



Corrosion-Resistant Non-Carbon Electrocatalyst Supports for PEFCs

PI: Vijay K. Ramani
Washington University in St. Louis

Project # FC145

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Overview

Timeline and budget

Competitively selected project

- **Project start date:** 03/01/16
- **Project end date:** 02/28/21
- **Total project budget:** \$ 3,397,431
 - **Total recipient share:** \$ 397,431
 - **Total federal share:** \$ 3,000,000
 - **Total DOE funds spent**:** ca.\$ 2,700,000

* ** As of 4/30/20.

Barriers to be addressed:

- A. Durability
- C. Performance
- B. Cost

	2020 Target
Loss in catalytic (mass) activity ^{a,b}	<40% loss
Loss in performance at 0.8 A/cm ² _a	30mV
Loss in performance at 1.5 A/cm ² _b	30mV
Mass activity @ 900 mV _{iR-free} ^c	0.44A/mg _{PGM}

Partners

- Project lead: Washington University in St. Louis
- Partners (sub-contractors):
 - Nissan Technical Center, North America
 - University of California, Irvine



Relevance

Impact of carbon corrosion on PEFCs

Carbon is mainly used as an electrocatalyst support due to its:

- High electrical conductivity ($> 20 \text{ S/cm}$)
- High BET surface area : $200 - 300 \text{ m}^2/\text{g}$
- Low cost

Electrochemical oxidation of carbon occurs during fuel cell operation

- $\text{C} + 2\text{H}_2\text{O} \rightarrow \text{CO}_2 + 4\text{H}^+ + 4\text{e}^-$ $E^\circ = 0.207 \text{ V vs. SHE}$

Carbon corrosion is accelerated:

- During start/stop operation (cathode carbon corrosion)
- Under fuel starvation conditions (anode carbon corrosion)

Kinetic and ohmic losses result due to:

- Pt sintering and loss of contact between Pt and C

Mass transport losses occur due to

- Formation of hydrophilic groups => flooding



Relevance

Research objectives: Technical targets

- Conducting, doped, non-PGM metal oxides (electron conductivity >0.2 S/cm)
- High surface area (>70 m²/g)
- Exhibits SMSI with Pt
- Corrosion resistant (DOE 2020 targets)
- High electrocatalyst performance (DOE 2020 targets)

Metric	Units	SoA (Pt/C)*	SoA (Pt/RTO)	Proposed approach status (Pt/TiO ₂ -Ta)**	Project target
Total PGM content	g kW ⁻¹	0.55	0.55	Not Available	0.25
Total PGM loading	mg cm ⁻²	0.4	0.4	0.6	0.25
Voltage at 1.5 A cm ⁻² (air)	V	0.45	0.48	0.3	0.55
Loss in mass activity ^{a,b}	% loss	32	33	<10%	<5%
Voltage loss at 0.8 A cm ⁻² ^a	mV	81	9	< 15	<10
Voltage loss at 1.5 A cm ⁻² ^b	mV	182 ⁺	20	N/A; 20 mV at 1Acm ⁻²	<20
Mass activity@900 mV _{iR-free} ^c	A mg ⁻¹ _{PGM}	0.07	0.07	ca. 0.05	0.3

^a-Table E1, ^b-Table E2; Appendix E of FOA; ^c DOE protocol per appendix E of FOA; *Pt/C refers to Pt/Graphitized Ketjen Black tested at NTCNA; **Results from entirely un-optimized MEAs run primarily to test stability. ⁺Pt/HSAC durability is much worse – MEA does not run beyond 0.5 A cm⁻² after start-stop cycling. **Data from MEA in a PEFC**



Approach

Milestones

2nd
Year

- | | |
|----|---|
| Q5 | <ul style="list-style-type: none"> Demonstrate SMSI as ascertained by Pt d-band filling (XPS) (100%) Meet durability target in RDE (ECSA Loss <5% - 10,000 start-stop cycles) (100%) |
| Q6 | <ul style="list-style-type: none"> Demonstrate 10% increase in mass activity (BoL in RDE) at 0.9V over Pt/C benchmark (100%) |
| Q7 | <ul style="list-style-type: none"> B.E.T. Area > 70 m² g⁻¹; Particle size < 70nm; conductivity of at least 0.2 S cm⁻¹ (100%) Meets stability and durability in RDE per DOE metrics (ECSA Loss <5%) (100%) |
| Q8 | <ul style="list-style-type: none"> 20-40wt%Pt; Surface area > 70 m² g⁻¹ Pt particle size 3-6nm; (100%) Meets DOE 2020 durability targets in RDE and MEA (100%) |

- | | |
|----|--|
| Q9 | <ul style="list-style-type: none"> Demonstrate “End Project” durability metrics and at least 80% of “end project” mass activity metric in MEA (80%) |
|----|--|

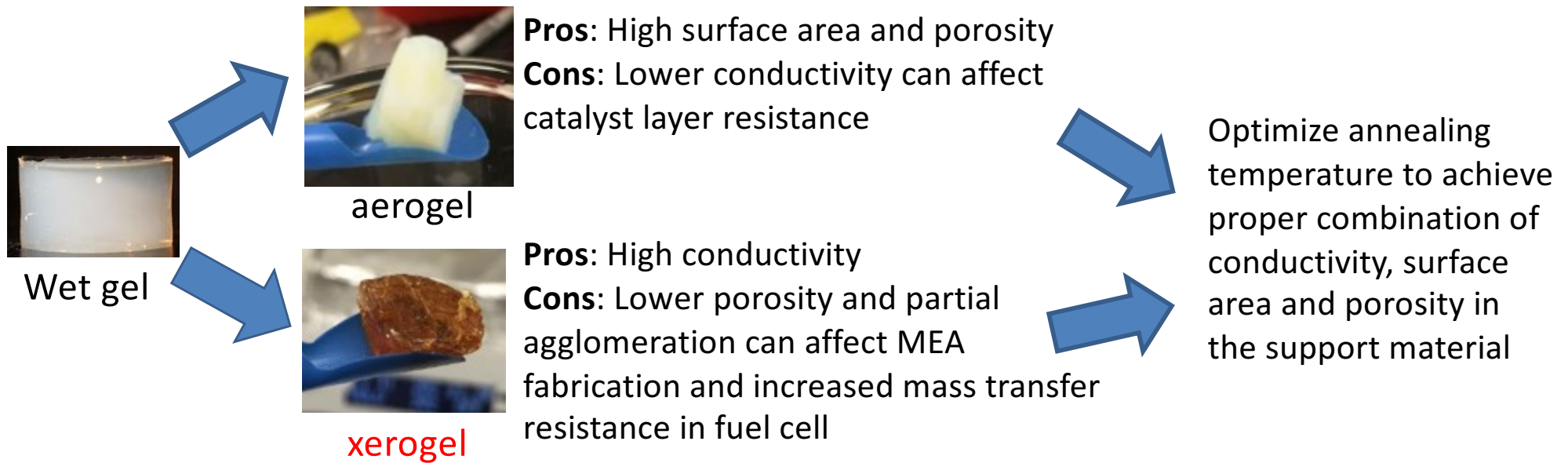
3th
Year

- | | |
|----|---|
| Q2 | <ul style="list-style-type: none"> In addition to Milestone 6.2.1, meet “End Project” BoL mass activity target (Table 2) (80%) |
| Q3 | <ul style="list-style-type: none"> Specify cost of best 2 Pt/DS materials (80%) |
| Q4 | <ul style="list-style-type: none"> Meet “End Project” durability, activity, and performance targets in Table 2 (80%) |

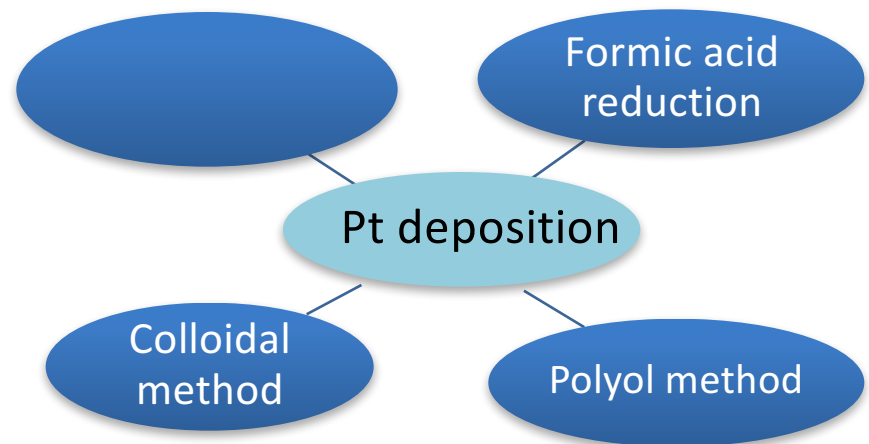
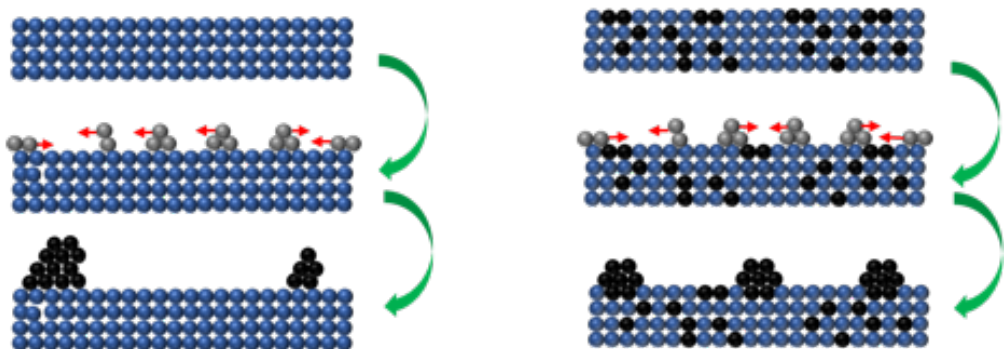


Approach

Support Synthesis and Pt deposition strategy

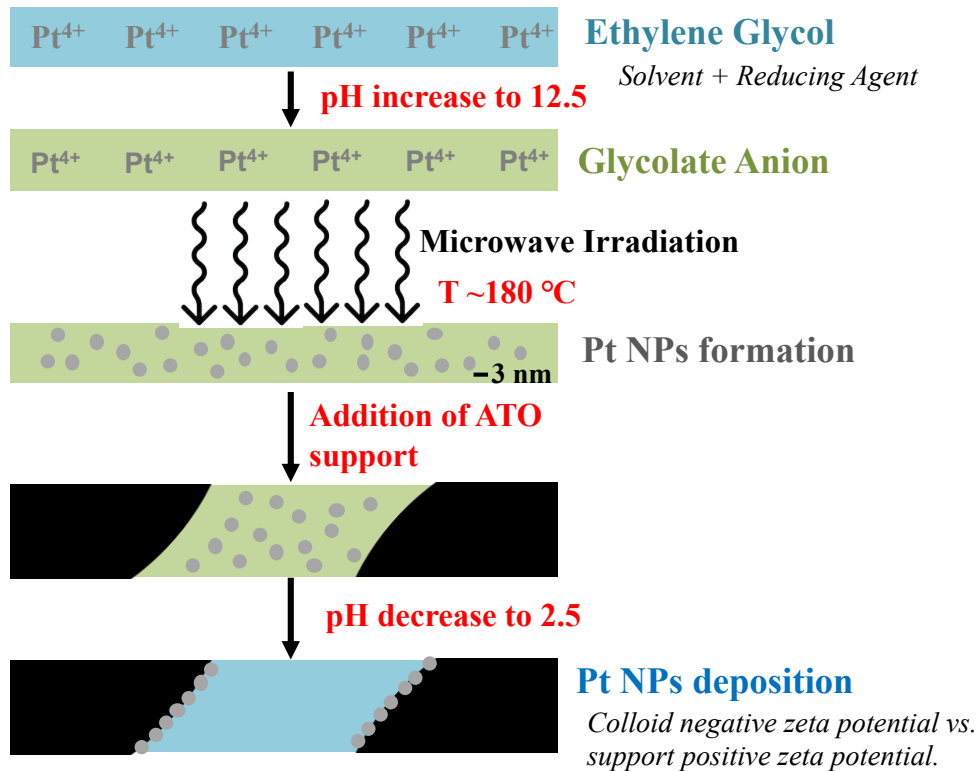


Pt seeded Support



Approach

Support Synthesis and Pt deposition strategy

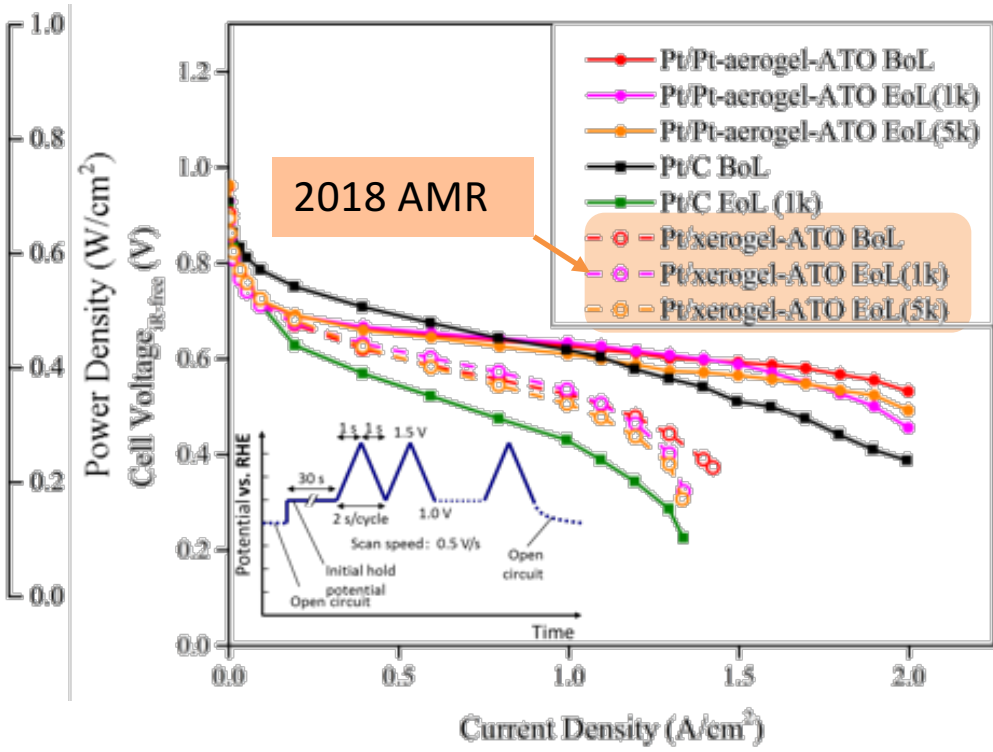
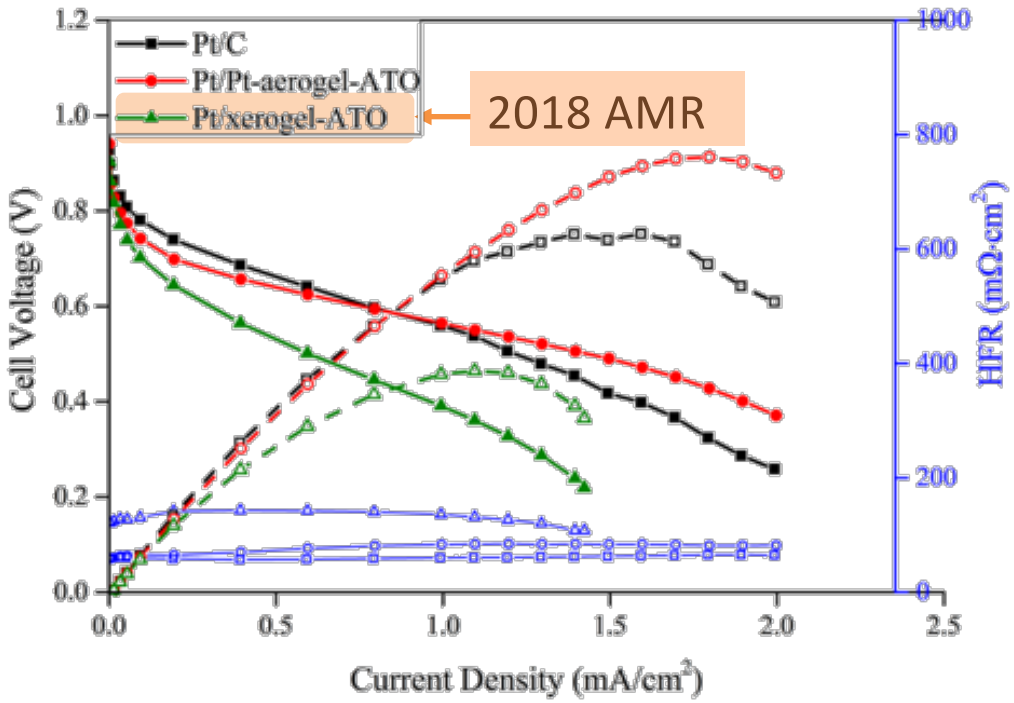


Schematic of Microwave assisted Polyol synthesis

Both Microwave-assisted Polyol Synthesis and ALD have also been used for alloy (e.g. Pt-Ni) deposition

Accomplishments and Progress (Prior)

Pt-aerogel-ATO MEAs exhibit excellent performance and durability



Comparison of fuel cell performance (H₂/Air) obtained for Pt/xerogel-ATO, Pt/Pt-aerogel-ATO and Pt/Vulcan Carbon before (BoL) and after (EoL) start-stop protocol for 1,000 and 5,000 cycles at 80°C, 90%RH and 200 kPa_{abs}. Pt loading at the cathode: 0.10 mg_{Pt}/cm². Pt loading at the anode: 0.10 mg_{Pt}/cm².



Accomplishments and Progress

Characterization results of various oxide supports and alloy catalysts:

Metal Oxide	BET SA ($\text{m}^2 \text{g}^{-1}$)	Electrical Conductivity (S cm^{-1})
Sb-SnO ₂	60.6685	Need to be measured
Ru-TiO ₂	40.0111	Need to be measured

Metal Oxide	Pt Loading (wt%)	Pt:Ni ratio
Pt/Sb-SnO ₂	5.92	---
Pt/Ru-TiO ₂	1.90	---
Pt-Ni/Sb-SnO ₂	9.53	0.83:0.17
Pt-Ni/Ru-TiO ₂	2.81	0.77:0.23



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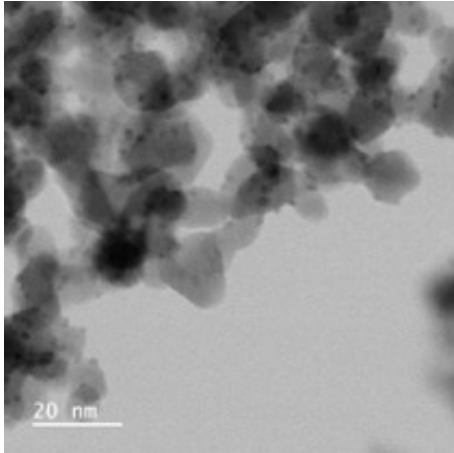


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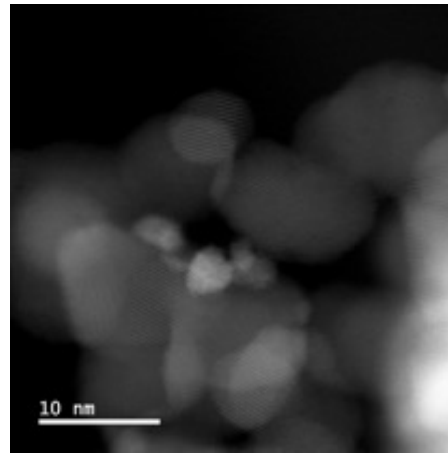
Accomplishments and Progress

Characterization results of various oxide supports and alloy catalysts:

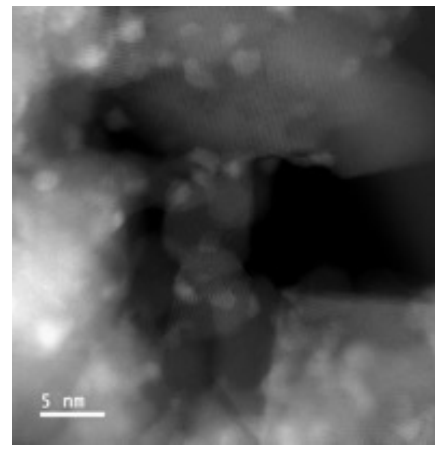
Pt-Sb-SnO₂



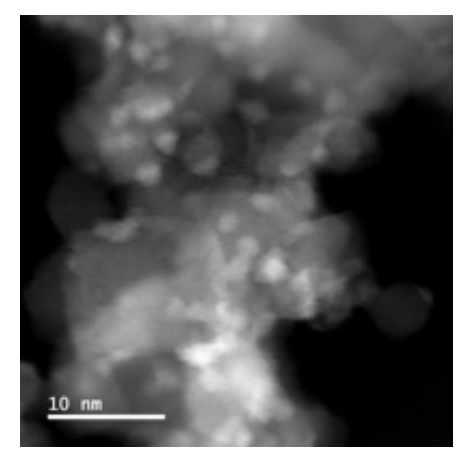
Pt-Ni/Sb-SnO₂



'Pt-Ru-TiO₂



Pt-Ni-Ru-TiO₂

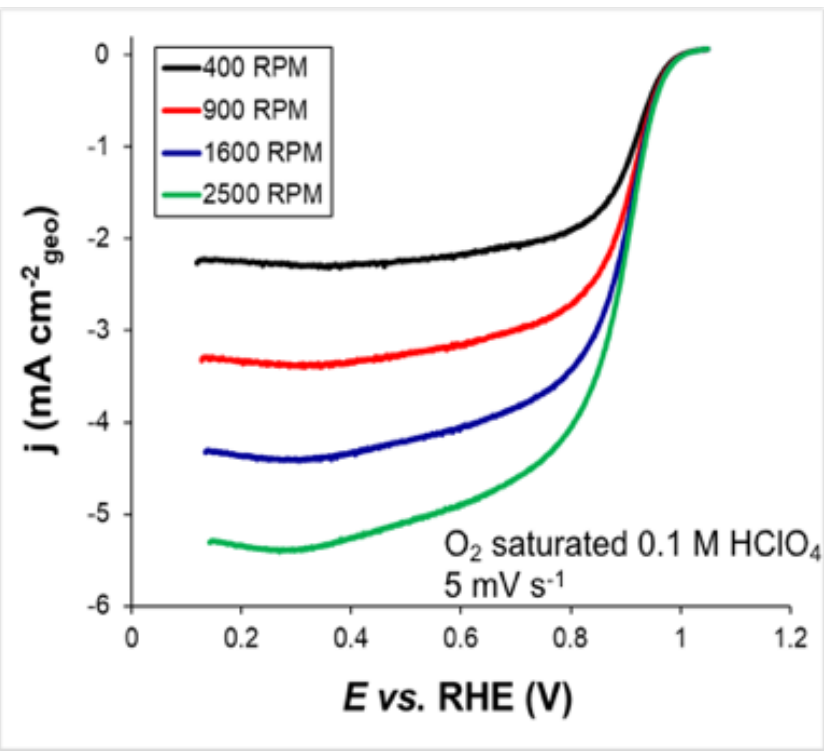
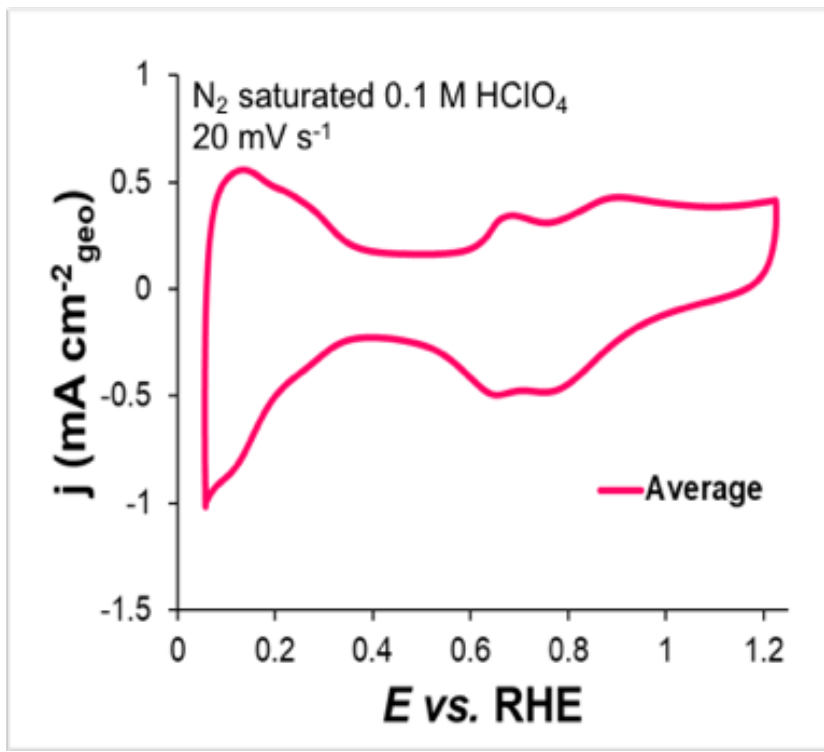


Well-dispersed alloy electrocatalysts obtained on our metal oxide supports
Further optimization of synthesis is ongoing

Accomplishments and Progress

Electrochemical Characterization

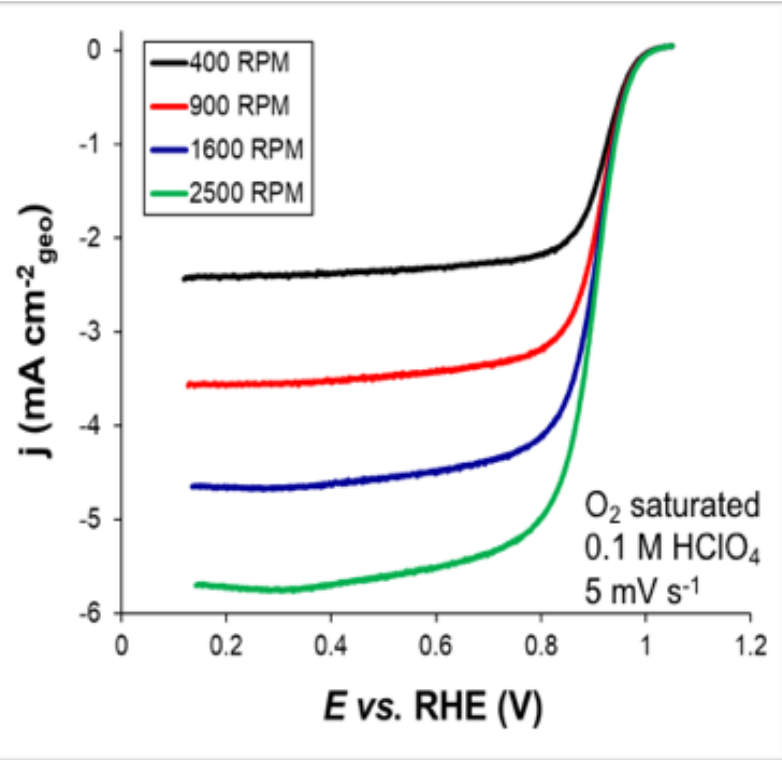
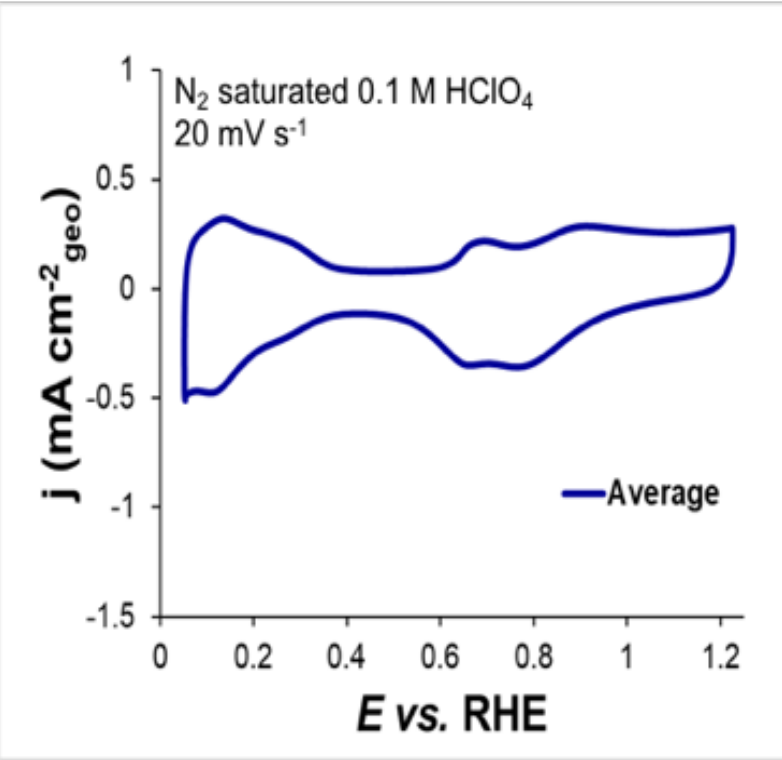
Pt/Sb-SnO₂



Accomplishments and Progress

Electrochemical Characterization

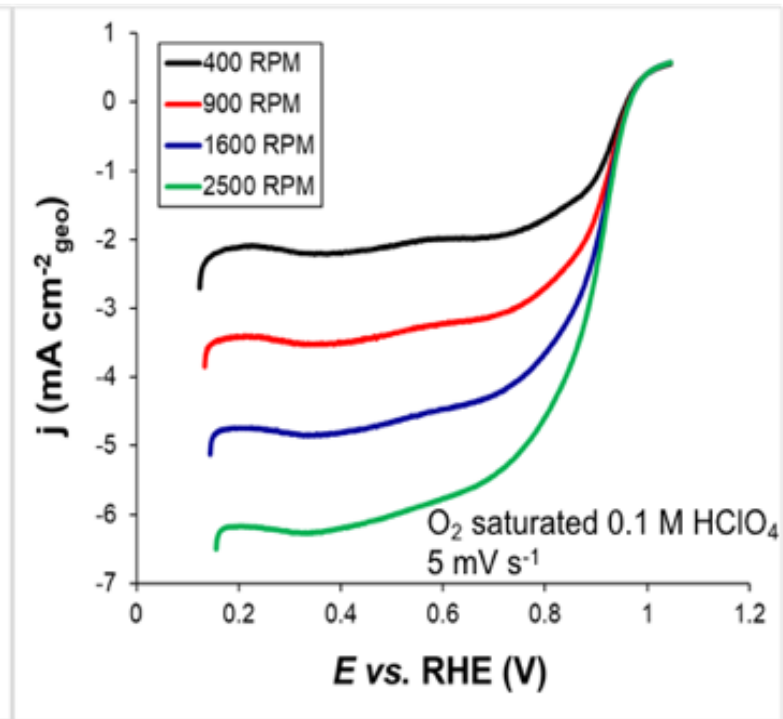
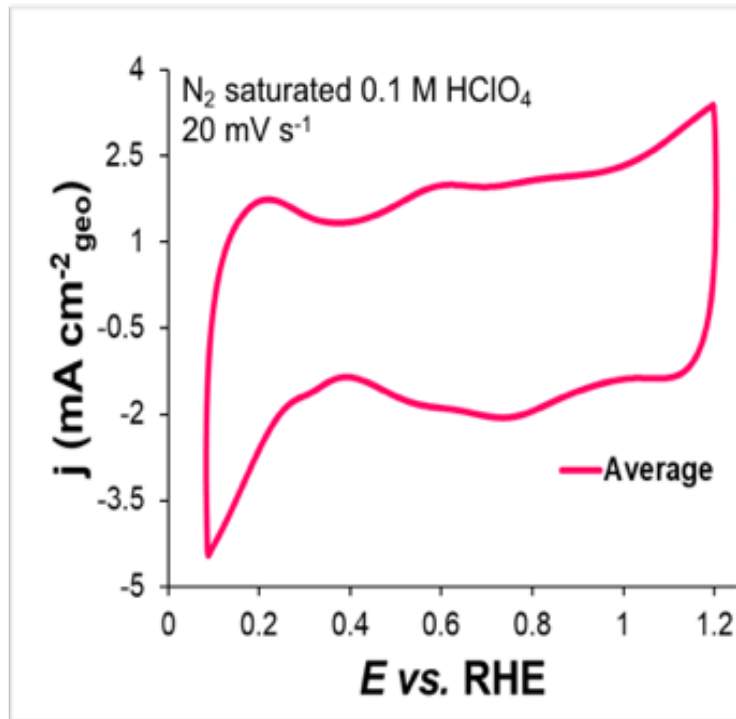
Pt-Ni/Sb-SnO₂



Accomplishments and Progress

Electrochemical Characterization

Pt/Ru-TiO₂



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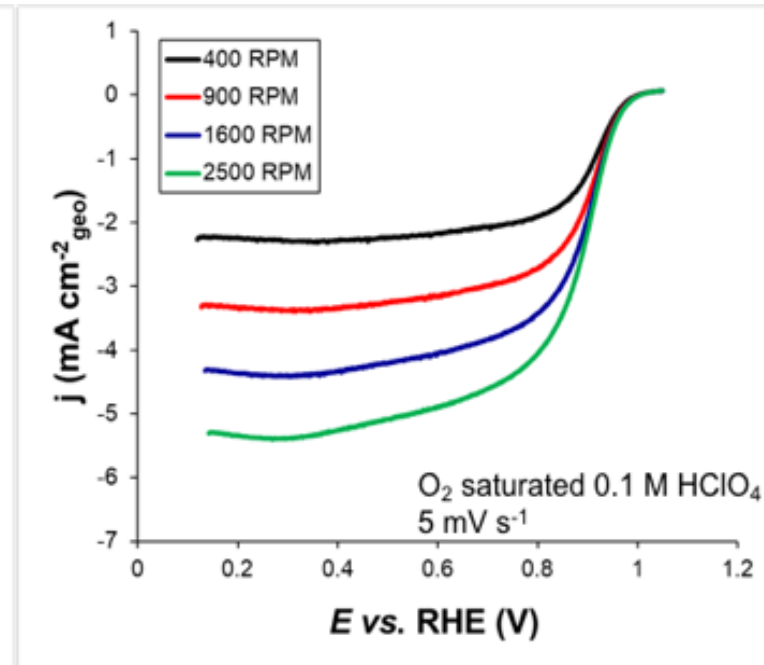
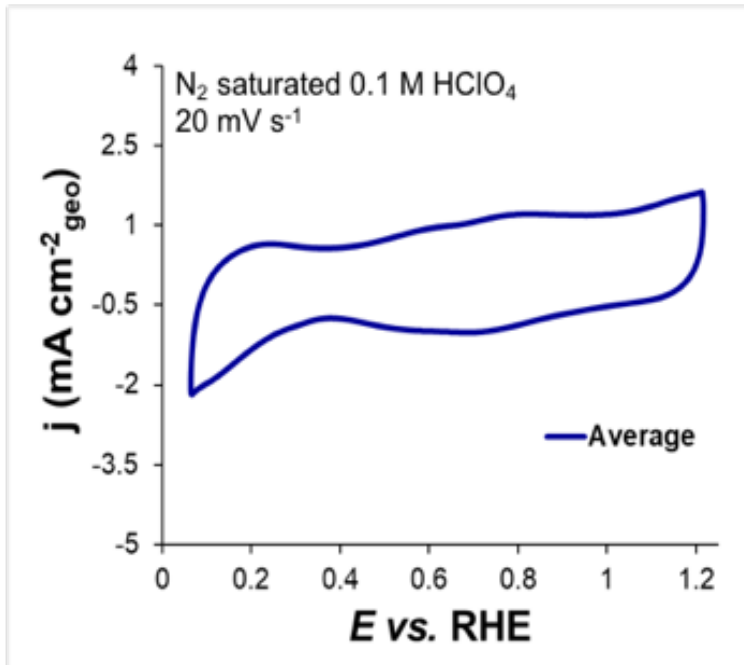


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Accomplishments and Progress

Electrochemical Characterization

Pt-Ni/Ru-TiO₂



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Accomplishments and Progress

Electrochemical Characterization: Analysis

Catalyst	Pt Specific Surface Area (m ² /g)	MA (A g ⁻¹ _{Pt}) @0.95 V	Current Density (μA cm ⁻²)	MA (A ⁻¹ g _{Pt}) @ 0.90 V	Current Density (μA cm ⁻²)
Pt/Sb-SnO ₂	45.56 ± 2.63	18.84 ± 0.51	41.46 ± 3.50	91.97 ± 0.77	202.14 ± 9.96
Pt-Ni/Sb-SnO ₂	29.04 ± 1.22	21.98 ± 1.63	75.72 ± 5.31	132.31 ± 11.72	456.14 ± 46.65

*all data presented here are corrected from the diffusion in solution and of the ohmic losses in solution

Catalyst	Pt Specific Surface Area (m ² /g)	MA (A g ⁻¹ _{Pt}) @0.95 V	Current Density (μA cm ⁻²)	MA (A g ⁻¹ _{Pt}) @0.90 V	Current Density (μA cm ⁻²)
Pt/Ru-TiO ₂	36.69 ± 10.82	31.15 ± 1.59	89.88 ± 25.45	151.2 ± 11.36	461.04 ± 125.36
Pt-Ni/Ru-TiO ₂	7.97 ± 1.76	18.18 ± 1.38	238.13 ± 67.99	63.50 ± 6.10	868.96 ± 273.22

*all data presented here are corrected from the diffusion in solution and of the ohmic losses in solution



Accomplishments and Progress

Electrochemical Characterization: Discussion

- Using appropriate synthesis methods, UCI is able to deposit Pt-Ni alloy catalysts on the WashU metal oxide supports to yield viable catalysts.
- Optimization remains to be done to further increase mass activity, but the first estimates of mass activity are quite promising
- Sb-SnO₂ supports are the primary target here given cost considerations.
- Nb-TiO₂ and Ta-TiO₂, two other candidates, had issues with electrical conductivity.



Reviewer Comments

Rotating disk electrode results show better mass activity for Pt/aerogel-NbTiOx. However, the MEA performance is well below that of Pt/C. Even worse, the durability of the Pt/aerogel is substantially worse. Comments were made that this is due to loss of conductivity, which is likely going to happen under other conditions as well. Thus, these materials do not seem overly promising for long-term durability. Therefore, it seems like work can end on these materials.

We are on our way to down-selecting with ATO emerging as a prime candidate. Early alloy work also supports this choice.

In the future, load-cycling data should be discussed to confirm that these catalysts and supports are also effective for the drive-cycle requirements. It is good that the project is presenting cost modeling results; however, the team needs to consider the system mitigation cost, not a stack replacement, as the baseline. It is known publicly that Toyota and General Motors have system mitigation strategies that would not require a stack replacement. Determining the cost of this mitigation may not be easy, but some type of estimate should be derived to determine the real value of the non-carbon support.

The team will appreciate any DOE insight on the cost value of OEM mitigation system and associated mitigation cost. The team has no sources or resources to technically make these assumptions. Based on insights that we have received in private conversations with automotive OEMs (with people heavily involved in stack development), it would appear that the mitigation approaches are quite expensive (equivalent to stack cost or significant fraction thereof), and also that they can exacerbate anode catalyst corrosion. We continue to believe that a materials solution is the best approach.



Reviewer Comments

Pt alloy development should have started earlier in the project. It is doubtful the project will be able to accomplish good activity performance in such a short time before the final deliverable. There is no mention of catalyst durability testing. While the support stability seems reasonable, the Pt stability on the metal oxide supports might be affected.

It was NOT originally in the funded SOPO, we accepted modification without seeking additional funds, and with a NCE (due to moving) we will manage to do it!

Preparing Pt-alloy can lead to improved mass activity and meeting the project milestone of achieving 0.3 A/mgPGM. However, the PI did not specify the type of Pt-alloy catalysts that the project will prepare in the third year.

We will begin with Pt-Ni, as shown in our results.



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Collaboration

Washington University in St. Louis

- Lead PI and Technical PoC: **Vijay K. Ramani**, Roma B. and Raymond H. Wittcoff Professor of Washington University in St. Louis
- Metal oxide synthesis and characterization, RDE testing (ORR activity and electrochemical stability), PEFC evaluation



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- PI and Technical PoC: **Nilesh Dale** (Manager-Fuel Cell and Business Research)
- Electrochemical evaluation of the catalysts in PEMFC



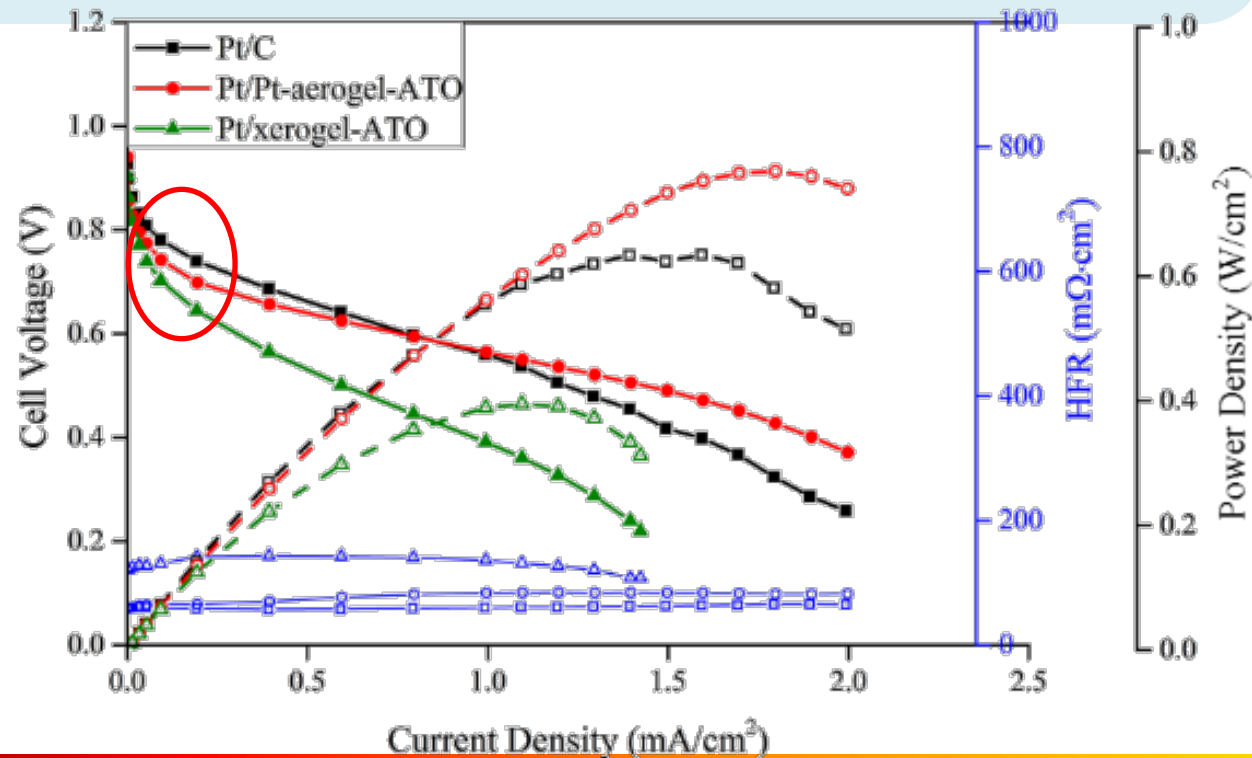
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- PI and Technical PoC: **Plamen Atanassov** (Chancellor's Professor)
- Modeling of doped MO conductivity and SMSI (DFT), scale-up of doped metal oxide synthesis



Remaining Challenges and Barriers

- Enhance the mass activity in low current region and retain stability at the same time.
- Optimize the ionomer loading in fuel cell for the metal oxide supported catalyst



Remaining Challenges and Barriers

- We will need to optimize the synthesis of Pt-alloy catalysts on our stable supports (likely Sb-SnO₂) – this was an addition to the project scope and we are underway to accomplish this with a NCE.
- Both Microwave-assisted polyol synthesis and ALD methods are in use to accomplish this task
- The alloy catalysts will provide a pathway to meeting remaining activity milestones.



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Proposed Future Work

FY 2020/21

- WUSTL: Materials synthesis and characterization
 - ✓ Support UCI efforts to prepare Pt-Alloy/MO_x support catalysts by providing adequate quantities of support.
- Nissan North America Inc.: durability/performance testing
 - ✓ NTCNA role is concluded. But they will serve to prepare and evaluate Pt-alloy MEAs on a no additional cost basis.
- University of California, Irvine
 - ✓ Pt-alloy catalyst deposition on WUSTL supports using ALD and microwave-assisted polyol synthesis methods
 - ✓ Physico-chemical and electrochemical characterization of synthesized Pt-alloy catalysts
 - ✓ Providing catalyst to NTCNA for MEA fabrication and evaluation



Summary

- **Objectives and approach:**
 - Synthesize doped metal oxides and Pt seeded metal oxide for catalyst supports.
 - High conductivity, BET surface area, and high porosity.
 - Exhibits SMSI and corrosion resistance (attaining DOE 2020 targets)
- **Relevance**
 - Material-level mitigation strategies can solve cathode durability issues
- **Accomplishments**
 - Pt deposited on Niobium doped titanium oxides shown high mass activity in the fuel cell in kinetic region. NTO – not stable in MEA. ATO is highly stable.
 - Added 1wt% Pt as seed during aerogel ATO synthesis (Pt-aerogel-ATO) to engineer the morphology and crystal structure of the. Met durability target in fuel cell test.
 - **ALD and microwave-assisted polyol synthesis used to deposit Pt-alloy catalysts onto ATO supports**
- **Collaborations**
 - Washington University in St. Louis
 - Nissan Technical Center, North America
 - University of California, Irvine

