

Hybrid Electrical/Thermal Hydrogen Production Process Integrated with a Molten Salt Reactor Nuclear Power Plant

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Project ID: H2026

PROJECT OVERVIEW

TIMELINE:

Start: July 1, 2018

End: Sept. 30, 2020

TOTAL CENTER FUNDING:

DOE Share: \$600K

Cost Share: \$823K

DOE Share Expended: \$510K

BARRIERS:

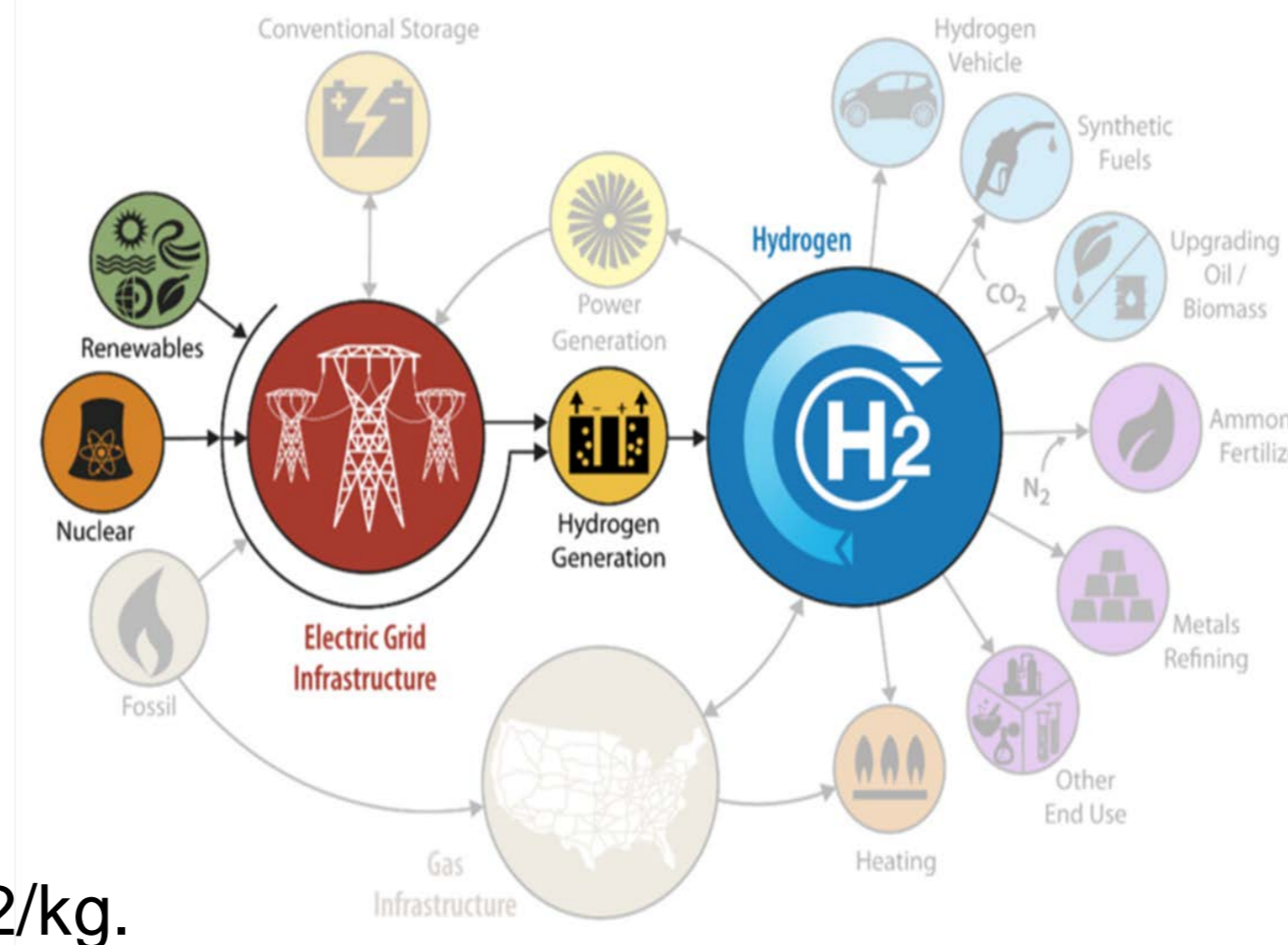
- A. Hydrogen Levelized Cost
- B. System Energy Efficiency
- C. Total Capital Investment

PARTNERS:



RELEVANCE TO H2@SCALE

- The Hybrid Sulfur (HyS) Hydrogen Generation process has the potential to produce hydrogen gas using both thermal and electrical energy at a cost of <\$2/kg.
- HyS can utilize thermal energy from a molten salt reactor (MSR) along with renewable electrical energy from either wind or solar generation to efficiently produce hydrogen.
- The HyS process, being a two step process, can act as a buffer and store thermal energy chemically as liquid SO₂, to be used to generate hydrogen as required to minimize generation and storage costs.



APPROACH

THIS PROGRAM WILL:

- System Analysis**
 - Develop a plausible path to hydrogen production cost less than \$2/kgH₂ based on the process design and cost estimation.
 - Develop a conceptual plant design for MSR-HyS
 - Develop a techno-economic analysis of H₂ production via MSR-HyS
- MEA Development**
 - Develop an SDAPP membrane composition showing better ion conductivity than Nafion®112 in 6 M sulfuric acid.
 - Develop electro-catalyst that show a 20mV performance improvement over Pt/C in 3.5M sulfuric acid solution containing dissolved sulfur dioxide or sodium sulfite
 - Demonstrate performance of at least 100mV lower cell voltage than Nafion® of an MEA using higher temperature membranes and improved catalysts.

HyS CHEMISTRY

- Hybrid Sulfur (HyS) is a two-step thermo-chemical cycle based on sulfur oxidation/reduction
- Key Reaction Step is electro-chemical water splitting using an SO₂ depolarized electrolyzer (SDE).
- All fluid processing minimizes entropic losses due to phase changes
- HyS is "hybrid" cycle requiring both electrical and thermal energy input
- Optimization of the system requires trade-offs between the various components

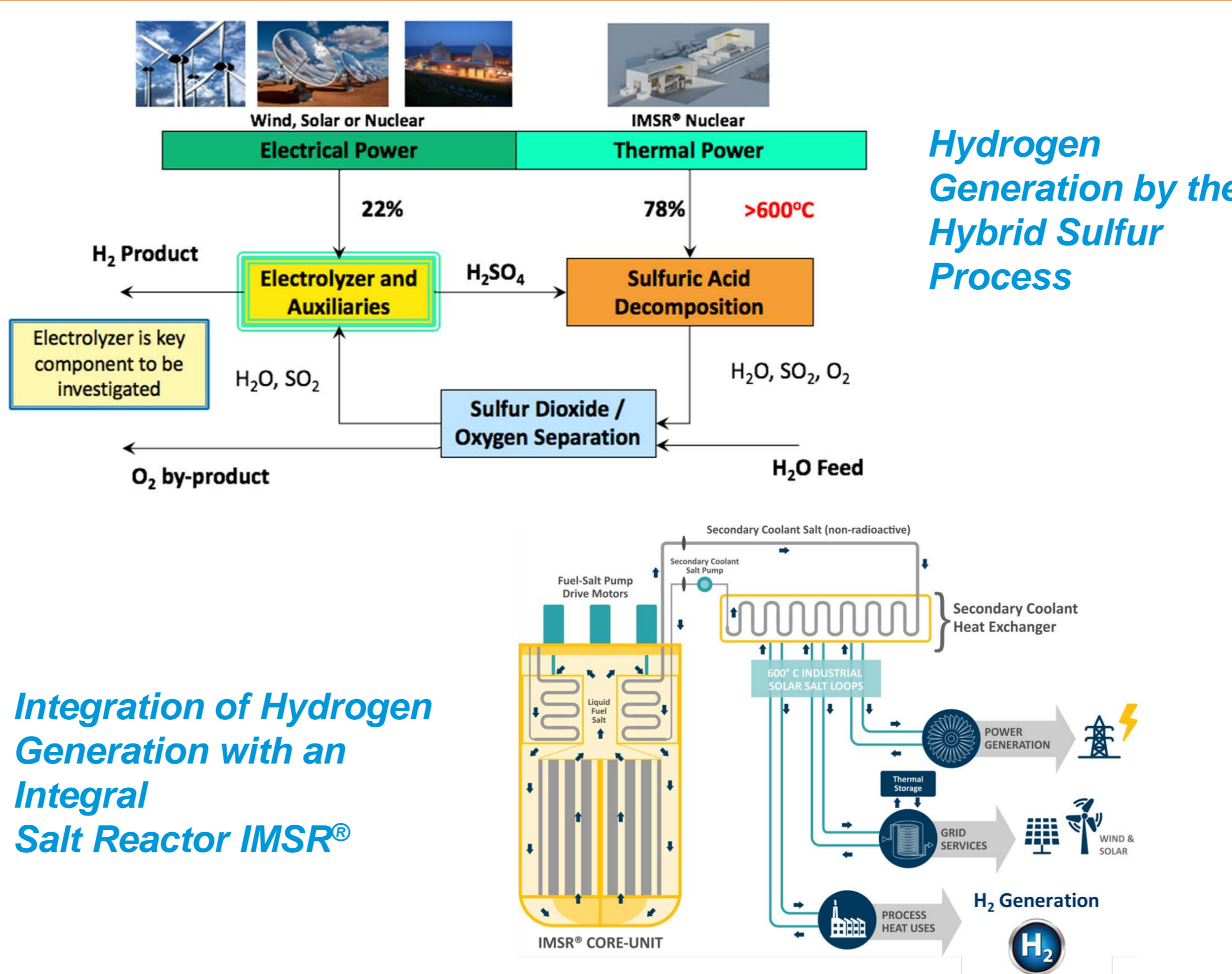
HyS Process



vs. Low Temperature Electrochemical

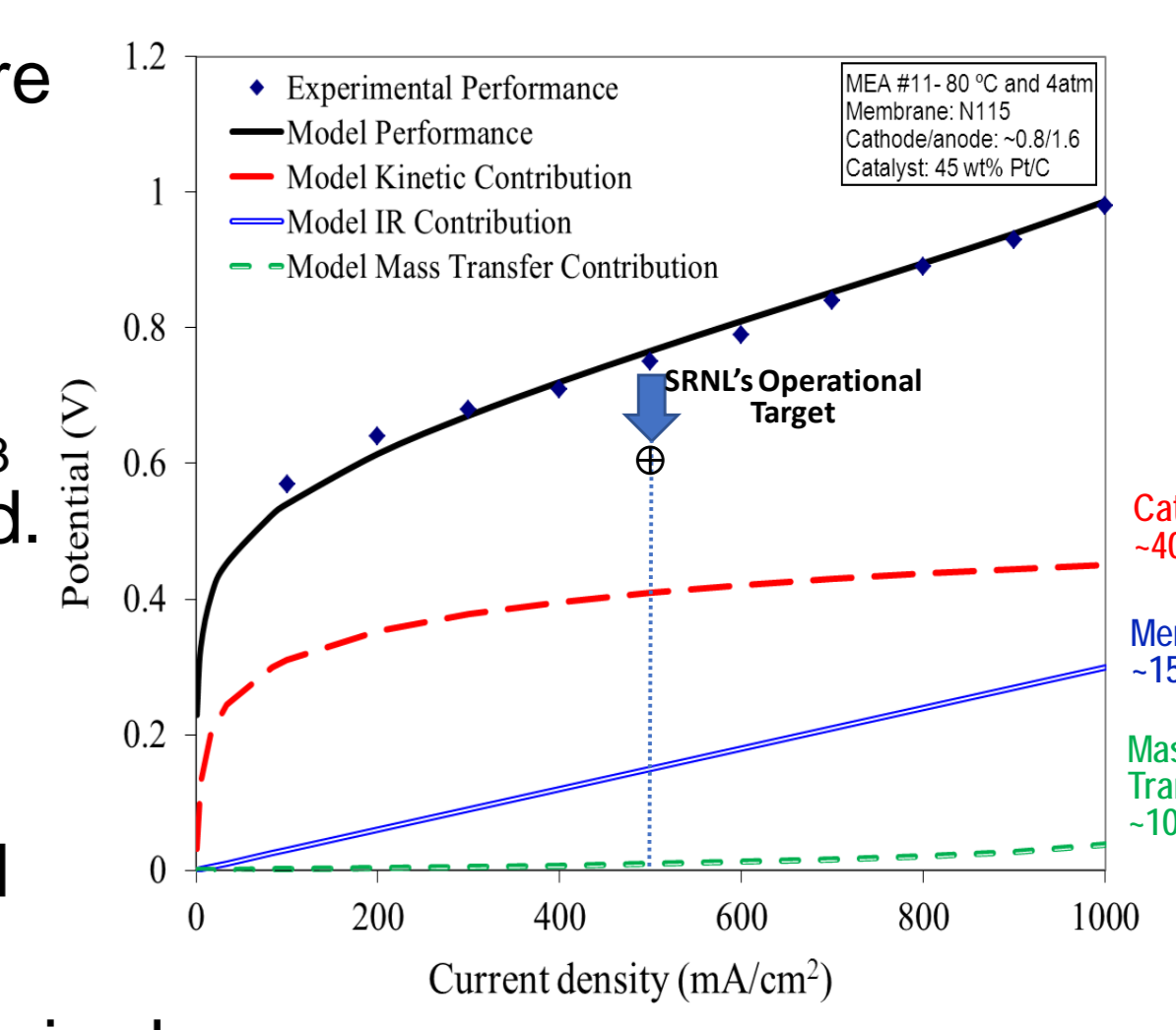


INTEGRATION WITH MOLTEN SALT REACTOR



MEMBRANE ELECTRODE ASSEMBLY (MEA)

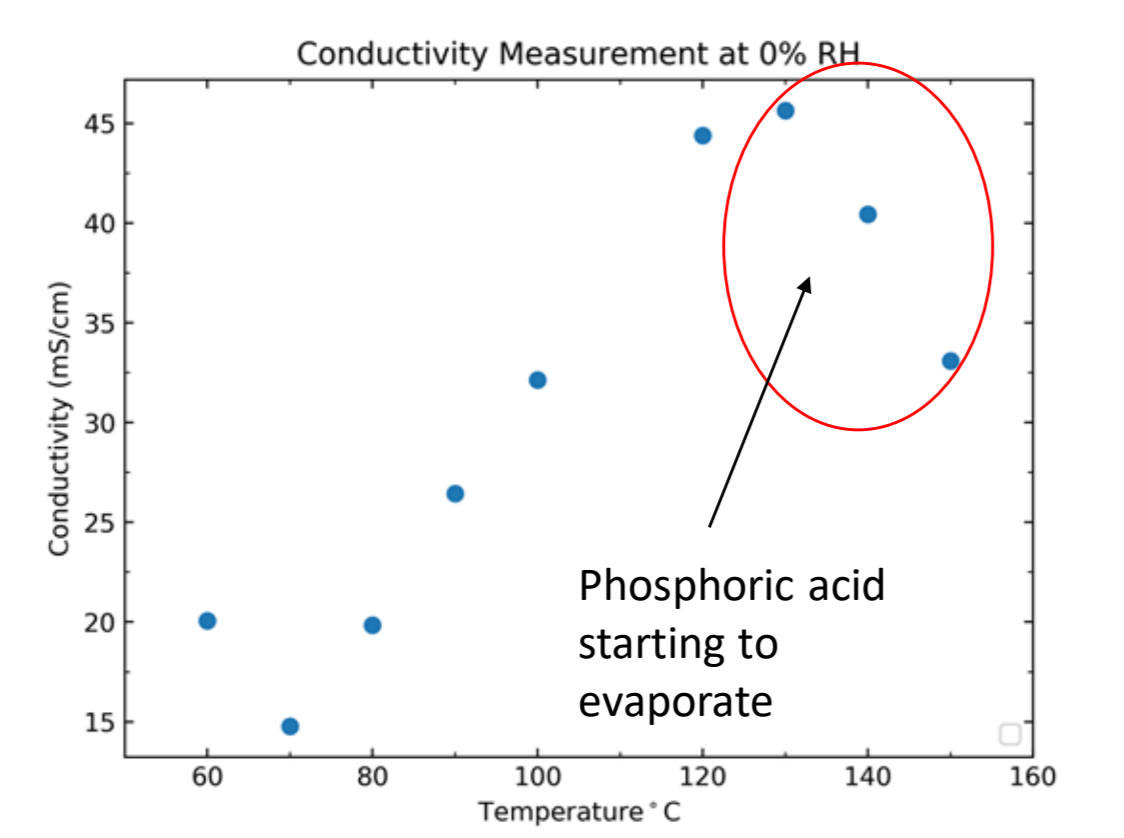
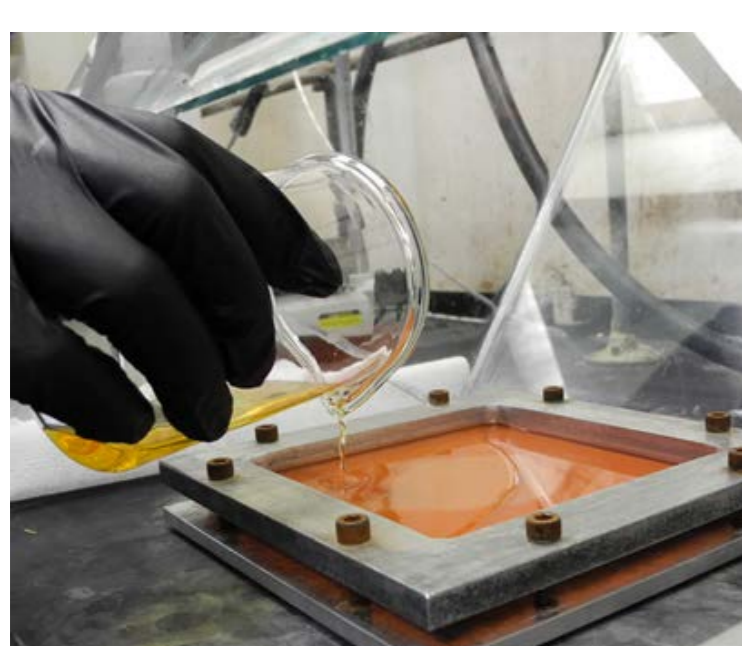
- New high temperature membranes having minimal SO₂ permeability and durability in SO₂/SO₃ environment required.
- New catalysts and supports resulting in 600mV potential at 500mA/cm² required
- Membrane electrode Assembly (MEA) required having >10% degradation in potential after 700 hrs. operation.



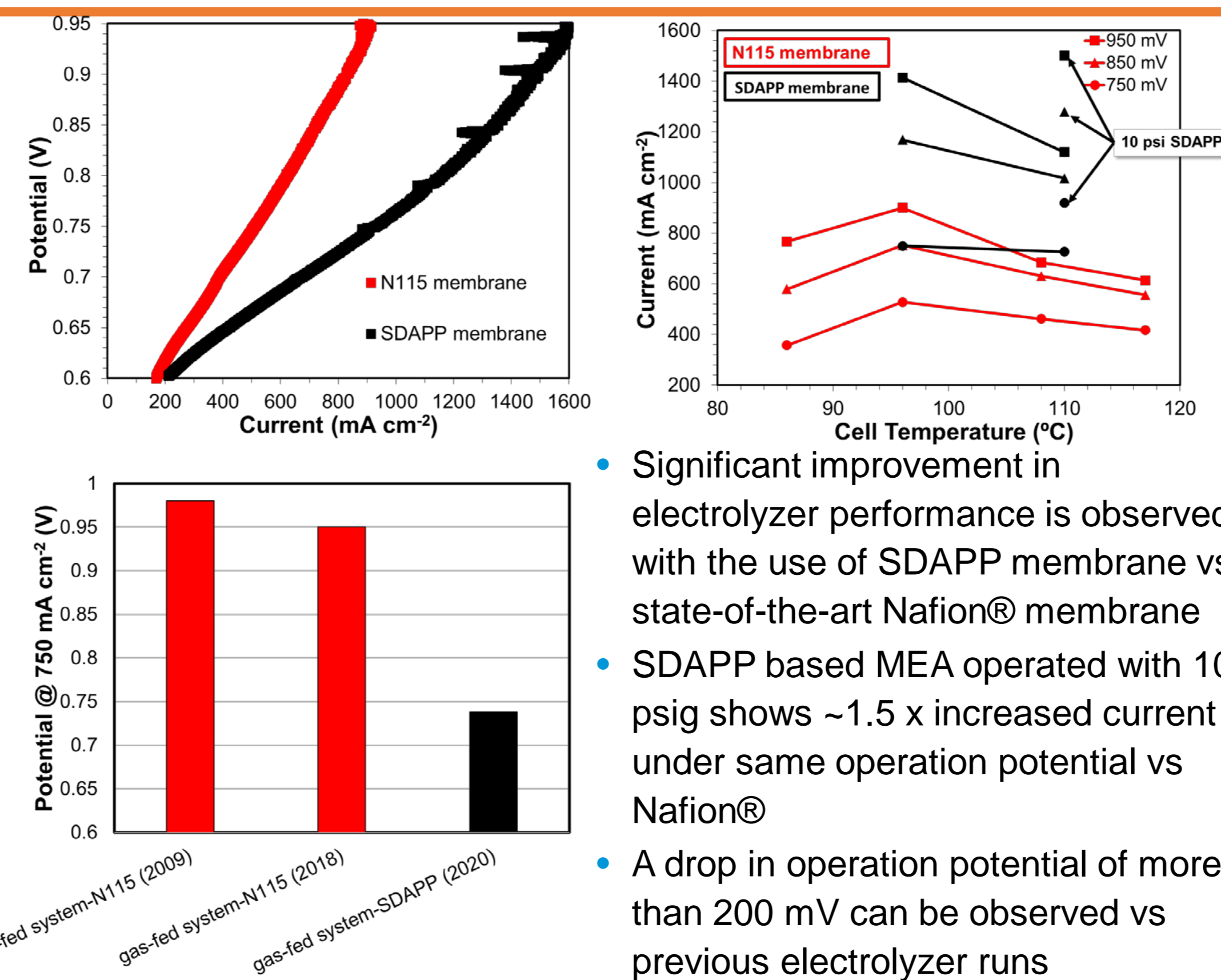
- Kinetics (catalyst)**
 - ↑ Operating temperature
 - ↑ Intrinsic higher activity
- Cell resistance (membrane)**
 - ↑ Operating temperature
 - ↑ ionic conductivity

MEMBRANE DEVELOPMENT

- Improve ionic conductivity and stability at high acid concentrations and temperatures
- Prevent sulfur formation at the cathode
 - Limit or eliminate formation H₂S and SO₂ reactants*
- Utilize membranes with low SO₂ permeability
- Developed SDAPP membranes with alternate acid concentrations to optimize MEA performance

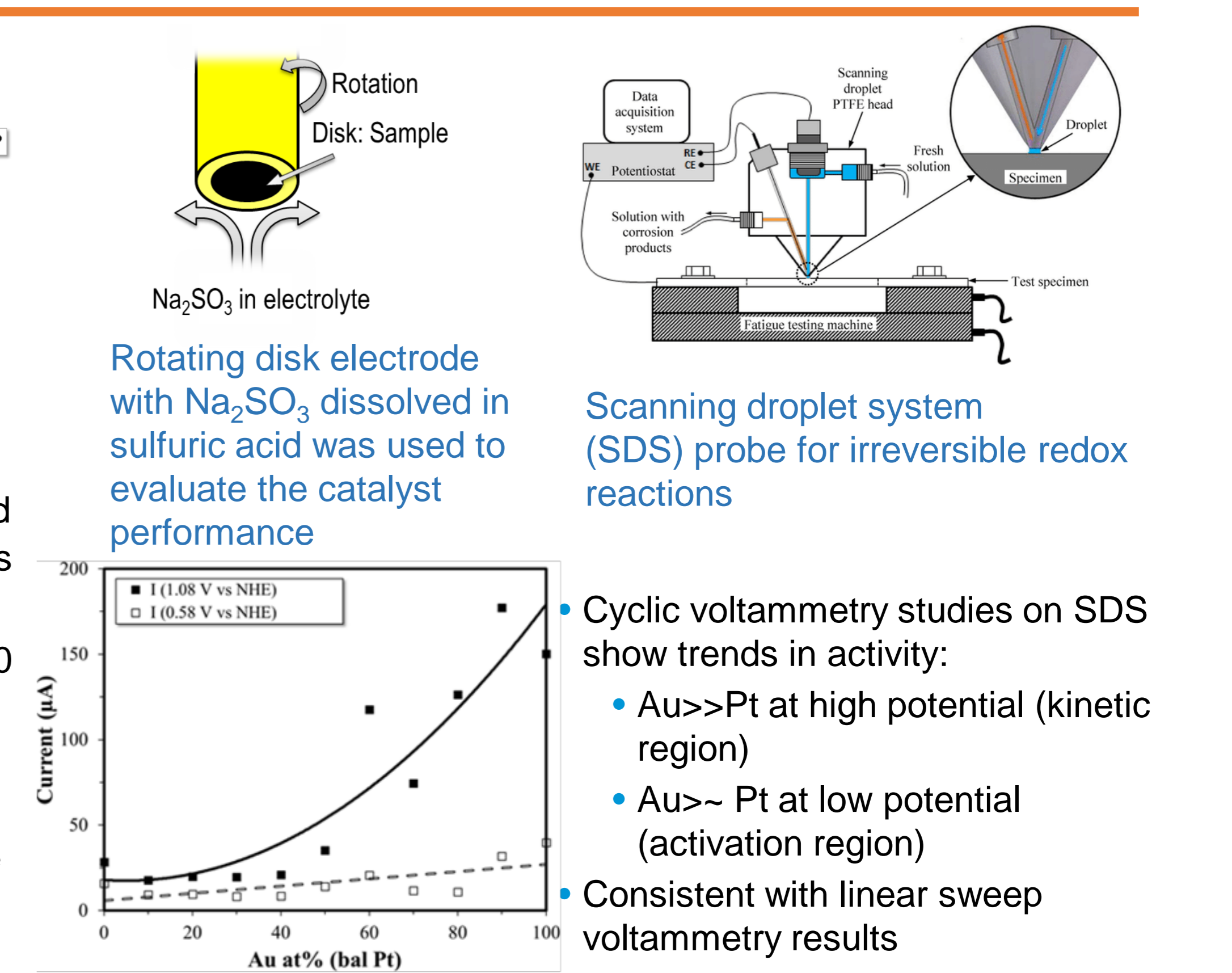


IN-SITU CATALYST TESTING



- Significant improvement in electrolyzer performance is observed with the use of SDAPP membrane vs state-of-the-art Nafion® membrane
- SDAPP based MEA operated with 10 psig shows ~1.5 x increased current under same operation potential vs Nafion®
- A drop in operation potential of more than 200 mV can be observed vs previous electrolyzer runs

EX-SITU CATALYST TESTING



- Rotating disk electrode with Na₂SO₃ dissolved in sulfuric acid was used to evaluate the catalyst performance
- Scanning droplet system (SDS) probe for irreversible redox reactions
- Cyclic voltammetry studies on SDS show trends in activity:
 - Au>>Pt at high potential (kinetic region)
 - Au>~ Pt at low potential (activation region)
- Consistent with linear sweep voltammetry results

TECHNOECONOMIC ANALYSIS

- Given projected performance of IMSR® and HyS process, production cost estimated to be 2.55 \$/kg H₂.
 - 650°C upper limit major hurdle
 - Path to \$1.93\$/kg H₂ identified
 - Requires 25% reduction in heat, power cost
- Conceptual plant design based on s-PBI MEA SDE
 - Being updated for SDAPP MEA
 - Wet cathode for SDAPP MEA alters flowsheet, energy balance
- TEA for H₂ production via MSR-HyS
 - Previous TEA being updated for SDAPP MEA
 - More flexible SDE performance targets

PROPOSED FUTURE WORK

- Evaluate electrolyzer performance at process relevant conditions
- Evaluate electrolyzer performance under pressure
- Incorporate Au based catalyst into catalyst layer
- Explore ternary alloys of PtAuM (M = transition metal) via combinatorial sputter deposition
 - e.g. V used industrially in H₂SO₄ production
- Identify combinations of cell potential, current density, and acid concentration that will achieve specific production cost targets

SUMMARY

- The HyS process could add value to nuclear generation and serve as an energy storage mechanism for concentrating solar
- Thermal energy can be used most effectively through hybrid thermo-chemical/electro-chemical process.
- HyS process utilizes 78% thermal energy and 22% electrical energy with ability to store SO₂ or H₂SO₄ indefinitely as required.
- Electro-chemical step key to efficient SO₂ oxidation
 - Potential high temperature membrane with minimal SO₂ permeation identified as SPP which needs to be optimized for SO₂/SO₃ environment.
 - Potential Pt_xAu_yV_z alloy catalyst identified to greatly reduce required cell potential and needs further investigation.