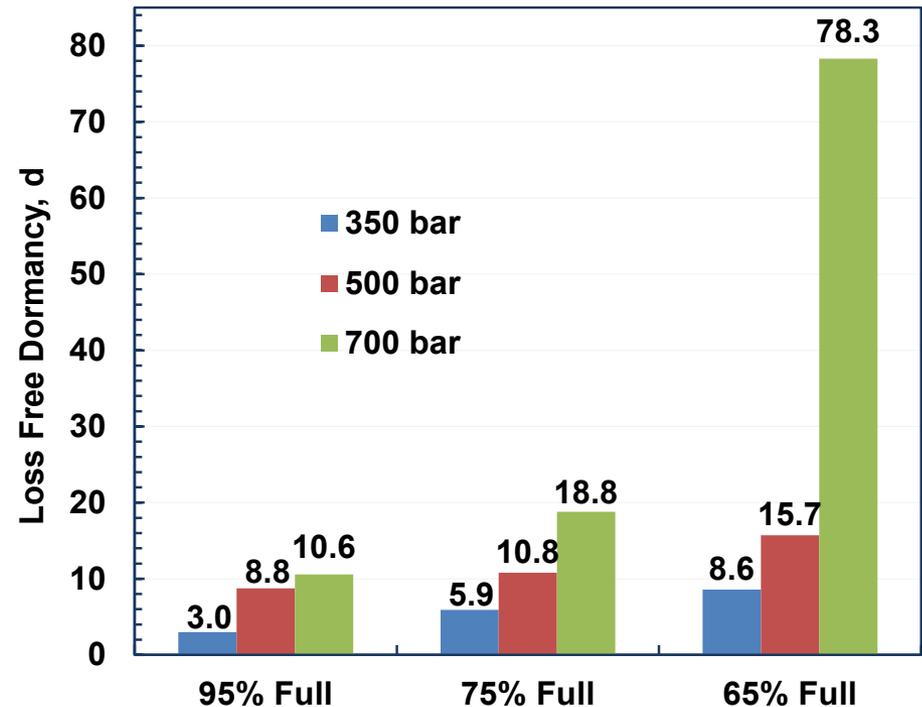
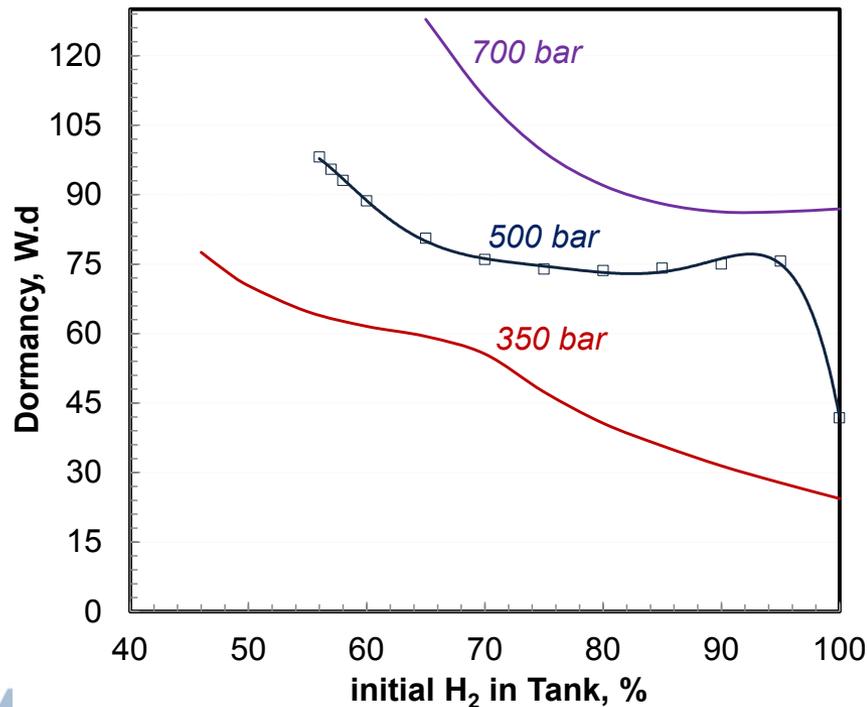
Dormancy

>7-d dormancy for 95% full tank at 500-bar storage pressure

- Increase in dormancy with storage pressure also depends on amount of H₂ stored; 700 vs. 350 bar: 3.5x at 95% full, 9x at 65% full

Simulation parameters

- Pressure relief valve (PRV) set point: 1.25 X normal working pressure
- Initial tank temperature function of prevailing tank pressure
- Heat gain function of tank temperature
- Para-to-ortho conversion



Summary and Evaluation

Liner material of choice: SS for CcH₂ and Al for Type-3 350-bar, RT cH₂ storage

- LH₂ pump efficiency impacts off-board H₂ loss and recovery more than the storage temperature and gravimetric/volumetric efficiency
- 5 kg/min H₂ refueling rate for FC buses requires a LH₂ pump that has 3 times the capacity of the pump tested at LLNL
- 66% (64%) increase in gravimetric capacity, 132% (74%) increase in volumetric capacity, and 36% (64%) saving in CF composite for FC buses (LDVs)

Storage Method	Fuel Cell Bus				Fuel Cell LDV	
	CcH ₂	CcH ₂	CcH ₂	cH ₂	CcH ₂	cH ₂
Storage Pressure	500 bar	500 bar	500 bar	350 bar	500 bar	700 bar
Usable H ₂	4 x 10 kg	4 x 10 kg	4 x 10 kg	8 x 5 kg	1 x 5.6 kg	1 x 5.6 kg
Liner	2-mm SS	12.2 mm Al	2-mm SS	7.1 mm-Al	2-mm SS	5-mm HDPE
LH ₂ Pump Efficiency	High	High	Low		High	
Storage Temperature	107.9 K	101.5 K	115.8 K	288 K	102.3 K	288 K
Storage Density	61.9 kg/m ³	63.9 kg/m ³	59.5 kg/m ³	24 kg/m ³	63.6 kg/m ³	40.2 kg/m ³
Usable Hydrogen	95.6%	95.6%	95.5%	96.1%	98.3%	95.8%
Gravimetric Capacity	7.3%	5.6%	7.1%	4.4%	6.9%	4.2%
Volumetric Capacity	43.0 kg/m ³	39.2 kg/m ³	41.4 kg/m ³	18.5 kg/m ³	42.7 kg/m ³	24.6 kg/m ³
CF Composite	4 x 64.2 kg	4 x 70.3 kg	4 x 66.9 kg	8 x 50 kg	1 x 34.5 kg	1 x 96 kg
Dormancy						
95% Full	8.8 d	9.3 d	9.3 d	NA	9.4 d	NA
75% Full	10.8 d	12.5 d	12.0 d	NA	11.2 d	NA
60% Full	23.9 d	26.2 d	35.0 d	NA	23.1 d	NA

Updated 700-bar cH₂ System

Updated system physical parameters

- Ambient temperature: consistent with SAE regulations (15°C vs. 20°C), 1.1% saving in CF
- Tank empty pressure: 1 (20 bar) or 2-stage (10-15 bar) pressure regulator and supply pressure effect, 1.1-2.1% saving in CF
- Tank design: conventional (Conv.) vs. alternate (Alt.) design similar to Mirai tank, 4.9% saving in CF

	A	B	C	D	E	F
Empty pressure, bar	20 ⁽¹⁾	20	15 ⁽²⁾	10 ⁽³⁾	15	10
Ambient temperature, °C	20	15	15	15	15	15
Tank design	Conv.	Conv.	Conv.	Conv.	Alt. ⁽⁴⁾	Alt.
CF composite, kg	97	95.9	94.9	93.9	90.3	89.3
Gravimetric capacity, wt%	4.19	4.23	4.26	4.29	4.41	4.45
Volumetric capacity, g-H ₂ /L	24.38	24.64	24.88	25.13	25.23	25.48

(1) Quantum 1 or 2-stage pressure regulator

(2) Aerodyne Controls 2-stage pressure regulator

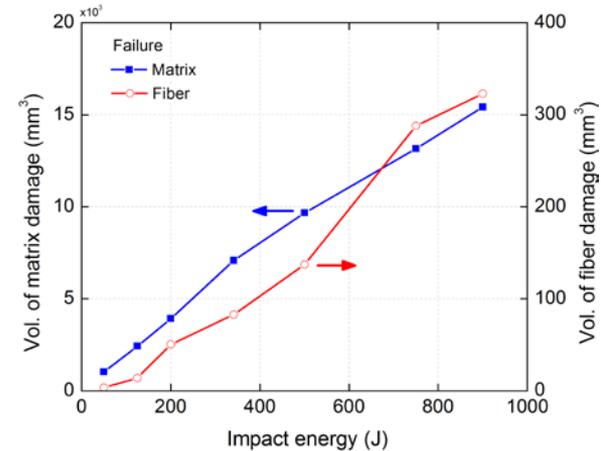
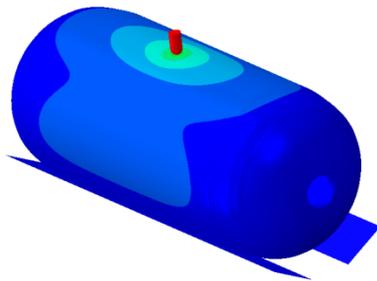
(3) JTEKT 2-stage pressure regulator in Toyota Mirai, empty pressure unknown

(4) Similar in design to the storage tank used in Toyota Mirai

Preliminary ABAQUS Impact Damage Analysis Results

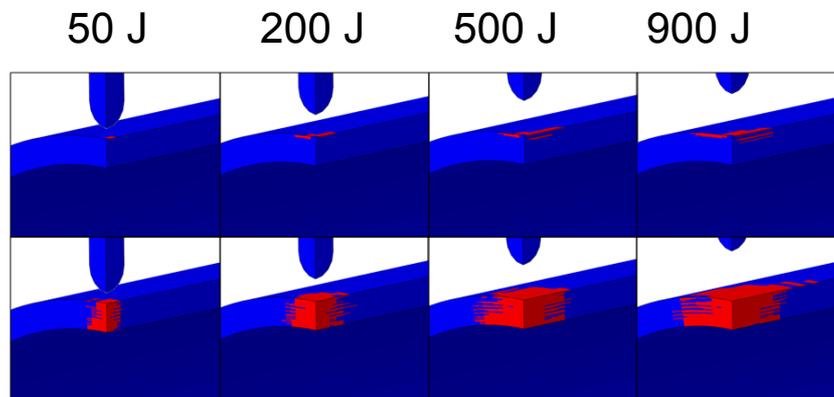
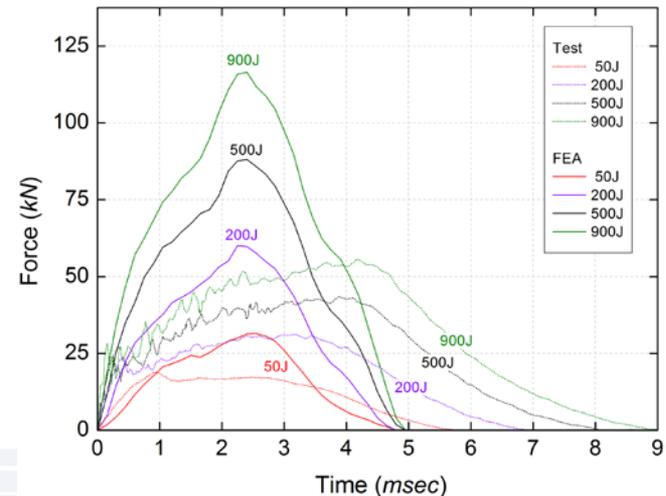
- Deformation extends as far as the dome region for energy as low as 50 J
- For impact energy $E < 200$ J, fiber damage occurs only in the outer layers (GF/epoxy)
- For $E > 340$ J, fibers in the inner composite layers (CF/GF/epoxy) are also damaged
- Matrix is damaged before fibers and matrix damage occurs throughout the thickness of the composite
- The damage volume is $>50X$ higher in matrix than in fiber

Deformation at 50 J impact



Impact Load History

Compared to test data*, the peak force is $\sim 2X$ higher, but the measured and modeled areas under the curves are in good agreement. The FE models will be improved to include the effects of layers delamination, void content in laminate, and resin crushing.

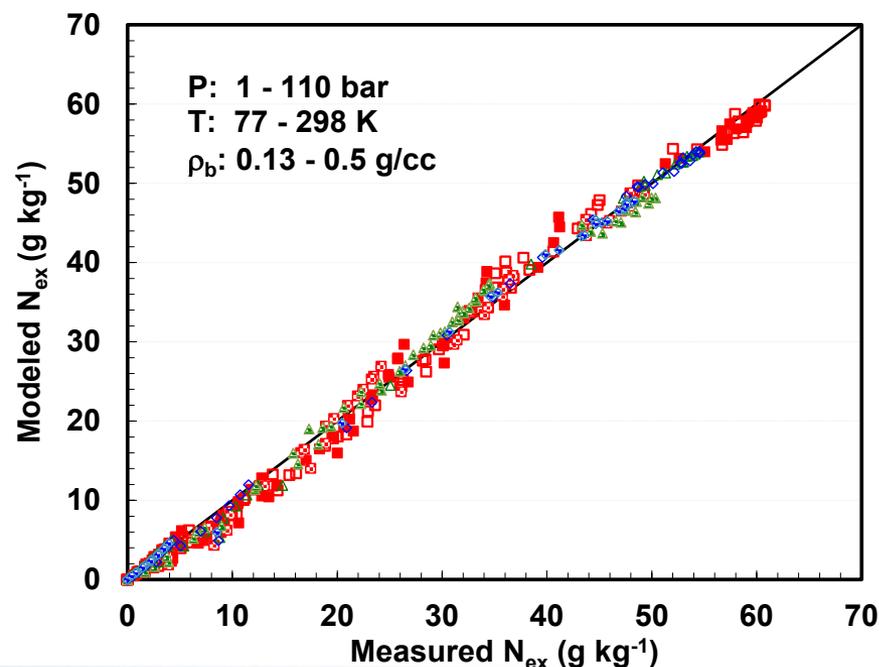
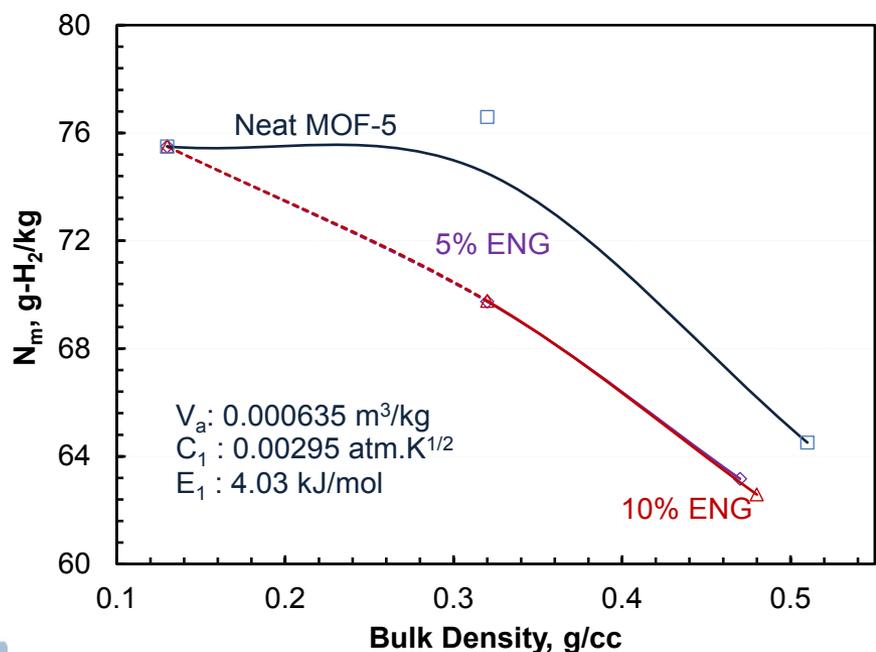


* Norm Newhouse, Hexagon Lincoln, private communication

Adsorption Isotherms for Pellets

Single-Langmuir equation can correlate Ford/UM excess H_2 uptake (N_{ex}) data for MOF-5 powder and pellets (0.13-0.5 g/cc bulk density) with 0-10 wt% expanded natural graphite (ENG) at 77-298 K, 1-110 bar

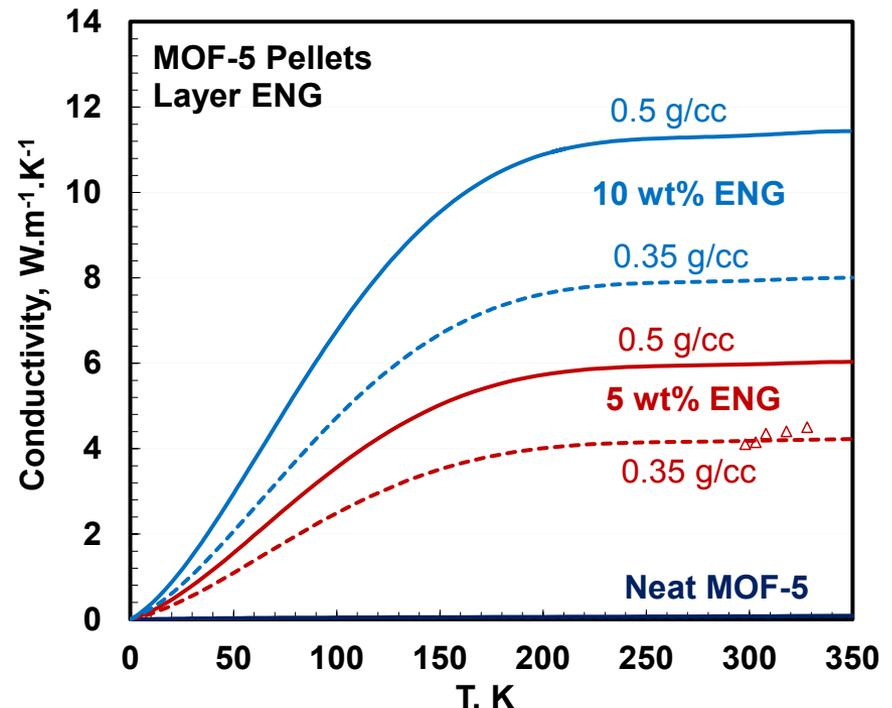
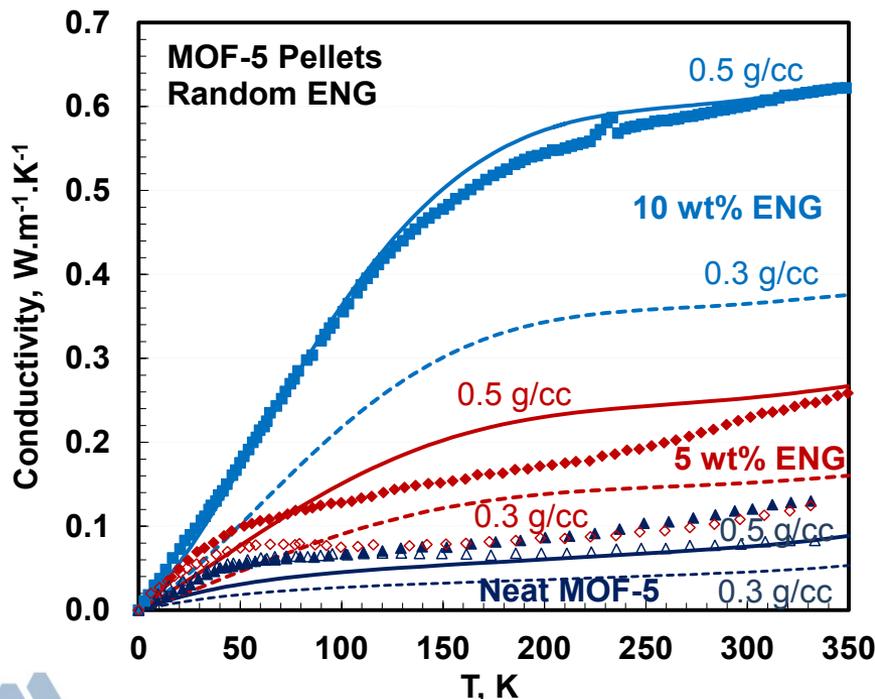
- M. Veenstra, et al, Ford/BASF-SE/UM Activities in Support of the HSECoE, ST010, AMR 2013, 2014. and 2015
- Same adsorption parameters (ΔH^0 , ΔS^0 , V_a), but sorption capacity parameter (N_m , g- H_2 /kg-sorbent) depends on bulk density and ENG weight fraction.
- Up to 15% decrease in N_m with compaction to 0.5 g/cc bulk density; N_m can further decrease by 6% with addition of 5-10 wt% ENG



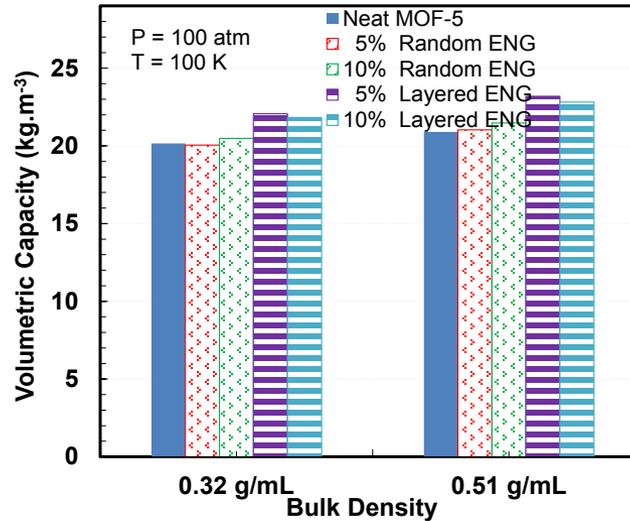
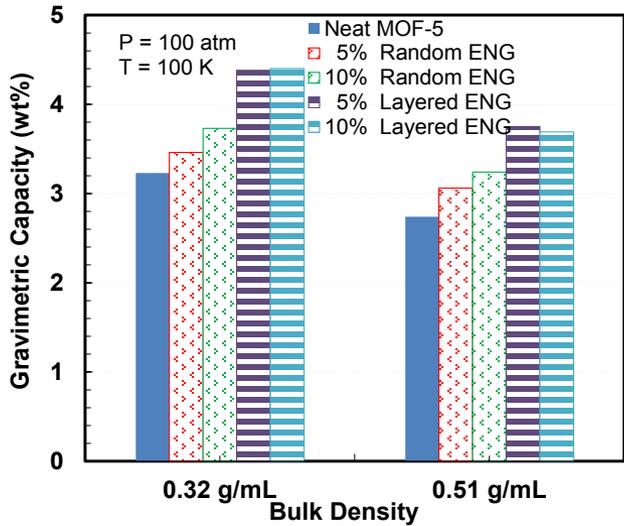
Medium Thermal Conductivity

Heat transfer model for ENG and sorbent compacts

- M. Veenstra, et al, Ford/BASF-SE/UM Activities in Support of the HSECoE, ST010, AMR 2013, 2014. and 2015
- Thermal conductivity (λ_{eff}) is a function of the graphite to sorbent powder weight ratio and the fill factor¹
- Series-parallel resistance model for heat transfer in random ENG structures
- Parallel resistance model for heat transfer in layered ENG structures
- Anisotropic conductivity model for heat transfer in layered ENG structures with source terms²



Performance of Sorbent H₂ Storage System: PRELIMINARY RESULTS



Study 1: 100 K Storage Temperature

- Addition of 5-wt% layered ENG to compacted MOF-5 improves gravimetric capacity by 35.6% and volumetric capacity by 9.4%

Study 2: Reverse Engineering Update

	Material Targets 2014	Material Targets 2017	Comments
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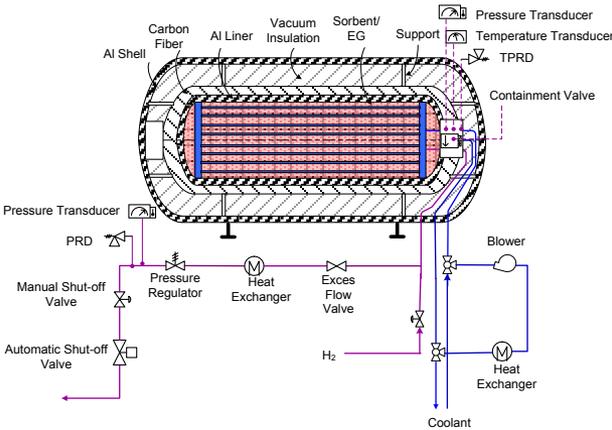
Operating Pressures and Temperatures

Storage Pressure (P)	100 bar	100 bar	
Storage Temperature (T)	155 K	155 K	20 K above coolant T
Discharge Pressure (P _d)	5 bar	5 bar	In addition to P swing, 60-K
Temperature Swing (ΔT)	60 K	60 K	ΔT allowed for 95% usable H ₂
Off-board Coolant T (T _f)	135 K	135 K	55% WTT efficiency

Material Properties

Peak Excess Uptake at 77 K	190 g-H ₂ .kg ⁻¹	150 g-H₂.kg⁻¹	5.5 wt% gravimetric capacity E ₁ = 5 KJ.mol ⁻¹
Excess Uptake at Storage P and T	120 g-H ₂ .kg ⁻¹	90 g-H₂.kg⁻¹	V _a = 0.0125 m ³ .kg ⁻¹
Medium Bulk Density	500 kg.m ⁻³	530 kg.m⁻³	C ₁ = 0.0053 atm.K ^{0.5}
Bed Thermal Conductivity	1 W.m ⁻¹ .K ⁻¹	5.5 W.m⁻¹.K⁻¹	40 g.L ⁻¹ volumetric capacity
Added ENG	20-wt% Random	5-wt% Layered	

- >25% smaller target uptake with improved thermal conductivity¹, lower ENG weight fraction, and more compact HX



FY2017 Collaborations

Cryo-Compressed Hydrogen	LLNL, BMW: LH ₂ pumps, fatigue behavior of metal liners, supercritical hydrogen storage, vacuum insulation, model validation
Compressed Hydrogen Storage	PNNL Team: 700-bar tank performance (ST101) Ford: Alternate tank design concepts Hexagon Lincoln (HL): Impact damage in Type 4 tanks Materia: Low-void resins
Sorbents	Ford, LANL: Material properties of sorbents, reverse engineering, acceptability envelope
Metal Hydrides	ORNL: reverse engineering of high-pressure metal hydrides, acceptability envelope
Off-Board Fuel Cycle Efficiency	ANL (H2A Group), ANL (HDSAM), H2IT Taskforce
Off-Board Cost	ANL (H2A Group), ANL (HDSAM), H2IT Taskforce
On-Board Cost	Strategic Analysis Inc (SA)

- Argonne develops the storage system configuration, determines performance, identifies and sizes components, and provides this information to SA for manufacturing cost studies



Physical Storage

- Validate ABAQUS model against cryogenic burst test data for cold gas storage (PNNL collaboration)
- MultiMech/ABAQUS simulation of CF composite performance degradation due to void defects, fatigue performance due to crack initiation and growth (Materia/Spencer Composite collaboration)
- Validate impact damage model and calibrate fatigue model against room temperature tank data (PNNL/HL collaboration)
- Support on-going tank projects (graded CF structure, conformable design, improved composites, low-cost glass fibers)
- Independently identify potential of cryo-CH₂ systems in fleet applications (such as buses and waste trucks) with particular focus on dormancy

Material Based Storage

- Analyze system performance with compacted sorbents using HSECoE data for materials and prototypes
- Expand system analysis of hydrogen storage in high-pressure metal hydrides
- Provide system-level support to new projects on material discovery projects, as requested

Document models and publish papers in IJHE



Project Summary

Relevance:	Independent analysis to evaluate on-board and off-board performance of materials and systems
Approach:	Develop and validate physical, thermodynamic and kinetic models of processes in physical and material-based systems Address all aspects of on-board and off-board targets including capacities, rates and efficiencies
Progress:	Demonstrated that 2-mm stainless steel (SS) liner is preferable to aluminum liner in cryo-compressed H ₂ (CCH ₂) storage systems for buses Showed that compared to the baseline 350-bar cH ₂ tanks currently in use, 500-bar CCH ₂ can achieve 66% improvement in gravimetric capacity, 132% increase in volumetric capacity, and 36% saving in carbon fiber composite (CF) Determined >7-d loss free dormancy with 95% full 500-bar CCH ₂ tanks
Collaborations:	Ford, HL, LANL, LLNL, Materia, ORNL, PNNL, SA
Future Work:	Propose, analyze and validate methods of reducing cost of CF wound storage tanks Validate models for heat transfer and H ₂ uptake models in compacted sorbents, high-pressure metal hydrides Provide system-level support to new material discovery projects

Reviewer Comments

Generally favorable reviews with the following comments/recommendations

- Reverse engineering approach to provide guidance about storage solutions for different vehicle platforms that could be considered for hydrogen delivery
- Assessment of high pressure MHs needs more emphasis on thermal management and in-depth comparison of Type 3 versus Type 4 hydride-based tanks
- Include some sensitivity analyses of key parameters is recommended
- The team should keep up efforts to publish results in a timely fashion

FY17 work scope consistent with above recommendations

- ✓ ANL is providing information and support to the Hydrogen Interface Taskforce for detailed holistic hydrogen pathway analysis
- ✓ We plan to include detailed analysis of thermal management for charging high-pressure MH tanks, in-depth comparison of Type III v. Type IV tanks, and estimates of economic value of hydride system relative to 700-bar CH₂ system
- ✓ Sensitivity analyses of key parameters were included in recent reverse engineering work
- ✓ We plan to publish the work on system analysis of cryo-compressed hydrogen storage and ABAQUS analysis of impact damage in Type IV tanks in 2017.



Technical Back-Up Slides



Publications and Presentations

Journal Publications

R.K. Ahluwalia, J.K. Peng, and T.Q. Hua, “Chemical Hydrogen Storage Material Requirements for Automotive Fuel Cell Systems,” In preparation for submission to International Journal of Hydrogen Energy. 2017.

R.K. Ahluwalia, J.K. Peng, and N. T. Stetson, “Characteristics of Low-Enthalpy Metal Hydrides for On-Board High-Pressure Hydrogen Storage Applications,” In preparation for submission to International Journal of Hydrogen Energy. 2017.

T.Q. Hua, H.S. Rho, R.K. Ahluwalia “Performance of Type-IV Compressed Hydrogen Storage System,” In preparation for submission to International Journal of Hydrogen Energy. 2017.

Book Chapters

R.K. Ahluwalia, J.K. Peng, and T.Q. Hua, “Cryo-Compressed Hydrogen Storage,” Chapter 5 in Compendium of Hydrogen Energy, Vol 2: Hydrogen Storage, Distribution and Infrastructure, R. Gupta, A. Basile, T. N. Veziroglu (Editors), Woodhead Publishing, 2016, 119-144.

R.K. Ahluwalia and T.Q. Hua, “Pressurized Systems,” Chapter 15 in Data, Facts and Figures on Fuel Cells, Detlef Stolten and Remzi and Nancy Garland (Editors), Wiley-VCH, 2016, 143-148.

R.K. Ahluwalia and T.Q. Hua, “Onboard Safety,” Chapter 18 in Fuel Cells Data, Facts and Figures, Detlef Stolten and Remzi Samsun and Nancy Garland (Editors), Wiley-VCH, 2016, 177-182.

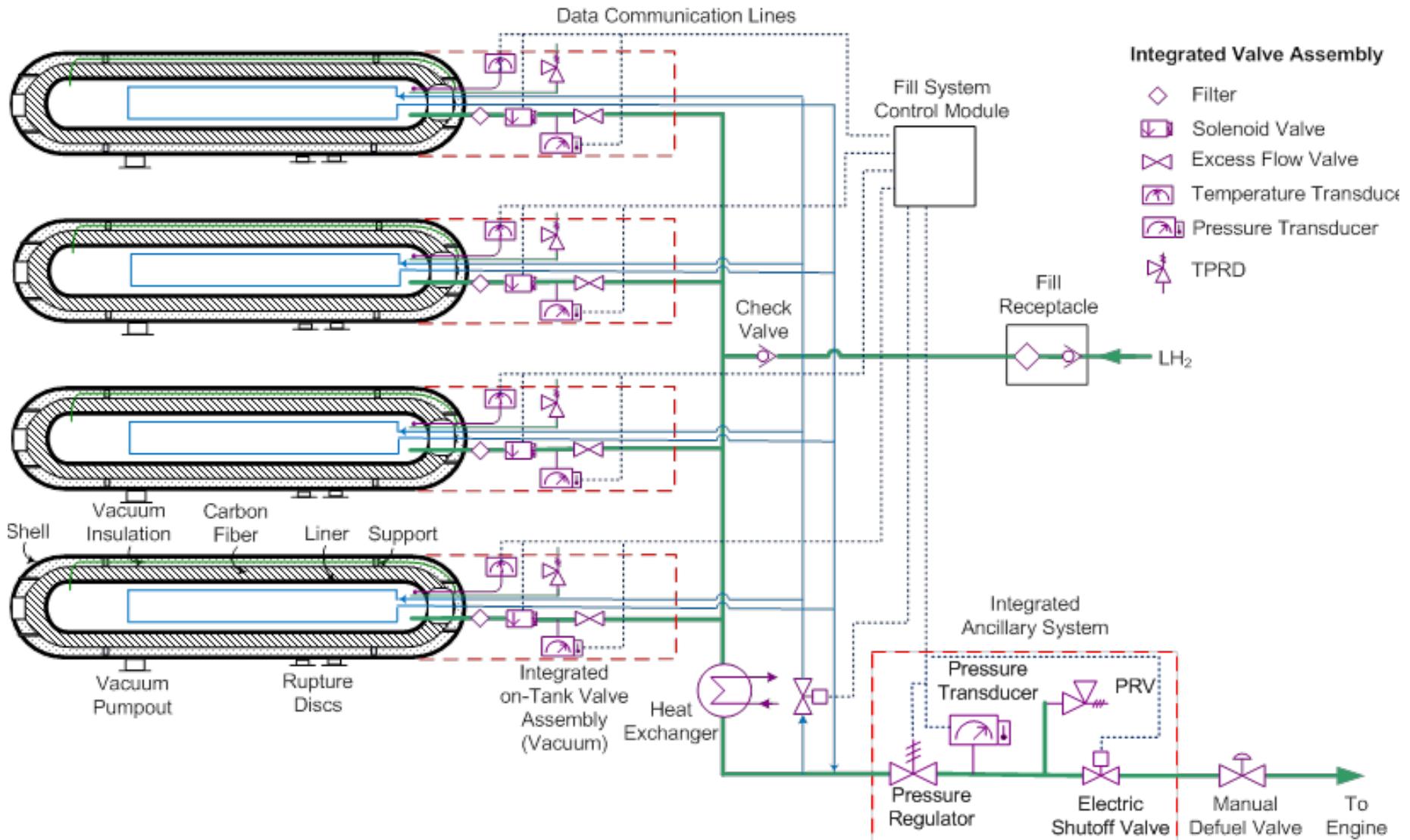
R.K. Ahluwalia, J.K. Peng, and T.Q. Hua, “Implementing Hydrogen Storage Based on Metal Hydrides,” Chapter 32 in Hydrogen Science and Engineering, Materials, Processes, Systems and Technology, Vol 2, Detlef Stolten and Bernd Emonts (Editors), Wiley-VCH, 2016, 791-808.

Presentations

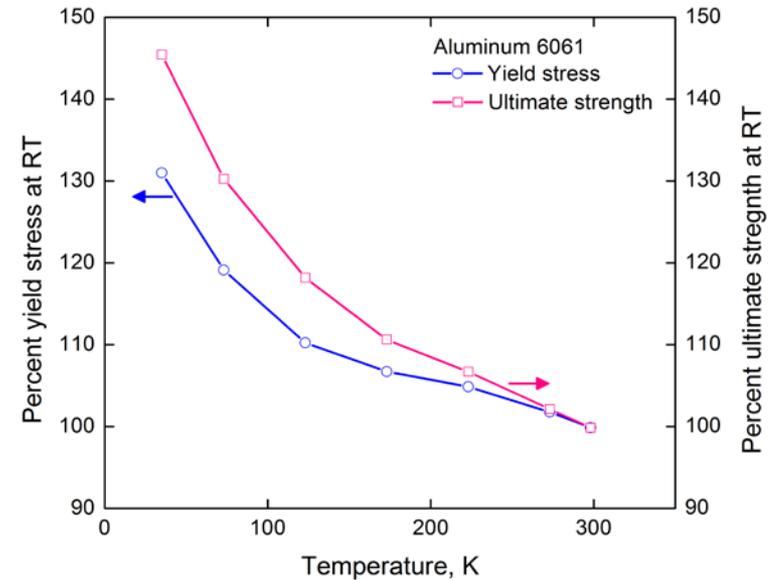
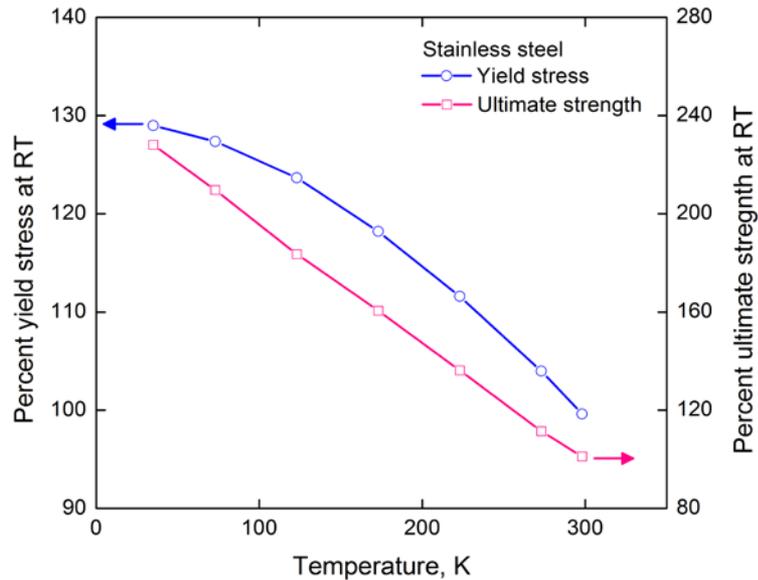
N.T. Stetson, R.K. Ahluwalia, J.K. Peng, and G. Ordaz, “Characteristics of Low-Enthalpy Metal Hydrides Favorable for High-Pressure Hydrogen Storage Applications,” 15th International Symposium on Metal-Hydrogen Systems, MH2016, Interlaken, Switzerland, August 7-12, 2016.

R.K. Ahluwalia, T.Q. Hua, J.K. Peng, and H.S. Roh, “System Level Analysis of Hydrogen Storage Options,” Hydrogen Storage Tech Team Meeting, Southfield, MI, January 9, 2017.

Schematic of CCH₂ Storage System for Buses



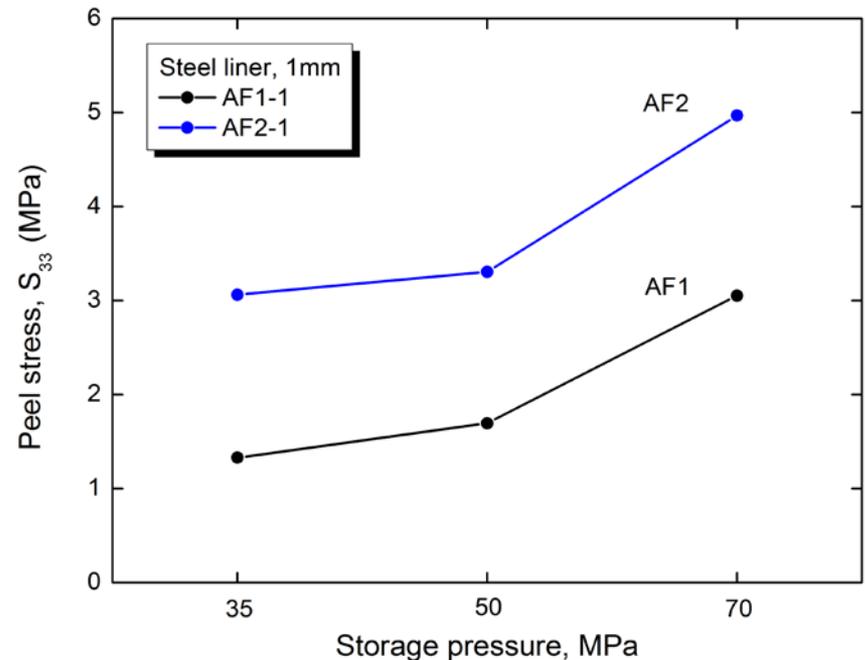
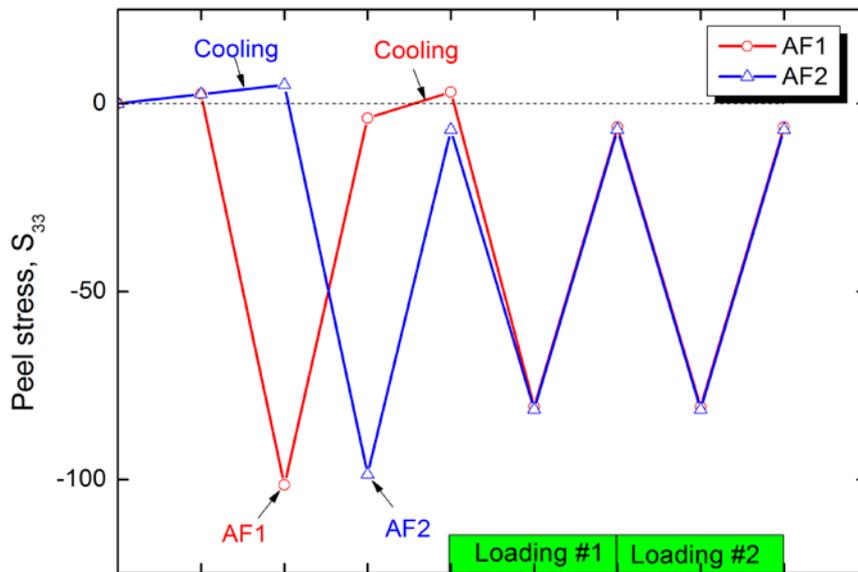
Yield Stress and Ultimate Strength



	Yield stress (MPa)		Strength (MPa)	
	84K	298K	84K	298K
Aluminum	335	282	433	333
Steel	605	475	1079	515

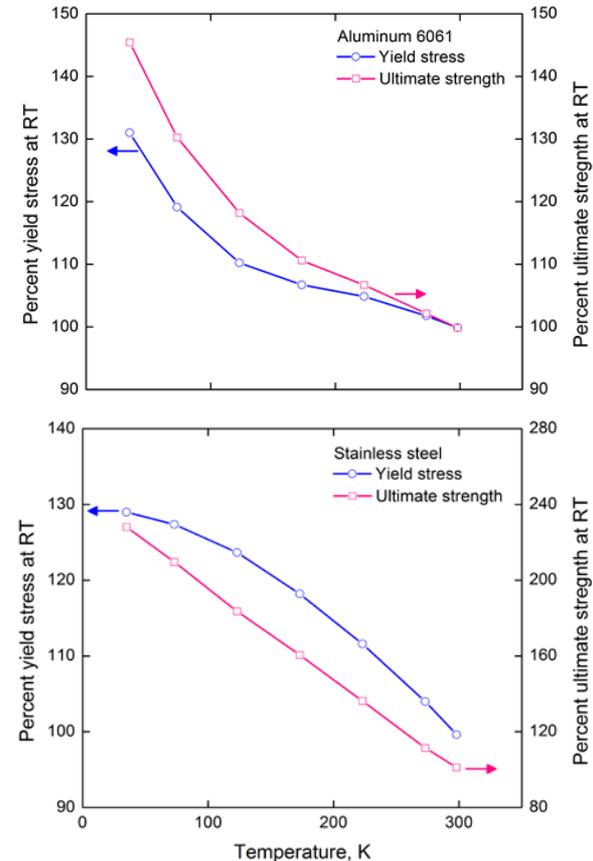
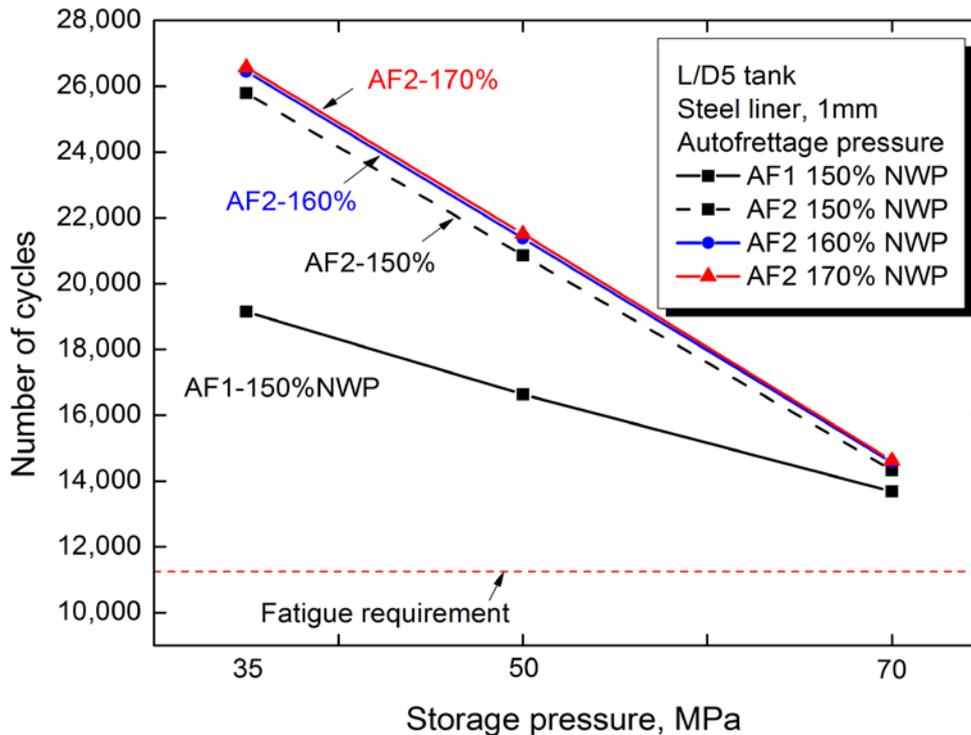
Peel Stress

- During cool down to cryogenic temperature, tensile (peel) stress is induced at the liner/CF interface due to mismatch in CTE
 - Lower peel stress if autofrettage is performed at RT
- For a 70 MPa tank, internal pressure must be maintained at >5 MPa during cool down to prevent liner debonding from composite
- Results shown are for the tank cylinder section, gaps developed during cool down (unpressurized tank) are larger in the dome than in the cylinder



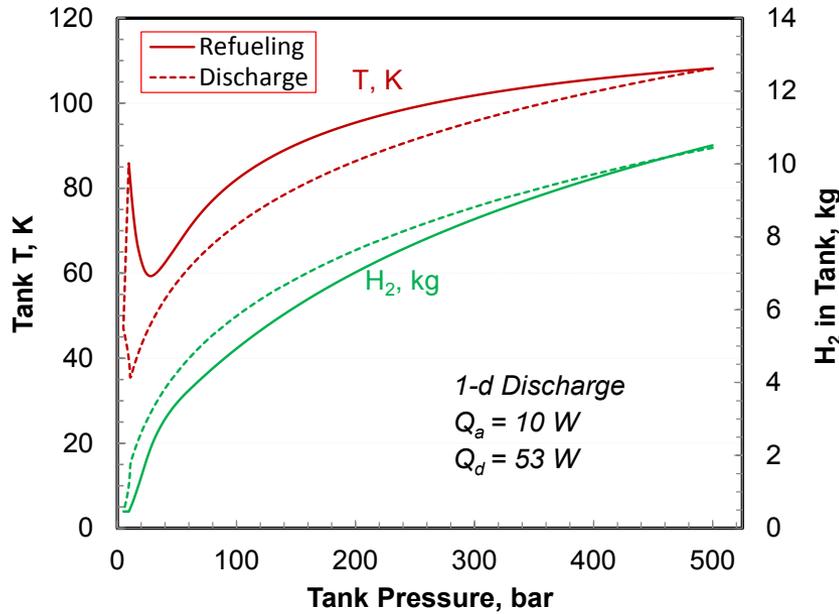
Autofrettage Pressure

- For pressure vessels, autofrettage pressure typically corresponds to proof pressure (150% NWP)
- Autofrettage performed at low temperature may be subjected to higher autofrettage pressure because yield stress and modulus of the metal are higher at lower temperature
 - Small enhancement in fatigue life by raising autofrettage to 170% NWP

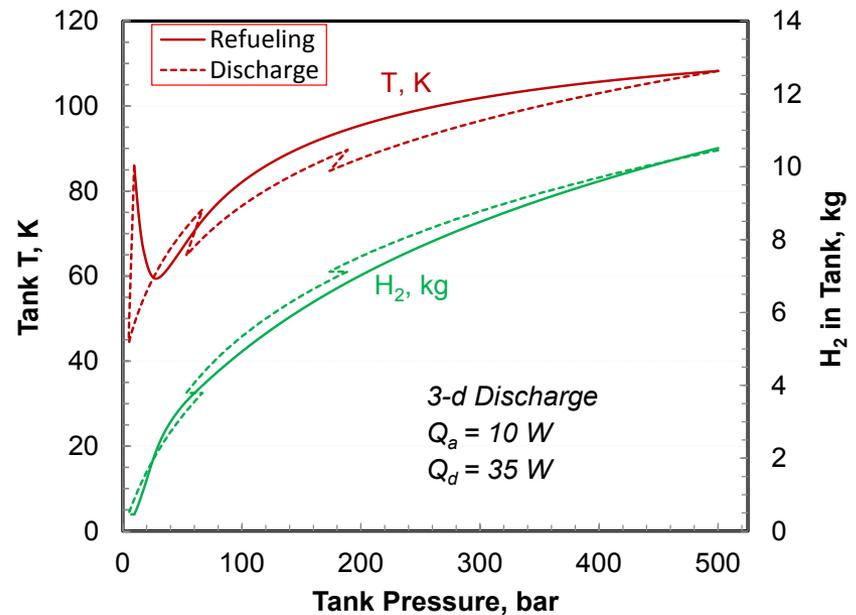
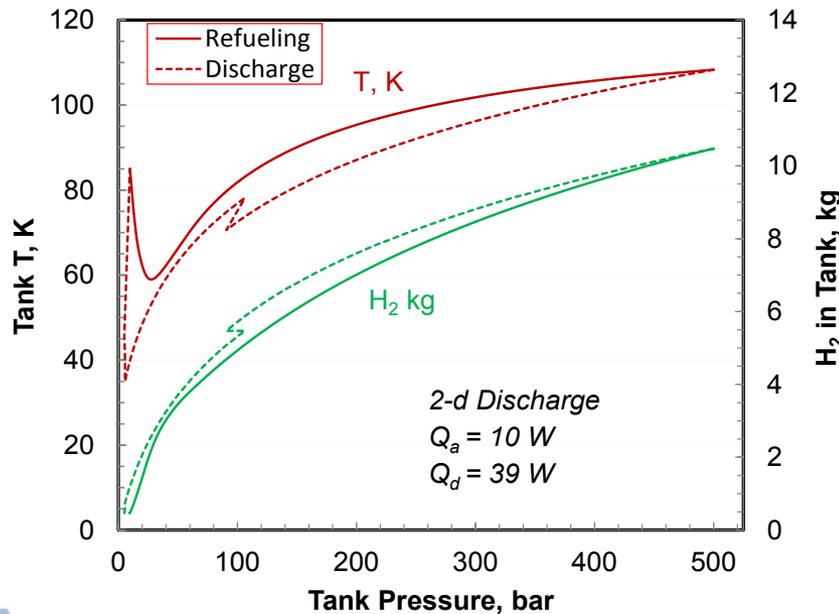


3. Repeat Charge-Discharge Cycle: 2-mm SS Liner, 500 bar

Supercritical CcH₂ storage: small heater or HX to prevent liquid formation



Storage Pressure	500 bar
Storage Temperature	108 K
Storage Density	61.9 g/L
Usable H ₂	95.6%
Gravimetric Capacity	7.3%
Volumetric Capacity	43.0 g/L

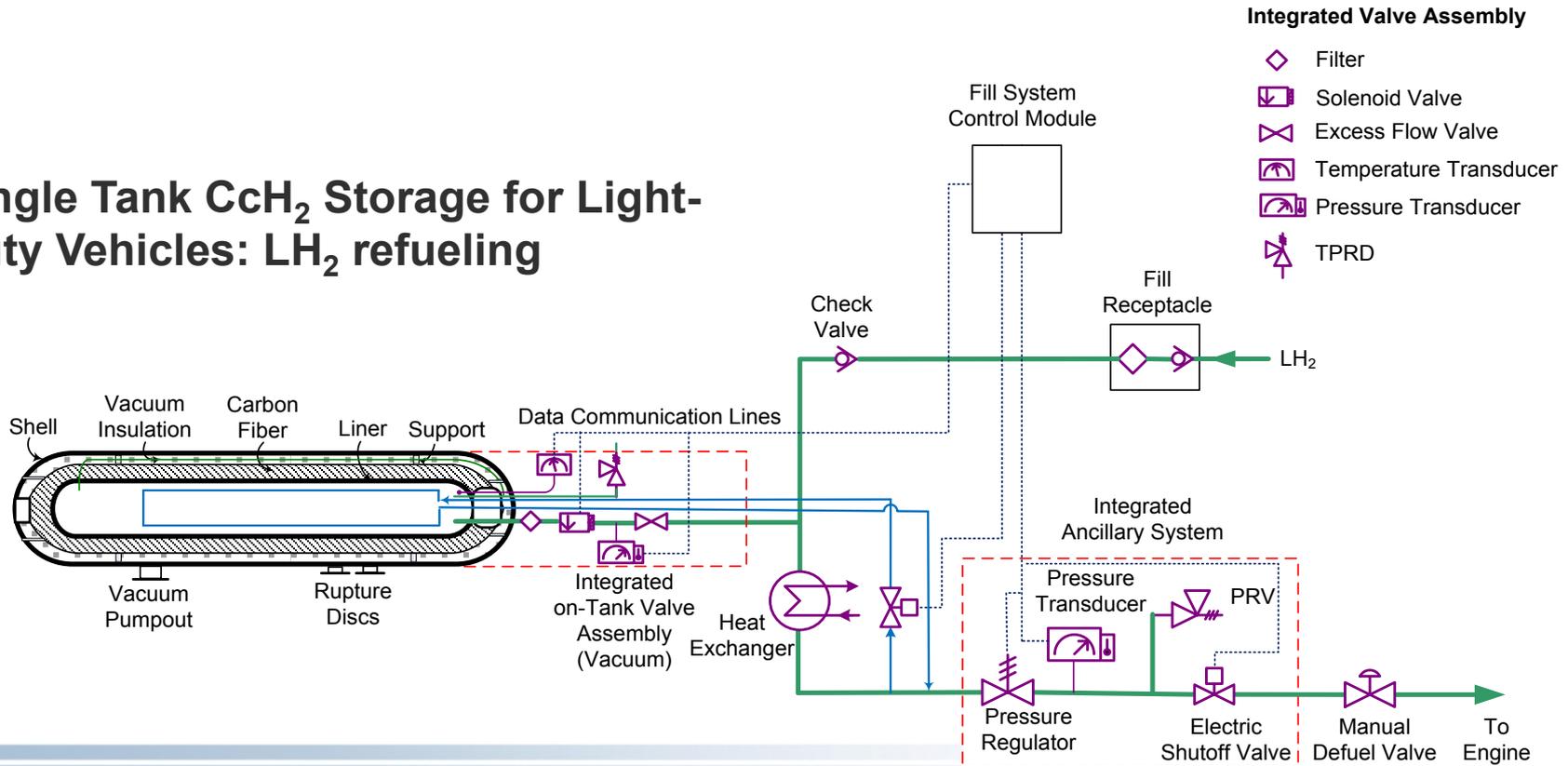


Remaining Work

Issues needing further investigation

- Effect of empty tank pressure on usable capacity
- ABAQUS fatigue modeling for combined pressure and temperature cycling
- In-tank heaters or heat exchangers, refueling receptacle and nozzle for 700-bar system
- Possible credit for using LH₂ to reduce radiator and AC loads
- CcH₂ system for light-duty vehicles (5.6 kg)

Single Tank CcH₂ Storage for Light-Duty Vehicles: LH₂ refueling



Impact Damage Analysis

Model tank damage (CF/GF composite) due to physical impact

- Transient behaviors of impact force and composite displacement
- Damage model includes fiber and matrix damage
- Horizontal and 45° drop tests (future work)
- Burst pressure after impact (degradation of tank safety factor, ongoing)
- Overwrap design to reduce impact damage (future work)

Validate FE damage model of Type IV tank with Hexagon Lincoln data

- 54-L tanks, 883 mm long, 350 mm OD, wound with CF and GF (0.9:1 ratio)
- 50 to 900 J impact energies, 24-mm hemisphere tip impactor
- Data includes force history and burst pressure

As a first step, the tank was modeled with ABAQUS to determine the failure strain at burst without impact damage

