

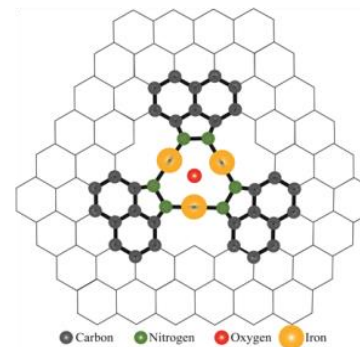
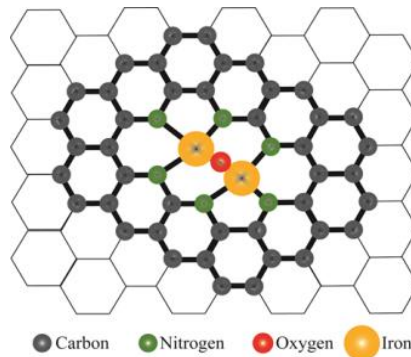
# Developing Platinum Group Metal-Free Catalysts for Oxygen Reduction Reaction in Acid: Beyond the Single Metal Site

P. I. Qingying Jia

Northeastern University

Project ID# FC302

05/29/2020



This presentation does not contain any proprietary, confidential, or otherwise restricted information



Northeastern University  
Center for Renewable Energy Technology



# Overview



## Timeline

- Project Start Date: 10/01/2018
- Project End Date: 03/31/2021

## Budget

- Total Project Budget:  
\$1,020,000.00
  - Total Recipient Share:  
\$250,000.00
  - Total Federal Share:  
\$770,000.00
  - Total DOE Funds Spent\*:  
\$460,397.86

\* As of 05/25/2020

## Barriers

- Performance in PEMFCs
- Durability in PEMFCs

## Partners

- Lawrence Berkeley National Laboratory  
Adam Weber
- Northeastern University  
Sanjeev Mukerjee
- Project lead  
Qingying Jia (NEU)



**Objectives**: Development of PGM-free ORR catalysts with high performance and durability in PEMFCs.

- Development of  $M_x$ -N-C catalysts featured with multiple metal centers (MMCs).
- Synthesis of  $M_{(x)}$ -N-C catalysts via surface deposition methods to bypass the necessity of pyrolysis.

**Relevance**: Our approaches move beyond the M-N-C catalysts featured with single metal sites and traditional synthesis routes pyrolyzing the mixture of metal, N, and C precursors. The new catalysts may address the limited activity, durability, and active site density of M-N-C catalysts and meet the DOE targets.

## **Targets**:

- $0.035 \text{ A/cm}^2$  at  $0.9 \text{ V}$  in a  $\text{H}_2$ - $\text{O}_2$  PEMFC (1.0 bar partial pressure,  $80^\circ\text{C}$ )
- Loss in activity  $\leq 40\%$  after 30,000 square wave cycles with steps between  $0.6 \text{ V}$  (3 s) and  $0.95 \text{ V}$  (3 s) .
- Power density of  $0.5 \text{ W/cm}^2$  in a  $\text{H}_2$ -Air PEMFC with a MEA size  $\geq 50 \text{ cm}^2$

# Approach and Targets



## ➤ Synthesis

1. Ionothermal Carbonization (abandoned)
2. Chemical vapor deposition (CVD)
3. Ion Beam-Assisted Deposition (IBAD)
4. Flash pyrolysis

## ➤ Characterizations

Spectroscopy: *in situ* XAS, Mossbauer, XPS, NMR, XRD  
Microscopy: SEM, HAADF-STEM, HRTEM

## ➤ MEA fabrication

electrospinning, IBAD

## ➤ Mass transport modeling

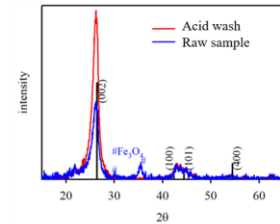
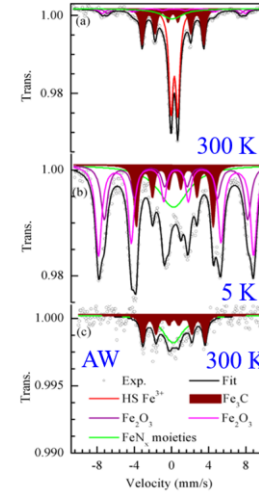
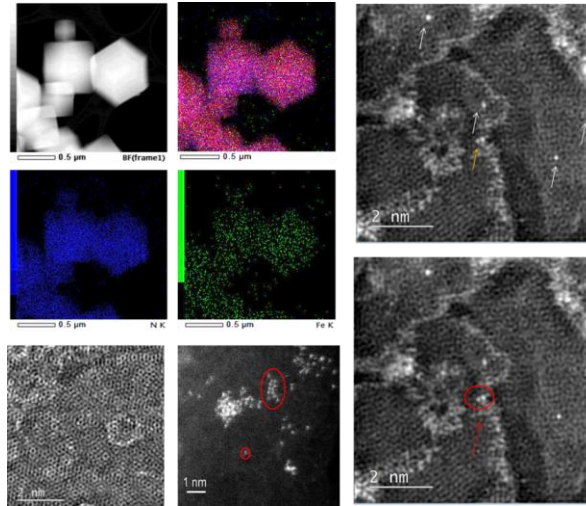
## ➤ Milestones

1.  $0.025 \text{ A/cm}^2$  at  $0.90 \text{ V}$  in a  $\text{H}_2/\text{O}_2$  PEMFC (Period 1 Go/No-Go)
2. Loss in activity  $\leq 40\%$  after 30,000 square wave cycles
3. Power density of  $0.5 \text{ W/cm}^2$  in a  $\text{H}_2/\text{Air}$  PEMFC

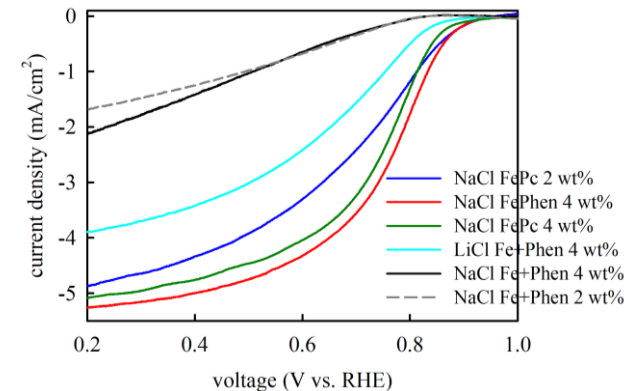
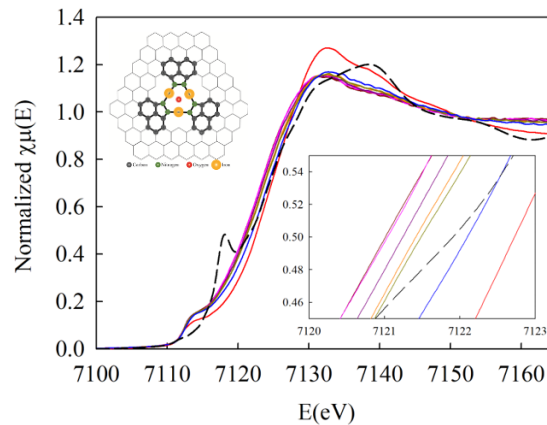
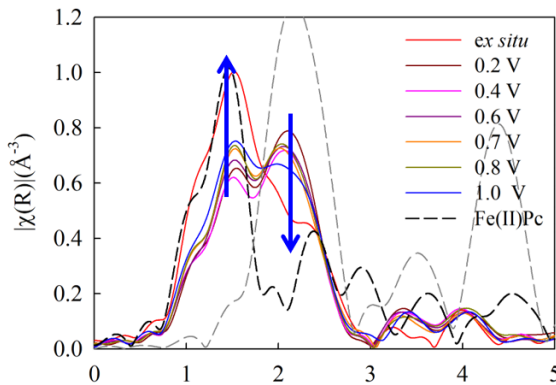


## Ionothermal Carbonization synthesis (ceased)

NaCl+ZnCl<sub>2</sub> (1:7 by wt) as molten salt; adenine as C and N precursor; Fe(Phen)<sub>3</sub>(ClO<sub>4</sub>)<sub>2</sub> as Fe precursor (Fe-N<sub>6</sub>)



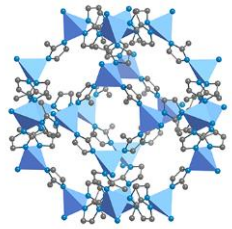
Sample	Mössbauer component	Mössbauer RA % (300 K)	Mössbauer RA % (5 K)
ICM-FePhen <sub>3</sub>	Singlet	12	22
	Fe <sub>2</sub> O <sub>3</sub> <sup>(1)</sup>	58	62
	Fe <sub>3</sub> C	30	16
ICM-FePhen <sub>3</sub> -AW	Singlet	55	NA
	Fe <sub>2</sub> O <sub>3</sub> <sup>(1)</sup>	0	NA
	Fe <sub>3</sub> C	45	NA



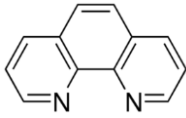
Combined characterizations show the presence of electrochemically active MMC sites in the M<sub>x</sub>-N-C catalysts, but poor ORR activities in RDEs.



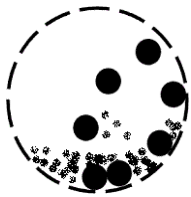
## Synthesis of microporous N-C substrate without iron



ZIF-8



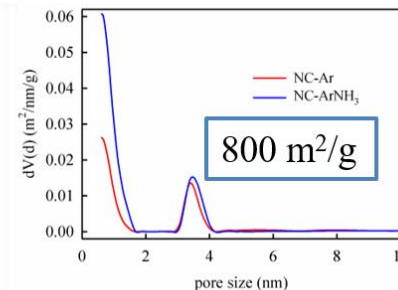
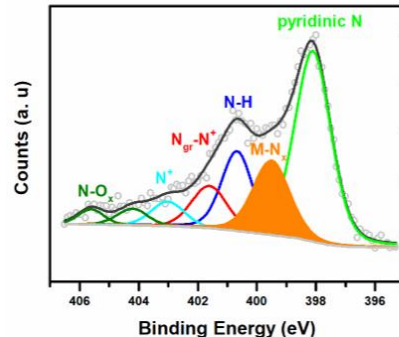
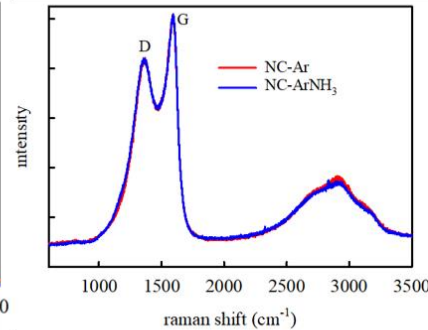
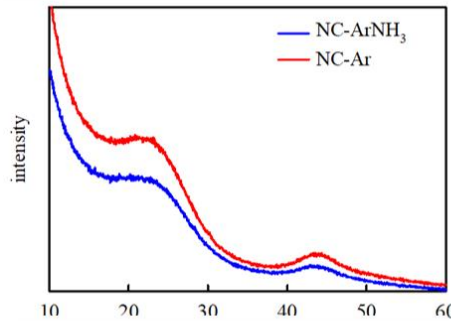
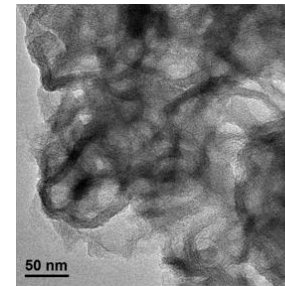
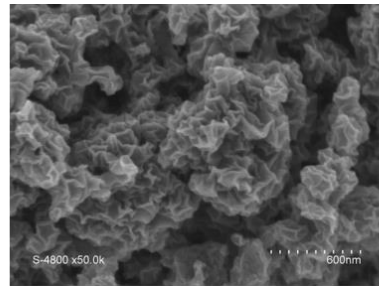
Ball milling



Pyrolysis  
Ar

Pyrolysis  
NH<sub>3</sub>

N-C



Highly porous N-doped carbon substrate with abundant micropores and enriched pyridinic N content was produced for in-temperature XAS studies and for deposition methods.

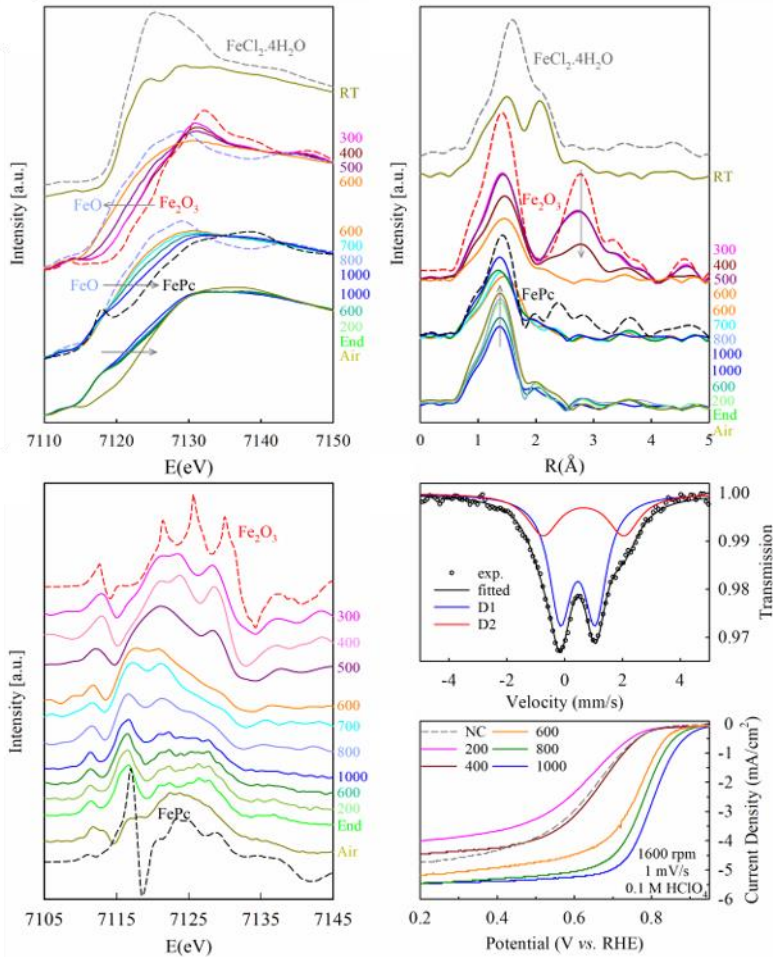
Jia *et al.*, JACS, 2019

Highly microporous and well-defined N-C substrate was achieved.

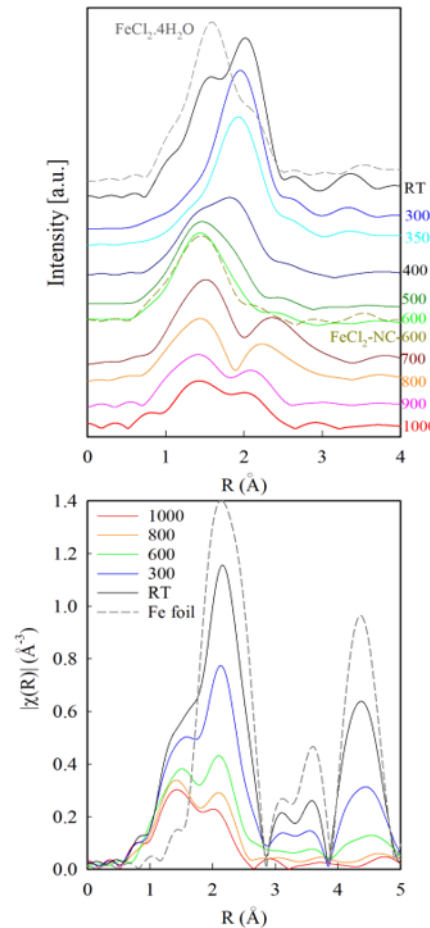


## In-temperature XAS characterizations

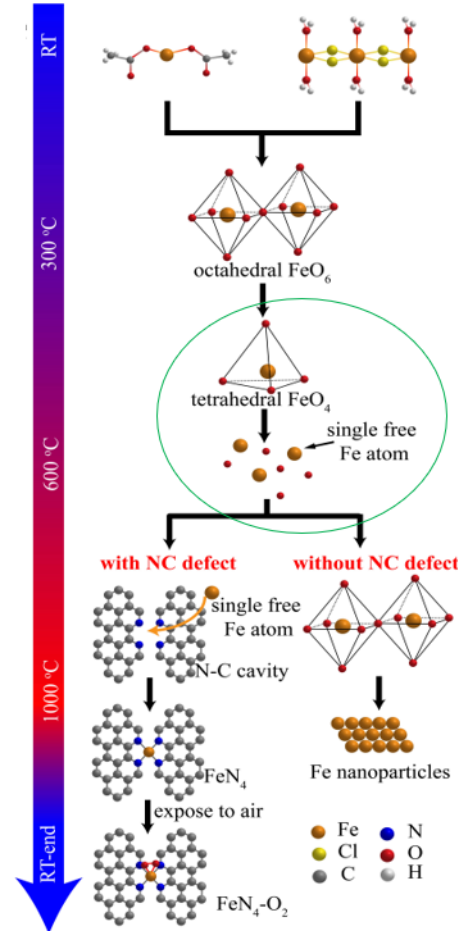
$\text{FeCl}_2 \cdot 4\text{H}_2\text{O} + \text{N-C}$



$\text{FeCl}_2 \cdot 4\text{H}_2\text{O} + \text{SiO}_2$

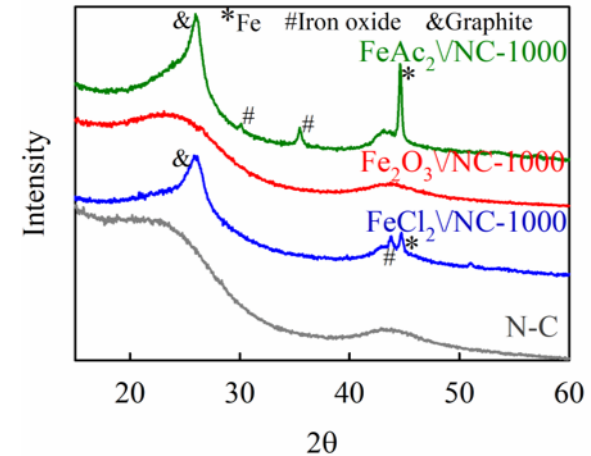
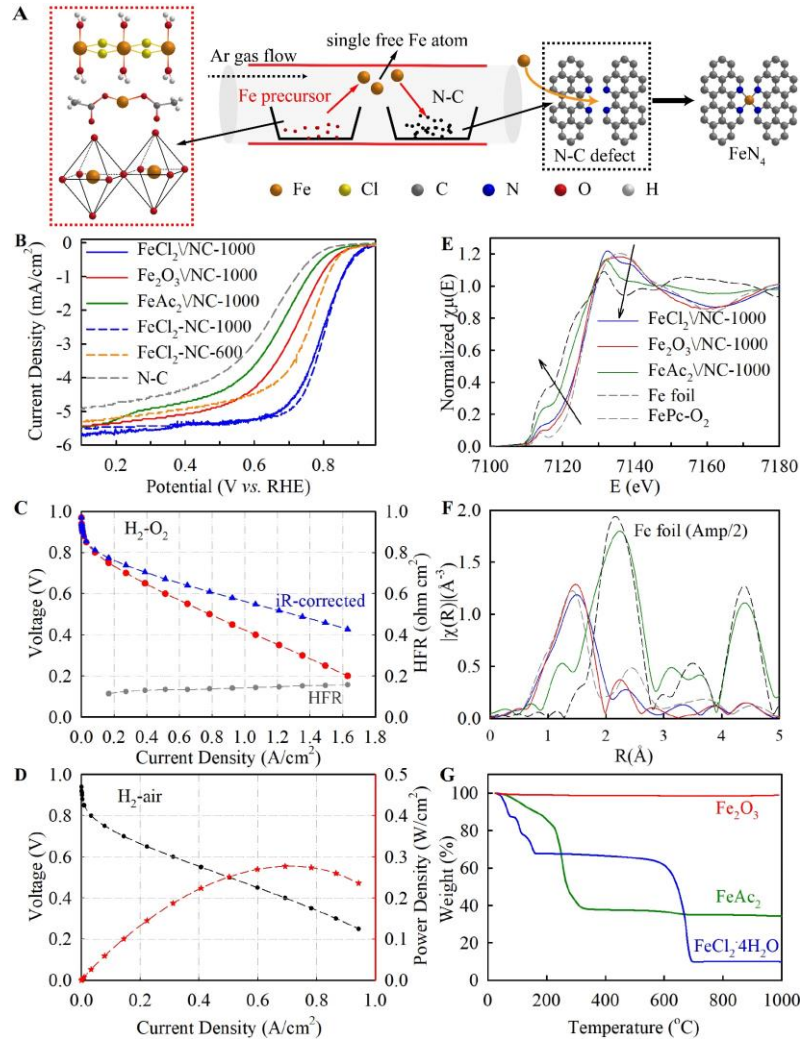


Jia *et al.*, JACS, 2019



In-temperature XAS reveals the stepwise formation of Fe-N<sub>4</sub> sites during pyrolysis.

## Non-contact pyrolysis



Residual powders in the Fe boat.

Inspired by the evolution pathway of Fe-N<sub>4</sub> sites (Fe-O<sub>4</sub> → Fe<sub>1</sub> (g) → Fe-N<sub>4</sub>) that involves diffusion of gaseous Fe<sub>1</sub>, we initiated non-contact pyrolysis.

Three representative Fe precursors with distinctly different evaporation temperatures and N-C substrate were placed in two separate bolts during pyrolysis:

FeCl<sub>2</sub>·4H<sub>2</sub>O: abundant Fe-N<sub>4</sub> sites formed

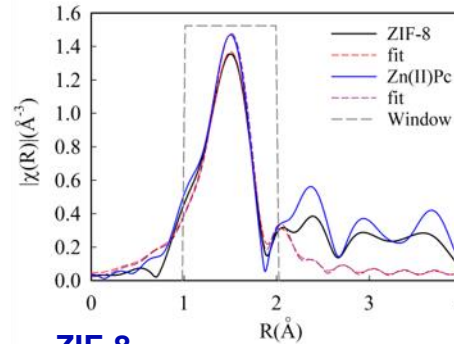
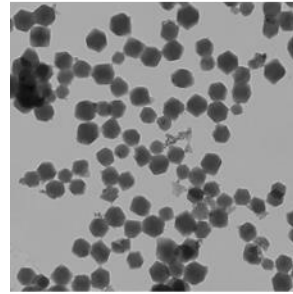
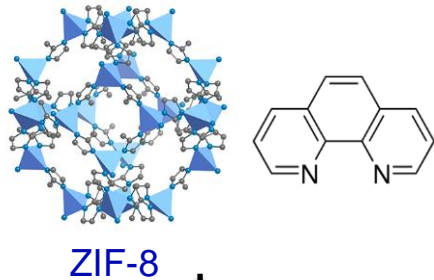
FeAc<sub>2</sub>: no Fe-N<sub>4</sub> sites but Fe nanoparticles formed

Fe<sub>2</sub>O<sub>3</sub>: trace amounts of Fe-N<sub>4</sub> sites formed

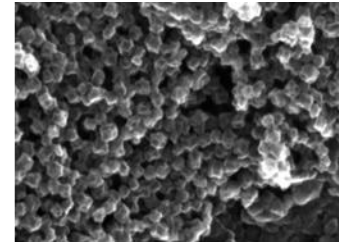
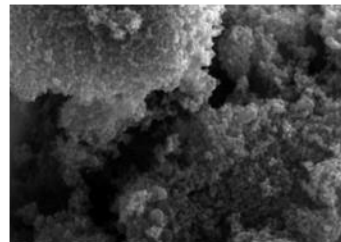
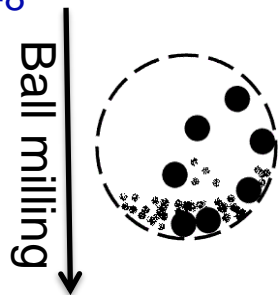




## N-C substrate for chemical vapor deposition (CVD)

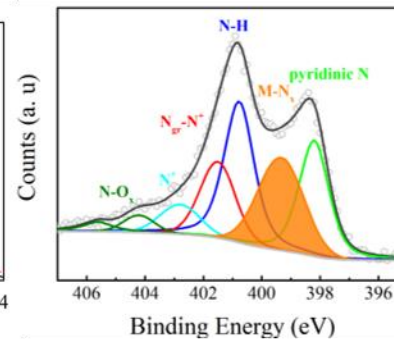
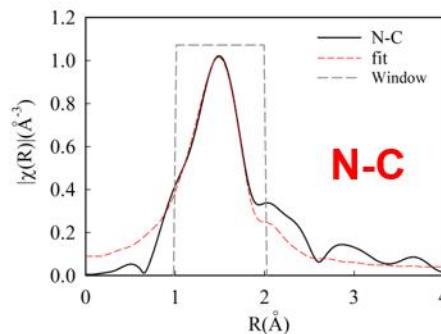
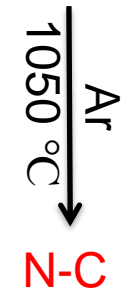


In-house ZIF-8 has an average particle size of ~80 nm, dominated by Zn-N<sub>4</sub>.



FT-EXAFS fit

Zn-N bond	R (Å)	N
ZIF-8	1.99(1)	4.1(5)
Zn(II)Pc	1.98(1)	3.8(8)
N-C	2.00(1)	4.8(5)

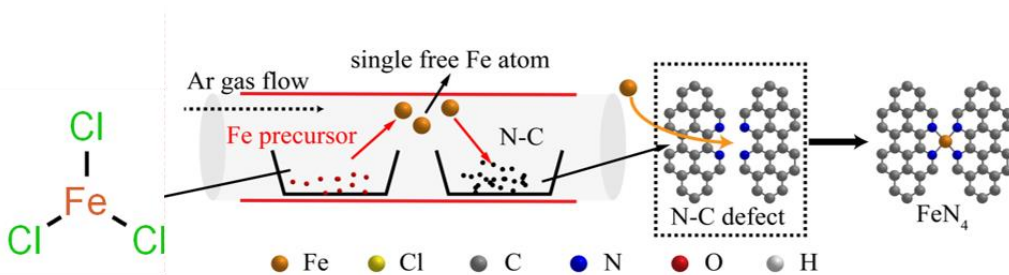


Zn-N<sub>4</sub> structure and particle size are retained upon pyrolysis.  
N-C is composed of Zn-N<sub>4</sub> sites embedded in highly porous carbon matrix.

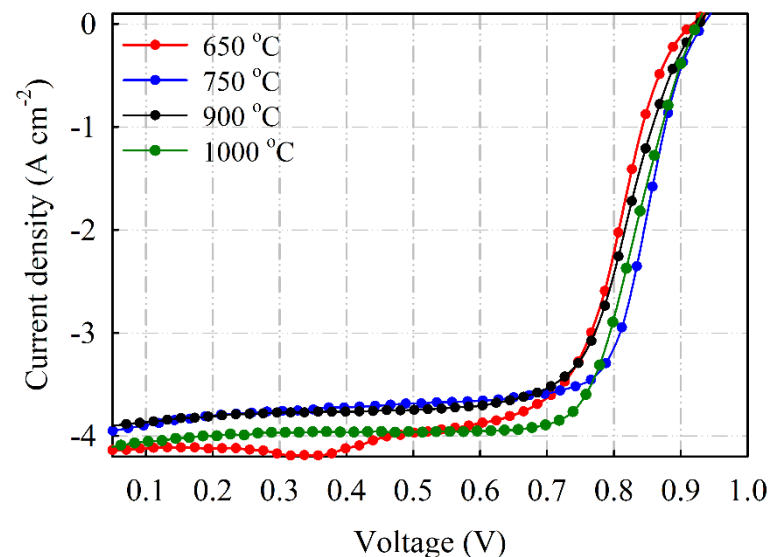
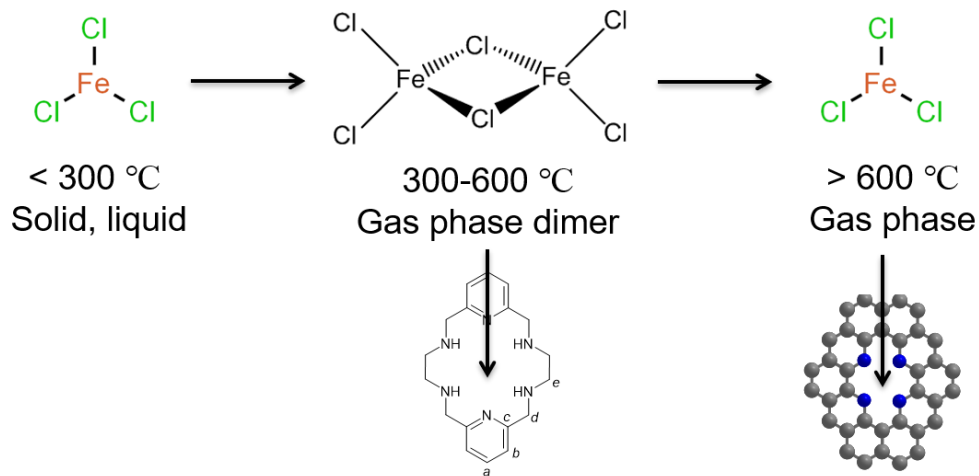
No NH<sub>3</sub> pyrolysis

Make new N-C substrate from in-house ZIF-8 with optimized particle size.

## Chemical vapor deposition (CVD)



ICP	Fe	Zn	N	C
N-C	-	2.16	4.23	84.00
FeNC-CVD-650	2.25	1.05	3.97	85.42
FeNC-CVD-750	<b>2.00</b>	0.12	4.24	85.48
FeNC-CVD-900	3.76	0.23	3.32	85.42
FeNC-CVD-1000	2.72	0.03	2.36	84.20



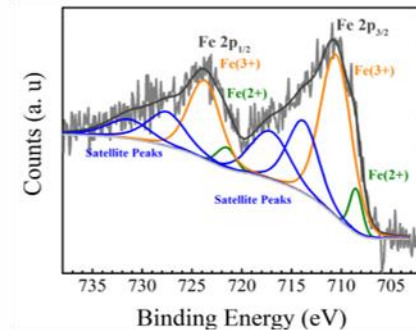
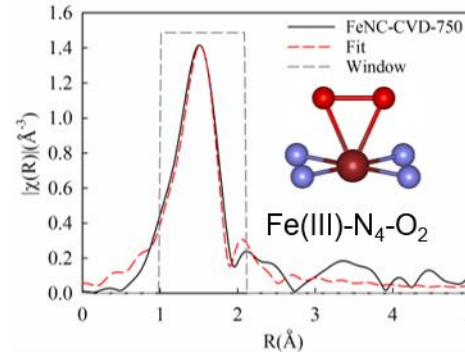
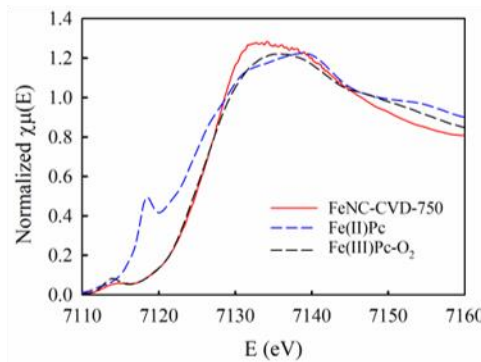
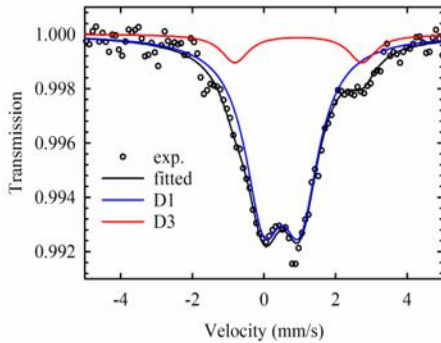
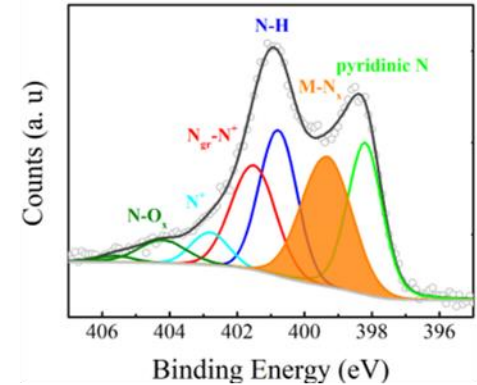
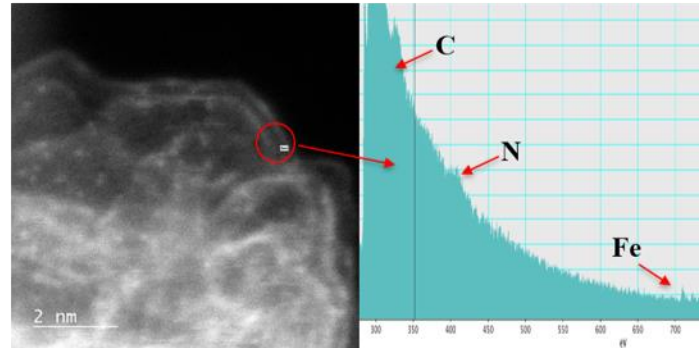
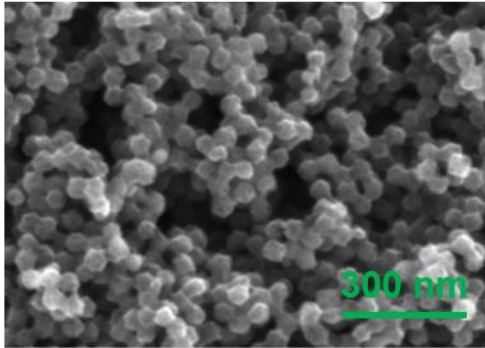
CVD method is demonstrated by using anhydrous FeCl<sub>3</sub>, taking advantage of its low evaporation temperature. It holds the potential to make Fe<sub>2</sub>-N<sub>x</sub>-C sites signified by the gaseous Fe<sub>2</sub>Cl<sub>6</sub> at 300-600 °C.

Among a wide temperature range 750 °C gives the best ORR activity in a RDE.

**CVD method produces highly active Fe-N-C catalysts for the ORR.**



## CVD: *ex situ* characterizations



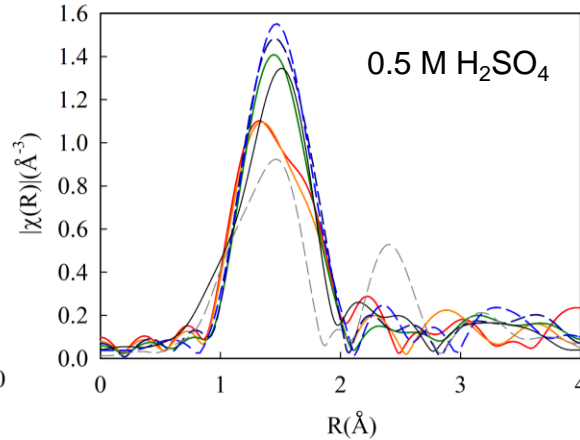
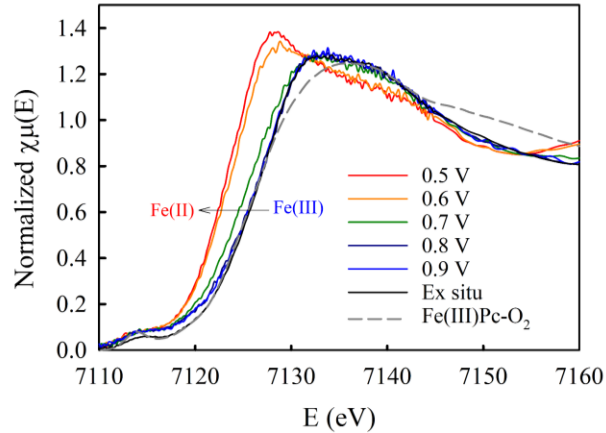
Comp.	RA %	IS mm s <sup>-1</sup>	QS mm s <sup>-1</sup>	LW mm s <sup>-1</sup>	Assignment
Doublet 1	89	0.50	1.02	1.25	Fe(III)-N <sub>4</sub> -O <sub>2</sub>
Doublet 3	11	0.97	3.56	0.92	FeCl <sub>2</sub>

Multiple *ex situ* characterizations converge to the conclusion that the FeNC-CVD-750 contains predominately (~90%) Fe(III)-N<sub>4</sub>-O<sub>2</sub> (D1) species and is absent of Fe(II)-N<sub>4</sub> (D2).

All Fe(II)-N<sub>4</sub> sites in FeNC-CVD-750 located on surface in the form of Fe(III)-N<sub>4</sub>-O<sub>2</sub>.

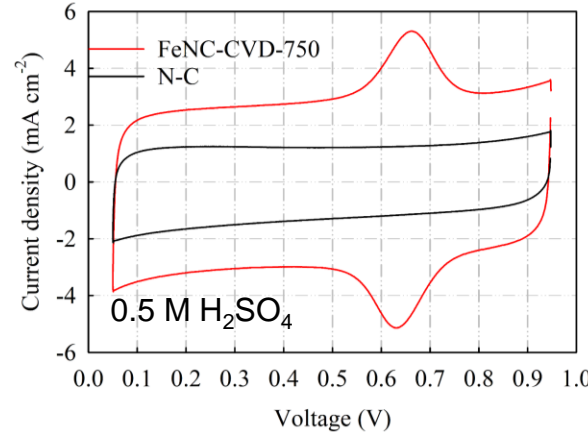
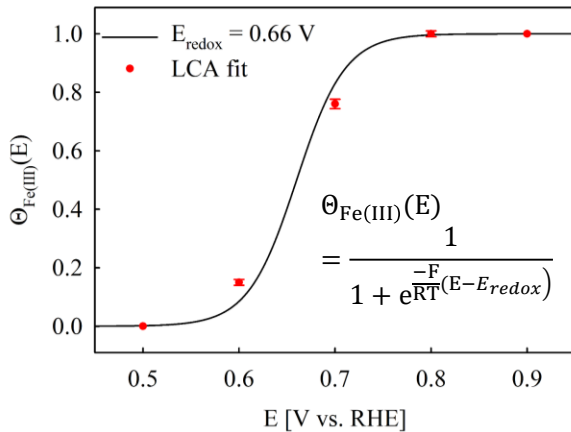


## CVD: *in situ* XAS characterizations

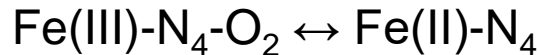


*In situ* XAS identifies the Fe(III)/Fe(II) redox transition at 0.66 V vs RHE, consistent with the CV. It further identifies all Fe(II)-N<sub>4</sub> sites are electrochemically active towards the ORR.

FeNC-CVD-750 contains predominately Fe-N<sub>4</sub> sites with ~1.8 wt<sub>Fe</sub>% that are all located on surface accessible by air, corresponding to nearly 100% Fe-N<sub>4</sub> utilization or ~90% Fe utilization (~10% residual FeCl<sub>2</sub>). This is distinctly different from previous Fe-N-C catalysts that contain both exposed (D1) and buried Fe-N<sub>4</sub> (D2) sites.



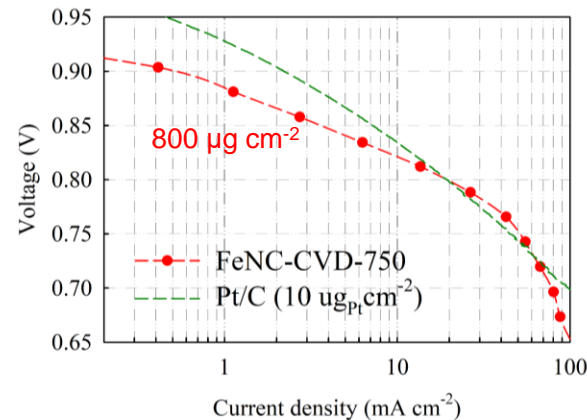
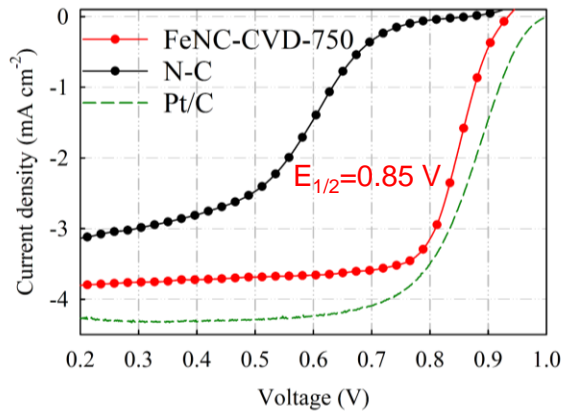
By CVD method, Fe-N<sub>4</sub> sites are formed at locations accessible by gaseous FeCl<sub>3</sub>. They are thus accessible by air. Whereas in previous methods the sufficient mixing of Fe, N, C precursors prior to pyrolysis makes the Fe-N<sub>4</sub> formed and distributed throughout the carbon matrix.



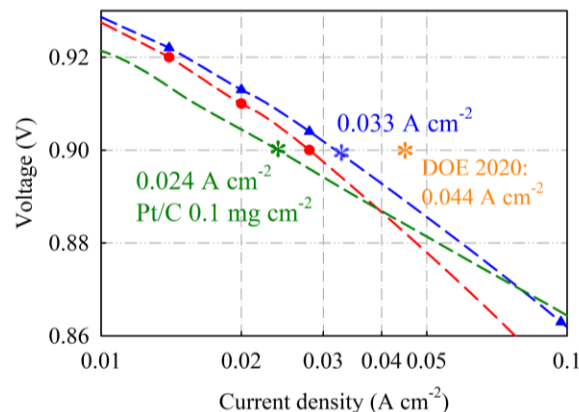
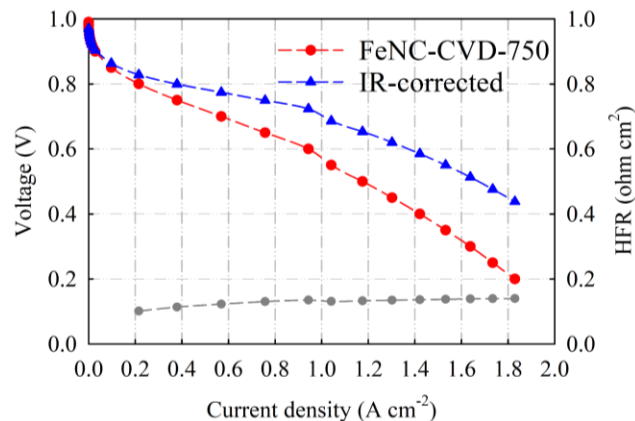
Nearly 100% utilization of Fe-N<sub>4</sub> sites (1.8 wt<sub>Fe</sub>%) is identified *in situ*.



## CVD: ORR activity assessments



In a RDE, the FeNC-CVD-750 ( $800 \mu\text{g cm}^{-2}$ ) exhibits a half-wave potential of 0.85 V in  $0.5 \text{ M H}_2\text{SO}_4$ , and a kinetic current density comparable to that of Pt/C (TKK,  $10 \mu\text{g cm}^{-2}$ ) in  $0.1 \text{ M HClO}_4$ .



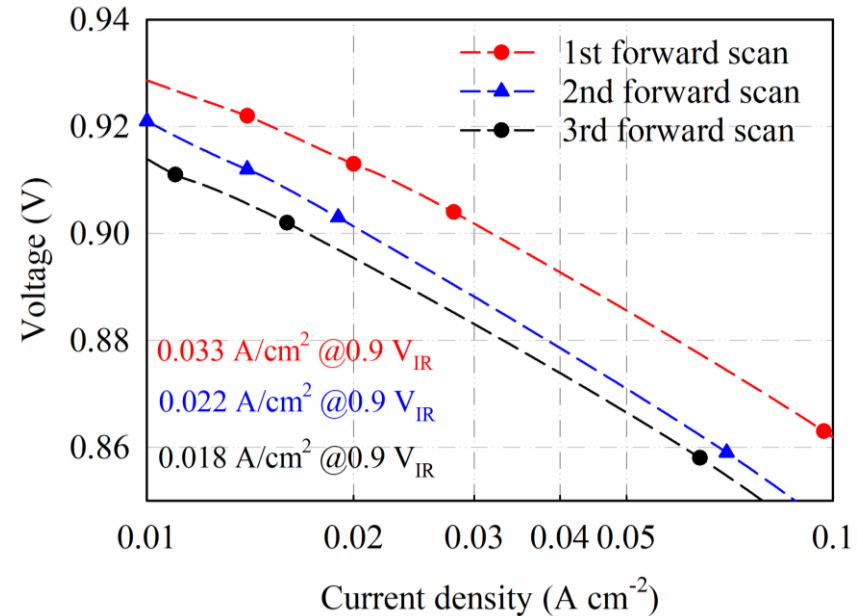
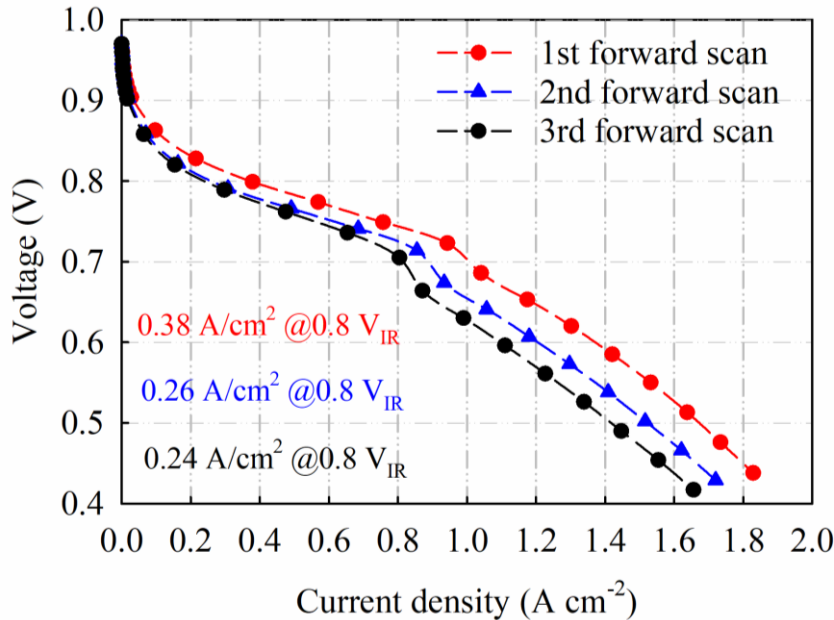
In a  $\text{H}_2\text{-O}_2$  PEMFC, the FeNC-CVD-750 ( $6 \text{ mg}\cdot\text{cm}^{-2}$ ) delivers a current density of  $0.033 \text{ A}\cdot\text{cm}^{-2}$  at 0.9 V, surpassing Budget Period 1 Go/No-Go Decision Point of  $0.025 \text{ A}\cdot\text{cm}^{-2}$ , and that ( $0.024 \text{ A}\cdot\text{cm}^{-2}$ ) of Pt/C (TKK,  $0.1 \text{ mg}\cdot\text{cm}^{-2}$ ).

$5 \text{ cm}^2$  MEA; Cathode:  $6 \text{ mg}/\text{cm}^2$ , Anode:  $0.3 \text{ mg}_{\text{Pt}}/\text{cm}^2$ ;  $\text{H}_2$ : 200 ml/min;  $\text{O}_2$ : 200 ml/min;  $P_{\text{O}_2} = P_{\text{H}_2} = 1$  bar partial pressure, 100% relative humidity (RH),  $80 \text{ }^\circ\text{C}$ ; Nafion-212. Conducted by Giner Inc.

**FeNC-CVD-750 delivers  $0.033 \text{ A}\cdot\text{cm}^{-2}$  at 0.9 V in  $\text{H}_2\text{-O}_2$  PEMFCs.**



## CVD: PEMFC durability

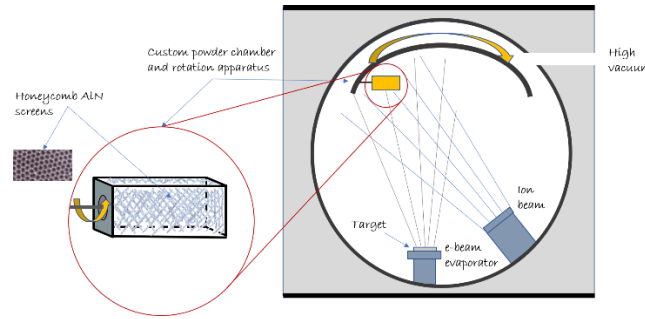
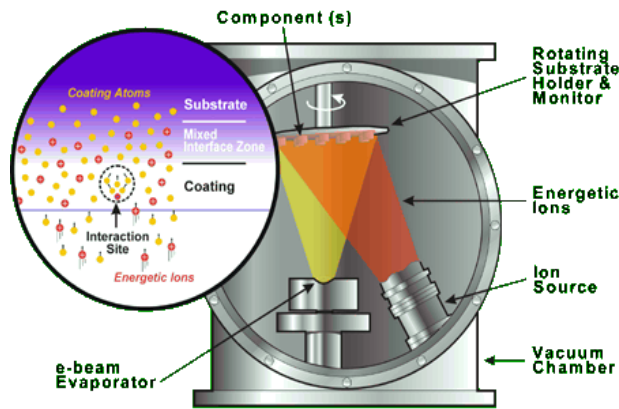


The current density @ 0.8 V degrades ~ **37%** at the third scan.  
The current density @ 0.9 V degrades ~ **45%** at the third scan.  
Major loss occurs upon the first scan.

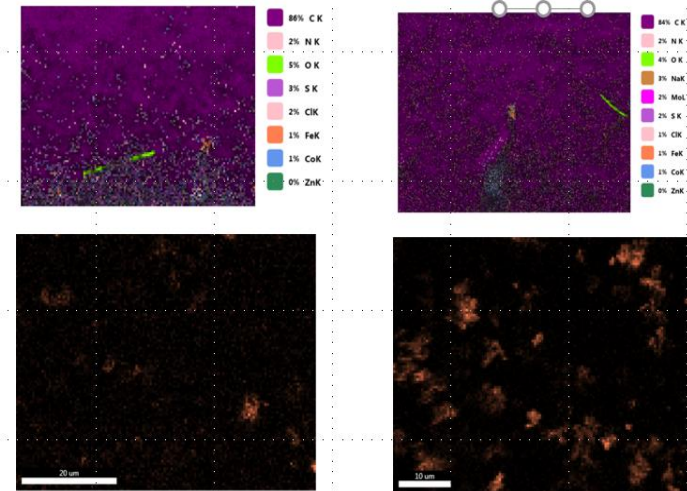
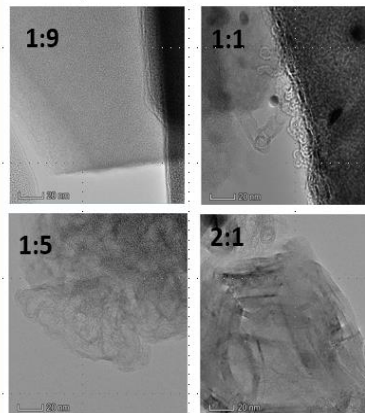
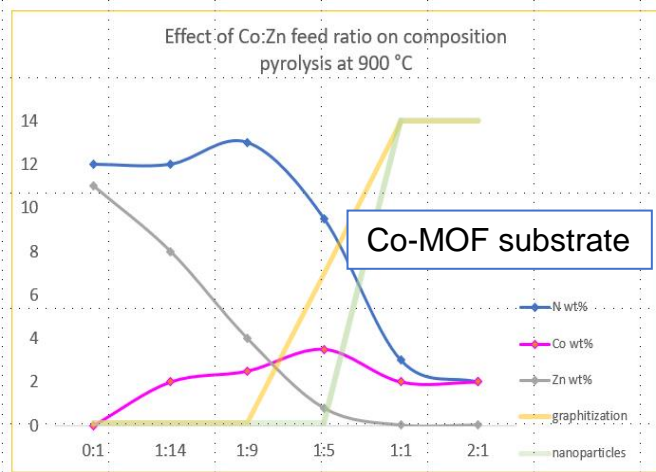
FeNC-CVD-750 is not durable in H<sub>2</sub>-O<sub>2</sub> PEMFCs.



## IBAD: RT-deposition of Fe metal onto Co-MOF substrate



IBAD adjusted to enable metal deposition on powder substrate



Metallic Fe is deposited on Co-MOF. Next step is to deposit single-atom Fe.

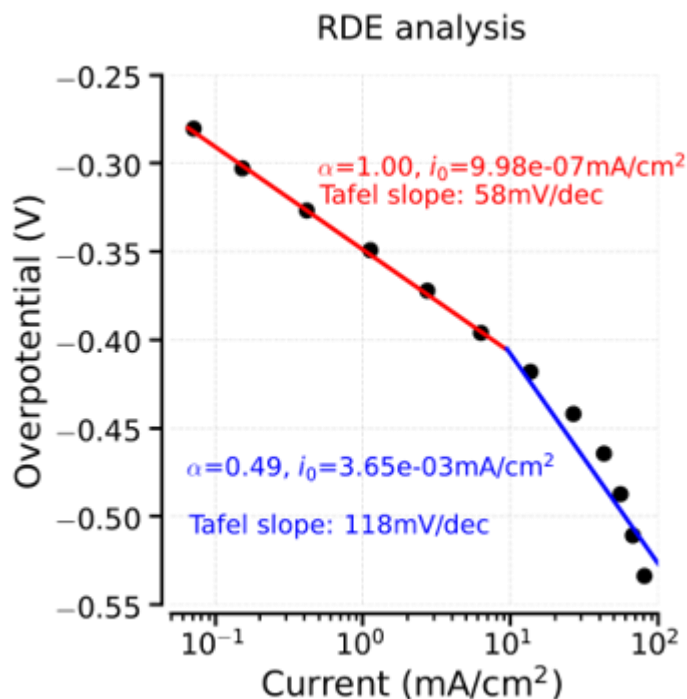
Deposition of Fe metal onto Co-MOF substrate by IBAD at RT is achieved.

# Accomplishments and Progress

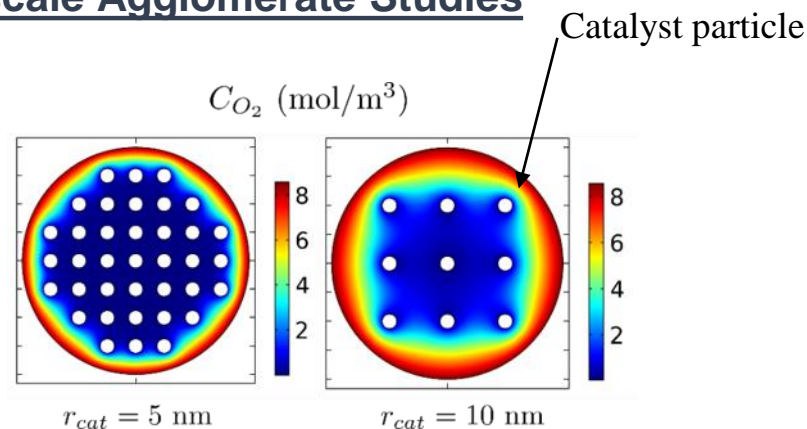
## Non-PGM MEA Kinetics & Microscale modeling

### Kinetics modeling:

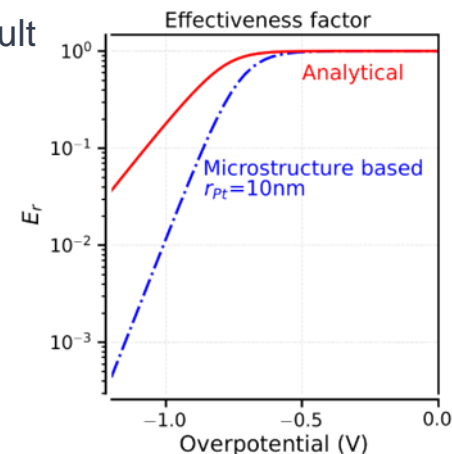
- RDE data fitted to ORR Tafel kinetics
- Two Tafel slopes observed. Slope doubling at higher overpotentials. Similar to ORR with Pt catalyst



### Microscale Agglomerate Studies



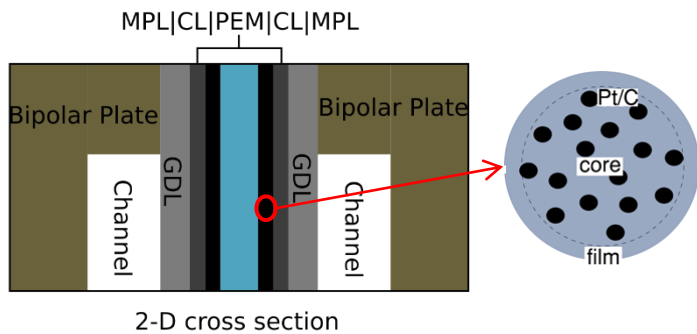
- Smaller particles result in better utilization
- Discrete catalyst particles result in lower effectiveness factor at higher overpotential (transport limited behavior)



Discreet catalyst particles result in local losses and lower catalyst utilization.



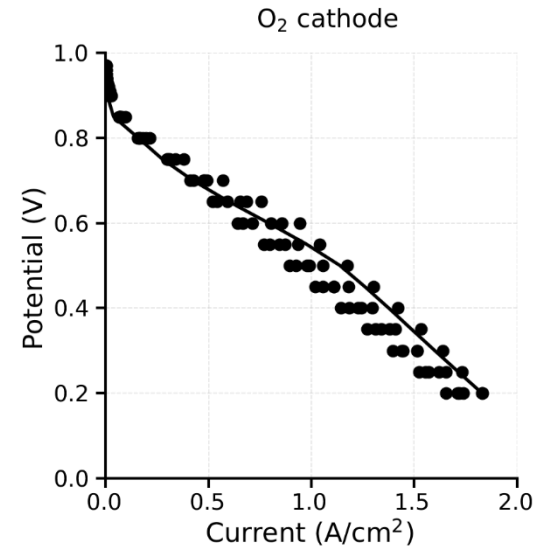
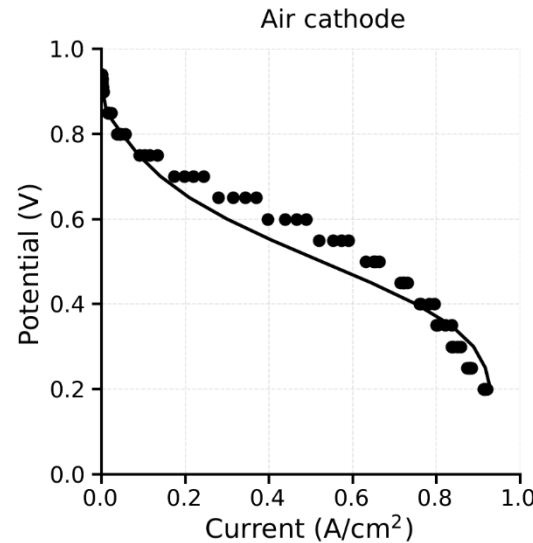
## MEA level macro-scale modeling



### 2-D MEA cross-section model

#### • Incorporated physics:

- ↪ Non-isothermal, two-phase model
- ↪ Multicomponent diffusion
- ↪ Electronic and protonic conduction
- ↪ BV kinetics in anode, Dual slope Tafel in Cathode
- ↪ Agglomerate model uses micro-scale simulated effectiveness factor



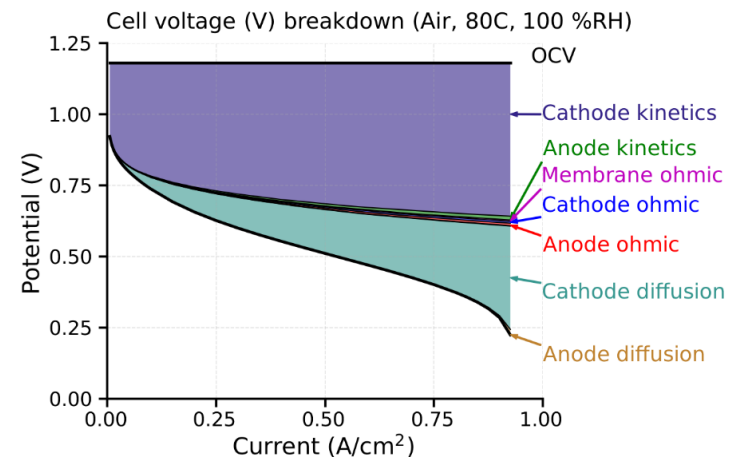
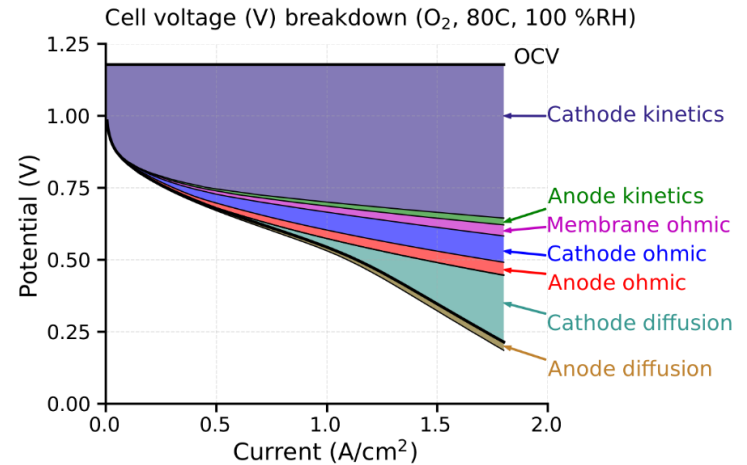
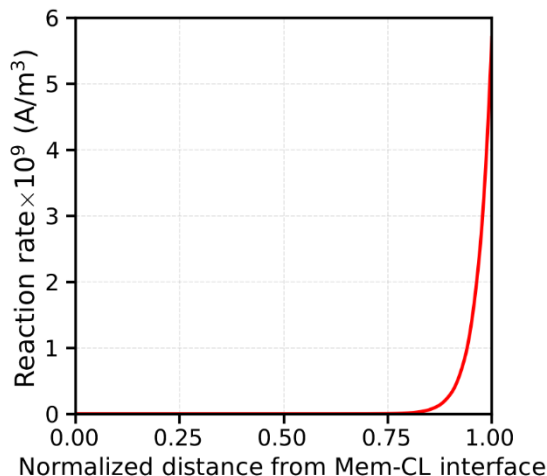
### Experimental validation

- The model can predict the cell performance for various O<sub>2</sub> concentrations
- Dual slope kinetics predicts kinetics region accurately
- Transport limited behavior observed in air-based cathode due to lower O<sub>2</sub> concentrations

## Mass transport modeling

### Voltage breakdown analysis

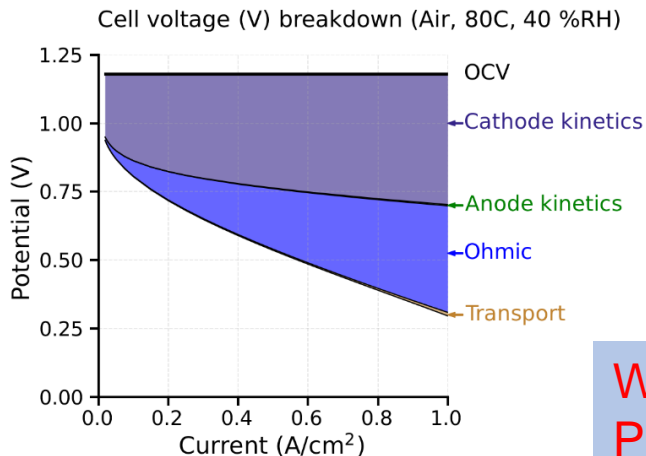
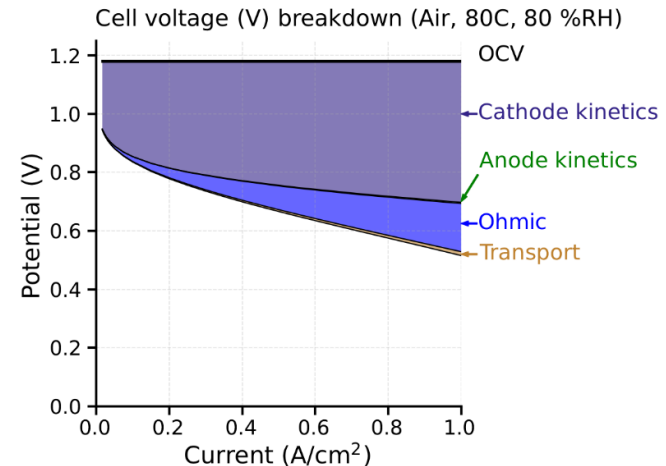
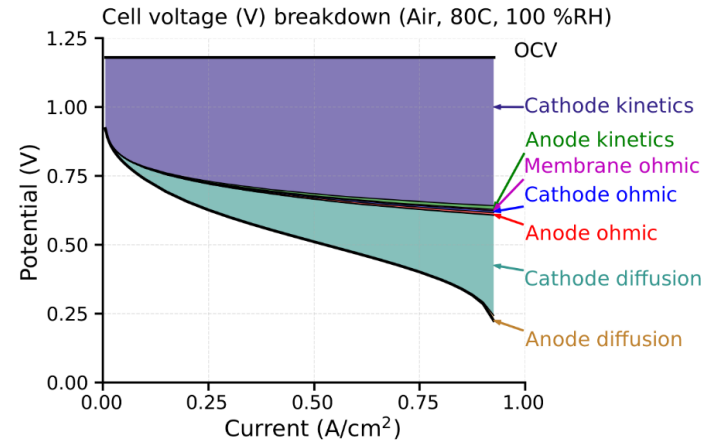
- Significant cathode kinetics loss due to slow ORR kinetics
- Significant transport losses in cathode due to high thickness and low porosity
- Higher transport losses for lower O<sub>2</sub> concentration
- Higher ohmic losses in O<sub>2</sub> electrode due to higher cathode thickness
- Due to transport limitation, reaction is focused at CL-MPL interface
- Almost 75% of the Cathode CL is not utilized



## Mass transport modeling

### Voltage breakdown analysis

- **Saturated conditions (100 % RH)**
  - ↪ High transport losses due to flooding
- **Higher humidity + unsaturated (80% RH)**
  - ↪ Improved performance
  - ↪ Lower transport resistance (no flooding)
  - ↪ Higher ohmic losses (lower membrane water content)
- **Low humidity, dry conditions (40% RH):**
  - ↪ Lower performance
  - ↪ Very high ohmic loss (dry membrane)
  - ↪ Transport gains not enough to compensate



**Water management plays a crucial role in PGM-free catalyst-layers.**



## Response to Previous Year Reviewers' Comments

*Several comments on the performance of the catalysts. "No MEA data were presented that would support the main expectations of this project. For that reason, all claims from the approach fall into the category of predictions and are speculative. The PIs should be acknowledged for the materials that were made and for the fact that structural characterization is consistent with what was proposed. It is not clear why these systems should be more active and durable, as well as what the foundation is for such claims." and "MEA testing is required"*

- MEA evaluations in H<sub>2</sub>-O<sub>2</sub> PEMFCs were conducted on the FeNC-CVD-750 catalyst, and the activity exceeded 1<sup>st</sup> year Go/No-go decision point. We are still in the process of optimizing electrodes and PEMFC operation including using differential cells for the PEMFC testing. We will also work heavily on the durability testing in PEMFCs. By the end of the project, MEA-based activity and durability will be reported.

*Several concerns on the activity, durability, and site density of the M<sub>(x)</sub>-N-C catalysts such as "the potential impact would be significant if it could be demonstrated that a multi-metal active site was more active and could be reliably synthesized at high density".*

- Although Fe<sub>(x)</sub>-N-C with MMC sites was synthesized by ionothermal carbonization synthesis (slide 5), their ORR activities were not good in RDEs, and we could not improve the activities to the state-of-the-art level. We speculate that it is because either the site density is too low and/or the produced Fe<sub>x</sub>-N<sub>y</sub> sites are not inherently active. We decided to cease this method and focused on the CVD method because when trying to synthesize MMC sites via deposition methods, we found that the CVD method can produce highly active Fe-N-C catalysts with dense Fe-N<sub>4</sub> sites located exclusively on surface. Meanwhile, synthesis of MMC sites have been undergone using CVD, flash pyrolysis, and IBAD methods. One particular effort is to create N-C substrates with multiple vacancies that can host the MMC sites.

*Several concerns on the collaborations "For example, it is unclear who is doing the MEA integration work, how the feedback loop from the testing is given, or how the preliminary evaluation is aligned with subsequent diagnostics." and "The value of the mass transport modeling will be apparent only if the catalyst activity becomes sufficient; otherwise, there is too much uncertainty in future catalyst morphologies that will meet activity targets"*

- Although this project involves only one prime (NEU) and one sub (LBNL), productive and extensive collaborations have been undergone within these two parties, EMN Consortium Members (APS, ORNL), and unfunded partners (Giner Inc). Collaborations with APS on the in-temperature XAS revealed the Fe-N<sub>4</sub> site evolution pathway and led to the CVD method. Dense Fe-N<sub>4</sub> sites were directly visualized by STEM and EELS at ORNL. By far the PEMFC assessments reported were conducted by NEU's local partner Giner; meanwhile NEU has been learning and optimizing PEMFC testing systems and will work on the durability assessment in PEMFCs. The mass transport modeling by LBNL provided invaluable insights since NEU had a catalyst that is relatively well-defined (all Fe-N<sub>4</sub> sites on surface) and exhibits exceptional ORR activity in both RDE and PEMFCs for the modeling. NEU is trying to improve the catalyst from the mass transport point of view, and then on durability as well. IBAD involves collaboration between NEU and Thin-film Research inc. We will keep collaborating with EMN Consortium Members for advanced catalyst, electrode, and MEA characterizations.

# Collaboration & Coordination



## **Northeastern University (University Prime)**

Qingying Jia (PI), Sanjeev Mukerjee (Co-PI), Lynne LaRochelle Richard, Li Jiao, Qiang Sun  
Catalyst design and characterizations, in situ XAS, mechanism and degradation studies, MEA fabrication and testing, management and coordination.



## **Lawrence Berkeley National Laboratory (National lab sub)**

Adam Weber (Co-PI), Lalit Pant

Mass transport modeling



## **Argonne National Laboratory (EMN Consortium Member)**

Deborah J. Myers, Evan Wegener, A. Jeremy Kropf

In-temperature XAS



## **Oak Ridge National Laboratory (EMN Consortium Member)**

Dave Cullen, Karren More

STEM, EELS



## **Giner. Inc. (Industry unfunded partner)**

Hui Xu, Fan Yang, Sichen Zhong, Thomas Stracensky

PEMFC performance and durability evaluations



## **Institut Charles Gerhardt Montpellier (University unfunded partner)**

Frederic Jaouen, Jingkun Li, Moulay Tahar Sougrati

Mossbauer, *ex situ* XAS



## **Thin-films Research, Inc (Industry sub-contractor)**

T.R. Raghunath

IBAD

# Remaining Challenges and Barriers



- Improve the activity of Fe-N-C catalysts to reach  $0.035 \text{ A}\cdot\text{cm}^{-2}$  and then  $0.044 \text{ A}\cdot\text{cm}^{-2}$  at 0.9 V in  $\text{H}_2\text{-O}_2$  PEMFCs.
- Improve the powder density of Fe-N-C catalysts to  $0.5 \text{ W}\cdot\text{cm}^{-2}$  in a  $\text{H}_2\text{-Air}$  PEMFC.
- Improve the durability of Fe-N-C catalysts to  $\leq 50\%$  activity loss upon AST.
- Produce MMC sites with high ORR activities.
- Characterizations and Identification of MMC sites.
- Validate IBAD for the synthesis of  $\text{Fe}_{(x)}\text{-N-C}$  catalysts at room temperature.
- Validate flash pyrolysis for the synthesis of  $\text{Fe}_{(x)}\text{-N-C}$  catalysts.
- Understand the degradation modes of  $\text{M}_{(x)}\text{-N-C}$  catalysts and electrodes in PEMFCs.
- Scale-up of Fe-N-C catalysts made by CVD.

# Proposed Future Work



- Optimize the CVD method to further improve the activity and durability of Fe-N-C catalysts.
  1. site densification (N enrichment in the N-C substrate; tune Zn-N<sub>4</sub> content).
  2. improve MOF-derived N-C substrate for better mass transport and durability.
  3. improve the understanding of the Fe-N<sub>4</sub> formation mechanism in the CVD method.
- Implement IBAD to:
  1. produce M<sub>(x)</sub>-N-C catalysts with MMC sites.
  2. realize room temperature synthesis of M<sub>(x)</sub>-N-C catalysts.
  3. densify M-N<sub>4</sub> and/or MMC sites.
- Implement flash pyrolysis to improve the CVD method and to synthesize MMC sites.
- Identification of MMC sites via STEM and *in situ* XAS.
- Improve the understandings of degradation of Fe-N-C catalysts in PEMFCs via XAS studies.
- Improve the durability of Fe<sub>(x)</sub>-N-C catalysts by:
  1. adding protective layers
  2. incorporating sacrificing oxides in N-C substrates.
  3. implementing strategies based on the new understanding of Fe-N-C degradation modes.
- Conduct IBAD and electrospinning for MEA fabrication.
- Conduct mass transport modeling to understand the bases of the activity and durability of synthesized catalysts.

Any proposed future work is subject to change based on funding levels.

# Summary



- Objective:** Produce PGM-free catalysts with high ORR activity and durability in PEMFCs.
- Relevance:** Our approaches move beyond traditional M-N-C catalysts and synthesis routes. The new catalysts and synthesis methods may address the limited activity, durability, and active site density of  $M_{(x)}$ -N-C catalysts and meet the DOE targets.
- Approach:**  $M_{(x)}$ -N-C catalysts with MMC sites are targeted candidates to improve the ORR activity and durability of M-N-C catalysts. Ionothermal carbonization synthesis, non-contact pyrolysis, CVD, IBAD, and flash pyrolysis have been conducted for catalyst synthesis. Advanced characterizations are implemented to understand the catalyst formation mechanisms, ORR mechanisms, degradation mechanisms. Mass transport modeling has been implemented to understand the PEMFC performance of synthesized catalysts.
- Accomplishments:**
1. Fe-N<sub>4</sub> formation pathway during pyrolysis was revealed by in-temperature XAS.
  2. CVD method was validated producing highly active Fe-N-C catalysts with all Fe-N<sub>4</sub> sites located on surface with 100% utilization.
  3. The FeNC-CVD-750 demonstrated a current density of 0.033 A·cm<sup>-2</sup> at 0.9 V in H<sub>2</sub>-O<sub>2</sub> PEMFCs.
  4. Metal deposition onto powder substrates was achieved by engineering IBAD.
- Collaboration:** Strong teams and effective collaborations within university (NEU), national labs (LBNL, ANL), local industry partner (Giner, Thin-Films Research), and international partner (CNRs).
- Future work:**
1. improve the CVD method and the flash pyrolysis.
  2. implement the IBAD to synthesize  $M_{(x)}$ -N-C catalysts at room temperature.
  3. improve the understanding of degradation of  $M_{(x)}$ -N-C catalysts and their durability.



# Acknowledgements



## Northeastern University

Sanjeev Mukerjee (Co-PI)  
Lynne LaRochelle Richard  
Li Jiao  
Qiang Sun  
Ershuai Liu  
Serge Pann



## Lawrence Berkeley National Laboratory

Adam Weber (LBNL PI),  
Lalit Pant



## Giner, Inc.

Hui Xu  
Fan Yang  
Sichen Zhong  
Thomas Stracensky



## Institut Charles Gerhardt Montpellier

Frederic Jaouen  
Jingkun Li  
Moulay-Tahar Sougrati



## University of California, Los Angeles

Yu Huang, Zipeng Zhao



## Thin-films Research, Inc

T.R. Raghunath

## DOE Hydrogen and Fuel Cell Technologies Office (HFTO)

Nancy Garland (Technology manager)  
Dimitrios Papageorgopoulos  
Dave Peterson



## Argonne National Laboratory



Deborah J. Myers,  
Evan Wegener,  
A. Jeremy Kropf  
Magali S. Ferrandon  
Jae Hyung Park



## Oak Ridge National Laboratory

Dave Cullen, Karren More



## Los Alamos National Laboratory

Piotr Zelenay, Edward F. Holby



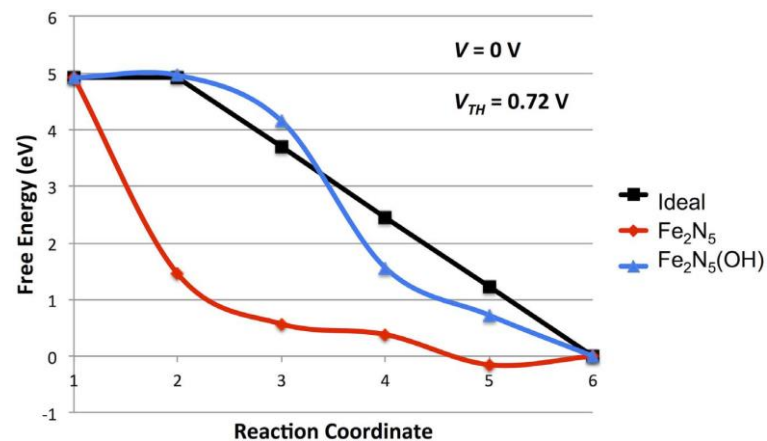
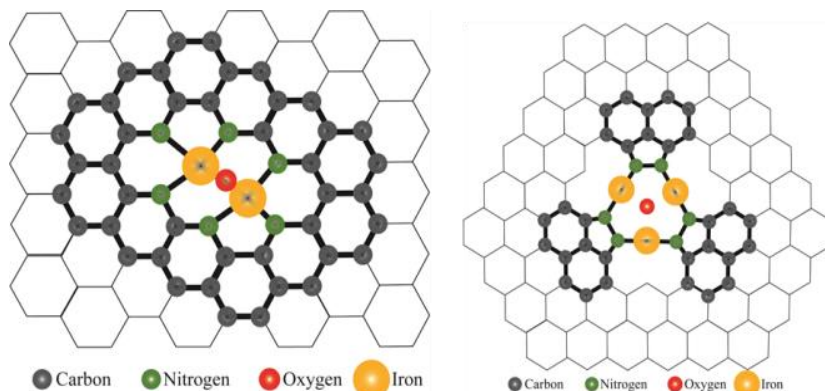
## National Renewable Energy Laboratory

KC Neyerlin

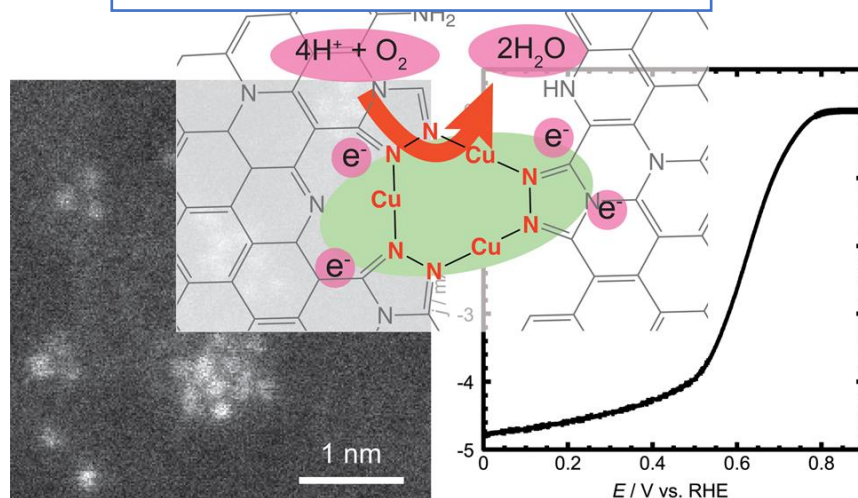


# Technical Back-Up Slides

## Literature reports of the presence of MMC sites



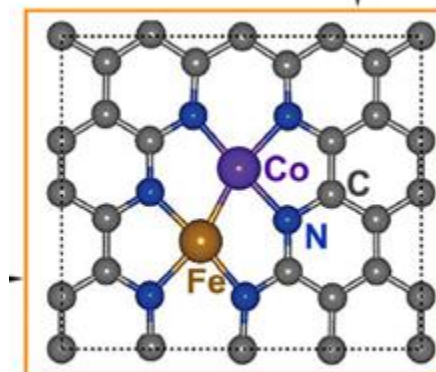
Schematic illustration of MMC sites.



ACS Appl. Energy Mater. **2018**, 1, 2358–2364

Holby, E. F.; Taylor, C. D. *Sci. Rep.* **2015**, 5.

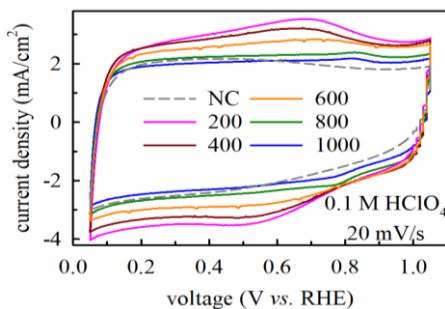
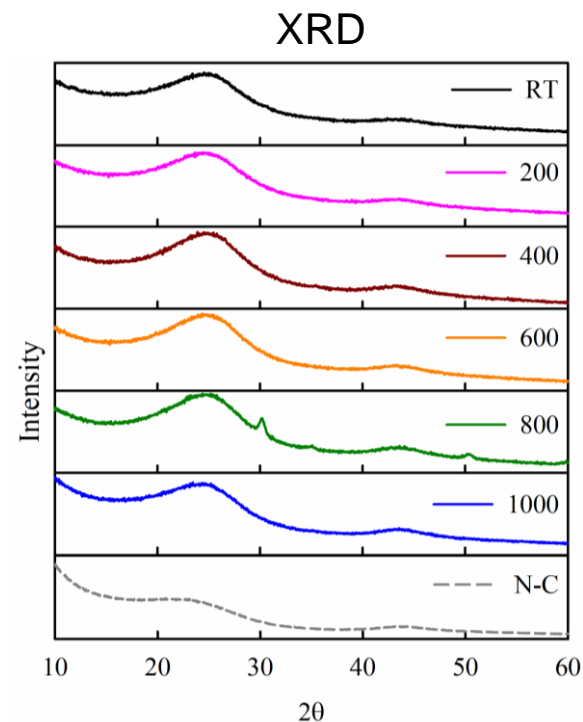
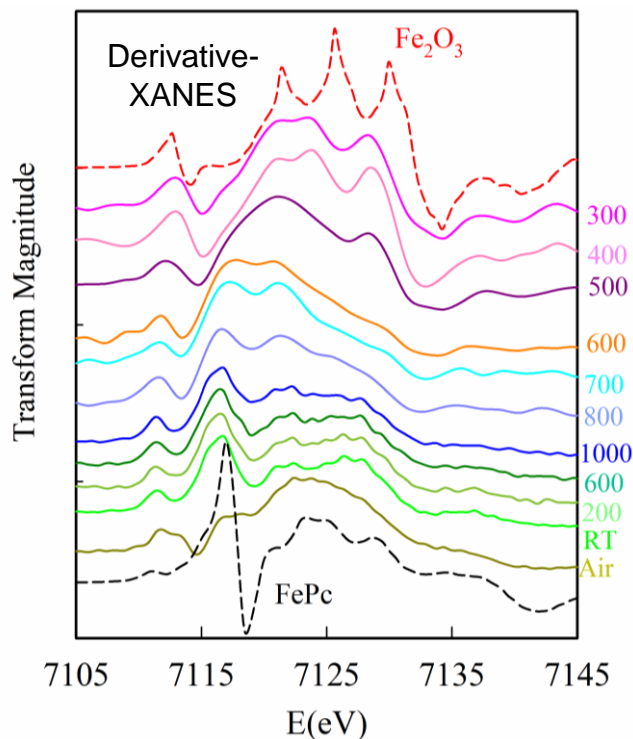
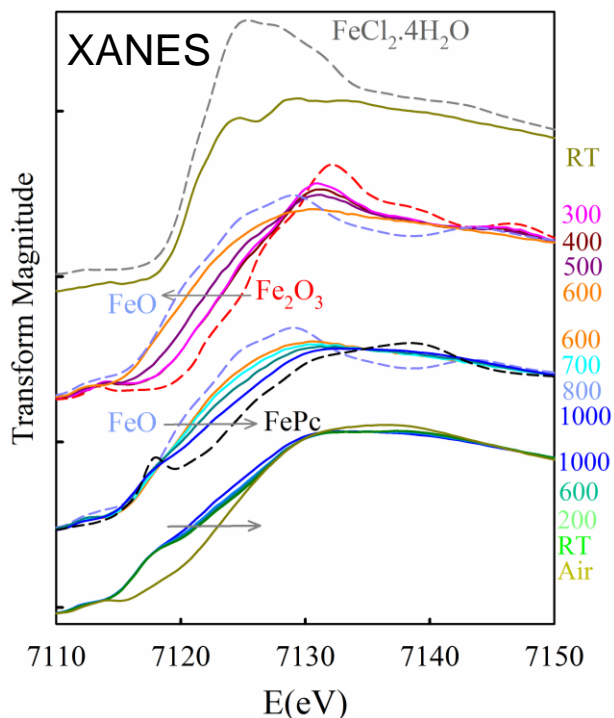
Desired ORR kinetics of MMC sites by DFT



J. Am. Chem. Soc. **2017**, 139, 17281



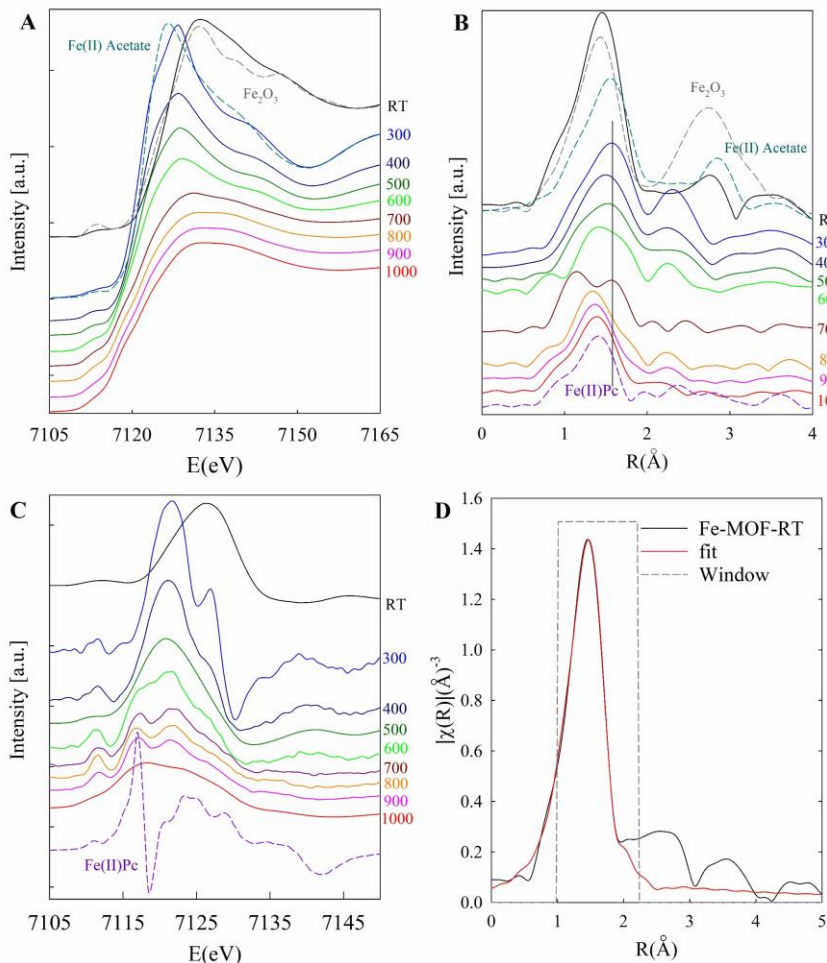
## In-temperature XAS on $\text{FeCl}_2 \cdot 4\text{H}_2\text{O}$ + N-C



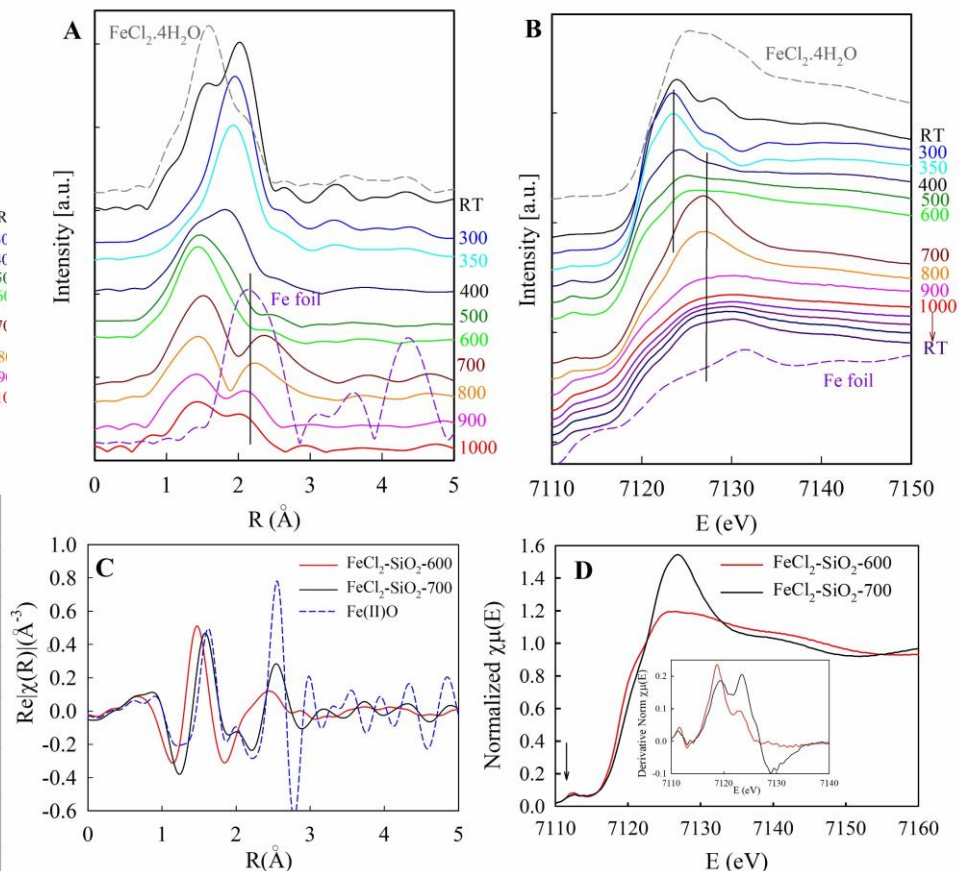
EXAFS fits	R ( $\text{\AA}$ )	N	$\sigma^2 \times 10^{-3}$ ( $\text{\AA}^2$ )	$E_0$ (eV)
$\text{FeCl}_2$ -NC-600	$1.99 \pm 0.01$	$3.6 \pm 0.4$	$17 \pm 2$	$-0.3 \pm 0.9$
$\text{FeCl}_2$ -NC-1000	$1.92 \pm 0.01$	$4.5 \pm 0.7$	$12 \pm 2$	$-1.1 \pm 1.2$
$\text{FeCl}_2$ -NC-RT	$1.91 \pm 0.01$	$4.3 \pm 0.4$	$7 \pm 2$	$-0.2 \pm 1.5$



## FeAc<sub>2</sub> + ZIF-8 + Phen



## FeCl<sub>2</sub>·4H<sub>2</sub>O + SiO<sub>2</sub>



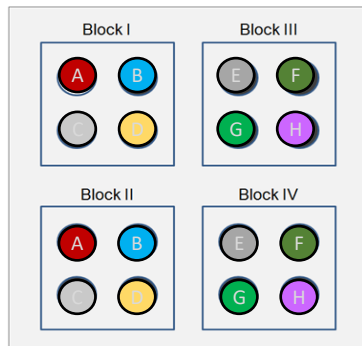
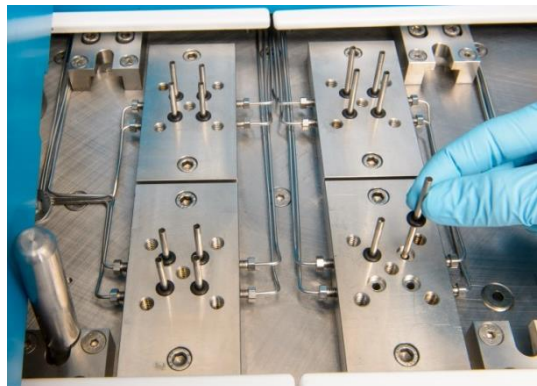
	R (Å)	N	$\sigma^2 \times 10^{-3} (\text{Å}^2)$
FeCl <sub>2</sub> -SiO <sub>2</sub> -600	2.00±0.02	3.9±0.6	19±5

	Bond	R (Å)	N	$\sigma^2 \times 10^{-3} (\text{Å}^2)$	E <sub>0</sub> (eV)
Fe-MOF-RT	Fe-O	1.98±0.01	6.0±0.8	10±2	0.1±1.0
Fe-MOF-1000	Fe-O	1.94±0.01	3.7±0.5	13±3	-1.8±1.8

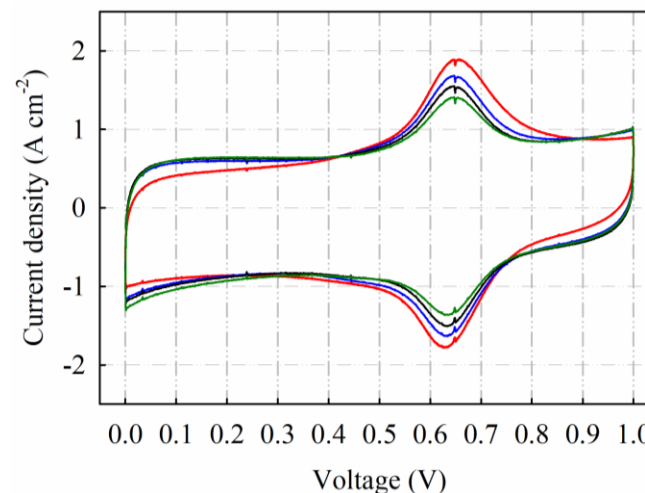
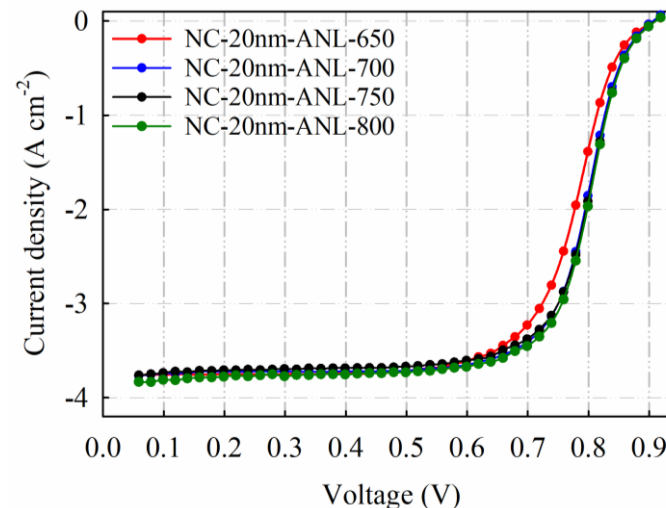
In-temperature XAS on other mixtures.

## Vertical CVD method (ANL)

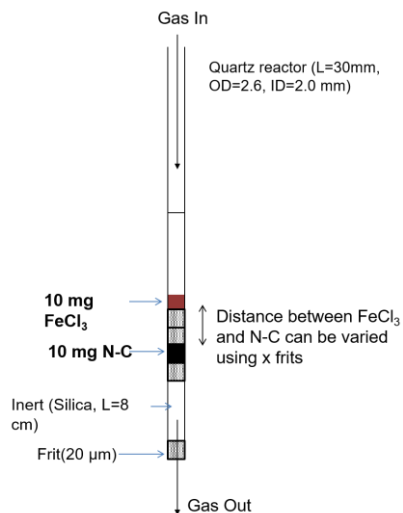
HT Parallel Reactor System (T1224, Avantium)



Each block can be temperature-controlled independently



Deborah J. Myers,  
Magali S. Ferrandon  
Jae Hyung Park

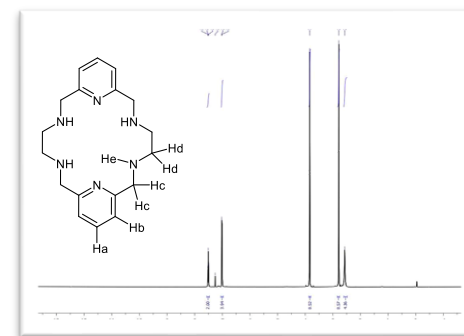
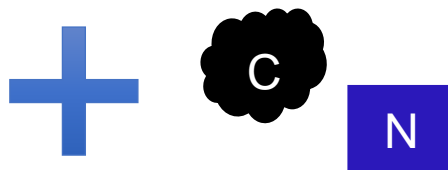
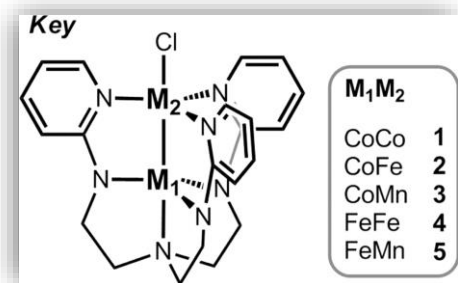


CVD was also demonstrated by another group using another system (parallel reactor).

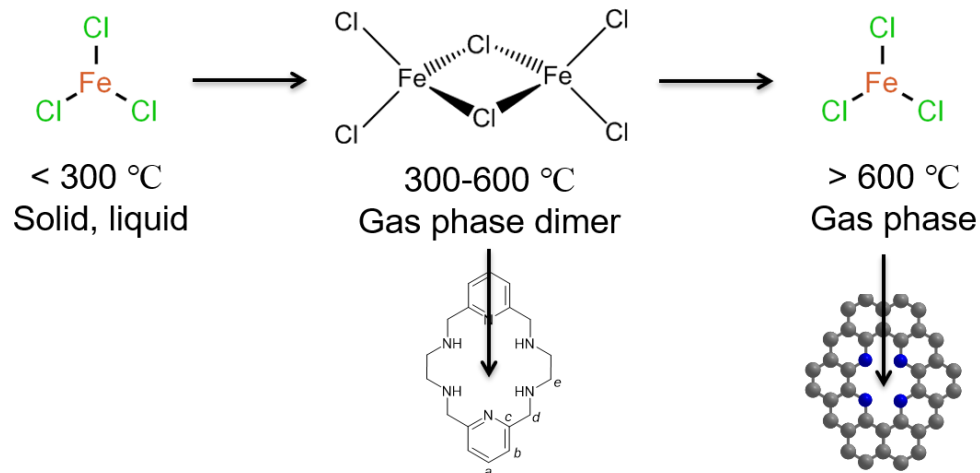
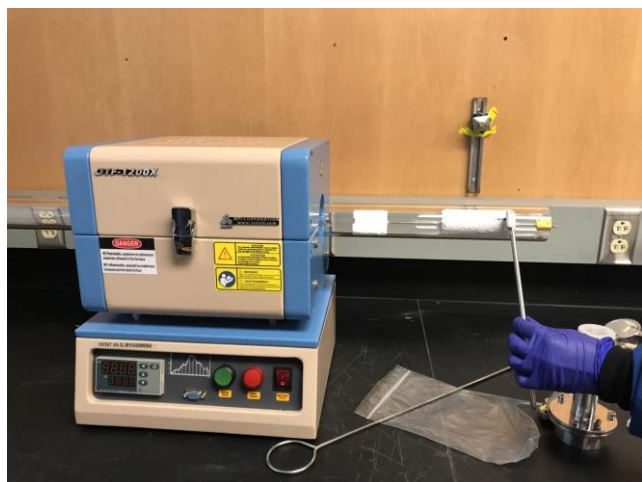
# Technical Back-Up



## Flash pyrolysis



*J. Am. Chem. Soc.* 2014, 136, 5, 1842

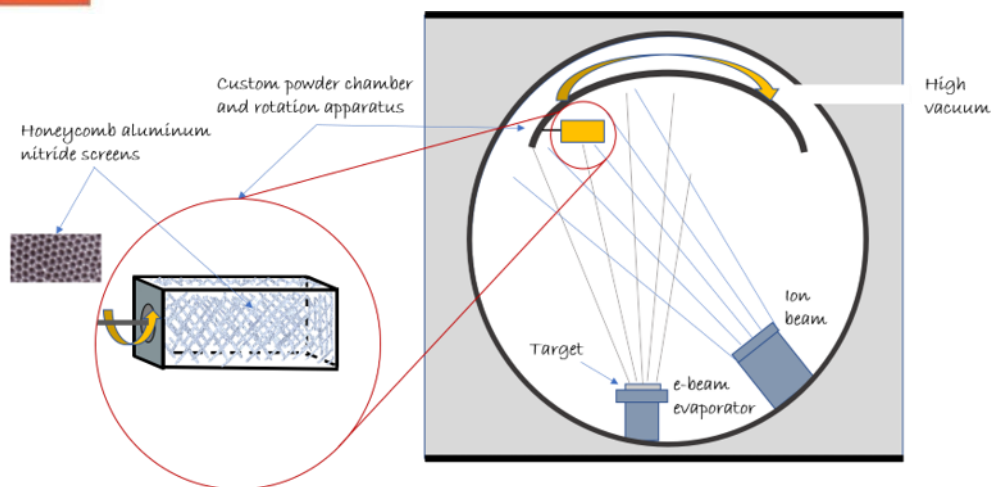


Synthesis of  $\text{M}_{(x)}\text{-N-C}$  from pre-existing MMC precursors via flash pyrolysis by a slide furnace that allows for pyrolysis at a constant temperature with controllable time.

## Engineering IBAD on powder substrates



Thin-Films Research, Inc.  
270 Littleton Road  
Westford MA 01886  
Tel: 978-692-9530 Fax: 978-692-9531  
www.thinfilmsresearch.com



- Optimized Co/N-doped precursor developed
- 9 g of optimized precursor produced for IBAD trials
- IBAD contract engineering partner identified and hired: Thin-Films Research, Inc, Westford, MA
- Tooling in late stage development and small-scale trials
- Process scalable to 5 g batches with current tool set





## Publications

- Jiao, L.; Li, J.; Richard, L.; Stracensky, T.; Liu, E.; Sun, Q.; Sougrati, Z.; Zhao, Z.; Yang, F.; Zhong, S.; Xu, H.; Mukerjee, S.; Huang, Y.; Myers, D\*, Jaouen, F.,\* and Jia, Q\*. High-performance iron-based ORR catalysts synthesized via chemical vapor deposition. Under Preparation; Preprint available on ChemRxiv
- Li, J., Jiao, L., Wegener, E., Richard, L., Liu, E., Zitolo, A., Sougrati, M., Mukerjee, S., Zhao, Z., Huang, Y., Kropf, A., Jaouen, F., Myers, D\*, and Jia, Q\*. Evolution pathway from iron compounds to Fe<sub>1</sub>(II)-N<sub>4</sub> sites through gas-phase iron during pyrolysis, J. Am. Chem. Soc. 2020, 142, 1417-1423.

## Conference Presentations

- Q. Jia, L. Jiao, J. Li, T. Stracensky, M. Sougrati, S. Mukerjee, F. Jaouen, D. Myers. Move beyond the evolution pathway for the formation of M-N<sub>4</sub> sites upon pyrolysis of the mixture of M, N, and C precursors, PRiME 2020
- Q. Jia, J. Li, D. Myers, A. J. Kropf, S. Mukerjee. Revisiting the Nature of Active Sites in Pyrolyzed Fe-N-C Electrocatalysts: In Situ Monitoring the Structure Evolution of Active Sites in Fe-N-C Catalysts during Pyrolysis. 235th ECS Meeting, 05/26/2019 **(Invited)**
- L Jiao, E Liu, LLR Richard, S Mukerjee, Q Jia. Developing Platinum Group Metal Free Catalysts with Multiple Metal Centers for the Oxygen Reduction Reaction in Acid, 235th ECS Meeting
- LLR Richard, L Jiao, E Liu, Q Jia. Development of Bimetallic Non-Platinum Group Metal Catalysts Based on Metal Organic Framework Precursors, 235th ECS Meeting
- S. Mukerjee, Q. Jia., Structural and Mechanistic Basis for the Oxygen Reduction Activity of Pyrolyzed Fe-N-C Electrocatalysts. 235th ECS Meeting

## Patent

- Provisional patent: 19815-0588-INV-20028, “synthesizing highly active Fe-N-C electrocatalysts for oxygen reduction via vapor deposition of gas-phase iron”