Durable Fuel Cell MEA through Immobilization of Catalyst Particle and Membrane Chemical Stabilizer

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Project Goal: <u>Develop highly stable catalysts and membrane materials</u> for use in direct-H₂ fed PEM fuel cell MEA in medium-duty (MD) and heavy-duty (HD) truck applications featuring

- Iow cost cathode PGM loading of ≤ 0.2 mg_{Pt}/cm²
- high efficiency fuel efficiency of >65%
- high durability < 10% degradation in power density after 30,000 hours of operation (a lifetime of 1 Million miles, ~3X compared to light-duty (LD) vehicles)



Outcome: if successful, this project will deliver highly durable MEA for PEMFC applications to enable heavy-duty truck applications and elucidate the fundamental degradation mechanisms.

Timeline

- Project start date: 1 Oct 2019
- Project end date: 31 May 2023
- Percent complete: 70%

Budget

- Total Project Budget: \$2.73M
 - Total DOE Share: \$2.0M
 - Total Cost Share: \$0.73M (26.8%)
- Total Funding Spent: \$2.1M*
 - DOE Billable: \$1.5M
 - Participants Cost Share Funds Spent: \$0.6M
 - * As of 03/31/2022 (amount by billings)

Barriers

- A. Durability
 - < 10% power degradation after 30,000 hrs.
- B. Cost
 - $\leq 0.2 \text{ mg}_{Pt}/\text{cm}^2$ cathode Pt metals loading
- C. Efficiency
 - > 65% efficiency to decrease fuel cost

Partners

- General Motors LLC (Project lead)
- Subcontractors:
 - 3M Company (sub)
 - Pajarito Powder LLC (sub)
 - Colorado School of Mines (sub)
 - Cornell University (sub)
- M²FCT Consortium





Relevance/Impact

Targets and Status



 Objective - develop highly stable catalyst and membrane materials to be integrated into an MEA for heavy-duty truck applications that meet or exceed technical targets in terms of <u>cost, performance, durability & efficiency</u>

	Metric Units		DOE/Project Target	Pt/HSC-a	Pajarito Pt/Zr-ECS3701	
VLYST	PGM loading (total)	mg _{PGM} /cm ²	< 0.25	0.25	0.25	
	Mass activity (MA) ^a	A/mg _{PGM}	>0.44	0.68	0.49	
	Loss in initial catalytic activity (post-30k catalyst cycles) $^{ extsf{b}}$	% MA loss	< 40	34%	18%	
	Performance at 0.8 V (150 kPa, 80°C)	A/cm ²	0.3	0.39	0.22	
5	Performance at rated power (250 kPaabs, 94 °C)	W/cm ²	> 1.3	1.3	1.3	
	Loss in performance at 0.8 A/cm ² (post-30k catalyst cycles) ^b	mV	< 30	15	8	
	HD Combined Target (at 0.7 V, post-90k catalyst cycles) ^d	kW/g _{PGM}	2.5	4.0	3.7	

- Cost < 0.25 mg_{total}/cm²
- HD combined durability and efficiency target – achieved ~ 4.0 g/kW at EOT
- membrane chemical durability of 300 to 600 hours with immobilized additives

			Status of Proposed approach				
Metric	Units DOE/Proje		PFSA (no additive)	PFSA w/ 8% CeZrO _x	PFSA blend with HPA		
Membrane thickness	μm	n/a	12	12	25 to 48		
H ₂ crossover	mA/cm ²	< 2	1.1	1	4.6		
H ⁺ area specific resistance	$\Omega \text{ cm}^2$	<0.02	0.02	0.02	0.02		
Electrical resistance	$\Omega \text{ cm}^2$	> 1000	> 3000	9000	6000		
Chemical durability	hours	> 500	< 100	306	671		
Membrane durability	Hours	30000	n/a	n/a	n/a		

Impact: Project is progressing towards delivering and cost-effective and durable MEA for heavy-duty applications

- catalysts with better ECSA retention
- membrane with longer lifetime



Progress

100%

100%

100%

100%

TASK 1: Materials Development – Catalysts and Membranes with Chemical Stabilizers

Go/No-go criteria: Anchored Pt catalyst with >60 m²/g_{Pt} at BOL and >35 m²/g_{Pt} ECSA at EOT (30k LDV AST MEA) \checkmark

- Develop anchored Pt-M/MO_x nanocluster catalysts supported on GMC
- □ PFSA synthesis and HPA functionalization
- Ce_xZr_yO₄ nanofiber dispersed PFSA membrane development
- Fuel cell MEA performance and diagnostics

TASK 2: Integration – Highly Durable Catalysts and Membranes into MEAs

Go/No-go criteria : Anchored Pt catalyst with <30 mV loss at 0.8 A/cm² (60k LDV AST MEA) and membrane that meets all DOE Technical Targets (gas crossovers, ASR, chemical and mechanical durability)

Optimization of down-selected anchored GMC catalyst	80%
ePTFE supported membrane development	80%
Fuel cell MEA performance and durability (AST)	80%
Advanced characterizations of catalysts and membranes	70%

TASK 3: Optimization – Focus on High Performance, Efficiency and Durability

Milestone: Deliver MEA with <0.2 mg_{Pt}/cm² cathode, <40% MA loss in MEA, <10% loss in power after 25000 hours based on fuel cell system modeling lifetime projection studies

- Deliver MEA with state-of-the-art durable catalyst and membranes with high performance, efficiency and durability
- □ Ordered intermetallic PtCo catalyst development on down-selected anchored GMC support
- Optimization for durability of membranes with chemical stabilizers
- □ MEA degradation mechanisms analysis; MEA durability modeling and projections to life



Collaborations and Coordination



- > All the partners are within of the DOE Hydrogen and Fuel Cells Program
- There is extensive collaboration between the funded partners who are experts in their fields of research and all of them play a critical role in achieving the project objectives

<u>Catalyst durability - mitigate Pt surface area loss:</u>

Approach 1: Pt-Carbon interface modification (anchored Pt/C catalysts)

- a. Zr/ZrO_x additives to stabilize Pt against surface area loss
- Approach 2: Pt-ionomer interface modification (advanced polymer additives)
 - a. Hyflon® and Fluorolink® additives to stabilize Pt/C catalyst layer

Membrane durability – mitigate Ce³⁺ migration:

Approach 3: Covalent tethering of heteropoly acid (HPA) anti-oxidant

a. Silicotungstic acid as an immobilized radical scavenger for membrane durability

Approach 4: Dispersed $CeZrO_x$ (CZO) nanofibers for membrane stabilization

a. Demonstration of improved chemical durability with CZO additive

<u>Outcome</u>: Durable fuel cell MEA for heavy-duty application consisting of catalyst with improved resistance towards surface area loss and/or Co-dissolution, and membranes that meet 30,000 hours of lifetime requirement.







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Engineered carbon support (ECS) – synthesis and key features



Pajarito's Varipore[™] manufacturing platform used to develop catalysts with three focal points:

- Mesoporosity (~8 & ~40 nm) for Pt dispersion, accessibility & transport
- Graphitization (300 to 800 m²/g) for carbon stability
- Metal dopants (ex: zirconium) for Pt stability



Zr dopant added in two discrete stages:

- 1) added to the organic carbon precursor (~0.5 wt.%)
- 2) added after carbon synthesis (~2.5 wt.%)

Features of the Engineered Carbon Support (ECS)

Interconnected, built-in, open mesopores with better Pt accessibility & durability





Characterization of Zr-doped Engineered Carbon Support

• Zr is likely dispersed as a mix of ZrC and ZrO₂ nanoclusters on the carbon support

30% Pt / 3% Zr doped-ECS3701 (fresh coating)

Zr K-edge XANES profiles 1.6 1.4 30 1.2 1.0 0.8 0.8 0.6 0.4 0.2 0.0 17960 17980 18000 18020 18040 18060 18080 18100 18120 energy (eV)



- XAS indicates primarily ZrO₂ feature
- XPS suggests the presence of ZrC (possibly on the surface)
- STEM-EDS dispersion of Pt nanoparticles along with ZrO₂



Pt distribution





MEA durability of 30% Pt/Zr-doped ECS3701 catalyst

• Durability of 30% Pt dispersed on 3% Zr-doped carbon has been evaluated in MEA up to 90k cycles



Membrane: 12 μm PFSA, anode: 0.05 $mg_{\textrm{Pt}}/cm^2$

- Pt/ZrO_x-doped carbon shows 25% improvement in ECSA after extended V-cycles
 - enables ~40 mV higher cell voltage after 90k voltage cycles





Catalyst AST protocol

Trapezoidal waveform (H₂/N₂) 0.60 to 0.95 V, **90k cycles 90 °C**, 4s/cycle, 100% RH





Characterization of degraded Zr-doped ECS3701 catalyst

• Catalysts characterized via STEM imaging and SAXS to understand particle size growth







- Pt nanoparticles appear elongated and coarsened after 30k cycles but with a lower average particle size for the Zr-doped catalyst
 - agrees with the higher ECSA for Zr-doped catalyst at EOT
- Detailed STEM-EDS analysis of the cycled catalyst is ongoing





Technical Barrier: i) Pt surface area loss via dissolution-redeposition, and ii) dissolution of cobalt-alloying element

Approach: Pt-ionomer/water interface modification





- Presence of H₂O at the Pt/ionomer interface is critical for ORR kinetics & reactant transport but is also a precursor in de-stabilizing the Pt surface via the Ostwald ripening mechanism (Pt oxidation/dissolution kinetics, Pt^{z+} migration and re-deposition)
- > Catalyst layer becomes more hydrophilic as it ages during voltage (load) cycles
- > Also, need to stabilize Pt interface with ionomer/water against hydrophobicity changes
- > This approach to evaluate the use of fluorinated polymers that need only low temperature sintering, if any

- Identified a new amorphous perfluoro-polymer with a cyclic structure for modification of the catalyst layer
 - Hyflon® high thermal stability, hydrophobicity and chemical resistance with very low surface energy
- Added to the catalyst layer either as a topcoat, requires a thermal sintering step at 100 °C



- Improvement in Pt surface area (~23%) and mass activity retention (<8% loss) at EOT (30k cycles) with Hyflon® additive
- Cell voltage loss after durability cycling is lower with Hyflon® additive compared to Baseline electrode
 - higher HFR with Hyflon® limits the beginning of life cell voltage

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- Identified a new fluorinated perfluoropolyether (PFPE) material for modification of the catalyst layer
- Added to the catalyst layer either as a topcoat or as an additive in the ink formulation stage
- Requires a thermal sintering step at 80 °C, compatible with existing electrode fabrication procedures





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- PFPE enables improvement in cell voltage at EOT, specifically at high current densities
 - No notable durability differences in kinetic activity and ECSA parameters
- PFPE likely stabilizes the catalyst layer against hydrophobicity changes that occurs during load cycling
 - Minimal differences at dry operating conditions (data not shown)



- Use of silicotungstic acid as a representative heteropoly acid (HPA) additive with radical scavenging properties
- Developed synthesis chemistry to covalently bind silicotungstic acid to the PFSA membrane backbone



- Vinylidene fluoride (VDF) monomer (-CF₂-CH₂-) acts as an anchor point to covalently tether anti-oxidant to PFSA backbone
- Vary VDF monomer ratio to optimize performance and durability



Successfully fabricated 25-80 µm thick membranes composed of HPA modified PFSA blended with conventional 3M PFSA



- Minor loss in conductivity for the blended membrane
- Conductivity improvement expected with better HPA dispersion
- Negligible difference in
 H₂/air polarization behavior

Technical Accomplishment (approach 3: membrane durability – immobilization of HPA antioxidant Characterization of HPA immobilized blended PFSA membrane

- Blended PFSA membrane with 10% HPA immobilized component was characterized using TEM imaging and SAXS
 - to understand HPA dispersion and covalent attachment to the backbone

Cross-sectional TEM images of HPA immobilized membrane



Bottom – substrate or liner side

- TEM cross-section shows HPA dispersed as fine nm sized additives (blue arrows)
- Further, HPA is also observed as
 - 100 to 200 nm sized agglomerates that are either dispersed (red arrows)
 - or dense deposit near the substrate or liner-side of the membrane (green arrows)

SAXS profile as a function of RH



- SAXS corroborates successful covalent binding of HPA to anchoring group and morphological ordering induced by HPA
- Peak at 0.6 Å⁻¹ (d-spacing of 1.0 nm)
 - water molecules favor HPA moieties
 - Enlarge d-spacing between HPAs





- HPA immobilized membranes were subjected to OCV durability testing in MEAs at both GM and 3M laboratories
- Representative results are shown based on OCV testing at 3M

OCV Testing, unsupported membranes (90 °C, 38% RH)



 $H_2/air,$ 90 °C, 38% RH, 696 sccm H_2 , 1650 sccm air Anode – 0.1 $mg_{\text{Pt}}/\text{cm}^2$ Cathode – 0.3 $mg_{\text{Pt}}/\text{cm}^2$

		OCV Lifetir	ne (hrs)	Average Fluoride release rate (µg/cm²/day)			
Membrane	Samples	Mean Stdev		Mean	Stdev		
HPA-PFSA	8	671 (running)	193	3.9	0.8		
3M Baseline	4	242	112	7.4	1.8		

- OCV durability shows decreased voltage loss, and improved chemical durability (reduced FRR)
- Longer lifetimes achieved relative to unsupported, additive-free 3M PFSA; tests ongoing.



 $CZO - CeZrO_x, CN - Ce(NO_3)_3$

mol % - w.r.t. total MEA SO₃H content

- CZO nanofiber additives dispersion in ionomer solutions have been studied by beads milling with objective of obtaining homogenous coating solution. CZO particle size distribution was measured using HORIBA Laser Particle Size Analyzer, as a function of milling beads size, milling speed, additive concentrations.
- Homogeneous solution obtained and uniform additive distribution obtained within membrane.
- Fuel cell performance tests show similar performance of membrane with CZO additive to non-additive membrane.
- Preliminary data from LBNL shows membrane with CZO additive has higher water uptake than no-additive membrane.

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- Homogeneous membranes, and ePTFE reinforced membranes w/ and w/o CZO additives were fabricated and tested for performance and OCV chemical durability
- OCV durability of membranes with CZO show decreased OCV voltage loss, and improved chemical durability (reduced FRR)
- 500 hrs. OCV tests are scheduled for ePTFE reinforced membranes with CZO additives.
- Post OCV tests, ex situ analyses such as XRF and SEM cross-sections will be conducted on the MEA samples.



Reinforced membranes – 12 μm

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- End of test analysis was conducted at ORNL on membrane with CZO additive after fuel cell performance and 200 hrs OCV durability tests.
- CZO nanofibers/particles still observable after fuel cell chemical degradation tests.
- EDX analysis confirmed the chemical component by detecting Ce and Zr elements in the particles.
- CZO also can be potentially used for gradually releasing Ce cation.







Continued material optimization & post-mortem



	Item	Remaining challenges	Proposed future work
Focus of Phase 3	MEA Integration	 identify concepts/approaches to integrate durability evaluation of the integrated MEA and lifetime projection studies 	 evaluate combination of the two catalyst approaches (June 2022) perform a combinatorial study of the two catalyst approaches with membrane concepts (July – August 2022) perform catalyst AST and combined chemical/mechanical stress tests on the integrated MEA, durability modeling for lifetime projection
	Zr-doped catalyst	 investigate the role of the Zr dopant 	• characterize Zr doped ECS3701 material using STEM-EDS, XPS, XAS, in situ ICP, in situ carbon corrosion
analysis	Polymer additives	 evaluate mechanism of improvement 	 perform electrochemical diagnostics of ionomer adsorption, transport resistances & spectroscopic analysis of the polymer
	HPA tethered PFSA	 improve HPA dispersion, mechanical integrity and morphological properties of the membrane 	 fabricate e-PTFE reinforced to blended HPA-PFSA membrane XRF imaging of W to understand HPA migration, if any.
	CZO dispersed PFSA	 understand Ce redistribution from CZO 	• XRF imaging of Ce to understand CZO dissolution/migration, if any.

Any proposed future work is subject to change based on funding levels.

Summary



- □ Promising new materials for both cathode catalyst and membrane durability
 - Zr-doped Engineered Carbon Support enables improvement in ECSA at EOT (post-90k V cycles)
 - > Perfluoropolyether and Hyflon® additives improve cathode catalyst layer durability
 - > HPA immobilized membranes enables ~400 to 800 hours of OCV durability with improved chemical stability
 - > CZO nanofiber additive enables improved chemical durability based on OCV durability testing
- □ M²FCT consortium has been engaged for materials characterizations (ANL SAXS/XAS) & imaging (ORNL TEM)
- □ Future studies will focus on
 - integration of stabilized catalysts and membranes to deliver highly durable MEA
 - execute durability tests of membranes subjected to combined chemical and mechanical stresses and the mapping of scavenger migration (in collaboration with M2FCT)
 - > post-mortem analysis to understand the material structure-property relationships

so far: 50 different catalysts, 8 different polymer additives, 2 different membrane stabilizers, 5 conference presentations, 2 publications, 2 patent applications, 2 invited talks

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Technical Back-Up and Additional Information

Technology Transfer Activities

Patent/Invention Submission

- 1. "Advanced Ionomers Based on Covalently Bound Hetero Poly Acids" Michael Yandrasits, Matthew Lindell, Arne Thaler, Andrew Herring, ChulOong Kim, Mei-Chun Kuo, Craig Gittleman, *filed January 2021* (Joint invention submission with inventors from GM, 3M, and Colorado School of Mines was filed in January of 2021 with all three partners. Independent council has been identified to draft the patent application. Provisional patent application filing will be completed before June 7th.)
- 2. "Fuel Cell Cathode and Fuel Cell System Including a Polymeric Additive", Nagappan Ramaswamy, Roland Koestner, Swami Kumaraguru, filed on January 11, 2022.

Publications and Presentations

Publications

1. "High-Current Density Durability of Pt/C and PtCo/C Catalysts at Similar Particle Sizes in PEMFCs" Nagappan Ramaswamy, Swami Kumaraguru, Wenbin Gu, Ratandeep Singh Kukreja, Kang Yu, Daniel Groom and Paulo Ferreira, *J. Electrochem. Soc.* (2021) 168 (2) 024519.

Electrochemical diagnostics of Zr-doped ECS3701 catalyst

• Durability of 30% Pt dispersed on 3% Zr-doped carbon has been evaluated in MEA up to 90k cycles



<u>Catalyst AST protocol</u> Trapezoidal waveform (H₂/N₂) 0.60 to 0.95 V, **90k cycles 90 °C**, 4s/cycle, 100% RH



Membrane: 12 μ m PFSA, anode: 0.05 mg_{Pt}/cm²

- Is direct Pt-ZrO_x interaction responsible for improvement in surface area retention and cell voltages?
 - since Zr is doped into the organic carbon precursor, the possibility of better ECSA retention due to the modified carbon micro/meso-structure remains open
 - double-layer capacitance of Zr-doped ECS is reasonably higher than the non-doped carbon

Synthesis of ionomer with anchored heteropoly acid (HPA)

Accomplishments:

- Developed synthesis chemistry successfully to covalently bind HPA to the PFSA membrane backbone
 - Attach phosphate ester linking group before hydrolysis of SO₂F group but prior to the attachment of HPA anti-oxidant
 - Mild hydrolysis conditions developed to convert SO_2F to SO_3X



Blended Membrane

Successfully fabricated 40-80 μ m thick membranes composed of HPA modified PFSA blended with conventional 3M PFSA $_2$



VDF Precursor Polymer Synthesis and Hydrolysis

Scheme for synthesis of PFSA ionomer with covalently tethered heteropoly acid radical scavenger additive



- VDF link anchor point to tether HPA
- Two pathways
 - Functionalize in the $(\sim SO_2F)$ form 1)
 - Hydrolyze and acidify SO_2 to SO_3H 2) followed by functionalization
- Optimize VDF/HPA content ratio

Hydrolysis Experiments – Harsh vs. mild hydrolysis conditions



Harsh hydrolysis (NaOH) conditions lead to dehydrofluorination and formation of double bond in backbone (undesirable)



Mild hydrolysis $((NH_4)_2CO_3)$ shows no de-hydrofluorination Disappearance of SO₂F at 1460 cm⁻¹ demonstrates successful hydrolysis (desirable)

VDF Precursor Polymers Synthesized to Date

		VDF	EW*
lonomer	Synthesized	(mol%)	(g/mol)
Exp. Polymer -1	Nov '19	18	903
Exp. Polymer -2	Feb. '21	5	810
Exp. Polymer -3	Feb. '21	11	791
Exp. Polymer -4	Feb. '21	17	795
Exp. Polymer -5	Feb. '21	23	784
* Based on solid state NM	R		

Accomplishments:

- Five precursor polymers with VDF anchor points synthesized
- Mild hydrolysis conditions identified
- Preliminary success in dispersing VDF polymer (no HPA) in alcohol/water solution which is also desirable for membrane production

- The BOL membrane sample has non-uniform Tungsten (W) distribution
 - will be improved by better synthesis process control in the next iteration
 - could be improved with better membrane casting conditions as well
 - improved W distribution may lead to improved durability
- Cross section analysis is on going







Technical Accomplishment (Membrane Durability) CZO electrode additives – OCV durability and H₂/air performance

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- CZO nanofiber additives have been successfully incorporated into cathode at various loadings (4 to 16 mole % CZO)
- OCV durability shows improved chemical durability (reduced FRR)
- H₂/air iV curves show comparable MEA performance at low CZO levels (≤ 8 mol %). Minor Performance penalty observed at higher CZO loadings.
- XRF: EOT XRF shows Ce redistribution after performance and OCV durability tests. CZO additives still observed in electrode layers after tests.



Next steps: Evaluate CZO additives incorporated directly into the membrane





Reviewer-Only Slides

Assumptions and Risks

Technical assumptions:

- The project has 5 main approaches to address the technical barriers 2 approaches to immobilize chemical stabilizer in the membrane and 3 approaches to mitigate catalyst dissolution and surface area loss. All of these have shown promising results at TRL 3-4.
 - □ Pt migration/coalescence is the dominant mechanism of surface area loss.
 - □ M/MO_x additives anchor catalyst nanoparticles on the support and that they do not have any negative impacts by itself
 - □ HD truck operating conditions and drive cycle profiles are not overly restrictive than LD vehicles
 - □ CZO is stable and active for peroxide radical decomposition
 - While HPAs have been tethered to fluoroelastomer in the past, we assume that it can be tethered to the PFSA backbone. HPA remains stable and active when anchored to the PFSA backbone.

Execution risks:

- □ M²FCT resources (support & timing) are critical to accomplishing project objectives as laid out.
- Delays in receiving the DOE award contract, internal approvals, etc. were experienced but are complete now
 - □ Conditional award received on Oct. 1, 2019 which was lifted on Feb. 27. 2020.
 - □ The Subrecipient Agreements have been finalized and approved.
 - □ Approvals for NDA to work with M²FCT consortium are complete.
- Due to the ongoing pandemic situation caused by the outbreak of Covid-19 virus, we are experiencing significant delays in experimental work with minimal or no access to the lab since mid-March 2020. Major delays were experience, particularly in 2020 Q2. Since the end of June 2020, better on-demand access to the laboratory facilities were available that helped significantly ramp up activities to accomplish the Tasks and Milestones.

Proposed Future Work

M²FCT engagement and timeline

M²FCT consortium laboratories will be engaged for achieving the overall goals of the project (electrochemical diagnostics, x-ray characterizations, analytical measurements, post-mortem experiments, fuel cell system modeling studies)

M2FCT Engagement Timeline				Year 1		L	Year 2		2	Year 3			
ТАЅК	FCPAD Lab	Sample Type	Q4	Q1 0	2 Q3	Q4	Q1 (2 Q	3 Q4	Q1	Q2 (Q3 Q4	4
Year 1 - 2020													
Light scattering and viscosity (CZO - PFSA dispersions)	LBNL	Ionomer dispersions											
SAXS and XCT characterizations	ANL	Electrodes											
Ex situ membrane characterizations	LBNL	Membranes											
Imaging of stabilizing additives in membranes	ORNL	Membranes											
Fuel cell MEA diagnostics (cathode and membrane)	NREL	MEAs											
Year 2 - 2021													
MEA electrochemical diagnostics	NREL	MEAs											
Cathode carbon corrosion (<i>in situ</i> NDIR)	LANL	MEAs											
X-ray absorption spectroscopy (XAS) of catalysts	ANL	Electrodes											
Electrochemical ICPMS for PtCo catalyst durability	ANL	Catalysts											
Imaging of stabilizing additives in membranes	ORNL	Membranes											
Year 3 - 2022													
MEA voltage cycling sensitivity measurements	NREL	MEAs											
MEA post-mortem analysis	All/FC-PAD	MEAs											
MEA Durability Modeling and Life-Projections	ANL	n/a											

Milestone Summary Table									
	Recipient Name: Project Title:	ח	urable Fuel Ce	General Motors LLC	d Membrane Ch	emical Stabili	7er		
Task Number	Task Title	Milestone Type (Milestone or Go/No- Go Decision Point)	Milestone Number* (Go/No-Go Decision Point Number)	Milestone Description (Go/No-Go Decision Criteria)	Milestone Verification Process (What, How, Who, Where)	Anticipated Quarter (Quarters from Start of the Project)	Progress		
1.2.1	Catalyst characterizations	Milestone	M1.1	Establish baseline catalysts and ex situ surface area measurement protocols	GM/Pajarito/C	Q1	80%		
1.1.1	Develop Pt-MOx nanocluster catalysts supported on GMC	Milestone	M1.2	Provide >5g of first iteration of Pt-MOx/GMC catalyst to GM	Pajarito/GM	Q2	80%		
1.1.5	Prepare and characterize CexZryO4 nanoparticle/PFSA dispersions	Milestone	M1.3	Prepare CexZryO4 nanofiber or nanoparticle /PFSA dispersions with at least 3 different CexZryO4 loading levels	GM/FC-PAD	Q3	80%		
1.1.3	Polymer Synthesis	Milestone	M1.4	Copolymers with 3 different levels of tetherable monomer delivered for functionalizing with HPA	3M	Q4	80%		
Phase 1	Development of Catalysts and Membranes with Chemical Stabilizers	Go/No-go	MA1	Anchored supported Pt catalyst with > 60 m ² /g _{Pt} ECSA at BOL in MEA and > 35 m ² /g _{Pt} ECSA after 30,000 cycles of DOE LDV catalyst AST.	^{Брт} r All Q4		Completed, GO		
2.2.1	MEA performance, electrochemical diagnostics and modeling	Milestone	M2.1	Validate anchored Pt/GMC catalysts in MEAs (BOL ECSA >60 m ² /g)	GM/FC-PAD	Q5	50%		
2.2.2	AST for anchored Pt/GMC catalyst durability	Milestone	M2.2	Demonstrate durability enhancements with anchored Pt/GMC catalysts (<30% ECSA loss after 30000 cycles)	GM	Q6	60%		
2.1.2	Prepare ePTFE supported membranes with chemical stabilizers	Milestone	M2.3	HPA immobilized membranes that enable 200 hours of OCV at 90°c/30% RH	GM/CSM/3M	Q7	40%		
2.2.3 2.2.4	 Quantify anchored GMC support corrosion in MEA using in situ NDIR X-ray absorption spectroscopy of MOx anchoring site durability 	Milestone	M2.4	Report on the mitigation of carbon corrosion with GMC and the stability of MOx anchoring sites	FC-PAD	Q8	10%		
Phase 2	Integration of Highly Durable Catalysts and Membranes into MEAs	Go/No-go	MA2	 Anchored supported Pt catalyst with < 30 mV loss at 0.8 A/cm² after 60,000 cycles of DOE LDV catalyst AST protocol. Membrane with H₂ & O crossovers (<2mA/cm²), 80°C proton ASR (<0.02 ohm cm2), electrical resistance (<1000 ohm cm2), chemical durability (>500h in AST), mechanical durability (>20,000 cycles in AST) 	All	Q8	Completed, GO		
3.1.3	Catalyst, support and membrane AST on SOA MEA	Milestone	M3.1	Anchored Pt/GMC catalyst with <30% ECSA loss after catalyst AST.	GM	Q9			
3.1.1	Develop ordered intermetallic PtCo catalysts on down-selected support	Milestone	M3.2	Deliver >2g of ordered catalyst with mass activity >0.44 A/mg _{Pt} .	Pajarito/GM/C ornell	Q10			
3.1.3 3.2.1	Catalyst, support and membrane AST on SOA MEA MEA post-mortem analysis	Milestone	M3.3	 MEA that achieves 1750h of 90 °C HAST testing Report on the Pt nanoparticle location before and after AST 	AII/FC-PAD	Q11			
3.3.1 3.3.2	 MEA durability modeling and life-projections Deliver Final MEA with High Efficiency and Durability to DOE 	Milestone	M3.4	 Report on the MEA life projections using durability models Deliver six or more 50 cm2 MEAs to DOE 	GM/FC-PAD	Q12			
Phase 3	Optimization for High Performance, Efficiency and Durability	Final Review	MA3	Deliver MEA with < 0.2 mg _{Pt} /cm ² _{cathode} , < 40% loss in mass activity, < 10% loss in power after 25000 hours based on fuel cell system model lifetime projection studies. The MEA will have BOL efficiency of 65% at 10% power and a rated power of >1.2 W/cm ² measured in a 50 cm ² active area cell.	All	Q12			